Ion Recognition Approach to Volume Reduction of Alkaline Tank Waste by Separation of Sodium Salts

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ANNUAL PROGRESS REPORT

U.S. Department of Energy

Ion Recognition Approach to Volume Reduction of Alkaline Tank Waste by Separation of Sodium Salts

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Number of undergraduate students: 0

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Number of postdocs: 1

Abstract

In this project, now completing its third year of its second renewal period, a collaborative project involving Oak Ridge National Laboratory, Pacific Northwest National Laboratory, and the University of North Texas has been addressing outstanding questions regarding the separation of the bulk sodium constituents of alkaline tank waste. The principal potential benefit of this research is a major reduction in the volume of radioactive tank waste, obviating the building of expensive new tanks and reducing the costs of vitrification. As a general approach, principles of ion recognition are being explored toward discovery and basic understanding of liquid-liquid extraction systems that selectively separate sodium hydroxide and sodium salts from waste-like matrices. Questions being addressed pertain to applicable extraction equilibria and how extraction properties relate to extractant structure. Progress has included the elucidation of the promising concept of pseudo hydroxide extraction (PHE), demonstration of crown-ether synergized PHE, demonstration of combined sodium hydroxide/sodium nitrate separation, and synthesis of novel ditopic receptors for ditopic PHE. In future efforts (pending renewal), a thermochemical study of PHE relating extractant acidity to extraction strength is proposed, and this study will be extended to systems containing crown ethers, including proton-ionizable ones. A series of crown ethers will be synthesized for this purpose and to investigate the extraction of bulk sodium salts (e.g., nitrate, nitrite, and sulfate), possibly in combination with sodium hydroxide. Simple proof-of-principle tests with real tank waste at PNNL will provide feedback toward solvent designs that have desirable properties. In view of the upcoming milestone of completion of the second renewal period, this report will, in addition to providing a summary of the past year's progress, summarize all of the work completed since the start of this project.

Research Objectives

General objectives. The overall goal of this research conducted under the auspices of the USDOE Environmental Management Science Program (EMSP) is to provide a scientific foundation upon which the feasibility of new liquid-liquid extraction chemistry applicable to the bulk reduction of the volume of tank waste can be evaluated. Disposal of high-level nuclear waste is horrendously expensive, in large part because the actual radioactive matter in the tanks has been diluted over 10,000-fold by ordinary inorganic chemicals.¹ Quite simply, if the radioactive matter and bulk inorganic chemicals could be separated into separate streams, large cost savings would accrue, because the latter stream is much cheaper to dispose of. In principle, one could remove the radionuclides from the waste, leaving behind the bulk of the waste; or one could remove certain bulk chemicals from the waste, leaving behind a mixture of radionuclides and minor inorganic salts. The preponderance of effort over the past two decades has focused on the former approach, which produces a high-level stream for vitrification and a low-activity stream for either vitrification (Hanford) or grout (Savannah River). At Hanford, a particular concern arises in that vitrification of a large volume of low-activity waste will be unacceptably expensive. To make matters worse, a projected future deficit of tank space may necessitate construction of expensive new tanks. These problems have raised questions as to whether a solution could be devised based on separation of sodium from the waste, resulting in the reduction of the total volume of waste that must be vitrified.²

The research reported herein focuses on fundamental chemistry that could support

development of methods for separation of sodium hydroxide and sodium salts from alkaline tank wastes. In particular, sodium hydroxide is an attractive target, because it is a bulk waste constituent that can be recycled, and it is also compatible with grout, possibly enhancing the regulatory acceptability of this economical waste form. Waste retrieval and sludge washing, for example, will require copious amounts of sodium hydroxide. If the needed sodium hydroxide could be separated from the waste and recycled, the addition of fresh sodium hydroxide could be avoided, ultimately reducing the final waste volume and associated disposal costs.³ Although the percent volume reduction is rather modest, perhaps 15%, the savings is possibly still significant and may be enough to avoid construction of new tanks. Even more tantalizing, if nitrate and nitrite anions in the waste could be reduced to nitrogen gas and hydroxide (e.g., electrochemically), the bulk of the sodium in the waste could then be separated as a single component, sodium hydroxide.

Based on the above considerations, the major objective of this project since FY 1998 has been to explore new solvent-extraction approaches to the selective separation of sodium hydroxide from alkaline tank wastes. In the renewal period beginning in FY 2002, attention is also being given to the separation of salts of the other abundant anions, especially nitrate. A comprehensive approach toward understanding the extractive chemistry of sodium salts is envisioned, involving systems of varying complexity, from use of simple solvents to new bifunctional host molecules for sodium cation exchange. Ideal extractants will require no adjustment of the waste composition and will release the extracted salt into water, thereby consuming no additional chemicals and producing no additional waste volume.

This research reported herein was carried out in a collaboration involving Oak Ridge National Laboratory (ORNL), Pacific Northwest Laboratory (PNNL), and the University of North Texas (UNT). ORNL and PNNL investigated the extraction chemistry, and UNT synthesized new crown ethers.

Objectives for the past year. Experiments were carried out to understand the underlying properties of the controlling equilibria in pseudo hydroxide extraction (PHE, see below) using 1-octanol as the diluent. Additional fluorinated alcohols and phenols that function by cation exchange at elevated pH values were tested. Synergized PHE using a crown ether was examined, especially with a view toward increasing sodium nitrate extraction efficiency and thereby boosting the total fraction of sodium that may be extracted from the waste. New ionizable lariat ethers were synthesized and tested as representatives of the class of ditopic PHE materials (UNT). The primary goal of the extraction experiments using these compounds was to demonstrate that PHE is operating and to determine whether the ditopic receptors offer advantages over the simpler synergized PHE systems.

Background

Making no presumption as to the best practical approach to separating sodium, we have found it very useful to consider a hierarchy of applicable fundamental chemical processes. These rely on principles of solvation, acid-base reactions, and host-guest chemistry. Table 1 lists eight basic approaches that one might take to effect a separation of sodium hydroxide or sodium salts.^{4,5} The first five approaches entail ion-pair extraction processes in which the extracted cation M^+ and anion X^- may either be solvated or complexed. The receptor in each case is indicated by a circle without implying any particular structure. The last three approaches entail

Table 1. Fundamental Approaches Applicable to NaOH or NaX Separation using Host-Guest and Liquid-Liquid Extraction Principles

Case	System	Organic-phase species
#1	No receptors	$M^+ + X^-$
#2	Cation receptor	$\langle M^+ \rangle + X^-$
#3	Anion receptor	$M^+ + \langle X^- \rangle$
#4	Cation receptor + Anion receptor	$\langle M^+ \rangle + \langle X^- \rangle$
#5	Ditopic ion-pair receptor	$\langle M^+ X^- \rangle$
#6	Cation exchanger	$\sim\sim\sim A^- + M^+$
#7	Cation exchanger + Cation receptor	$\sim\sim\sim A^- + \langle M^+ \rangle$
#8	Proton-ionizable receptor	$\langle M^+ \rangle - A^-$

an acid-base reaction to transfer a hydroxide equivalent to the solvent with or without receptor for the cation M^+ . The cation exchanger is depicted with an alkyl tail to indicate lipophilicity. Although the product cation and anion species are written as free ions for all cases except #5 and #8, ion pairing is expected to be important in many systems to be encountered, though its effect on extraction selectivity tends to be minor relative to solvation and binding phenomena. Species may also be aggregated.

When one or both of the extracted ions is not bound by a host, as in Cases #1, #2, #3, and #6 (Table 1), then the selectivity for the unbound ion is determined solely by the solvent (in the absence of ion pairing). We have reviewed the pertinent principles of solvation,^{6,7} and the reader is referred to these and other sources^{8,9} for details. Although many fundamental interactions determine the value of ΔG_p° for a given ion,⁹ statistical analysis¹⁰ indicates that the solvation of small inorganic ions is dominated by electrostatic hard-hard interactions. Thus, for Na^+ , the solvent must supply electron-pair donor (EPD) groups for coordination.⁶ Likewise for OH^- and NO_3^- hydrogen-bond donor (HBD) groups are needed.⁷ In principle, for favorable ion partitioning, the EPD and HBD groups must be significantly stronger than the H_2O molecules in the source phase. This is difficult to achieve in a water-immiscible liquid, and indeed, ion partitioning for typical inorganic ions is unfavorable ($\Delta G_p^\circ > 0$).⁸

Solvation effects provide strong selectivity that may be best categorized as "bias" rather than "recognition".⁷ Specifically, the partitioning process tends to select on the basis of ion size for ions of like charge, usually favoring large or charge-diffuse (q^2/r) ions; there is no "recognition" per se, because it is always possible to find a more highly selected ion, namely a more charge-diffuse one. Thus, for ions pertinent to present purposes, we normally obtain the selectivity orders (thermochemical radii in nm in parentheses):^{7,8} Cs^+ (0.167) > K^+ (0.138) > Na^+ (0.102) and TcO_4^- (0.252) > NO_3^- (0.196) > Cl^- (0.172) > OH^- (0.133). We have termed such solvation-based selectivity for anions as Hofmeister bias,¹¹ in reference to the ordering of anions by hydration first noted by Franz Hofmeister.¹² One mainly manipulates solvation bias by varying the EPD and HBD strength of the diluent, though one cannot thereby change the ordering of ions fundamentally. Rather, one only changes the magnitude of the bias.⁷ In

principle, then, bias may be reversed for cations and anions, respectively, when the EPD and HBD strengths of the solvent exceed that of water. In this case, charge-dense ions would be selected in a competitive extraction. Unfortunately, most water-immiscible solvents fail to meet these conditions, and thus Hofmeister bias is ubiquitous.

Ironically, cation exchange provides an alternative approach for an effective separation of OH^- ion. Possessing exchangeable acidic protons, cation-exchange extractants (HA) have many variants, as found in standard texts.¹³ Focusing on univalent ions and neglecting aggregation, cation exchange as driven by neutralization of the released hydrogen ion by hydroxide may be written most simply as:

The reverse reaction affords recovery of sodium hydroxide upon stripping with water, whereby the alcohol returns to its protonated form in the organic phase. When used in tandem, the forward and reverse steps constitute a cyclic process affording the transfer of alkali metal hydroxide from an aqueous mixture into water.¹⁴ Because only hydroxide equivalents rather than actual hydroxide ions are transferred, this approach has been termed pseudo hydroxide extraction (PHE, Case #6 in Table 1).^{4,15–18} Surprisingly, a single study involving phenols represents the only citation of such a process in the literature prior to our work.¹⁹

Research Progress and Implications

Summary of Prior Results

This section outlines progress in the first three years of this project, for which a detailed progress report has been issued.²⁰ Eight fundamental approaches to hydroxide extraction were considered (Table 1).⁴ Two promising approaches among them were introduced and received focused attention, PHE (Case #6) and synergized PHE (SPHE, Case #7). PHE represents the most developed concept in terms of a possible application. A patent has been issued.¹⁴ Applied development was spun-off into a separately funded one-year project that demonstrated that recovery of NaOH from actual waste is possible for recycle to sludge washing.²¹ Although the concept appears viable, issues identified include selectivity, phase behavior, and stripping efficiency. The first observation of SPHE was communicated,²² wherein it was shown that enhanced NaOH extraction may be effected by combining fluorinated alcohols with macrocyclic extractants. Although the macrocycles used alone tend to favor the extraction of salts of large anions, sodium extraction from hydroxide solutions jumps sharply when the macrocycles are combined with certain lipophilic fluorinated alcohols or phenols. Large synergistic effects were demonstrated, sufficient to make hydroxide separation competitive with the more abundant nitrate. Prof. Alan Marchand and his group at UNT carried out the synthesis of novel crown ethers and podands.^{23–26} Synthetic methodology was devised to produce new cage-annulated oxa-, thia-, and aza-crown ethers that possess varying cavity sizes and shapes and that differ in the number and nature of the donor atoms in the macrocyclic system. Crystal structures provided valuable information on the macrocycles' preferred conformations.²⁷ By appropriate variation of

macrocycle structure, the strength and selectivity of extraction of alkali metal cations may be controlled, as shown in standard picrate extraction surveys.^{23,26}

Results in the Past Three Years

Pseudo Hydroxide Extraction. Experiments were focused on questions related to the capacity and selectivity of lipophilic weak cation exchangers and to the underlying extraction mechanism. Figure 1 displays the major cation exchangers examined, including alkyl phenols and lipophilic fluorinated alcohols. Compounds **2a–c** are new compounds.

A study was completed to address several issues pertaining to solvent capacity.¹⁵ High capacity is essential in view of the high concentration of sodium that we wish to separate. It was found that good loading of the solvent to approximately 1 M sodium can be achieved, but high solvent viscosity or even gelation occurs at 25 °C. This may be overcome by performing extraction and stripping at 60 °C, and isotherms have been obtained for several candidate extractants. Extraction strength increases qualitatively with hydroxyl proton acidity, being strongest with two alkyl phenols (**1a** and **1b**) and 4-*n*-octyl- α,α -bis(trifluoromethyl)benzyl alcohol (**2a**). Complete and selective removal of free hydroxide from a solution containing sodium hydroxide, nitrate, and aluminate was accomplished using 1 M 4-*tert*-octylphenol (**1a**) at 60 °C. Aluminum precipitates slowly as $\text{Al}(\text{OH})_3$ from the hydroxide-depleted aqueous phase. At least two extractants for PHE appear to be viable for process use in terms of efficacy and cost (**1a** and **1b**), though the fluorinated alcohols may have superior stability, yet to be investigated.

Figure 1. Compounds investigated for pseudo hydroxide extraction.

Considerable insight into the extraction mechanism of PHE was gained. Spectroscopic experiments were conducted to probe sodium hydroxide extraction from aqueous media by three fluorinated alcohols and a phenol in 1-octanol.²⁸ Specifically, it was the aim to use vibrational spectroscopy to identify a signature of the putative alkoxides or phenoxide, which could clarify whether the extraction mechanism involves the postulated ion exchange as opposed to ion-pair extraction, thought to be less likely. Infrared and Raman spectra were collected from the pure extractants in 1-octanol as well as in extracts of aqueous sodium hydroxide solutions. The authentic alkoxide or phenoxide of each extractant was prepared independently, and its spectrum was obtained to assist in the assignment of the bands observed in the extracts. In all cases, the extracts contained only two discernable species, that of the starting alcohol or phenol and the corresponding alkoxide or phenoxide. This result thus confirms the cation-exchange mechanism.

In light of the spectroscopic results, investigations are under way to identify the chemical equilibria responsible for PHE and to measure the corresponding extraction constants. Experiments completed to date^{18,29} show that PHE by the weak-acid extractants (HA) in 1-octanol can indeed be quantitatively modeled by a basic cation-exchange process in which salts in the solvent formed by the deprotonated weak acids can be ion-paired or dissociated. Ion pairing predominates, however, as the dissociation into free ions becomes important only at organic-phase concentrations of sodium below 10^{-4} M. Extensive data sets have been collected for 1-octanol alone, phenol **1b**, and fluorinated alcohol **3** in 1-octanol as a function of the concentrations of organic-phase extractant and aqueous NaOH.¹⁸ At an aqueous NaOH concentration of 1 M, the organic-phase concentration of sodium is only $7.6 (\pm 0.2) \times 10^{-4}$ M, but addition of **1b** or **3** strongly enhances extraction.¹⁸ The data have been subjected to rigorous mass-action analysis using the program SXLSQI. The results quantitatively confirm the postulated model given by eqs. 3–6 in Table 2.

We have extended the study to the other compounds in Fig. 1, establishing the generality of our model to these other cation exchangers. Table 2 defines the equilibria in the model. Equations 5 and 6 are defined by subtraction of the water autoionization from respectively eqs. 1 and 2 to express the reactions in terms of hydrogen ion dissociation, the usual way to describe an acid dissociation process. Table 3 reports the log K values found for the various compounds studied. The log K entries for 1-octanol account for the weak extraction without an added HA. These background log K values remain constant for all HA compounds. One may note from the values of log K_5 and log K_6 that the organic acids are indeed very weak and will be appreciably

Table 2. Equilibria Associated with Sodium Extraction

Eq. No.	Equation
3	$\text{Na}^+(\text{aq}) + \text{OH}^-(\text{aq}) \xrightleftharpoons{K_3} \text{Na}^+(\text{org}) + \text{OH}^-(\text{org})$
4	$\text{Na}^+(\text{aq}) + \text{OH}^-(\text{aq}) \xrightleftharpoons{K_4} \text{Na}^+\text{OH}^-(\text{org})$
5	$\text{Na}^+(\text{aq}) + \text{HA}(\text{org}) \xrightleftharpoons{K_5} \text{Na}^+(\text{org}) + \text{A}^-(\text{org}) + \text{H}^+(\text{aq})$
6	$\text{Na}^+(\text{aq}) + \text{HA}(\text{org}) \xrightleftharpoons{K_6} \text{Na}^+\text{A}^-(\text{org}) + \text{H}^+(\text{aq})$

Table 3. Equilibrium Constants Obtained from SXLSQI

	$\log K_3$	$\log K_4$	$\log K_5$	$\log K_6$
<i>1-Octanol</i>	-7.86 ± 0.07	-2.74 ± 0.03		
1a			-18.47 ± 0.11	-13.14 ± 0.01
1b			-18.89 ± 0.11	-13.50 ± 0.01
1c			-20.23 ± 0.12	-15.60 ± 0.06
2a			-19.83 ± 0.07	-12.25 ± 0.02
2b			-19.83 ± 0.01	-15.01 ± 0.02
2c			-20.00 ± 0.10	-15.62 ± 0.04
3			-19.58 ± 0.10	-14.62 ± 0.01
4			-19.03 ± 0.09	-14.74 ± 0.02

deprotonated only at pH values greater than 12. At practical loadings, eq. 6 dominates, and one may thus compare extraction strengths based on $\log K_6$. Extraction efficiency follows the qualitative order of acidity of the HAs, **1a** > **1b** > **1c** > **1d** and **2a** > **2b** > **2c**, reflecting a combination of inductive effects as well as steric constraints to solvation of the deprotonated anionic product species.

Synergized pseudo hydroxide extraction. In recently published work,⁵ SPHE was examined using a series of lipophilic weak-acid extractants (HA) including fluorinated alcohols and phenols in combination with *csc*-DC18C6 in nitrobenzene (NB). The high permittivity of NB favors dissociation of ion-pairs, making it easier to discern separate binding and proton-dissociation processes. The nature of the proton-ionizable extractant was found to have a strong effect, both on extraction strength and selectivity. Sodium extraction by the crown ether used alone was quantified, and the corresponding equilibrium constants ($\log K_{\text{ex}\pm}$) correlated with the standard Gibbs energy (ΔG_p°) of anion partitioning into NB; extraction was weak and nonselective for the hydroxide ion, in accord with Hofmeister bias. Upon addition of HA into the crown ether solution in NB, sodium extraction was selectively enhanced for hydroxide. The resulting SPHE qualitatively correlates with the aqueous $\text{p}K_a$ of the employed HA; the most acidic cation exchangers provide the greatest synergism. The synergistic factor obtained using a fluorinated alcohol was as high as 256. One particularly effective synergistic combination of crown with **2a** preferentially extracted NaOH over all other sodium salts, including the strongly extracted nitrate and perchlorate salts. Quantitative recovery of NaOH from the NB phase was demonstrated upon a single contact of the loaded solvent with water.

Combined Sodium Hydroxide and Sodium Nitrate Extraction. The feasibility of extracting both sodium hydroxide and sodium nitrate, two major sodium components of the tank waste, has been under investigation in the past year at PNNL.³⁰ Building on the concept of PHE, the approach taken was to introduce a neutral receptor capable of binding sodium ion, essentially in the manner of SPHE. The combination of a weak lipophilic cation exchanger (e.g., alkylated phenol) and a neutral sodium receptor (e.g., crown ether) in a suitable organic diluent thus will allow separation of the sodium ion via two mechanisms: hydroxide-driven ion-exchange and ion-pair extraction. The question being addressed concerns whether one can extend this concept to a simultaneous removal of NaOH and NaNO₃ by a single SPHE solvent system.

Given that the alkalinity and corresponding OH⁻/NO₃⁻ concentration ratio of the waste varies from tank to tank, SPHE as opposed to simple PHE provides a universal approach to effective Na⁺ extraction independently of its chemical form present in the waste solution. It also makes possible successful design of a multicycle extraction separation process. It may be envisioned that on multiple contacts of the aqueous waste by small volumes of fresh solvent, the hydroxide ion in the aqueous phase will be gradually depleted by PHE, which then gives way to ion-pair extraction of sodium nitrate. Overall, more sodium may be extracted, as it is not limited by the hydroxide content of the waste solution. To this end, the high concentration of nitrate ion in the aqueous waste is desirable, as its moderately large radius relative to other univalent aqueous inorganic anions makes it the most extractable bulk anion in the waste stream. It may also be expected that water stripping will be possible. It was discussed above that ion-pair extraction by use of a crown ether is reversible upon contact of the solvent with water. By analogy with PHE, SPHE is also reversible by water stripping, provided HA is very weak.

One of the challenges of making this type of system practical, however, results from the desirability of employing an aliphatic hydrocarbon diluent. The enhanced SPHE extraction strength toward NaOH is expected to allow flexibility in diluent selection, for example, substitution of 1-octanol with an aliphatic diluent like Isopar[®] L, a branched isoparaffinic diluent. Added crown ether is also expected to improve phase behavior in that its binding of the metal ion effectively deaggregates lipophilic metal salts at high loading.³¹

A crown ether representing the 18-crown-6 family, namely 4,4'(5')-di-*tert*-butylcyclohexano-18-crown-6 and two cation exchangers of different acidity, 1,1,1-trifluoro-3-(3,5-di-*tert*-butylphenoxy)-2-propanol **3** (pK_a = 12.5⁵) and 3,5-di-*tert*-butylphenol **1b** (pK_a = 9.9⁵) (Fig. 2), were tested using Isopar[®] L diluent and three kinds of aqueous phases: NaOH, NaNO₃, and their combination. These experiments revealed strong SPHE at high alkalinity and moderate ion-pair extraction of sodium nitrate under neutral conditions. Effect of the HA acidity on SPHE and ion-pair extraction was pronounced, phenol **1b** being stronger than fluorinated alcohol **3**. As expected, reverse efficiency order was observed for stripping. Combined extraction of sodium hydroxide and nitrate was demonstrated. The contribution of the NaNO₃ ion-pair extraction to the overall Na⁺ extraction was found to be dependent upon HA acidity and concentration in the diluent and was significantly higher for the less acidic **3**. It was shown to be possible to strip the extracted sodium with water. Although the results are promising, the following needs were identified: a) increased solubility of neutral and proton-ionizable extractants, b) higher sodium loading, and c) higher sodium nitrate extraction efficiency.

Figure 2. Crown Ethers, Cation Exchangers, and EPD Modifiers Employed.

Effect of EPD modifiers on NaNO_3 ion-pair extraction. Under neutral conditions, our results with crown ethers demonstrated that certain lipophilic alcohols mildly enhance NaX extraction by anion solvation.⁵ Further enhancement of sodium nitrate extraction is desirable, and we proposed the use of modifiers with electron-pair donor (EPD) groups to lower the sodium ion partitioning energy. The detailed investigation of such modifiers was conducted at PNNL. Again, *csc*-DC18C6 (Fig. 5) served as a model lipophilic sodium extractant. As documented by numerous crystal structures, encapsulation of Na^+ into the crown ether cavity often does not saturate its inner coordination sphere, and as a result, Na^+ readily coordinates additional ligands such as water or organic solvent molecules, oxygen donor anions, or another crown ether molecule to form a sandwich complex.³² To this end, it seems feasible to exploit this effect by introducing EPD solvating agents into the solvent. A series of EPD modifiers with strong H-bond acceptor abilities was investigated, including tri-*n*-butyl- and triphenylphosphate, tri-*n*-butyl- and triphenylphosphine oxide, *N,N*-di-*n*-butyl- and *N,N*-di-phenylacetamide, and 1-octanol (Fig. 2). The extraction behavior of *csc*-DC18C6 was characterized by systematic variation of the aqueous-phase sodium nitrate concentration at fixed composition of the NB phases containing 0.2 M EPD modifier and 0.05 M *csc*-DC18C6 (Fig. 3). Comparison of the extraction isotherms obtained with and without EPD modifiers in the NB phase indicates that the EPD modifiers moderately increase NaNO_3 extraction by *csc*-DC18C6. Distribution results for the crown ether used alone or with the solvating agents were successfully fit using the SXLSQI modeling program, whereupon the obtained extraction constants were found to correlate linearly

with the EPD strength of the added modifiers described by the Kamlet-Taft β solvatochromic parameter³³ (Figure 4-a). These results provide the means for the quantitative prediction of the extraction performance of the modified diluent. In the presence of the phenol, the EPD solvating agents slightly lowered NaNO_3 extraction by *csc*-DC18C6 and phenol, which, however, remained higher than NaNO_3 extraction by *csc*-DC18C6 alone. This slight reduction in extraction strength was attributed to the competitive interaction between phenol and EPD modifier.

Figure 3. Dependence of NaNO_3 extraction on the aqueous NaNO_3 concentration by *csc*-DC18C6 into NB with and without solvent modifier.

Figure 4. Dependence of NaNO_3 extraction by *csc*-DC18C6 into NB on a) basicity of the EPD solvent modifier or b) hydrogen-bond donicity of the HBD solvent modifier.

Investigation of hydrogen bonding in ion-pair extraction. Addition of a weak organic acid to an organic phase lowers the anion-partitioning energy barrier based upon an H-bond interaction between the organic acid and the anion.^{9,10} As demonstrated previously, the stability of the anionic solvate formed in the NB phase depends on the pK_a of the organic acid.⁵ Quantitative assessment of this effect on the $NaNO_3$ extraction was conducted employing solvating agents **1b** and **11** possessing different abilities to donate an H-bond as given by the solvatochromic parameter³³ α equal to 0.77 and 1.65, respectively. 1-Octanol **11** also exhibits EPD properties similar to those of EPD modifiers discussed above; its β parameter³³ is 0.81. Phenol **1b** is a weak EPD with a β parameter of 0.3, similar to that of NB.³³ The extraction behavior of *csc*-DC18C6 was characterized by systematic variation of the aqueous-phase sodium nitrate concentration at fixed composition of the NB phases containing 0.2 M **1b** or **11** and 0.05 M *csc*-DC18C6 (Fig. 3). 1-Octanol **11** exhibited only marginal enhancement of $NaNO_3$ extraction, on a par with the EPD modifiers tested. Significant extraction enhancement was observed with the phenol **1b** which surpassed the performance of the EPD solvating agents. The distribution data were fit using the SXLSQI modeling program. Values of $\log K_{ex\pm}$ exhibited a linear dependence on α (Fig. 4-b).

Understanding the effect of an HBD modifier on ion-pair extraction involves assessment of many different processes such as H-bonding with the anion, aggregation, and solvation of the free extractant and its cationic complex. While EPD properties of the solvent modifier are important in solvation of the complex cation, solvation of the free crown ether is based upon specific H-bond interactions with the HBD groups of the modifier. One example is the hydration of crown ethers, a phenomenon which was extensively investigated over the last two decades.³³ Among organic acids, formation of the phenol-crown ether H-bond-based aggregates in the solid state was found to influence the conformation of the macrocycle.³⁴ In solution, a similar effect was demonstrated in a study of the reverse-phase HPLC separation of phenol and its derivatives.³⁵ For compounds containing the hydroxyl group, the addition of 18-crown-6 to the mobile phase led to a decrease in retention time, which was explained by the complexation between the hydroxy compounds and the crown ether. This H-bonding of the HBD modifier to the oxygen donor atoms of the crown ether could potentially compete with metal ion interaction and partially suppress the gain in extraction due to favorable anion solvation by HBD modifier.

To probe H-bonding interactions in the NB extraction phase, an IR investigation of the O–H bonds of phenol and water in NB in the presence of free or Na^+ -loaded crown ether *csc*-DC18C6 is under way. A series of FTIR spectra of the water-washed solutions of phenol **1b** in the 0.05–0.8 M concentration range were acquired. Phenol **1b** exhibited no self-aggregation in NB, as no signal broadening, position shift, or appearance of new bands was found for the narrow band of its O–H group. In agreement with literature reports,³⁶ the free crown ether *csc*-DC18C6 in NB without phenol was found to exist in the hydrated form. The broad water O–H band in the 3200–3700 cm^{-1} region has three maxima corresponding presumably to a crown-water adduct in which the water molecule is coordinated to the crown ether in mono- and bidentate fashion (Fig. 5). Loading of the crown ether with Na^+ ion slightly shifts, and increases the relative intensity of, the high-energy water O–H band at 3665 cm^{-1} . Addition of the phenol to the Na^+ -loaded crown ether causes the appearance of the new band at 3250 cm^{-1} due to the H-bonding of the phenolic O–H group to the NO_3^- anion. This phenol-nitrate interaction lowers the energy barrier of the nitrate partitioning into NB and boosts the ion-pair sodium extraction.

Figure 5. IR spectra of the O–H bond of phenol and water in NB in presence of *csc*-DC18C6 and/or NaNO₃.

Ditopic pseudo hydroxide extraction. Synthesis efforts at UNT (A. P. Marchand) have focused on the synthesis of crown ethers³⁷ and calixarene crown ethers³⁸ with appended weakly ionizable functionalities. Most examples have employed cage substituents on the polyether ring to confer lipophilicity and ring rigidity. The proton-ionizable substituents are essentially the same groups used in the weakly acidic fluorinated alcohols tested for PHE. The ditopic compounds by contrast are expected to lead to a greater degree of control over cation selectivity and possibly enhanced extraction strength. The compounds shown in Figs 6 and 7 were prepared.

Survey extraction experiments under way entail examining sodium distribution ratios (D_{Na}) for the synthesized weakly acidic crown compounds dissolved in purified NB. The non-ionizable control compounds are run by themselves and also with added control fluorinated alcohols that match the type of ionizable group on the corresponding ditopic extractants. One ionizable control is 1H,1H,9H-hexadecafluoro-1-nonanol (**4**), and the other is 4-*n*-octyl- α,α -(trifluoromethyl)benzyl alcohol (**2a**). The former is commercially available, and the latter was prepared at ORNL by the Friedel-Crafts reaction between phenyloctane and hexafluoroacetone.¹⁵ Two experiments are being run: a) variation of aqueous [NaCl] and b) variation of aqueous [NaOH] in a constant aqueous concentration of NaCl. The first experiment essentially measures the relative strength of Na⁺ binding and extraction without dissociation of the terminal –OH group. The second experiment then measures the total Na⁺ binding and extraction as proton-dissociation is "turned on". Preliminary assessment of the data collected thus far reveals expected behavior in terms of the NaCl and NaOH dependences described earlier. Unfortunately, there is as yet no evidence for any of the new ditopic compounds exhibiting enhanced NaOH extraction

Figure 6. Synthesized weakly acidic proton-ionizable crown ethers and calixarene crown ethers for ditopic pseudo hydroxide extraction.

over and above their corresponding control systems (SPHE systems consisting of crown control plus proton-ionizable control). This may be attributed to the length of the proton-ionizable sidearms and its lack of preorganization for cooperativity with the crown ring.

Planned Activities

A renewal proposal has been submitted, outlining a plan for continued effort toward the objectives given above. In the proposed efforts, a thermochemical study of PHE relating extractant acidity to extraction strength will be completed, and this study will be extended to systems containing crown ethers, including proton-ionizable ones. A series of crown ethers will be synthesized at ORNL for this purpose as well as to investigate the extraction of bulk sodium salts (e.g., nitrate, nitrite, and sulfate), possibly in combination with sodium hydroxide. Simple proof-of-principle tests with real tank waste at PNNL will provide feedback toward solvent designs that have desirable properties.

Figure 7. Additional synthesized weakly acidic proton-ionizable crown ethers and calixarene crown ethers for ditopic pseudo hydroxide extraction.

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Information Access

A complete list of publications, patent application, and presentations for this project is also available as an attachment to this report. A final report for the first three years of the project provides detailed information on early accomplishments of this project.²⁰ See also the www home page of the ORNL Chemical Separations Group: URL <http://www.ornl.gov/csg>.

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