

**ENGINEERING DEVELOPMENT OF COAL-FIRED
HIGH-PERFORMANCE POWER SYSTEMS**

DE-AC22-95PC95143--13

**TECHNICAL PROGRESS REPORT NO. 12
APRIL THROUGH JUNE 1998**

**Prepared for
Department of Energy
Federal Energy Technology Center
Pittsburgh, Pennsylvania**

November 1998

“This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.”

ABSTRACT

A High Performance Power System (HIPPS) is being developed. This system is a coal-fired, combined cycle plant with indirect heating of gas turbine air. Foster Wheeler Development Corporation and a team consisting of Foster Wheeler Energy Corporation, Bechtel Corporation, University of Tennessee Space Institute and Westinghouse Electric Corporation are developing this system. In Phase 1 of the project, a conceptual design of a commercial plant was developed. Technical and economic analyses indicated that the plant would meet the goals of the project which include a 47 percent efficiency (HHV) and a 10 percent lower cost of electricity than an equivalent size PC plant.

The concept uses a pyrolyzation process to convert coal into fuel gas and char. The char is fired in a High Temperature Advanced Furnace (HITAF). The HITAF is a pulverized fuel-fired boiler/air heater where steam is generated and gas turbine air is indirectly heated. The fuel gas generated in the pyrolyzer is then used to heat the gas turbine air further before it enters the gas turbine.

The project is currently in Phase 2, which includes engineering analysis, laboratory testing and pilot plant testing. Research and development is being done on the HIPPS systems that are not commercial or being developed on other projects. Pilot plant testing of the pyrolyzer subsystem and the char combustion subsystem are being done separately, and after each experimental program has been completed, a larger scale pyrolyzer will be tested at the Power Systems Development Facility (PSDF) in Wilsonville, Al. The facility is equipped with a gas turbine and a topping combustor, and as such, will provide an opportunity to evaluate integrated pyrolyzer and turbine operation.

The design of the char burner was completed during this quarter. The burner is designed for arch-firing and has a maximum capacity of 30 MMBtu/hr. This size represents a half scale version of a typical commercial burner. The burner is outfitted with nozzles for separate injection of char, coal, and limestone. Burner performance will be rated according to three criteria, carbon conversion efficiency, NO_x generation, and flame stability. If initial testing in the arch configuration proves successful, further tests will be performed in the wall-fired arrangement.

A complete set of process and instrumentation drawings (P&ID's) were completed for the Combustion and Environmental Test Facility (CETF) this quarter. These drawings established an ISA approved instrument tagging structure, and provided a coherent database for the development of a data acquisition system. The data acquisition system polls tag information (value, range, engineering units, etc.) from the distributed control system (DCS) highway, and provides a platform for data reduction.

The quadropole mass spectrometer, used during the pyrolyzer tests performed at the pilot plant in Livingston, N.J., has been redesigned for use at the CETF. The mass spectrometer is designed to provide on-line gas analysis by identifying all of the chemical components within the secondary air line, the flue gas recycle line, and the furnace exit ducting.

The construction effort at the CETF continued this quarter with the completion of the char storage system, reheat burner, flue gas recycle piping, and the pulverized coal feed system.

TABLE OF CONTENTS

PAGE
NO.

EXECUTIVE SUMMARY	1
INTRODUCTION	2
TECHNICAL PROGRESS	6
Task 1 - Project Planning and Management.....	7
Task 2 - Engineering Research and Development.....	7
Subtask 2.1- Char Combustor Two-Phase Flow Modeling Tests	7
Task 3 - Subsystem Test Unit Design	13
Subtask 3.2 - Char Combustion Subsystem Design.....	13
Task 4 - Subsystem Test Unit Construction	18
Subtask 4.2 - Char Combustion System Test Unit Construction	18
Task 5 - Subsystem Test Unit Testing.....	24
Subtask 5.1 – Char Combustor Test Plan	24
Subtask 5.2 – Char Combustion System Test Unit Testing.....	26

LIST OF FIGURES

<u>FIGURE NO.</u>		<u>PAGE NO.</u>
1	All Coal-Fired HIPPS	3
2	35 Percent Natural Gas HIPPS	5
3	HIPPS Repowering.....	6
4	Two-Phase Flow Model Schematic	8
5	Two-Phase Flow Injector	9
6	Char Burner (Elevation).....	14
7	Tertiary Air Swirler.....	16
8	Mass Spectrometer Process Schematic.....	17
9	Char Silo	19
10	Char Feed System.....	20
11	Reheat Burner	21
12	Flue Gas Recycle	22
13	Pulverized Coal Unloading Station.....	23

LIST OF TABLES

<u>TABLE NO.</u>		<u>PAGE NO.</u>
1	Test Data for Two-Phase HIPPS Model	11, 12
2	Major Variables and Parameters for HIPPS Testing at CETF	25
3	PC Unloading Station Screw Feeder Calibration	26

EXECUTIVE SUMMARY

The High Performance Power System is a coal-fired, combined cycle power generating system that will have an efficiency of greater than 47 percent (HHV) with NO_x and SO_x less than 0.025 Kg/GJ (0.06 lb/MMBtu). This performance is achieved by combining a coal pyrolyzation process with a High Temperature Advanced Furnace (HITAF). The pyrolyzation process consists of a pressurized fluidized bed reactor which is operated at about 926°C (1700°F) at substoichiometric conditions. This process converts the coal into a low-Btu fuel gas and char. These products are then separated.

The char is fired in the HITAF where heat is transferred to the gas turbine compressed air and to the steam cycle. The HITAF is fired at atmospheric pressure with pulverized fuel burners. The combustion air is from the gas turbine exhaust stream. The fuel gas from the pyrolyzation process is fired in a Multi-Annular Swirl Burner (MASB) where it further heats the gas turbine air leaving the HITAF. This type of system results in very high efficiency with coal as the only fuel.

We are currently in Phase 2 of the project. In Phase 1, a conceptual plant design was developed and analyzed both technically and economically. The design was found to meet the project goals. The purpose of the Phase 2 work is to develop the information needed to design a prototype plant that would be built in Phase 3. In addition to engineering analysis and laboratory testing, the subsystems that are not commercial or being developed on other projects will be tested at pilot plant scale. The FWDC Second-Generation PFB pilot plant in Livingston, NJ, has been modified to test the pyrolyzer subsystem. The FWDC Combustion and Environmental Test Facility (CETF) in Dansville, NY, has been modified to test the char combustion system. Integrated operation of a larger scale pyrolyzer and a commercial gas turbine are planned for the PSDF in Wilsonville, AL.

The results of the “cold” two-phase flow tests were used to determine the design of the char combustor for “hot” operation at the CETF. The design of the burner was completed during this quarter, and is outfitted with separate injection nozzles for char, coal, and limestone. The burner is based upon a cyclone design, where the char and the limestone are mixed with hot vitiated air (appx. 800 Deg. F.) to effectively preheat the fuel before firing into the boiler. This preheat concept is employed to promote stable combustion of the char, as its lack of volatile matter makes it a particularly hard to burn fuel. The char burner is also equipped with swirler vanes to impart rotation to the tertiary air. This swirling effect tends to stabilize and control the burner flame front in an effort to increase carbon conversion efficiency and to reduce NO_x generation. A series of nine scanners were installed on the north wall of the boiler to provide a mapping of the burner flame. These scanners are to be calibrated to a fixed source, and will output a 4-20 ma signal to the DCS proportional to the intensity of the flame. These scanners will serve to quantitatively define the stability and shape of the flame.

The construction effort continued during this quarter with the completion of the following items:

1. Flue Gas Recycle Piping
2. Pulverized Coal Feed System
3. Char Storage Feed System
4. Reheat Burner

Installation of the char burner is scheduled for next quarter.

INTRODUCTION

In Phase 1 of the project, a conceptual design of a coal-fired high performance power system was developed, and small scale R&D was done in critical areas of the design. The current Phase of the project includes development through the pilot plant stage, and design of a prototype plant that would be built in Phase 3.

Foster Wheeler Development Corporation (FWDC) is leading a team of companies in this effort. These companies are:

- Foster Wheeler Energy Corporation (FWEC)
- Bechtel Corporation
- University of Tennessee Space Institute (UTSI)
- Westinghouse Electric Corporation

The power generating system being developed in this project will be an improvement over current coal-fired systems. Goals have been identified that relate to the efficiency, emissions, costs and general operation of the system. These goals are:

- Total station efficiency of at least 47 percent on a higher heating value basis.
- Emissions:
 - $\text{NO}_x < 0.06 \text{ lb/MMBtu}$
 - $\text{SO}_x < 0.06 \text{ lb/MMBtu}$
 - Particulates $< 0.003 \text{ lb/MMBtu}$
- All solid wastes must be benign with regard to disposal.
- Over 95 percent of the total heat input is ultimately from coal, with initial systems capable of using coal for at least 65 percent of the heat input.

The base case arrangement of the HIPPS cycle is shown in Figure 1. It is a combined cycle plant. This arrangement is referred to as the All Coal HIPPS because it does not require any other fuels for normal operation. A fluidized bed, air blown pyrolyzer converts coal into fuel gas and char. The char is fired in a high temperature advanced furnace (HITAF) which heats both air for a gas turbine and steam for a steam turbine. The air is heated up to 760°C (1400°F) in the HITAF, and the tube banks for heating the air are constructed of alloy tubes. The fuel gas from the pyrolyzer goes to a topping combustor where it is used to raise the air entering the gas turbine to 1288°C (2350°F). In addition to the HITAF, steam duty is achieved with a heat recovery steam generator (HRSG) in the gas turbine exhaust stream and economizers in the HITAF flue gas exhaust stream.

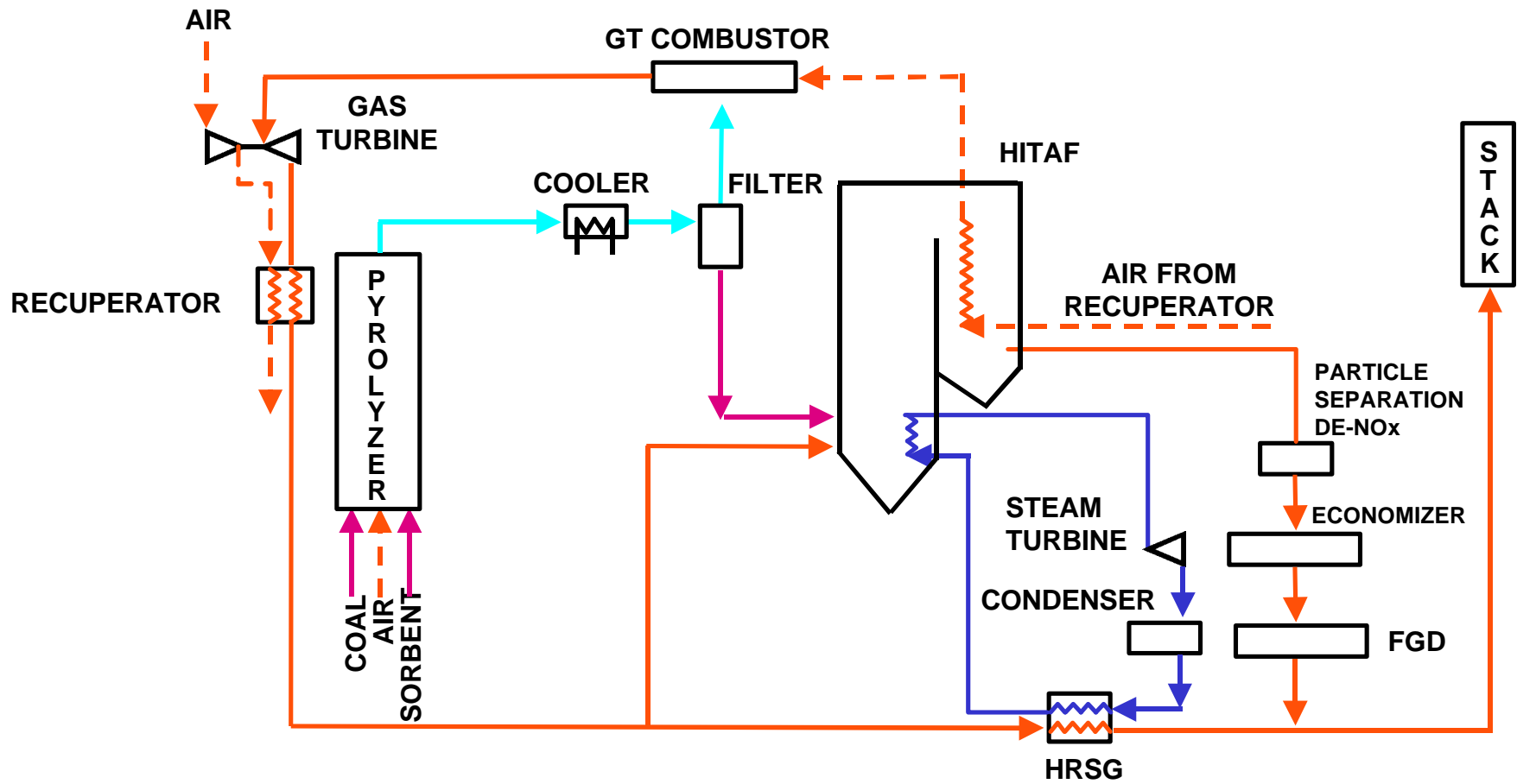


Figure 1 All Coal Fired HIPPS

An alternative HIPPS cycle is shown in Figure 2. This arrangement uses a ceramic air heater to heat the air to temperatures above what can be achieved with alloy tubes. This arrangement is referred to as the 35 percent natural gas HIPPS, and a schematic is shown in Figure 2. A pyrolyzer is used as in the base case HIPPS, but the fuel gas generated is fired upstream of the ceramic air heater instead of in the topping combustor. Gas turbine air is heated to 760°C (1400°F) in alloy tubes the same as in the All Coal HIPPS. This air then goes to the ceramic air heater where it is heated further before going to the topping combustor. The temperature of the air leaving the ceramic air heater will depend on technological developments in that component. An air exit temperature of 982°C (1800° F) will result in 35 percent of the heat input from natural gas.

A simplified version of the HIPPS arrangement can be applied to existing boilers. Figure 3 outlines the potential application of the HIPPS technology for repowering existing pulverized coal fired plants. In the repowering application, the gas turbine exhaust stream provides the oxidant for co-fired combustion of char and coal. The existing boiler and steam turbine infrastructure remain intact. The pyrolyzer, ceramic barrier filter, gas turbine, and gas turbine combustor are integrated with the existing boiler to improve overall plant efficiency and increase generating capacity.

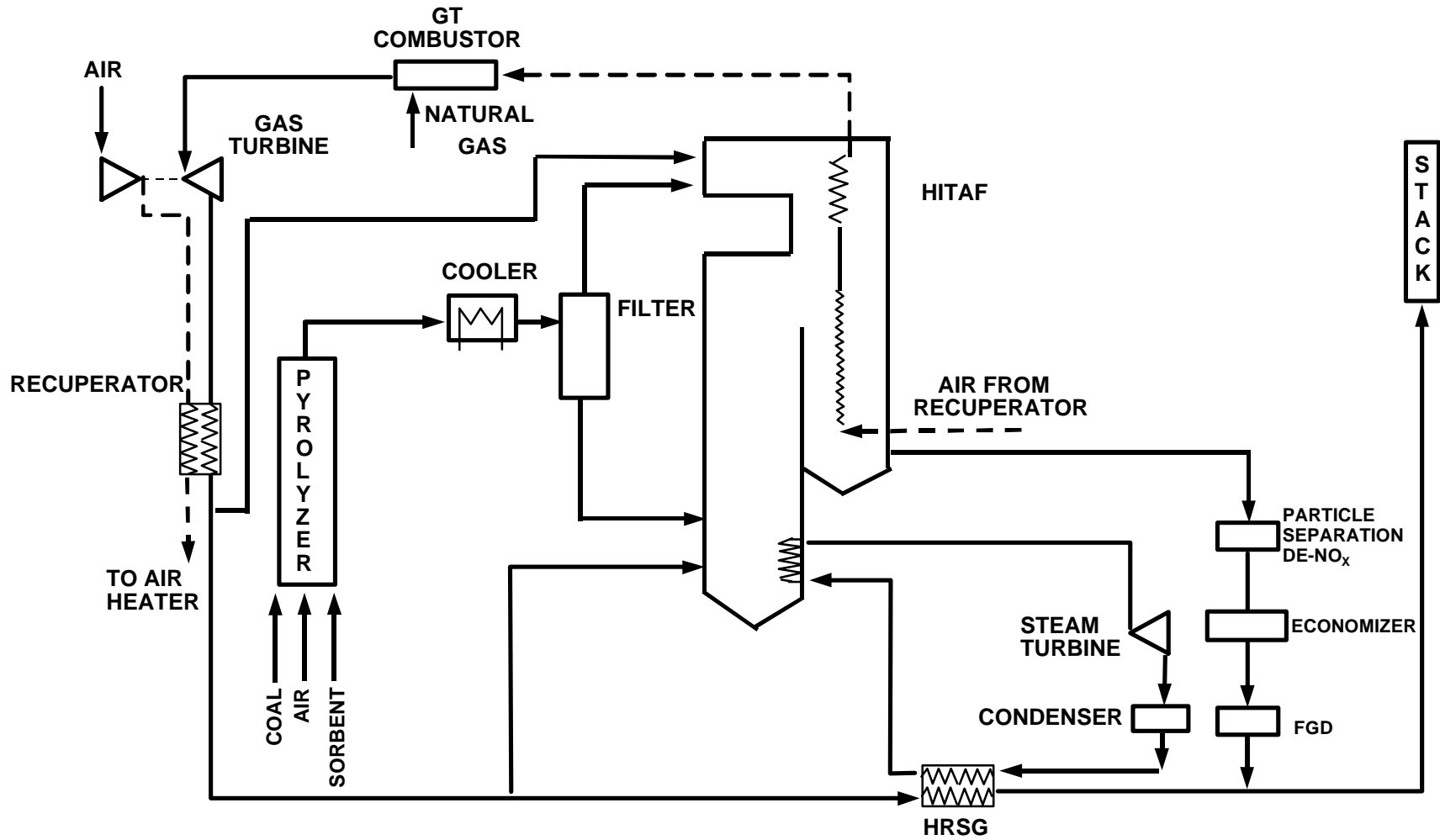


Figure 2 35-Percent Natural Gas HIPP

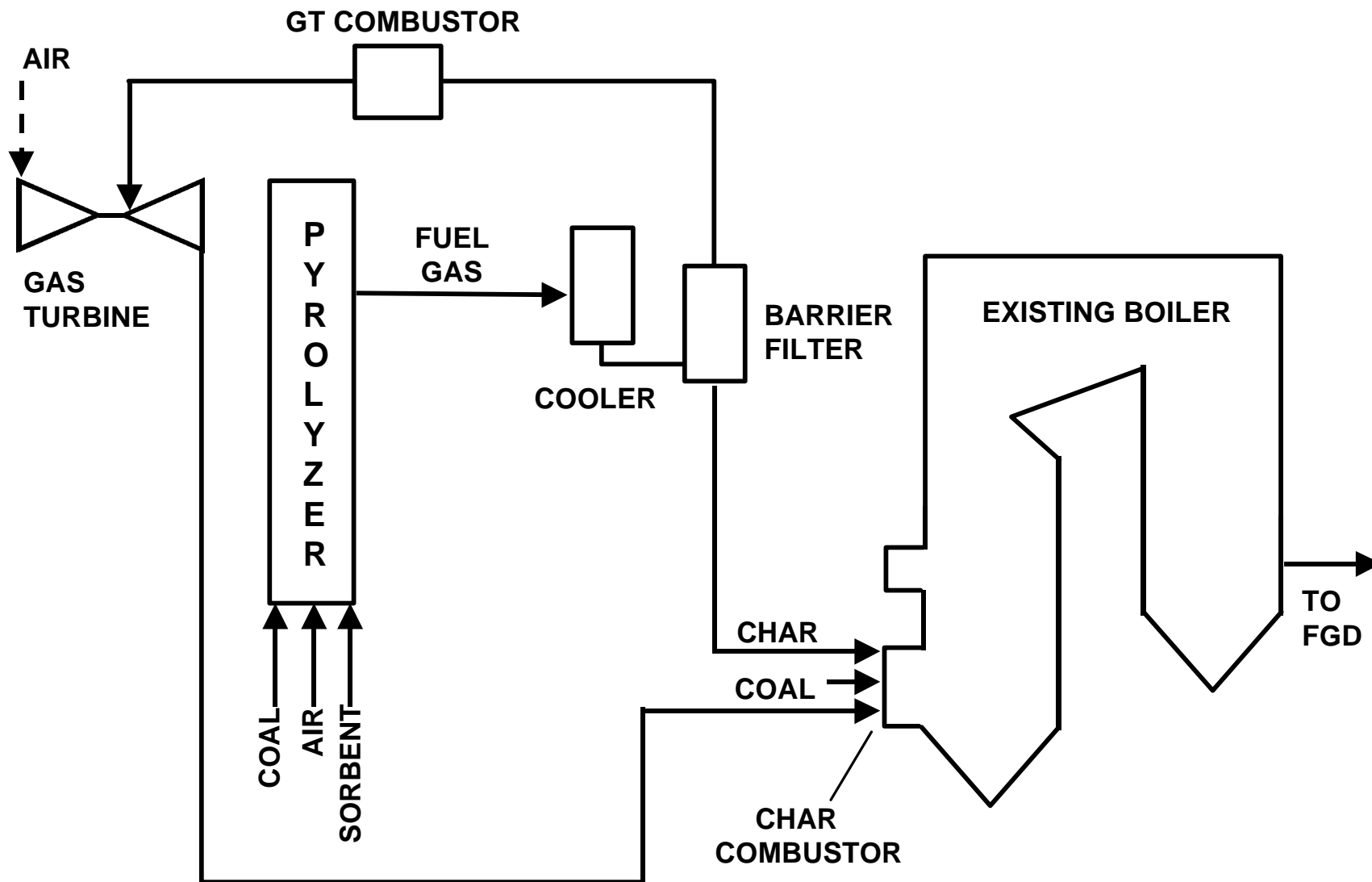


Figure 3 Simplified HIPPS Repowering Process Flow Diagram

TECHNICAL PROGRESS

Task 1 - Project Planning and Management

Work is proceeding in accordance with the Project Plan.

Task 2 – Engineering Research and Development

Subtask 2.1 – Char Combustor Two-Phase Flow Model Test

A HIPPS char combustor will be tested at Foster Wheeler’s Combustion and Environmental Test Facility (CETF). In order to gain an understanding of the fuel injector pressure drop and air-solids mixing characteristics prior to hot combustion testing at CETF, two-phase modeling of a one-half scale HIPPS fuel injector is conducted at the Two-Phase Cold Flow Test Facility in Livingston, NJ.

During this reporting period, the test article was fabricated, the test facility was modified, necessary instruments were installed, and tests were conducted as detailed below.

A schematic of the model layout is shown in Figure 4 and photographs of the arrangement are provided in Figure 5. The injector design required three piping arrangements with one piping arrangement each for the heated primary air, ambient tertiary air, and ambient pumice/carrier air. Two fans were employed to provide the three air streams. Piping from a 7.5 hp fan was divided into two runs, with one flow stream used for the tertiary air and the other stream passing across an electric heater and entering the injector’s tangential inlet. Another 7.5 hp fan was used to provide the required flow and outlet pressure to convey the pumice along the seven feet of vertical run and eleven feet of horizontal run to the injector. A screw feeder below the pumice hopper was used to control the mass flow rate of the pumice. The pumice was then fed into a rotary airlock valve that discharged the solids into the 2 inch sch80 carbon steel carrier air piping.

Instrumentation for the intermediate piping and the injector model included thermocouples, pressure taps, pitot-static tubes, orifice, Dietrich Standard Annubar and Veris Verabar. The tertiary air dynamic pressure was measured with a Dietrich Standard Annubar. This value and the flow rate were recorded on the ROC data acquisition system. The flow rate was confirmed with a pitot-static tube placed within the tertiary air pipe thirteen diameters downstream of a 51% open perforated plate used to straighten the flow. The primary air dynamic pressure was also measured with a Veris Verabar prior to an electric heater. The dynamic pressure and flow rate were recorded onto a LOTUS spreadsheet. The primary air flow rate was also measured with a pitot-static tube at the injector’s tangential inlet. A 51% open perforated plate was placed upstream of the pitot-static tube in order to straighten the flow. The pressure differential across the pumice carrier air orifice was measured with a water-filled manometer (0.1 inch wc resolution) and was used to calculate the mass flow rate. The orifice was located prior to the discharge of solids and had 40 diameters upstream and 17 diameters downstream of straight piping run.

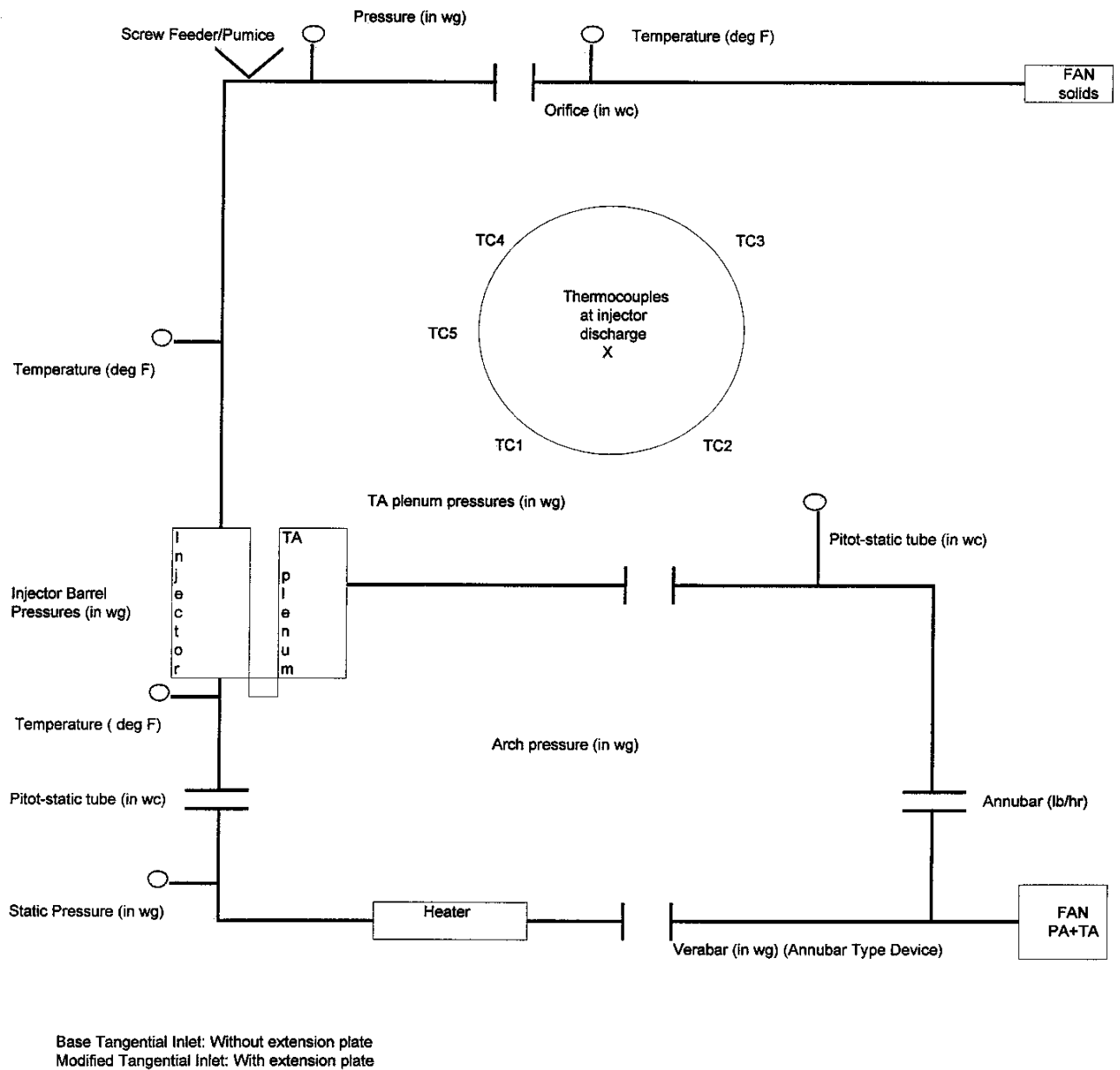


Figure 4 Two-Phase Flow Model Schematic

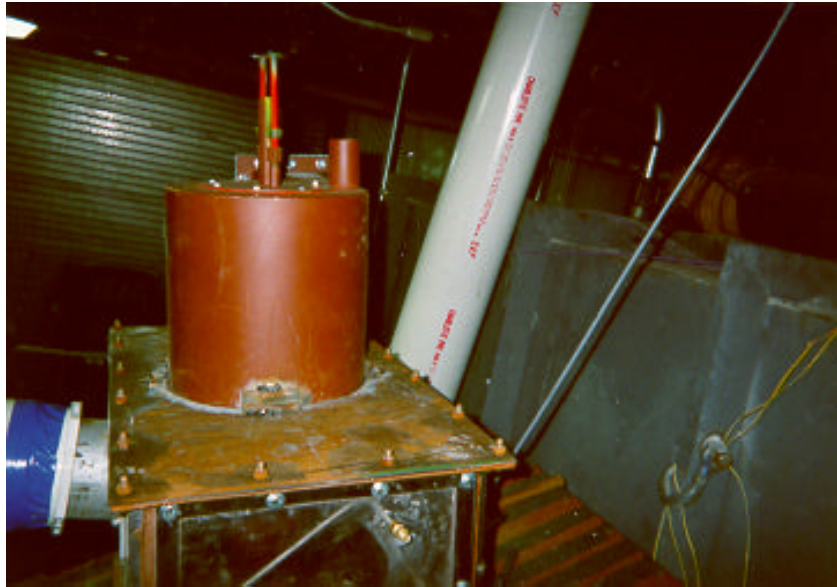
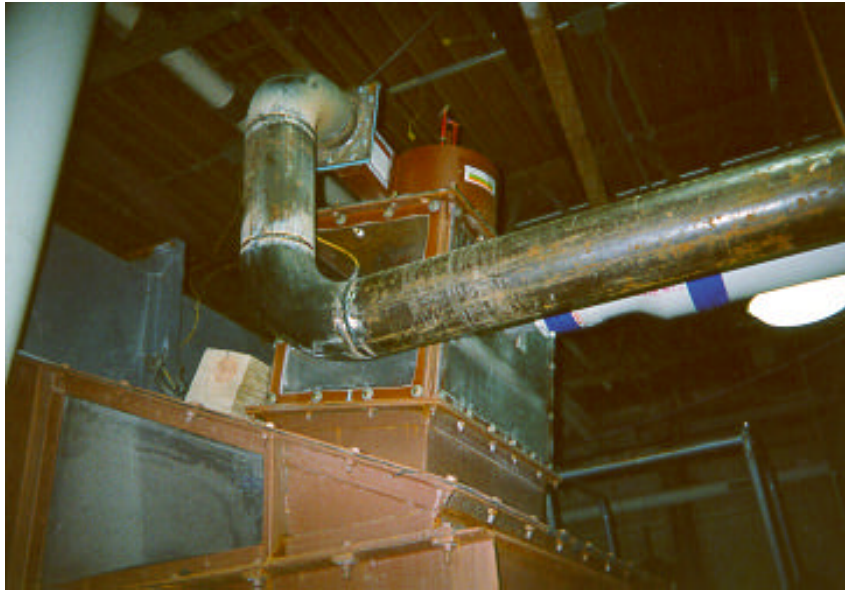


Figure 5 Two-Phase Flow Injector

Pressure taps were placed in various locations in order to obtain accurate density calculations and to observe trends along the system. A pressure tap was included in the primary air line prior to the electric heater. Three pressure taps were placed along the perimeter of the tertiary air plenum which fed into the tertiary air tube. Three pressure taps were also placed circumferentially along the barrel of the injector model ten inches from the barrel top. The pressure taps associated with the tertiary air plenum and injector barrel were put in place in the event that additional data was necessary to make a pressure drop correlation. This was not the case and pitot-static information was sufficient in providing pressure drop data. A pressure tap was also placed prior to the discharge of the pumice into the 2 inch sch80 pipe. Pressure readings were also recorded at the pitot-static tubes. The dynamic pressure and pressure readings from the pitot-static tubes were recorded and averaged using a Solomat Zephyr micromanometer. Pressure tap lines were fed into a Pressure Systems, pressure scanner (Model 9010) that saved the pressure data in an EXCEL format for later review. The pressure scanner had an accuracy of .0015 inch wc.

Omega Type K thermocouples were placed at various locations along the system in order to calculate density and energy balances. Thermocouples were placed at the pumice carrier air fan outlet, inside the pumice hopper, and in the pumice/carrier air stream prior to the inlet to the injector. Five thermocouples were also placed along the periphery of the injector outlet to record the outlet air/pumice mixture temperature discharging into the exhaust chamber. A thermocouple was placed at the injector's tangential inlet to record the heated primary air temperature. The primary air temperature before the electric heater was also measured. The thermocouples were wired to a rotary-switch digital panel meter so that temperature could be more easily recorded. Ambient temperature, pressure, and relative humidity were also recorded for each test.

A test sequence typically included the following steps. The injector's straightening vanes were set to the desired test position. The exhaust ID fan was started followed by the primary air fan and pumice carrier air fan. The tertiary air and primary air flows were set to the desired values. The primary air electric heater was started with a set point between 150 deg F and 200 deg F for heated air tests. Although dependent on ambient conditions, steady-state operation required approximately thirty minutes. Pressure, flow, and temperature data were recorded once steady-state operation was achieved. Most tests included a clean air condition (no solids) followed by solids flow condition. All of the data was recorded on a standard test data sheet. Once the data was collected for the clean air tests, the desired solids flow rate was selected and a K-TRON screw feeder/MAC rotary airlock fed the pumice into the 2 inch sch80 line. The data was then recorded for the solids operation. Pumice mass flow rate was measured by recording the change in the pumice hopper load cell measurements (Sensortronics 65059 TWA) over the test period. Tests continued with different straightening vane settings, primary air flow, and solids flow.

A total of 140 tests were conducted and the major test parameters are presented in Table 1. Test data will be analyzed and the results will be reported in the next report.

Test #	PA Flow (lb/hr)	Pumice (lb/hr)	Solids/PA	PA Density (lbm/ft3)	PA Inlet Velocity (ft/sec)	PA Vel HD (in wc)	PA Static (in wg)	Arch Static (in wc)	PA static - Arch static (in wc)	Inlet Loss Coef.	Vhoutlet	Outlet Loss Coef.	Straightening Vanes	Tangential Inlet
a5-11	1287	0	0	0.074	50.67	0.57	4.40	-0.50	4.90	9.59	2.21	2.47	Inserted	w/o Extension
a5-12	1078	0	0	0.075	42.10	0.40	2.32	-0.47	2.80	8.04	1.71	1.86	Inserted	w/o Extension
a5-12b	1104	0	0	0.062	52.41	0.51	3.31	-0.41	3.71	8.34	1.98	2.13	Inserted	w/o Extension
a5-14	1232	0	0	0.073	49.16	0.53	3.87	-0.56	4.43	9.36	2.08	2.39	Inserted	w/o Extension
a5-15a	1073	0	0	0.065	48.20	0.45	3.16	-0.38	3.54	8.81	1.87	2.13	Inserted	w/o Extension
a5-26b	1206	0	0	0.061	57.72	0.61	4.81	-0.27	5.08	9.35	2.29	2.49	Inserted	w/o Extension
a5-26c	660	0	0	0.060	32.17	0.19	1.03	-0.25	1.28	7.89	1.08	1.36	Inserted	w/o Extension
a5-28a	669	0	0	0.060	32.55	0.19	0.84	-0.52	1.36	8.13	1.09	1.43	Inserted	w/o Extension
a5-28b	816	0	0	0.060	39.57	0.28	1.64	-0.43	2.07	8.33	1.37	1.71	Inserted	w/o Extension
a5-29a	1205	0	0	0.062	57.30	0.60	4.91	-0.38	5.29	9.76	2.23	2.65	Inserted	w/o Extension
a5-29b	1563	0	0	0.062	73.96	1.01	9.37	-0.33	9.70	10.59	3.30	3.25	Inserted	w/o Extension
a5-29f	1002	0	0	0.060	48.67	0.43	2.80	-0.25	3.05	8.16	1.78	1.96	Inserted	w/o Extension
a6-5d	1120	0	0	0.061	56.67	0.59	4.98	-0.34	5.32	10.08	1.99	2.96	Inserted	w/ Extension
a6-5e	819	0	0	0.061	41.85	0.32	3.01	-0.30	3.31	11.46	1.39	2.62	Inserted	w/ Extension
a6-5f	663	0	0	0.060	34.45	0.21	2.12	-0.29	2.41	12.41	1.09	2.40	Inserted	w/ Extension
a6-5g	1207	0	0	0.061	61.18	0.68	5.75	-0.26	6.01	9.81	2.30	2.91	Inserted	w/ Extension
a6-5h	1561	0	0	0.061	79.12	1.14	8.98	-0.23	9.21	9.08	3.32	3.12	Inserted	w/ Extension
a6-5i	1559	0	0	0.061	78.89	1.14	9.01	-0.19	9.20	9.10	3.31	3.12	Inserted	w/ Extension
a6-17a	1536	0	0	0.062	76.72	1.09	8.79	-0.63	9.42	9.66	3.19	3.29	Inserted	w/ Extension
a6-17b	1533	0	0	0.062	76.45	1.08	8.66	-0.53	9.19	9.49	3.19	3.22	Inserted	w/ Extension
a6-17c	1193	0	0	0.061	60.47	0.67	5.58	-0.46	6.03	10.06	2.24	2.99	Inserted	w/ Extension
a6-17d	1095	0	0	0.061	55.50	0.56	4.94	-0.42	5.36	10.55	1.86	3.18	Inserted	w/ Extension
a6-17e	809	0	0	0.060	41.69	0.31	3.06	-0.39	3.45	12.07	1.00	3.77	Inserted	w/ Extension
a6-17f	650	0	0	0.060	33.49	0.20	2.15	-0.37	2.52	13.52	1.06	2.56	Inserted	w/ Extension
a6-24c	757	0	0	0.061	38.12	0.27	2.59	-0.48	3.07	12.54	1.25	2.68	Inserted	w/ Extension
a6-24d	650	0	0	0.061	32.89	0.20	2.06	-0.46	2.52	13.78	1.04	2.61	Inserted	w/ Extension
a6-24e	744	0	0	0.071	32.35	0.22	2.70	-0.45	3.14	15.15	1.13	2.98	Inserted	w/ Extension
a6-24f	860	0	0	0.071	37.45	0.30	2.95	-0.42	3.37	12.32	1.34	2.74	Inserted	w/ Extension
a6-24g	613	0	0	0.071	26.81	0.15	1.68	-0.40	2.08	14.71	0.91	2.44	Inserted	w/ Extension
h6-24a	1093	0	0	0.062	54.42	0.55	4.94	-0.44	5.38	10.79	1.97	3.01	Inserted	w/ Extension
h6-24b	1092	0	0	0.062	54.90	0.55	2.31	-0.44	2.75	5.97	0.89	3.72	Inserted	w/ Extension
a6-26f	1138	0	0	0.071	49.77	0.52	3.75	-0.34	4.09	8.83	1.86	2.48	Inserted	w/ Extension
aa6-26f	1143	0	0	0.070	50.25	0.53	1.55	-0.35	1.90	4.58	0.86	2.84	Inserted	w/ Extension
a6-30b	1164	0	0	0.072	50.05	0.54	3.26	-0.36	3.61	7.71	1.70	2.44	Inserted	w/ Extension
h6-30a	1153	0	0	0.059	60.01	0.64	4.17	-0.37	4.54	8.11	2.16	2.40	Inserted	w/ Extension
a5-15b	1057	0	0	0.065	47.93	0.44	2.46	-0.31	2.77	7.25	1.83	1.76	Retracted	w/o Extension
a5-15c	1195	0	0	0.071	49.02	0.51	3.29	-0.26	3.55	7.92	2.03	2.00	Retracted	w/o Extension
a5-19	1186	0	0	0.061	57.04	0.59	3.48	-0.47	3.95	7.67	2.21	2.06	Retracted	w/o Extension
a5-20	1195	0	0	0.062	56.73	0.59	3.59	-0.36	3.95	7.67	2.24	2.03	Retracted	w/o Extension
a5-22a	667	0	0	0.061	31.92	0.19	0.35	-0.55	0.90	5.82	1.09	0.99	Retracted	w/o Extension
a5-22b	827	0	0	0.061	39.65	0.29	1.16	-0.38	1.55	6.39	1.39	1.32	Retracted	w/o Extension
a5-22c	1207	0	0	0.061	57.77	0.61	3.89	-0.34	4.23	7.94	2.28	2.12	Retracted	w/o Extension
a5-26a	1209	0	0	0.062	57.58	0.61	3.93	-0.30	4.23	7.95	2.28	2.12	Retracted	w/o Extension
a5-29c	1561	0	0	0.062	74.35	1.02	7.06	-0.29	7.35	8.24	3.30	2.53	Retracted	w/o Extension
a5-29d	1201	0	0	0.061	57.86	0.61	4.00	-0.26	4.27	8.02	2.27	2.15	Retracted	w/o Extension
a5-29e	996	0	0	0.060	48.54	0.42	2.23	-0.24	2.47	6.85	1.77	1.64	Retracted	w/o Extension
a6-3a	1211	0	0	0.061	61.68	0.69	4.77	-0.38	5.15	8.47	2.31	2.53	Retracted	w/ Extension
a6-3b	1571	0	0	0.061	79.37	1.15	7.40	-0.31	7.70	7.69	3.35	2.64	Retracted	w/ Extension
a6-3c	1570	0	0	0.061	79.32	1.15	7.35	-0.27	7.62	7.63	3.35	2.62	Retracted	w/ Extension
a6-3d	663	0	0	0.060	34.16	0.21	1.84	-0.25	2.09	11.01	1.09	2.11	Retracted	w/ Extension
a6-5a	667	0	0	0.060	34.37	0.21	1.51	-0.53	2.04	10.64	1.11	2.03	Retracted	w/ Extension
a6-5b	828	0	0	0.061	42.17	0.32	2.47	-0.45	2.92	10.06	1.42	2.29	Retracted	w/ Extension
a6-5c	1122	0	0	0.061	56.96	0.59	4.17	-0.40	4.57	8.74	2.08	2.48	Retracted	w/ Extension
a6-18a	1540	0	0	0.061	78.44	1.12	7.19	-0.61	7.80	7.99	3.31	2.69	Retracted	w/ Extension
a6-18b	1187	0	0	0.061	59.77	0.66	4.34	-0.50	4.84	8.39	2.19	2.51	Retracted	w/ Extension
a6-18c	1095	0	0	0.061	55.41	0.56	3.95	-0.43	4.38	8.83	1.96	2.53	Retracted	w/ Extension
a6-18d	808	0	0	0.061	41.29	0.31	2.46	-0.38	2.85	10.24	1.34	2.35	Retracted	w/ Extension
a6-18e	659	0	0	0.060	33.85	0.21	1.77	-0.36	2.13	11.32	1.05	2.21	Retracted	w/ Extension
a6-18f	1530	0	0	0.061	77.80	1.10	7.28	-0.33	7.61	7.93	3.22	2.71	Retracted	w/ Extension
a6-23a	749	0	0	0.073	31.77	0.22	1.66	-0.65	2.31	11.49	1.13	2.23	Retracted	w/ Extension
a6-23b	868	0	0	0.073	36.86	0.30	2.28	-0.59	2.86	10.69	1.34	2.36	Retracted	w/ Extension
a6-24a	651	0	0	0.065	31.01	0.19	1.50	-0.54	2.04	11.94	1.02	2.18	Retracted	w/ Extension
a6-24b	758	0	0	0.062	37.92	0.27	2.22	-0.50	2.72	11.25	1.25	2.39	Retracted	w/ Extension
a6-26e	1146	0	0	0.071	49.97	0.53	3.11	-0.34	3.45	7.53	1.87	2.13	Retracted	w/ Extension
aa6-26e	1146	0	0	0.070	50.33	0.53	1.17	-0.35	1.52	3.85	0.85	2.41	Retracted	w/ Extension
a6-30a	1165	0	0	0.072	50.10	0.54	2.74	-0.39	3.14	6.82	1.74	2.11	Retracted	w/ Extension
h6-30b	1153	0	0	0.060	59.81	0.64	3.52	-0.37	3.88	7.10	2.15	2.10	Retracted	w/ Extension
a5-29g	999	0	0	0.060	48.45	0.42	2.63	-0.22	2.85	7.74	1.78	1.84	+4.75"	w/o Extension
a6-2a	1107	0	0	0.061	56.20	0.57	4.60	-0.51	5.11	9.90	2.02	2.82	+4.75"	w/ Extension
a6-2b	998	0	0	0.060	51.17	0.47	3.82	-0.41	4.23	9.97	1.77	2.66	+4.75"	w/ Extension
a6-26a	1110	0	0	0.072	47.80	0.49	3.01	-0.46	3.48	8.10	1.79	2.22	+8.75"	w/ Extension
a6-26b	742	0	0	0.071	32.22	0.22	1.29	-0.40	1.69	8.64	1.08	1.76	+8.75"	w/ Extension
a6-26c	741	0	0	0.071	32.27	0.22	1.15	-0.38	1.53	7.95	1.09	1.62	+16.75"	w/ Extension
a6-26d	1106	0	0	0.071	48.16	0.49	2.68	-0.37	3.05	7.19	1.78	1.99	+16.75"	w/ Extension

Table 1 Test Data for Two-Phase HIPPS Model

Test #	PA Flow (lb/hr)	Pumice (lb/hr)	Solids/PA	PA Density (lbm/ft3)	PA Inlet Velocity (ft/sec)	PA Vel HD (in wc)	PA Static (in wg)	Arch Static (in wc)	PA static - Arch static (in wc)	Loss Coef.	Vhoutlet (in wc)	Outlet Loss Coef.	Straightening Vanes	Tangential Inlet
s5-11	1293	1030	0.80	0.074	50.90	0.58	4.36	-0.46	4.81	9.36	1.90	2.84	Inserted	w/o Extension
s5-12	1075	996	0.93	0.075	41.93	0.39	3.18	-0.41	3.60	10.13	1.52	2.63	Inserted	w/o Extension
s5-12b	1110	969	0.87	0.062	52.87	0.51	3.97	-0.36	4.33	9.43	1.63	2.97	Inserted	w/o Extension
s5-14	1230	1080	0.88	0.073	49.29	0.53	3.94	-0.40	4.34	9.18	1.38	3.53	Inserted	w/o Extension
s5-15a	1070	1177	1.10	0.065	48.22	0.45	3.71	-0.31	4.03	9.92	1.55	2.89	Inserted	w/o Extension
s5-26b	1206	1136	0.94	0.061	57.72	0.61	4.72	-0.25	4.97	9.16	1.90	2.94	Inserted	w/o Extension
s5-26c	659	580	0.88	0.060	32.22	0.19	1.51	-0.24	1.75	10.44	0.93	2.09	Inserted	w/o Extension
s5-28a	668	640	0.96	0.060	32.61	0.19	1.32	-0.45	1.76	10.26	0.94	2.08	Inserted	w/o Extension
s5-28b	815	748	0.92	0.061	39.46	0.28	2.19	-0.39	2.58	10.17	1.18	2.42	Inserted	w/o Extension
s5-29a	1204	1132	0.94	0.061	57.53	0.61	4.70	-0.35	5.05	9.34	2.05	2.76	Inserted	w/o Extension
s5-29b	1561	1148	0.74	0.062	74.23	1.01	7.22	-0.31	7.53	8.43	2.87	2.98	Inserted	w/o Extension
s5-29f	1000	975	0.98	0.060	48.49	0.42	3.28	-0.23	3.51	9.29	1.47	2.68	Inserted	w/o Extension
s6-5d	1121	1154	1.03	0.061	56.63	0.59	5.23	-0.31	5.54	10.45	1.71	3.58	Inserted	w/ Extension
s6-5e	818	715	0.87	0.060	41.94	0.32	2.86	-0.28	3.14	10.91	1.20	2.88	Inserted	w/ Extension
s6-5f	663	582	0.88	0.060	34.45	0.21	1.93	-0.27	2.20	11.42	0.95	2.54	Inserted	w/ Extension
s6-5g	1207	1059	0.88	0.061	61.18	0.68	5.99	-0.24	6.22	10.12	1.93	3.58	Inserted	w/ Extension
s6-5h	1560	1325	0.85	0.061	78.68	1.13	9.17	-0.20	9.37	9.27	2.87	3.66	Inserted	w/ Extension
s6-5i	1565	1066	0.68	0.062	78.68	1.14	9.15	-0.18	9.32	9.20	2.89	3.62	Inserted	w/ Extension
s6-17a	1534	1080	0.70	0.062	76.87	1.09	8.76	-0.55	9.31	9.55	2.79	3.73	Inserted	w/ Extension
s6-17b	1529	1360	0.89	0.061	77.50	1.09	8.91	-0.47	9.38	9.57	2.78	3.77	Inserted	w/ Extension
s6-17c	1186	1093	0.92	0.061	59.92	0.66	5.71	-0.43	6.13	10.35	1.88	3.61	Inserted	w/ Extension
s6-17d	1089	1216	1.12	0.061	55.38	0.56	5.06	-0.39	5.45	10.78	1.65	3.64	Inserted	w/ Extension
s6-17e	809	754	0.93	0.060	41.48	0.31	2.90	-0.38	3.27	11.56	1.17	3.06	Inserted	w/ Extension
s6-17f	660	600	0.91	0.060	34.18	0.21	1.96	-0.36	2.32	12.13	0.93	2.72	Inserted	w/ Extension
s6-24c	757	865	1.14	0.061	38.12	0.27	2.47	-0.47	2.94	12.04	1.05	3.05	Inserted	w/ Extension
s6-24d	659	805	1.22	0.061	33.35	0.20	1.82	-0.45	2.27	12.19	0.91	2.72	Inserted	w/ Extension
s6-24e	743	882	1.19	0.071	32.26	0.22	2.22	-0.43	2.65	12.98	0.96	2.99	Inserted	w/ Extension
s6-24f	860	905	1.05	0.071	37.45	0.30	2.91	-0.40	3.31	12.13	1.18	3.06	Inserted	w/ Extension
s6-24g	613	764	1.25	0.071	26.81	0.15	1.54	-0.38	1.93	13.70	0.80	2.60	Inserted	w/ Extension
s6-30b	1164	1076	0.92	0.072	49.91	0.54	3.46	-0.36	3.83	8.13	1.73	2.52	Inserted	w/ Extension
s5-15b	1055	1234	1.17	0.065	47.84	0.44	2.75	-0.25	3.00	7.79	1.52	2.26	Retracted	w/o Extension
s5-15c	1191	1122	0.94	0.071	49.06	0.51	3.15	-0.20	3.36	7.57	1.74	2.22	Retracted	w/o Extension
s5-19	1191	1237	1.04	0.061	57.47	0.60	3.29	-0.38	3.66	7.12	1.88	2.27	Retracted	w/o Extension
s5-20	1194	994	0.83	0.061	56.96	0.59	3.24	-0.30	3.55	6.96	1.94	2.14	Retracted	w/o Extension
s5-22a	665	597	0.90	0.061	32.09	0.19	0.61	-0.40	1.01	6.41	0.99	1.21	Retracted	w/o Extension
s5-22b	827	760	0.92	0.061	39.58	0.29	1.43	-0.36	1.80	7.27	1.21	1.72	Retracted	w/o Extension
s5-22c	1206	1113	0.92	0.061	58.10	0.61	3.51	-0.31	3.82	7.24	1.92	2.31	Retracted	w/o Extension
s5-26a	1208	1132	0.94	0.061	57.91	0.61	3.42	-0.27	3.70	7.04	2.04	2.11	Retracted	w/o Extension
s5-29c	1559	1127	0.72	0.061	74.49	1.02	5.45	-0.27	5.72	6.63	2.87	2.35	Retracted	w/o Extension
s5-29d	1200	1126	0.94	0.061	58.00	0.61	3.45	-0.25	3.70	7.08	1.91	2.26	Retracted	w/o Extension
s5-29e	996	960	0.96	0.060	48.62	0.42	2.47	-0.23	2.70	7.38	1.91	1.64	Retracted	w/o Extension
s6-3a	1210	1101	0.91	0.061	61.84	0.69	4.93	-0.33	5.26	8.61	1.99	2.99	Retracted	w/ Extension
s6-3b	1571	1097	0.70	0.061	79.37	1.15	7.67	-0.29	7.95	7.91	2.93	3.11	Retracted	w/ Extension
s6-3c	1570	1360	0.87	0.061	79.32	1.15	7.83	-0.25	8.08	8.03	2.89	3.19	Retracted	w/ Extension
s6-3d	673	595	0.88	0.060	34.68	0.22	1.56	-0.24	1.80	9.34	0.99	2.03	Retracted	w/ Extension
s6-5a	677	613	0.91	0.060	34.71	0.22	1.29	-0.47	1.76	9.12	0.98	2.02	Retracted	w/ Extension
s6-5b	836	700	0.84	0.061	42.65	0.33	2.23	-0.41	2.64	9.01	1.23	2.41	Retracted	w/ Extension
s6-5c	1119	1163	1.04	0.061	56.72	0.59	4.21	-0.35	4.56	8.78	1.76	2.92	Retracted	w/ Extension
s6-18a	1537	1357	0.88	0.061	78.55	1.11	7.37	-0.52	7.89	8.07	2.81	3.20	Retracted	w/ Extension
s6-18b	1186	1048	0.88	0.062	59.62	0.65	4.46	-0.44	4.90	8.51	1.86	2.99	Retracted	w/ Extension
s6-18c	1096	1162	1.06	0.061	55.55	0.56	4.00	-0.39	4.39	8.82	1.66	2.99	Retracted	w/ Extension
s6-18d	808	730	0.90	0.060	41.36	0.31	2.29	-0.36	2.66	9.61	1.18	2.51	Retracted	w/ Extension
s6-18e	659	600	0.91	0.060	33.79	0.21	1.55	-0.34	1.89	10.20	0.92	2.28	Retracted	w/ Extension
s6-18f	1530	1090	0.71	0.061	77.68	1.10	7.43	-0.30	7.73	8.05	2.82	3.13	Retracted	w/ Extension
s6-23a	749	535	0.71	0.073	31.72	0.22	1.44	-0.60	2.04	10.31	1.03	2.20	Retracted	w/ Extension
s6-23b	866	900	1.04	0.073	36.80	0.29	2.10	-0.54	2.63	9.95	1.17	2.50	Retracted	w/ Extension
s6-24a	662	802	1.21	0.065	31.49	0.19	1.24	-0.51	1.75	10.09	0.91	2.13	Retracted	w/ Extension
s6-24b	749	866	1.16	0.061	37.90	0.26	1.90	-0.49	2.39	10.10	1.07	2.47	Retracted	w/ Extension
s6-30a	1164	1071	0.92	0.072	49.98	0.54	2.89	-0.40	3.29	7.12	1.73	2.21	Retracted	w/ Extension
s5-29g	998	960	0.96	0.060	48.40	0.42	3.10	-0.21	3.31	8.83	1.58	2.36	+4.75"	w/o Extension
s6-2a	1106	1185	1.07	0.061	56.52	0.58	4.86	-0.42	5.28	10.15	1.69	3.47	+4.75"	w/ Extension
s6-2b	996	1153	1.16	0.060	51.15	0.47	4.04	-0.36	4.39	10.34	1.45	3.36	+4.75"	w/ Extension
s6-26a	1104	1043	0.94	0.072	47.74	0.49	3.07	-0.40	3.47	8.14	1.58	2.51	+8.75"	w/ Extension
s6-26b	741	849	1.15	0.071	32.27	0.22	1.25	-0.39	1.63	8.39	0.96	1.93	+8.75"	w/ Extension
s6-26c	740	854	1.15	0.071	32.32	0.22	1.04	-0.37	1.41	7.41	0.96	1.70	+16.75"	w/ Extension
s6-26d	1099	1100	1.00	0.071	47.99	0.49	2.74	-0.35	3.08	7.33	1.56	2.29	+16.75"	w/ Extension

Table 1 Test Data for Two-Phase HIPPS Model (continued)

Task 3 - Subsystem Test Unit Design

Subtask 3.2 - Char Combustion Subsystem Design

Based on the extremely low volatile content of the char the HIPPS burner was to be designed for, an arch fired burner arrangement was chosen. This offers a greater residence time for particle burnout in an effort to reduce unburned carbon in the flyash. Foster Wheeler has vast experience in the design of arch fired burners, and the HIPPS burner was designed using these standards as loose guidelines.

The basic design is that of a cyclone without an outlet nozzle. A vortex tube was included in the design to maintain the effect of keeping the solids at the outer wall. The burner was designed to have char pneumatically transported separate from the burner air and enter via a 2" Schedule 40 pipe from the roof of the burner. A center core pipe carrying bituminous coal was also included in the design. This center stream of fuel will be used to stabilize flame if the char proves to be difficult to burn alone. This center 1-1/2" Sch. 40 pipe extends the entire length of the burner and ends flush with the outlet nozzle tip.

The center pipe was designed as a pipe within a pipe design. Between the two pipes a layer of insulation will be wrapped along with four (4) thermocouples. The intent is to prevent the internal pipe from heating up enough to cause the bituminous coal to stick to the walls. The thermocouples allow operators to monitor the transport pipe wall temperature.

A third stream was included in the CETF HIPPS burner design, also to the roof of the burner, to carry sorbent to the burner via a 1½" Schedule 40 pipe. This stream was designed because the synthetic char to be tested doesn't contain any sorbent, which is present in the char that would be burned coming directly from a pyrolyzer unit. The two streams entering the roof of the burner are located 180° from each other.

Straightening vanes, internal to the burner, were designed to be adjustable along the entire length of the burner. These vanes will be adjusted to see the effect on flame stability by reducing the swirl of the fuel particles. The vanes were designed such that when they are fully retracted they will be located inside the vortex tube, and when fully inserted, located flush with the outlet nozzle tip. Figure 6 shows the burner arrangement. The dimensions of the burner are as follows:

Barrel Diameter	= 23" ID
Barrel Length	= 23"
Hopper Length	= 23"
Outlet Diameter	= 8" ID (8" Schedule 40)
Outlet Nozzle Length	= 18"
Inlet Height	= 11.5"
Inlet Width	= 4.8"
Vortex Diameter	= 8.6" OD (8" Schedule 40)
Vortex Length	= 14.5"

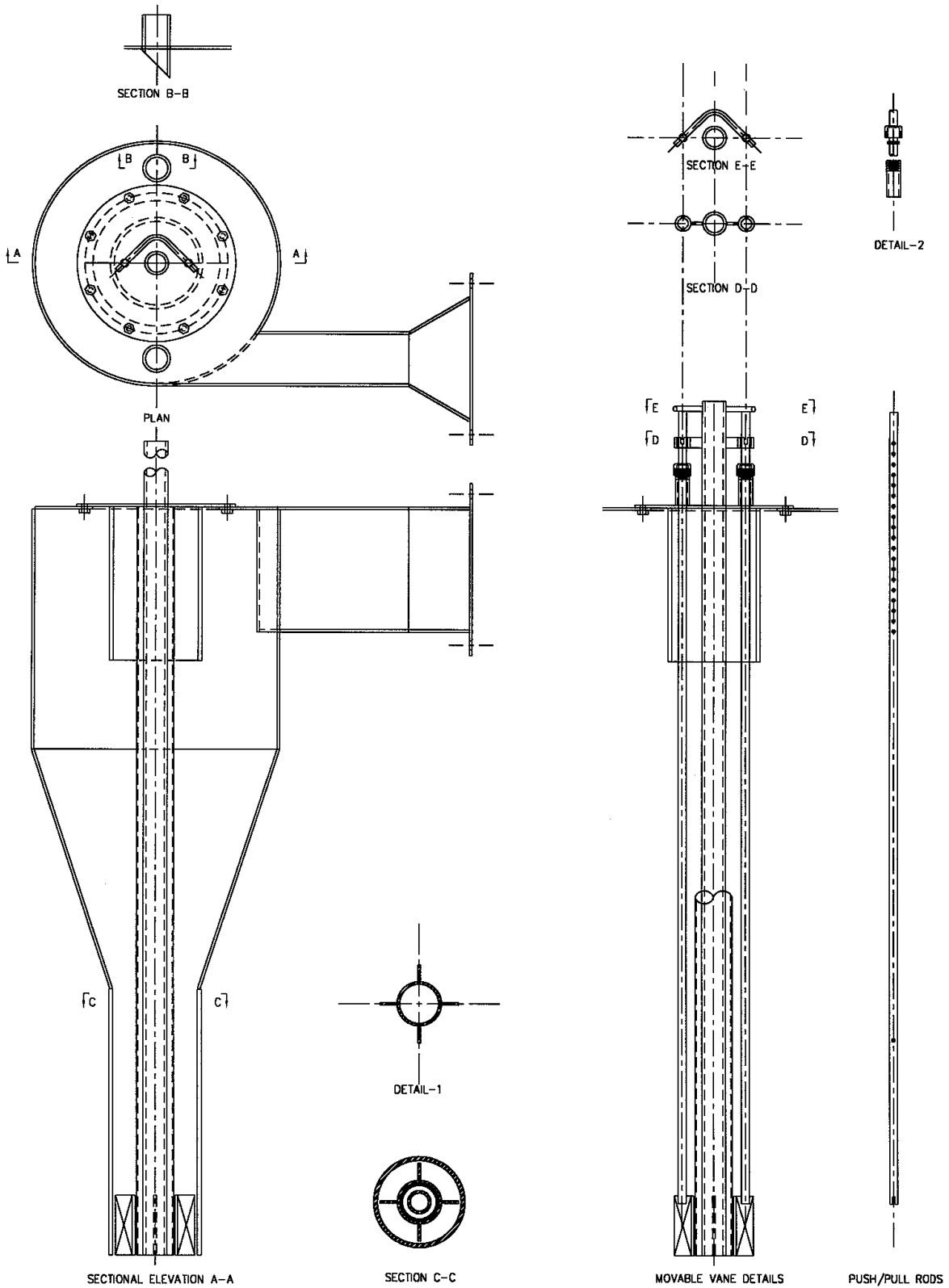


Figure 6 Char Burner (Elevation)

Tertiary air to the burner will be provided from the windbox, and will enter the furnace around the outlet nozzle through a tertiary air can. A tertiary air swirler was designed based on Foster Wheeler experience with horizontal burner registers. The swirler was designed to be 5¾" high with 50° vane angles and a 14.5" OD. The vanes are designed with a ¼" overlap. This design is intended to produce a strong swirl, which will assist in maintaining flame stability with the char. The swirler is removable. Figure 7 shows the design of the tertiary air swirler.

Prior to entering the storage silo, samples of the char are to be taken to monitor any changes in fuel size and/or composition. The first sample will be taken from the outlet of the weighfeeder that feeds the ball mill. An automatic sampling device has been designed to take a sample as the coarse fuel drops off the weighfeeder. The system is pneumatic and will be operated locally by an operator. The sampling cup will make a traverse across the width of the weighbelt to collect the fuel.

When the fuel exits the ball mill a second sample will be taken. This sampling station will be located in the 12" transport pipe between the mill exhauster and the char storage silo. The sample will be taken using an ASME iso-kinetic sampling probe. A similar sampling station to this will be placed at the furnace exit to collect flyash for UBC determination.

Once the flyash sample is taken, the unburned carbon (UBC) will be measured. The UBC measuring system located at the CETF consists of a muffle furnace, capable of variable atmosphere, and an accurate scale. The flyash sample is weighed and placed into the muffle furnace set at 975°C, in an O₂ atmosphere. The O₂ atmosphere is intended to speed up the ashing process. After ashing is complete, the flyash sample is removed and weighed. The weight difference divided by the initial weight is the percent UBC in the flyash. This simple method will give the operators an idea of how the burner is operating and how any changes made to the burner arrangement affect the UBC. Flyash samples will be sent to FWDC's Chemistry Lab for a more accurate analysis of UBC and ash composition.

The sampling system for the mass spectrometer was designed to provide chemical composition identification for three separate streams. A general process schematic is outlined in Figure 8. Sample probes are connected to the vitiated air line into the burner and windbox, the furnace exit, and the inlet line to the stack. The sample lines are heat traced to maintain the sample gas above the water dewpoint prior to entering the instrument. Since the pressure at each one of the sample points is different, the extraction pump will operate at various power levels to maintain constant flow. A primary speed loop is designed into the sampling system to provide sufficient gas flow to maintain a representative "real time" sample at the instrument inlet at all times. The vitiated air line is monitored to determine the oxygen concentration of the mixture of recycle flue gas and incoming air, the furnace exhaust is monitored to aid in determining carbon conversion efficiency, and the stack inlet gas composition is sampled to determine the air heater leak rates. The mass spectrometer is capable of monitoring for O₂, N₂, CO, CO₂, Ar, NO_x, and SO_x simultaneously.

A full set of process and instrumentation drawings were created during this quarter, and are used to define the database of tags for the data archiving system. An Instrument Society of America (ISA) format was used.

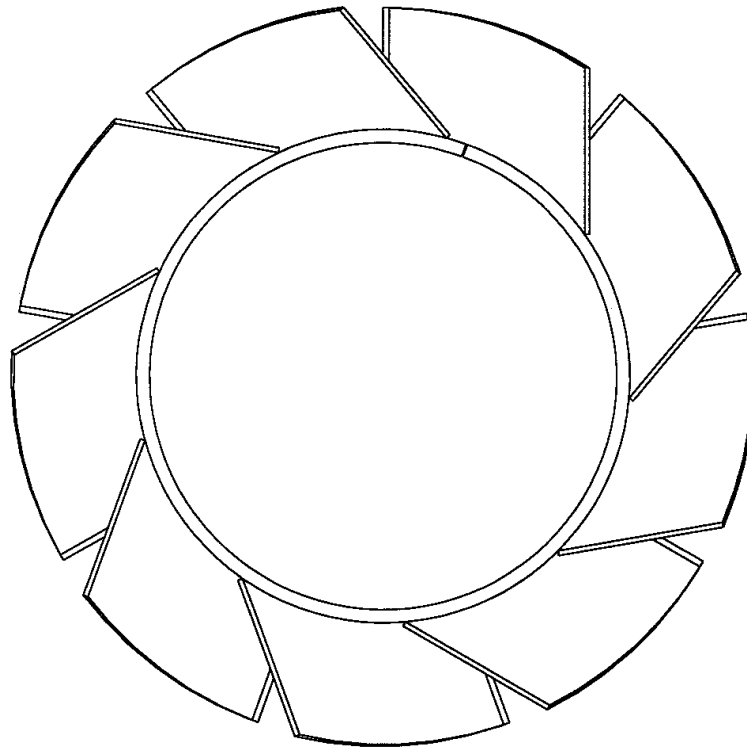
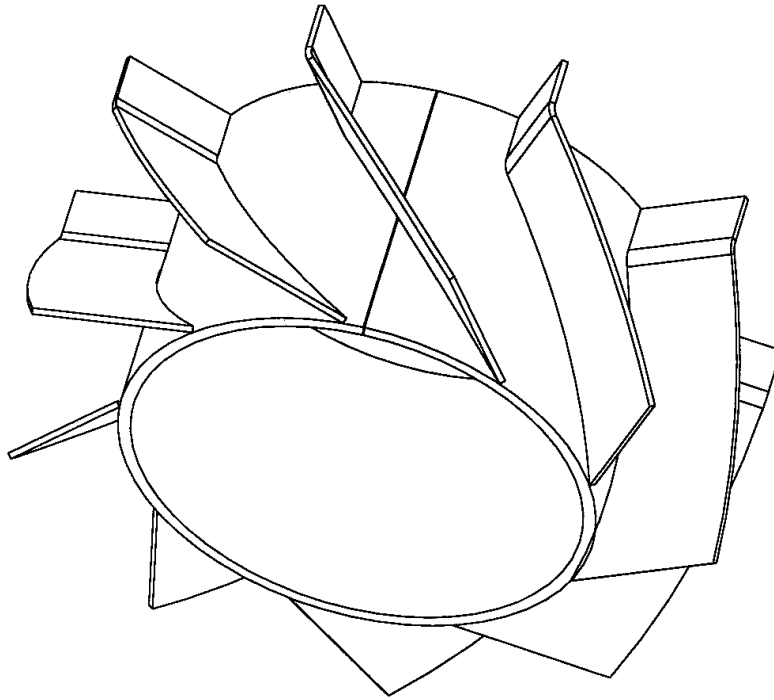


Figure 7 Tertiary Air Swirler

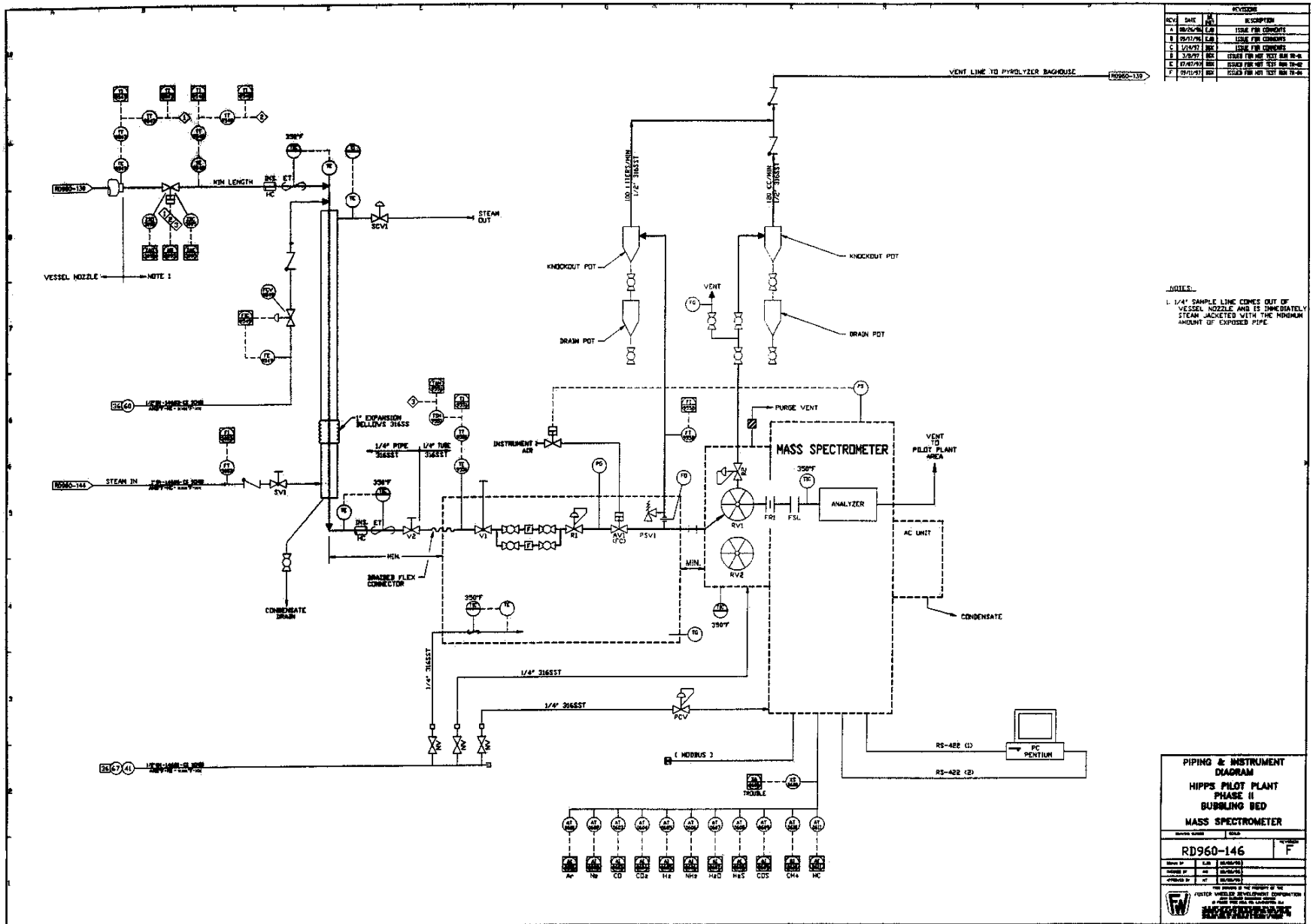


Figure 8 Mass Spectrometer Process Schematic

Task 4 - Subsystem Test Unit Construction

Subtask 4.2 - Char Combustion System Test Unit Construction

The construction effort continued at the CETF during this quarter. The following subsystems were installed:

1. Char Storage System (Figure 9 & 10)
2. Reheat Burner (Figure 11)
3. Flue Gas Recycle Piping (Figure 12)
4. Pulverized Coal Feed System (Figure 13)

The design and operation of these subsystems was described in the previous quarterly report.



Figure 9 Char Storage Silo



Figure 10 Char Feed Hopper Skirt



Figure 11 Reheat Burner



Figure 12 Flue Gas Recycle Piping



Figure 13 Pulverized Coal Unloading System

Task 5 - Subsystem Test Unit Testing

Subtask 5.1 – Char Combustor Test Plan

The fifteen variables, identified in Table 2 have been selected as the important parameters to be investigated during the HIPPS burner test program. Exploration of variables 1 to 8 (which include burner and furnace air flow rates, distribution, and swirl) will allow optimization of the burner and burner operation. are the burner variables. Studying variables 9 to 15 will investigate the boundaries of the “optimum” burner design by varying the HIPPS system parameters such as vitiated air temperature, char fineness, and char flow rate. The major test criteria are combustion stability (determined by both visual observation and flame scanner measurements taken throughout the furnace), NO_x emission, and carbon conversion (analyzed by loss of ignition (LOI) tests of actual bottom ash and flyash samples). The “optimal” burner design will be selected as the combination of burner and furnace flow rates which produce the best combustion and flame stability and the lowest Nox generation.

Table 2 - Major Variables and Parameters for HIPPS Testing at CETF

Variable Name	Units	Ranges/Levels		
		Low	Mid-point	High
1. Vitiated Air O ₂	% wt. wet.	13	15	18
2. Flue Gas Outlet O ₂	% vol. wet.	2.0	3.5	4.5
3. Burner Air Flow Rate	Lbs/hr	2,000	3,430	max
4. Tertiary Air Flow Rate	Lbs/hr	4,400	6,600	max
5. OFA Flow Rate	% Total Flow	0	10	max
6. Air Wall Flow Bias	% (top mid.,bot.)	1 st set 100, 100, 20	2 nd set 50, 50, 30	3 rd set 10, 30, 60
7. Support Fuel Flow Rate	lb/hr	0	258	130
8. Straightening Vanes Location	Relative Position	In	Middle	Out
9. Vitiated Air Temperature	° F		800	maximum
10. Char Fineness	% through 200 mesh	70	80	90
11. Tertiary Air Swirl	Relative Position	No	Yes	
12. Nozzle Length		Short	Long	
13. Sorbent Injection Flow Rate	lb/hr	0	340	maximum
14. Char Flow Rate	Lbs/hr	2,000	2,500	3,000
15. Char Fuel Type	Origin	Pyrolyzer	McLain	

Subtask 5.2 - Char Combustion System Test Unit Testing

The pulverized coal feed system is designed to provide support fuel for the burner. Coal is metered through a screw feeder into a rotary valve. The rotary valve provides a pressure boundary between the pneumatic transport line and the coal supersack, while the screw feeder speed is varied to control coal flow. The screw feeder is not equipped with a load cell, and therefore only the speed, not the coal feedrate, is output to the DCS. The screw feeder was calibrated during this quarter, and the relationship between speed and flow is defined in Table 3.

Table 3. Coal Screw Feeder Calibration

SCREW RPM	LBS COLLECTED	TIME (MIN)	LB/HR
4.5	9.8	20.0	29.4
14.6	18.6	12.0	93.0
23.0	21.6	9.0	144.0
34.6	21.8	6.0	218.0
44.3	19.2	4.0	288.0
56.1	18.2	3.0	364.0
62.6	20.2	3.0	404.0
6.1	10.4	15.0	41.6
19.2	20.2	10.0	121.2
29.4	23.4	7.5	187.2
39.6	17.0	4.0	255.0
48.6	15.8	3.0	316.0
59.7	19.6	3.0	392.0