# BISON Theory Manual The Equations Behind Nuclear Fuel Analysis

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October 2013



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# **BISON Theory Manual**

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# **Contents**

1	Intro	oduction	4
2	Gove	erning Equations	5
3	Elen	nent Kinematics	6
4	Axis	symmetric Equations	7
5	Sphe	erically Symmetric Equations	8
6	Elas	ticity	9
7	Nonl	linear Materials	10
8	Fuel	Material and Behavioral Models	12
	8.1	Thermal Properties	12
		8.1.1 UO <sub>2</sub> thermal conductivity	12
		8.1.2 MOX thermal conductivity	18
	8.2	Fission Product Swelling	22
	8.3	Densification	23
	8.4	Relocation	23
	8.5	Thermal and Irradiation Creep	24
		8.5.1 UO <sub>2</sub> model	24
		8.5.2 MOX model	25
	8.6	Smeared Cracking	27
	8.7	Grain Growth	28
	8.8	Fission Gas Behavior	29
		8.8.1 Simple Physics-Based Model	29
		8.8.2 Modified Forsberg-Massih Fission Gas Release Model	33
9	Clad	l Material and Behavioral Models	36
	9.1	Irradiation Creep	36
	9.2	Thermal Creep	36
		9.2.1 Hayes Secondary Creep	36
		9.2.2 Limbäck Primary and Secondary Creep	37
	9.3	Combined Creep and Instantaneous Plasticity	37
	9.4	Irradiation Growth	38
	9.5	Damage	38

10	Other Material Models	39
	10.1 Pyrolitic Carbon	39
	10.2 SiC Irradiation Creep	39
	10.3 HT9 Thermal Properties	40
	10.4 HT9 Mechanical Properties	40
	10.5 HT9 Thermal and Irradiation Creep	40
	10.6 Mass Diffusion Coefficients	41
	10.7 U <sub>3</sub> Si <sub>2</sub> Thermal Properties	41
11	Power, Burnup, and Related Models	42
	11.1 Power	42
	11.1.1 Radial Power Profile	42
	11.2 Decay Heat	44
	11.3 Burnup Calculation	46
	11.4 Fission Rate	46
	11.5 Fast Neutron Flux	46
	11.6 Fast Neutron Fluence	47
12	2 Evolving Density	48
13	B Gap/Plenum Models	49
	13.1 Gap Heat Transfer	49
	13.2 Mechanical Contact	50
	13.3 Gap/plenum pressure	51
	13.4 Gap/plenum temperature	51
14	Coolant Channel Model	53
	14.1 Coolant enthalpy rise in a single channel	53
	14.2 Heat transfer correlations	54
	14.2.1 Critical heat flux correlations	56
	14.2.2 Criteria to select heat transfer correlations	58
	14.3 Properties for water and steam	58
15	Cladding Corrosion Model	60
	15.1 Zirconium Alloy	60
	15.1.1 Introduction	60
	15.1.2 EPRI SLI Model	61
	15.1.3 Zirconium Oxide Thermal Conductivity	62
	15.1.4 Numerical Method	63
	15.2 Aluminum	64
	Bibliography	65

## 1 Introduction

BISON [1] is a finite element-based nuclear fuel performance code applicable to a variety of fuel forms including light water reactor fuel rods, TRISO particle fuel [2], and metallic rod [3] and plate fuel. It solves the fully-coupled equations of thermomechanics and species diffusion, for either 1D spherical, 2D axisymmetric or 3D geometries. Fuel models are included to describe temperature and burnup dependent thermal properties, fission product swelling, densification, thermal and irradiation creep, fracture, and fission gas production and release. Plasticity, irradiation growth, and thermal and irradiation creep models are implemented for clad materials. Models are also available to simulate gap heat transfer, mechanical contact, and the evolution of the gap/plenum pressure with plenum volume, gas temperature, and fission gas addition. BISON is based on the MOOSE framework [4] and can therefore efficiently solve problems using standard workstations or very large high-performance computers.

This document describes the theoretical and numerical foundations of BISON.

# 2 Governing Equations

The BISON governing relations consist of fully-coupled partial differential equations for energy, species, and momentum conservation. The energy balance is given in terms of the heat conduction equation

$$\rho C_p \frac{\partial T}{\partial t} + \nabla \cdot \mathbf{q} - e_f \dot{F} = 0, \tag{2.1}$$

where T,  $\rho$  and  $C_p$  are the temperature, density and specific heat, respectively,  $e_f$  is the energy released in a single fission event, and  $\dot{F}$  is the volumetric fission rate.  $\dot{F}$  can be prescribed as a function of time and space, or input from a separate neutronics calculation. The heat flux is given as

$$\mathbf{q} = -k\nabla T,\tag{2.2}$$

where k denotes the thermal conductivity of the material.

Species conservation is given by

$$\frac{\partial C}{\partial t} + \nabla \cdot \mathbf{J} + \lambda C - S = 0, \tag{2.3}$$

where C,  $\lambda$ , and S are the concentration, radioactive decay constant, and source rate of a given species, respectively. The mass flux J is specified as

$$\mathbf{J} = -D\nabla C,\tag{2.4}$$

where D is the diffusion coefficient; this definition has been used to simulate fission product transport within the fuel. Also implemented in BISON is a hyperstoichiometric model for oxygen diffusion in  $UO_2$  fuel as described in [5]. In this case J denotes the oxygen flux in the hyperstoichiometric regime with,

$$\mathbf{J} = -D\left(\nabla C - \frac{CQ^*}{FRT^2}\nabla T\right),\tag{2.5}$$

where D is diffusivity, F is the thermodynamic factor of oxygen,  $Q^*$  is the heat of transport of oxygen, and R is the universal gas constant.

Momentum conservation is prescribed assuming static equilibrium at each time increment using Cauchy's equation,

$$\nabla \cdot \mathbf{\sigma} + \mathbf{\rho} \mathbf{f} = 0, \tag{2.6}$$

where  $\sigma$  is the Cauchy stress tensor and  $\mathbf{f}$  is the body force per unit mass (e.g. gravity). The displacement field u, which is the primary solution variable, is connected to the stress field via the strain, through a constitutive relation.

## 3 Element Kinematics

For geometrically linear analysis, the strain  $\varepsilon$  is defined as  $1/2[\nabla \mathbf{u} + \nabla \mathbf{u}^T]$ . Furthermore, with a linear elastic constitutive model, the stress is simply  $C \varepsilon$ . We now outline our approach for nonlinear analysis. We follow the approach in [6] and the software package [7].

We begin with a complete set of data for step n and seek the displacements and stresses at step n+1. We first compute an incremental deformation gradient,

$$\hat{\mathbf{F}} = \frac{\partial x^{n+1}}{\partial x^n}.\tag{3.1}$$

With  $\hat{\mathbf{f}}$ , we next compute a strain increment that represents the rotation-free deformation from the configuration at n to the configuration at n+1. Following [6], we seek the stretching rate  $\mathbf{D}$ :

$$\mathbf{D} = \frac{1}{\Delta t} \log(\hat{\mathbf{U}}) \tag{3.2}$$

$$= \frac{1}{\Delta t} \log \left( \operatorname{sqrt} \left( \hat{\mathbf{f}}^T \hat{\mathbf{f}} \right) \right) \tag{3.3}$$

$$= \frac{1}{\Delta t} \log \left( \operatorname{sqrt} \left( \hat{\mathbf{C}} \right) \right). \tag{3.4}$$

Here,  $\hat{\mathbf{U}}$  is the incremental stretch tensor, and  $\hat{\mathbf{C}}$  is the incremental Green deformation tensor. Through a Taylor series expansion, this can be determined in a straightforward, efficient manner.  $\mathbf{D}$  is passed to the constitutive model as an input for computing  $\sigma$  at n+1.

The next step is computing the incremental rotation,  $\hat{\mathbf{R}}$  where  $\hat{\mathbf{F}} = \hat{\mathbf{R}}\hat{\mathbf{U}}$ . Like for  $\mathbf{D}$ , an efficient algorithm exists for computing  $\hat{\mathbf{R}}$ . It is also possible to compute these quantities using an eigenvalue/eigenvector routine.

With  $\sigma$  and  $\hat{\mathbf{R}}$ , we rotate the stress to the current configuration.

# 4 Axisymmetric Equations

For the axisymmetric case (RZ), the nonlinear strains are derived starting from the Green-Lagrange strain:

$$E = \frac{1}{2} \left( F^T F - I \right) = \frac{1}{2} \left( \left( I + \frac{\partial u}{\partial X} \right)^T \left( I + \frac{\partial u}{\partial X} \right) - I \right) = \frac{1}{2} \left( \frac{\partial u}{\partial X} + \frac{\partial u}{\partial X}^T + \frac{\partial u}{\partial X}^T \frac{\partial u}{\partial X} \right)$$
(4.1)

This leads to:

$$\varepsilon_{rr} = \frac{\partial u_r}{\partial r} + \frac{1}{2} \left( \frac{\partial u_r}{\partial r}^2 + \frac{\partial u_z}{\partial r}^2 \right) \tag{4.2}$$

$$\varepsilon_{zz} = \frac{\partial u_z}{\partial z} + \frac{1}{2} \left( \frac{\partial u_r}{\partial z}^2 + \frac{\partial u_z}{\partial z}^2 \right) \tag{4.3}$$

$$\varepsilon_{\theta\theta} = \frac{u_r}{r} + \frac{1}{2} \left(\frac{u_r}{r}\right)^2 \tag{4.4}$$

$$\varepsilon_{rz} = \frac{1}{2} \left( \frac{\partial u_r}{\partial z} + \frac{\partial u_z}{\partial r} + \frac{\partial u_r}{\partial r} \frac{\partial u_r}{\partial z} + \frac{\partial u_z}{\partial r} \frac{\partial u_z}{\partial z} \right)$$
(4.5)

We can recover the linear strain by ignoring the higher-order terms.

# 5 Spherically Symmetric Equations

For the spherically symmetric case, the nonlinear strains are derived starting from the Green-Lagrange strain:

$$E = \frac{1}{2} \left( F^T F - I \right) = \frac{1}{2} \left( \left( I + \frac{\partial u}{\partial X} \right)^T \left( I + \frac{\partial u}{\partial X} \right) - I \right) = \frac{1}{2} \left( \frac{\partial u}{\partial X} + \frac{\partial u}{\partial X}^T + \frac{\partial u}{\partial X}^T \frac{\partial u}{\partial X} \right)$$
(5.1)

This leads to:

$$\varepsilon_{rr} = \frac{\partial u_r}{\partial r} + \frac{1}{2} \left( \frac{\partial u_r}{\partial r}^2 \right) \tag{5.2}$$

$$\varepsilon_{\theta\theta} = \frac{u_r}{r} + \frac{1}{2} \left(\frac{u_r}{r}\right)^2 \tag{5.3}$$

$$\varepsilon_{\phi\phi} = \frac{u_r}{r} + \frac{1}{2} \left(\frac{u_r}{r}\right)^2 \tag{5.4}$$

We can recover the linear strain by ignoring the higher-order terms.

# 6 Elasticity

For elastic behavior, a hypoelastic formulation is used, specifically,

$$\sigma_{ij}^{n+1} = \sigma_{ij}^n + \Delta t \mathbf{C}_{ijkl} \mathbf{D}_{kl}$$
 (6.1)

where C is the elasticity tensor. For isotropic elasticity, this becomes

$$\sigma_{ij}^{n+1} = \sigma_{ij}^{n} + \Delta t \left( \delta_{ij} \lambda \mathbf{D}_{kk} + 2\mu \mathbf{D}_{ij} \right)$$
(6.2)

with  $\lambda$  as Lame's first parameter and  $\mu$  as the shear modulus. This stress update occurs in the configuration at n. Thus as a final step, the stress must be rotated to the configuration at n+1.

### 7 Nonlinear Materials

Fuel materials often exhibit nonlinear mechanical behavior. As a first step to modeling this behavior, von Mises linear isotropic strain hardening via an implicit radial return method was implemented in BISON. A summary of this implementation is described in the following steps.

1. An elastic trial stress is calculated using the previous stress state and a total strain increment

$$\sigma^{trial} = \sigma_{old} + C\Delta\varepsilon \tag{7.1}$$

where C is the linear isotropic elasticity tensor,  $\Delta \epsilon$  is the total strain increment tensor, and  $\sigma_{old}$  is the stress from the previous time step.

2. A yield function is evaluated

$$f = \sigma_{eff}^{trial} - r - \sigma_{yield} \tag{7.2}$$

where f is the yield function,  $\sigma_{eff}^{trial}$  is the effective trial stress based on the deviatoric trial stress, r is the hardening variable, and  $\sigma_{yield}$  is the yield stress. If the yield function is greater than zero, then permanent deformation has occurred and a the plastic strain increment must be calculated. Otherwise, the trial stress is the new stress.

3. The hardening variable, r, and the plastic strain increment are solved via Newton iteration.

$$r = r_{old} + h\Delta p \tag{7.3}$$

$$residual = \frac{\sigma_{effective}^{trial} - 3G\Delta p - r - \sigma_{yield}}{3G + h}$$
 (7.4)

$$\Delta p = \Delta p_{old} + residual \tag{7.5}$$

In step 3.  $r_{old}$  is the hardening variable from the previous time step, h is the hardening constant, which defines the slope of the linear strain hardening section of the stress vs. strain plot,  $\Delta p$  and  $\Delta p_{old}$  are the plastic strain increment for the current and previous time steps respectively, and G is the shear modulus. In this Newton iteration, the residual is driven to some predefined small number as the hardening variable r and the plastic strain increment  $\Delta p$  are updated to achieve such a small residual.

4. When the residual is sufficiently small, the new plastic strain increment is used to update a plastic strain increment tensor  $(\Delta \varepsilon_p)$  that is used to calculate an elastic strain  $(\Delta \varepsilon_e)$  from the total strain  $(\Delta \varepsilon)$  and a new stress increment is calculated using this new elastic strain.

$$\Delta \varepsilon^p = \frac{3}{2} \Delta p \frac{\sigma_{dev}^{trial}}{\sigma_{eff}^{trial}},\tag{7.6}$$

$$\Delta \varepsilon^e = \Delta \varepsilon - \Delta \varepsilon^p, \tag{7.7}$$

$$\Delta \sigma = \mathbf{C} \Delta \varepsilon^e \tag{7.8}$$

5. Now, the stress and the plastic strain are updated

$$\sigma = \sigma_{old} + \Delta \sigma \tag{7.9}$$

$$p = p_{old} + \Delta p \tag{7.10}$$

6. In conventional nonlinear solvers, the material Jacobian is calculated and used to solve the nonlinear problem. Note however, that the material Jacobian is NOT required using the JFNK method. It can be used as a preconditioner and it is therefore presented here.

$$\frac{\partial \delta \sigma}{\partial \delta \varepsilon} = 2GQ \frac{\sigma_{dev}^{trial}}{\sigma_{eff}^{trial}} \frac{\sigma_{dev}^{trial}}{\sigma_{eff}^{trial}} + 2GRI + \left(K - \frac{2}{3}GR\right)II$$
 (7.11)

where

$$R = \frac{\sigma_{eff}^{trial} - 3G\Delta p}{\sigma_{eff}^{trial}} \tag{7.12}$$

and

$$Q = \frac{3}{2} \left( \frac{h}{h+3G} \right) - R \tag{7.13}$$

The source used for guidance in implementing this plasticity model into BISON was "Introduction to Computational Plasticity" [8].

### 8 Fuel Material and Behavioral Models

### 8.1 Thermal Properties

#### 8.1.1 UO<sub>2</sub> thermal conductivity

Five empirical models are available in BISON to compute UO<sub>2</sub> thermal conductivity and its dependence on temperature, porosity, burnup, and, for three of the models, Gadolinia content. Choices for UO<sub>2</sub> fuel include models referred to as Fink-Lucuta [9][10], Halden [11], NFIR [12], MATPRO [13], and modified NFI [14] (modifications described in [11]). The Halden, MATPRO, and modified NFI models can account for Gadolinia content.

Empirical fits for the temperature dependent specific heat of UO<sub>2</sub> accompany both the Fink-Lucuta and MATPRO conductivity models.

For the most part, the thermal conductivity of urania is represented as the sum of a lattice vibration (phonon) and an electronic (electron hole pair effect) term or for unirradiated material at 95% theoretical density (TD)

$$k_{95} = k_{\text{phonon}} + k_{\text{electronic}} \tag{8.1}$$

The first term in Equation 8.1 is typically inversely proportional to the sum of temperature and burnup dependent functions, while the second term, usually an exponential function of inverse temperature, is inversely proportional to temperature or temperature squared. For example,

$$k_{phonon} = 1.0/(A + B * T + f(Bu) + g(Bu) * h(T))$$
 (8.2)

$$k_{\text{electronic}} = i(T) * \exp(-F/T)$$
 (8.3)

where A, B, and F are constants, Bu is burnup, T is temperature, and f, g, h, and i are functions of burnup or temperature. While each of the thermal conductivity models has the basic form given by Equations 8.2 and 8.3, each has their own specific set of constants and perhaps additional corrections that account for effects of dissolved fission products, precipitated fission products, porosity, deviation from stoichiometry, and radiation damage. In general, the final conductivity corrected for these effects is given as

$$k = k_{95} * f_d * f_p * f_{por} * f_x * f_r$$
(8.4)

where:

f<sub>d</sub> – dissolved fission products correction

f<sub>p</sub> – preipitated fission products correction

fpor - porosity correction

 $f_x$  – deviation from stoichiometry (1.0 for urania fuel but  $\neq 1$  if Gadolinia present)

f<sub>r</sub> – radiation damage correction

#### 8.1.1.1 Fink-Lucuta

In the Fink-Lucuta model, the temperature-dependence of unirradiated material is defined using the equation suggested by Fink [9]. This relationship is then modified to account for the effects of irradiation, porosity and burnup using a series of multipliers, as outlined in detail by Lucuta et al. [10]. The Fink equation is

$$k_{95} = \left(\frac{1}{7.5408 + 17.692 \cdot T_n + 3.6142 \cdot T_n^2} + \frac{6400}{T_n^{5/2}} \exp\left(-\frac{16.35}{T_n}\right)\right)$$
(8.5)

where  $T_n$  is the temperature in K divided by 1000. Equation 8.5 is multiplied by the following factor to obtain 100% TD thermal conductivity

$$k = k_{95} \cdot \left(\frac{1}{1 - (2.6 - 0.5 \cdot T_n) \cdot 0.05}\right)$$
(8.6)

Equation 8.6 is then corrected per Equation 8.4 as perscribed by Lucuta where

$$f_{d} = \left(\frac{1.09}{bu^{3.265}} + 0.0643 \cdot \sqrt{\frac{T}{bu}}\right) \cdot \arctan\left(\frac{1.0}{\frac{1.09}{bu^{3.265}} + 0.0643 \cdot \sqrt{\frac{T}{bu}}}\right)$$
(8.7)

$$f_{p} = 1.0 + \left(\frac{0.019 \cdot bu}{3.0 - 0.019 \cdot bu}\right) \cdot \left(\frac{1.0}{1.0 + \exp\left(\frac{-(T - 1200)}{100}\right)}\right)$$
(8.8)

$$f_{por} = \left(\frac{1.0 - p}{1.0 + 0.5 \cdot p}\right) \tag{8.9}$$

$$f_{\rm r} = 1.0 - \frac{0.2}{1.0 + \exp\left(\frac{(T - 900)}{80}\right)}$$
(8.10)

where T is the temperature in K, p is the porosity, and bu is the burnup in at.%.

The Fink-Lucuta model is valid from 298 to 3120 K [15].

#### 8.1.1.2 MATPRO

The MATPRO model [13] is based on an equation proposed by Ohira and Itagakia [14]. The thermal conductivity for 95% theroetical density is given as

$$k_{95} = 1/(\text{term0} + \text{term1} + \text{term2} + \text{term3} + \text{term4} \cdot \text{term5}) + \text{term6}$$

$$(8.11)$$

where the recriprocal expression and term6 correspond to  $k_{\text{phonon}}$  and  $k_{\text{electronic}}$ , respectively. The terms are defined as

term0 = 
$$0.0452$$
  
term1 =  $0.000246 \cdot T$   
term2 =  $0.00187 \cdot Bu$   
term3 =  $1.1599 \cdot Gdcon$   
term4 =  $(1 - 0.9 \cdot exp(-0.04 \cdot Bu)) \cdot 0.038 \cdot Bu^{0.28}$   
term5 =  $1/(1 + 396 \cdot exp(-6380/T))$   
term6 =  $3.5e9/T^2 \cdot exp(-16360/T)$ 

and T is temperature in K, Bu is burnup in MWd/kgU, and Gdcon is the Gadolinia concentration in wt.%. Equation 8.11 is multiplied by the appropriate factor to return the thermal conductivity to 100% TD and then multiplied by a density correction factor (similar to Equation 8.9 but written in terms of %TD) to provide a thermal conductivity representative of the material of interest

$$k = k_{95} \cdot 1.0789 \cdot \frac{D}{(1 + 0.5 \cdot (1 - D))}$$
(8.12)

where D is the fractional TD. The multiplier 1.0789 is the inverse of the density correction factor evaluated at 0.95 TD.

The MATPRO correlation is valid over the following ranges [11]

$$300 \le T (K) \le 3000$$
  
 $0 \le Bu \le 62 \text{ MWd/kgU}$   
 $0.92 \le D \le 0.97$   
 $0 \le Gdcon \le 10 \text{ wt.}\%$ 

Figure 8.1 compares the two models as a function of temperature and burnup for fully dense  $UO_2$ .

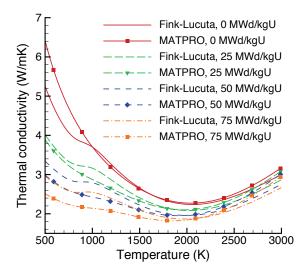


Figure 8.1: A comparison of the Fink-Lucuta and MATPRO empirical models for the thermal conductivity of full density UO<sub>2</sub>, as a function of temperature and burnup.

#### 8.1.1.3 Halden

The Halden model has the same form as Equation 8.11. However, the terms are different, and different temperature and burnup units are used. For 95% TD fuel, the terms are

```
\begin{split} \text{term0} &= 0.1148 \\ \text{term1} &= 1.1599 \cdot \text{Gdcon} \\ \text{term2} &= 1.1599 \cdot \text{f}_x \\ \text{term3} &= 4\text{e-}3 \cdot \text{BuUO2} \\ \text{term4} &= 2.475\text{e-}4 \cdot (1 - 3.33\text{e-}3 \cdot \text{BuUO2}) \cdot \min(1650,\text{Tc}) \\ \text{term5} &= 1 \\ \text{term6} &= 1.32\text{e-}2 \cdot \exp(0.00188 \cdot \text{Tc}) \end{split}
```

where Gdcon is the Gadolinia concentration in wt.%,  $f_x$  is the deviation from stoichiometry, i.e. (2 - oxygen/metal ratio), BuUO2 is the burnup in MWd/kgUO2, and Tc is the temperature in C. Equation 8.12 is used to compute the thermal conductivity at the TD of interest.

The Halden UO<sub>2</sub> correlation is valid over the following ranges [11]

 $\begin{aligned} 300 &\leq T \; (K) \leq 3000 \\ 0 &\leq Bu \leq 62 \; MWd/kgU \\ 0.92 &\leq D \leq 0.97 \\ 0 &\leq Gadolinia \; content \leq 10 \; wt.\% \end{aligned}$ 

Figure 8.2 compares the Fink-Lucuta and Halden models as a function of temperature and burnup for 95% theoretical density UO<sub>2</sub>.

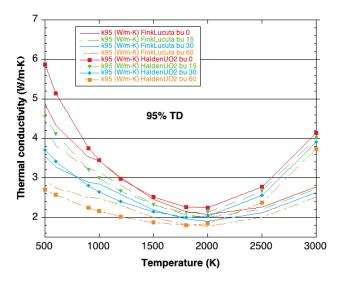


Figure 8.2: A comparison of the Fink-Lucuta and Halden empirical models for the thermal conductivity of 95% theoretical density UO<sub>2</sub>, as a function of temperature and burnup.

#### 8.1.1.4 NFIR

The NFIR correlation also has the general form of Equation 8.1. However, the NFIR model contains a temperature dependent thermal recovery function that accounts for self-annealing of defects in the fuel as it heats up. The ultimate effect of the self-annealing is a slight increase of the thermal conductivity over a range of temperatures up to  $\sim\!1200$  K. As a result of this formulation, two components of  $k_{phonon}$  are used, one at the start of thermal recovery and one at the end of thermal recovery. The thermal recovery function is used to interpolate between these two values to compute  $k_{phonon}$ . Thus

$$k_{95} = (1 - RF(Tc)) \cdot k_{phonon,start} + RF(Tc) \cdot k_{phonon,end} + k_{electronic}$$
(8.13)

where RF(Tc) is the thermal recovery function, Tc is temperature in C,  $k_{phonon,start}$  is the phonon contribution at the start of thermal recovery, and  $k_{phonon,end}$  is the phonon contribution at the end of thermal recovery. The individual terms are

$$k_{phonon,start} = 1/(9.592e-2 + 6.14e-3 \cdot Bu - 1.4e-5 \cdot Bu^2 + (2.5e-4 - 1.81e-6 \cdot Bu) \cdot Tc)$$
 (8.14)

$$k_{phonon,end} = 1/(9.592e-2 + 2.6e-3 \cdot Bu + (2.5e-4 - 2.7e-7 \cdot Bu) \cdot Tc)$$
 (8.15)

$$RF(Tc) = 0.5 \cdot (1 + \tanh((Tc-900)/150))$$
(8.16)

$$k_{electronic} = 1.32e-2 \cdot exp(1.88e-3 \cdot Tc)$$

$$(8.17)$$

where Bu is burnup in MWd/kgU. Equation 8.13 is then multiplied by a temperature dependent density correction factor to get

$$k = k_{95} \frac{[1 - (2.58 - 5.8e - 4 \cdot Tc) \cdot (1 - D)]}{[1 - 0.05 \cdot (2.58 - 5.8e - 4 \cdot Tc)]}$$
(8.18)

where D is the fractional density. Figure 8.3 compares the the Fink-Lucuta and NFIR models as a function of temperature and burnup for 95% theoretical density  $UO_2$ .

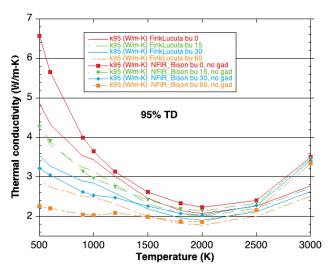


Figure 8.3: A comparison of the Fink-Lucuta and NFIR empirical models for the thermal conductivity of 95% theoretical density UO<sub>2</sub>, as a function of temperature and burnup.

#### 8.1.1.5 Modified NFI

The modified NFI model is also of the form of Equation 8.11. Terms are defined as

term0 = 
$$0.0452$$
  
term1 =  $1.1599 \cdot \text{Gdcon}$   
term2 =  $2.46e - 4 \cdot \text{T}$   
term3 =  $1.87e - 3 \cdot \text{Bu}$   
term4 =  $(1 - 0.9 \cdot \exp(-0.04 \cdot \text{Bu})) \cdot 0.038 \cdot \text{Bu}^{0.28}$   
term5 =  $1/(1 + 396 \cdot \exp(-6380/\text{T}))$   
term6 =  $3.5e9/\text{T}^2 \cdot \exp(-16360/\text{T})$ 

where Gdcon is the Gd concentration in wt.%, T is the temperature in K, Bu is the burnup in MWd/kgU. Again, Equation 8.12 is used to convert to the TD of interest.

The modified NFI model is valid over the following ranges [11]

$$300 \le T (K) \le 3000$$
  
 $0 \le Bu \le 62 \text{ MWd/kgU}$   
 $0.92 \le D \le 0.97$   
 $0 \le Gdcon \le 10 \text{ wt.}\%$ 

Figure 8.4 compares the Fink-Lucuta and NFI modified models as a function of temperature and burnup for 95% theoretical density UO<sub>2</sub>.

#### 8.1.2 MOX thermal conductivity

#### 8.1.2.1 Reference documents

- Unirradiated thermal conductivity of UO<sub>2</sub> fuel: [9]
- Irradiated thermal conductivity of UO<sub>2</sub> fuel: [10]
- Review of available models for thermal conductivity of UO<sub>2</sub> and MOX: [15]
- Ronchi model for thermal conductivity of MOX: [16]
- Duriez model for thermal conductivity of MOX: [17]
- Amaya model for thermal conductivity of MOX: [18]

Three models are available to compute MOX thermal properties in BISON. For these models, thermal conductivity of unirradiated material is first defined. In general, these relationships are then multiplied by correction factors, which account for effects of irradiation, burnup, MOX content, and porosity. The corrections factors used in BISON have been developed by Lucuta et al. [10] and are recommended by Carbajo et al. [15].

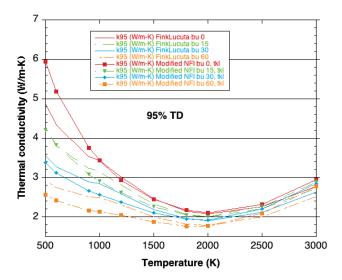


Figure 8.4: A comparison of the Fink-Lucuta and modified NFI empirical models for the thermal conductivity of 95% theoretical density UO<sub>2</sub>, as a function of temperature and burnup.

#### 8.1.2.2 Duriez-Ronchi

The first model is recommended by Carbajo et al. in [15] and is a combination of Duriez [17] and Ronchi [16] models. In this first model, thermal conductivity of unirradiated MOX is given by:

$$\lambda_0(T, x) = 1.158 \cdot \left( \frac{1}{A + CT_n} + \frac{6400}{T_n^{5/2}} \exp\left(-\frac{16.35}{T_n}\right) \right)$$
(8.19)

where:

 $\lambda_0 = \text{ thermal conductivity in } W \cdot m^{-1} \cdot K^{-1}$ 

 $T_n = T (K)/1000$  reduced temperature

x = deviation from stoichiometry (unitless)

A(x) = 2.85x + 0.035

C(x) = -0.715x + 0.286

This model provides temperature and deviation from stoechiometry. It is valid from 700 to 3100 K, x less than 0.05, and plutonium concentration between 3 wt.% and 15 wt. %. According to [15], thermal conductivity does not depend on Pu concentration in this range. Thus this model is valid essentially for thermal reactor MOX.

#### 8.1.2.3 Amaya

The second model available in BISON has been proposed by Amaya et al. [18]. Unlike the previous model, Amaya provides a plutonium concentration dependence. It starts from pure UO<sub>2</sub> thermal conductivity and applies corrections to account for Pu content. Unirradiated MOX thermal conductivity is given by:

$$\lambda_{MOX,0} = \sqrt{\frac{\lambda_0}{D_{0,Pu} \exp(D_{1,Pu} \cdot T) \cdot y}} \cdot \arctan(\sqrt{D_{0,Pu} \exp(D_{1,Pu} \cdot T) \cdot y \cdot \lambda_0})$$
(8.20)

where:

 $\lambda_{MOX,0} = \text{MOX}$  unirradiated thermal conductivity in W·m<sup>-1</sup>·K<sup>-1</sup>  $\lambda_0 = \text{UO}_2$  unirradiated thermal conductivity in W·m<sup>-1</sup>·K<sup>-1</sup> T = temperature(K) y = plutonium concentration(wt.%)  $D_{0,Pu} = 0.209 \text{ m} \cdot \text{W} \cdot \text{K}^{-1}$   $D_{1,Pu} = 1.09 \cdot 10^{-3} \text{ K}^{-1}$ 

BISON uses Fink model to compute unirradiated UO<sub>2</sub> thermal conductivity. Amaya model's coefficients have been fitted in the temperature range from 400 K to 1500 K and the plutonium concentration up to 30 wt.% ([18]). Figure 8.5 shows a comparison of the computed thermal conductivities for the Fink-Lucuta (for reference), Fink-Amaya, and Duriez-Ronchi models for unirradiated MOX at 95% theoretical density.

#### 8.1.2.4 Halden

The Halden correlation discussed in the previous section for urania fuel is also applicable, with one change, to MOX fuel. Reduction in thermal conductivity due to the presence of mixed oxides is accounted for by multiplying the  $k_{phonon}$  term in Equation 8.1 by 0.92. This is consistent with the statement above regarding the lack of dependence of MOX thermal conductivity on Pu concentration. The  $k_{electronic}$  part of the equation is unchanged and Equation 8.12 is used to account for the TD of interest.

The Halden MOX correlation is valid over the following ranges [11]

$$300 \le T \text{ (K)} \le 3000$$
 
$$0 \le Bu \le 62 \text{ MWd/kgU}$$
 
$$0.92 \le D \le 0.97$$
 
$$0 \le \text{plutonia content} \le 7 \text{ wt.\%}$$
 plutonia particle size  $< 20\text{e-6 m}$ 

Figure 8.6 is a comparison of the Fink-Lucuta (for reference) urania correlation and the Fink-Amaya, Duriez-Ronchi, and Halden correlations for MOX for unirradiated 95% theoretical density MOX fuel with 0.07% Pu concentration.

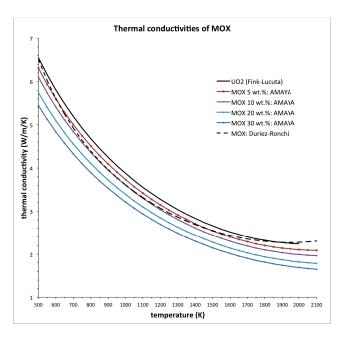


Figure 8.5: Unirradiated thermal conductivities for UO<sub>2</sub> and MOX from different models implemented in BISON.

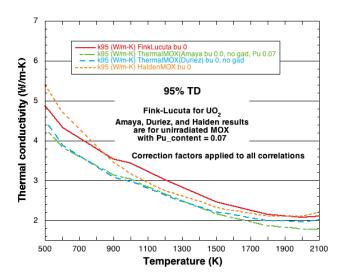


Figure 8.6: Unirradiated thermal conductivities for UO<sub>2</sub> (for reference) and MOX from different models implemented in BISON. Results are for 95% theoretical density and Pu concentration of 7 wt.%. Correction factors appropriate for each correlation have been applied.

### 8.2 Fission Product Swelling

Empirical relations from MATPRO [13] are available in BISON for calculating the swelling due to both solid and gaseous fission products. The same model is provided for both UO<sub>2</sub> and MOX. Solid fission product swelling is expressed as a simple linear function of burnup:

$$\Delta \varepsilon_{sw-s} = 5.577 \times 10^{-5} \rho \Delta Bu \tag{8.21}$$

where  $\Delta \varepsilon_{sw-s}$  is the volumetric solid swelling increment,  $\Delta Bu$  the burnup increment (fissions/atoms-U), and  $\rho$  is the density (kg/m<sup>3</sup>). Swelling due to gaseous fission products is approximated by a semi-empirical model:

$$\Delta \varepsilon_{sw-g} = 1.96 \times 10^{-31} \rho \Delta B u (2800 - T)^{11.73}$$

$$*e^{-0.0162(2800 - T)} e^{-0.0178 \rho B u}$$
(8.22)

where  $\Delta \varepsilon_{sw-g}$  is the volumetric gas swelling increment, Bu and  $\Delta Bu$  are the burnup and burnup increment (fissions/atoms-U), respectively,  $\rho$  is the density (kg/m<sup>3</sup>) and T is the temperature (K). Figure 8.7 shows a plot of the gaseous and total fission product swelling as a function of temperature and burnup. The MATPRO [13] correlations indicate that gaseous swelling does not become significant until above 1500 K and is saturated at a burnup of 20 MWd/kgU.

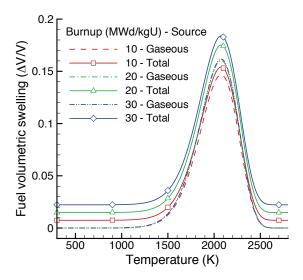


Figure 8.7: UO<sub>2</sub> gaseous and total swelling, as a function of temperature and burnup, based on the MATPRO [13] correlations.

Alternatively, the gaseous fission product swelling can be calculated using a physics-based model that takes into account the coupling with the fission gas release (see Subsection 8.8.1).

#### 8.3 Densification

Fuel densification is computed using the ESCORE empirical model [19] given by:

$$\varepsilon_D = \Delta \rho_0 \left( e^{\left(\frac{Bu \ln(0.01)}{C_D B u_D}\right)} - 1 \right) \tag{8.23}$$

where  $\varepsilon_D$  is the densification strain,  $\Delta \rho_0$  is the total densification that can occur (given as a fraction of theoretical density), Bu is the burnup, and  $Bu_D$  is the burnup at which densification is complete. For temperatures below 750 °C the parameter  $C_D$  is given by 7.2 - 0.0086(T - 25); above 750 °C it is 1.0 (T in °C).

In MATPRO ([13]), the same model is provided for  $UO_2$  and MOX. As this correlation relies on a wide database, the same model is also used in BISON for MOX and  $UO_2$  densification.

#### 8.4 Relocation

One way to model the effect of UO<sub>2</sub> cracking on gap width is fuel relocation. Thermal gradients in a LWR fuel pellet result in corresponding stress gradients that exceed the fuel fracture stress, causing radial cracks. The free surfaces of the crack result in a overall increase of fuel pellet diameter. This effect can be modeled by applying a radial strain to the fuel pellet. This strain is similar to a volumetric strain, but only in the radial direction. A method for calculating this strain is the ESCORE relocation model [20] which is given as

$$\left(\frac{\Delta D}{D_o}\right)_{REL} = 0.80Q\left(\frac{G_t}{D_o}\right)\left(0.005Bu^{0.3} - 0.20D_o + 0.3\right)$$
(8.24)

This relocation model is a function of power, as-fabricated pellet diameter, as-fabricated gap thickness, and burnup. The model is applicable between 8 and 22 kW/ft and to burnup levels between 0 and 11,500 MWd/MTU, and mean-diameter measurements were used in the correlation development. The following is a list of variables definitions.

 $(\frac{\Delta D}{D_o})_{REL}$ : Diametral strain due to relocation,

 $D_o$ : As-fabricated cold diameter of the pellet (in),

q': Pellet average linear heating rate (kW/ft),

 $BU_t$ : Pellet average fuel burnup (MWd/MTU), and

 $G_t$ : As-fabricated cold diametral gap (in)

$$Q : \begin{cases} 0 & \text{for } q' \le 6 \text{kW/ft} \\ (q' - 6)^{1/3} & \text{for } 6 \text{kW/ft} < q' \le 14 \text{ kW/ft} \\ (q' - 10)/2 & \text{for } q' > 14 \text{ kW/ft} \end{cases}$$

The fuel relocation strain is applied incrementally by calculating the relocation strain at the burnup for the current step and subtracting the relocation strain at the previous burnup. In other applications of this model, the addition of relocation strain is stopped when the gap is closed. In BISON, the relocation strain is stopped at a specified burnup.

Note that the pellet average linear heating rate q' has units of kW/ft in the empirical model. However, this quantity is passed into the model as a function with units of W/m. The conversion is handled inside the model.

### 8.5 Thermal and Irradiation Creep

### 8.5.1 UO<sub>2</sub> model

A model for combined secondary thermal creep and irradiation creep of UO<sub>2</sub> fuel is available, with the creep rate modeled as a function of time, temperature, effective stress, density, grain size, fission rate, and oxygen to metal ratio (O/M). The constitutive relation is taken from the MATPRO FCREEP material model [21] and given as

$$\dot{\varepsilon} = \frac{A_1 + A_2 \dot{F}}{(A_3 + D)G^2} \sigma e^{\left(\frac{-Q_1}{RT}\right)} + \frac{A_4}{(A_6 + D)} \sigma^{4.5} e^{\left(\frac{-Q_2}{RT}\right)} + A_7 \dot{F} \sigma e^{\left(\frac{-Q_3}{RT}\right)}$$
(8.25)

where  $\dot{\epsilon}$  is the creep rate (1/s),  $\sigma$  is the effective (Mises) stress (Pa), T is the temperature (K), D is the fuel density (percent of theoretical), G is the grain size ( $\mu m$ ), F is the volumetric fission rate (fissions/ $m^3$ -s),  $Q_i$  are the activation energies (J/mol), R is the universal gas constant (8.3143 J/mol-K) and  $A_{1-7}$  are material constants given as  $A_1 = 0.3919$ ,  $A_2 = 1.3100x10^{-19}$ ,  $A_3 = -87.7$ ,  $A_4 = 2.0391x10^{-25}$ ,  $A_6 = -90.5$ , and  $A_7 = 3.7226x10^{-35}$ . The first term represents diffusional thermal creep and is applicable to low stress and low temperature conditions. The second term represents thermal dislocation or power-law creep and is applicable to high stress and high temperature conditions. Note that irradiation effects are included in both the first and third terms.

The activation energies for the thermal creep terms  $(Q_1 \text{ and } Q_2)$  are strongly dependent upon the fuel oxygen to metal ratio x and, in MATPRO, are defined using the Arrhenius type relations

$$Q_1 = 74,829 f(x) + 301,762 (8.26)$$

$$Q_2 = 83,143 f(x) + 469,191$$
 (8.27)

where the energies are given in J/mole and

$$f(x) = \frac{1}{e^{\left(\frac{-20}{\log(x-2)} - 8\right)} + 1}$$
 (8.28)

This function is plotted in Figure 8.8. The activation energy for the irradiation term  $(Q_3)$  is given in MATPRO as 21,759 J/mole.

In MATPRO, a transition stress is defined to govern the transition between the first (low stress) and second (high stress) regions. When the applied stress is larger than the transition stress, the applied stress is used in the power-law relation and the transition stress is used in the linear creep relation. When the applied stress is lower than the transition stress, the applied stress is used in the linear relation and the power-law contribution is zero. Mai et al. [22] investigated the MATPRO transition approach in comparison to experimental data and concluded that a better fit to the data could be achieved by simply ignoring the transition stress and applying both the low

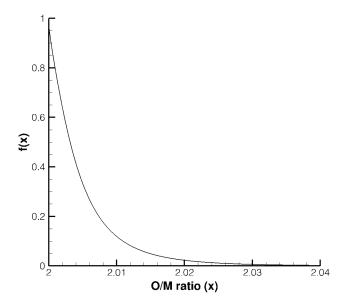


Figure 8.8: The function defining the dependence of the activation energies for thermal creep on the  $UO_2$  oxygen to metal ratio.

and high stress terms in all cases. This approach, termed here the Modified MATPRO model, has been adopted in BISON. The procedure outlined above for time-independent plasticity was used here to implement time-dependent plasticity (creep).

Young's modulus, Poisson's ratio and the coefficient of thermal expansion can each be specified in two ways. The values can be given directly, or the values can be computed using MAT-PRO correlations.

#### 8.5.2 MOX model

#### 8.5.2.1 Reference Documents

- Implementation of non linear materials in BISON: F. Dunne in [8]
- Thermal creep of MOX: MATPRO [13]
- Irradiation creep of MOX: Y. Guerin in [23] and C. Milet [24]

#### 8.5.2.2 Available model

The creep model for MOX implemented in BISON for MOX is a combined model from MAT-PRO [13] and Guerin [23]. Experimental data used by MATPRO for MOX cover indeed a range of temperature above 1500 K, so that the proposed model accounts essentially for thermal creep.

In [23], Guerin provides an semi-empirical law for MOX irradiation creep, hired from Milet's experiments, whose results have been published in [24]. MATPRO provides a time-dependant multiplier which allows to account for primary and secondary creep. Thus the creep model for MOX implemented in BISON is given by:

$$\dot{\boldsymbol{\varepsilon}}_{cr} = (1 + a \exp(-b \cdot t)) \cdot \dot{\boldsymbol{\varepsilon}}_{s} \tag{8.29}$$

with

$$\dot{\varepsilon}_s = \frac{B_1 + B_2 \dot{F}}{G^2} \sigma \exp\left(-\frac{Q_3}{T} + B_7(1 - D) + B_4 C\right)$$
(8.30)

$$+B_5\sigma^{4.5}\exp\left(-\frac{-Q_4}{T}+B_7(1-D)+B_4C\right)$$
 (8.31)

$$+A\sigma\dot{F}$$
 (8.32)

where

T = Temperature(K)

 $\sigma$  = Effective stress (Pa)

 $\dot{F} = \text{Fission rate m}^{-3} \cdot \text{s}^{-1}$ 

 $G = \text{grain size } (\mu \text{m})$ 

a = 2.5

 $C = PuO_2$  concentration (wt.%)

and in SI

$$b = 1.40 \cdot 10^{-6}$$
$$A = 4.8\dot{1}0^{-36}$$

$$B_1 = 0.1007$$

$$B_2 = 7.57 \cdot 10^{-20}$$

$$B_3 = 33.3$$

$$B_4 = 0.014$$

$$B_5 = 6.4691 \cdot 10^{-25}$$

$$B_7 = 10.3$$

$$Q_3 = 55354.0$$

$$Q_4 = 70451.0$$

Figure 8.9 shows a comparison between creep models implemented in BISON for  $UO_2$  and MOX.

The time origin for primary creep is updated in BISON when the stress rate is greater than a value specified by the user. Two successive time origins cannot be closer than 5 times the characteristic time of transient creep.

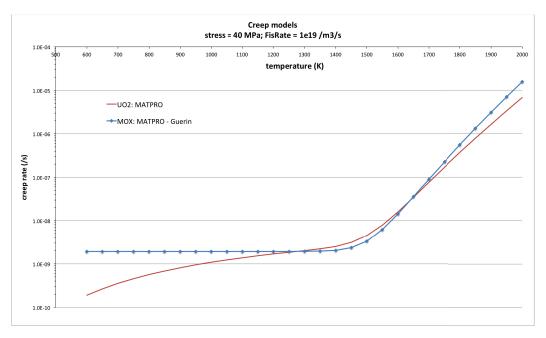


Figure 8.9: Comparison of creep rates for MOX and UO<sub>2</sub>. The creep rate for MOX is higher than that of UO<sub>2</sub>.

### 8.6 Smeared Cracking

In ceramic fuel such as UO<sub>2</sub>, a significant temperature gradient develops from the fuel center to the radial edge. This gradient appears early and is strong enough to induce cracking in the fuel due to the accompanying stress. The cracks reduce the stress in the fuel and increase the effective fuel volume (decrease the gap size).

A smeared cracking model in BISON may be invoked to account for this cracking. A smeared cracking model adjusts the elastic constants at material points as opposed to introducing topographic changes to the mesh, as would be the case with a discrete cracking model.

When the smeared cracking model is active, principal stresses are compared to a critical stress. If the material stress exceeds the critical stress, the material point is considered cracked in that direction, and the stress is reduced to zero. From that point on, the material point will have no strength unless the strain becomes compressive.

The orientation of the principal coordinate system is determined from the eigenvectors of the elastic strain tensor. However, once a crack direction is determined, that direction remains fixed and further cracks are considered in directions perpendicular to the original crack direction. Note that for axisymmetric problems, one crack direction is known *a priori*. The theta or out-of-plane direction is not coupled to the r and z directions (i.e., no  $r\theta$  or  $z\theta$  shear strain/stress exists) and is therefore a known or principal direction.

If we store a scalar value,  $c_i$ , for each of the three possible crack directions at a material point, these in combination with the principal directions (eigenvectors or rotation tensor) provide a

convenient way to eliminate stress in cracked directions. A value of 1 for  $c_i$  indicates that the material point has not cracked in that direction. A value very close to zero (not zero for numerical reasons) indicates that cracking has occurred.

We define a cracking tensor in the cracked orientation as **c**:

$$\mathbf{c} = \begin{bmatrix} c_1 & & \\ & c_2 & \\ & & c_3 \end{bmatrix} . \tag{8.33}$$

The rotation tensor **R** is defined in terms of the eigenvectors  $e_i$ :

$$\mathbf{R} = \begin{bmatrix} e_1 & e_2 & e_3 \end{bmatrix}. \tag{8.34}$$

This leads to a transformation operator **T**:

$$\mathbf{T} = \mathbf{R}\mathbf{c}\mathbf{R}^T. \tag{8.35}$$

**T** is useful for transforming uncracked tensors in the global frame to cracked tensors in the same frame. For example, the cracked stress  $\sigma_{cg}$  in terms of the stress  $\sigma_g$  is (subscript *c* indicates cracked, *l* local frame, and *g* global frame):

$$\sigma_{cg} = \mathbf{T}\sigma_g \mathbf{T}^T \tag{8.36}$$

$$= \mathbf{R} \mathbf{c} \mathbf{R}^T \mathbf{\sigma}_{\varrho} \mathbf{R} \mathbf{c} \mathbf{R}^T \tag{8.37}$$

$$= \mathbf{R} \mathbf{c} \mathbf{\sigma}_{l} \mathbf{c} \mathbf{R}^{T} \tag{8.38}$$

$$= \mathbf{R} \sigma_{cl} \mathbf{R}^T. \tag{8.39}$$

When many material points have multiple cracks, the solution becomes difficult to obtain numerically. For this reason, controls are available to limit the number and direction of cracks that are allowed.

#### 8.7 Grain Growth

When a polycrystalline material is subject to high temperatures, larger grains tend to grow at the expense of the smaller ones. As a consequence, the latter gradually disappear, thus reducing the total number of grains per unit volume and increasing the average grain size. This phenomenon is known as grain growth. The granular structure of the fuel affects physical processes such as fission gas behavior (see Section 8.8).

A simple empirical model [25] is implemented in BISON for calculating grain growth in UO<sub>2</sub> fuel. According to this model, the kinetics of grain growth is described by the equation:

$$\frac{dD}{dt} = k \left( \frac{1}{D} - \frac{1}{D_m} \right) \tag{8.40}$$

where D ( $\mu$ m) is the 2-dimensional (linear intercept) average grain diameter, t (h) the time, k ( $\mu$ m²/h) the rate constant, which is  $5.24 \cdot 10^7 \exp(-2.67 \cdot 10^7/(RT))$  for R = 8.314 J/(mol·K), and  $D_m$  ( $\mu$ m) is the limiting grain size. The latter is a function of the temperature such that

$$D_m = 2.23 \cdot 10^3 \exp(-7620/T) \tag{8.41}$$

To obtain the 3-dimensional grain diameter, D is multiplied by a factor of 1.56 [26].

#### 8.8 Fission Gas Behavior

The processes induced by the generation of the fission gases xenon and krypton in nuclear fuel have a strong impact on the thermo-mechanical performance of the fuel rods. On the one hand, the fission gases tend to precipitate into bubbles resulting in fuel swelling, which promotes pellet-cladding gap closure and the ensuing pellet-cladding mechanical interaction (PCMI). On the other hand, fission gas release (FGR) to the fuel rod free volume causes pressure build-up and thermal conductivity degradation of the rod filling gas.

The fundamental physical processes, which control the kinetics of fission gas swelling and release in irradiated UO<sub>2</sub> fuel, may be summarised as follows. Fission gas atoms generated in the fuel grains diffuse towards the grain boundaries through repeated trapping in and irradiation-induced resolution from nanometre-size intra-granular gas bubbles. Although a part of the gas atoms that reach the grain boundaries is dissolved back to the grain interior by irradiation, the majority of the gas diffuses into grain-face gas bubbles, giving rise to grain-face swelling. Bubble growth brings about bubble coalescence and inter-connection, eventually leading to the formation of a tunnel network through which a fraction of the gas is released to the fuel rod free volume.

In BISON, fission gas behavior is computed for each integration point in the fuel finite element mesh. The gas produced at each integration point is computed by a numerical time integration of the gas production rate, given as the product of the fission rate and fractional yield of gas atoms per fission.

The Sifgrs model is recommended.

#### 8.8.1 Simple Physics-Based Model

The Simple Integrated Fission Gas Release and Swelling (Sifgrs) model is intended for consistently evaluating the kinetics of both fission gas swelling and release in UO<sub>2</sub>. The model incorporates the fundamental features of fission gas behavior, among which are gas diffusion and precipitation in grains, growth and coalescence of gas bubbles at grain faces, thermal, athermal, steady-state, and transient gas release. Through a direct description of the grain-face gas bubble development, the fission gas swelling and release are calculated as inherently coupled processes, on a physical basis. The level of complexity of the model is consistent with reasonable computational cost and the uncertainties inherent in engineering-scale fuel analysis. The Sifgrs model draws on and extends the approach described in [27].

#### 8.8.1.1 Intra-granular gas behavior

Fission gas transport from within the fuel grains to the grain faces is computed through numerical solution of the relevant diffusion equation in one-dimensional spherical geometry

$$\frac{\partial C_t}{\partial t} = D_{eff} \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial C_t}{\partial r} \right) + \beta \tag{8.42}$$

where  $C_t$  (m<sup>-3</sup>) is the intra-granular gas concentration, t (s) the time,  $D_{eff}$  (m<sup>2</sup>s<sup>-1</sup>) the effective gas diffusion coefficient, r (m) the radial co-ordinate in the spherical grain, and  $\beta$  (m<sup>-3</sup>s<sup>-1</sup>) the gas generation rate. The effective diffusion coefficient, which accounts for the effects of repeated trapping in and irradiation-induced resolution from intra-granular bubbles, is calculated based on [28, 29].

Moreover, an empirical contribution to gas transport from within the grains to the grain faces is considered during power ramps, aimed at representing the rapid increase of FGR observed under these conditions. In particular, the simple empirical ramp release model of Koo et al. [30] is adopted. According to this model, during a rapid power increase an additional fraction of the intra-granular gas is transferred to the grain faces, which depends on local temperature, linear power and linear power change during the transient.

The contribution of intra-granular bubbles to fission gas swelling (intra-granular swelling), which is generally less important than the swelling due to grain-face bubbles (at least for burnup below about 45 GWd/t [31]), is presently not considered in the model.

#### 8.8.1.2 Grain-face gas behavior

Numerical solution of Eq. 8.42 allows estimating the arrival rate of gas at the grain faces, thus providing the source term for the grain-face gas behavior module. The latter computes both the fission gas swelling and release through a direct description of the grain-face bubble development, including bubble growth and coalescence (which are reflected in fuel swelling), and eventual inter-connection (leading to thermal FGR). In outline:

- Peculiarities related to the presence of grain edges (where three grains meet) are neglected (e.g., [32, 33]).
- The flux of gas atoms dissolved from the grain faces back to the grain interior by irradiation is neglected [34].
- An initial number density of grain-face bubbles (nucleation centers) is considered, and further nucleation during the irradiation is neglected (one-off nucleation, e.g., [35]).
- The absorption rate of gas at the grain-face bubbles is assumed to equal the arrival rate of gas at the grain faces [35, 36].
- All grain-face bubbles are considered to have, at any instant, equal size and equal lenticular shape of circular projection (e.g., [37]). Hence, the fractional volume grain-face fission gas swelling is given by

$$\left(\frac{\Delta V}{V}\right) = \frac{1}{2} \frac{N_{gf}}{(1/3)r_{gr}} \left(\frac{4}{3} \pi \varphi(\Theta) R_{gf}^3\right) \tag{8.43}$$

where  $N_{gf}$  is the number density of grain-face bubbles per unit surface,  $r_{gr}$  the grain radius,  $\Theta$  the bubble semi-dihedral angle,  $\varphi(\Theta)$  the geometric factor relating the volume of a lenticular-shape bubble to that of a sphere, which is  $1 - 1.5\cos(\Theta) + 0.5\cos^3(\Theta)$ , and  $R_{gf}$  the bubble radius of curvature. The factor 1/2 is introduced in Eq. 8.43 because a grain-face bubble is shared by two neighboring grains.

• Bubble growth is treated using the model of Speight and Beere [38], which describes the growth (or shrinkage) of grain-face bubbles as proceeding by absorption (or emission) of vacancies in grain boundaries, induced by the difference between the pressure of the gas in the bubble, p (Pa), and the mechanical equilibrium pressure,  $p_{eq}$  (Pa). The vacancy absorption/emission rate at a bubble is given by

$$\frac{dn_{v}}{dt} = \frac{(2\pi D_{v}\delta_{g})}{kTS}(p - p_{eq})$$
(8.44)

where  $n_{\nu}$  (-) is the number of vacancies in the bubble,  $D_{\nu}$  (m<sup>2</sup>· s<sup>-1</sup>) the vacancy diffusion coefficient in grain boundaries,  $\delta_g$  (m) the thickness of the diffusion layer in grain boundaries, and the parameter S (-) may be calculated as [35]

$$S = -\frac{1}{4} \left[ (3 - F_c) \cdot (1 - F_c) + 2ln(F_c) \right]$$
 (8.45)

with  $F_c$  being the fraction of grain faces covered by bubbles (fractional coverage). The mechanical equilibrium pressure,  $p_{eq}$ , of the gas in a lenticular bubble of circular projection is given by

$$p_{eq} = \frac{2\gamma}{R_{of}} - \sigma_h \tag{8.46}$$

where  $\gamma$  (J·m<sup>-</sup>2) is the UO<sub>2</sub>/gas specific surface energy,  $R_{gf}$  (m) the bubble radius of curvature, and  $\sigma_h$  (Pa) the hydrostatic stress (considered to be negative if the solid medium is under compression). For describing the bubble thermodynamic state, the Van der Waals' equation of state is adopted in the following form:

$$p(V_{of} - n_o \omega) = n_o kT \tag{8.47}$$

where  $n_g$  (-) is the number of fission gas atoms per bubble, k [J·K<sup>-1</sup>] the Boltzmann constant, T (K) the temperature,  $V_{gf}$  (m<sup>3</sup>) the bubble volume, and  $\omega$  (m<sup>3</sup>) the Van der Waals' volume of a fission gas atom. Given that each bubble consists of vacancies and gas atoms, the volume of a bubble comprising  $n_g$  fission gas atoms and  $n_v$  vacancies is given by

$$V_{gf} = n_g \omega + n_v \Omega_{gf} \tag{8.48}$$

where  $\Omega_{gf}$  (m<sup>3</sup>) is the atomic (vacancy) volume in the bubble. Combination of Eqs. 8.47 and 8.48 gives for the pressure of the gas in the bubble

$$p = \frac{kT}{\Omega_{gf}} \frac{n_g}{n_v} \tag{8.49}$$

The above approach allows computing the bubble growth rate from the rate of inflow of gas atoms along with the rate of absorption (emission) of vacancies at the bubble. The combined effects of gas atom inflow and vacancy absorption (emission) are interactive, since the addition of fission gas atoms gives rise to a change in the bubble pressure via Eq. 8.49, which affects the propensity of the bubble to absorb (or emit) vacancies through Eq. 8.44. Given the volume,  $V_{gf}$ , of a lenticular bubble of circular projection, the bubble radius of curvature is calculated as

$$R_{gf} = \left(\frac{3V_{gf}}{4\pi\varphi(\Theta)}\right)^{\frac{1}{3}} \tag{8.50}$$

• The process of grain-face bubble coalescence, which leads to a progressive decrease of the bubble number density throughout irradiation, is described using an improved model of White [27, 35]. According to this model, the rate of loss of bubbles by coalescence is given by

$$\frac{dN_{gf}}{dt} = -\frac{6N_{gf}^2}{3 + 4N_{gf}A_{gf}} \frac{dA_{gf}}{dt}$$
 (8.51)

where  $N_{gf}$  and  $A_{gf}$  represent the number density and projected area of grain-face bubbles, respectively.

• The release of fission gas to the fuel rod free volume following inter-connection of grainface bubbles and consequent formation of pathways for gas venting to the fuel exterior (thermal release) is modeled based on a principle of grain face saturation. More specifically, a saturation coverage concept is adopted, namely, it is considered that once the fractional coverage,  $F_c$ , attains a saturation value,  $F_{c,sat}$ , the bubble number density and projected area obey the saturation coverage condition

$$F_c = N_{gf} A_{gf} = F_{c,sat} \tag{8.52}$$

where  $N_{gf}$  is the bubble number density and  $A_{gf} = \pi(\sin(\Theta))^2 R_{gf}^2$  is the bubble projected area on the grain face. The commonly accepted value for  $F_{c,sat}$  is 0.5. Eq. 8.52 implies that, after attainment of the saturation coverage, a fraction of the gas reaching the grain faces is released to the fuel exterior to compensate for continuing bubble growth.

#### 8.8.1.3 Athermal gas release

At low temperature, the fission gas in the matrix of the solid is relatively immobile. Only the gas formed at the external surface of the solid is capable of escape, with an emission rate that is independent of temperature. This athermal contribution to FGR arises from the surface-fission

release mechanisms of recoil (direct release of a fission fragment due to its high kinetic energy) and knockout (ejection of a gas atom following elastic interaction with either a primary fragment or energetic particle created in a collision cascade) [39]. These release mechanisms affect only the outer layer of the fuel (within about 10  $\mu$ m from the surface). The rate of gas atom release per unit fuel volume due to recoil and knock-out,  $R_a$  (m<sup>-3</sup>s<sup>-1</sup>), may be calculated as [39]

$$R_a = \frac{yF}{4V} \left( S_g \mu_f + 2S_t \mu_U^{ko} \right) \tag{8.53}$$

where y(I) is the fractional yield of fission gas atoms, F the fission rate density (m<sup>-3</sup>s<sup>-1</sup>), V (m<sup>3</sup>) the volume of fuel,  $S_g$  (m<sup>2</sup>) the geometrical surface area of fuel,  $S_t$  (m<sup>2</sup>) the total surface area of fuel (including cracked surface),  $\mu_f$  (m) the fission fragment range in the fuel, and  $\mu_U^{ko}$  (m) the range of the higher order uranium knock-on in UO<sub>2</sub>.

In line with [40], the number and length of cracks in each fuel pellet is estimated in a simple way. First, radial cracks are considered to cross the outer, brittle region of the fuel pellet with a temperature lower than 1200 C [41]. Second, the number of pellet cracks is considered to increase linearly with fuel linear power [42]. Then, once the linear power and pellet dimensions are given, the total pellet surface area available for athermal gas release can be calculated.

#### 8.8.1.4 Grain growth and grain boundary sweeping

Being the fission gas behavior physically dependent on the granular structure of the fuel, the Sifgrs model is coupled with the grain growth model (Section 8.7). The grain growth phenomenon affects the fission gas release in three ways. First of all, due to the low solubility of the fission gas, the moving grain boundary does not redeposit any gas in the newly-formed crystal behind it, thus acting as a filter and contributing to the collection of gas at the grain faces ( $grain\ bound$  $ary\ sweeping$ ). This effect is taken into account in Sifgrs by adding a supplementary fractional release term (f) from within the grains to the grain faces that is equal to the volume fraction of the fuel swept by the moving boundaries:

$$f = \frac{r_i^3 - r_{i-1}^3}{r_i^3} \tag{8.54}$$

where the indices i-1 and i refer to the previous and current time, respectively. Secondly, the diffusion distance for the fission gas atoms created in the grains increases as the grains grow. Unlike the first consequence this tends to reduce the release rate. Thirdly, grain growth reduces the capacity of the grain boundaries to store fission gas, as it results in a decrease of the total grain surface-to-volume ratio.

#### 8.8.2 Modified Forsberg-Massih Fission Gas Release Model

As an additional option, fission gas release (FGR) can be computed based on the traditional Forsberg-Massih model (ForMas) [43]. This model considers FGR only, hence the fission gas swelling must be calculated separately by means of an empirical model (see Section 8.2).

ForMas incorporates a two-stage approach to predict gas release. The first stage computes diffusion of fission gas atoms from within the fuel grains to the grain boundaries, by solving numerically the relevant diffusion equation in spherical co-ordinates. An effective diffusion coefficient is employed, which accounts for gas atom resolution from and trapping into intra-granular bubbles. A formulation based on Turnbull et al. [44, 45] is used to calculate the single gas atom diffusion coefficient, and correction for the effects of intra-granular bubbles is modeled based on the correlations reported in [28]. The second stage of the model utilizes time-dependent boundary conditions to determine grain boundary gas accumulation as inter-granular lenticular bubbles, resolution, saturation, and release. FGR from the grain boundaries is controlled using a grain boundary saturation criterion that involves a threshold concentration of gas at the grain boundaries.

For the current implementation, the fuel grains are assumed to be constant in diameter, thus grain growth and grain-boundary sweeping effects are not considered. Further, the model describes a smooth continuous release process, and is thus not applicable to sudden releases or bursts. These are significant limitations, which must be alleviated to provide more realistic FGR predictions. Accordingly, a more mechanistic model is currently being implemented in BISON which considers the structure of both the fuel (fuel grains and pores) and grain boundaries, and includes the effects of grain growth and grain boundary sweeping. This model will be directly coupled to the volumetric swelling calculation, thus replacing the empirical model described in Eq. 8.22.

Following [46], the ForMas model implemented in BISON includes some modifications compared to the original Forsberg-Massih [43] model, namely:

• The following three-term formulation, based on Turnbull et al. [44, 45], is used to calculate the single gas atom diffusion coefficient

$$D_{atomic} = D_1 + D_2 + D_3$$

$$D_1 = 7.6 \cdot 10^{-10} \cdot exp\left(-\frac{35250}{T}\right)$$

$$D_2 = 1.41 \cdot 10^{-25} \sqrt{\dot{F}} \cdot exp\left(-\frac{13800}{T}\right) \cdot 4.0$$

$$D_3 = 2.0 \cdot 10^{-40} \cdot \dot{F}$$
(8.55)

where T (K) is the temperature and  $\dot{F}$  (m<sup>-3</sup>·s<sup>-1</sup>) is the fission rate.

- The rate of gas atom resolution from the grain boundaries back into the grains is scaled by fission rate, in line with [28].
- Instead of assuming release of the total gas inventory at the grain boundaries upon saturation [43], only the gas above the saturation level is considered to be released.

The modified Forsberg-Massih model implemented in BISON was tested using a single LWR fuel pellet, assuming uniform constant power. Typical input parameters for UO<sub>2</sub> fuel, as shown

in Table 8.1, were assumed. Calculations were compared to the well known Vitanza or Halden threshold [47], which correlates a large set of FGR data in terms of fuel centerline temperature versus burnup at roughly one percent gas release; this threshold is often used to evaluate and calibrate FGR models. A typical comparison is shown in Figure 8.10, which considers the effect of hydrostatic pressure on the computed gas release. Symbols in the figure indicate individual simulations at various axial power levels. As has been reported earlier [48], an increase in hydrostatic pressure significantly shifts the onset of gas release to higher burnups.

Table 8.1: Input parameters for the modified Forsberg-Massih fission gas release model

1 1	_	_
Fuel grain radius (m)		$1.0 \times 10^{-5}$
Frac. yield of fission gas atoms per	fission	0.3017
Reference resolution rate of intergra	anular gas (s <sup>-1</sup> )	$1.0 \times 10^{-7}$
Resolution layer depth (m)		$1.0 \times 10^{-8}$
Grain boundary bubble radius (m)		$0.5 \times 10^{-6}$
Nonspherical bubble shape factor [A	/]	0.287
Bubble surface tension (J/m <sup>2</sup> )		0.626
Grain boundary frac. coverage at sa	aturation [/]	0.5

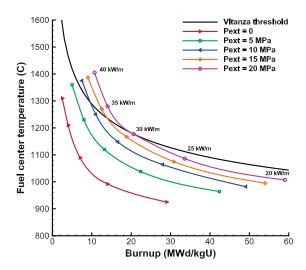


Figure 8.10: Effect of hydrostatic pressure on centerline temperature versus burnup for 1 percent average fission gas release. The Vitanza threshold [47] is included for comparison.

# 9 Clad Material and Behavioral Models

Focusing initially on Zircaloy clad material, models have been implemented for irradiation creep, primary and secondary thermal creep, irradiation growth and damage.

## 9.1 Irradiation Creep

Irradiation-induced creep of cladding materials is based on an empirical model developed by Hoppe [49] that relates the creep rate to the current fast neutron flux and stress. The specific relation implemented is:

$$\dot{\varepsilon}_{ir} = C_0 \Phi^{C_1} \sigma_m^{C_2} \tag{9.1}$$

where  $\dot{\epsilon}_{ir}$  is the effective irradiation creep rate (1/s),  $\Phi$  is the fast neutron flux (n/m<sup>2</sup>-s),  $\sigma_m$  is the effective (Mises) stress (MPa), and  $C_0$ ,  $C_1$ , and  $C_2$  are material constants. Note that the original Hoppe formulation is given in terms of circumferential stress, whereas the relation implemented in BISON assumes an effective (Mises) stress.

## 9.2 Thermal Creep

Two thermal creep models are available. The Hayes model describes only secondary creep while the Limback model includes both primary and secondary creep.

#### 9.2.1 Hayes Secondary Creep

Secondary thermal creep of zirconium alloys was thoroughly investigated by Hayes and Kassner [50] and found to be well-described by a traditional power-law creep formulation. The specific equation recommended there and implemented in BISON is

$$\dot{\varepsilon}_{ss} = A_0 \left(\frac{\sigma_m}{G}\right)^n e^{\left(\frac{-Q}{RT}\right)} \tag{9.2}$$

where  $\dot{\mathbf{e}}_{ss}$  is the effective thermal creep rate (1/s),  $\sigma_m$  is the effective (Mises) stress (Pa), Q is the activation energy (J/mol), R is the universal gas constant (J/mol-K), T is the temperature (K), G is the shear modulus (Pa), and  $A_0$  and n are material constants. For Zr-4, Moon et al. [51] recommend a temperature dependent shear modulus given by  $G = 4.2519 \times 10^{10} - 2.2185 \times 10^7 T$  and Hayes and Kassner [50] specify a creep law power (n) of 5. A value for  $A_0$  is not reported in [50]; however, based on experimental data presented there, an approximate value of  $A_0 = 3.14 \times 10^{24}$  (1/s) was computed.

#### 9.2.2 Limbäck Primary and Secondary Creep

The creep model proposed by Limbäck [52] includes an expression for primary creep. This can be important as part of power changes when the load on the cladding changes relatively suddenly.

Thermal creep in the Limbäck model is given as the Matsuo model [53] where the creep rate  $(hr^{-1})$  is

$$\dot{\varepsilon}_{th} = A \frac{E}{T} \left( \sinh \frac{a_i \sigma_{eff}}{E} \right)^n e^{-Q/RT}$$
(9.3)

$$a_i = a \left[ 1 - A_1 \left( 1 - e^{(-A_2 \Phi^{A_3})} \right) \right] \tag{9.4}$$

$$E = 1.148 \times 10^5 - 59.9T \tag{9.5}$$

with  $A = 1.08 \times 10^9$  (K/MPa/hr), T as temperature (K), Q = 201 (kJ/mol), a = 650 (dimensionless), R = 8.314 (J/mol/K), N = 2 (dimensionless), a = 650 (dimensionless),  $A_1 = 0.56$  (dimensionless),  $A_2 = 1.4 \times 10^{-27}$  ((n/cm<sup>2</sup>)<sup>-A<sub>3</sub></sup>), and  $A_3 = 1.3$  (dimensionless).

Irradiation-induced creep in the Limbäck model is of the form given in Eq. 9.1. The secondary creep rate is then

$$\dot{\varepsilon}_s = \dot{\varepsilon}_{th} + \dot{\varepsilon}_{ir}. \tag{9.6}$$

Primary creep is defined as

$$\varepsilon_p = \varepsilon_p^s \left( 1 - e^{(-C\sqrt{\hat{\varepsilon}_s t})} \right) \tag{9.7}$$

$$\varepsilon_p^s = B\dot{\varepsilon}_s^b \left[ 2 - \tanh(D\dot{\varepsilon}_s) \right]^d \tag{9.8}$$

where C = 52 (dimensionless), B = 0.0216 (hr<sup>b</sup>), b = 0.109 (dimensionless), D = 35500 (hr), and d = -2.05 (dimensionless).

Total creep strain is the combination of the primary and secondary creep:

$$\varepsilon_c = \varepsilon_p^s \left( 1 - e^{(-C\sqrt{\hat{\varepsilon}_s t})} \right) + \dot{\varepsilon}_s t. \tag{9.9}$$

## 9.3 Combined Creep and Instantaneous Plasticity

A material model is also available for combined instantaneous plasticity and time-dependent creep. Creep is modeled using the irradiation and thermal creep constitutive equations described above (Eqns. 9.1 and 9.2). Time-independent plasticity is modeled assuming J2 plasticity based on a simple linear strain hardening curve. For each stress update, the model first consideres only the creep contribution to compute a new stress, which is then compared to the yield strength. If above yield, instantaneous plasticity is applied to reduce the stress onto the yield curve. Iteration is employed to insure stress convergence.

### 9.4 Irradiation Growth

A model for irradiation growth of Zr4 cladding is available. It is taken from the ESCORE model (see [19], Volume 1: Theoretical and Numerical Bases, section 5.3.4). The axial strain is given as

$$\varepsilon = A(\phi t)^n \tag{9.10}$$

where A and n are constants and  $\phi t$  is fast neutron fluence. The value for A is  $3 \times 10^{-20}$  N/cm<sup>2</sup>. The value for n is 0.794. We generate a strain increment for the irradiation growth as

$$\Delta \varepsilon = A \left( (\phi t_i)^n - (\phi t_{i-1})^n \right) \tag{9.11}$$

with *i* representing the current step number.

Since irradiation growth should occur in the axial direction only while being volume conserving, it is necessary to specify a strain increment for the other two directions. This is given by

$$\Delta \varepsilon_{lateral} = -(1 - (1 + \Delta \varepsilon)^{-0.5}) \tag{9.12}$$

## 9.5 Damage

Intergranular stress corrosion cracking, typically caused by pellet-clad interaction (PCI), can lead to clad failure during normal operation. A cumulative damage model by Rashid [54] is used in BISON to estimate clading damage for low temperature steady-state conditions. The model is based on the notion of a cumulative damage index, which has the following form.

$$D = \int_0^{t_n} \frac{dt}{t_f(\sigma_{\text{hoop}}, B, T)}$$
(9.13)

In Eq.9.13, D is the amount of damage at time  $t_n$  (all time in seconds),  $t_f$  is the failure time at stress  $\sigma_{\text{hoop}}$  (all stress in units of MPa), T is temperature (K), and B is burnup (MWd/MTU). The variable  $t_f$  has the form:

$$t_f = \bar{t} \exp[(1.015\sigma_v + 1.74\sigma_{ref} - 2.755\sigma_{hoop})0.01]$$
 (9.14)

where  $\sigma_{v}$  is the clad yield stress, and

$$\bar{t} = 5 \times 10^5 (1.13 \times 10^{-4} B - 0.13)^{-0.75} exp[-30(1 - 611/T)]$$
 (9.15)

where the stress  $\sigma_{ref}$  is a threshold stress, which has the form:

$$\sigma_{\text{ref}} = \begin{cases} 336.476(B - 5000)^{-0.07262} & \text{for Zr2} \\ 310.275(B - 5000)^{-0.0440} & \text{for Zr4.} \end{cases}$$
(9.16)

The model for cumulative damage index (Eq.9.13) activates only when  $\sigma_{hoop} > \sigma_{ref}$  and B > 5000 MWd/MTU.

## 10 Other Material Models

## 10.1 Pyrolitic Carbon

Pyrolitic carbon experiences irradiation-induced strain which is a function of fluence. For low-density pyrolitic carbon, such as that used in the buffer layer of a TRISO fuel particle, the irradiation strain is given by [55] as

$$\dot{\varepsilon}_r = \dot{\varepsilon}_{\theta} = -0.176 \, e^{(-1.75\Phi)}$$
 (10.1)

where  $\dot{\epsilon}$  is in units of  $1/(10^{25} n/m^2)$  and  $\Phi$ , the fluence, is in units of  $10^{25} n/m^2$ .

For dense pyrolitic carbon, the irradiation strain differs in the radial and tangential directions [55] of a TRISO particle:

$$\dot{\varepsilon}_r = -0.077 \, e^{(-\Phi)} + 0.031 \tag{10.2}$$

$$\dot{\varepsilon}_{\theta} = -0.036 \, e^{(-2.1\Phi)} - 0.01. \tag{10.3}$$

The irradiation creep correlation is taken from [55] and [56]. With K as the creep constant,  $\sigma_i$  as one component of the principal stress,  $\nu_c$  as the Poisson ratio for creep, and  $\dot{\Phi}$  as the fast neutron flux, the creep rate is given as

$$\dot{\mathbf{\epsilon}}_1 = K[\mathbf{\sigma}_1 + \mathbf{v}_c(\mathbf{\sigma}_2 + \mathbf{\sigma}_3)]\dot{\mathbf{\Phi}}.\tag{10.4}$$

The value of  $v_c$  is 0.5. K is

$$K = K_0[1 + 2.38(1.9 - \rho)]M_{Irr,Creep}$$
(10.5)

where

$$K_0 = 1.996 \times 10^{-29} - 4.415 \times 10^{-32}T + 3.6544 \times 10^{-35}T^2$$
 (10.6)

and with  $M_{\rm Irr,Creep} = 2$ ,  $\rho$  in g/cm<sup>3</sup> and T in C. At the expense of inverting a 3 × 3 matrix, it is possible to determine the creep strain increment in an implicit fashion, allowing arbitrarily large time steps without unstable creep response.

## 10.2 SiC Irradiation Creep

The model for irradiation creep of silicon carbide (SiC) is taken as (see [57]):

$$\dot{\varepsilon}_{cr} = K \sigma \phi \tag{10.7}$$

where  $\dot{\varepsilon}_{cr}$  is the irradiation creep rate, K is a temperature-dependent conversion factor (Pa-n/m<sup>2</sup>)<sup>-1</sup>,  $\sigma$  is the stress, and  $\phi$  is the flux.

The reference mentioned above gives K as  $2 \times 10^{-37}$  (Pa-n/m<sup>2</sup>)<sup>-1</sup> at 640° C and  $4 \times 10^{-37}$  (Pa-n/m<sup>2</sup>)<sup>-1</sup> at 900° C. However, a figure in that reference seems to indicate that typical values for K are about one-tenth those mentioned in the text. Little creep data for SiC is available at lower temperatures.

## 10.3 HT9 Thermal Properties

Thermal conductivity k (W/m-K) of HT9 is from [58]:

$$k = 17.622 + 2.42 \times 10^{-2} T - 1.696 \times 10^{-5} T^2,$$
  $T < 1030 \text{ K}$  (10.8)

$$k = 12.027 + 1.218 \times 10^{-2} T,$$
  $T \ge 1030 \text{ K}$  (10.9)

Specific heat  $C_p$  (J/kg-K) of HT9 is from [59]:

$$C_p = (T - 500)/6 + 500,$$
  $T < 800 \text{ K}$  (10.10)

$$C_p = 3(T - 800)/5 + 550,$$
  $T \ge 800 \text{ K}$  (10.11)

## 10.4 HT9 Mechanical Properties

Young's modulus (MPa) and Poisson's ratio for HT9 are reported by [60].

$$E = 234468.6944 - 79.65914T - 0.0131706T^2$$
 (10.12)

$$v = 0.221956 + 2.643235 \times 10^{-4} T - 2.028888 \times 10^{-7} T^2$$
 (10.13)

Linear thermal expansion coefficient (%) [58] is:

$$\Delta L/L = -0.2191 + 5.678 \times 10^{-4} T + 8.111 \times 10^{-7} T^2 - 2.576 \times 10^{-10} T^3$$
 (10.14)

T is temperature in K.

## 10.5 HT9 Thermal and Irradiation Creep

Thermal and irradiation creep models and material properties from [61] are used for the HT9 model. The following equation is for secondary creep.

$$\dot{\varepsilon}_{cr} = C_5 \exp(-\frac{Q_4}{RT})\bar{\sigma}^2 + C_6 \exp(-\frac{Q_5}{RT})\bar{\sigma}^5 + [B_o + A\exp(-\frac{Q}{RT})]\phi\bar{\sigma}^{1.3}$$
(10.15)

Where:

$$C_5 = 1.17 \times 10^9$$

$$C_6 = 8.33 \times 10^9$$

 $Q_4 = 83142 \text{ (Cal/g-mol)}$ 

 $Q_5 = 108276$  (Cal/g-mol)

$$B_o = 1.83 \times 10^{-4}$$

$$A = 2.59 \times 10^{14}$$

Q = 73000 (Cal/g-mol)

R = 1.987 (Cal/g-mol)

T = Temperature (K)

 $\phi = \text{Neutron Flux}(10^{22} \text{ n/cm}^2/\text{s})$ 

 $\bar{\sigma} = \text{Effective stress (MPa)}$ 

 $\dot{\epsilon}_{cr}$  = Effective Thermal and Irradiation Creep Strain Rate (%/s)

#### 10.6 Mass Diffusion Coefficients

Mass diffusion coefficients are defined using an Arrhenius form [62]

$$D(T) = \sum_{i} D_{0,i} \exp\left(\frac{-Q_i}{RT}\right)$$
 (10.16)

where  $D_{0,i}$  is a pre-exponential factor and  $Q_i$  is the activation energy.

## 10.7 U<sub>3</sub>Si<sub>2</sub> Thermal Properties

Using experimental data from figure 4 of [63], a conservative expression for thermal conductivity k (W/m-K) of arc cast U<sub>3</sub>Si<sub>2</sub> pellets is obtained:

$$k = 7.98 + 0.0051 \times (T - 273.15)$$
 (10.17)

where T is temperature in K. This expression is valid for temperatures from room temperature to 1473.15 K. This expression may underestimate the true thermal conductivity of  $U_3Si_2$ .

Specific heat  $C_p$  (J/kg-K) of U<sub>3</sub>Si<sub>2</sub> is taken from [64]:

$$C_p = 199 + 0.104 \times (T - 237.15)$$
 (10.18)

where T is temperature in K. The reference does not state the validity range of this expression.

# 11 Power, Burnup, and Related Models

## 11.1 Power

The power associated with an LWR fuel rod is typically given as rod averaged linear power (or linear heat rate) in units of W/m. This power varies in time and space. The axial variation in power is given as a scaling factor as a function of distance from the bottom of the rod.

#### 11.1.1 Radial Power Profile

The power density in a fuel pellet varies radially as a function of geometry, initial fuel characteristics, and irradiation history. With increasing burnup, the concentration of Pu toward the outer rim is relatively high, resulting in a local power density that can be 2-3 times that found elsewhere in the pellet. This variation needs to be captured in order to calculate the heat generation and temperature distribution in the pellet accurately.

BISON uses the TUBRNP model of Lassmann ([65]; see also [19]). In this model, the average isotope concentrations are

$$\frac{d\overline{N}_{235}}{dt} = -\sigma_{a,235}\overline{N}_{235}\phi,$$

$$\frac{d\overline{N}_{238}}{dt} = -\sigma_{a,238}\overline{N}_{238}\phi,$$
(11.1a)

$$\frac{d\overline{N}_{238}}{dt} = -\sigma_{a,238}\overline{N}_{238}\phi, \tag{11.1b}$$

$$\frac{\mathrm{d}t}{\mathrm{d}t} = -\sigma_{a,j}\overline{N}_{j}\phi + \sigma_{c,j-1}\overline{N}_{j-1}\phi, \tag{11.1c}$$

where  $\overline{N}$  is the number of atoms per unit volume,  $\sigma_a$  is the absorption cross section,  $\sigma_c$  is the capture cross section, φ is the neutron flux, and j represents each of the <sup>239</sup>Pu, <sup>240</sup>Pu, <sup>241</sup>Pu, and <sup>242</sup>Pu isotopes.

Recognizing the relationship between an increment of fluence ( $\phi \Delta t$ ) and an increment of burnup ( $\Delta$ bu), these equations can be reformed as

$$\frac{d\overline{N}_{235}}{dbu} = -\sigma_{a,235}\overline{N}_{235}A,$$

$$\frac{d\overline{N}_{238}}{dbu} = -\sigma_{a,238}\overline{N}_{238}A,$$
(11.2a)

$$\frac{d\overline{N}_{238}}{dbu} = -\sigma_{a,238}\overline{N}_{238}A,\tag{11.2b}$$

$$\frac{d\overline{N}_{j}}{dbu} = -\sigma_{a,j}\overline{N}_{j}A + \sigma_{c,j-1}\overline{N}_{j-1}A, \qquad (11.2c)$$

where

$$A = 0.8815 \frac{\rho_{fuel}}{\alpha \sum_{k} \sigma_{f,k} \overline{N}_{k}}.$$
(11.3)

The leading coefficient (0.8815) is the ratio of the mass of U in UO<sub>2</sub> to the mass of UO<sub>2</sub> (238/270). Burnup here is in units of megawatt days per ton heavy metal.  $\sigma_f$  is the fission cross section, and  $\alpha$  is the energy released per fission.

The local isotope concentrations are model using

$$\frac{dN_{235}}{dbu} = -\sigma_{a,235}N_{235}(r)A, \tag{11.4a}$$

$$\frac{dN_{235}}{dbu} = -\sigma_{a,235}N_{235}(r)A,$$
(11.4a)
$$\frac{dN_{238}}{dbu} = -\sigma_{a,238}\overline{N}_{238}\overline{f}(r)A,$$
(11.4b)
$$\frac{dN_{239}}{dbu} = -\sigma_{a,239}N_{239}(r)A + \sigma_{c,238}\overline{N}_{238}\overline{f}(r)A,$$
(11.4c)

$$\frac{dN_{239}}{dhu} = -\sigma_{a,239}N_{239}(r)A + \sigma_{c,238}\overline{N}_{238}\overline{f}(r)A, \tag{11.4c}$$

$$\frac{dN_j}{dbu} = -\sigma_{a,j}N_j(r)A + \sigma_{c,j-1}N_{j-1}(r)A,$$
(11.4d)

where j represents each of the <sup>240</sup>Pu, <sup>241</sup>Pu, and <sup>242</sup>Pu isotopes. The function  $\overline{f}(r)$  is given as

$$\overline{f}(r) = \frac{f(r)}{\int_{r_{in}}^{r_{out}} f(r) r \, \mathrm{d}r}$$
(11.5)

which guarantees that

$$\frac{2\int_{r_{in}}^{r_{out}} \overline{f}(r)r \, \mathrm{d}r}{r_{out}^2 - r_{in}^2} = 1. \tag{11.6}$$

The function f(r) is given as

$$f(r) = 1 + p_1 e^{-p_2(r_{out} - r)^{p_3}}$$
(11.7)

where  $p_1$ ,  $p_2$ , and  $p_3$  are constants,  $r_{out}$  is the outer radius of the pellet, and r is the radial position.

The neutron flux,  $\phi(r)$ , is a function of the modified Bessel functions:

$$\phi(r) = C_1 I_0(\kappa r) \tag{11.8a}$$

for a solid cylindrical pellet, or

$$\phi(r) = C_1 \left( I_0(\kappa r) + \left[ \frac{I_1(\kappa r_{in})}{K_1(\kappa r_{in})} \right] K_0(\kappa r) \right)$$
(11.8b)

for a hollow cylindrical pellet

where I and K are the modified Bessel functions,  $C_1$  is a constant, and  $\kappa$  is the inverse diffusion length. k is given as

$$\kappa = \sqrt{\frac{\sum_{a,tot}}{D}} \tag{11.9}$$

where

$$\sum_{a,tot} = \sum_{k} \sigma_{a,k} \overline{N}_{k}$$

and

$$D = \frac{1}{3\sigma_s \overline{N}_{tot}}.$$

 $\overline{N}_k$  is the average concentration for each isotope,  $\overline{N}_{tot}$  is the average concentration of all isotopes, and  $\sigma_s$  is a constant.

Standard cross section values are given in Table 11.1. By default, BISON uses these fission and capture cross section values. For the absorption cross section values, BISON follows the approach in FRAPCON and sums the fission and capture cross section values for each isotope to get the absorption cross section. Note also that no support for Gd content is available at this time.

Table 11.1: Spectrum average cross sections for the TUBRNP model (in barns). See [19].

Light Water Reactor (BWR and PWR)									
	$^{235}U$	$^{238}U$	<sup>239</sup> Pu	<sup>240</sup> Pu	<sup>241</sup> Pu	<sup>242</sup> Pu	<sup>155</sup> Gd	$^{157}$ Gd	
Fission	41.5	0	105	0.584	120	0.458	-	-	
Capture	9.7	0.78	58.6	100	50	80	490	1267	
Absorption (Thermal)	359.68	1.56	1207.5	193.5	1095.24	11.11	19800	85000	
Heavy Water Reactor									
	$^{235}U$	$^{238}U$	<sup>239</sup> Pu	<sup>240</sup> Pu	<sup>241</sup> Pu	<sup>242</sup> Pu	<sup>155</sup> Gd	<sup>157</sup> Gd	
Fission	107.95	0	239.18	0.304	296.95	0.191	-	-	
Capture	22.3	1.16	125.36	127.26	122.41	91.3	1471	3800	
Absorption (Thermal)	395.59	1.7	1095.7	202.2	1113.7	11.98	23924	102477	

As a benchmark problem, a comparison between BISON and FRAPCON radial power factors has been made for a simple fuel pellet. In this problem, the fuel outer diameter is 8.2 mm, the linear power is 20 kW/m, and the fuel is 5% enriched with 95% theoretical density. Figure 11.1 shows the radial power factor at the beginning of the irradiation. Figure 11.2 shows the radial power factor at 33 MWd/kgU. BISON shows excellent agreement with the FRAPCON results.

## 11.2 Decay Heat

Heat generation due to the radioactive decay of fission products is computed using the "simplified method" described in the 1979 ANS-5.1 Standard on Decay Heat Power in Light Water Reactors [66]. This method assumes that the decay heat power from fissioning isotopes other than  $^{235}U$  is identical to that of  $^{235}U$  and that the fission rate is constant over the operating history at a maximum level corresponding to  $P_{max}$ . This simplified method overestimates decay heat power, especially with respect to LWR cores having an appreciable amount of plutonium. For finite reactor operating time, the decay heat power is approximated as

$$P_d(t,T) = P_{max} \frac{1.02G_n (F(t,\infty) - F(t+T,\infty))}{Q_{mev}}$$
(11.10)

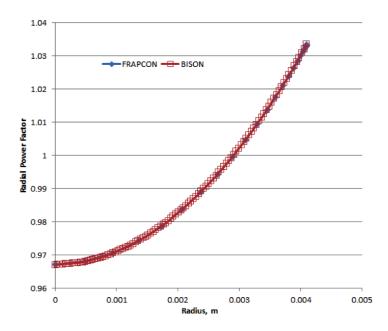


Figure 11.1: BISON and FRAPCON radial power factors for new fuel.

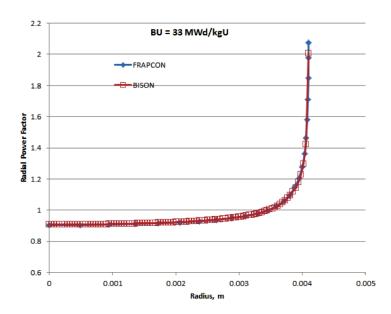


Figure 11.2: BISON and FRAPCON radial power factors at 33 MWd/kgU.

where t is the time following reactor shutdown (s), T is the total operating time including intermediate periods at zero power (s),  $G_n$  is the neutron capture factor,  $Q_{mev}$  is the energy released per fission (MeV/fission), and  $F(t,\infty)$  is the decay heat power (MeV/fission) for thermal fission

of  $^{235}U$  for an infinite-time base irradiation (tabulated in Table 4 of [66]).

As implemented in BISON, the decay and peak powers are prescribed as fission power densities at finite element material volumes. Spatial variation of the peak power is dictated by the axial and radial power profiles in the fuel, thus the decay power follows the same profiles.

## 11.3 Burnup Calculation

Burnup is used to calculate fuel properties and the fuel densification and swelling rates. It is computed at each material or integration point based on the following equation from Olander [41]

$$\beta = \frac{\dot{F}t}{N_f^0} \tag{11.11}$$

where  $\dot{F}$  is the volumetric fission rate, t is time, and  $N_f^0$  is the initial density of heavy metal atoms in the fuel, which can be computed as

$$N_f^0 = \frac{\rho N_{av}}{M_w} \tag{11.12}$$

where  $\rho$  is the initial fuel density,  $N_{av}$  is Avagrado's number, and  $M_w$  is the molecular weight. A burnup increment is computed for each time increment and summed to give the total burnup.

$$\beta_i = \beta_{i-1} + \frac{\dot{F}\Delta t}{N_f^0} \tag{11.13}$$

### 11.4 Fission Rate

The fission rate is calculated from the local power density.

$$\dot{F} = \frac{P}{\alpha} \tag{11.14}$$

where  $\dot{F}$  is the fission rate (fission/m<sup>3</sup>/s), P is the power density (W/m<sup>3</sup>), and  $\alpha$  is the energy released per fission (J/fission).  $\alpha$  is commonly taken to be 3.28451e-11 J/fission.

#### 11.5 Fast Neutron Flux

Fast neutron flux may be specified as problem input. However, it may also be estimated given the linear heat rate.

$$\dot{\Phi} = cP \tag{11.15}$$

where  $\dot{\Phi}$  is the fast neutron flux, c is a conversion factor, typically 3e13 (n/(m<sup>2</sup>s)/(W/m)), and P is the linear heat rate (W/m).

## 11.6 Fast Neutron Fluence

Fast neutron fluence is the time-integrated fast neutron flux. In incremental form,

$$\Phi_{n+1} = \Phi_n + \Delta t \dot{\Phi} \tag{11.16}$$

where  $\Phi_n$  is the value of the fast neutron fluence at step n,  $\Delta t$  is the timestep size, and  $\dot{\Phi}$  is the fast neutron flux.

# 12 Evolving Density

BISON computes the current density throughout the finite element mesh. Conservation of mass requires

$$\rho = \frac{\rho_0 V_0}{V} \tag{12.1}$$

where  $\rho$  and  $\rho_0$  are the current and original mass densities, and V and  $V_0$  are the current and original volumes.

The deformation gradient F is defined as

$$F = I + \nabla u \tag{12.2}$$

where I is the identity tensor and u is the displacement vector. The determinant of the deformation gradient is a measure of volume change:

$$\det(F) = \frac{dV}{dV_0}. (12.3)$$

This allows

$$\rho = \frac{\rho_0}{\det(F)}.\tag{12.4}$$

This calculation is done at each integration point throughout the finite element mesh.

# 13 Gap/Plenum Models

## 13.1 Gap Heat Transfer

Gap heat transfer is modeled using the relation,

$$h_{gap} = h_g + h_s + h_r \tag{13.1}$$

where  $h_{gap}$  is the total conductance across the gap,  $h_g$  is the gas conductance,  $h_s$  is the increased conductance due to solid-solid contact, and  $h_r$  is the conductance due to radiant heat transfer.

The gas conductance  $h_g$  is described using the form proposed by Ross and Stoute [67]:

$$h_g = \frac{k_g(T_g)}{d_g + C_r(r_1 + r_2) + g_1 + g_2}$$
 (13.2)

where  $k_g$  is the conductivity of the gas in the gap,  $d_g$  is the gap width (computed in the mechanics solution),  $C_r$  is a roughness coefficient with  $r_1$  and  $r_2$  the roughnesses of the two surfaces, and  $g_1$  and  $g_2$  are jump distances at the two surfaces. The conductivity of the gas mixture  $(k_g)$  is computed based on the mixture rule from MATPRO [21], which permits mixtures of ten gases (helium, argon, krypton, xenon, hydrogen, nitrogen, oxygen, carbon monoxide, carbon dioxide, and water vapor). The gas temperature is the average of the local temperatures of the two surfaces.

Temperature jump distance is calculated using Kennard's model based on a review by Lanning [68].

$$g_1 + g_2 = 5756 \left(\frac{2 - a_{mix}}{a_{mix}}\right) \left(\frac{k_g \sqrt{T_g}}{P}\right) \left(\sum_{i=1}^{10} \frac{f_i}{M_i}\right)^{-1/2}$$
(13.3)

where  $f_i$  is mole fraction of i-th gas species,  $M_i$  is moleular weight of i-th gas species, and  $a_{mix}$  is accommodation coefficient for the gas mixture. The accommodation coefficients for helium and xenon are as follows:

$$a_{He} = 0.425 - 2.3 \times 10^{-4} T_{g} \tag{13.4}$$

$$a_{Xe} = 0.749 - 2.5 \times 10^{-4} T_g \tag{13.5}$$

For a gas mixture,

$$a_{mix} = a_{He} + \frac{(a_{Xe} - a_{He})(M_{mix} - M_{He})}{(M_{Xe} - M_{He})}$$
(13.6)

where  $M_{Xe}$  is molecular weight of xenon,  $M_{He}$  is molecular weight of helium, and  $M_{mix}$  is molecular weight of gas mixture.

The increased conductance due to solid-solid contact,  $h_s$ , is described using the correlation suggested by Ross and Stoute [67]:

$$h_s = C_s \frac{2k_1 k_2}{k_1 + k_2} \frac{P_c}{\delta^{1/2} H}$$
 (13.7)

where  $C_s$  is an empirical constant,  $k_1$  and  $k_2$  are the thermal conductivities of the solid materials in contact,  $P_c$  is the contact pressure,  $\delta$  is the average gas film thickness (approximated as  $0.8(r_1 + r_2)$ , and H is the Meyer hardness of the softer material. From measurements on steel in contact with aluminum, Ross and Stoute [67] recommend  $C_s = 10 \ m^{-1/2}$ , which is the default value in BISON.

The conductance due to radiant heat transfer,  $h_r$ , is computed using a diffusion approximation. Based on the Stefan-Boltzmann law

$$q_r = \sigma F_e(T_1^4 - T_2^4) \approx h_r(T_1 - T_2) \tag{13.8}$$

where  $\sigma$  is the Stefan-Boltzmann constant,  $F_e$  is an emissivity function, and  $T_1$  and  $T_2$  are the temperatures of the radiating surfaces. The radiant conductance is thus approximated

$$h_r \approx \frac{\sigma F_e (T_1^4 - T_2^4)}{T_1 - T_2} \tag{13.9}$$

which can be reduced to

$$h_r = \sigma F_e(T_1^2 + T_2^2)(T_1 + T_2) \tag{13.10}$$

For infinite parallel plates, the emissivity function is defined as

$$F_e = \frac{1}{1/\epsilon_1 + 1/\epsilon_2 - 1} \tag{13.11}$$

where  $\varepsilon_1$  and  $\varepsilon_2$  are the emissivities of the radiating surfaces. This is the specific function implemented in BISON.

#### 13.2 Mechanical Contact

Mechanical contact between fuel pellets and the inside surface of the cladding is based on three requirements:

$$g \le 0, \tag{13.12}$$

$$t_N \ge 0,\tag{13.13}$$

$$t_N g = 0. (13.14)$$

That is, the penetration distance (typically referred to as the gap g in the contact literature) of one body into another must not be positive; the contact force  $t_N$  opposing penetration must be positive in the normal direction; and either the penetration distance or the contact force must be zero at all times.

In BISON, these contact constraints are enforced through the use of node/face constraints. Specifically, the nodes of the fuel pellets are prevented from penetrating cladding faces. This is accomplished in a manner similar to that detailed by Heinstein and Laursen [69]. First, a geometric search determines which fuel pellet nodes have penetrated cladding faces. For those nodes, the internal force computed by the divergence of stress is moved to the appropriate cladding face at the point of contact. Those forces are distributed to cladding nodes by employing the finite element shape functions. Additionally, the pellet nodes are constrained to remain on the pellet faces, preventing penetration. BISON supports frictionless and tied contact. Friction is an important capability, and preliminary support for frictional contact is available.

Finite element contact is notoriously difficult to make efficient and robust in three dimensions. That being the case, effort is underway to improve the contact algorithm.

## 13.3 Gap/plenum pressure

The pressure in the gap and plenum is computed based on the ideal gas law,

$$P = \frac{nRT}{V} \tag{13.15}$$

where P is the gap/plenum pressure, n is the moles of gas, R is the ideal gas constant, T is the temperature, and V is the volume of the cavity. The moles of gas, the temperature, and the cavity volume in this equation are free to change with time. The moles of gas n at any time is the original amount of gas (computed based on original pressure, temperature, and volume) plus the amount in the cavity due to fission gas released. The temperature T is taken as the average temperature of the pellet exterior and cladding interior surfaces, though any other measure of temperature could be used. The cavity volume V is computed as needed based on the evolving pellet and clad geometry.

## 13.4 Gap/plenum temperature

The gap/plenum pressure (Section 13.3) requires the temperature of the gas inside the cladding. Many choices are possible when supplying this temperature. It may be appropriate to supply the temperature at a node, the average temperature of several nodes, or data from an experiment. In this section, we outline an approach for calculating an average gas temperature that takes into account the entire fuel/cladding system.

We seek a weighted average temperature that accounts for the fact that the majority of the gas is in the plenum region. Using a volume-weighted average, the average gas temperature  $\bar{T}$  can be approximated as

$$\bar{T} = \frac{\int T \, \mathrm{d}V}{\int \, \mathrm{d}V} \tag{13.16}$$

where T is the temperature at a point in the gap/plenum and V is the volume occupied by the gas.

It is necessary to make some approximations in the calculation of this temperature since the gap and plenum volumes are not meshed. We assume that a differential volume (dV) is equal

to a varying distance times a differential area ( $\delta$  dA). This change is appropriate for replacing the integral over the volume of an enclosed space with the integral of the medial surface of that space times a distance representing the depth of the volume at a particular point on the surface.

With this change, it is necessary to replace T with the temperature associated with  $\delta$  dA. We take this temperature to be the average temperature of the outer and inner surfaces bounding the volume:

 $T = \frac{T_o + T_i}{2}.$ 

The medial surface of the gas volume is not known. We instead use the fuel surface. This gives

 $\bar{T} = \frac{\int_{A_f} \frac{T_o + T_i}{2} \delta \, dA}{\int_{A_f} \delta \, dA}$ 

where  $A_f$  is the fuel surface,  $T_o$  is the temperature across the gap,  $T_i$  is the temperature on the fuel surface, and  $\delta$  is the gap distance. This approximation is a good one for the plenum region since the plenum volume can be accurately calculated given our assumptions. The accuracy of the calculation will be lower for the gap volume contribution, but since this volume is small (zero in areas of fuel/cladding contact) it is less important.

Note that since this approach places an appropriately large weight on the gas in the plenum, it is important that the temperature of the fuel adjacent to the plenum be accurate. It may be necessary to place insulating pellets in a model in order to calculate realistic temperatures at the top of the fuel stack.

# 14 Coolant Channel Model

In the operating conditions of Light Water Reactors, fuel rods are surrounded by flowing water coolant; the flowing coolant carries the thermal energy generated from fission and transfers the heat into a steam generator or drives a turbine directly. To predict the performace of a fuel rod, thermal hydraulic condition of the surrounding coolant must be accurately determined. Such condition in modeling the energy transport aspect of the coolant in BISON code is described by a single coolant channel model. This single channel is used mathematically to describe the thermal boundary condition for modeling the fuel rod behavior. This model covers two theoretical aspects, i.e., the local heat transfer from cladding wall into the coolant and the thermal energy deposition in the coolant in steady state and slow operating transient conditions.

Assumptions and limitations of the coolant channel model are summarized below:

#### 1. Closed channel

The lateral energy, mass, and momentum transfer in the coolant channel within a fuel assembly is neglected. Therefore, the momentum, mass continuity, and the energy equations are only considered in one-dimension, i.e., the axial direction.

#### 2. Homogeneous and equilibrium flow

For the flow involving both the vapor and liquid phases, the thermal energy transport and relative motions between the two phases are neglected. This essentially assumes the two-phase flow is in a form of one pseudo fluid.

#### 3. Fully developed flow

In the application of most heat transfer correlations, the entrance effects are neglected. The heat transfer is assumed to happen in a condition that the boundary layer has grown to occupy the entire flow area, and the radial velocity and temperature profiles are well established.

## 4. Pressure drop neglected

The pressure drop due to flow induced resistance is not accounted for in the coolant channel model. Instead, coolant pressure as a function of time and axial location can be an input provided by user through a hand calculation or using a computer code.

## 14.1 Coolant enthalpy rise in a single channel

In steady state operation, the enthalpy rise in a coolant channel with incompressible fluid can be derived using energy conservation equation:

$$H(z) = H_{in} + \frac{\int_0^Z q''(z)\pi D_h dz + \int_0^Z f_c q' dz}{GA}$$
 (14.1)

where

 $H_{in}$  is the coolant enthalpy at inlet in (J/kg)

H(z) is the coolant enthalpy at axial location z in (J/kg)

z is axial location (m)

q'' is fuel rod surface heat flux (W/m<sup>2</sup>)

q' is fuel rod linear heat generation rate (W/m)

 $f_c$  is the fraction of heat generated in the coolant by neutron and gamma rays (dimensionless)

 $D_h$  is heated diameter (m)

G is coolant mass flux (kg/sec- $m^2$ )

A is flow area of the coolant channel (m<sup>2</sup>)

The mass flux, pressure, and coolant temperature at the inlet of coolant channel are provided as input for calculating coolant enthalpy rise. With calculated enthalpy and input coolant pressure, the corresponding thermodynamic condition can be determined using a steam table, and the thermal-physical properties of water and steam are evaluated at the corresponding bulk coolant temperature or at the cladding wall temperature for the use of calculating heat transfer coefficients between the cladding wall and the coolant.

The BISON code input allows the mass flux, pressure, and coolant temperature to change as a function of time, although the coolant enthalpy is still solved using the same equation above. Allowing the variation of inlet thermal-hydraulic conditions can be used to model a quasi-steady state when the velocity and thermal energy of coolant at a given location are assumed to achieve the equilibrium condition instantaneously.

#### 14.2 Heat transfer correlations

Depending on the flow rate, flow pattern, and cladding wall surface heat flux, the heat transfer from cladding wall outer surface to coolant can be characterized into different heat transfer regimes.

A set of heat transfer correlations to describe the heat transfer condition prior to the point of Critical Heat Flux (CHF) is described follows:

#### • Dittus-Boelter correlation:

Under forced flow condition and when the coolant is still in the liquid phase, the heat transfer from the cladding wall to the coolant is in the regime of single phase forced convection, and the heat transfer can be described by Dittus-Boelter equation.

$$Nu = 0.023Re^{0.8}Pr^{0.4} (14.2)$$

The equation is applicable for 0.7 < Pr < 100, Re > 10,000, and L/D > 60. Fluid properties are evaluated at the arithmetic mean bulk temperature [70].

• Jens-Lottes correlation:

$$\Delta T = 25 \left(\frac{q''(z)}{10^6}\right)^{0.25} / e^{P/6.2 \times 10^6}$$
 (14.3)

Where,  $\Delta T$  is the cladding wall super heat =  $T_W$ - $T_{sat}$  in (K). q" is the cladding wall surface heat flux (W/m<sup>2</sup>-K)), and P is the coolant pressure (Pa). This correlation is developed based on data at a pressure between 500 psi (3.45 MPa) and 2000 psi (13.79 MPa) in sub-cooled boiling regime. The heat transfer coefficient is given as:

$$h = \frac{[(T_W - T_{sat})e^{P/6.2 \times 10^6}/25]^4 \times 10^6}{T_W - T_b}$$
(14.4)

### • Thom correlation:

A similar correlation is given as follows:

$$\Delta T = 22.7 \left(\frac{q''(z)}{10^6}\right)^{0.5} / e^{P/8.7 \times 10^6}$$
 (14.5)

The heat transfer coefficient is:

$$h = \frac{[(T_W - T_{sat})e^{P/8.7 \times 10^6}/22.7]^2 \times 10^6}{T_W - T_b}$$
 (14.6)

This correlation is for water at a pressure between 750 psi (5.17 MPa) and 2000 psi (13.79 MPa); but much of Thom's data were obtained at relatively low heat fluxes according to Tong [71].

#### • Shrock-Grossman correlation

Shrock-Grossman heat transfer correlation is used in the regime of saturated boiling. The heat transfer coefficient is given as:

$$h = \left(a_1 \frac{q''}{Gh_{fg}} + a_2 X_{tt}^{-b}\right) h_l \tag{14.7}$$

$$X_{tt}^{-1} = \left(\frac{x}{1-x}\right)^{0.9} \left(\frac{\rho_f}{\rho_g}\right)^{0.5} \left(\frac{\mu_g}{\mu_f}\right)^{0.1}$$
 (14.8)

Where,

x is the steam quality

 $h_{fg}$  is the latent heat of vaporization (J/kg)

 $h_l$  is the heat transfer coefficient in the liquid phase at the same mass flux (J/kg)

G is the mass flux (kg/m $^2$ -sec)

 $a_1$ ,  $a_2$ , and b are constants as follows:

 $a_1 = 7400$ 

 $a_2 = 1.11$ 

b = 0.66

#### Chen's correlation

An alternative correlation that is used in the saturated boiling regime is Chen's correlation. Chen's correlation consists of a convective part and a nucleation part:

$$h = Fh_c + Sh_{NB} \tag{14.9}$$

 $h_c$  is the modified Dittus-Boelter correlation:

$$h_c = 0.023 \left(\frac{G(1-x)D_e}{\mu_f}\right)^{0.8} Pr_f^{0.4} \frac{k_f}{D_e}$$
 (14.10)

F is a factor to account for the enhanced heat transfer due to the turbulence caused by vapor.

$$F = 1$$
, for  $\frac{1}{X_{tt}} < 0.1$  (14.11)

$$F = 2.35 \left( 0.213 + \frac{1}{X_{tt}} \right)^{0.736}$$
, for  $\frac{1}{X_{tt}} > 0.1$  (14.12)

The nucleation part is the Forster-Zuber equation:

$$h_{NB} = 0.00122 \left[ \frac{(k^{0.79} c_p^{0.45} \rho^{0.49})_f}{\sigma^{0.5} \mu_f^{0.29} h_{fg}^{0.25} \rho_g^{0.24}} \right] \Delta T_{sat}^{0.24} \Delta P^{0.75}$$
(14.13)

$$\Delta T_{sat} = T_W - T_{sat} \tag{14.14}$$

$$\Delta P = P(T_W) - P(T_{sat}) \tag{14.15}$$

S is a suppression factor:

$$S = \frac{1}{1 + 2.53 \times 10^{-6} Re^{1.17}} \tag{14.16}$$

Where  $Re = Re_l F^{1.25}$ ;  $Re_l$  is the Reynold number for liquid phase only.

### 14.2.1 Critical heat flux correlations

The sub-cooled and saturated boiling can enhance the heat transfer; however at a critical condition when the cladding outer surface is enclosed by vapor film, the heat transfer can deteriorate significantly, the corresponding heat flux is the Critical Heat Flux (CHF). The following correlations are implemented in BISON to calculate CHF, which can be used to estimate the thermal margin in a coolant channel.

#### • EPRI-Columbia correlation

$$\frac{q_{CHF}}{10^6} = \frac{A - x_{in}}{C + \left(\frac{x - x_{in}}{q''}\right)}$$
(14.17)

where

 $A = F_a p_1 p_r^{p_2} G^{(p_5 + p_7 p_r)}$ 

 $C = F_c F_{AP} p_3 p_r^{p_4} G^{(p_6 + p_8 p_r)}$ 

 $p_1 = 0.5328$ 

 $p_2 = 0.1212$ 

 $p_3 = 1.6151$ 

 $p_4 = 1.4066$ 

 $p_5 = -0.3040$ 

 $p_6 = 0.4843$ 

 $p_7 = -0.3285$ 

 $p_8 = -2.0749$ 

 $p_r$  = critical pressure ratio=system pressure/critical pressure

 $G = local mass velocity (Mlbm/hr-ft^2)$ 

 $x_{in}$  = inlet quality

 $F_a = G^{0.1}$ 

 $F_c = 1.183G^{0.1}$ 

 $F_a = F_c = 1$  for no cold wall

 $q'' = local heat flux (MBtu/hr-ft^2)$ 

 $F_{AP}$  is the non-uniform axial heat flux distribution parameter:

$$F_{AP} = 1 + \frac{(Y-1)}{(1+G)} \tag{14.18}$$

Y is Bowring's non-uniform parameter defined as:

$$Y = \frac{\int_0^z q''(z) dz}{q''(z)z}$$
 (14.19)

• GE correlation

$$q_{CHF} = 10^6 (0.8 - x) \text{ for } G \ge 0.5 \times 10^6 \text{ lb}_{\text{m}}/\text{ft}^2\text{-hr}$$
 (14.20)

$$q_{CHF} = 10^6 (0.84 - x) \text{ for } G < 0.5 \times 10^6 \text{ lb}_m/\text{ft}^2\text{-hr}$$
 (14.21)

The correlation is applicable for mass fluxes less than  $0.75 \times 10^6$  lb<sub>m</sub>/ft<sup>2</sup>-hr.

The EPRI correlation is used as the correlation for a Pressurized Water Reactor (PWR) environment. The GE correlation is used as the correlation for a Boiling Water Reactor (BWR) environment.

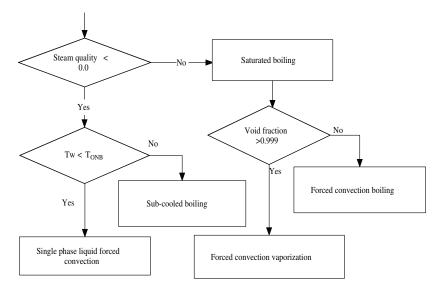


Figure 14.1: Schematic of heat transfer regimes selection criteria prior to critical heat flux.

#### 14.2.2 Criteria to select heat transfer correlations

The diagrams in Figure 14.1 shows the criteria used in the selection of different heat transfer regimes prior to the point of critical heat flux.

Dittus-Boelter correlation is used for the single phase liquid forced convection. Thom or Jens-Lottes correlation is used for the sub-cooled boiling regime. Thom, Jens-Lottes, or Chen correlation is used for the forced boiling convection regime. Shrock-Grossman correlation is used for the forced boiling convection and vaporization regime.  $T_{ONB}$  is the temperate at the onset of nucleate boiling.

## 14.3 Properties for water and steam

Properties for water and steam consist of thermodynamic properties, transport properties, and other physical properties used in the heat transfer correlations. They are implemented based on a few standards specified by the International Association or Properties for Water and Steam (IAPWS). The thermodynamic properties, or the steam tables, are implemented in the code package ELK using a standard for industry application, IAPWS-IF97 standard [72].

IAPWS-IF97 covers thermodynamic properties for water and steam in following range:

$$273.15 \text{ K} < T < 1073.15 \text{ K}, p < 100 \text{ MPa}$$
 (14.22)

$$1073.15 \text{ K} < T < 2273.15 \text{ K}, \ p \le 50 \text{ MPa}$$
 (14.23)

Figure 14.2 shows the five regions defined in IAPWS-IF97. Region 1 represents the liquid phase. Region 2 describes the vapor phase. Region 4 is the saturation curve that separates the liquid phase and the vapor phase. Region 3 describes water properties near the critical

point. Region 5 is used for very high temperature condition and is not of interest to any reactor operation; thus region 5 is not included in the BISON coolant channel model.

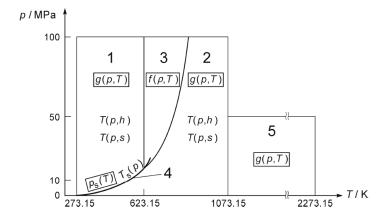


Figure 14.2: Regions and Equations of IAPWS-IF97 [72]

Ref [72] describes the equations used in the calculation of thermodynamic properties using basic equations which are functions of temperature and/or pressure or temperature and density.

Viscosity and thermal conductivity of water and steam are functions of density and temperature; these transport properties are implemented based on the information in [73] and [74]. Surface tension of water as a function of temperature is given in [75].

These physical properties are used together with IAPWS-IF97 standard in evaluating properties for water and steam.

# 15 Cladding Corrosion Model

## 15.1 Zirconium Alloy

#### 15.1.1 Introduction

Zirconium alloy cladding can have an exothermic reaction with coolant water which converts metal to oxide at the cladding outer surface:

$$Zr + H_2O \rightarrow ZrO_2 + 2H_2 + 6.5 \times 10^6 \text{ J/kgZr}$$
 (15.1)

Such an oxidation process, which is referred to as water-side corrosion, is a fundamental aspect of LWR fuel performance. The resultant oxide film on the outer surface of cladding can affect both the thermal and mechanical properties of cladding. Because of the lower thermal conductivity of zirconium oxide in comparison with zirconium alloys, the oxidation of the cladding adds to thermal resistance to heat transfer from the fuel to the coolant. Zirconium oxide is a brittle material and can be easily cracked. Thus it is expected that the mechanical strength of cladding is mainly determined by the metallic wall, which is thinned after corrosion. Concurrent to the oxidation process, a fraction of hydrogen can be absorbed into the metal and can diffuse under the influences of both temperature and stress. Due to the low solubility of hydrogen in zirconium and its alloys, hydrogen can precipitate as  $\delta$ -phase hydrides (ZrH<sub>1.66</sub>), which are known to further reduce the ductility of irradiated cladding material. In fact, the hydrogen content in the zircaloy cladding has become a limiting parameter for burnup extension of LWR fuel. An oxidation model which can predict the growth of oxide layer as a function of operation conditions and metallurgical variables of cladding materials is essential to the study of LWR fuel performance. In addition, it is also of interest to account for the effects of the oxide layer on the thermal and mechanical properties of cladding.

Low temperature (250 °C/ 523 K to 400 °C/ 673 K) oxidation is calculated considering that cladding oxidation under normal LWR conditions occurs in two stages: a pre-transition oxidation process that follows a cubic time dependence up to a transition oxide thickness, and a post-transition process that follows a linear time dependence. The transition between the two stages typically occurs at 2 micron.

For the pre-transition period, the corrosion rate is given by an Arrhenius equation [76]:

$$\frac{dS^3}{dt} = C_1 \exp\left(\frac{-Q_1}{RT_I}\right), \text{ for } S \le S_{trans}.$$
 (15.2)

For the post-transition period, the corrosion rate is given by [76]:

$$\frac{dS}{dt} = C_2 \exp\left(\frac{-Q_2}{RT_I}\right), \text{ for } S > S_{trans}$$
 (15.3)

where

S is the oxide thickness

 $T_I$  is the metal-oxide interface temperature

 $C_1$  is the rate constant for pre-transition oxidation

 $Q_1$  is the activation energy for pre-transition oxidation

 $C_2$  is the rate constant for post-transition oxidation

 $Q_2$  is the activation energy for post-transition oxidation

R is the universal gas constant

 $S_{trans}$  is the transition oxide thickness

The metal-oxide interface temperature,  $T_I$ , is calculated assuming steady-state heat conduction across the oxide thickness as:

 $T_I = T_{co} + \frac{q''S}{k_{ox}} \tag{15.4}$ 

where  $T_{co}$  is the outer surface (waterside) oxide temperature and  $k_{ox}$  is thermal conductivity of zirconium oxide.

#### 15.1.2 EPRI SLI Model

The EPRI/SLI model is implemented as the default corrosion model for PWR Zry-4 cladding material. This model uses enhancement factors on  $C_1$  and  $C_2$ . For the pre-transition period,  $C_1$  is multiplied by two factors, one related to the lithium concentration in the coolant and the other related to the iron concentration in the cladding. These are given as [77]

$$C_1 = C_{10}F_{Li}(1 + F_{Fe}) (15.5)$$

$$F_{Li} = exp\left(C_{Li}(0.12[Li] - 23[Li]/T)\right) \tag{15.6}$$

$$F_{Fe} = C_{Fe}[Fe] \tag{15.7}$$

where [Li] = lithium concentration [ppm] in the coolant, and [Fe] = fraction of iron particles dissolved (%) for a given initial particle size distribution. The parameters used in above equations are as follows:

 $C_{10} = 5.876^{10} \mu \text{m}^3/\text{day}$ 

 $Q_1$ =33662.7 cal/mol

 $C_{Li} = 0.65$ 

 $C_{Fe}=0.02(\%)^{-1}$ 

The post-transition coefficient  $C_2$ , is multiplied by several enhancement coefficients as follows:

$$C_2 = C_{20}F_{Li}F_{Sn}F_{Q/A}(1 + F_H + F_{Fe} + F_{\phi}]C_{20} = 7.619 \times 10^6 \mu \text{m/day}$$
 (15.8)

The coolant chemistry (LiOH) enhancement factor is given by:

$$F_{Li} = \exp(C_{Li}(0.17[Li] - 20.4[Li]/T_I)) \tag{15.9}$$

The cladding tin content enhancement factor is given by:

$$F_{Sn} = \begin{cases} 1.25(\text{Sn} - 1.38) + 1.0 & \text{for Sn} \le 1.38 \text{ wt\%} \\ 0.75(\text{Sn} - 1.38) + 1.0 & \text{for Sn} > 1.38 \text{ wt\%} \end{cases}$$
 (15.10)

where Sn is tin content of cladding in (wt%). The heat flux normalization factor is given by:

$$F_{O/A} = 1 + 0.0881(Q/A)/100 (15.11)$$

where Q/A (W/cm<sup>2</sup>) is the heat flux at cladding outer surface.

The hydrogen redistribution enhancement factor is:

$$F_H = \begin{cases} 0 & \text{for } [H_2] < 400 \text{ ppm} \\ 0.699 ln([H_2]/400) & \text{for } 18811.25 \text{ ppm} \ge [H_2] \ge 400 \text{ ppm} \\ 2.691 & \text{for } [H_2] > 18811.25 \text{ ppm} \end{cases}$$
(15.12)

where  $[H_2]$  = cold side hydrogen content in the cladding metal-oxide interface.

The fast neutron flux enhancement factor is:

$$F_{\phi} = C_{\phi} \phi^{P_O} \tag{15.13}$$

where  $\phi$  = fast flux (E > 1 MeV, n/cm<sup>2</sup>-s),  $C_{\phi}$  = 1.2 ×10<sup>-4</sup> (n/cm<sup>2</sup>-s)<sup>-0.24</sup>, and Po = 0.24.

The iron enhancement factor is defined by Eq. 15.7.

Activiation energy in the post-transition period is found to be dependent on hydrogen content [78]:

$$Q_{2} = \begin{cases} Q_{2L} & \text{for } [H_{2}] < 400 \text{ ppm} \\ (Q_{2U} - Q_{2L})F_{H}/F_{HU} + Q_{2L} & \text{for } 18811.25 \text{ ppm} \ge [H_{2}] \ge 400 \text{ ppm} \\ Q_{2U} & \text{for } [H_{2}] > 18811.25 \text{ ppm} \end{cases}$$
(15.14)

where  $F_{HU}$  = hydrogen enhancement factor at hydride rim ([ $H_2$ ] = 18811.25 ppm),  $Q_{2L}$  = 24825 cal/mol, and  $Q_{2U}$  = 9135.6 cal/mol.

### 15.1.3 Zirconium Oxide Thermal Conductivity

Thermal conductivity of zirconia in the model is a constant value of 1.5 W/m-K for PWR applications [77]. However the reported value of zirconium oxide thermal conductivity varies greatly from different sources.

In the NFIR experimental program, the  $ZrO_2$  thermal conductivity was estimated using cladding elongation measurements during power ramps as a representation of cladding temperature changes [79]. By comparing the cladding elongation of a fuel rod with an external oxide to a reference rod without an external oxide, the thermal impact of the oxide layer was determined. Experiments were performed at oxide layer thicknesses between 30 and 82  $\mu$ m. In determining the thermal conductivity from the measured data, considerations were made for external crud layers, power increases, power decreases, and oxide layer thickness. The results of the experiments found that the thermal conductivity of  $ZrO_2$  is independent of oxide thickness and temperature in the temperature range between 240°C and 300°C. An NFIR corrosion model was developed with a constant thermal conductivity value of 2.7 W/m-K (which tends to be on the high side of the data). The NFIR model is based on a series of in-pile experiments performed in the Halden test reactor that were designed to determine the thermal conductivity of external oxide layers on fuel rods [79].

The MATPRO-11 Rev. 2 model for Zircaloy oxide thermal conductivity is based on several different data sources of thermal conductivity measurements [13]. These measurements were performed using a variety of oxide morphologies (stabilized oxides, nodular, and black) and oxide formation techniques (steam oxidation and plasma sputtering).

Using thermal diffusivity measurements, the thermal conductivity was determined for the different oxide types as a function of temperature. The MATPRO model used primarily data from tests with black oxide layers to develop the thermal conductivity as a function of temperature [13].

The resulting correlation is

$$k_{ox} = 0.835 + 1.81 \times 10^{-4} T \tag{15.15}$$

where  $k_{ox}$  is the oxide thermal conductivity (W/m-K) T is the oxide temperature (K).

The correlation above is applicable to solid Zircaloy oxide found on fuel rods. These other values are typical of other models found in the literature. Further information on the MATPRO Zircaloy oxide model can be found in Reference [13].

Nuclear Electric (NE PLC) use a different correlation starting at a value of 1.5 W/m-K. The value then decreases with oxide thickness according to the following relationship [77]:

$$k_{ox} = \begin{cases} 1.5, & 0 \,\mu\text{m} < S \le 48 \,\mu\text{m} \\ 3.48 - 0.0412S, & 48 \,\mu\text{m} < S \le 65 \,\mu\text{m} \\ 0.8, & S > 65 \,\mu\text{m} \end{cases}$$
(15.16)

The CEA Cochise code uses a constant value of 1.6 W/m-K [77].

#### 15.1.4 Numerical Method

Numerical solution of the oxide thickness growth consists of pre-transition and post-transition period.

In the pre-transition period:

$$\Delta S = \sqrt[3]{C_1 \exp\left(\frac{-Q_1}{RT_{co}}\right) \Delta t + S}$$
 (15.17)

where

S is oxide thickness at previous time step ( $\mu$ m)

 $C_1$  is rate constant for pre-transition oxidation ( $\mu$ m<sup>3</sup>/day)

 $Q_1$  is activation energy for pre-transition oxidation (cal/mol)

R is gas constant = 1.987 (cal/mol-K)

 $T_{co}$  is cladding outer surface temperature (K)

 $\Delta t$  is time increment (day)

 $\Delta S$  is oxide thickness increment ( $\mu$ m)

In the post-transition oxidation period, an approximate integral method is used [80] to account for the metal-oxide interface temperature change on the oxygen weight gain:

$$\Delta S = \gamma \Delta W / 100 \tag{15.18}$$

$$\Delta W = \frac{RT_{co}^2 k_{ox}}{\gamma Q_2 q''} \ln \left[ 1 - \frac{\gamma Q_2 q''}{RT_{co}^2 k_{ox}} k_0 \exp\left(-\frac{Q_2}{RT_{co}}\right) \exp\left(\frac{\gamma Q_2 q''W}{RT_{co}^2 k_{ox}}\right) \right]$$
(15.19)

where

 $T_{co}$  is cladding outer surface temperature (K)

 $k_{ox}$  is thermal conductivity of zirconium oxide (W/cm-K)

 $\Delta W$  is weight gain (g/cm<sup>2</sup>)

 $\gamma$  (=0.6789 cm<sup>3</sup>/g) is a factor that converts weight gain (g/cm<sup>2</sup>) to thickness (cm)

 $Q_2$  is activation energy for post-transition phase

q is heat flux  $(W/cm^2)$ 

k0 is rate constant for post-transition phase (g/cm<sup>2</sup>-day)

 $\Delta t$  is time increment (day)

R is ideal gas constant = 1.987 (cal/mol-K)

W is weight gain at previous time step  $(g/cm^2)$ 

S is oxide layer thickness at previous time step ( $\mu$ m)

## 15.2 Aluminum

According to [81, 82], corrosion of aluminum in ATR follows

$$t_{ox} = 0.7 \cdot 25.4 \cdot 443 \cdot \theta^{0.778} \exp(-4600/T)$$
 (15.20)

where

 $t_{ox}$  is the oxide thickness ( $\mu$ m)

 $\theta$  is time (hours)

T is temperature (K)

This corrosion thickness may be used in the coolant channel model.

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