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Quarterly Review of 241-SY-101 Mixer Pump Data: October - December, 1998

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1.0 QUARTERLY SUMMARY

This report presents data obtained on 241-SY-101 pump performance. The period covered is October 1 through December 31, 1998.

During the quarter:

- There was an indication of a 7.0-inch increase in the waste level at riser 1A, and an average growth rate of 0.076 inches per day.
- There was an indication of a 2.3-inch increase in the waste level at riser 1C. This riser was flushed with water several times, which would lower the level of the crust at this location.
- Gases continued to be released at less than the pre-pump installation baseline rate, indicating a decrease in the gas generation rate, or an increase in gas retention, or both. The release rate was about 60 percent of the rate in the previous few quarters, and only 44 percent of the pre-pump release rate.
- There was no change in the parameters that monitor pump performance.

Key controls exist for waste temperature, gas concentration, pump parameters, and long-term waste behavior associated with the safe operation of the mixer pump that mitigates the buoyant displacement gas release event behavior of 241-SY-101. Table 1-1 compares the key controls and the current state of the waste as of December 31, 1998.

The pump was run 35 times between October 1 and December 31, 1998. Most of the pump runs were normal 25-minute, 1000-rpm excavation runs performed to mix the waste and release gas. Beginning in November, the pump oil high temperature alarm, set at 190 °F, would sometimes go off towards the end of pump runs. In those cases, the pump runs were shortened by approximately 1-2 minutes. The pump schedule was nominally three runs per week. However, core sampling activities interrupted the usual pump schedule several times during the quarter, resulting in less pump runs than normal. During this quarter, the pump showed no indication of degradation.

The Enraf level gauge in riser 1A indicated a level increase of 7.0 inches. The estimated growth rate is 0.076 inches per day, which is much higher than the growth rate of 0.043 inches per day during the previous quarter. It appears that the level growth is due to gas being retained in or under the crust. A temperature validation probe at MIT 17C indicated that the crust is thickening and the level of settled solids may have increased slightly. The level growth phenomenon is discussed further in Section 7.0.

The gas chromatograph (GC) GC-3, was operational 94% of the time. GC-1 was operational 95% of the time. During the quarter, the calculated gas releases were 44% of the baseline generation rate prior to pump installation (and significantly less than last quarter). The final run of the quarter, on December 29, 1998, was the 1002nd time the pump was operated since its installation in the tank. Hydrogen and nitrous oxide concentrations were lower than in previous quarters.

Table 1-1. Key Controls

Control	Requirement for Normal Pump Operation	Status as of 12/31/98
Level	N/A ¹	Riser 1A ² : 10.81 m (425.7 in.) Riser 1C: 10.34 m (407.3 in.)
Maximum Waste Temperature	< 51.7 °C (125 °F)	50.2 °C (122.4 °F)
Minimum Average Waste Temperature	> 43.3 °C (110 °F)	48.2 °C (118.8 °F)
Hydrogen	weekly average H ₂ concentration > 10 ppm < 7500 ppm during pump run	weekly average H ₂ concentrations ranged from 15 to 32 ppm < 150 ppm during pump runs
Long-Term Tank Conditions	any significant adverse change	level increase of 0.076 in./day ⁽³⁾ ; level growth is being evaluated (LMHC 1998)

¹Level controls were removed by Standing Order TWO-99-001 (LMHC 1998). For tank intrusive operations, the standing order requires a review of level data to ensure a change of > 0.5 inches has not occurred in the previous 24 hrs.

²See Appendix A for a discussion of riser numbering.

³Based on linear regression of the daily level at riser 1A. The level growth data from riser 1C were not used because 1C was subjected to several flushes.

2.0 LEVEL

The level at the end of the December quarter, according to the Enraf level gauge in riser 1C, was 10.34 m (407.3 in.), indicated a level increase of 2.3 inches for the quarter. The other Enraf in riser 1A indicated a level increase of 7.0 inches over the quarter. The level increases are discussed further in Section 6.0.

For the period from September 30 to December 31, 1998, the average difference (offset) between the two Enrafs was 42.2 cm (16.6 in.). This offset is 4.3 inches bigger than last quarter. The larger offset appears to be a result of flushes of the riser 1C level gauge. Figure 1 shows the Enraf-1C and Enraf-1A waste level measurements over the last year. Figure 2 shows the 1A level and the 120-day rolling average for the growth rate at riser 1A. The average growth rate has increased from about 0.020 at the beginning of 1998 to 0.076 at the end of 1998.

3.0 TEMPERATURES

The mixed slurry layer had an average temperature of 48.2 °C (118.8 °F) on December 31, 1998, based on Data Acquisition and Control System (DACS) readings from MIT-17B. The mixed slurry layer average temperature was 48.4 °C (119.1 °F) on December 31, 1998, based on DACS readings from MIT-17C. These average waste temperatures are above the minimum control temperature of 43.3 °C (110 °F). The maximum temperature from the current temperature profile (DACS readings) is 50.2 °C (122.4 °F) which is below the maximum control temperature of 51.7 °C (125 °F). Figure 3 shows the vertical temperature profiles at MIT-17B and -17C as of December 31, 1998.

Figure 4 shows the bulk average waste temperatures since January 1994. Temperatures at both MITs are following a seasonal trend, although the waste is approximately 1.5 °F hotter than in previous years. In addition, it is not yet clear that the seasonal peak has been reached. Previously, the maximum temperature had been reached by the end of the December quarter. Possible reasons for the increased temperature are discussed in Section 7.

4.0 GASES

There were no unexpected large gas releases during the quarter. Gas continued to be released at less than the pre-pump installation baseline rate, consistent with past quarters. However, the rate of release is much lower than in previous quarters. The weekly average hydrogen concentrations have been above 10 ppm, although some weekly averages have approached this level. Table 4-1 lists this quarter's monthly average gas concentrations. Table 4-2 compares this quarter's average gas concentrations with past quarterly averages. Hydrogen and nitrous oxide concentrations are lower than in previous quarters.

Table 4-1. Gas Monthly Average Concentrations

Gas (Instrument)	Monthly Average Concentrations (ppm)		
	10/1/98 - 10/31/98	11/1/98 - 11/30/98	12/1/98 - 12/31/98
Hydrogen (GC-1)	24	20	18
Hydrogen (GC-3)	21	23	23
Ammonia (FTIR)	48	49	47
Nitrous Oxide (FTIR)	17	19	19

Table 4-2. Quarterly Average Concentrations

Gas (Instrument)	4/1/98 - 6/30/98	7/1/98 - 9/30/98	10/1/98 - 12/31/98
Hydrogen (GC-1)	31	39	21
Hydrogen (GC-3)	31	33	22
Ammonia (FTIR) (conc. varies seasonally)	40	54	48
Nitrous Oxide (FTIR)	27	24	18

Figures 5, 6, and 7 show the hydrogen concentrations measured by GC-3 for each of the three months of this quarter. The hydrogen concentration in the dome reached as high as 188 ppm during the pump run on December 20, 1998. Peaks in previous quarters have been higher – the peak one year ago was 350 ppm. Notable natural releases are indicated on October 1, November 15 and 20, and December 27.

Figures 8, 9, and 10 show the GC-1 measured hydrogen concentrations for October through December 1998. Based on this instrument, the hydrogen concentration in the dome reached as high as 229 ppm during the pump run on October 19, 1998. Figures 11, 12, and 13 show the Fourier transform infrared spectrometer (FTIR) measured concentrations of ammonia and nitrous oxide for each month. High ammonia spikes on October 19 and December 23 are the result of ventilation shutdowns of 10 and 12 hours, respectively.

Figure 14 shows the calculated weekly total gas releases from January 1, 1994, to December 27, 1998. Daily total gas release volumes are calculated by integrating the product of the hydrogen concentration (GC-1) and the vent header flow rate and dividing by an assumed hydrogen fraction of 0.29 in the tank gas. These daily gas release volumes are summed on a weekly basis. Between October 4, 1998, and December 27, 1998, the average release was about 8.7 m³ (307 ft³) per week compared with the pre-pump installation baseline rate of 19.8 m³ (700 ft³) per week. A reduction in total gas release rate over time has been observed since the pump was installed in 1993. The release rate for this quarter is only 57 percent of the previous quarter's calculated release rate.

An overall release rate can also be derived from estimates of gas generation and retention. The average generation/release rate prior to pump installation was 19.8 m³ (700 ft³) per week. The reduction in the generation rate can be calculated by assuming the key radionuclide in the waste is ¹³⁷Cs. In the 5 years since the pump was installed, the ¹³⁷Cs concentration has dropped 11 percent because of radioactive decay. Assuming a linear relationship between the ¹³⁷Cs concentration and the gas generation rate, the current generation rate would be lower by 2.2 m³ (77 ft³) per week, or 17.6 m³ (623 ft³). The average level rise for the quarter (0.076 in/day from ENRAF in riser 1A) corresponds to 5.5 m³ (196 ft³) of retained gas per week, assuming the gas is retained in the crust at nearly atmospheric pressure. Subtracting this retention estimate from the generation estimate 17.6 m³ (623 ft³) yields an estimated release rate of 12.1 m³ (427 ft³) per week. This calculation is somewhat higher than the 8.7 m³ (307 ft³) per week derived from the H₂ release rate. Other than measurement

errors, a possible reason for the discrepancy is that these calculations rely on assumptions for generation rates and H_2 gas fractions that may no longer be valid.

Figure 15 shows the weekly volumes of ammonia and nitrous oxide released from January 1, 1994 to December 27, 1998. The seasonal variation of ammonia release is evident in the figure, although the latest upswing has been higher than the peak weekly values from previous years. A general decrease in nitrous oxide is also apparent. Figures 16, 17, and 18 show the weekly concentrations of hydrogen, nitrous oxide, and ammonia for the same period. The average N_2O/H_2 ratio calculated from this quarter's weekly averages is 0.83. Three years ago, from October to December 1995, the ratio was about 1.3.

5.0 PUMP PARAMETERS

The pump was run 35 times this quarter between October 1 and December 31, 1998. The schedule was typically three 25-minute, 1000-rpm excavation runs per week at the 12 standard orientations. Beginning in November, the pump oil high temperature alarm, set at 190 °F, would sometimes go off towards the end of pump runs. In those cases, the pump runs were shortened by approximately 1-2 minutes. Core sampling activities restricted the pumping schedule several times because of the restriction that the pump not be run with the drill string in the waste. There were several stretches of approximately 1 week where the pump was not run. The runs on October 16 and 17 were not complete 25-minute runs due to equipment problems.

Mixer pump performance remained unchanged during the quarter. Monitoring of the current, voltage, motor speed, volute and nozzle pressures, and oil temperature rate of rise indicated no degradation in performance. The current, voltage, and motor speed relationships have remained constant, as have the volute and nozzle pressures. There has been no indication of moisture in the motor oil. A sensor is located in the pump sump specifically for detecting water in the motor oil.

Data for a typical run during this quarter, on December 28, 1998, are presented in Figures 19-25. Figures 19 and 20 show nozzle pressures on a coarse and fine scale. Figure 21 shows volute pressure; Figure 22 shows pump current, voltage, and speed on a coarse scale; and Figures 23, 24, and 25 show the same data on a finer scale. Figure 26 shows the motor oil heat-up during the run. There were no significant changes in the values of these parameters during the quarter.

Although the oil temperature rise during pump runs has remained consistent, the oil cooling rate was identified as an issue in late December. The oil cooling rate is much slower than it was just a few months ago (Figure 27). The most likely explanations for the different cooling rate are that the bulk waste temperature is higher, leading to reduced heat transfer, or that a small hole in the top of the pump housing which previously allowed the hot waste around the pump to convect away, has become plugged. This issue is being evaluated.

The annual mixer pump motor winding insulation resistance check was completed December 29, 1998. All measured resistances were satisfactory (Gauck 1999).

6.0 CORE SAMPLING ACTIVITIES

Core sampling activities were initiated in accordance with Conner (1998). One of the three full depth, push mode core samples had been taken by the end of December. Laboratory results will be referenced in a future quarterly report.

7.0 WASTE BEHAVIOR

As discussed in Section 2.0, the Enraf level gauge in riser 1A showed an increase of 7.0 inches during the quarter. This gauge showed approximately 3.5-inch increases in the two previous quarters, and a two-inch increase during the two quarters before that. Prior to one year ago, the level only increased about an inch per quarter. The growth rate at riser 1A was 0.076 in. per day based on a linear regression of the daily level data. This rate is about the same as the pre-pump baseline growth rate (0.08 in. per day).

A very slight, adverse trend towards build-up of nonconvective solids appears to be occurring. Figure 28 shows the bottom four thermocouples of MIT-17B during the pump run on December 10, when a nozzle was pointed in the direction of this MIT (97 degrees). All of the thermocouples responded, although the bottom thermocouple did not quite reach the bulk temperature. This indicates an undisturbed layer of slightly greater than 4 inches thick at a distance of 8.60-m (28.2 ft) from the pump at this location. This is the first time since 1994 that the bottom thermocouple at MIT 17B did not reach the bulk slurry temperature during a pump run at this angle.

Figure 29 shows the MIT-17C bottom four thermocouples during the pump run of December 1, when a nozzle was pointed in the direction of the MIT (28 degrees). The data indicate an undisturbed solids layer somewhat higher than 16 inches. The thermocouple at the 16-inch level responds, but does not reach the bulk slurry temperature. The MIT is 9.32 m (30.6) feet from the pump, or 2.4 feet further than MIT 17B. Pump runs at this angle have occasionally excavated solids down to the 16-inch level, but not in the last year or so. The pump seems to be slightly less effective at excavating the settled solids at the MITs. This behavior is being monitored closely.

According to the MIT validation probe temperature profiles, an increase in crust thickness is occurring. The crust is approximately 2.5 m (100 in) thick based on the latest validation probe in MIT 17C (Figure 30). The crust thickness was reportedly 1 m (40 in.) thick in 1993 and for several years thereafter, and was estimated at 1.6 m (63 in) last quarter. Since the estimates from the last two quarters are from different risers, the sudden change may be at least partly due to variations in the crust topography and thickness. Figure 30 also shows the validation probe from October 24, 1996 in MIT 17C. The major differences between that probe and the December 8 probe are that the crust is now thicker, the settled solids layer appears thicker, and the waste is generally hotter by about 1.5 °F. The increase in temperature may be due to the thicker crust providing more insulation, limiting heat loss to the dome space.

The gas volumes calculated from the VFI data (Stewart et al. 1998), combined with a hydrostatics model for crust buoyancy, accurately reflected the waste level changes from

January 1995 to July 1998. This confirms that the SY-101 level growth is mainly due to gas accumulation in the crust (Stewart et al. 1998). A large buoyant displacement is not credible given the current configuration of the waste. The settled solids layer in the tank no longer stores enough gas to cause a large rollover.

In summary, many changes have been observed in the tank recently. The level growth issue was identified to be a significant problem approximately a year ago. The growth rate has accelerated to a current level of 0.076 inches per day, near the level growth rate prior to mixer pump installation. The level growth has been attributed to an increase in the amount of gas stored in the crust. The bulk slurry appears to be relatively free of gas voids. The crust thickness has increased significantly. The settled solids may have increased slightly and are not as readily excavated by the pump. The hydrogen dome concentration and release rates have dropped recently, as has the peak hydrogen concentrations following pump runs. This is consistent with a thicker crust (providing more resistance to gas migration). The nitrous oxide concentrations and release rates have been trending downward for at least two years. Finally, the bulk waste temperature is hotter than it has been for at least 4 years. The Test Review Group (TRG) will continue to monitor the tank parameters and determine what changes (if any) to pump operations should occur.

8.0 OTHER PARAMETERS

There were no unexpected changes in the other tank parameters that were monitored for changes in waste behavior. Figure 31 shows the tank pressure and vent header flow rate histories. The pressure and flow rate were normal for the quarter. Ventilation shutdowns occurred on October 19, November 6, and December 23. Figure 32 shows the vent header and atmospheric relative humidity histories. The water balance between ambient and vent header humidity indicates that during the quarter the waste gained about 2.0 gallons of water per day. Figure 33 shows the vent header and atmospheric temperatures during the quarter.

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- Gauck, G. J., 1999, *Data From Mixer Pump Windings Test*, HNF-3900, Lockheed Martin Hanford Corporation, Richland, Washington.
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- Stewart, C. W., J. M. Alzheimer, G. Chen, and P. A. Meyer, 1998, *In Situ Void Fraction and Gas Volume in Hanford Tank 241-SY-101 as Measured with the Void Fraction Instrument*, PNNL-12033, Pacific Northwest National Laboratory, Richland, Washington.

APPENDIX A

RISER NUMBERING

This document continues to use the historical riser numbers assigned when the tank was designed. A drawing was recently released (H-14-010531) which changed the riser numbering of tank 241-SY-101. The table below lists the old and new riser numbers for risers that are used for monitoring or sampling.

Old Riser Number	New Riser Number	Function
1C	001	Enraf
1A	002	Enraf
4A	006	Spare
11B	011	Spare
11A	012	Spare
17B	018	MIT
17C	019	MIT
22A	021	Gas Monitoring
23A	022	Spare

Figure 1.
Tank 241-SY-101 Surface Level

Figure 2. Riser 1A (002) Level and 120 Day Level Change

Figure 3. Tank 241-SY-101 Temperature

—♦— MIT 17B 12/31/98 (corrected) —△— MIT 17B 12/31/98 (corrected) —×— MIT 17C 12/31/98 (corrected) —□— MIT 17C 12/31/98 (corrected)

Figure 4. Average Waste Temperature of MIT 17B & 17C

All data values are corrected to the latest validation probe run. Validation probe average temperatures are shown as "X" (17B) and "+" (17C).

Figure 5. 241-SY-101 Gas Chromatograph 3 (GC3) Data for October

Figure 6. 241-SY-101 Gas Chromatograph 3 (GC3) Data for November

Figure 7. 241-SY-101 Gas Chromatograph 3 (GC3) Data for December

**Figure 8. Tank 241-SY-101
Gas Chromatograph 1 (GC1) Hydrogen Data for October 1998**

**Figure 9. Tank 241-SY-101
Gas Chromatograph 1 (GC1) Hydrogen Data for November 1998**

**Figure 10. Tank 241-SY-101
Gas Chromatograph 1 (GC1) Hydrogen Data for December 1998**

**Figure 11. Tank 241-SY-101
FTIR Gas Compositions for October 1998**

**Figure 12. Tank 241-SY-101
FTIR Gas Compositions for November**

Figure 13. Tank 241-SY-101
FTIR Gas Compositions for December

Figure 14. Tank 241-SY-101 Total Gas

Figure 15. Tank 241-SY-101 FTIR Gas Volume Released

June 23, 1993 - December 27, 1998

**Figure 16. Tank 241-SY-101
Gas Concentrations - Weekly Average of**

January 1, 1994 - December 27, 1998

**Figure 17. Tank 241-SY-101
Gas Concentrations - Weekly Average of**

January 1, 1994 - December 27, 1998

**Figure 18. Tank 241-SY-101
Gas Concentrations - Weekly Average of**

January 1, 1994 - December 27, 1998

Figure 19. SY-101 Pressures at Mixer Pump Nozzles

Figure 20. SY-101 Pressures at Mixer Pump Nozzles

Figure 21. SY-101 Mixer Pump Volume Pressure

Figure 22. SY-101 Mixer Pump Voltage, Power, and Speed

Figure 23. SY-101 Mixer Pump Power

Figure 25. SY-101 Mixer Pump Speed

Figure 26. SY-101 Mixer Pump Oil Temperature

Figure 27. Tank 241-SY-101 Mixer Pump Oil Temperature

Figure 28. Tank SY-101 MIT 17B Bottom Thermocouples

Figure 29. Tank SY-101 MIT 17C Bottom Thermocouples

Figure 30. Tank 241-SY-101
Comparison of Validation Probe Runs at MIT

**Figure 31. Tank 241-SY-101
Tank Pressure & Vent. Header Flow Rate**

**Figure 32. Tank 241-SY-101
Vent Header & Atmospheric Relative**

Figure 33. Tank 241-SY-101
Vent Header & Atmospheric Temperatures

DISTRIBUTION SHEET

To	From	Page 1 of 1
Distribution	Process Control	Date 02/12/99
Project Title/Work Order		EDT No. EDT-611451
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