**RELAP5/MOD3.2 Analysis of INSC Standard Problem INSCSP-V4:
Investigation of Heat Transfer for Partly Uncovered VVER-1000 Core at the
Test Facility KS (RRC KI)**

by
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ABSTRACT

The RELAP5/MOD3.2 computer program has been used to analyze a series of tests investigating heat-transfer from a partly uncovered VVER-1000 core in the KS test facility at the Russian Research Center “Kurchatov Institute” (RRC-KI). The analysis documented represents VVER Standard Problem 4 in Joint Project 6, which is the investigation of Computer Code Validation for Transient Analysis of RBMK and VVER Reactors, between the United States and Russian International Nuclear Safety Centers. The experiment facility and data, RELAP5 nodalization, and results are shown for one of the six tests defined in Standard Problem 4. Only part of the data was analyzed due to our conclusion that the available experimental data is not sufficient to allow the modeling of the actual experiment sequence. The experiment initial conditions were reached through a series of transient processes, about which no quantitative information was available. This has required the modeling of an arbitrary computational transient, with the goal of reaching initial conditions similar to those observed during the experiment. The use of an arbitrary transient introduces many degrees of freedom in the analysis, i.e. initial computational values that influence the entire sequence of events, including the loop behavior during the experiment time window.

Reasonable agreement between RELAP5 and the experiment data can be obtained by manipulating a number of initial computational values, including the liquid level in the fuel assembly model, the liquid level in the annular region, the quality of the saturated vapor in the voided loop regions, etc. Our study has focused on exploring the sensitivity of results to changes in these initial values which are not based on experimental information, but are selected with the goal of matching the experimentally observed behavior during the experiment time window. We have shown that changes in several initial arbitrary values can lead to similar changes in the calculated loop behavior. Other parameters exist which can directly influence the calculated results, which have been only minimally explored, or have not been explored at all due to lack of time. Because we are not modeling the entire sequence of events which led to the initial experiment conditions, it is not possible to assume that by matching a limited set of measured parameters at the beginning of the experiment time window we have reproduced all the initial actual conditions. We conclude that the analysis of these experiments, while providing a useful demonstration of the RELAP5 capabilities to describe the experimental sequence of events, cannot be used to draw quantitative conclusions about the adequacy of specific RELAP5 models.

TABLE OF CONTENTS

	<u>Page</u>
ABSTRACT.....	3
LIST OF FIGURES	5
LIST OF TABLES.....	5
LIST OF SYMBOLS AND ABBREVIATIONS	6
1. Introduction	7
1.1 Objective.....	7
1.2 Background.....	7
1.3 Study Description	7
1.4 Report Organization	8
2. Description of KS-1 Test Section.....	8
2.1 Description of Experimental Section Hydraulic Circuit.....	8
2.2 Description of Measurement System.....	9
3. Description of Tests	12
3.1 Experimental Methodology	13
4. Released Code Version and Input Deck Descriptions	14
4.1 Description of RELAP5/MOD3.2	14
4.2 Description of Baseline Input Deck.....	14
4.3 Initialization of Base Case.....	18
4.4 Description of Sensitivity Cases.....	20
4.4.1 Sensitivity Cases Examining Initial Thermal-Hydraulic Conditions.....	20
4.4.2 Sensitivity to Loop Nodalization	20
5. Results	20
5.1 Base Case Results.....	21
5.1.1 KS1-18-2 Test Data Description.....	21
5.1.2 KS1-18-2 Test Modeling of Initial and Boundary Conditions.	21
5.1.3 Base Case Computational Results and Comparison to Test Data.....	24
5.1.3.1 Calculated Initial Conditions.	24
5.1.3.2 Calculated results during the experiment time window.	33
5.2. Sensitivity Case Results	34
5.2.1 Effect of vapor quality in the voided loop regions.	34
5.2.2 Effect of initial liquid level in the heated core region.	35
5.2.3 Effect of initial liquid level in the annular region.....	37
5.2.4 Effect of core exit nodalization and related liquid level.	37
6. Conclusions	39
Appendix A – Model Nodalization Summary	43
Appendix B – Base Case RELAP Input File	44
Appendix C – Peer Review of Input File.....	121

LIST OF FIGURES

	<u>Page</u>
2-1 Schematic of KS-1 VVER Test Loop	11
2-2 Schematic of KS-1 VVER Core Simulator	11
2-3 KS-1 VVER Primary System Measurement	12
2-4 KS-1 FA Thermocouple and Pressure Sampling Points	12
4-1 Baseline V4 RELAP5 Loop Nodalization.....	16
4-2 Baseline V4 RELAP5 Core Nodalization	16
5-1 Fuel Assembly Model Power, Test KS1-18-2.....	22
5-2 Loop Heat Loss Correction Coefficient, Test KS1-18-2.....	22
5-3 Pressure at FA Model Outlet Pout, Test KS1-18-2.	25
5-4 Measured rod wall temperatures at time t _{0exp} , Test KS1-18-2.....	25
5-5 Calculated rod wall temperatures at time t _{0exp} , Test KS1-18-2	26
5-6 Coolant temperature at core model inlet T _{Fin} , Test KS1-18-2.....	26
5-7 Calculated Inner Wall Temperatures, Test KS1-18-2.	27
5-8 Calculated Inner Rod Wall Temperatures, Test KS1-18-2.	27
5-9 Calculated Inner Rod Wall Temperatures, Test KS1-18-2.	28
5-10 Calculated Inner Rod Wall Temperatures, Test KS1-18-2.	28
5-11 Calculated and Measured Rod Wall Temperatures , Test KS1-18-2.	29
5-12 Calculated and measured rod wall temperatures, Test KS1-18-2.	29
5-13 Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.	30
5-14 Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.	30
5-15 Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.	31
5-16 Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.	31
5-17 Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.	32
5-18 Collapsed Liquid Level in the FA Model, Test KS1-18-2.....	32
5-19 Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 1.	36
5-20 Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 2.	36
5-21 Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 3.	38
5-22 Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 4.	38
5-23 Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 5.	39
5-24 Core Exit Nodalization – A.....	40
5-25 Core Exit Nodalization - B.....	40

LIST OF TABLES

	<u>Page</u>
3-1 Quasi-steady parameter values for the 6 experiments chosen.....	12
4-1 Baseline Input Deck Numbering Scheme.....	16
A-1 Baseline RELAP5 Model Nodalization.....	43

LIST OF SYMBOLS AND ABBREVIATIONS

Symbols

Closs	=	heat loss multiplier
FA	=	fuel assembly
Hannulus(liquid)	=	liquid level in the annular space surrounding the fuel assembly, m
Hcore(liquid)	=	liquid level in the fuel assembly, m
Hdowncomer (liquid)	=	liquid level in the downcomer, m
LP	=	lower plenum
P _{out}	=	core outlet pressure, Pa
SG	=	steam generator
t0(calc)	=	RELAP calculation at the beginning of the experiment time window
t0 (exp)	=	experiment time at the beginning of the experiment time window
TF _{in}	=	water temperature in the lower plenum, K
TF _{fa}	=	coolant temperature at fuel assembly outlet, K
TF _{dc}	=	coolant temperature at the downcomer, K
TF _{up}	=	coolant temperature in the upper plenum, K
TW _{i-k}	=	heated rod wall temperature, K
UP	=	upper plenum
VVER	=	Russian Light Water Pressurized Reactor

Abbreviations

ANL	Argonne National Laboratory
RMINSC	Russian Minatom International Nuclear Safety Center
RRC KI	Russian Research Center Kurchatov Institute
SP	Standard Problem
USDOE	United States Department of Energy
USINSC	United States International Nuclear Safety Center
USNRC	United States Nuclear Regulatory Commission

1. Introduction

1.1 Objective

Validation of computer codes for use in safety analysis of VVER reactors has been identified as a topic for a joint research project between the U.S. and the Russian Minatom International Nuclear Safety Centers (USINSC/RMINSC). The goal of Joint Project 6 is to initiate the collaboration between the U.S. and Russian Minatom International Nuclear Safety Centers on the validation of computer codes related to nuclear power plant operational and safety analysis. The computer code covered in this project is RELAP5/MOD3.2 [1], which is the code in use for the in-depth safety assessment projects under the USDOE International Nuclear Safety Program.

1.2 Background

Earlier phases of Joint Project 6 included the development of a prioritization report, documenting the safety significant processes and phenomena occurring in VVER type reactors. The resulting VVER prioritization report [2] was used to develop a validation plan for ranking potential Russian tests relative to these safety significant processes and phenomena. The resulting VVER validation plan [3] identifies a number of potential standard problems that could be defined for assessing the capabilities of RELAP5/MOD3.2 in modeling VVER specific safety issues. The working basis for the code validation project is to establish standard problems based on experimental data and then perform the analysis for the standard problems with RELAP5/MOD3.2. The results of the computer analysis will be compared with the experimental results, and the adequacy of the code to model the specific phenomena will be assessed. The standard problems are defined by the RMINSC using experimental data from Russian facilities that simulate VVER behavior. The standard problems will be analyzed by U.S. and Russian analysts, and potentially by other international participants. Following the analysis of each specific standard problem by all teams involved, the results will be compared to assess the modeling capabilities of RELAP5 relative to the specific safety parameters thought to be addressed by the standard problem.

1.3 Study Description

The purpose of this report is to document the USINSC analysis for VVER standard problem 4 that has been defined in the “Standard Problem INSCSP-V4 Definition Report” [4]. This standard problem represents heat-transfer under partly uncovered core conditions.

The VVER validation plan [3] identified one phenomenon that was well covered by the data in Standard Problem 4. This phenomenon was **“heat transfer in a partially uncovered core”**. The adequacy of RELAP5/MOD3.2 to model the above phenomena is limited by the measurements available in the KS-1 facility and the facility design. As identified in [4], the test section configuration is such that heat losses to the ambient air (due to condensation dominated heat-transfer) exceed the heat injected into the coolant through the rod simulators. This leads to unsteady or quasi-steady behavior of the system resulting in a slow pressure decrease during the test measurement period and significant changes in the core liquid coolant level. Because the RELAP5 initialization does not simulate the actual sequence of events preceding the data collection window, the correct modeling of the unsteady conditions during the experiment is

difficult and must be verified carefully. The test results do not include coolant flow measurements, which adds to the difficulty in initializing the RELAP5 model.

1.4 Report Organization

Sections 2 and 3 of this report describe the KS-1 test section and the specific tests conducted, respectively. Section 4 provides a brief description of the RELAP5/MOD3.2 code as well as descriptions of the baseline input deck and sensitivity case input decks. Section 5 presents the results of the present RELAP5 analysis with comparisons to the specific test data described in the Definition Report. Conclusions from this analysis are shown in Section 6. The appendices include the RELAP model nodalization details, the base case RELAP5 input files, and peer review comments. A similar report is being prepared by the Russian analysis team. These two reports will be used to prepare a comparative analysis report covering the work of both teams.

2. Description of KS-1 Test Section

VVER Standard Problem 4 is based on heat-transfer under partly uncovered core conditions in the KS-1-VVER test section of the KS test facility at RRC Kurchatov Institute (KI). The KS test facility was designed to study thermal-hydraulic processes under normal, transient, and emergency conditions in water-cooled, water-moderated power reactors of the VVER-type, channel uranium-graphite reactors of the RBMK type, and water-cooled, water-moderated reactors of an integral layout (AST and VPBER type). The test facility was designed to investigate both separate effects and integral thermal and hydraulic processes in sections of the primary circuit

Experimental section KS-1 was developed within the KS test facility for the purpose of modeling thermal-hydraulic processes in a VVER core under postulated small break LOCA conditions. This special section used the RBMK fuel channel model as a downcomer and test section 1 as the rising section of a closed circuit to evaluate integral loop effects. Experimental section KS-1-VVER-1000 has been designed for modeling of heat transfer processes in a partly uncovered VVER-1000 core at small residual heat power under conditions of natural coolant circulation stagnation and for medium and low pressure ranges.

2.1 Description of Experimental Section Hydraulic Circuit

The KS-1-VVER-1000 test section is a semi-integral, one loop model of a VVER primary system. A schematic of the test section is shown in Fig. 2-1. The experimental section includes models of the main elements of a VVER type reactor, including a downcomer, upper plenum (UP), lower plenum (LP), hot and cold legs of the primary coolant loop and the steam generator (SG) simulator. The hydraulic circuit, depicted in Fig. 2-1, consists of the following components:

- downcomer model (1),
- lower plenum model (2),
- core model (3),
- upper plenum model (4),
- loop hot leg model (5),
- horizontal steam generator tube bundle simulator (6, 7),

loop cold leg model (8), and
lower pipeline (9).

The lower pipeline connects the bottom of the downcomer model and lower plenum model. The hot leg simulator and the steam generator simulators are slightly inclined to allow drainage of liquid condensate back to the upper plenum and downcomer regions of the loop. The entire loop represents a natural coolant circulation circuit which simulates a semi-integral, one loop model of a VVER primary system.

The unforced water flow rate at the core model inlet under steam-condensate circulation conditions is governed by the natural hydraulic head in the loop. This is established by the heating of the water in the core simulator, steam generation and superheating in the core model, followed by subsequent cooling and condensation of steam in the upper plenum, in the hot leg model, in the SG tube bundle simulators, in the cold leg model and also in the DC model.

The initial conditions for partly uncovered core regimes and for coolant natural circulation regimes following potential break conditions were established by a combination of the following actions:

- releasing steam from SG tube bundle simulator to expansion tank through valve 1, or
- by draining water from the lower pipeline (9) to the expansion tank through valve 2, or
- feed water connections to the lower pipeline (9) through valve 2 or valve 3.

The VVER horizontal tube bundle SG is simulated by two un-insulated piping sections with passive heat removal. The SG simulator only qualitatively simulates the hydrodynamics and heat transfer processes under steam condensation in the horizontal, steam generator tube bundle. For this reason the KS-1 experimental section is considered to be a semi-integral model of a VVER primary system. The core simulator, depicted in Fig. 2-2, incorporates a fuel assembly (FA) model consisting of 19 electrically heated tubes with a diameter of 9 mm and a heated zone height of 2.505 m. The pertinent geometrical details describing the test loop components as well as the fuel assembly simulator are incorporated into the Definition Report [4].

2.2 Description of Measurement System

The measurement scheme for the KS-1 VVER primary system model is shown in Fig. 2-3. The locations of the gauges in the downcomer model, lower plenum model, core model, upper plenum model and lower pipeline are presented on this schematic diagram. The parameters measured are summarized below:

Static pressure (***P_{out}***) of the coolant in the core model outlet was measured with a reference manometer. Pressure differences around the major loop components (***DL13-12***, ***DL2-4*** and ***DL4-14***) were measured with difmanometers. Pressure

Figure 2-1. Schematic of KS-1 VVER Test Loop

Figure 2-2. Schematic of KS-1 VVER Core Simulator

Figure 2-3. KS-1 VVER Primary System Measurement

Figure 4 KS-1 FA Thermocouple and Pressure

Figure 2-4. KS-1 FA Thermocouple and Pressure Sampling Points

differences in the core model (*DL4-3, DL5-4, DL6-5, DL7-6, DL8-7, DL9-8, and DL11-10*) were also measured with difmanometers.

The coolant temperatures in the lower plenum model (*TFin*), at the FA model outlet (*TFfa*), at the upper plenum model inlet (*TFup*) and in the DC model (*TFdc*) were measured with chromel-copel thermocouples connected to the data acquisition computer through transducers.

The measurement scheme for the KS-1 VVER core fuel assembly model is shown in Fig. 2-4. This figure indicates the axial locations of the various fuel assembly temperature and pressure sampling locations. Measurements of axial and radial temperature distributions in the FA model were made with 33 thermocouples installed inside 14 rod simulators on 20 elevations. The temperatures of the rod simulator inner surface (*TWi-k*) were measured with chromel-copel and chromel-alumel thermocouples. All thermocouples were connected to the data acquisition computer through transducers.

3. Description of Tests

In 1991, investigations of unsteady boiloff, core uncovering and heat-transfer in partly uncovered FA models were conducted under quasi-steady and unsteady conditions at experimental section KS-1. Fuel pin transient temperatures were measured for a VVER-1000 FA model at small values of residual heat power under conditions of steam-condensate circulation for different levels of two-phase mixture in the core for quasi-steady flow regimes. The results of six experiments were chosen to formulate standard problem V4 to evaluate the adequacy of RELAP5 for modeling the conditions corresponding to a partly uncovered core at residual power. The tests selected (KS-1-18-1, KS-1-18-2, KS-1-19-1, KS-1-19-2, KS-1-33-1, and KS-1-34-1) represent variations in mixture level, heat flux, pressure, and steam flow rates as depicted in Table 3-1.

Table 3-1 Parameter values for the 6 experiments chosen at time t0(exp)

Experiment	Power W(t0), kW	Pressure Pout(t0), bar	Mixture level Lm(t0), m	Temperature TFin(t0), °K
KS1-18-1	20.5	67	1.62	478.15
KS1-18-2	14.5	60	1.78	479.15
KS1-19-1	21.2	35	2.29	489.15
KS1-19-2	12.9	31	1.78	488.15
KS1-33-1	9.6	31	< 0	507.15
KS1-34-1	9.4	34	0.62	511.15

Test data was recorded for the following parameters: the loop pressure at the core model outlet, differential pressures in the core region and around the primary loop, coolant temperatures at the core inlet, outlet and downcomer, 33 rod simulator wall temperatures at combinations of 14 radial and 20 axial locations, as well as the current and voltage drop across the heated channel

(representing the electrical power of the FA model). Coolant flow rates were not measured due to insufficient measurement ranges of the instrumentation.

The goals of the experiments included:

- 1) obtaining test data on axial and radial temperature distributions within the fuel rod simulators under various power and coolant levels in the core model,
- 2) determination of the influence of thermal and hydraulic processes in the primary loop component models under partly uncovered core conditions,
- 3) determination of the influence of loop pressure on the temperature distribution of the rod simulators under constant values of power and core mixture level for partly uncovered core conditions.

3.1 Experimental Methodology

Experiments on modeling of quasi-steady regimes of steam-condensate circulation and partly uncovering of the core were conducted under various pressures, coolant temperatures in the lower plenum model, different mixture levels in the core and various power levels. To establish the appropriate experimental conditions, preliminary heating of the coolant water and pipeline metal to the required temperature at the core model inlet was performed under forced coolant circulation. The VVER loop model was next isolated from the forced circulation circuit of the KS facility. A smooth increase of the FA power was imposed to establish a single-phase (non-boiling) natural circulation regime. Heating of the coolant water increased the coolant pressure to 80-90 bar. Coolant drainage from the SG tube bundle simulator to the expansion tank was initiated through valve 1. After the onset of boiling at the core outlet, a natural circulation, boiling regime was established in the loop under slightly greater pressure and coolant inlet temperature than specified for the test. Some steam was released from the tube bundle simulator to the expansion tank through valve 1.

Full draining of the UP model was made after the pipeline metal temperature in the upper part of the VVER circuit model reached saturation conditions near the specified values of pressure and coolant temperature at the core inlet for the individual tests. Also the core mixture level was established by draining water from the lower pipeline to the expansion tank through valve 2.

After establishment of the appropriate inlet coolant temperature and mixture level in the core model, the main test was conducted for investigating heat-transfer in the partly uncovered FA model under conditions of steam-condensate circulation with constant FA power under a quasi-steady regime. During the test measurement window, valves 1, 2, and 3 were closed. The quasi-steady behavior of these tests is due to the condensation dominance of the test loop design. The condensation dominance is the result of heat losses from the test loop exceeding the electrical power added to the core simulator rods, thereby causing a slow decrease in system pressure, core mixture level variations and variations in rod simulator wall temperatures.

4. Released Code Version and Input Deck Descriptions

The RELAP5/MOD3.2 computer program was used for the calculations reported in this report. A detailed description of RELAP5/MOD3.2 is given in Reference 1

4.1 Description of RELAP5/MOD3.2

The RELAP5 code has been developed for best-estimate transient simulation of light water reactor coolant systems during postulated accidents. The code models the coupled behavior of the reactor coolant system and the core for loss-of-coolant accidents and operational transients such as anticipated transient without scram, loss of offsite power, loss of feedwater, and loss of flow. A generic modeling approach is used that permits simulating a variety of thermal hydraulic systems. Control system and secondary system components are included to permit modeling of plant controls, turbines, condensers, and secondary feedwater systems.

The RELAP5 computer program was developed by staff at the Idaho National Engineering and Environmental Laboratory (INEEL) under funding from the U. S. Nuclear Regulatory Commission (USNRC) for the analysis of transient behavior in light water reactors. This computer program continued the development which began in 1966 with the RELAPSE code, followed by RELAP2, RELAP3, and RELAP4. The principle new feature of the RELAP5 series is the use of a two-fluid, non-equilibrium, non-homogeneous, hydrodynamic model for transient simulation of two-phase system behavior. The hydrodynamic model is a one-dimensional, transient, two-fluid model for flow of a two-phase liquid-vapor mixture which can contain noncondensable components in the vapor phase and/or a soluble component in the liquid phase. Eight field equations are solved for eight primary independent variables: pressure, two phasic (i.e., one for liquid and one for vapor) specific internal energies, vapor volume (i.e., void) fraction, two phasic velocities, noncondensable quality, and soluble component (e.g., boron) density.

The RELAP5/MOD3.2 computer program was obtained from the INEEL, which, at that time, was the RELAP5 maintenance organization for the USNRC. The program has been installed in such a way as to be accessible to a network of Sun Microsystem workstation computers running under SunOS/5.6 (a version of UNIX) in the Reactor Analysis and Engineering Division at Argonne National Laboratory. No modifications have been made to the source code.

4.2 Description of Baseline Input Deck

All of the major features of the KS-1-VVER-1000 test circuit were included in the RELAP5 input model. Figure 4-1 depicts a nodalization diagram of the baseline input model. Figure 4-2 presents a more detailed diagram of the upper core nodalization. The hydraulic model contains 182 volumes with 182 junctions. The integrated hydraulic circuit model represents a system volume of 0.448 m³ consisting of a total system fluid mass of 125.66 kg. The zero reference elevation was specified at the bottom of the active (heated) core region for monitoring loop

closure calculations. Standard modeling guidelines were followed to the extent possible in developing the nodalization of the system.

The heat loss from the circuit primary and secondary system components to the ambient air was represented in the RELAP5/MOD3.2 model by entering convective boundary conditions at the exterior surfaces of all pipe volumes and other component boundaries. The definition report [4] prescribed specific constant heat transfer coefficients as a function of circuit component pipe diameter. These heat transfer coefficients were applied as constant values during the data measurement window. The code calculated the heat transferred to a constant temperature boundary condition held at the ambient room temperature (300 K). Appropriate temperature dependent material properties were input for the various piping components modeled. The external insulation surrounding the various circuit components was not modeled as separate heat structures because specific data was not provided for insulation thickness. Rather, the insulation was modeled by applying the convective heat transfer coefficients provided in the definition report. The RELAP5 heat structure model consists of 202 heat structures with 730 mesh points. The estimated total exterior circuit heat-transfer surface area of the model is approximately 25.7 m².

Table A1 in Appendix A provides a summary of the baseline RELAP5 model nodalization. This table describes for each major facility component the corresponding RELAP5 components which are defined to model the facility component. The description incorporates the RELAP5 component number, a brief description of the RELAP5 component, the RELAP5 component name and type, the number of volumes within each component, the hydraulic diameter, the flow area, the length, the number of associated junctions, and the connecting volume components if the component is a junction. The correspondence of the KS-1-VVER-1000 test section components with the baseline input deck numbering scheme is presented in Table 4-1 which identifies the RELAP5 component numbers and corresponding heat structures.

Table 4-1 Baseline Input Deck Numbering Scheme

KS-1 Component	RELAP5 Components	Heat Structures
Downcomer	100, 101, 150, 151	1000, 1010, 1500, 1510
Lower Pipeline	900, 901, 940, 941, 960, 961	9000, 9400, 9600
Lower Plenum	200	2000
Core Inlet	220, 250, 251, 280, 281	2200, 2500, 2501, 2800
Fuel Assembly	300	3000, 3001
Core Annulus	350, 351	3500
Core Outlet	399, 400, 401, 450, 480	4000, 4001, 4002, 4500, 4800
Upper Plenum	490, 491	4900
Loop Hot Leg	500, 501	5000, 5010
SG Tube Bundles	600, 601, 700	6000, 6010, 7000
Steam Release Pipe	650	6500
Loop Cold Leg	701, 800, 801, 850, 851	7010, 8000, 8010, 8500, 8510

The following is a brief narrative description of the RELAP5 nodalization. All volume components are numbered with even component numbers, with the exception of branch components. Typically, all junction components, including branch components, are numbered with odd component numbers.

The KS-1 downcomer is simulated by two pipe components (100, 150) and their corresponding outlet junctions represented by two branch components (101, 151). Heat-transfer from the exterior surfaces of these components to the ambient air is simulated by corresponding heat structures 1000, 1500, 1010, and 1510.

The KS-1 lower pipeline is simulated by three pipe components (900, 940, 960) and their corresponding outlet junctions represented by three single junctions (901, 941, 961). Heat-transfer from the exterior surfaces of these components to the ambient air is simulated by corresponding heat structures 9000, 9400, and 9600.

The KS-1 lower plenum is simulated by a single pipe component (200). Heat-transfer from the exterior surfaces of this component to the ambient air is simulated by corresponding heat structure 2000.

The KS-1 core simulator is represented by a core inlet section, a fuel assembly section, a core annulus section and a core outlet section as follows:

- The core inlet section is simulated by an inlet branch component (220), two annulus components (280, 250) representing the region below the fuel assembly and the surrounding annular region, and two connecting single junctions (251, 281). Heat-transfer from the exterior surfaces of these components to the ambient air is simulated by corresponding heat structures 2200, 2500, and 2501. Additionally, heat structure 2800 simulates heat-transfer between the lower, inner annulus (component 280), the surrounding annular region (component 250) and the steel separating these two regions.
- The fuel assembly section is simulated by a single pipe component (300) consisting of 20 volumes along the fuel pin axis. Heat generated within the fuel pins is simulated by a heat source (3000). Heat-transfer from the exterior surfaces of fuel pins to the coolant channel fluid is simulated by a convective boundary condition from a vertical bundle without crossflow. Heat-transfer from the coolant channel fluid to the surrounding core simulator shroud is simulated by a convective boundary condition in heat structure 3001. The shroud is modeled as a composite heat structure with steel and insulation thermal properties incorporated.
- The core annulus section is simulated by a single annulus component (350) and a single junction connecting the annulus to core inlet annulus 250. Heat-transfer from the exterior surfaces of the core simulator annulus to the ambient air is simulated by corresponding heat structure 3500.
- The core outlet section is simulated by an outlet branch component to the upper plenum (480), two annulus components (400, 450) representing the space above the fuel assembly and the surrounding annular region, and a connecting junction (401). Heat-transfer from the exterior surfaces of these components to the ambient air is simulated by

corresponding heat structures 4800, 4500, 4001, and 4002. Additionally, heat structure 4000 simulates heat-transfer between the upper, inner annulus (component 400), the surrounding annular region (component 450) and the steel separating these two regions.

The KS-1 upper plenum is simulated by a single pipe component (490) and a corresponding outlet single junction (491). Heat-transfer from the exterior surfaces of this component to the ambient air is simulated by corresponding heat structure 4900.

The KS-1 loop hot leg is simulated by a single pipe component (500) and outlet branch component (501). Heat-transfer from the exterior surfaces of these components to the ambient air is simulated by corresponding heat structures 5000 and 5010.

The KS-1 steam generator tube bundles are simulated by two pipe components (600, 700) and a connecting tee represented by branch 601. Heat-transfer from the exterior surfaces of these components to the ambient air is simulated by corresponding heat structures 6000, 7000 and 6010. The KS-1 steam generator tube bundles are not insulated. Therefore, the enhanced heat-transfer expected from these uninsulated surfaces is modeled by specifying larger heat-transfer coefficients as indicated in the definition report [4].

The KS-1 steam release pipe is simulated by a single pipe component (650). Heat-transfer from the exterior surfaces of this component to the ambient air is simulated by corresponding heat structure 6500.

The KS-1 loop cold leg is simulated by two pipe components (800, 850), connecting outlet connections represented by single junctions (801, 851) and a branch component (701) connecting the cold leg to the steam generator tube bundle. Heat-transfer from the exterior surfaces of these components to the ambient air is simulated by corresponding heat structures 8000, 8500, and 7010.

Horizontal pipes connecting directly to vertical pipes were modeled with the momentum flux turned off at the connections to the vertical components to better simulate the effects of the change in flow direction. These modeling assumptions were applied at the hot leg connection to the upper plenum, the upper downcomer connection to the lower downcomer section, the lower pipeline connection to the lower downcomer section, and both the inlet and outlet connections to the core simulator.

The RELAP5/MOD3.2 CCFL model was applied at single junction 251, the junction between the volume beneath the core simulator and the bottom annular chamber in the core simulator. This junction was selected because it represents a location where the flow path was horizontally oriented, the flow area is reduced substantially, and it modeled a region of the flow circuit where CCFL might be expected to occur.

Choking was turned off at all junctions as recommended in the code user guidelines.

4.3 Initialization of Base Case

The test conditions were determined by both the initial conditions at the beginning of the experiment and the boundary conditions imposed on the experimental loop during the

measurements. To correctly model the experiment using RELAP5 both the initial conditions at the beginning of the experiment and the boundary conditions should match the actual values. To achieve this would require the RELAP simulation of the thermo-hydrodynamic transients which preceded the experimental window. The complex series of actions taken to initiate the experiment, combined with the lack of quantitative information (e.g. sequence and timing of events) have prevented the use of this approach. Instead, a simplified transient event was modeled, as described below, with the goal of reaching a set of reasonable initial conditions at the beginning of the experiment period.

The RELAP5 simulation was initiated at the time $t_0(\text{calc})$ using a set of simple initial conditions. These conditions were selected to reflect a reasonable and consistent state of the loop, assuming certain liquid levels and temperatures in various loop sections. The loop pressure was initiated to the core outlet pressure $P_{\text{out}}(t_0(\text{calc}))$, selected to be higher than the measured pressure $P_{\text{out}}(t_0(\text{exp}))$. The lower part of the loop was assumed to contain saturated liquid up to a certain level. Above that level the loop was assumed to contain saturated wet vapor. The RELAP5 simulation was run for a time interval of 100 s, with no fuel assembly (FA) heat release and zero heat losses. This calculation allows the liquid levels around the loop to reach consistent values and the equilibration of coolant and loop structure temperatures.

The simulation was continued by a second phase, between 100-400 s, during which the both the FA power and the loop heat losses were increased from zero to the levels observed during the experiment. The FA power was increased linearly from zero to the value $W(t_0, \text{experiment})$. The heat losses were increased by increasing the heat loss coefficient C_{loss} from zero to a maximum value $C_{\text{loss}}(\text{max})$. The coefficient C_{loss} is used as a multiplier applied to the theoretical loop heat losses calculated by RELAP, and accounts for uncertainties in the calculation of these heat losses. The value $C_{\text{loss}}(\text{max})$ was selected to provide the best agreement between the calculated pressure $P_{\text{out}}(\text{calculated})$ and the corresponding measured pressure $P_{\text{out}}(\text{measured})$ during the experiment time window.

After 400 s, both the FA power and the C_{loss} coefficient were kept constant. During this third phase, the calculation describes the quasi-steady-state phase of the experiment, during which the pressure P_{out} decreases gradually. The beginning time of the experiment window $t_0(\text{exp})$ was associated with the calculation time $t_1(\text{calc})$ at which $P_{\text{out}}(t_1(\text{calc})) = P_{\text{out}}(t_0(\text{exp}))$. Similarly, the end time of the experiment window $t_1(\text{exp})$ was associated with the calculation time $t_2(\text{calc})$ at which $P_{\text{out}}(t_2(\text{calc})) = P_{\text{out}}(t_1(\text{exp}))$. Several parameters, such as the liquid level, initial pressure $P_{\text{out}}(t_0(\text{calc}))$, and the quality of the vapor were varied in order to obtain a calculated FA liquid level which matches the corresponding liquid level inferred based on the experimental data, at the beginning of the experiment time window.

It is noted that this approach, which relies on an arbitrary transient to simulate the actual loop transient was dictated by the lack of information about the actual initial transient. This methodology introduces substantial uncertainties concerning the general agreement between the calculated and experimental initial loop conditions. Only a limited number of initial conditions can be matched by the calculated transient in the complex experimental loop analyzed. Because the calculations indicate that the loop is still in a transient during the third phase, and because detailed information about the experimental conditions prior to the experiment time window is limited, it is not clear that the simulated loop conditions are the same as the experimental conditions. While the comparison of the calculated results with the experimental data is

instructive, no firm conclusions can be drawn about the adequacy of RELAP models based on such comparisons.

4.4 Description of Sensitivity Cases

4.4.1 Sensitivity Cases Examining Initial Thermal-Hydraulic Conditions

A large number of parametric cases were run, with the goal of examining the influence of initial thermal hydraulic conditions on the fuel assembly temperatures during the experiment window. Parameters studied included the core water level, the annular zone water level, and the steam quality in the upper regions of the experimental loop. The results of selected cases are presented in Sections 5.2.1-5.2.3. They show that the FA temperatures during the experiment window are significantly affected by these parameters. By adjusting the values of these parameters, and other input parameters described in the next section, 4.4.2, reasonable agreement between the calculated and measured FA temperatures can be obtained. However, other combinations of input conditions could lead to similar (and possibly better) agreement between calculations and experimental data. The sensitivity of results to these unknown input parameters indicates that no firm conclusions concerning the adequacy of RELAP models can be drawn from this analysis.

4.4.2 Sensitivity to Loop Nodalization

The sensitivity of the computed results to the loop nodalization was also examined. Special attention was given to the nodalization of the FA top section which connects the FA and the upper plenum. The results of these cases, which indicate a significant sensitivity of results to the nodalization and initial conditions of this loop section, are presented in Section 5.2.4. The sensitivity of the FA temperatures to the FA exit section nodalization highlights the fact that the transient behavior of the FA temperatures during the experiment window is influenced by a combination of initial conditions and nodalization of complex loop components. Because of the experimental loop complexity, and the limited information about the initial conditions, an exhaustive study of the loop nodalization effects is impractical. This further reinforces the conclusion that the analysis of this experiment is not suitable for the evaluation of the adequacy of RELAP models.

5. Results

This section describes the results of analyses of test KS1-18-2, starting with the base case results which are presented in Section 5.1 and continuing with a number of sensitivity analyses, the results of which are presented in Section 5.2.

Substantial uncertainties about the experimental initial conditions were identified in the analysis of Test KS1-18-2. Because similar uncertainties clearly exist in the other tests, we decided to limit our analysis to the Test KS1-18-2.

5.1 Base Case Results

5.1.1 KS1-18-2 Test Data Description

During the experiment time window, $t_{exp} = 0\text{--}250$ s the power was kept constant at $W(t_{exp})=14.5$ kW, and natural circulation was established in the closed loop circuit. A slow pressure decrease was measured, with the rate $dP_{out} / dt = -0.028$ bar/s, which is attributed to the fact that the total loop heat losses $Q_{loss}(t_{exp})$ were greater than the FA power $W(t_{exp})$, leading to a dominance of steam condensation over steam generation. The initial value of the the pressure P_{out} was $P_{out}(t_{0exp}) = 60.2$ bar, and the final value was $P_{out}(t_{exp}=250s) = 53.3$ bar. The measured P_{out} values are shown in Fig. 5-3.

The initial value of the mixture level in the FA, based on the rod wall temperature axial distribution, was $L_m(T_{0exp}) = 1.78$ m. During the experiment the mixture level increased gradually, leading to an increased wall-to-coolant heat transfer at higher FA elevations, and causing the local rod wall temperatures to decrease close to the coolant saturation temperature. This is illustrated by the measured rod wall temperatures in the upper part of the FA, shown in Fig. 5-11 - 5-13. The temperatures recorded at elevation $L=2.485$ m (Fig. 5-11) indicate that the mixture level reached the top of the FA channel during the experiment time window.

Because the experimental data was limited to the 250 s experiment time window, it is not possible to clearly determine how far the loop was from reaching a steady-state condition. However, the FA liquid level increase illustrated in Figs. 5-11 – 5-13 seems to indicate that the loop was still in a transient oscillatory state. The liquid level increase in the FA leads to an increase in the amount of heat transferred to the coolant and therefore to an increase in the amount of vapor formed. As the vaporization rate overtakes the condensation rate, the FA liquid level would begin to decrease, until the process reverses again.

When modeling a complex hydraulic system in a transient state it is necessary, in order to be able to evaluate the adequacy of the models, to follow the entire transient sequence. Replacing the initiating transient with an arbitrary transient introduces substantial uncertainties about the equivalence of experimental and calculated conditions at the beginning of the experiment time window. The fact that a limited set of measured parameters are matched by the calculated results at the beginning of the experiment window does not guarantee that all other relevant conditions are matched and that the modeled system is following the same transient as the experiment.

5.1.2 KS1-18-2 Test Modeling of Initial and Boundary Conditions.

The initial conditions of the RELAP simulation at the beginning of the simulation and the boundary conditions were selected with the goal of matching key experimental values at the beginning of the experiment time window $t=t_0(exp)=t_1(calc)$ and other key experimental data

Fig. 5-1. Fuel Assembly Model Power, Test KS1-18-2.

Fig. 5-2. Loop Heat Loss Correction Coefficient, Test KS1-18-2.

observed during the experiment. In particular, we were interested in matching the following experimental parameters:

- the FA heat release was constant and equal to $W=14.5$ kW during the experiment time window;
- the core outlet pressure was equal to $P_{out}(t_{0exp}) = 60.2$ bar, and then decreased during the experiment to $P_{out}(t_{1exp}) = 53.3$ bar, with the rate $dP_{out}/dt = -0.028$ bar/s;
- initial coolant temperature at the core inlet was $T_{Fin}(t_{0exp})=479$ K;
- initial FA liquid level location was inferred based on the FA rod wall temperature profile to be $L_m(t_{0exp}) = 1.78$ m, and then the level increased during the experiment with the rate $dL_m/dt \sim 4.4$ mm/s.

Due to the fact that an arbitrary power and heat loss computational transient was used to arrive to the desired conditions at the beginning of the experiment time window, the initial computational conditions are not well defined, and multiple calculations were necessary to reach a quasi-optimal set of initial computational conditions. This set of initial conditions, presented below, was selected to define the base case. However, as an exhaustive exploration of all possible initial computational conditions is not practically possible, other combinations of initial computational conditions might exist which provide a better match with the experimental conditions at the beginning of the experiment window and throughout the experiment. The following initial computational conditions were used for the base case:

- FA power $W(t_{0calc}) = 0$ and the heat loss coefficient $C_{loss}(t_{0calc}) = 0$;
- the initial pressure was $P_{out}(t_{0calc}) = 66.7$ bar. This pressure, which is higher than the pressure $P_{out}(t_{0exp}) = 60.2$ bar, was selected to allow the pressure, which decreases during the initial computational transient, to match the observed pressure P_{out} at the beginning of the experiment time window.
- the lower plenum and lower pipeline were assumed filled with liquid with temperature $T_{Fin}(t_{0calc}) = T_{Fin}(t_{0exp}) = 479$ K;
- the liquid level in the core $H_{core}(liquid) = 1.25$ m, core annulus $H_{annulus}(liquid) = 0.12625$ m, and downcomer $H_{downcomer}(liquid) = 0.019$ m were selected to provide optimal agreement with the experimental data mentioned above;
- the remaining parts of the loop were assumed filled with saturated wet vapor, with the pressure $P_{out}(t_{0calc})$ and quality $X(t_{0calc})$ selected to provide optimal agreement with the experimental data mentioned above;
- the temperatures of the loop components filled with liquid were assumed equal to the liquid temperature, 479 K.

- the temperatures of the loop components filled with saturated steam were assumed equal to the saturation temperature, 556 K, corresponding to the initial loop pressure $P_{out}(t_{0calc})$.

The RELAP simulation was initiated by an initial calculation with the core power $W=0$ and the heat loss coefficient $C_{loss}=0$ for the $t = 0 - 100$ s. This calculation allows the equilibration of initial loop liquid levels and temperatures. Between 100 - 500 s the FA power and the loop heat losses were increased to reach the levels observed during the experiment. During this time interval the FA power was increased linearly from zero to $W = 14.5$ kW and the loop heat losses were also increased by linearly increasing the heat loss coefficient C_{loss} from zero to $C_{loss} = 2.8$. After $t = 500$ s both the FA power W and the heat loss coefficient C_{loss} were kept constant. The maximum value of the heat loss coefficient $C_{loss} = 2.8$ was selected because it provides good agreement between the calculated and experimental pressure P_{out} during the experiment time window. The use of this coefficient, which reflects uncertainties in the heat loss calculations, introduces an additional degree of freedom in the analysis and increases the uncertainty in the boundary conditions adequacy. The magnitude of these uncertainties is underscored by the fact that, in order to achieve agreement between the calculated and measured values of the pressures P_{out} , the loop heat losses need to be approximately 3 times higher than expected based on the loop geometry and heat transfer coefficients. The values of the FA power W and the heat loss coefficient C_{loss} are shown, as a function of time, in Figures 5-1 and 5-2.

As the heat losses are larger than the FA energy deposition, the calculated core outlet pressure P_{out} decreases gradually after $t = 500$ s. The computation time t_{1calc} that corresponds to the beginning of the experiment window t_{0exp} was selected such that $P_{out}(t_{1calc}) = P_{out}(t_{0exp}) = 60.2$ bar. This led to the selection of $t_{1calc} = 507$ s. It is observed that at this time the FA power W and the heat loss coefficient C_{loss} have been kept constant for only 7 seconds, which is too short a time for the loop to reach an equilibrium, or quasi-equilibrium state. Based on the computational results, we conclude that the loop was in a transient condition during the experiment time window. This increases substantially the difficulty of establishing the equivalence of initial states of the computational and experimental systems, when the computational transient used to reach the time t_{1calc} is different from the actual sequence used in the experiment to reach the state at t_{0exp} . To establish the equivalence of the computational and experimental systems in the presence of a transient requires not only the matching of the basic thermo-hydrodynamic variables but also the matching of many time derivatives of these variables.

5.1.3 Base Case Computational Results and Comparison to Test Data.

This section discusses first the calculated initial conditions at the beginning of the experiment time window and then the calculated transient results during the experiment.

5.1.3.1 Calculated Initial Conditions.

The computational time that corresponds to the beginning of the experimental time window $t_{1calc} = t_{0exp}$ is determined by the requirement that $P_{out}(t_{1calc}) = P_{out}(t_{0exp})$. This equality is satisfied at $t_{1calc} = 507$ s. The calculated values of $P_{out}(t_{calc})$ are shown in Figure 5-3, which

Fig. 5-3. Pressure at FA Model Outlet Pout, Test KS1-18-2.

Fig. 5-4. Measured rod wall temperatures at time t_{0exp} , Test KS1-18-2.

Fig. 5-5. Calculated rod wall temperatures at time t_{0exp} , Test KS1-18-2

Fig. 5-6. Coolant temperature at core model inlet T_{Fin} , Test KS1-18-2.

Fig. 5-7. Calculated Inner Wall Temperatures, Test KS1-18-2.

Fig. 5-8. Calculated Inner Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-9. Calculated Inner Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-10. Calculated Inner Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-11. Calculated and Measured Rod Wall Temperatures , Test KS1-18-2.

Fig. 5-12. Calculated and measured rod wall temperatures, Test KS1-18-2.

Fig. 5-13. Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-14. Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-15. Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-16. Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-17. Calculated and Measured Rod Wall Temperatures, Test KS1-18-2.

Fig. 5-18. Collapsed Liquid Level in the FA Model, Test KS1-18-2.

also indicates the beginning and end of the experimental time window. Figure 5-3 compares the calculated and measured values of P_{out} during the experimental window. The slope of the P_{out} curve is directly influenced by the magnitude of the loop heat losses, and the value of the heat loss coefficient C_{loss} was adjusted to ensure good agreement between the calculated and measured P_{out} values. The value of the heat loss coefficient $C_{loss} = 2.8$ was found to be adequate and was used in this analysis.

The liquid/vapor mixture level in the FA channel was determined from the analysis of experimental inner wall temperature data TW at various axial locations. The temperature data shown in Figure 5-4 indicates that at time t_{0exp} the mixture level was $L_{mexp}(t_{0exp}) \approx 1.78$ m. At t_{0exp} the wall temperature measured at level 1.78 m (TW-03-08) is still approximately 550 K, while the next higher wall temperature, measured at level 1.89 m (TW-04-06) is substantially higher, approximately 630 K, indicating a reduced heat transfer coefficient due to the presence of a larger void fraction. A similar analysis of the calculated temperatures, shown in Figure 5-5, indicates that at $t_{0exp} \approx t_{1calc} = 507$ s the computed liquid/vapor mixture level in the FA channel was ≈ 2.06 m.

A comparison of the measured coolant temperature at the core inlet, T_{Fin} , with the corresponding calculated values is shown in Figure 5-6. The calculated T_{Fin} values are shown to be in good agreement with the measured values.

5.1.3.2 Calculated results during the experiment time window.

To assess the adequacy of the simulation, the calculated rod wall temperatures $TW(t_{calc})$ were compared with the corresponding data recorded during the experiment. The calculated rod wall temperatures in the upper, middle, and bottom parts of the heated FA model are shown in Figs. 5-7 – 5-10, respectively. These figures also show the location of the experiment time window. The calculated rod wall temperatures in the upper part of the FA model are compared with the corresponding measured temperatures in Figs. 5-11 – 5-17. Fig. 5-18 shows the time evolution of the collapsed liquid level in the FA model. This level shows the core height which would be filled with liquid if all the coolant in the core (vapor and liquid) were collapsed to liquid. It provides a measure of the coolant mass in the FA model, but is only an approximate measure of the mixture level. The mixture level is determined by both the coolant mass present in the core and the void fraction at each axial location.

An examination of Figs. 5-11 – 5-17 indicates that the calculated wall temperatures are in reasonable agreement with the experimental data, although timing discrepancies are clearly present. At time $t_0(exp) = t_1(calc)$ the calculated mixture level in the FA model is approximately 2.06 m, higher than the 1.78 m inferred from the experimental data. The calculated and measured wall temperatures below the 1.78 m level are in good agreement, as shown in Figs. 5-16 and 5-17. In this region the wall temperature has decreased close to the coolant saturation temperature due to the high heat transfer between the rod wall and the coolant mixture. At levels between 1.78 m - 2.06 m, as shown in Figs. 5-14 and 5-15, the calculated rod wall temperatures have already decreased close to coolant saturation temperature, while the measured temperatures are shown to decrease to the same level during the experiment time window. This is due to the fact that the initial calculated level of the coolant mixture is higher than the level observed in the experiment at the same time. Fig. 5-13 shows both the calculated and measured wall temperatures decreasing from the same higher temperature, approximately 625 K, to a

temperature close to the coolant saturation temperature. The calculated wall temperature decrease occurs about 100 s earlier than the experimental temperature decrease, indicating an earlier arrival of the liquid mixture at that level. Figs. 5-11 and 5-12 show fairly good agreement between the calculated and measured temperatures, both in terms of magnitude and timing. This indicates that the calculated liquid mixture level is rising slower than the experimental level and by this time the calculated level, which was initially higher, is about the same as the experimental level.

The general features of the transient events analyzed can be better understood by studying the transient wall temperatures in the core during the entire calculation, i.e. including the period that precedes the experiment time window. The calculated wall temperatures in the lower half of the FA model (Figs. 5-9 and 5-10) remain close to the liquid saturation temperature during the entire calculation, indicating a high heat transfer coefficient between the wall and the coolant, and thus the presence of a high liquid volume fraction. In the upper half of the FA model, predominantly filled with vapor, the wall temperatures begin to rise above the coolant saturation temperature starting at approximately $t(\text{calc}) = 200$ s (Figs. 5-7 and 5-8). This temperature increase is due to the reduced heat transfer between the fuel rod and the coolant vapor. As the mixture level in the coolant channel increases, causing the local heat transfer between the rods and the coolant to increase, the rod wall temperatures at successively higher locations decrease rapidly to the coolant saturation temperature. As shown in Fig. 5-7, the mixture level continues to increase, at decreasing rates, after $t(\text{calc}) = 500$ s, at which time the power and heat losses reach their maximum values. Although the power and heat losses are held constant after $t(\text{calc}) = 500$ s and throughout the experimental time window $t(\text{calc}) = 507$ s – 757 s, the mixture level in the FA model is still in a transient mode, rather than in a quasi steady state, and is strongly influenced by the transient conditions prior to $t(\text{calc}) = 500$ s. This is due to the small time interval between the end of the power and heat loss transient and the beginning of the experimental time window. This time interval, which is only 7 s, is not sufficient to allow the system to reach a quasi steady state.

5.2. Sensitivity Case Results

A number of initial conditions which are not known from measurements, such as the vapor quality in the voided loop regions, the initial liquid level in the FA model and the liquid level in the annular region, etc. can be changed in order to obtain better agreement between the computed and measured rod wall temperatures. These initial conditions determine the amount of coolant in the loop and the distribution of this mass at the beginning of computations. A significant number of calculations were carried out in order to evaluate the impact of these parameters on the computed results during the experiment time window. The results of some of these calculations are described in this section.

5.2.1 Effect of vapor quality in the voided loop regions.

One of the parameters influencing the transient behavior of FA model temperatures during the experimental time window is the quality of the vapor in the voided loop regions. Initial calculations, which assumed the presence of saturated dry vapor ($x = 1.0$) in the voided loop regions have consistently led to fuel rod temperatures higher than those observed in the experiment. The presence of wet saturated vapor in the upper parts of the loop allows the uncovered part of the fuel rods to remain at lower temperatures during the early part of the

transient, leading to transient temperatures comparable with those observed during the experiment. The vapor quality value used for the base case presented above was $x = 0.7$. The results of two parametric calculations using the quality values $x = 0.72$ and $x = 0.68$ are presented in Figs. 5-19 and 5-20 respectively. These results, which show the calculated transient behavior of the rod wall temperatures at various elevations are to be compared with the corresponding base case results shown in Fig. 5-7. Relatively small changes in the vapor quality are shown to have a significant effect on the transient temperature behavior. While the general temperature behavior and the maximum temperatures at various elevations remain similar, the timing of the quenching changes significantly when the initial vapor quality changes. In the case using the initial vapor quality $x = 0.72$, illustrated in Fig. 5-19, the coolant mixture level at the beginning of the experimental time window ($t(\text{calc}) = 507 \text{ s}$) is approximately 1.93 m, lower than the base case corresponding level 2.06 m, and closer to the experimental value of 1.78 m. This is consistent with the presence of smaller amounts of liquid in the voided loop region and in the loop in general, leading to lower mixture level when compared with the base case. The time intervals between the occurrence of quenching at various levels are larger than those in the base case, indicating a slower rise of the mixture level. In both cases these intervals are seen to increase as the elevation increases, indicating a decelerated rise of the mixture level, but this deceleration is considerably larger in the parametric case 1 (Fig. 5-19) than in the base case. In fact, quenching at elevations 19 ($H=2.3125 \text{ m}$) and 20 ($H= 2.4375 \text{ m}$) which in the base case were in good agreement with the experimentally observed quenching, do not occur within the experimental time window in Fig. 5-19. Opposite trends are clearly observed in Fig. 5-20, which shows the results of a calculation using the initial vapor quality $x = 0.68$, instead of the $x = 0.7$ value used in the base case. In this case quenching at all locations occurs earlier than in the base case, and the mixture level at the beginning of the experimental time window is approximately $H=2.1875$, higher than the $H= 2.06 \text{ m}$ in the base case and consistent with the presence of larger amounts of liquid in the loop. The mixture level is rising faster than in the base case, as indicated by the earlier quenching times and the smaller time intervals between the quenching occurrence at successive elevations.

5.2.2 Effect of initial liquid level in the heated core region.

Another parameter influencing the transient behavior of FA model temperatures during the experimental time window is the initial liquid level in the FA model. Increasing or decreasing this level at the beginning of the calculations changes the amount of liquid in the loop and leads to a higher or lower mixture level, respectively, at the beginning of the experimental time window. The results of a sensitivity case performed with a lower initial liquid level in the FA model, $H_{\text{core}}(\text{liquid}) = 1.0 \text{ m}$ instead of the value used in the base case, $H_{\text{core}}(\text{liquid}) = 1.25 \text{ m}$, is shown in Fig. 5-21. These results are compared with the corresponding transient rod wall temperatures obtained in the base case, illustrated in Fig. 5-7. The mixture level at the beginning of the experiment time window is lower than 2.0625 m, the elevation at node 17 which is just beginning to quench. This level is lower than the base level, where the quenching at node 17 occurs before the beginning of the experiment time window. The mixture level increases slower than calculated in the base case, as evidenced by the larger time intervals between the occurrence of quenching at successive elevations. As a result, the quenching at node 20, level 2.375 m, which in the base case was in good agreement with the experimental data, is now delayed and

Fig. 5-19. Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 1 ($x = 0.72$).

Fig. 5-20. Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 2 ($x = 0.68$).

does not occur during the experiment time window. In fact, quenching at node 20 has not yet occurred at $t(\text{calc}) = 800$ s, when the calculation ended. As expected, the effect of decreasing the initial liquid level in the heated core region is similar to that of the increased initial vapor quality in the voided loop regions. This is evidenced by a comparison of Figs. 5.21 and 5.19. In both cases the mixture level at the beginning of the experiment window is lower than in the base case, and the mixture level increases at a lower rate than in the base case during the experiment window time interval.

5.2.3 Effect of initial liquid level in the annular region.

The transient behavior of FA model temperatures during the experimental time window is also directly influenced by the initial liquid level in the annular region surrounding the heated core region. The results appear to be particularly sensitive to changes in this level, which could be explained by the large cross sectional area of the annular region. A small increase in the initial liquid level in the annular region to 0.13125 m, instead of 0.12625 m used in the base case, leads to significant changes in the calculated rod wall temperatures, as illustrated in Fig. 5-22. A comparison of these results with the base case results shown in Fig. 5-7 indicates that the mixture level at the beginning of the experiment time window is lower than in the base case, and thus closer to the observed experiment data. However, the mixture level is rising slower than calculated in the base case, as evidenced by the longer time intervals between successive quenching events, and quenching in the upper nodes 19 and 20 does not occur during the experiment time window. These changes are not consistent with previously observed changes, as an increased level, and therefore an increased amount of coolant in the loop, was expected to lead to a faster rise of the coolant mixture. A larger increase in the annular region initial liquid level to 0.25 m leads, as expected, to a more rapid rise of the mixture level in the heated core region, and transient rod wall temperatures illustrated in Fig. 5-23. In this case, the mixture level at the beginning of the experiment time window is approximately 2.1875 m, higher than the level calculated in the base case. The coolant mixture level is rising faster than in the base case, and quenching at node 20 occurs before $t(\text{calc}) = 600$ s, approximately 140 s before the corresponding time calculated in the base case and illustrated in Fig. 5-7.

5.2.4 Effect of core exit nodalization and related liquid level.

Several calculations have focused on the effect of the core exit nodalization and the associated liquid level. These effects are discussed here in order to highlight the sensitivity of computed results to seemingly minor modeling assumptions. The experimental loop has a rather complex geometry and other similar sensitivities are likely to be present. It was found that the core exit nodalization and the initial liquid level in the annular outlet plenum can affect significantly the rod wall calculated temperatures. An earlier core exit nodalization (A), illustrated in Fig. 5-24 allows the communication between the annular outlet plenum and the upper shroud region (Junction 401) at a level higher than the communication between the annular outlet plenum and the core outlet nozzle. This nodalization led to maximum rod wall temperatures considerably higher than the experimentally measured values and was abandoned. The nodalization used in the base case, illustrated in Fig. 5-25, has the communication between the core outlet nozzle, the annular outlet plenum, and the upper shroud (Junction 401) region at the same level. This later nodalization facilitates the flow of condensed liquid from the upper loop regions into the core

Fig. 5-21. Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 3.
(Hcore(liquid) = 1.25 m)

Fig. 5-22. Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 4.
(Hannulus(liquid) = 0.13125 m)

and results in lower maximum rod wall temperatures. Even more important, the initial liquid level in the annular outlet plenum has a similar impact on the rod wall temperatures. Assuming that the lower two nodes of the annular outlet plenum are initially filled with liquid, as was done in the base case, leads to considerably lower maximum rod wall temperatures (by about 55 K) than those achieved when the annular outlet plenum is assumed to be initially voided. While the presence of liquid trapped in the lower nodes of the annular outlet plenum during the experiment is possible, the fact that the rod wall temperatures are quite sensitive to this unknown level points to the uncertainties involved in the analysis of this experiment. An exhaustive analysis of the effects of various liquid levels in the annular outlet plenum and the core exit nodalization was not possible within the time frame of this analysis.

6. Conclusions

We conclude that, while a qualitative simulation of the experimental conditions was achieved by varying various computational initial conditions, the available experimental data is not sufficient to draw conclusions about the adequacy of the RELAP simulation. Additional quantitative information about the nature of the experimental transient that precedes the experimental data time window is necessary in order to allow a realistic simulation of the experiment, which would allow an evaluation of the RELAP models adequacy. While the use of an artificial transient to reach a system steady state might be acceptable, the same is not the case when trying to model a system which is still in a transient state.

Reasonable agreement between RELAP5 and the experiment data can be obtained by manipulating a number of initial computational values, including the liquid level in the fuel assembly model, the liquid level in the annular region, the quality of the saturated vapor in the voided loop regions, etc. Our study has focused on exploring the sensitivity of results to changes in these initial values, which are not based on experimental information but are selected with the

Fig. 5-23. Calculated Inner Rod Wall Temperatures, Test KS1-18-2 Parametric Case 5.
(Hannulus(liquid) = 0.25 m)

Fig. 5- 24. Core Exit Nodalization – A.

Fig. 5-25. Core Exit Nodalization - B.

goal of matching the experimentally observed behavior during the experiment time window. We have shown that changes in several initial computational values can lead to similar changes in the calculated loop behavior during the experiment time window. Other parameters exist which can directly influence the calculated results, which have been only minimally explored, or have not been explored at all due to lack of time. Because we are not modeling the entire sequence of events which led to the initial experiment conditions, it is not possible to assume that by matching a limited set of measured parameters at the beginning of the experiment time window we have reproduced all the initial actual conditions.

In view of the substantial uncertainties about the experimental initial conditions identified in the analysis of Test KS1-18-2, and because similar uncertainties clearly exist in the other tests, we decided to limit our analysis to the Test KS1-18-2. We conclude that the analysis of these experiments, while providing a useful demonstration of the RELAP5 capabilities to describe the experimental sequence of events, cannot be used to draw quantitative conclusions about the adequacy of specific RELAP5 models.

REFERENCES

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2. "Computer Code Validation for Transient Analysis of VVER and RBMK Reactors: *Validation Prioritization on VVER*", International Nuclear Safety Center of MINATOM of Russia, deliverable 5 of Phase 1 of Joint project 6, Moscow, Russia (1998).
3. "Computer Code Validation for Transient Analysis of VVER and RBMK Reactors: *A Final RELAP5 Validation Plan for Application to VVER*", International Nuclear Safety Center of MINATOM of Russia, deliverable 3 of Phase 2 of Joint project 6, Moscow, Russia (1998).
4. "Computer Code Validation for Transient Analysis of VVER and RBMK reactors: *Standard Problem INSCSP-V4 Definition Report*", International Nuclear Safety Center of MINATOM of Russia, Task 2, Deliverable V4-1 of Phase 3 of Joint project 6, Moscow, Russia (2000).

Appendix A

RELAP Model Nodalization Summary

This appendix incorporates a nodalization summary of the baseline RELAP5 model (Table A-1).

Table A-1
Baseline RELAP5 Model Nodalization Summary

SYSTEM COMPONENT	RELAP Comp. No.	Description	Comp. Name	Comp. Type	No. of Vols	Deq or ID (m)	Flow Area (m ²)	Length (m)	No. Juncts	From Component	To Component
Downcomer	100	vertical pipe	upper-dc	pipe	9	0.073	0.0041854	1.9876			
	101		dc-intb	branch	1	0.073	0.0041854	0.3500	2	100-09 101-1	101-1 150-01 (*CJ)
	150	vertical pipe	lower-dc	pipe	13	0.080	0.0050265	8.1340			
	151		dc-lpipe	branch	1	0.065	0.0033183	0.3500	2	150-13 (*CJ) 151-1	151-1 900-01
Lower Pipeline	900	horizontal pipe	low-pipa	pipe	11	0.065	0.0033183	7.8062			
	901		dc-olj	sngljun					1	900-11	940-01
	940	slightly declined	low-pipb	pipe	10	0.020	0.0003142	7.0000			
	941		lpb-lpc	sngljun					1	940-10	960-01
	960		low-pipe	pipe	15	0.065	0.0033183	9.8808			
	961		lp-lpl-j	sngljun					1	960-15	200-01
Lower Plenum	200		lowpl-in	pipe	4	0.065	0.0033183	3.0400			
Core Inlet	220	core inlet nozzle	core-inl	branch	1	0.100	0.0078540	0.3000	2	200-04 220-1	220-1 250-02 (*CJ)
	250	bottom annular chamber	annul-in	annulus	3	0.170	0.0574100	0.2560			
	251		lowan-jn	sngljun					1	250-03 (*CJ)	280-02 (*CJ)
	280	lower core (vert)	l-shroud	annulus	5	0.013	0.0022800	0.3140			
Fuel Assembly	281		fa-injun	sngljun					1	280-05	300-01
	300	fuel assembly	core	pipe	20	0.0098	0.0018060	2.5050			
	399		fa-outjn	sngljun					1	300-20	400-01
Core Annulus	350	Shroud annulus	core-gap	annulus	21	0.1020	0.0224310	2.5250			
	351		stag-jct	sngljun					1	250-01	350-01
Core Outlet	400	upper core (vert)	u-shroud	annulus	7	0.00974/ 0.01661/ 0.1575	0.001806/ 0.003209/ 0.05395	0.2950			
	401		cfloutjn	sngljun					1	400-04	450-01 (*CJ)
	450	upper annular chamber	annul-ot	annulus	3	0.220	0.0656600	0.1500			
	480	core outlet nozzle	core-out	branch	1	0.100	0.0078540	0.3000	2	450-01 (*CJ) 480-1	480-1 490-01
Upper Plenum	490	vertical pipe	upper-pl	pipe	12	0.1/ 0.102	0.0078540/ 0.0081713	8.5100			
	491		upln-hlj	sngljun					1	490-12 (*CJ)	500-01
Loop Hot Leg	500	~horiz. pipe	hot-leg	pipe	11	0.065	0.0033183	7.6854			
	501		hl-elbow	branch	1	0.065	0.0033183	0.7854	2	500-11 501-1	501-1 600-01
SG Tube Bundle 1	600	~horiz. pipe	sg-bun1	pipe	2	0.065	0.0033183	0.9675			
	601	tee	sg-tee	branch	1	0.065	0.0033183	0.0650	3	600-02 601-1 601-1 (*CJ)	601-1 700-01 650-01
Stm Release Pipe	650	~horiz. pipe	stm-rels	pipe	8	0.065	0.0033183	16.0000			
SG Tube Bundle 2	700	~horiz. pipe	sg-bun2	pipe	2	0.065	0.0033183	0.9675			
Loop Cold Leg	701		cl-elbow	branch	1	0.065	0.0033183	0.7854	2	700-02 701-1	701-1 800-01
	800	~horiz. pipe	upper-cl	pipe	10	0.065	0.0033183	6.4500			
	801		low-clj	sngljun					1	800-10	850-01
	850	vertical pipe	lower-cl	pipe	9	0.057/ 0.067	0.00721/ 0.00488	6.9790			
	851		cl-outjn	sngljun					1	850-09	100-01

*CJ indicates crossflow junction

Appendix B
Base Case RELAP Input File

```

=
*           INSP Standard Problem V4
*           Behavior of Heated Rod Temperatures
*           in the Partially Uncovered VVER Core Model
*
*=====
* The following data comprises a RELAP5 input model of the
* KS-1 Facility at RRC Kurchatov Institute, Moscow, Russia.
*
*-----
*=====
* This deck is initialized for Test KS1-18-2.  Closs=2.15          *|
*      Nearly Implicit numerical scheme imposed.                  *|
*      Mixture level and thermal front tracking imposed.           *|
*      Cntrlvar for Condensation Rates added.                      *|
*                                                                    *|
*      Renodalization of Core from 10 to 20 volumes                *|
*      Time step sensitivity (dt=0.005:steady state)               *|
*                           (dt=0.01: transient)                   *|
*      HTC ramp turned off - first 205sec                          *|
*      Steady State Initial Temps calculated by RELAP.            *|
*      Changed surface roughness to 4.57e-5m for all               *|
*      piping except for core simulator.                            *|
*      Pressure distribution specified around loop                 *|
*                                                                    *|
*      Bestion interphase friction correlation invoked              *|
*      ( v4-18-2.i)                                                 *|
*                                                                    *|
*      RENODALIZATION OF CORE EXIT 01/29/2001                     *|
*                                                                    *|
*=====
*-----
*
*
* This represnts VVER standard problem #4 of joint project #6.
*$=====
*
*
*=====
*
* This model was developed by Argonne National Laboratory,
*
*      AUTHOR:  John W. Ahrens
*
*=====
*
*$=====
*$
*$      This deck should be run with RELAP5/MOD3 version 3.2      $
*$                                                                    $
*$=====
*
*
*
*=====
* General Input Data Cards Begin Here:
*=====
*

```

```

* Developmental Model Control Card
*01      19      * Bestion correlation for interphase friction
*
*problem      type      option
100          new      transnt
*
101          run
*101          inp-chk
*
102          si      si
*          noncondensible gas type
110          nitrogen
*
*      Ref.Vol.      elev      fluid      name
120      300010000      0.0625      h2o      primary      * Ref. Elev. is 0.0625 m below
Vol.1 center
*
*          t end      mindt      maxdt      cntrl      min      maj      res
201          5.0      1.e-7      0.005      00015      200      40000      40000      *
*202          50.0      1.e-7      0.02      00015      50      500      500      *
*203          205.0      1.e-7      0.01      00015      100      500      500      *
*204          215.0      1.e-7      0.001      00015      1000      5000      5000      *
*205          225.0      1.e-7      0.005      00015      200      2000      2000      *
*206          250.0      1.e-7      0.01      00015      100      2500      2500      *
*202          1000.0      1.e-7      0.01      00015      100      10000      10000      *
*202          1000.0      1.e-7      0.1      00015      20      5000      10000      *
202          800.0      1.e-7      0.1      00015      20      5000      10000      *
*
*201          100.0      1.e-3      0.02      00003      50      500      5000      *TTTTT
*
20800001 dt      0
20800002 dtcrnt 0
20800003 systms 1
20800004 gammai 300010000
20800005 gammai 300020000
20800006 gammai 300030000
20800007 gammai 300040000
20800008 gammai 300050000
20800009 gammai 300060000
20800010 gammai 300070000
20800011 gammai 300080000
20800012 gammai 300090000
20800013 gammai 300100000
20800014 gammaw 300010000
20800015 gammaw 300020000
20800016 gammaw 300030000
20800017 gammaw 300040000
20800018 gammaw 300050000
20800019 gammaw 300060000
20800020 gammaw 300070000
20800021 gammaw 300080000
20800022 gammaw 300090000
20800023 gammaw 300100000
20800024 gammac 300010000
20800025 gammac 300020000
20800026 gammac 300030000
20800027 gammac 300040000
20800028 gammac 300050000

```



```

*          area          vol no
1000101    4.185e-3        9
*
*          vol lgh       vol no
1000301      0.267         5    *Sensor P2
1000302      0.238         6
1000303      0.138209      7
1000304      0.138209      8
1000305      0.138209      9
*
*          vr ang        vol no
1000601     -90.0         6
1000602     -75.0         7
1000603     -45.0         8
1000604     -15.0         9
*
*          elv ch        vol no
1000701     -0.267         5
1000702     -0.238         6
1000703     -0.1335        7
1000704     -0.097729      8
1000705     -0.035771      9
*
*          rough    hy dia    vol no
1000801     4.57e-5    0.073    9
*
*          floss    rloss    jn.no.
1000901      0.0      0.0      5
1000902      0.078    0.078    8
*
*          tlpvbf     vol no
1001001     110000      9
*
*          fvcchs     jn no
1001101     0001000     8
*
*          ctl    pressure    qual          vol no
1001201    102    6.67e6      0.7    0.0    0.0    0.0    9
*
*          ctl
1001300    1
*          flow-f    flow-g    velj    jun no
1001301      0.0      0.0      0.      8
*1001301      0.5      0.0      0.      8
*
*-----
*----- upper dc to lower dc connection -----
*          name          type
1010000     dc-intb      branch
*
*          no jun        in ctl
1010001      2          1
*
*          area    length    vol    hz ang    vr ang    elv ch
1010101     4.1854e-3    0.35    0.0      0.0      0.0      0.0
*
*          rough    hydia    pvbfe

```

```

1010102      4.57e-5      0.073      10000      *
*
*      ctl      pressure      qual
1010200      102      6.67e6      0.7
*
*      from      to      jun area      f loss r loss efvcahs vfrlim
1011101      100090002      101010001 4.1854e-3      0.0      0.0      001000      *
1012101      101010002      150010003 0.0      1.08      1.08      1001101      * abrupt
* exp/turn
*
*      flow-f      flow-g      velj
1011201      0.0      0.      0.      *
1012201      0.0      0.      0.      *
*1011201      0.5      0.      0.      *
*1012201      0.5      0.      0.      *
*
*-----
*----- lower-dc section -----
*
*      name      type
1500000      lower-dc      pipe
*
*      no.vol
1500001      13
*
*      area      vol no
1500101      5.0265e-3      13
*
*      vol lgh      vol no
1500301      0.534      1
1500302      0.158      2      * Sensor P4
1500303      0.75      7
1500304      0.50      8
1500305      0.442      9      * Sensor P14
1500306      0.75      11
1500307      0.716      12
1500308      0.534      13
*
*      vr ang      vol no
1500601      -90.0      13
*
*      elv ch      vol no
1500701      -0.534      1
1500702      -0.158      2
1500703      -0.75      7
1500704      -0.50      8
1500705      -0.442      9
1500706      -0.75      11
1500707      -0.716      12
1500708      -0.534      13
*
*      rough      hy dia      vol no
1500801      4.57e-5      0.080      13
*
*      floss      rloss      jn.no.
1500901      0.0      0.0      12
*
*      tlpvbf      vol no

```

```

1501001      1110000      13
*
*          fvcahs      jn no
1501101      0001000      12
*
*      ctl      pressure      qual      vol no
1501201      102      6.67e6      0.7      0.0      0.0      0.0      4
*      ctl      pressure      temp      vol no
1501202      103      6.67e6      479.0      0.0      0.0      0.0      13
*
*      ctl
1501300      1
*      flow-f      flow-g      velj      jun no
1501301      0.0      0.0      0.      12
*1501301      0.5      0.0      0.      12
*
*
*-----
*-----
*----- lower dc to lower pipeline connection -----
*      name      type
1510000      dc-lpipe      branch
*
*      no jun      in ctl
1510001      2      1
*
*      area      length      vol      hz ang      vr ang      elv ch
1510101      3.3183-3      0.35      0.0      0.0      0.0      0.0
*
*      rough      hydia      pvbfe
1510102      4.57e-5      0.065      10000      *
*
*      ctl      pressure      temp
1510200      103      6.67e6      479.0
*
*      from      to      jun area      f loss r loss      vcahs      vfrrlim
1511101      150130004      151010001      0.0      1.08      1.08      01102      * abrupt
*      contr./turn
1512101      151010002      900010001      3.3183e-3      0.0      0.0      01000      *
*
*      flow-f      flow-g      velj
1511201      0.0      0.      0.      *
1512201      0.0      0.      0.      *
*1511201      0.5      0.      0.      *
*1512201      0.5      0.      0.      *
*
*-----
*
*----- LOWER PIPELINE MODEL -----
*-----
*----- lower-pipeline section 'A'-----
*
*      name      type
9000000      low-pipa      pipe
*
*      no.vol

```

```

9000001      11
*
*      area      vol no
9000101      3.3183e-3      11
*
*      vol lgh      vol no
9000301      0.85      1
9000302      0.6354      2
9000303      0.80      4
9000304      0.4954      5
9000305      0.71      8
9000306      0.4954      9
9000307      0.80      11
*
*      vr ang      vol no
9000601      0.0      2
9000602      -90.0      4
9000603      0.0      9
9000604      90.0      11
*
*      elv ch      vol no
9000701      0.00      2
9000702      -0.80      4
9000703      0.00      9
9000704      0.80      11
*
*      rough      hy dia      vol no
9000801      4.57e-5      0.065      11
*
*      floss      rloss      jn.no.
9000901      0.0      0.0      1
9000902      0.413      0.413      2      * 90 deg bend
9000903      0.0      0.0      3
9000904      0.413      0.413      4      * 90 deg bend
9000905      0.0      0.0      8
9000906      0.413      0.413      9      * 90 deg bend
9000907      0.0      0.0      10
*
*      pvbfe      vol no
9001001      10000      11
*
*      fvcchs      jn no
9001101      0001000      10
*
*      ctl      pressure      temp      vol no
9001201      103      6.67e6      479.0      0.0      0.0      0.0      11
*
*      ctl
9001300      1
*      flow-f      flow-g      velj      jun no
9001301      0.0      0.0      0.      10
*9001301      0.5      0.0      0.      10
*-----
*-----
*
*      name      type
9010000      lpa-lpb      sngljun

```

```

*
*          from          to      jn area    f loss  r loss fvcchs
9010101 900110002 940010001    0.0      0.413   0.413 001100 * abrupt area
* change plus 90deg turn
*
*          ctl  flow-f      flow-g  velj
9010201    1      0.0        0.0    0. *
*9010201    1      0.5        0.0    0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*          hyd dia    beta      y-int      slope
*9010110    0.035     0.00      0.725     1.00
*
*-----
*
*----- lower-pipeline section 'B'-----
*
*          name          type
9400000      low-pipb      pipe
*
*          no.vol
9400001      10
*
*          area          vol no
9400101      3.1416e-4     10
*
*          vol lgh       vol no
9400301      0.70         10
*
*          vr ang        vol no
9400601      -3.214809     10
*
*          elv ch        vol no
9400702      -0.0392557     10
*
*          rough         hy dia    vol no
9400801      4.57e-5       0.020     10
*
*          floss  rloss  jn.no.
9400901      0.0      0.0      1
9400902      1.5      1.5      2  * 90 deg bend
9400903      0.0      0.0      3
9400904      1.5      1.5      4  * 90 deg bend
9400905      0.0      0.0      5
9400906      1.5      1.5      6  * 90 deg bend
9400907      0.0      0.0      7
9400908      1.5      1.5      8  * 90 deg bend
9400909      0.0      0.0      9
*
*          pvbfe         vol no
9401001      10000        10
*
*          fvcchs         jn no
9401101      0001000      9
*
*          ctl  pressure    temp          vol no
9401201      103    6.67e6    479.0    0.0  0.0  0.0    10

```

```

*
*      ctl
9401300  1
*      flow-f      flow-g      velj      jun no
9401301      0.0      0.0      0.      9
*9401301      0.5      0.0      0.      9
*
*-----
*
*-----
*
*      name      type
9410000      lpb-lpc      sngljun
*
*      from      to      jn area      f loss      r loss      fvcchs
9410101 940100002 960010001      0.0      0.413      0.413 001100      * abrupt area
* change plus 90deg turn
*
*      ctl      flow-f      flow-g      velj
9410201      1      0.0      0.0      0.
*9410201      1      0.5      0.0      0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*      hyd dia      beta      y-int      slope
*9410110      0.035      0.00      0.725      1.00
*
*-----
*----- lower-pipeline section 'C'-----
*
*      name      type
9600000      low-pipc      pipe
*
*      no.vol
9600001      15
*
*      area      vol no
9600101      3.3183e-3      15
*
*      vol lgh      vol no
9600301      0.60      2
9600302      0.4954      3
9600303      0.71      6
9600304      0.4954      7
9600305      0.695      15
*
*      vr ang      vol no
9600601      -90.0      2
9600602      0.0      7
9600603      90.0      15
*
*      elv ch      vol no
9600701      -0.60      2
9600702      0.00      7
9600703      0.695      15
*
*      rough      hy dia      vol no
9600801      4.57e-5      0.065      15

```

```

*
*      floss  rloss  jn.no.
9600901      0.0      0.0      1
9600902      0.413    0.413    2  * 90 bend
9600903      0.0      0.0      6
9600904      0.413    0.413    7  * 90 bend
9600905      0.0      0.0     14
*
*      pvbfe      vol no
9601001     10000      15
*
*      fvcahs      jn no
9601101     0001000     14
*
*      ctl      pressure      temp      vol no
9601201     103      6.67e6      479.0 0.0  0.0  0.0      15
*
*      ctl
9601300      1
*      flow-f      flow-g      velj      jun no
9601301      0.0      0.0      0.      14
*9601301      0.5      0.0      0.      14
*
*-----
*
*      name      type
9610000      lp-lpl-j      sngljun
*
*      from      to      jn area  f loss  r loss fvcahs
9610101 960150002 200010001 3.3183e-3 0.0  0.0  001000 * no choking
*
*      ctl flow-f      flow-g velj
9610201      1      0.0      0.0  0.
*9610201      1      0.5      0.0  0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*      hyd dia      beta      y-int      slope
*9610110 0.035      0.00      0.725      1.00
*
*-----
*----- LOWER PLENUM MODEL -----
*-----
*
*-----
*      name      type
2000000      lowpl-in      pipe
*
*      no.vol
2000001      4
*
*      area      vol no
2000101 3.3183e-3      4
*
*      vol lgh      vol no
2000301 0.770      2
2000302 0.750      4
*

```

```

*          vr ang      vol no
2000601      90.0        2
2000602      0.0        4
*
*          elv ch      vol no
2000701      0.770      2
2000702      0.0        4
*
*          rough      hy dia      vol no
2000801      4.57e-5    0.065      4
*
*          floss      rloss      jn.no.
2000901      0.0      0.0      1
2000902      1.08     1.08      2
2000903      0.0      0.0      3
*
*          pvbfe      vol no
2001001      10000      4
*
*          fvcchs      jn no
2001101      001000      3
*
*          ctl      pressure      temp      vol no
2001201      103      6.67e6      479.0      0.0      0.0      0.0      4
*
*          ctl
2001300      1
*          flow-f      flow-g      velj      jun no
2001301      0.0      0.0      0.      3
*2001301      0.5      0.0      0.      3
*
*-----
*
*----- lower chamber of FA inlet -----
*          name      type
2200000      core-inl      branch
*
*          no jun      in ctl
2200001      2      1
*
*          area      length      vol      hz ang      vr ang      elv ch
2200101      7.854e-3      0.300      0.0      0.0      0.0      0.0
*
*          rough      hydia      pvbfe
2200102      4.57e-5      0.100      10000      *
*
*          ctl      pressure      temp
2200200      103      6.67e6      479.0
*
*          from      to      jun area      f loss      r loss      efvcchs
2201101      200040002      220010001      7.854e-3      0.0      0.0      01000      *
2202101      220010002      250020003      7.854e-3      1.63      9.05      1001001      *
* Note for Junction #2: abrupt area change losses per K's/momentum flux off
*
*          flow-f      flow-g      velj
2201201      0.0      0.      0.      *
2202201      0.0      0.      0.      *
*2201201      0.5      0.      0.      *

```



```

*2202201      0.5      0.      0.  *
*
*-----
*
*-----
*
*      name      type
2500000      annul-in      annulus
*
*      no.vol
2500001      3
*
*      area      vol no
2500101      5.741e-2      2
2500102      3.387e-2      3
*
*      vol lgh      vol no
2500301      0.081      1
2500302      0.100      2
2500303      0.075      3
*
*      vr ang      vol no
2500601      -90.0      3
*
*      elv ch      vol no
2500701      -0.081      1
2500702      -0.100      2
2500703      -0.075      3
*
*      rough      hy dia      vol no
2500801      4.57e-5      0.17      2
2500802      4.57e-5      0.115      3
*
*      floss      rloss      jn.no.
2500901      0.0      0.0      1
2500902      0.0      0.0      2  * RELAP compute area chg losses
*
*      pvbfe      vol no
2501001      10000      3
*
*      fvcchs      jn no
2501101      001000      1
2501102      001100      2  * abrupt area chg model invoked
*
*      ctl      pressure      temp      vol no
2501201      103      6.67e6      479.0      0.0      0.0      0.0      3
*
*      ctl
2501300      1
*      flow-f      flow-g      velj      jun no
2501301      0.0      0.0      0.      2
*2501301      0.5      0.0      0.      2
*
*-----
*
*-----
*
*      name      type
2510000      lowan-jn      sngljun

```

```

*
*          from          to      jn area    f loss    r loss    fvcchs
*2510101 250030004 280020003  3.06e-2    0.99      1.62    001002 * momentum flux
* off
2510101 250030004 280020003  2.14e-3    0.0        0.0    101100 * same as 18-2R
*
*          ctl    flow-f          flow-g    velj
2510201      1      0.0          0.0      0.
*2510201      1      0.5          0.0      0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*          hyd dia    beta          y-int      slope
*2510110    0.035      0.00        0.725      1.00
*
*-----
*-----
*
*          name          type
2800000      l-shroud      annulus
*
*          no.vol
2800001          5
*
*          area          vol no
2800101      2.28e-3          2
2800102      7.922e-3          4
2800103      1.806e-3          5
*
*          vol lgh      vol no
2800301      0.038          1
2800302      0.075          2
2800303      0.100          3
2800304      0.081          4
2800305      0.020          5
*
*          vr ang      vol no
2800601      90.0          5
*
*          elv ch      vol no
2800701      0.038          1
2800702      0.075          2
2800703      0.100          3
2800704      0.081          4
2800705      0.020          5
*
*          rough      hy dia      vol no
2800801      4.57e-5      0.013          2
2800802      4.57e-5      0.05605          4
2800803      4.57e-5      0.0227          5
*
*          floss    rloss      jn.no.
2800901      0.0      0.0          4
*
*          pvbfe      vol no
2801001      10000          5
*
*          fvcchs      jn no
2801101      001000          1

```

```

2801102      001100      2      * abrupt area change
2801103      001000      4      * smooth area change
*
*          ctl    pressure    temp                      vol no
2801201    103    6.67e6    479.0    0.0    0.0    0.0      5
*
*          ctl
2801300      1
*          flow-f    flow-g    velj    jun no
2801301          0.0          0.0          0.          4
*2801301          0.5          0.0          0.          4
*
*-----
*
*-----
*
*          name          type
2810000      fa-injun    sngljun
*
*          from          to    jn area    f loss    r loss    fvcahs
2810101 280050002 300010001 1.806e-3    0.26    0.26    001000 * no choking
*
*          ctl    flow-f    flow-g    velj
2810201      1          0.0          0.0          0.
*2810201      1          0.5          0.0          0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*          hyd dia    beta          y-int    slope
*2810110    0.035    0.00          0.725    1.00
*
*-----
*
*-----
*----- ACTIVE CORE MODEL -----
*-----
*
*          name          type
3000000      core          pipe
*
*          no.vol
3000001          20
*
*          area          vol no
3000101    1.806e-3          20
*
*          vol lgh          vol no
3000301          0.125          19
3000302          0.130          20
*
*          vr ang          vol no
3000601          90.0          20
*
*          elv ch          vol no
3000701          0.125          19
3000702          0.130          20
*

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```

*          rough      hy dia      vol no
3000801    1.5e-6      9.75e-3      20
*
*          floss      rloss      jn.no.
3000901    0.00      0.00        1
3000902    0.26      0.26        2
3000903    0.00      0.00        3
3000904    0.26      0.26        4
3000905    0.00      0.00        5
3000906    0.26      0.26        6
3000907    0.00      0.00        7
3000908    0.26      0.26        8
3000909    0.00      0.00        9
3000910    0.26      0.26       10
3000911    0.00      0.00       11
3000912    0.26      0.26       12
3000913    0.00      0.00       13
3000914    0.26      0.26       14
3000915    0.00      0.00       15
3000916    0.26      0.26       16
3000917    0.00      0.00       17
3000918    0.26      0.26       18
3000919    0.00      0.00       19
*
*          tlpvbf      vol no
*3001001    1100000      20      * REVISED 5/17/00
3001001    0010100      20
*
*          fvcahs      jn no
3001101    001000      19
*
*          ctl      pressure      qual      vol no
3001201    102      6.67e6      0.0      0.0  0.0  0.0      10
*
*          ctl      pressure      qual      vol no
3001202    102      6.67e6      0.7      0.0  0.0  0.0      15
3001203    102      6.67e6      0.7      0.0  0.0  0.0      20
*
*          ctl
3001300    1
*          flow-f      flow-g      velj      jun no
3001301    0.0      0.0      0.      19
*3001301    0.5      0.0      0.      19
*
*          hy-dia      jun no.
*3001401    9.75e-3      0.0      1.0      1.0      19
*-----
*
*-----
*----- CORE SHROUD ANNULAR GAP -----
*-----
*
*          name      type
3500000    core-gap      annulus
*
*          no.vol
3500001    21

```

```

*
*          area          vol no
3500101    2.2431e-2      21
*
*          vol lgh       vol no
3500301    0.020         1
3500302    0.125         20
3500303    0.130         21
*
*          vr ang        vol no
3500601    90.0          21
*
*          elv ch        vol no
3500701    0.020         1
3500702    0.125         20
3500703    0.130         21
*
*          rough   hy dia   vol no
3500801    4.57e-5   0.102   21
*
*          floss   rloss   jn.no.
3500901    0.0     0.0     20
*
*          tlpvbf   vol no
*3501001    00000    21      * REVISED 5/17/00
3501001    1110000    21
*
*          fvcahs   jn no
3501101    001000    20
*
*          ctl      pressure   qual          vol no
3501201    102     6.67e6      0.0          0.0 0.0 0.0      1
3501202    102     6.67e6      0.01         0.0 0.0 0.0      2
*          ctl      pressure   qual          vol no
3501203    102     6.67e6      0.7          0.0 0.0 0.0      16
3501204    102     6.67e6      0.7          0.0 0.0 0.0      21
*
*          ctl
3501300    1
*          flow-f   flow-g   velj   jun no
3501301    0.0     0.0       0.      20
*
-----
*
*
*          name          type
3510000    stag-jct      sngljun
*
*          from          to      jn area   f loss   r loss   fvcahs
3510101 250010001 350010001    0.0       0.0       0.0    001100 * abrupt area
* change
*
*          ctl   flow-f   flow-g   velj
3510201    1     0.0       0.0     0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance

```

```

*          hyd dia    beta      y-int      slope
*3510110    0.035      0.00      0.725      1.00
*
*-----
*
*          name          type
3990000      fa-outjn      sngljun
*
*          from          to      jn area    f loss    r loss      fvcahs
3990101 300200002 400010001 1.806e-3    0.26      0.26      001000 * no choking
*
*          ctl  flow-f      flow-g  velj
3990201    1      0.0      0.0      0
*3990201    1      0.5      0.0      0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*          hyd dia    beta      y-int      slope
*3990110    0.00974    0.00      0.725      1.00      * AMT 02/01/01
*
*-----
*-----
*----- UPPER PLENUM SECTION -----
*-----
*
*----- upper shroud region -----
*
*          name          type
4000000      u-shroud      pipe
*
*          no.vol
4000001          7
* 4000001          2      * MODIFIED 01/29/2001
*
*          area          vol no
4000101      1.806e-3      1
4000102      3.209e-3      5
4000103      5.395e-2      7
* 4000102      3.209e-3      2      * MODIFIED 01/29/2001
*
*          vol lgh      vol no
4000301      0.044      1
4000302      0.050      2
4000303      0.030      3
4000304      0.020      4
4000305      0.020      5
4000306      0.065      6
4000307      0.066      7
* 4000302      0.150      2      * MODIFIED 01/29/2001
*
*          vr ang      vol no
4000601      90.      7
* 4000601      90.      2      * MODIFIED 01/29/2001
*
*          elv ch      vol no
4000701      0.044      1
4000702      0.050      2
4000703      0.030      3
4000704      0.020      4

```

```

4000705      0.020      5
4000706      0.065      6
4000707      0.066      7
* 4000702      0.150      2      * MODIFIED 01/29/2001
*
*      rough      hy dia      vol no
4000801      4.57e-5      0.00974      1      * AMT 02/01/01
4000802      4.57e-5      0.01661      5
4000803      4.57e-5      0.15750      7
* 4000802      4.57e-5      0.0358      2      * MODIFIED 01/29/2001
*
*      floss      rloss      jn.no.
4000901      0.0      0.0      6
* 4000901      0.0      0.0      1      * MODIFIED 01/29/2001
*
*      pvbfe      vol no
4001001      10000      7
* 4001001      10000      2      * MODIFIED 01/29/2001
*
*      fvcahs      jn no
4001101      001100      1      * abrupt area change
4001102      001000      4
4001103      001100      5      * abrupt area change
4001104      001000      6
* 4001101      001100      1      * abrupt area change      * MODIFIED 01/29/2001
*
*      ctl      pressure      qual      vol no
4001201      102      6.67e6      0.7      0.0      0.0      0.0      7
* 4001201      102      6.67e6      0.7      0.0      0.0      0.0      2      * MODIFIED 01/29/2001
*
*      ctl
4001300      1
*      flow-f      flow-g      velj      jun no
4001301      0.0      0.0      0.      6
* 4001301      0.0      0.0      0.      1      * MODIFIED 01/29/2001
*4001301      0.5      0.0      0.      1
*
*      hy-dia      jun no
*4001401      9.74e-3      0.0      1.0      1.0      1      * AMT 01/31/01
*4001402      16.61e-3      0.0      1.0      1.0      5      * AMT 01/31/01
*4001403      157.50e-3      0.0      1.0      1.0      6      * AMT 01/31/01
*-----
* NEW CROSSFLOW JUNCTION ADDED 01/29/2001
*-----
*
*      name      type
4010000      cfloutjn      sngljun
*
*      from      to      jn area      f loss      r loss      fvcahs
4010101 400040002 450010003 4.71e-3      0.0      0.0      001003 * no choking
*
*      ctl      flow-f      flow-g      velj
4010201      1      0.0      0.0      0
*4010201      1      0.5      0.0      0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*      hyd dia      beta      y-int      slope

```

```

*4010110    0.035      0.00      0.725      1.00
*
*-----
*
* NEW CROSSFLOW JUNCTION ADDED 01/29/2001
*-----
*
*          name      type
* 4020000      cf2outjn  sngljun
*
*      from      to      jn area  f loss  r loss  fvcahs
* 4020101 400040004 450020003 9.413e-3  0.0    0.0    001003 * no choking
*
*      ctl  flow-f      flow-g  velj
* 4020201    1      0.0      0.0    0
* 4010201    1      0.5      0.0    0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*      hyd dia  beta      y-int  slope
* 4010110    0.035      0.00      0.725      1.00
*
*-----
*----- upper chamber of FA discharge -----
*
*          name      type
* 4200000      up-chamb  branch
*
*      no jun      in ctl
* 4200001          2      1
*
*      area      length      vol      hz ang      vr ang      elv ch
* 4200101      5.395e-2      0.101      0.0      0.0      90.0      0.101
*
*      rough      hydia      pvbfe
* 4200102      4.57e-5      0.2258      10000  *
*
*      ctl      pressure      qual
* 4200200      102      6.67e6      0.7
*
*      from      to      jun area  f loss  r loss  efvcahs
* 4201101      400050002      420010001 3.209e-3  0.0    0.0    1001100  *
* abrupt area change
* 4201101      400020002      420010001 3.209e-3  0.0    0.0    1001100  *  *
* MODIFIED 01/29/2001
* 4202101      420010001      450010001 5.395e-2  0.0    0.0    1001100  *
* abrupt area change
*
*      flow-f      flow-g      velj
* 4201201      0.0      0.      0. *
* 4202201      0.0      0.      0. *
* 4201201      0.5      0.      0. *
* 4202201      0.5      0.      0. *
*
*-----
*----- annular outlet plenum -----
*
*          name      type
4500000      annul-ot      annulus
*

```



```

*          no.vol
4500001      3
*4500001      2          * MODIFIED 01/29/2001
*
*          area      vol no
4500101      6.566e-2      3
* 4500101      6.566e-2      2          * MODIFIED 01/29/2001
*
*          vol lgh      vol no
4500301      0.040      1
4500302      0.030      2
4500303      0.050      3
* 4500301      0.100      2          * MODIFIED 01/29/2001
*
*          vr ang      vol no
4500601      -90.      3
* 4500601      -90.      2          * MODIFIED 01/29/2001
*
*          elv ch      vol no
4500701      -0.040      1
4500702      -0.030      2
4500703      -0.050      3
* 4500701      -0.10      1          * MODIFIED 01/29/2001
*
*          rough      hy dia      vol no
4500801      4.57e-5      0.220      3
* 4500801      4.57e-5      0.220      2          * MODIFIED 01/29/2001
*
*          floss      rloss      jn.no.
4500901      0.0      0.0      2
* 4500901      0.0      0.0      1          * MODIFIED 01/29/2001
*
*          pvbfe      vol no
4501001      10000      3
* 4501001      10000      2          * MODIFIED 01/29/2001
*
*          fvcchs      jn no
4501101      001000      2
* 4501101      001000      1          * MODIFIED 01/29/2001
*
*
*          ctl      pressure      qual      vol no
4501201      102      6.67e6      0.7      0.0      0.0      0.0      1          * AMT
* 01/18/01
4501202      102      6.67e6      0.0      0.0      0.0      0.0      3
* 4501202      102      6.67e6      0.7      0.0      0.0      0.0      2          * MODIFIED
* 01/29/2001
*
*          ctl
4501300      1
*          flow-f      flow-g      velj      jun no
4501301      0.0      0.0      0.      2
*4501301      0.5      0.0      0.      1
* 4501301      0.0      0.0      0.      1          * MODIFIED
* 01/29/2001
*
*-----
*----- Core outlet nozzle -----

```

```

*
*      name      type
4800000      core-out  branch
*
*      no jun      in ctl
4800001      2      1
*
*      area      length      vol      hz ang      vr ang      elv ch
4800101      7.854e-3      0.30      0.0      0.0      0.0      0.0
*
*      rough      hydia      pvbfe
4800102      4.57e-5      0.10      10000  *
*
*      ctl      pressure      qual
4800200      102      6.67e6      0.7
*
*      from      to      jun area  f loss r loss vcahs
4801101      450010004      480010001 7.854e-3  9.05  1.63  01002
*Note for Junction 1: abrupt area change losses per K's/momentum flux off
4802101      480010002      490010001 7.854e-3  0.0  0.0  01000  * no choked
* flow/smooth area change
* 4801101      450010004      480010001 7.854e-3  9.05  1.63  01002      *
* MODIFIED 01/29/2001
*
*      flow-f      flow-g      velj
4801201      0.0      0.      0.  *
4802201      0.0      0.      0.
*4801201      0.5      0.      0.  *
*4802201      0.5      0.      0.  *
*
*-----
*-----
*
*      name      type
4900000      upper-pl      pipe
*
*      no.vol
4900001      12
*
*      area      vol no
4900101      7.854e-3      1
4900102      8.1713e-3      12
*
*      vol lgh      vol no
4900301      0.420      1
4900302      0.751      11
4900303      0.580      12
*
*      vr ang      vol no
4900601      0.0      1
4900602      90.0      12
*
*      elv ch      vol no
4900701      0.0      1
4900702      0.751      11
4900703      0.580      12
*
*      rough      hy dia      vol no
4900801      4.57e-5      0.100      1
4900802      4.57e-5      0.102      12

```

```

*
*      floss  rloss  jn.no.
4900901      1.02  1.02    1
4900902      0.0   0.0   11
*
*      pvbfe    vol no
4901001      10000    12
*
*      fvcahs    jn no
4901101      0001100    1  * abrupt area change
4901102      0001000   11
*
*      ctl    pressure    qual    vol no
4901201    102    6.67e6    0.7 0.0 0.0 0.0    12
*
*      ctl
4901300    1
*      flow-f    flow-g    velj    jun no
4901301      0.0      0.0      0.    11
*4901301      0.5      0.0      0.    11
*
*-----
*
*      name      type
4910000      upln-hlj    sngljun
*
*      from      to      jn area    f loss  r loss fvcahs
4910101 490120003 500010001    0.0      2.85    1.40 001002 * momentum flux
* off
*
*      ctl    flow-f    flow-g    velj
4910201    1      0.0      0.0    0.
*4910201    1      0.5      0.0    0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*      hyd dia    beta      y-int    slope
*4910110    0.035    0.00    0.725    1.00
*
*-----
*-----  HOT LEG MODEL  -----
*-----
*
*      name      type
5000000      hotleg    pipe
*
*      no.vol
5000001      11
*
*      area      vol no
5000101    3.3183e-3    11
*
*      vol lgh    vol no
5000301      0.500      1
5000302      0.3927     2
5000303      0.6327     3
5000304      0.770      11

```

```

*
*          vr ang      vol no
5000601      1.0        11
*
*          elv ch      vol no
5000701      0.0087262    1
5000702      0.0068536    2
5000703      0.0110421    3
5000704      0.013438     11
*
*          rough      hy dia      vol no
5000801      4.57e-5    0.065     11
*
*          floss      rloss      jn.no.
5000901      0.0        0.0        1
5000902      0.413      0.413      2
5000903      0.0        0.0       10
*
*          pvbfe      vol no
5001001      10000      11
*
*          fvcchs      jn no
5001101      001000     10
*
*          ctl      pressure      qual      vol no
5001201      102      6.67e6      0.7 0.0 0.0 0.0      11
*
*          ctl
5001300      1
*          flow-f      flow-g      velj      jun no
5001301      0.0        0.0        0.        10
*5001301      0.5        0.0        0.        10
*
*-----
*
*----- 90deg, R500mm Elbow from Comp.500 to Comp.600 -----
*
*          name      type
5010000      hl-elbow      branch
*
*          no jun      in ctl
5010001      2          1
*
*          area      length      vol      hz ang      vr ang      elv ch
5010101      3.3183-3  0.7854      0.0      0.0      1.0      0.013707
*
*          rough      hydia      pvbfe
5010102      4.57e-5    0.065     10000  *
*
*          ctl      pressure      qual
5010200      102      6.67e6      0.7
*
*          from      to      jun area  f loss r loss  vcchs
5011101      500110002  501010001  3.3183e-3  0.0    0.0    01000  *
5012101      501010002  600010001  3.3183e-3  0.413  0.413  01000  *
*
*          flow-f      flow-g      velj
5011201      0.0        0.        0.  *

```

```

5012201      0.0      0.      0.
*5011201      0.5      0.      0. *
*5012201      0.5      0.      0. *
*
*
*-----
*----- SG BUNDLE #1 MODEL -----
*-----
*
*----- steam generator tube bundle #1 -----
*
*      name      type
6000000      sg-bun1      pipe
*
*      no.vol
6000001      2
*
*      area      vol no
6000101      3.3183e-3      2
*
*      vol lgh      vol no
6000301      0.500      1
6000302      0.4675      2
*
*      vr ang      vol no
6000601      1.0      2
*
*      elv ch      vol no
6000701      0.0087262      1
6000702      0.008159      2
*
*      rough      hy dia      vol no
6000801      4.57e-5      0.065      2
*
*      floss      rloss      jn.no.
6000901      0.0      0.0      1
*
*      pvbfe      vol no
6001001      10000      2
*
*      fvcchs      jn no
6001101      001000      1
*
*      ctl      pressure      qual      vol no
6001201      102      6.67e6      0.7      0.0      0.0      0.0      2
*
*      ctl
6001300      1
*      flow-f      flow-g      velj      jun no
6001301      0.0      0.0      0.      1
*6001301      0.5      0.0      0.      1
*
*-----
*----- SG bundle/steam release pipeline Tee connection -----
*
*      name      type
6010000      sg-tee      branch
*
*      no jun      in ctl

```

```

6010001      3      1
*
*      area      length      vol      hz ang      vr ang      elv ch
6010101      3.3183-3      0.065      0.0      0.0      0.0      0.0
*
*      rough      hydia      pvbfe
6010102      4.57e-5      0.065      10000      *
*
*      ctl      pressure      qual
6010200      102      6.67e6      0.7
*
*      from      to      jun area      f loss      r loss      vcahs
6011101      600020002      601010001      3.3183e-3      0.0      0.6      01000      *
6012101      601010002      700010001      3.3183e-3      0.6      0.0      01000      *
6013101      601010004      650010001      3.3183e-3      1.0      0.24      01002      * momentum
* flux off
*
*      flow-f      flow-g      velj
6011201      0.0      0.      0.      *
6012201      0.0      0.      0.      *
6013201      0.0      0.      0.
*6011201      0.5      0.      0.      *
*6012201      0.5      0.      0.      *
*6013201      0.0      0.      0.      *
*
*-----
*----- steam release pipe -----
*      name      type
6500000      stm-rels      pipe
*
*      no.vol
6500001      8
*
*      area      vol no
6500101      3.3183e-3      8
*
*      vol lgh      vol no
6500301      2.000      8
*
*      vr ang      vol no
6500601      1.0      8
*
*      elv ch      vol no
6500701      0.0349      8
*
*      rough      hy dia      vol no
6500801      4.57e-5      0.065      8
*
*      floss      rloss      jn.no.
6500901      0.0      0.0      7
*
*      pvbfe      vol no
6501001      10000      8
*
*      fvcchs      jn no
6501101      001000      7
*

```

```

*          ctl    pressure    qual          vol no
6501201    102    6.67e6      0.7  0.0  0.0  0.0      8
*
*          ctl
6501300    1
*          flow-f    flow-g    velj    jun no
6501301      0.0      0.0      0.      7
*
*
*-----
*
*----- SG BUNDLE #2 MODEL -----
*-----
*
*----- steam generator tube bundle #2 -----
*          name          type
7000000      sg-bun2      pipe
*
*          no.vol
7000001          2
*
*          area          vol no
7000101      3.3183e-3      2
*
*          vol lgh      vol no
7000301      0.4675      1
7000302      0.500      2
*
*          vr ang      vol no
7000601      -1.0      2
*
*          elv ch      vol no
7000701      -0.008159      1
7000702      -0.0087262      2
*
*          rough      hy dia      vol no
7000801      4.57e-5      0.065      2
*
*          floss      rloss      jn.no.
7000901      0.0      0.0      1
*
*          pvbfe      vol no
7001001      10000      2
*
*          fvcchs      jn no
7001101      001000      1
*
*          ctl    pressure    qual          vol no
7001201    102    6.67e6      0.7  0.0  0.0  0.0      2
*
*          ctl
7001300    1
*          flow-f    flow-g    velj    jun no
7001301      0.0      0.0      0.      1
*7001301      0.5      0.0      0.      1
*
*-----

```

```

*
*----- 90deg, R500mm Elbow from Comp.700 to Comp.800 -----
*
*      name      type
7010000      cl-elbow      branch
*
*      no jun      in ctl
7010001          2          1
*
*      area      length      vol      hz ang      vr ang      elv ch
7010101      3.3183-3      0.7854      0.0      0.0      -1.0      -0.013707
*
*      rough      hydia      pvbfe
7010102      4.57e-5      0.065      10000      *
*
*      ctl      pressure      qual
7010200      102      6.67e6      0.7
*
*      from      to      jun area      f loss      r loss      vcahs
7011101      700020002      701010001      3.3183e-3      0.0      0.0      01000      *
7012101      701010002      800010001      3.3183e-3      0.413      0.413      01000      *
*
*      flow-f      flow-g      velj
7011201      0.0      0.      0.      *
7012201      0.0      0.      0.
*7011201      0.5      0.      0.      *
*7012201      0.5      0.      0.      *
*
*
*-----
*
*----- COLD LEG MODEL -----
*
*----- upper-cold leg section -----
*
*      name      type
8000000      upper-cl      pipe
*
*      no.vol
8000001          10
*
*      area      vol no
8000101      3.3183e-3      10
*
*      vol lgh      vol no
8000301      0.645      10
*
*      vr ang      vol no
8000601      -1.0      10
*
*      elv ch      vol no
8000701      -0.0112569      10
*
*      rough      hy dia      vol no
8000801      4.57e-5      0.065      10
*
*      floss      rloss      jn.no.

```



```

8000901      0.0      0.0      9
*
*
*      pvbfe      vol no
8001001      10000      10
*
*      fvcahs      jn no
8001101      001000      9
*
*      ctl      pressure      qual      vol no
8001201      102      6.67e6      0.7      0.0      0.0      0.0      10
*
*      ctl
8001300      1
*      flow-f      flow-g      velj      jun no
8001301      0.0      0.0      0.      9
*8001301      0.5      0.0      0.      9
*
*-----
*
*      name      type
8010000      low-clj      sngljun
*
*      from      to      jn area      f loss      r loss      efvcahs
8010101 800100002 850010003      0.0      1.22      1.153      1001001 * ccfl and
* momentum flux off
*
*      ctl      flow-f      flow-g      velj
8010201      1      0.0      0.0      0.
*8010201      1      0.5      0.0      0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*      hyd dia      beta      y-int      slope
*8010110      0.035      0.00      0.725      1.00
*
*-----
*
*----- lower-cold leg section -----
*      name      type
8500000      lower-cl      pipe
*
*      no.vol
8500001      9
*
*      area      vol no
8500101      7.21e-3      2
8500102      4.88e-3      4
8500103      7.21e-3      9
*
*      vol lgh      vol no
8500301      0.580      1
8500302      0.639      2
8500303      0.535      4
8500304      0.938      9
*
*      vr ang      vol no
8500601      -90.0      9

```

```

*
*          elv ch          vol no
8500701    -0.580          1
8500702    -0.639          2
8500703    -0.535          4
8500704    -0.938          9
*
*          rough    hy dia    vol no
8500801    4.57e-5    0.057      2
8500802    4.57e-5    0.067      4
8500803    4.57e-5    0.057      9
*
*          floss    rloss    jn.no.
8500901    0.0      0.0      8
*
*          pvbfe    vol no
8501001    10000      9
*
*          fvcchs    jn no
8501101    001000      8
*
*          ctl    pressure    qual    vol no
8501201    102    6.67e6    0.7    0.0    0.0    0.0    9
*
*          ctl
8501300    1
*
*          flow-f    flow-g    velj    jun no
8501301    0.0      0.0      0.      8
*8501301    0.5      0.0      0.      8
*
*-----
*
*          name          type
8510000    cl-outjn    sngljun
*
*          from          to    jn area    f loss    r loss    fvcchs
8510101 850090002 100010001    0.0      0.0      0.0      1100 * abrupt area
* change
*
*          ctl    flow-f    flow-g    velj
8510201    1      0.0      0.0      0.
*8510201    1      0.5      0.0      0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*          hyd dia    beta    y-int    slope
*8510110    0.035    0.00    0.725    1.00
*
*-----
*
*          name          type
*9XX0000    SNG-JUN    sngljun
*
*          from          to    jn area    f loss    r loss    fvcchs
*9XX0101 9XX110002 910010001 3.1416e-4 0.0      0.0      00100 * abrupt area
* change (COMPUTE K)
*

```

```

*          ctl  flow-f          flow-g  velj
*9XX0201    1      0.5          0.0    0. *
*
* use Wallis
* use the y-int for tubes with a sharp-edged entrance
*          hyd dia    beta          y-int    slope
*9XX0110    0.035    0.00          0.725    1.00
*
*-----
*$=====
**          name          type
*9100000          TDV          tmdpv01
**
**          area          lgh          vol          hz ang          vr ang          elv ch
*9100101          0.0          1.0          1.e6          0.0          0.0          0.0
**
**          rough          hy dia          flg
*9100102          4.57e-5          0.0          00
**
**          ctl
*9100200          003
**
**          time          pressure          temp
*9100201          0.0          6.0129e6          478.
*9100202          10000.0          6.0129e6          478.
**
**
$=====
*
*
*=====
*          HEAT STRUCTURE INPUT DATA
*=====
*
*          *=====
*          Upper Downcomer Model
*          *=====
*
*gl data  nh      np      type          s-flg          l-cor          refl b-ind itv-num
11000000  9      3      2          0          0.0365
*
*mesh          loc-flg          frm flg
11000100          0          1
*
*          no-itv          r-cor          no-itv          r-cor
11000101          1          0.0405          1          0.0445
*
*          cmp-no          itv-no          cmp-no          itv-no
11000201          1          1          1          2
*
*          source          itv-no          source          itv-no
11000301          0.0          1          0.0          2
*
*ini temp          flg
11000400          0
*
11000401          556.0  1          556.0  2          556.0  3
*

```

*l-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
11000501	100010000	0	1	1	0.267	1
11000502	100020000	0	1	1	0.267	2
11000503	100030000	0	1	1	0.267	3
11000504	100040000	0	1	1	0.267	4
11000505	100050000	0	1	1	0.267	5
11000506	100060000	0	1	1	0.238	6
11000507	100070000	0	1	1	0.1382	7
11000508	100080000	0	1	1	0.1382	8
11000509	100090000	0	1	1	0.1382	9

*

*r-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
11000601	-800	0	3101	1	0.267	1
11000602	-800	0	3101	1	0.267	2
11000603	-800	0	3101	1	0.267	3
11000604	-800	0	3101	1	0.267	4
11000605	-800	0	3101	1	0.267	5
11000606	-800	0	3101	1	0.238	6
11000607	-800	0	3101	1	0.1382	7
11000608	-800	0	3101	1	0.1382	8
11000609	-800	0	3101	1	0.1382	9

*

*source	type	is-mplr	l-dr-ht	r-dr-ht	ht-str-no
11000701	0	0.0	0.0	0.0	9

*

*l-h-st	h-eq	dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f	grd-l-r	boil	num
11000801	0.0	11.0	11.0	0.0	0.0	0.0	0.0	0.0	1.0	9

*

*r-h-st	h-eq	dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f	grd-l-r	boil	num
11000901	0.0	11.0	11.0	0.0	0.0	0.0	0.0	0.0	1.0	9

*

*

* *****

* Upper/Lower Downcomer Connecting Branch

* *****

*

*gl data	nh	np	type	s-flg	l-cor	refl	b-ind	itv-num
11010000	1	3	2	0	0.0365			

*

*mesh	loc-flg	frm	flg
11010100	0		1

*

	no-itv	r-cor	no-itv	r-cor
11010101	1	0.04050	1	0.04450

*

	cmp-no	itv-no	cmp-no	itv-no
11010201	1	1	1	2

*

	source	itv-no	source	itv-no
11010301	0.0	1	0.0	2

*

*ini temp	flg
11010400	-1

*

	556.0	556.0	556.0
11010401			

*

*l-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
---------	--------	-----	-------	--------	-----------	-----------

```

11010501      101010000      0      1      1      0.35      1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
11010601      -800      0      3101      1      0.35      1
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
11010701      0      0.0      0.0      0.0      1
*
*l-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
11010801      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      1
*
*r-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
11010901      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      1
*
*-----
*
*      *****
*      Lower Downcomer Model
*      *****
*
*gl      data      nh      np      type      s-flg      l-cor      refl      b-ind      itv-num
11500000      13      5      2      0      0.04
*
*mesh      loc-flg      frm      flg
11500100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
11500101      2      0.0545      2      0.0605
*
*      cmp-no      itv-no      cmp-no      itv-no
11500201      3      2      1      4
*
*      source      itv-no      source      itv-no
11500301      0.0      4
*
*ini      temp      flg
11500400      -1
*
11500401      556.0      556.0      556.0      556.0      556.0
11500402      556.0      556.0      556.0      556.0      556.0
11500403      556.0      556.0      556.0      556.0      556.0
11500404      556.0      556.0      556.0      556.0      556.0
11500405      479.0      479.0      479.0      479.0      479.0
11500406      479.0      479.0      479.0      479.0      479.0
11500407      479.0      479.0      479.0      479.0      479.0
11500408      479.0      479.0      479.0      479.0      479.0
11500409      479.0      479.0      479.0      479.0      479.0
11500410      479.0      479.0      479.0      479.0      479.0
11500411      479.0      479.0      479.0      479.0      479.0
11500412      479.0      479.0      479.0      479.0      479.0
11500413      479.0      479.0      479.0      479.0      479.0
*
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
11500501      150010000      0      1      1      0.534      1
11500502      150020000      0      1      1      0.158      2
11500503      150030000      0      1      1      0.750      3
11500504      150040000      0      1      1      0.750      4

```

11500505	150050000	0	1	1	0.750	5
11500506	150060000	0	1	1	0.750	6
11500507	150070000	0	1	1	0.750	7
11500508	150080000	0	1	1	0.500	8
11500509	150090000	0	1	1	0.442	9
11500510	150100000	0	1	1	0.750	10
11500511	150110000	0	1	1	0.750	11
11500512	150120000	0	1	1	0.716	12
11500513	150130000	0	1	1	0.534	13

*

*r-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
11500601	-800	0	3102	1	0.534	1
11500602	-800	0	3102	1	0.158	2
11500603	-800	0	3102	1	0.750	3
11500604	-800	0	3102	1	0.750	4
11500605	-800	0	3102	1	0.750	5
11500606	-800	0	3102	1	0.750	6
11500607	-800	0	3102	1	0.750	7
11500608	-800	0	3102	1	0.500	8
11500609	-800	0	3102	1	0.442	9
11500610	-800	0	3102	1	0.750	10
11500611	-800	0	3102	1	0.750	11
11500612	-800	0	3102	1	0.716	12
11500613	-800	0	3102	1	0.534	13

*

*source	type	is-mplr	l-dr-ht	r-dr-ht	ht-str-no
11500701	0	0.0	0.0	0.0	13

*

*l-h-st	h-eq	dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f	grd-l-r	boil	num
11500801	0.0	11.0	11.0	0.0	0.0	0.0	0.0	0.0	1.0	13

*

*r-h-st	h-eq	dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f	grd-l-r	boil	num
11500901	0.0	11.0	11.0	0.0	0.0	0.0	0.0	0.0	1.0	13

*

*

Lower Downcomer/Lower Pipeline Connecting Branch

*

*gl data	nh	np	type	s-flg	l-cor	refl	b-ind	itv-num
11510000	1	3	2	0	0.0325			

*

*mesh	loc-flg	frm flg
11510100	0	1

*

	no-itv	r-cor	no-itv	r-cor
11510101	2	0.0375		

*

	cmp-no	itv-no	cmp-no	itv-no
11510201	1	2		

*

	source	itv-no	source	itv-no
11510301	0.0	2		

*

*ini temp	flg
11510400	-1

*

```

11510401      479.0      479.0      479.0
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
11510501      151010000      0      1      1      0.35      1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
11510601      -800      0      3101      1      0.35      1
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
11510701      0      0.0      0.0      0.0      1
*
*l-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
11510801      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      1
*
*r-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
11510901      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      1
*
*-----
*
*      *****
*      Lower Pipeline - Section A Model
*      *****
*
*gl data      nh      np      type      s-flg      l-cor      refl      b-ind      itv-num
19000000      11      3      2      0      0.0325
*
*mesh      loc-flg      frm flg
19000100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
19000101      2      0.0375
*
*      cmp-no      itv-no      cmp-no      itv-no
19000201      1      2
*
*      source      itv-no      source      itv-no
19000301      0.0      2
*
*ini temp      flg
19000400      0
*
19000401      479.0      1      479.0      2      479.0      3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
19000501      900010000      0      1      1      0.85      1
19000502      900020000      0      1      1      0.6354      2
19000503      900030000      0      1      1      0.80      3
19000504      900040000      0      1      1      0.80      4
19000505      900050000      0      1      1      0.4954      5
19000506      900060000      0      1      1      0.71      6
19000507      900070000      0      1      1      0.71      7
19000508      900080000      0      1      1      0.71      8
19000509      900090000      0      1      1      0.4954      9
19000510      900100000      0      1      1      0.80      10
19000511      900110000      0      1      1      0.80      11
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
19000601      -800      0      3101      1      0.85      1

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```

19000602      -800      0      3101      1      0.6354      2
19000603      -800      0      3101      1      0.80      3
19000604      -800      0      3101      1      0.80      4
19000605      -800      0      3101      1      0.4954      5
19000606      -800      0      3101      1      0.71      6
19000607      -800      0      3101      1      0.71      7
19000608      -800      0      3101      1      0.71      8
19000609      -800      0      3101      1      0.4954      9
19000610      -800      0      3101      1      0.80      10
19000611      -800      0      3101      1      0.80      11
*
*source          type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
19000701          0          0.0          0.0          0.0          11
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
19000801      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  11
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
19000901      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  11
*
*-----
*
*      *****
*      Lower Pipeline - Section B Model
*      *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
19400000  10      3      2          0      0.01
*
*mesh      loc-flg      frm flg
19400100          0          1
*
*      no-itv      r-cor      no-itv      r-cor
19400101          2      0.013
*
*      cmp-no      itv-no      cmp-no      itv-no
19400201          1          2
*
*      source      itv-no      source      itv-no
19400301          0.0          2
*
*ini temp      flg
19400400          0
*
19400401      479.0  1      479.0  2      479.0  3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
19400501      940010000      0      1      1      0.70      1
19400502      940020000      0      1      1      0.70      2
19400503      940030000      0      1      1      0.70      3
19400504      940040000      0      1      1      0.70      4
19400505      940050000      0      1      1      0.70      5
19400506      940060000      0      1      1      0.70      6
19400507      940070000      0      1      1      0.70      7
19400508      940080000      0      1      1      0.70      8
19400509      940090000      0      1      1      0.70      9
19400510      940100000      0      1      1      0.70      10
*

```



```

*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
19400601     -800         0       3103         1         0.70           1
19400602     -800         0       3103         1         0.70           2
19400603     -800         0       3103         1         0.70           3
19400604     -800         0       3103         1         0.70           4
19400605     -800         0       3103         1         0.70           5
19400606     -800         0       3103         1         0.70           6
19400607     -800         0       3103         1         0.70           7
19400608     -800         0       3103         1         0.70           8
19400609     -800         0       3103         1         0.70           9
19400610     -800         0       3103         1         0.70          10
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
19400701         0         0.0         0.0         0.0         10
*
*l-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
19400801         0.0      11.0      11.0      0.0         0.0         0.0         0.0         0.0         1.0      10
*
*r-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
19400901         0.0      11.0      11.0      0.0         0.0         0.0         0.0         0.0         1.0      10
*
*-----
*
*      *****
*      Lower Pipeline - Section C Model
*      *****
*
*gl data      nh      np      type      s-flg      l-cor      refl      b-ind      itv-num
19600000      15       3       2         0         0.0325
*
*mesh      loc-flg      frm flg
19600100         0         1
*
*      no-itv      r-cor      no-itv      r-cor
19600101         2         0.0375
*
*      cmp-no      itv-no      cmp-no      itv-no
19600201         1         2
*
*      source      itv-no      source      itv-no
19600301         0.0         2
*
*ini temp      flg
19600400         0
*
19600401      479.0      1      479.0      2      479.0      3
*
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
19600501      960010000      0       1         1         0.60           1
19600502      960020000      0       1         1         0.60           2
19600503      960030000      0       1         1         0.4954          3
19600504      960040000      0       1         1         0.71           4
19600505      960050000      0       1         1         0.71           5
19600506      960060000      0       1         1         0.71           6
19600507      960070000      0       1         1         0.4954          7
19600508      960080000      0       1         1         0.695           8
19600509      960090000      0       1         1         0.695           9

```

19600510	960100000	0	1	1	0.695	10
19600511	960110000	0	1	1	0.695	11
19600512	960120000	0	1	1	0.695	12
19600513	960130000	0	1	1	0.695	13
19600514	960140000	0	1	1	0.695	14
19600515	960150000	0	1	1	0.695	15
*						
*r-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
19600601	-800	0	3101	1	0.60	1
19600602	-800	0	3101	1	0.60	2
19600603	-800	0	3101	1	0.4954	3
19600604	-800	0	3101	1	0.71	4
19600605	-800	0	3101	1	0.71	5
19600606	-800	0	3101	1	0.71	6
19600607	-800	0	3101	1	0.4954	7
19600608	-800	0	3101	1	0.695	8
19600609	-800	0	3101	1	0.695	9
19600610	-800	0	3101	1	0.695	10
19600611	-800	0	3101	1	0.695	11
19600612	-800	0	3101	1	0.695	12
19600613	-800	0	3101	1	0.695	13
19600614	-800	0	3101	1	0.695	14
19600615	-800	0	3101	1	0.695	15
*						
*source	type	is-mplr	l-dr-ht	r-dr-ht	ht-str-no	
19600701	0	0.0	0.0	0.0	15	
*						
*l-h-st	h-eq dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f
19600801	0.0	11.0	11.0	0.0	0.0	0.0
*						
*r-h-st	h-eq dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f
19600901	0.0	11.0	11.0	0.0	0.0	0.0
*						

*						
* *****						
* Lower Plenum Model						
* *****						
*						
*gl data	nh	np	type	s-flg	l-cor	refl b-ind itv-num
12000000	4	3	2	0	0.0325	
*						
*mesh	loc-flg	frm flg				
12000100	0	1				
*						
	no-itv	r-cor	no-itv	r-cor		
12000101	2	0.03750				
*						
	cmp-no	itv-no	cmp-no	itv-no		
12000201	1	2				
*						
	source	itv-no	source	itv-no		
12000301	0.0	2				
*						
*ini temp	flg					
12000400	0					
*						

```

12000401      479.0  1      479.0  2      479.0  3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12000501      200010000      0      1      1      0.77      1
12000502      200020000      0      1      1      0.77      2
12000503      200030000      0      1      1      0.75      3
12000504      200040000      0      1      1      0.75      4
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12000601      -800      0      3101      1      0.77      1
12000602      -800      0      3101      1      0.77      2
12000603      -800      0      3101      1      0.75      3
12000604      -800      0      3101      1      0.75      4
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
12000701      0      0.0      0.0      0.0      4
*
*l-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
12000801      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      4
*
*r-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
12000901      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      4
*
*-----
*
*
*      *****
*      Core Inlet Plenum
*      *****
*
*gl data      nh      np      type      s-flg      l-cor      refl      b-ind      itv-num
12200000      1      3      2      0      0.05
*
*mesh      loc-flg      frm      flg
12200100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
12200101      2      0.062
*
*      cmp-no      itv-no      cmp-no      itv-no
12200201      1      2
*
*      source      itv-no      source      itv-no
12200301      0.0      2
*
*ini temp      flg
12200400      -1
*
12200401      479.0      479.0      479.0
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12200501      220010000      0      1      1      0.30      1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12200601      -800      0      3101      1      0.30      1
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
12200701      0      0.0      0.0      0.0      1

```

```

*
*1-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
12200801      0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0    1
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
12200901      0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0    1
*
*-----*
*
*  ****
*    Lower Annulus Core Simulator Vessel
*    (heat-transfer from annulus to outer shell)
*  ****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
12500000   3       4       2         0        0.15
*
*mesh      loc-flg      frm flg
12500100         0         1
*
*          no-itv      r-cor      no-itv      r-cor
12500101         3      0.21
*
*          cmp-no      itv-no      cmp-no      itv-no
12500201         1         3
*
*          source      itv-no      source      itv-no
12500301         0.0         3
*
*ini temp      flg
12500400         0
*
12500401      479.0   1      479.0   2      479.0   3      479.0   4
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12500501     250010000      0       1         1         0.081         1
12500502     250020000      0       1         1         0.100         2
12500503     250030000      0       1         1         0.075         3
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12500601     -800         0      3105         1         0.081         1
12500602     -800         0      3105         1         0.100         2
12500603     -800         0      3105         1         0.075         3
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
12500701         0         0.0         0.0         0.0         3
*
*1-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
12500801      0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0    3
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
12500901      0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0    3
*
*-----*
*
*  ****
*    Lower Core Conductor - Endcap (Slab)
*  ****

```

```

*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
12501000  1        5        1          0          0.0
*
*mesh      loc-flg      frm flg
12501100      0          1
*
*          no-itv      r-cor      no-itv      r-cor
12501101      4          0.07
*
*          cmp-no      itv-no      cmp-no      itv-no
12501201      1          4
*
*          source      itv-no      source      itv-no
12501301      0.0          4
*
*ini temp      flg
12501400      -1
*
12501401      479.0      479.0      479.0      479.0      479.0
*
*l-bndy      hy-vol      inc      b-cdt      a-code      surf-area      ht-str-no
12501501      250030000      0          1          1          0.1385          1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      surf-area      ht-str-no
12501601      -800          0          3105          1          0.1385          1
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
12501701      0          0.0          0.0          0.0          1
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
12501801      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0    1
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
12501901      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0    1
*
*-----
*
*
*  *****
*  Core Simulator Lower Shroud
*  (heat-transfer from annulus to inner shroud)
*  *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
12800000  3        3        2          0          0.059
*
*mesh      loc-flg      frm flg
12800100      0          1
*
*          no-itv      r-cor      no-itv      r-cor
12800101      2          0.065
*
*          cmp-no      itv-no      cmp-no      itv-no
12800201      1          2
*
*          source      itv-no      source      itv-no
12800301      0.0          2

```

```

*
*ini temp      flg
12800400      0
*
12800401      479.0  1      479.0  2      479.0  3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12800501      280020000      0      1      1      0.075      1
12800502      280030000      0      1      1      0.100      2
12800503      280040000      0      1      1      0.081      3
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
12800601      250030000      0      1      1      0.075      1
12800602      250020000      0      1      1      0.100      2
12800603      250010000      0      1      1      0.081      3
*
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
12800701      0      0.0      0.0      0.0      3
*
*l-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
12800801      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      3
*
*r-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
12800901      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      3
*
*-----
*-----
*
*      *****
*      Core Heat Source
*      *****
*
*gl data      nh      np      type      s-flg      l-cor      refl b-ind      itv-num
13000000      20      4      2      0      0.00297
*
*mesh      loc-flg      frm flg
13000100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
13000101      3      0.0045
*
*      cmp-no      itv-no      cmp-no      itv-no
13000201      1      3
*
*      source      itv-no      source      itv-no
13000301      1.0      3
*
*ini temp      flg
13000400      -1
*
13000401      556.0      556.0      556.0      556.0
13000402      556.0      556.0      556.0      556.0
13000403      556.0      556.0      556.0      556.0
13000404      556.0      556.0      556.0      556.0
13000405      556.0      556.0      556.0      556.0
13000406      556.0      556.0      556.0      556.0

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13000407	556.0	556.0	556.0	556.0
13000408	556.0	556.0	556.0	556.0
13000409	556.0	556.0	556.0	556.0
13000410	556.0	556.0	556.0	556.0
13000411	556.0	556.0	556.0	556.0
13000412	556.0	556.0	556.0	556.0
13000413	556.0	556.0	556.0	556.0
13000414	556.0	556.0	556.0	556.0
13000415	556.0	556.0	556.0	556.0
13000416	556.0	556.0	556.0	556.0
13000417	556.0	556.0	556.0	556.0
13000418	556.0	556.0	556.0	556.0
13000419	556.0	556.0	556.0	556.0
13000420	556.0	556.0	556.0	556.0

*

*

*l-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
13000501	0	0	0	1	2.375	1
13000502	0	0	0	1	2.375	2
13000503	0	0	0	1	2.375	3
13000504	0	0	0	1	2.375	4
13000505	0	0	0	1	2.375	5
13000506	0	0	0	1	2.375	6
13000507	0	0	0	1	2.375	7
13000508	0	0	0	1	2.375	8
13000509	0	0	0	1	2.375	9
13000510	0	0	0	1	2.375	10
13000511	0	0	0	1	2.375	11
13000512	0	0	0	1	2.375	12
13000513	0	0	0	1	2.375	13
13000514	0	0	0	1	2.375	14
13000515	0	0	0	1	2.375	15
13000516	0	0	0	1	2.375	16
13000517	0	0	0	1	2.375	17
13000518	0	0	0	1	2.375	18
13000519	0	0	0	1	2.375	19
13000520	0	0	0	1	2.47	20

*

*r-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
13000601	300010000	0	110	1	2.375	1
13000602	300020000	0	110	1	2.375	2
13000603	300030000	0	110	1	2.375	3
13000604	300040000	0	110	1	2.375	4
13000605	300050000	0	110	1	2.375	5
13000606	300060000	0	110	1	2.375	6
13000607	300070000	0	110	1	2.375	7
13000608	300080000	0	110	1	2.375	8
13000609	300090000	0	110	1	2.375	9
13000610	300100000	0	110	1	2.375	10
13000611	300110000	0	110	1	2.375	11
13000612	300120000	0	110	1	2.375	12
13000613	300130000	0	110	1	2.375	13
13000614	300140000	0	110	1	2.375	14
13000615	300150000	0	110	1	2.375	15
13000616	300160000	0	110	1	2.375	16
13000617	300170000	0	110	1	2.375	17
13000618	300180000	0	110	1	2.375	18
13000619	300190000	0	110	1	2.375	19

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13000620      300200000      0      110      1      2.47      20
*
*source          type      is-implr      l-dr-ht      r-dr-ht      ht-str-no
13000701          300      0.0499          0.0          0.0          19
13000702          300      0.0519          0.0          0.0          20
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
*13000801      0.0  11.0  11.0      0.0      0.0          0.0          0.0      1.0  10
*
13000900      1
*
*r-h-st  heqd  hlf  hlr  glf  glr  gkf  gkr boil  ncl  p/d  ff  #
13000901 .01345  0.0625  2.4425  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1.  1
13000902 .01345  0.1875  2.3175  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1.  2
13000903 .01345  0.3125  2.1925  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1.  3
13000904 .01345  0.4375  2.0675  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1.  4
13000905 .01345  0.5625  1.9425  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1.  5
13000906 .01345  0.6875  1.8175  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1.  6
13000907 .01345  0.8125  1.6925  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1.  7
13000908 .01345  0.9375  1.5675  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1.  8
13000909 .01345  1.0625  1.4425  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1.  9
13000910 .01345  1.1875  1.3175  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1. 10
13000911 .01345  1.3125  1.1925  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1. 11
13000912 .01345  1.4375  1.0675  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1. 12
13000913 .01345  1.5625  0.9425  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1. 13
13000914 .01345  1.6875  0.8175  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1. 14
13000915 .01345  1.8125  0.6925  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1. 15
13000916 .01345  1.9375  0.5675  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1. 16
13000917 .01345  2.0625  0.4425  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1. 17
13000918 .01345  2.1875  0.3175  0.063  0.188  0.26  0.26  1.0  2.505  1.417  1. 18
13000919 .01345  2.3125  0.1925  0.188  0.063  0.26  0.26  1.0  2.505  1.417  1. 19
13000920 .01345  2.44      0.065  0.065  0.19  0.26  0.26  1.0  2.505  1.417  1. 20
*
*
*23456789021234567890312345678904123456789051234567890612345678907234567890
*-----
*
*      *****
*      Core Simulator Shroud/Insulation
*      *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
13001000  22      6      2      0      0.030975
*
*mesh      loc-flg      frm flg
13001100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
13001101      3      0.04      2      0.0445
*
*      cmp-no      itv-no      cmp-no      itv-no
13001201      3      3      1      5
*
*      source      itv-no      source      itv-no
13001301      0.0      5
*
*ini temp      flg
13001400      -1

```


*

13001401	556.0	556.0	556.0	556.0	556.0	556.0
13001402	556.0	556.0	556.0	556.0	556.0	556.0
13001403	556.0	556.0	556.0	556.0	556.0	556.0
13001404	556.0	556.0	556.0	556.0	556.0	556.0
13001405	556.0	556.0	556.0	556.0	556.0	556.0
13001406	556.0	556.0	556.0	556.0	556.0	556.0
13001407	556.0	556.0	556.0	556.0	556.0	556.0
13001408	556.0	556.0	556.0	556.0	556.0	556.0
13001409	556.0	556.0	556.0	556.0	556.0	556.0
13001410	556.0	556.0	556.0	556.0	556.0	556.0
13001411	556.0	556.0	556.0	556.0	556.0	556.0
13001412	556.0	556.0	556.0	556.0	556.0	556.0
13001413	556.0	556.0	556.0	556.0	556.0	556.0
13001414	556.0	556.0	556.0	556.0	556.0	556.0
13001415	556.0	556.0	556.0	556.0	556.0	556.0
13001416	556.0	556.0	556.0	556.0	556.0	556.0
13001417	556.0	556.0	556.0	556.0	556.0	556.0
13001418	556.0	556.0	556.0	556.0	556.0	556.0
13001419	556.0	556.0	556.0	556.0	556.0	556.0
13001420	556.0	556.0	556.0	556.0	556.0	556.0
13001421	556.0	556.0	556.0	556.0	556.0	556.0
13001422	556.0	556.0	556.0	556.0	556.0	556.0

*

*l-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
---------	--------	-----	-------	--------	-----------	-----------

13001501	280050000	0	1	1	0.020	1
13001502	300010000	0	1	1	0.1250	2
13001503	300020000	0	1	1	0.1250	3
13001504	300030000	0	1	1	0.1250	4
13001505	300040000	0	1	1	0.1250	5
13001506	300050000	0	1	1	0.1250	6
13001507	300060000	0	1	1	0.1250	7
13001508	300070000	0	1	1	0.1250	8
13001509	300080000	0	1	1	0.1250	9
13001510	300090000	0	1	1	0.1250	10
13001511	300100000	0	1	1	0.1250	11
13001512	300110000	0	1	1	0.1250	12
13001513	300120000	0	1	1	0.1250	13
13001514	300130000	0	1	1	0.1250	14
13001515	300140000	0	1	1	0.1250	15
13001516	300150000	0	1	1	0.1250	16
13001517	300160000	0	1	1	0.1250	17
13001518	300170000	0	1	1	0.1250	18
13001519	300180000	0	1	1	0.1250	19
13001520	300190000	0	1	1	0.1250	20
13001521	300200000	0	1	1	0.130	21
13001522	400010000	0	1	1	0.044	22

*

*r-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
---------	--------	-----	-------	--------	-----------	-----------

13001601	350010000	0	1	1	0.020	1
13001602	350020000	0	1	1	0.1250	2
13001603	350030000	0	1	1	0.1250	3
13001604	350040000	0	1	1	0.1250	4
13001605	350050000	0	1	1	0.1250	5
13001606	350060000	0	1	1	0.1250	6
13001607	350070000	0	1	1	0.1250	7
13001608	350080000	0	1	1	0.1250	8

13001609	350090000	0	1	1	0.1250	9
13001610	350100000	0	1	1	0.1250	10
13001611	350110000	0	1	1	0.1250	11
13001612	350120000	0	1	1	0.1250	12
13001613	350130000	0	1	1	0.1250	13
13001614	350140000	0	1	1	0.1250	14
13001615	350150000	0	1	1	0.1250	15
13001616	350160000	0	1	1	0.1250	16
13001617	350170000	0	1	1	0.1250	17
13001618	350180000	0	1	1	0.1250	18
13001619	350190000	0	1	1	0.1250	19
13001620	350200000	0	1	1	0.1250	20
13001621	350210000	0	1	1	0.130	21
13001622	350210000	0	1	1	0.044	22

*

*source	type	is-mplr	l-dr-ht	r-dr-ht	ht-str-no
13001701	0	0.0	0.0	0.0	22

*

*l-h-st	h-eq	dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f	grd-l-r	boil	num
13001801	0.0	11.0	11.0	0.0	0.0	0.0	0.0	0.0	1.0	22

*

*r-h-st	h-eq	dia	h-l-f	h-l-r	grd-f	grd-r	grd-l-f	grd-l-r	boil	num
13001901	0.0	11.0	11.0	0.0	0.0	0.0	0.0	0.0	1.0	22

*

*

Core Simulator Pressure Vessel

*

*gl data	nh	np	type	s-flg	l-cor	refl	b-ind	itv-num
13500000	21	3	2	0	0.0955			

*

*mesh	loc-flg	frm	flg
13500100	0		1

*

	no-itv	r-cor	no-itv	r-cor
13500101	2	0.1095		

*

	cmp-no	itv-no	cmp-no	itv-no
13500201	1	2		

*

	source	itv-no	source	itv-no
13500301	0.0	2		

*

*ini temp	flg
13500400	-1

*

13500401	556.0	556.0	556.0
13500402	556.0	556.0	556.0
13500403	556.0	556.0	556.0
13500404	556.0	556.0	556.0
13500405	556.0	556.0	556.0
13500406	556.0	556.0	556.0
13500407	556.0	556.0	556.0
13500408	556.0	556.0	556.0
13500409	556.0	556.0	556.0
13500410	556.0	556.0	556.0

13500411	556.0	556.0	556.0
13500412	556.0	556.0	556.0
13500413	556.0	556.0	556.0
13500414	556.0	556.0	556.0
13500415	556.0	556.0	556.0
13500416	556.0	556.0	556.0
13500417	556.0	556.0	556.0
13500418	556.0	556.0	556.0
13500419	556.0	556.0	556.0
13500420	556.0	556.0	556.0
13500421	556.0	556.0	556.0

*

*l-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
13500501	350010000	0	1	1	0.020	1
13500502	350020000	0	1	1	0.1250	2
13500503	350030000	0	1	1	0.1250	3
13500504	350040000	0	1	1	0.1250	4
13500505	350050000	0	1	1	0.1250	5
13500506	350060000	0	1	1	0.1250	6
13500507	350070000	0	1	1	0.1250	7
13500508	350080000	0	1	1	0.1250	8
13500509	350090000	0	1	1	0.1250	9
13500510	350100000	0	1	1	0.1250	10
13500511	350110000	0	1	1	0.1250	11
13500512	350120000	0	1	1	0.1250	12
13500513	350130000	0	1	1	0.1250	13
13500514	350140000	0	1	1	0.1250	14

13500515	350150000	0	1	1	0.1250	15
13500516	350160000	0	1	1	0.1250	16
13500517	350170000	0	1	1	0.1250	17
13500518	350180000	0	1	1	0.1250	18
13500519	350190000	0	1	1	0.1250	19
13500520	350200000	0	1	1	0.1250	20
13500521	350210000	0	1	1	0.13	21

*

*r-bndy	hy-vol	inc	b-cdt	a-code	cy-length	ht-str-no
13500601	-800	0	3105	1	0.020	1
13500602	-800	0	3105	1	0.1250	2
13500603	-800	0	3105	1	0.1250	3
13500604	-800	0	3105	1	0.1250	4
13500605	-800	0	3105	1	0.1250	5
13500606	-800	0	3105	1	0.1250	6
13500607	-800	0	3105	1	0.1250	7
13500608	-800	0	3105	1	0.1250	8
13500609	-800	0	3105	1	0.1250	9
13500610	-800	0	3105	1	0.1250	10
13500611	-800	0	3105	1	0.1250	11
13500612	-800	0	3105	1	0.1250	12
13500613	-800	0	3105	1	0.1250	13
13500614	-800	0	3105	1	0.1250	14
13500615	-800	0	3105	1	0.1250	15
13500616	-800	0	3105	1	0.1250	16
13500617	-800	0	3105	1	0.1250	17
13500618	-800	0	3105	1	0.1250	18
13500619	-800	0	3105	1	0.1250	19
13500620	-800	0	3105	1	0.1250	20
13500621	-800	0	3105	1	0.13	21

```

*
*source          type    is-implr    l-dr-ht    r-dr-ht    ht-str-no
13500701         0        0.0        0.0        0.0        21

*
*1-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
13500801      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  21
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
13500901      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  21
*
*-----
*
*
*
*  =====
*  Fuel Assembly Head Simulator
*  =====
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
14000000   3       3       2          0        0.0375
* 14000000   2       3       2          0        0.0375
* MODIFIED 01/29/2001
*
*mesh      loc-flg    frm flg
14000100         0        1
*
*          no-itv      r-cor      no-itv      r-cor
14000101         2        0.045
*
*          cmp-no      itv-no      cmp-no      itv-no
14000201         1        2
*
*          source      itv-no      source      itv-no
14000301         0.0        2
*
*ini temp      flg
14000400         0
*
14000401    556.0   1    556.0  2    556.0   3
*
*1-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
14000501    400020000      0        1        1        0.050        1
14000502    400030000      0        1        1        0.030        2
14000503    400040000      0        1        1        0.020        3
* 14000501    400020000      0        1        1        0.100        1
* MODIFIED 01/29/2001
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
14000601    450030000      0        1        1        0.050        1
14000602    450020000      0        1        1        0.030        2
14000603    450010000      0        1        1        0.020        3
* 14000601    450010000      0        1        1        0.100        1
* MODIFIED 01/29/2001
*
*source          type    is-implr    l-dr-ht    r-dr-ht    ht-str-no
14000701         0        0.0        0.0        0.0        3
* 14000701         0        0.0        0.0        0.0        2
* MODIFIED 01/29/2001

```

```

*
*l-h-st h-eq dia h-l-f h-l-r grd-f grd-r grd-l-f grd-l-r boil num
14000801 0.0 11.0 11.0 0.0 0.0 0.0 0.0 1.0 3
* 14000801 0.0 11.0 11.0 0.0 0.0 0.0 0.0 1.0 2
* MODIFIED 01/29/2001
*
*r-h-st h-eq dia h-l-f h-l-r grd-f grd-r grd-l-f grd-l-r boil num
14000901 0.0 11.0 11.0 0.0 0.0 0.0 0.0 1.0 3
* 14000901 0.0 11.0 11.0 0.0 0.0 0.0 0.0 1.0 2
* MODIFIED 01/29/2001
*
*-----
*
* *****
* Upper Cavity Pressure Vessel
* *****
*
*gl data nh np type s-flg l-cor refl b-ind itv-num
14002000 2 4 2 0 0.1325
*
*mesh loc-flg frm flg
14002100 0 1
*
* no-itv r-cor no-itv r-cor
14002101 3 0.21
*
* cmp-no itv-no cmp-no itv-no
14002201 1 3
*
* source itv-no source itv-no
14002301 0.0 3
*
*ini temp flg
14002400 -1
*
14002401 556.0 556.0 556.0 556.0
14002402 556.0 556.0 556.0 556.0
*
*l-bndy hy-vol inc b-cdt a-code cy-length ht-str-no
14002501 400060000 0 1 1 0.065 1
14002502 400070000 0 1 1 0.066 2
*
*r-bndy hy-vol inc b-cdt a-code cy-length ht-str-no
14002601 -800 0 3105 1 0.065 1
14002602 -800 0 3105 1 0.066 2
*
*source type is-mplr l-dr-ht r-dr-ht ht-str-no
14002701 0 0.0 0.0 0.0 2
*
*l-h-st h-eq dia h-l-f h-l-r grd-f grd-r grd-l-f grd-l-r boil num
14002801 0.0 11.0 11.0 0.0 0.0 0.0 0.0 1.0 2
*
*r-h-st h-eq dia h-l-f h-l-r grd-f grd-r grd-l-f grd-l-r boil num
14002901 0.0 11.0 11.0 0.0 0.0 0.0 0.0 1.0 2
*
*-----
*

```

```

*      *****
*      Upper Core Conductor - Endcap (Slab)
*      *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
14001000  1        5        1          0          0.0
*
*mesh      loc-flg      frm flg
14001100      0          1
*
*      no-itv      r-cor      no-itv      r-cor
14001101      4          0.07
*
*      cmp-no      itv-no      cmp-no      itv-no
14001201      1          4
*
*      source      itv-no      source      itv-no
14001301      0.0          4
*
*ini temp      flg
14001400      -1
*
14001401      556.0      556.0      556.0      556.0      556.0
*
*l-bndy      hy-vol      inc      b-cdt      a-code      surf-area      ht-str-no
14001501      400070000      0          1          1          0.1385          1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      surf-area      ht-str-no
14001601      -800          0          3105          1          0.1385          1
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
14001701      0          0.0          0.0          0.0          1
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14001801      0.0  11.0  11.0  0.0      0.0      0.0      0.0      1.0      1
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14001901      0.0  11.0  11.0  0.0      0.0      0.0      0.0      1.0      1
*
*-----
*
*
*      *****
*      Core Outlet Pressure Vessel
*      *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
14500000  3        4        2          0          0.15
* 14500000  2        4        2          0          0.15
* MODIFIED 01/29/2001
*
*mesh      loc-flg      frm flg
14500100      0          1
*
*      no-itv      r-cor      no-itv      r-cor
14500101      3          0.21
*
*      cmp-no      itv-no      cmp-no      itv-no

```

```

14500201          1          3

*
*          source      itv-no      source      itv-no
14500301          0.0          3
*
*ini temp          flg
14500400          0
*
14500401    556.0    1    556.0    2    556.0    3    556.0    4
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
14500501    450010000      0      1      1      0.040      1
14500502    450020000      0      1      1      0.030      2
14500503    450030000      0      1      1      0.050      3
* 14500501    450010000      0      1      1      0.100      1
* MODIFIED 01/29/2001
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
14500601     -800      0    3105      1      0.040      1
14500602     -800      0    3105      1      0.030      2
14500603     -800      0    3105      1      0.050      3
* 14500601     -800      0    3105      1      0.100      1
* MODIFIED 01/29/2001
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
14500701          0          0.0          0.0          0.0          3
* 14500701          0          0.0          0.0          0.0          2
* MODIFIED 01/29/2001
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14500801    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  3
* 14500801    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  2
* MODIFIED 01/29/2001
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14500901    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  3
* 14500901    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  2
* MODIFIED 01/29/2001
*
*-----
*
* *****
* Upper Plenum Model/Upper Core Simulator
* *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
14800000    1      3      2          0      0.05
*
*mesh      loc-flg      frm flg
14800100          0          1
*
*          no-itv      r-cor      no-itv      r-cor
14800101          2      0.062
*
*          cmp-no      itv-no      cmp-no      itv-no
14800201          1          2
*

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Page 96


```

*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14900801      0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0  1
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14900901      0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0  1
*
*-----
*
*  ****
*  Upper Plenum Model
*  ****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
14901000  11      3       2        0        0.051
*
*mesh      loc-flg      frm flg
14901100      0        1
*
*      no-itv      r-cor      no-itv      r-cor
14901101      2        0.057
*
*      cmp-no      itv-no      cmp-no      itv-no
14901201      1        2
*
*      source      itv-no      source      itv-no
14901301      0.0      2
*
*ini temp      flg
14901400      0
*
14901401      556.0  1  556.0  2  556.0  3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
14901501      490020000      0      1      1      0.751      1
14901502      490030000      0      1      1      0.751      2
14901503      490040000      0      1      1      0.751      3
14901504      490050000      0      1      1      0.751      4
14901505      490060000      0      1      1      0.751      5
14901506      490070000      0      1      1      0.751      6
14901507      490080000      0      1      1      0.751      7
14901508      490090000      0      1      1      0.751      8
14901509      490100000      0      1      1      0.751      9
14901510      490110000      0      1      1      0.751      10
14901511      490120000      0      1      1      0.580      11
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
14901601      -800      0      3104      1      0.751      1
14901602      -800      0      3104      1      0.751      2
14901603      -800      0      3104      1      0.751      3
14901604      -800      0      3104      1      0.751      4
14901605      -800      0      3104      1      0.751      5
14901606      -800      0      3104      1      0.751      6
14901607      -800      0      3104      1      0.751      7
14901608      -800      0      3104      1      0.751      8
14901609      -800      0      3104      1      0.751      9
14901610      -800      0      3104      1      0.751      10
14901611      -800      0      3104      1      0.580      11

```

```

*
*source          type    is-mplr    l-dr-ht    r-dr-ht    ht-str-no
14901701         0        0.0        0.0        0.0        11
*
*1-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14901801         0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  11
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
14901901         0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  11
*
*-----*
*
*  *****
*  Loop Hotleg Model
*  *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
15000000  11      3        2          0        0.0325
*
*mesh      loc-flg      frm flg
15000100          0          1
*
*          no-itv      r-cor      no-itv      r-cor
15000101          2      0.0375
*
*          cmp-no      itv-no      cmp-no      itv-no
15000201          1          2
*
*          source      itv-no      source      itv-no
15000301          0.0          2
*
*ini temp      flg
15000400          0
*
15000401  556.0  1  556.0  2  556.0  3
*
*1-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
15000501  500010000      0      1      1      0.50      1
15000502  500020000      0      1      1      0.3927      2
15000503  500030000      0      1      1      0.6327      3
15000504  500040000      0      1      1      0.77      4
15000505  500050000      0      1      1      0.77      5
15000506  500060000      0      1      1      0.77      6
15000507  500070000      0      1      1      0.77      7
15000508  500080000      0      1      1      0.77      8
15000509  500090000      0      1      1      0.77      9
15000510  500100000      0      1      1      0.77     10
15000511  500110000      0      1      1      0.77     11
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
15000601    -800          0     3101      1      0.50      1
15000602    -800          0     3101      1      0.3927      2
15000603    -800          0     3101      1      0.6327      3
15000604    -800          0     3101      1      0.77      4
15000605    -800          0     3101      1      0.77      5
15000606    -800          0     3101      1      0.77      6
15000607    -800          0     3101      1      0.77      7

```

```

15000608      -800          0      3101      1      0.77          8
15000609      -800          0      3101      1      0.77          9
15000610      -800          0      3101      1      0.77         10
15000611      -800          0      3101      1      0.77         11
*
*source          type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
15000701          0          0.0          0.0          0.0          11
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
15000801      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  11
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
15000901      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  11
*
*-----*
*
*  *****
*  Component 501 Elbow between 500/600
*  *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
15010000   1       3       2          0      0.0325
*
*mesh      loc-flg      frm flg
15010100          0          1
*
*          no-itv      r-cor      no-itv      r-cor
15010101          2      0.037500
*
*          cmp-no      itv-no      cmp-no      itv-no
15010201          1          2
*
*          source      itv-no      source      itv-no
15010301          0.0          2
*
*ini temp      flg
15010400          -1
*
15010401      556.0  556.0  556.0
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
15010501      501010000      0          1          1      0.7854          1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
15010601      -800          0      3101          1      0.7854          1
*
*source          type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
15010701          0          0.0          0.0          0.0          1
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
15010801      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  1
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
15010901      0.0  11.0  11.0  0.0    0.0    0.0    0.0    1.0  1
*
*-----*
*
*  *****

```

```

*   Steam Generator Tube Bundle No. 1
*   *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
16000000   2       3       2          0        0.0325
*
*mesh      loc-flg      frm flg
16000100          0          1
*
*          no-itv      r-cor      no-itv      r-cor
16000101          1      0.03500          1      0.037500
*
*          cmp-no      itv-no      cmp-no      itv-no
16000201          1          1          1          2
*
*          source      itv-no      source      itv-no
16000301          0.0          1          0.0          2
*
*ini temp      flg
16000400          0
*
16000401    556.0  1  556.0  2  556.0  3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
16000501    600010000          0          1          1          0.50          1
16000502    600020000          0          1          1          0.4675          2
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
16000601     -800          0        3100          1          0.50          1
16000602     -800          0        3100          1          0.4675          2
*
*source      type      is-implr      l-dr-ht      r-dr-ht      ht-str-no
16000701          0          0.0          0.0          0.0          2
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
16000801    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  1
16000802    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  2
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
16000901    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  1
16000902    0.0  11.0  11.0    0.0    0.0    0.0    0.0    1.0  2
*
*-----
*
*   *****
*   Steam Generator Tube Bundle TEE
*   *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
16010000   1       3       2          0        0.0325
*
*mesh      loc-flg      frm flg
16010100          0          1
*
*          no-itv      r-cor      no-itv      r-cor
16010101          1      0.03500          1      0.037500
*
*          cmp-no      itv-no      cmp-no      itv-no

```

```

16010201      1      1      1      2
*
*      source      itv-no      source      itv-no
16010301      0.0      1      0.0      2
*
*ini temp      flg
16010400      -1
*
16010401      556.0      556.0      556.0
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
16010501      601010000      0      1      1      0.065      1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
16010601      -800      0      3100      1      0.065      1
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
16010701      0      0.0      0.0      0.0      1
*
*l-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
16010801      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      1
*
*r-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
16010901      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      1
*
*-----
*
*      *****
*      Steam Release Pipe
*      *****
*
*gl data      nh      np      type      s-flg      l-cor      refl      b-ind      itv-num
16500000      8      3      2      0      0.0325
*
*mesh      loc-flg      frm      flg
16500100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
16500101      2      0.0375
*
*      cmp-no      itv-no      cmp-no      itv-no
16500201      1      2
*
*      source      itv-no      source      itv-no
16500301      0.0      2
*
*ini temp      flg
16500400      0
*
16500401      556.0      1      556.0      2      556.0      3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
16500501      650010000      0      1      1      2.0      1
16500502      650020000      0      1      1      2.0      2
16500503      650030000      0      1      1      2.0      3
16500504      650040000      0      1      1      2.0      4
16500505      650050000      0      1      1      2.0      5
16500506      650060000      0      1      1      2.0      6

```

```

16500507      650070000      0      1      1      2.0      7
16500508      650080000      0      1      1      2.0      8
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
16500601      -800      0      3101      1      2.0      1
16500602      -800      0      3101      1      2.0      2
16500603      -800      0      3101      1      2.0      3
16500604      -800      0      3101      1      2.0      4
16500605      -800      0      3101      1      2.0      5
16500606      -800      0      3101      1      2.0      6
16500607      -800      0      3101      1      2.0      7
16500608      -800      0      3101      1      2.0      8
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
16500701      0      0.0      0.0      0.0      8
*
*l-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
16500801      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      8
*
*r-h-st      h-eq      dia      h-l-f      h-l-r      grd-f      grd-r      grd-l-f      grd-l-r      boil      num
16500901      0.0      11.0      11.0      0.0      0.0      0.0      0.0      1.0      8
*
*-----*
*
*      *****
*      Steam Generator Tube Bundle No. 2
*      *****
*
*gl data      nh      np      type      s-flg      l-cor      refl      b-ind      itv-num
17000000      2      3      2      0      0.0325
*
*mesh      loc-flg      frm      flg
17000100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
17000101      1      0.03500      1      0.037500
*
*      cmp-no      itv-no      cmp-no      itv-no
17000201      1      1      1      2
*
*      source      itv-no      source      itv-no
17000301      0.0      1      0.0      2
*
*ini temp      flg
17000400      0
*
17000401      556.0      1      556.0      2      556.0      3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
17000501      700010000      0      1      1      0.4675      1
17000502      700020000      0      1      1      0.50      2
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
17000601      -800      0      3100      1      0.4675      1
17000602      -800      0      3100      1      0.50      2
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
17000701      0      0.0      0.0      0.0      1

```

```

17000702          0          0.0          0.0          0.0          2
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
17000801    0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0   1
17000802    0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0   2
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
17000901    0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0   1
17000902    0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0   2
*
*-----
*
*  *****
*  Component 701 Elbow between 700/800
*  *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
17010000   1       3       2          0        0.0325
*
*mesh      loc-flg      frm flg
17010100         0          1
*
*          no-itv      r-cor      no-itv      r-cor
17010101         2      0.037500
*
*          cmp-no      itv-no      cmp-no      itv-no
17010201         1          2
*
*          source      itv-no      source      itv-no
17010301        0.0          2
*
*ini temp      flg
17010400        -1
*
17010401    556.0    556.0    556.0
*

*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
17010501    701010000         0         1         1        0.7854         1
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
17010601    -800          0      3101         1        0.7854         1
*
*source      type      is-implr      l-dr-ht      r-dr-ht      ht-str-no
17010701         0          0.0          0.0          0.0          1
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
17010801    0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0   1
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
17010901    0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0   1
*
*-----
*
*  *****
*  Cold Leg Simulator - Upper ~Horiz. Section
*  *****
*

```

```

*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
18000000  10      3      2      0      0.0325
*
*mesh      loc-flg      frm flg
18000100      0      1
*
*      no-itv      r-cor      no-itv      r-cor
18000101      1      0.0350      1      0.03750
*
*      cmp-no      itv-no      cmp-no      itv-no
18000201      1      1      1      2
*
*      source      itv-no      source      itv-no
18000301      0.0      1      0.0      2
*
*ini temp      flg
18000400      0
*
18000401      556.0      1      556.0      2      556.0      3
*
*1-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
18000501      800010000      0      1      1      0.645      1
18000502      800020000      0      1      1      0.645      2
18000503      800030000      0      1      1      0.645      3
18000504      800040000      0      1      1      0.645      4
18000505      800050000      0      1      1      0.645      5
18000506      800060000      0      1      1      0.645      6
18000507      800070000      0      1      1      0.645      7
18000508      800080000      0      1      1      0.645      8
18000509      800090000      0      1      1      0.645      9
18000510      800100000      0      1      1      0.645      10
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
18000601      -800      0      3101      1      0.645      1
18000602      -800      0      3101      1      0.645      2
18000603      -800      0      3101      1      0.645      3
18000604      -800      0      3101      1      0.645      4
18000605      -800      0      3101      1      0.645      5
18000606      -800      0      3101      1      0.645      6
18000607      -800      0      3101      1      0.645      7
18000608      -800      0      3101      1      0.645      8
18000609      -800      0      3101      1      0.645      9
18000610      -800      0      3101      1      0.645      10
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
18000701      0      0.0      0.0      0.0      10
*
*
*1-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
18000801  0.0  11.0  11.0  0.0  0.0  0.0  0.0  1.0  10
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
18000901  0.0  11.0  11.0  0.0  0.0  0.0  0.0  1.0  10
*
*-----
*
*      *****
*      Cold Leg Simulator - Lower Vertical Section

```



```

*      *****
*
*gl data  nh      np      type      s-flg      l-cor      refl b-ind itv-num
18500000   9       3       2         0        0.051
*
*mesh      loc-flg      frm flg
18500100          0          1
*
*          no-itv      r-cor      no-itv      r-cor
18500101          1      0.0540          1      0.0570
*
*          cmp-no      itv-no      cmp-no      itv-no
18500201          1          1          1          2
*
*          source      itv-no      source      itv-no
18500301          0.0          1          0.0          2
*
*ini temp      flg
18500400          0
*
18500401    556.0   1    556.0   2    556.0   3
*
*l-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
18500501    850010000          0          1          1      0.580          1
18500502    850020000          0          1          1      0.639          2
18500503    850030000          0          1          1      0.535          3
18500504    850040000          0          1          1      0.535          4
18500505    850050000          0          1          1      0.938          5
18500506    850060000          0          1          1      0.938          6
18500507    850070000          0          1          1      0.938          7
18500508    850080000          0          1          1      0.938          8
18500509    850090000          0          1          1      0.938          9
*
*r-bndy      hy-vol      inc      b-cdt      a-code      cy-length      ht-str-no
18500601     -800          0      3101          1      0.580          1
18500602     -800          0      3101          1      0.639          2
18500603     -800          0      3101          1      0.535          3
18500604     -800          0      3101          1      0.535          4
18500605     -800          0      3101          1      0.938          5
18500606     -800          0      3101          1      0.938          6
18500607     -800          0      3101          1      0.938          7
18500608     -800          0      3101          1      0.938          8
18500609     -800          0      3101          1      0.938          9
*
*source      type      is-mplr      l-dr-ht      r-dr-ht      ht-str-no
18500701          0          0.0          0.0          0.0          9
*
*
*l-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
18500801   0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0    9
*
*r-h-st  h-eq dia  h-l-f h-l-r  grd-f  grd-r  grd-l-f  grd-l-r  boil num
18500901   0.0  11.0  11.0   0.0    0.0    0.0    0.0    1.0    9
*
*-----
*
*-----
*

```

```

*****
* MATERIAL THERMAL PROPERTY DATA
*****
*
*          type      cn flg      ca flg
*
* stainless steel (12X18H10T)
20100100      tbl/fctn          1          1  * (tables)
*
*          type      cn flg      ca flg
* stainless steel (12X18H9T)
20100200      tbl/fctn          1          1  * (tables)
*
*
* talkochlorit
20100300      tbl/fctn          1          1  * (tables)
*
* .....
*          thermal conductivity      w/(m*k)
* .....
*          *      temp      *      cond      *      temp      *      cond      *      temp      *      cond      *
* .....
* stainless steel (12X18H10T)
*
20100101          293.0          15.0          373.0          16.0          473.0          18.0
20100102          573.0          19.0          673.0          21.0          773.0          23.0
20100103          873.0          25.0          973.0          27.0          1073.0          26.0
20100104          1273.0          26.0
*
* stainless steel (12X18H9T)
*
20100201          293.0          16.0          373.0          16.0          473.0          18.0
20100202          573.0          20.0          673.0          21.0          773.0          23.0
20100203          873.0          25.0          973.0          26.0          1073.0          28.0
20100204          1173.0          29.0
*
* talkochlorit
20100301          293.0          1.50          393.0          1.20          493.0          1.1
20100302          593.0          1.0          693.0          0.9          793.0          0.8
20100303          893.0          0.75
*
* .....
*          volumetric heat capacity data      j/((m**3)*k)
* .....
*          temp      *      cap      *      temp      *      cap      *      temp      *      cap      *
* .....
* stainless steel (12X18H10T)
*
20100151          293.0      3649800.0      473.0      3878700.0      573.0      4022300.0
20100152          673.0      4164100.0      773.0      4229500.0      873.0      4307000.0
20100153          973.0      4370000.0      1073.0      4505800.0
*
* stainless steel (12X18H9T)
20100251          293.0      3705100.0      473.0      3800500.0      573.0      3874400.0
20100252          673.0      3955100.0      773.0      3991100.0      873.0      4039200.0
20100253          973.0      4043200.0      1073.0      4112600.0      1173.0      4115500.0
*
*

```

```

*   talkochlorit
20100351      293.0      2.204e6   393.0      2.4854e6 493.0      2.6812e6
20100352      593.0      2.8465e6 693.0      3.0114e6 793.0      3.146e6
20100353      893.0      3.28095e6

```

```

* .....

```

```

*
**=====

```

GENERAL TABLES

```

**=====

```

```

*

```

```

*

```

```

* specified heat transfer coefficients on ** SG tube surfaces **
(uninsulated)

```

```

*

```

	htc-t		time-fac	htc
20210000	htc-t	0	1.0	5.9

	time	htc-factor	(w/ ((m**2)*k)
20210001	0.0	0.0	
20210002	100.0	0.0	
20210003	500.0	2.8	
20210004	10000.0	2.8	

```

*

```

```

**-----

```

```

**

```

```

** specified heat transfer coefficients on ** Main Circulation Loop **
** 75 mm OD (insulated)

```

```

*

```

```

*

```

	htc-t		time-fac	htc
20210100	htc-t	0	1.0	3.2

	time	htc-factor	(w/ ((m**2)*k)
20210101	0.0	0.0	
20210102	100.0	0.0	
20210103	500.0	2.8	
20210104	10000.0	2.8	

```

**-----

```

```

**

```

```

** specified heat transfer coefficients on ** Lower Downcomer **
** 121 mm OD (insulated)

```

```

*

```

	htc-t		time-fac	htc
20210200	htc-t	0	1.0	3.4

```

**

```

	time	htc-factor	(w/ ((m**2)*k)
20210201	0.0	0.0	
20210202	100.0	0.0	
20210203	500.0	2.8	
20210204	10000.0	2.8	

```

**

```

```

**-----

```

```

**

```

```

** specified heat transfer coefficients on ** Lower Pipeline **
** 26 mm OD (insulated)

```

```

*

```

	time-fac	htc
--	----------	-----

```

20210300      htc-t      0      1.0      5.6
**
**              time              htc-factor      (w/ ((m**2)*k)
20210301          0.0              0.0
20210302          100.0            0.0
20210303          500.0            2.8
20210304         10000.0           2.8
**
**-----
**
** specified heat transfer coefficients on ** Upper Plenum Model **
** 114 mm OD (insulated)
*
*
*              time-fac      htc
20210400      htc-t      0      1.0      3.2
**
**              time              htc-factor      (w/ ((m**2)*k)
20210401          0.0              0.0
20210402          100.0            0.0
20210403          500.0            2.8
20210404         10000.0           2.8
**
**-----
**
** specified heat transfer coefficients on ** Core Simulator **
*
*
*              time-fac      htc
20210500      htc-t      0      1.0      2.8
**
**              time              htc-factor      (w/ ((m**2)*k)
20210501          0.0              0.0
20210502          100.0            0.0
20210503          500.0            2.8
20210504         10000.0           2.8
**
**-----
**
*              Core Power Table
*-----
*
*              table      trip      time coeff      power coeff
20230000      power      0      1.0      1.0      * fuel pins
*
*              time              power (Watts)
20230001          0.0              0.e3
20230002          100.0            0.e3
20230003          500.0            14.5e3
20230004         10000.0           14.5e3
*
*-----
*
*              atmosphere temperature
*-----
*
20280000      temp              * ambient air temperature
*
*              time              temp (k)
20280001          0.0              300.0

```

```

20280002          10000.0          300.0
*
*-----
*-----
*
**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==
*
*      CONTROL VARIABLES
*
**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==**==
*
*      Core water level
*
20593000      corelvl      sum      1.0      2.505      1
20593001      0.0          0.125      voidf      300010000
20593002          0.125      voidf      300020000
20593003          0.125      voidf      300030000
20593004          0.125      voidf      300040000
20593005          0.125      voidf      300050000
20593006          0.125      voidf      300060000
20593007          0.125      voidf      300070000
20593008          0.125      voidf      300080000
20593009          0.125      voidf      300090000
20593010          0.125      voidf      300100000
20593011          0.125      voidf      300110000
20593012          0.125      voidf      300120000
20593013          0.125      voidf      300130000
20593014          0.125      voidf      300140000
20593015          0.125      voidf      300150000
20593016          0.125      voidf      300160000
20593017          0.125      voidf      300170000
20593018          0.125      voidf      300180000
20593019          0.125      voidf      300190000
20593020          0.13      voidf      300200000
*
*
*      Core Annulus water level
*
20593500      annlslvl      sum      1.0      2.505      1
20593501      0.0          0.125      voidf      350020000
20593502          0.125      voidf      350030000
20593503          0.125      voidf      350040000
20593504          0.125      voidf      350050000
20593505          0.125      voidf      350060000
20593506          0.125      voidf      350070000
20593507          0.125      voidf      350080000
20593508          0.125      voidf      350090000
20593509          0.125      voidf      350100000
20593510          0.125      voidf      350110000
20593511          0.125      voidf      350120000
20593512          0.125      voidf      350130000
20593513          0.125      voidf      350140000
20593514          0.125      voidf      350150000
20593515          0.125      voidf      350160000
20593516          0.125      voidf      350170000
20593517          0.125      voidf      350180000
20593518          0.125      voidf      350190000
20593519          0.125      voidf      350200000
20593520          0.125      voidf      350210000
*

```

```

*      Upper Plenum water level
*
20594900      up-lvl      sum      1.0      8.08      1
20594901      0.0      0.751      voidf      490020000
20594902      0.751      voidf      490030000
20594903      0.751      voidf      490040000
20594904      0.751      voidf      490050000
20594905      0.751      voidf      490060000
20594906      0.751      voidf      490070000
20594907      0.751      voidf      490080000
20594908      0.751      voidf      490090000
20594909      0.751      voidf      490100000
20594910      0.751      voidf      490110000
20594911      0.580      voidf      490120000
*
*      Lower Downcomer water level
*
20591500      lwdc-lvl      sum      1.0      8.134      1
20591501      0.0      0.534      voidf      150010000
20591502      0.158      voidf      150020000
20591503      0.750      voidf      150030000
20591504      0.750      voidf      150040000
20591505      0.750      voidf      150050000
20591506      0.750      voidf      150060000
20591507      0.750      voidf      150070000
20591508      0.500      voidf      150080000
20591509      0.442      voidf      150090000
20591510      0.750      voidf      150100000
20591511      0.750      voidf      150110000
20591512      0.716      voidf      150120000
20591513      0.534      voidf      150130000
*
*
*      Lower Downcomer water level - absolute
*
20591600      lwdc-lva      sum      1.0      0.0      1
20591601      -5.925      1.000      cntrlvar      915
*
*      Upper Downcomer water level
*
20591000      updc-lvl      sum      1.0      1.84      1
20591001      0.0      0.267      voidf      100010000
20591002      0.267      voidf      100020000
20591003      0.267      voidf      100030000
20591004      0.267      voidf      100040000
20591005      0.267      voidf      100050000
20591006      0.238      voidf      100060000
20591007      0.1335      voidf      100070000
20591008      0.097729      voidf      100080000
20591009      0.035771      voidf      100090000
*
*
*****
*      HEAT LOSS CALCULATIONS      *
*****
*
*      Upper Downcomer heat loss
*

```

20510000	udc-heat	sum	1.0	0.0	1
20510001	0.0	0.0746537	htrnr	100000101	
20510002		0.0746537	htrnr	100000201	
20510003		0.0746537	htrnr	100000301	
20510004		0.0746537	htrnr	100000401	
20510005		0.0746537	htrnr	100000501	
20510006		0.0665452	htrnr	100000601	
20510007		0.038641	htrnr	100000701	
20510008		0.038641	htrnr	100000801	
20510009		0.038641	htrnr	100000901	

*

* Lower Downcomer heat loss

*

20515000	ldc-heat	sum	1.0	0.0	1
20515001	0.0	0.09786	htrnr	101000101	
20515002		0.20299	htrnr	150000101	
20515003		0.060061	htrnr	150000201	
20515004		0.28510	htrnr	150000301	
20515005		0.28510	htrnr	150000401	
20515006		0.28510	htrnr	150000501	
20515007		0.28510	htrnr	150000601	
20515008		0.28510	htrnr	150000701	
20515009		0.19007	htrnr	150000801	

20515010		0.16802	htrnr	150000901	
20515011		0.28510	htrnr	150001001	
20515012		0.28510	htrnr	150001101	
20515013		0.27218	htrnr	150001201	
20515014		0.20299	htrnr	150001301	
20515015		0.082467	htrnr	151000101	

*

*

* Lower Pipeline Section A heat loss

*

20590000	lpa-heat	sum	1.0	0.0	1
20590001	0.0	0.20028	htrnr	900000101	
20590002		0.14971	htrnr	900000201	
20590003		0.18850	htrnr	900000301	
20590004		0.18850	htrnr	900000401	
20590005		0.11673	htrnr	900000501	
20590006		0.16729	htrnr	900000601	
20590007		0.16729	htrnr	900000701	
20590008		0.16729	htrnr	900000801	
20590009		0.11673	htrnr	900000901	
20590010		0.18850	htrnr	900001001	
20590011		0.18850	htrnr	900001101	

*

*

* Lower Pipeline Section B heat loss

*

20594000	lpb-heat	sum	1.0	0.0	1
20594001	0.0	0.057177	htrnr	940000101	
20594002		0.057177	htrnr	940000201	
20594003		0.057177	htrnr	940000301	
20594004		0.057177	htrnr	940000401	
20594005		0.057177	htrnr	940000501	
20594006		0.057177	htrnr	940000601	
20594007		0.057177	htrnr	940000701	

20594008	0.057177	htrnr	940000801
20594009	0.057177	htrnr	940000901
20594010	0.057177	htrnr	940001001

*

*

*

* Lower Pipeline Section C heat loss

*

20596000	lpc-heat	sum	1.0	0.0	1
20596001	0.0	0.14137	htrnr	960000101	
20596002		0.14137	htrnr	960000201	
20596003		0.11673	htrnr	960000301	
20596004		0.16729	htrnr	960000401	
20596005		0.16729	htrnr	960000501	
20596006		0.16729	htrnr	960000601	
20596007		0.11673	htrnr	960000701	
20596008		0.16376	htrnr	960000801	
20596009		0.16376	htrnr	960000901	
20596010		0.16376	htrnr	960001001	
20596011		0.16376	htrnr	960001101	
20596012		0.16376	htrnr	960001201	
20596013		0.16376	htrnr	960001301	
20596014		0.16376	htrnr	960001401	
20596015		0.16376	htrnr	960001501	

*

*

* Lower Plenum heat loss

*

20520000	lpl-heat	sum	1.0	0.0	1
20520001	0.0	0.18143	htrnr	200000101	
20520002		0.18143	htrnr	200000201	
20520003		0.17671	htrnr	200000301	
20520004		0.17671	htrnr	200000401	

*

* Core Simulator Cylinder heat loss

*

20535000	corcylht	sum	1.0	0.0	1
20535001	0.0	0.086	htrnr	350000201	
20535002		0.086	htrnr	350000301	
20535003		0.086	htrnr	350000401	
20535004		0.086	htrnr	350000501	
20535005		0.086	htrnr	350000601	
20535006		0.086	htrnr	350000701	
20535007		0.086	htrnr	350000801	
20535008		0.086	htrnr	350000901	
20535009		0.086	htrnr	350001001	
20535010		0.086	htrnr	350001101	
20535011		0.086	htrnr	350001201	
20535012		0.086	htrnr	350001301	
20535013		0.086	htrnr	350001401	
20535014		0.086	htrnr	350001501	
20535015		0.086	htrnr	350001601	
20535016		0.086	htrnr	350001701	
20535017		0.086	htrnr	350001801	
20535018		0.086	htrnr	350001901	
20535019		0.086	htrnr	350002001	
20535020		0.08944	htrnr	350002101	

*


```

*          Core Simulator Inlet/Outlet heat loss
*
20535100      corendht      sum      1.0      0.0      1
20535101      0.0          0.11687    htrnr    220000101
20535102          0.10688    htrnr    250000101
20535103          0.13195    htrnr    250000201
20535104          0.09896    htrnr    250000301
20535105          0.1385     htrnr    250100101
*20535126          0.13327    htrnr    420000101
*20535127          0.13850    htrnr    420100101
20535128          0.13195    htrnr    450000101
20535139          0.065973   htrnr    450000101
20535110          0.01376    htrnr    350000101
20535111          0.11687    htrnr    480000101
*
*          Total Core Simulator heat loss
*
20535900      core-ht      sum      1.0      0.0      1
20535901      0.0          1.0        cntlvar  350
20535902          1.0        cntlvar  351
*
*
*          Upper Plenum heat loss
*
20549000      upl-heat      sum      1.0      0.0      1
20549001      0.0          0.16361    htrnr    490000101
20549002          0.26896    htrnr    490100101
20549003          0.26896    htrnr    490100201
20549004          0.26896    htrnr    490100301
20549005          0.26896    htrnr    490100401
20549006          0.26896    htrnr    490100501
20549007          0.26896    htrnr    490100601
20549008          0.26896    htrnr    490100701
20549009          0.26896    htrnr    490100801
20549010          0.26896    htrnr    490100901
20549011          0.26896    htrnr    490101001
20549012          0.20772    htrnr    490101101
*
*
*          Hot Leg heat loss
*
20550000      hl-heat      sum      1.0      0.0      1
20550001      0.0          0.11781    htrnr    500000101
20550002          0.092528   htrnr    500000201
20550003          0.14908    htrnr    500000301
20550004          0.18143    htrnr    500000401
20550005          0.18143    htrnr    500000501
20550006          0.18143    htrnr    500000601
20550007          0.18143    htrnr    500000701
20550008          0.18143    htrnr    500000801
20550009          0.18143    htrnr    500000901
20550010          0.18143    htrnr    500001001
20550011          0.18143    htrnr    500001101
20550012          0.11781    htrnr    501000101
*
*
*          SG heat loss (htrnr)
*

```

20560000	sg-heat	sum	1.0	0.0	1
20560001	0.0	0.11781	htrnr	600000101	
20560002		0.11015	htrnr	600000201	
20560003		0.015315	htrnr	601000101	
20560004		0.11015	htrnr	700000101	
20560005		0.11781	htrnr	700000201	
*					
*					
* SG heat loss (q)					
*					
20570000	sg-heat	sum	1.0	0.0	1
20570001	0.0	1.0	q	600010000	
20570002		1.0	q	600020000	
20570003		1.0	q	601010000	
20570004		1.0	q	700010000	
20570005		1.0	q	700020000	
*					
*					
* Steam Release Pipe heat loss					
*					
20565000	stm-heat	sum	1.0	0.0	1
20565001	0.0	0.47124	htrnr	650000101	
20565002		0.47124	htrnr	650000201	
20565003		0.47124	htrnr	650000301	
20565004		0.47124	htrnr	650000401	
20565005		0.47124	htrnr	650000501	
20565006		0.47124	htrnr	650000601	
20565007		0.47124	htrnr	650000701	
20565008		0.47124	htrnr	650000801	
*					
*					
* Upper Cold Leg heat loss					
*					
20580000	ucl-heat	sum	1.0	0.0	1
20580001	0.0	0.18506	htrnr	701000101	
20580002		0.15197	htrnr	800000101	
20580003		0.15197	htrnr	800000201	
20580004		0.15197	htrnr	800000301	
20580005		0.15197	htrnr	800000401	
20580006		0.15197	htrnr	800000501	
20580007		0.15197	htrnr	800000601	
20580008		0.15197	htrnr	800000701	
20580009		0.15197	htrnr	800000801	
20580010		0.15197	htrnr	800000901	
20580011		0.15197	htrnr	800001001	
*					
* Lower Cold Leg heat loss					
*					
20585000	lcl-heat	sum	1.0	0.0	1
20585001	0.0	0.20772	htrnr	850000101	
20585002		0.15197	htrnr	850000201	
20585003		0.15197	htrnr	850000301	
20585004		0.15197	htrnr	850000401	
20585005		0.15197	htrnr	850000501	
20585006		0.15197	htrnr	850000601	
20585007		0.15197	htrnr	850000701	
20585008		0.15197	htrnr	850000801	
20585009		0.15197	htrnr	850000901	

```

*
*
*      TOTAL LOOP heat loss
*
20500100      tot-hlos      sum      1.0      0.0      1
20500101      0.0      1.0      cntrlvar      100
20500102      1.0      cntrlvar      150
20500103      1.0      cntrlvar      900
20500104      1.0      cntrlvar      940
20500105      1.0      cntrlvar      960
20500106      1.0      cntrlvar      200
20500107      1.0      cntrlvar      359
20500108      1.0      cntrlvar      490
20500109      1.0      cntrlvar      500
20500110      1.0      cntrlvar      600
20500111      1.0      cntrlvar      650
20500112      1.0      cntrlvar      800
20500113      1.0      cntrlvar      850
*
*
*      TOTAL Core heat source
*
20500200      corepwr      sum      1.0      0.0      1
20500201      0.0      0.06715      htrnr      300000101
20500202      0.06715      htrnr      300000201
20500203      0.06715      htrnr      300000301
20500204      0.06715      htrnr      300000401
20500205      0.06715      htrnr      300000501
20500206      0.06715      htrnr      300000601
20500207      0.06715      htrnr      300000701
20500208      0.06715      htrnr      300000801
20500209      0.06715      htrnr      300000901
20500210      0.06715      htrnr      300001001
20500211      0.06715      htrnr      300001101
20500212      0.06715      htrnr      300001201
20500213      0.06715      htrnr      300001301
20500214      0.06715      htrnr      300001401
20500215      0.06715      htrnr      300001501
20500216      0.06715      htrnr      300001601
20500217      0.06715      htrnr      300001701
20500218      0.06715      htrnr      300001801
20500219      0.06715      htrnr      300001901
20500220      0.0698376      htrnr      300002001
*
*
*      NET heat input
*
20500300      net-heat      sum      1.0      0.0      1
20500301      0.0      1.0      cntrlvar      2
20500302      -1.0      cntrlvar      1
*
*
*+++++*
*      Core Steam Generation Rates      *
*+++++*
*
*      Core Steam Generation rate (kg/s)

```

```

*
20500400      core-sg1      sum      1.0      0.0      1
20500401      0.0      0.0002258      vapgen      300010000
20500402      0.0002258      vapgen      300020000
20500403      0.0002258      vapgen      300030000
20500404      0.0002258      vapgen      300040000
20500405      0.0002258      vapgen      300050000
20500406      0.0002258      vapgen      300060000
20500407      0.0002258      vapgen      300070000
20500408      0.0002258      vapgen      300080000
20500409      0.0002258      vapgen      300090000
20500410      0.0002258      vapgen      300100000
20500411      0.0002258      vapgen      300110000
20500412      0.0002258      vapgen      300120000
20500413      0.0002258      vapgen      300130000
20500414      0.0002258      vapgen      300140000
20500415      0.0002258      vapgen      300150000
20500416      0.0002258      vapgen      300160000
20500417      0.0002258      vapgen      300170000
20500418      0.0002258      vapgen      300180000
20500419      0.0002258      vapgen      300190000
20500420      0.0002348      vapgen      300200000

```

```

*
*
*      Core Steam Generation rate (kg/s)      (volume method)
*

```

```

20500500      core-sg2      sum      1.0      0.0      1
20500501      0.0      0.0002258      gammai      300010000
20500502      0.0002258      gammai      300020000
20500503      0.0002258      gammai      300030000
20500504      0.0002258      gammai      300040000
20500505      0.0002258      gammai      300050000
20500506      0.0002258      gammai      300060000
20500507      0.0002258      gammai      300070000
20500508      0.0002258      gammai      300080000
20500509      0.0002258      gammai      300090000
20500510      0.0002258      gammai      300100000
20500511      0.0002258      gammai      300110000
20500512      0.0002258      gammai      300120000
20500513      0.0002258      gammai      300130000
20500514      0.0002258      gammai      300140000
20500515      0.0002258      gammai      300150000
20500516      0.0002258      gammai      300160000
20500517      0.0002258      gammai      300170000
20500518      0.0002258      gammai      300180000
20500519      0.0002258      gammai      300190000
20500520      0.0002348      gammai      300200000

```

```

*
*
*      Core Steam Generation rate (kg/s)      (volume method)
*

```

```

20501400      core-sg3      sum      1.0      0.0      1
20501401      0.0      0.0002258      gammaw      300010000
20501402      0.0002258      gammaw      300020000
20501403      0.0002258      gammaw      300030000
20501404      0.0002258      gammaw      300040000
20501405      0.0002258      gammaw      300050000
20501406      0.0002258      gammaw      300060000

```

20501407		0.0002258	gammaw	300070000	
20501408		0.0002258	gammaw	300080000	
20501409		0.0002258	gammaw	300090000	
20501410		0.0002258	gammaw	300100000	
20501411		0.0002258	gammaw	300110000	
20501412		0.0002258	gammaw	300120000	
20501413		0.0002258	gammaw	300130000	
20501414		0.0002258	gammaw	300140000	
20501415		0.0002258	gammaw	300150000	
20501416		0.0002258	gammaw	300160000	
20501417		0.0002258	gammaw	300170000	
20501418		0.0002258	gammaw	300180000	
20501419		0.0002258	gammaw	300190000	
20501420		0.0002348	gammaw	300200000	
*					
*					
*					
* Annulus Steam Generation rate (kg/s) (volume method)					
*					
20501500	annul-sg	sum	1.0	0.0	1
20501501	0.0	0.002804	gammaw	350020000	
20501502		0.002804	gammaw	350030000	
20501503		0.002804	gammaw	350040000	
20501504		0.002804	gammaw	350050000	
20501505		0.002804	gammaw	350060000	
20501506		0.002804	gammaw	350070000	
20501507		0.002804	gammaw	350080000	
20501508		0.002804	gammaw	350090000	
20501519		0.002804	gammaw	350100000	
20501510		0.002804	gammaw	350110000	
20501511		0.002804	gammaw	350120000	
20501512		0.002804	gammaw	350130000	
20501513		0.002804	gammaw	350140000	
20501514		0.002804	gammaw	350150000	
20501515		0.002804	gammaw	350160000	
20501516		0.002804	gammaw	350170000	
20501517		0.002804	gammaw	350180000	
20501518		0.002804	gammaw	350190000	
20501519		0.002804	gammaw	350200000	
20501520		0.002916	gammaw	350210000	
*					
*					
* TOTAL Core Simulator Heat Generation rate (kg/s)					
*					
20501600	tot-sg	sum	1.0	0.0	1
20501601	0.0	1.0	cntrlvar	14	
20501602		1.0	cntrlvar	15	
20501603		0.000449	gammaw	350010000	
*					
*					
*					

* Steam Condensation Rates *					

*					
* Core Condensation rate (kg/s)					
*					
20502100	corecond	sum	1.0	0.0	1

20502101	0.0	0.0002258	gammac	300010000
20502102		0.0002258	gammac	300020000
20502103		0.0002258	gammac	300030000
20502104		0.0002258	gammac	300040000
20502105		0.0002258	gammac	300050000
20502106		0.0002258	gammac	300060000
20502107		0.0002258	gammac	300070000
20502108		0.0002258	gammac	300080000
20502109		0.0002258	gammac	300090000
20502110		0.0002258	gammac	300100000
20502111		0.0002258	gammac	300110000
20502112		0.0002258	gammac	300120000
20502113		0.0002258	gammac	300130000
20502114		0.0002258	gammac	300140000
20502115		0.0002258	gammac	300150000
20502116		0.0002258	gammac	300160000
20502117		0.0002258	gammac	300170000
20502118		0.0002258	gammac	300180000
20502119		0.0002258	gammac	300190000
20502120		0.0002348	gammac	300200000

*

*

* Core Annulus Condensation rate (kg/s)

*

20502200	ann-cond	sum	1.0	0.0	1
20502201	0.0	0.002804	gammac	350020000	
20502202		0.002804	gammac	350030000	
20502203		0.002804	gammac	350040000	
20502204		0.002804	gammac	350050000	
20502205		0.002804	gammac	350060000	
20502206		0.002804	gammac	350070000	
20502207		0.002804	gammac	350080000	
20502208		0.002804	gammac	350090000	
20502219		0.002804	gammac	350100000	
20502210		0.002804	gammac	350110000	
20502211		0.002804	gammac	350120000	
20502212		0.002804	gammac	350130000	
20502213		0.002804	gammac	350140000	
20502214		0.002804	gammac	350150000	
20502215		0.002804	gammac	350160000	
20502216		0.002804	gammac	350170000	
20502217		0.002804	gammac	350180000	
20502218		0.002804	gammac	350190000	
20502219		0.002804	gammac	350200000	
20502220		0.002916	gammac	350210000	

*

*

* Upper Plenum Condensation rate (kg/s)

*

20502300	upl-cond	sum	1.0	0.0	1
20502301	0.0	0.000079	gammac	400010000	
20502302		0.000481	gammac	400020000	
*20502303		0.005449	gammac	420010000	
20502304		0.006566	gammac	450010000	
20502305		0.003283	gammac	450020000	
20502306		0.002356	gammac	480010000	
20502307		0.006137	gammac	490010000	
20502308		0.006137	gammac	490020000	

20502309		0.006137	gammac	490030000	
20502310		0.006137	gammac	490040000	
20502311		0.006137	gammac	490050000	
20502312		0.006137	gammac	490060000	
20502313		0.006137	gammac	490070000	
20502314		0.006137	gammac	490080000	
20502315		0.006137	gammac	490090000	
20502316		0.006137	gammac	490100000	
20502317		0.006137	gammac	490110000	
20502318		0.006137	gammac	490120000	
*					
*					
* Hot Leg Condensation rate (kg/s)					
*					
20502400	ann-cond	sum	1.0	0.0	1
20502401	0.0	0.001659	gammac	500010000	
20502402		0.001303	gammac	500020000	
20502403		0.002099	gammac	500030000	
20502404		0.002555	gammac	500040000	
20502405		0.002555	gammac	500050000	
20502406		0.002555	gammac	500060000	
20502407		0.002555	gammac	500070000	
20502408		0.002555	gammac	500080000	
20502409		0.002555	gammac	500090000	
20502410		0.002555	gammac	500100000	
20502411		0.002555	gammac	500110000	
*					
*					
* SG Condensation rate (kg/s)					
*					
20502500	sg-cond	sum	1.0	0.0	1
20502501	0.0	0.0026062	gammac	501010000	
20502502		0.0016592	gammac	600010000	
20502503		0.0015513	gammac	600020000	
20502504		0.00021569	gammac	601010000	
20502505		0.0015513	gammac	700010000	
20502506		0.0016592	gammac	700020000	
20502507		0.0026062	gammac	701010000	
*					
*					
* Stm Release Pipe Condensation rate (kg/s)					
*					
20502600	sr-cond	sum	1.0	0.0	1
20502601	0.0	0.006637	gammac	650010000	
20502602		0.006637	gammac	650020000	
20502603		0.006637	gammac	650030000	
20502604		0.006637	gammac	650040000	
20502605		0.006637	gammac	650050000	
20502606		0.006637	gammac	650060000	
20502607		0.006637	gammac	650070000	
20502608		0.006637	gammac	650080000	
*					
*					
20502700	ucl-cond	sum	1.0	0.0	1
20502701	0.0	0.002140	gammac	800010000	
20502702		0.002140	gammac	800020000	
20502703		0.002140	gammac	800030000	
20502704		0.002140	gammac	800040000	

20502705		0.002140	gammac	800050000	
20502706		0.002140	gammac	800060000	
20502707		0.002140	gammac	800070000	
20502708		0.002140	gammac	800080000	
20502709		0.002140	gammac	800090000	
20502710		0.002140	gammac	800100000	
*					
*					
*					
20502800	lcl-cond	sum	1.0	0.0	1
20502801	0.0	0.004182	gammac	850010000	
20502802		0.004607	gammac	850020000	
20502803		0.002611	gammac	850030000	
20502804		0.002611	gammac	850040000	
20502805		0.006763	gammac	850050000	
20502806		0.006763	gammac	850060000	
20502807		0.006763	gammac	850070000	
20502808		0.006763	gammac	850080000	
20502809		0.006763	gammac	850090000	
*					
*					
*	Upper DC Condensation rate (kg/s)				
*					
20502900	udc-cond	sum	1.0	0.0	1
20502901	0.0	0.0011174	gammac	100010000	
20502902		0.0011174	gammac	100020000	
20502903		0.0011174	gammac	100030000	
20502904		0.0011174	gammac	100040000	
20502905		0.0011174	gammac	100050000	
20502906		0.00099693	gammac	100060000	
20502907		0.0005784	gammac	100070000	
20502908		0.0005784	gammac	100080000	
20502909		0.0005784	gammac	100090000	
*					
*	Lower DC Condensation rate (kg/s)				
*					
20503000	ldc-cond	sum	1.0	0.0	1
20503001	0.0	0.0011174	gammac	150010000	
20503002		0.0011174	gammac	150020000	
20503003		0.0011174	gammac	150030000	
20503004		0.0011174	gammac	150040000	
20503005		0.0011174	gammac	150050000	
20503006		0.00099693	gammac	150060000	
20503007		0.0005784	gammac	150070000	
20503008		0.0005784	gammac	150080000	
20503009		0.0005784	gammac	150090000	
*					
*	Integrated Loop Condensation rate (kg/s)				
*					
20503100	tot-cond	sum	1.0	0.0	1
20503101	0.0	1.0	cntrlvar	21	
20503102		1.0	cntrlvar	22	
20503103		1.0	cntrlvar	23	
20503104		1.0	cntrlvar	24	
20503105		1.0	cntrlvar	25	
20503106		1.0	cntrlvar	26	
20503107		1.0	cntrlvar	27	
20503108		1.0	cntrlvar	28	


```

20503109          1.0          cntrlvar    29
20503110          1.0          cntrlvar    30
20503111          0.000449      gammac      350010000
*
*
*
*-----*
*
*+++++*
*      Pressures      *
*+++++*
*
*      Core pressure drop
*
20500600      core-dp      sum      1.0      0.0      1
20500601      0.0      1.0      p      280050000
20500602      -1.0      p      400010000
*
*
*      Pout
*
20500700      p-out      sum      1.0      0.0      1
20500701      0.0      1.0e-5      p      480010000
*
*
*      DL2-4
*
20500800      updc-dp      sum      1.0      0.0      1
20500801      0.0      1.0      p      150020000
20500802      -1.0      p      850010000
*
*
*      DL4-14
*
20500900      ldc-dp      sum      1.0      0.0      1
20500901      0.0      1.0      p      150090000
20500902      -1.0      p      150020000
*
*
*      DL13-12
*
20501000      uppln-dp      sum      1.0      0.0      1
20501001      0.0      1.0      p      490010000
20501002      -1.0      p      490120000
*
*
*
.      * endcard

```

Appendix C
Peer Review of Input File

C.1 Input File Review

Review of RELAP5/MOD3.2 Input file for “RELAP5/MOD3.2 Analysis of INSC Standard Problem INSCSP-V4: Investigation of Heat Transfer for Partly Uncovered VVER-1000 Core at the Test Facility KS (RRC KI)”

R. T. Jensen ANL

I have reviewed the RELAP5 input file and the model nodalization contained in the subject report and have only minor comments and questions.

1. What is the reason or justification for setting the volume flag “p” to one for all or nearly all hydraulic volumes? This turns off the “water packing” option.
2. Components 280-01, 400-07, and 450-03 are dead ended volumes. This is contrary to INEL recommendations.
3. The from volume for single junction component 401 should specify face 3 or 4 instead of face 1.
4. The heat loss multiplier in general tables 101, 102, 103, 104, and 105 is 2.8 vs. 2.6 in the definition report.

I don't think any of these would change the analyses results.

C.2 Response to Input File Review Questions

A. M. Tentner ANL
J. W. Ahrens ANL

This memo responds to the questions about the *RELAP5/MOD3.2 Input file for “RELAP5/MOD3.2 Analysis of INSC Standard Problem INSCSP-V4: Investigation of Heat Transfer for Partly Uncovered VVER-1000 Core at the Test Facility KS (RRC KI)”* in the Input File Review presented in Appendix C.1.

1. What is the reason or justification for setting the volume flag “p” to one for all or nearly all hydraulic volumes? This turns off the “water packing” option.

A1 The volume flag "p" has been set to one for a number of hydraulic volumes to verify that no packing effect is present. No such effect was expected and none was observed.

2. Components 280-01, 400-07, and 450-03 are dead ended volumes. This is contrary to INEL recommendations.

A2 The volumes mentioned are indeed dead-end volumes and were modeled as such.

3. The from volume for single junction component 401 should specify face 3 or 4 instead of face 1.

A3 The from volume for single junction component 401 specifies face 2, not 1. This is consistent with the core exit nodalization used in the calculations, which is in Fig. 5-25, p.39. The single junction 401 connects the top face of volume 4, component 400 with the left face of volume 1, component 450. The impact of the core exit nodalization on results is discussed in Section 5.2.4.

4. The heat loss multiplier in general tables 101, 102, 103, 104, and 105 is 2.8 vs. 2.6 in the definition report.

A4 The heat loss multiplier used in our calculations was 2.8. This value was selected for our model because it provides optimal agreement between the calculated and measured pressures at the FA outlet, as discussed in Section 5.1.2, p. 23, and illustrated in Fig. 5-3. The value 2.6 mentioned in the definition report was based on the RMINSC model.