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Operational Test Report for 241-AN Primary Tank Inlet Air Control Stations

J. A. Tuck

Fluor-Daniel Hanford Co., Richland, WA 99352
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Abstract: This is the operational test report for 241-AN Tank Farm
primary ventilation system inlet air filter and control stations,
following their installation in the field and prior to their acceptance
for beneficial use.

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**OPERATIONAL TEST REPORT FOR 241-AN TANK FARM
INLET AIR CONTROL STATIONS**

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OPERATIONAL TEST REPORT**1.0 INTRODUCTION**

Tank inlet air control and filter stations (see Fig. 1, App. A) were installed to enhance ventilation control capability in the 241-AN tank farm (WHC 1996a). The air control stations are intended to be the primary air flow paths into the waste tanks, providing a new capability for maintaining an easily set and verifiable air flow rate into each waste tank. The air control stations can also be used to maintain tank vacuum at prescribed levels. In addition, each station acts as a filtered, pressure relief for the tank air space. The air control stations are completely system-operated (i.e., no external power sources needed).

The stations were installed on the seven waste tanks in October 1996 and January 1997. Acceptance testing was completed in January 1997 (FDHC 1997). On 28 January 1997 the operational test was performed. The test procedure (Tuck 1996a) consisted primarily of a simple functional test of each station's air flow controller, aerosol testing of each station's high efficiency particulate air (HEPA) filter, and ventilation system balancing (i.e., tank air flows and vacuum level) using the air control stations.

The Test Director for the operational test was Greg Hanson, of East Tank Farms Engineering, Lockheed-Martin Hanford Company (LMHC). The Person-in-Charge (PIC) for the operational test was James T. Ross, of East Tank Farms Operations, Lockheed-Martin Hanford Company (LMHC). The cognizant engineer for the operational test was Jack Thompson of SESC Equipment Engineering. The cognizant engineer for 241-AN Tank Farm, Bob Nicholson of East Tank Farms Engineering, LMHC, was also present. Additional field support during testing was provided by East Tank Farms Operations, Vent and Balance, and Dan Minter (Engineer, Duke Engineering Services Hanford Company). A reprint of the operational test plan (OTP), including the test procedure, is attached as Appendix A of this report. Test data sheets are attached as Appendix B. The Unreviewed Safety Question Screening tracking number for the operational test is TF-96-0084 Rev. 2.

2.0 RESULTS AND DISCUSSION

The air control stations were successfully tested in accordance with the OTP and shown to be ready for service. Actual recorded field data, notes, and observations are presented in Appendix B of this report. The following is a summary of results, arranged by corresponding sections of the OTP.

2.1 INITIAL SYSTEM BALANCING

Pit covers were opened and vapor monitoring was successfully completed, with acceptable measured levels of gas and oxygen. The primary vent valves were opened or verified as open. Tank pressure was monitored directly, during testing, from riser-mounted gauges WST-PI-101 through WST-PI-107. Average tank vacuum level was approximately 2 in. w.g. at the start of testing, and recorded tank vacuum levels ranged from 1.5 to 3.0 in. w.g. during the course of testing (ref. OTP data sheets, Appendix B).

2.2 AIR FLOW CONTROLLER FUNCTIONAL TEST

The air flow controller is "powered" by the air flowing through it. It is set by installing an orifice plate of known performance characteristics. Any variance in set air flow (i.e., caused by a change in tank vacuum or atmospheric pressure changes) will cause an automatic and immediate adjustment to the size of an internal flow area to return flow to the set point. Thus, the flow rate through one air flow controller can be adjusted without affecting the flow through any of the other air flow controllers. This flow control concept, and the capability of actual units, have been previously demonstrated through testing (Tuck 1996b & 1996c). Orifice sizes and their corresponding nominal flow rates are tabulated elsewhere (WHC 1996b).

The air flow controller is equipped with a view port to allow for visual verification that the set flow rate is occurring. Various visual inspections were the essence of the OTP's simple functional test. See the OTP in Appendix A for more details. All six air flow controllers were verified to be functional and operating at the set flow.

2.3 VAPOR MONITORING AND EQUIPMENT BONDING

Equipment bonding and vapor monitoring were performed in accordance with the OTP and facility procedural requirements relative to flammable gas. All bonding assemblies met the specified 1-M Ω resistance criterion. All recorded flammable gas readings were zero (0% LEL).

2.4 AEROSOL PENETRATION TEST

The HEPA filter aerosol test is a standard in-place test used to verify the integrity of the filter media, frame, and seal. The HEPA filters, rated at 500 ft³/min, were tested at 125 ft³/min using an onsite standard maintenance procedure (6-TF-156). The acceptance criteria for this test was that the calculated aerosol penetration, for each of three trials, must be less than 0.05%. The results are tabulated below. All filters passed all test trials.

Tank Number 241-AN-	Test Flow Rate (% of Rated)	% Penetration	% Penetration	% Penetration	Pass or Fail
		Trial 1	Trial 2	Trial 3	
101	25	.002	.002	.002	PASS
102	25	.002	.002	.002	PASS
103	25	.002	.002	.002	PASS
104	25	.002	.002	.002	PASS
105	25	.002	.002	.002	PASS
106	25	.002	.002	.002	PASS
107	25	.002	.002	.002	PASS

2.5 SYSTEM RESTORATION

Prior to installing the air control stations, air entered each waste tank primarily through the pump and valve pit cover blocks; their edges, seams, access plates, and valve handle penetrations. The pump and valve pits contain drain lines or other apertures which are in direct connection with the tank vapor spaces. Maintaining control of the numerous tank air inleakage paths was a problem in itself. With the multi-tank/single-fan arrangement, individual tank air flow control was nearly impossible.

The reduction of tank air inleakage (or any other ventilation system inleakage) plays a key role in maximizing the capabilities of the air control stations (i.e., the ability to control higher air flow rates and/or allow greater tank vacuum levels). Any residual difference between the sum of the nominal tank flow rates and a measured exhaust stack flow rate will depend upon how much other ventilation system or tank inleakage still exists. Drains in the pump and valve pits were identified as possible major sources of tank inleakage and were closed prior to the operational test. No additional sealing efforts were made in the course of running the OTP.

Special gaskets, per ECN 634901 (ref. H-2-71986 & H-2-90172) are available for installation in the valve handle penetrations in the various pit cover blocks to further reduce tank air inleakage.

After the aerosol penetration tests (Sec. 2.4, OTP) were completed, as part of system restoration, ventilation system balancing was achieved by simply installing an orifice plate of known flow performance into each air flow controller, which set each tank to a desired air flow apportionment. The table below shows the orifice sizes and set tank flow rates at the completion of the OTP. The air control stations on the three watchlist tanks (AN-103, -104, and -105) were left on line while the remaining 4 air stations were isolated until additional tank sealing could be accomplished.

Tank Number 241-AN-	Final Orifice Installed	
	Size, in.	Nominal Flow Rate, ft ³ /min
101	2-7/16	60*
102	2-7/16	60*
103	3-3/32	100*
104	3-3/32	100*
105	3-3/32	100*
106	2-7/16	60*
107	2-7/16	60*

* The verifiable, minimum tank ventilation rate (does not include tank inleakage), which is regulated by the set air flow controller as a function of the installed orifice size.

2.6 TEST EXCEPTIONS AND POST TESTING

No test exceptions were found in the course of testing. Data sheets were completed and were reviewed by Quality Assurance at the conclusion of testing.

3.0 CONCLUSIONS

An operational test of the newly installed air control stations in 241-AN Tank Farm was successfully completed, without exceptions. The systems are in service or are ready to be placed in service at the discretion of East Tank Farms Operations.

The air control stations make it possible to balance the ventilation system (i.e., tank flows and vacuum level) and maintain constant minimum tank flows by simply installing an orifice plate of known flow performance into each air flow controller. Orifice plate nominal flow ratings are given on the air flow controller drawing H-2-85647 (WHC 1996b). The set flow rate through one air flow controller can be changed, within system (e.g., fan) limitations, without affecting the flow through any of the other air flow controllers.

Tank vacuum levels can be easily manipulated for work activities (i.e., opening a riser) by temporarily isolating one or more air control stations. Note that all of the tank vacuum levels will be slightly affected by this action. Air flows through other air control stations will not be affected.

The proper operation of each air control station can be quickly and easily verified by performing a simple visual inspection of the air flow controller. This visual inspection and functional check is referenced in Operating Procedure TO-060-101.

Although tank air inleakage was reduced by sealing per Sec. 2.0 of the OTP, some tank inleakage was still apparent at the conclusion of testing and efforts are ongoing to seal remaining inleakage paths. The pump and valve pit cover blocks are possible sources of tank inleakage. Drains in these pits were closed prior to the operational test. Additional tank sealing efforts are continuing.

4.0 RECOMMENDATIONS

Though tank air inleakage has been significantly reduced, other sources of ventilation system or tank inleakage still may yet exist following testing. This inleakage should be verified from stack flow measurements, located, and further reduced to allow full benefit of the air control stations' capabilities.

5.0 REFERENCES

[See Appendix A of this document for additional references.]

FDHC, 1997, *Acceptance Test Report, Inlet Air Filter and Control Station Pressure Decay Test*, WHC-SD-WM-ATR-177 Rev 0, Fluor-Daniel Hanford Company, Richland, Washington

- Tuck, 1996a, *Operational Test Plan for 241-AN Tank Inlet Air Control Stations*, WHC-SD-WM-OTP-215 Rev 1, Westinghouse Hanford Company, Richland, Washington
- Tuck, 1996b, *Test Report, Constant Air Flow Control Device for Tank Farm Ventilation Systems*, WHC-SD-WM-TRP-247 Rev 0-A (incl. original Rev. 0), Westinghouse Hanford Company, Richland, Washington
- Tuck, 1996c, *Acceptance Test Report, Flow Controller and Vacuum Breaker Assemblies*, WHC-SD-WM-ATR-178 Rev 0, Westinghouse Hanford Company, Richland, Washington
- WHC, 1996a, *Air Control Station*, H-2-85646 Rev 0, Westinghouse Hanford Company, Richland, Washington
- WHC, 1996b, *Airflow Controller*, H-2-85647 Rev 0, Westinghouse Hanford Company, Richland, Washington

APPENDIX A: OPERATIONAL TEST PLAN FOR 241-AN TANK FARM INLET AIR CONTROL STATIONS, WHC-SD-WM-OTP-215 (REPRINTED)

1.0 INTRODUCTION

1.1 PURPOSE AND SCOPE

This document is the Operational Test Plan for waste tank inlet air control stations for 241-AN, and includes an Operational Test Procedure (OTP). The inlet air control stations include a Flow Controller Assembly (a passively operated, air flow control device) and a HEPA filter housing.

NOTE, this document IS NOT a plant operating or maintenance procedure. All operator actions are intended to be performed per valid, approved procedures or work control documents, as appropriate, in accordance with the requirements of Tank Farm Transition Projects.

The scope of this OTP will be to verify that the inlet air control stations operate in accordance with the design requirements. Specifically, the following items will be verified on each inlet air control station prior to final acceptance for use in the 241-AN Tank Farm:

- Operation of the Flow Controller Assembly.
- Ability to perform in place aerosol testing of the inlet air control station HEPA filter.

1.2 PERSONNEL AND RESPONSIBILITIES

Person In Charge (PIC)

- Ensures that personnel and equipment are scheduled and materials are obtained as required for this OTP.
- Is responsible for personnel safety during performance of the test.

Test Director

- Is the single person in charge during testing and determines when testing is, or is not, in progress.
- Directs the test personnel and test activities.
- Reviews and approves exceptions to the OTP.
- Witnesses and initials each step of the OTP, or designates a responsible person to do so.

Cognizant Engineer

- Represents TWRS Equipment Engineering.
- Prepares the OTP document and revisions.
- Prepares or assists in preparing exceptions to the OTP.
- Appoints a Test Director.
- Provides technical support as required during the OTP.
- Approves acceptability of test activities and results.
- Prepares the Operational Test Report (OTR) and revisions.

Vent & Balance

- Performs in place aerosol test of HEPA filter.

Quality Assurance

- Quality Assurance reviews data sheets for completeness and legibility (post testing).
- Quality Control verifies electrical bonding if required by procedures, or as requested by Operations or the Cog. Engineer.

Safety Assurance

- Inspects test equipment or facilities, if requested, to resolve safety concerns.

Operations

- Provides support for field preparation and execution of OTP.
- Performs all ventilation system adjustments required by OTP.

Health Physics Technician

- Provides support for field preparation and execution of OTP.
- Performs monitoring as required.

1.3 TEST EQUIPMENT REQUIRED

NOTE

All Measuring and Test Equipment (M&TE) used to perform this work must be within its current calibration cycle as shown on the calibration label.

Testing shall be conducted in 241-AN Tank Farm. No special prerequisites are placed on air temperature and pressure. Required test equipment includes:

- Inlet air control stations installed in 241-AN (ref. H-2-85646)
- Prefilter and HEPA filter installed in filter housings
- Standard pitot tube, as necessary
- Aerosol probe
- Aerosol (DOE-approved)
- Aerosol generator (must produce acceptable aerosol)
- Manometer or similar airflow equipment, as necessary
- Photometer

- Materials for sealing tank air infiltration paths (tape, gaskets, other sealing media, etc.).
- Materials for electrical bonding per Sec. 2.3 of this document.

1.4 PRECAUTIONS AND LIMITATIONS

- 1.4.1 Facility safety rules and Radiation Work Permits (RWP) shall be reviewed before performing this work.
- 1.4.2 Comply with WHC and facility specific lock and tag or overtagging requirements, as applicable.
- 1.4.3 If any waste is generated during performance of this work, consult Facility Hazardous Waste Coordinator for specific instructions to ensure compliance with WHC and DOE environmental standards, as applicable, for disposal.
- 1.4.4 Take special care to ensure contamination control when inserting and withdrawing vent and balance equipment.
- 1.4.5 Only Department of Energy (DOE) approved aerosols shall be used to perform this work (e.g., Emery 3004).
- 1.4.6 Don air purifying respirator fitted with HEPA filters if there is reason to suspect leakage of aerosol into breathing zone of employees.
- 1.4.7 If any of the following conditions are found when performing this work, stop work **immediately**, place equipment in a safe condition, and notify Facility Person In Charge (PIC):
 - Facility equipment malfunction.
 - Personnel error or procedure inadequacy that prevents fulfillment of procedure requirements.
 - Any condition which potentially affects worker health or safety.
- 1.4.8 All work must be done in accordance with OSD-00007 and OSD-00030 as applicable.

1.5 PREREQUISITES

- 1.5.1 Notify Operations Shift Manager before performing this work.
- 1.5.2 Facility PIC shall perform a pre-job safety meeting and Job Hazard Analysis, including all involved personnel, per WHC-CM-1-10, Safety Manual, Standard WKS-6, "Pre-job Safety Planning".
- 1.5.3 Any necessary ventilation pit equipment connections (including bonding) may be made prior to running this OTP to allow for vapor sampling during this OTP (without the need to reenter a

ventilation pit if possible). Monitoring shall be in accordance with OSD-T-151-00007 and OSD-T-151-00030 as applicable.

- 1.5.4 If potential for radiological contamination exists, request HPT perform equipment survey prior to maintenance or removal of equipment from installed location.
- 1.5.5 Verify that the four differential pressure gauges on each inlet air control station (seven stations total, one per tank) are calibrated.
- 1.5.6 Verify that pressure decay test (ref. WHC-SD-WM-ATP-177) has been completed.

1.6 SYSTEM DESCRIPTION

General

Each of the seven 241-AN waste tanks has an inlet air control station connected to a dedicated tank riser. See drawings H-2-71991 through -71996, and H-2-72039, for installation locations.

The inlet air control station is intended to be the primary path through which air can enter the waste tank. The purpose of the inlet air control station is to enhance tank air flow and tank vacuum control capability, and to provide a filtered pathway for air to exit each tank should tank pressure(s) exceed atmospheric pressure (i.e., if active ventilation is lost or during a gas release from the waste).

Figure 1 of this OTP shows the general design and equipment arrangement; see drawing H-2-85646 for equipment design details. Primary components of each inlet air control station include, in order of inward flow, an air flow controller, a test section, a prefilter, a HEPA filter, a flex connection, and a 12-in. isolation butterfly valve (normally open), with interconnecting duct transitions as needed. The inlet air control station connects to the tank riser at the 12-in. isolation valve. A vacuum breaker is connected in parallel with the flow controller to limit tank negative pressure in the event that flow control capability is lost.

An alternate tank air inlet, or filter bypass line, is connected in parallel with each inlet air control station for use during maintenance or in the event that the normal ventilation path becomes obstructed.

Air Flow Controller

The air flow controller (ref. H-2-85647) is an automatic, passively operated device which does not require electrical power or control instrumentation. It has a single moving part (called the Port Controller) which floats inside a stainless steel housing. Air enters the bottom of the housing through a coarse filter. Each air flow controller can be set to control nominal flow rate from 50 cfm to 500 cfm. Air flow rate setting can be easily adjusted in the field. Operation of the flow controller is verified by observing levitation of the Port Controller, which is visible through a view port in the housing.

For each air flow controller to have the maximum possible operating range, ventilation system and tank air inleakage paths must be reduced as much as possible. In addition, ventilation system pressure losses (i.e., from dampers, dirty filters, etc.) must be kept to a minimum.

Vacuum Breaker

The vacuum breaker is an automatic, passively operated device which does not require electrical power or control instrumentation (essentially a weighted damper capable of keeping a constant pressure drop). It is constructed primarily of stainless steel. The vacuum breaker is installed in parallel with the flow controller on each tank inlet, preset to actuate at a differential pressure of 3.3 in. w.g. The vacuum breaker is designed to limit tank negative pressure in the event that air flow through any combination of the seven air flow controllers becomes significantly restricted. If necessary (i.e., due to ice formation), the vacuum breaker relief port may be manually actuated. The vacuum breaker can be easily removed in the field and set to a new actuation point if necessary (ref. H-2-85647).

Test Section

The test section is a section of duct between the air flow controller and the filter housings, and provides the location for an aerosol injection port for the purpose of testing the HEPA filter (ref. H-2-85646-8, also port "A" on Figure 1 of this document).

Filters and Filter Housing

The HEPA filter is 24 x 24 x 5-7/8 in., rated for 500 cfm at 1 in. w.g., and is mounted together with a 24 x 24 x 4 in. prefilter in the manufacturer's standard stainless steel housing (ref. H-2-85646-17, -18, & -19).

Differential Pressure Indicators

There are four differential pressure indicators on each inlet air control station to provide status of filters and flow controller performance. These are labeled VTP-PDI-112 through -115 (see P&ID drawing H-14-020101). Each gauge number has a letter suffix A through G corresponding to tanks 241-AN-101 through 241-AN-107, respectively (e.g., VTP-PDI-112A through -115A for AN-101). Gauges -112, -113, and -114 are mounted on a common rack over the filter housing (ref. H-2-85646-5 & -20). Gauge -115 is mounted on the air flow controller (ref. H-2-85647).

NOTE

The sum of readings from gauges -112, -113, and -114 is approximately equal to corresponding tank negative pressure (for information only).

- VTP-PDI-112A (through -112G): This gauge indicates the differential pressure across the air flow controller (the gauge's high pressure port is open to atmospheric pressure). Normal air flow controller differential pressure readings are from 0.3 in. w.g. to the vacuum breaker set point.

- VTP-PDI-113A (through -113G): This gauge indicates the differential pressure across the pre-filter located inside the HEPA filter housing. Normal prefilter differential pressure readings are from 0 to 1 in. w.g.
- VTP-PDI-114A (through -114G): This gauge indicates the differential pressure across the HEPA filter. Filters are rated for a 1 in. w.g. pressure drop at 500 cfm. Normal HEPA filter differential pressure readings are from 0.1 and 2.0 in. w.g.
- VTP-PDI-115A (through -115G): This gauge indicates the differential pressure across some of the air flow controller's internal components (including its inlet screens and filter media). The gauge's high pressure port is open to atmospheric pressure. Readings from this gauge provide an early indication of screen or filter blockage, flow controller blockage or malfunction. Normal component differential pressure readings are from 0.3 to 1.0 in. w.g.

Filter Bypass Line

A 3-in. bypass line containing an orifice plate and 3-in. ball valve is connected to the tank riser in parallel with the inlet air control station. The orifice is designed to allow controlled air flow into the tank as needed to maintain air flow and tank negative pressure during maintenance or in the event that the normal air path becomes obstructed (ref. H-2-85646-4).

1.7 TEST EXECUTION AND TEST EXCEPTIONS

Testing shall be conducted by the responsible personnel as defined in this OTP. Blank field copies of the test data sheets shall be obtained for the operational test; one set shall be provided for each tank.

The Test Execution Data Sheet has an ACCEPT/REJECT box for each step of the OTP. The test director or designee shall initial and date each step as it is completed. This signifies that the step has been successfully completed according, with the required data recorded in the adjacent data and observations column, including units of measure where applicable, and acceptance criteria (if any) having been met.

The order in which the installations are tested is determined by the Test Director. Record the corresponding tank number on each set of data sheets. In addition, at the direction of the Test Director, steps or subsections within Sec. 2.0 may be performed in an order other than given.

Test exceptions shall be resolved during testing. Each exception and its resolution shall be documented on a copy of the Record of Test Exception sheet provided; one sheet per exception. Exceptions shall also be referenced in the COMMENTS column of Test Execution Data Sheet at the corresponding OTP step.

If an exception requires equipment adjustment or modification, or the Test Director determines continued operation may result in an unsafe situation, the equipment should be shut down and placed in a safe condition, and testing suspended. Testing shall be resumed by the Test Director only after the exception is resolved and documented, at a logical starting point that will provide retesting of the item that initiated the exception or concern.

Test exceptions are normally prepared by the Cognizant Engineer, but may be prepared by the Test Director or others with the technical assistance and approval of the Cognizant Engineer. Exceptions shall be approved by the Test Director and Cognizant Engineer.

This OTP, along with the notated data sheets (including test exceptions), shall be used in compiling a test report, released as a Supporting Document.

2.0 OPERATIONAL TEST PROCEDURE (OTP)

NOTE

At any step of the OTP, the Test Director or designee may request that the exhauster stack flow per procedure 7-GN-056, the on-line exhauster's filter and deentrainer differential pressures, or tank pressure be measured. Record measurement on the data sheets at the current step.

NOTE

Tank sealing efforts (ref. procedure TO-060-101) may continue as necessary throughout the remainder of this OTP, provided tank vacuum levels do not exceed 3.3 in. w.g. If the vacuum level in any tank exceeds 3.3 in. w.g., terminate sealing efforts. Remove sealing material as necessary on untested tanks to keep vacuum level below 3.3 in. w.g., or adjust flow rate on previously tested units by changing flow controller orifice plate.

2.1 INITIAL SYSTEM BALANCING

NOTE

Figure 1 and test data sheets follow Section 3.0. Valve and vent pit numbers are identified on P&ID for 241-AN, drawing H-14-020101.

2.1.1 Open hinged vent pit covers as required (4 total):

VENT PIT-101	≈	TANKS AN-102 & AN-103
VENT PIT-102	≈	TANKS AN-101 & AN-104
VENT PIT-103	≈	TANKS AN-105 & AN-106
VENT PIT-104	≈	TANK AN-107

2.1.2 Monitor for toxic gases, flammable gases and oxygen deficiencies before pit entry. A Confined Space Entry Permit shall be required for all pit entries.

2.1.3 Enter each pit (metal ladders and lights are permanently installed in these pits) and open each 12-in. (upper) primary vent valve or verify valve is open (7 total) as fully as possible in accordance with Sec. 5.2 of procedure TO-060-101.

VENT PIT-101	≈	TANKS AN-102 & AN-103	≈	VALVES V-132 & V-133
VENT PIT-102	≈	TANKS AN-101 & AN-104	≈	VALVES V-131 & V-134
VENT PIT-103	≈	TANKS AN-105 & AN-106	≈	VALVES V-135 & V-136
VENT PIT-104	≈	TANK AN-107	≈	VALVE V-137

- 2.1.4 Record tank pressures (i.e., vacuum levels) on all 7 tanks.
- 2.1.5 If necessary to remove lock & tag from the 12-in. inlet isolation valve (physically labeled VTP-V-154A for tank 241-AN-101 through -154G for tank 241-AN-107), contact the shift manager.

NOTE

At the direction of the Test Director, any one or more of the isolation valves, previously opened on other tanks per Step 2.1.6, may be closed at any time during the OTP as necessary for tank vacuum control, or flow rates on previously tested units adjusted by changing flow controller orifice plates.

- 2.1.6 Open the inlet 12-in. isolation butterfly valve to bring the inlet air control station on line per T0-060-101.
- 2.1.7 If directed by the Test Director, repeat steps 2.1.5 and 2.1.6 for some or all of the remaining tanks, in the order specified by the Test Director.
- 2.1.8 If directed by the Test Director, the orifice plates in any or all of the flow controllers may be changed per T0-060-101 to optimize tank flow rates. If changed, record tank numbers, orifice ID size and corresponding nominal flow rate as given on H-2-85647, and tank pressure after it stabilizes.

2.2 AIR FLOW CONTROLLER TEST

- 2.2.1 Ensure that a 3.5-in. ID orifice plate (corresponds to 125 ft³/min; ref. drawing H-2-85647) is installed in the flow controller, or install one per T0-060-101.

NOTE

The air flow controller (ref. H-2-85647) contains a 3-in. diameter view port, through which the top portion of the device's moving part (a 6-in. diameter cylinder called the Port Controller) may be seen. There is a narrow black ring painted around the top of the cylinder. If the air flow is below the set flow rate or if there is no flow, the Port Controller will be resting down on its stop and only this black ring will be visible. In normal operation (i.e., when the set flow rate is occurring), the Port Controller floats above its resting position and a portion of the unpainted outer surface of the cylinder is visible below the painted ring. Usually, a slight buoyant action can also be observed, indicating that the port controller is not stuck.

- 2.2.2 Verify that the Port Controller is levitated above its resting position (see NOTE above).
- 2.2.3 Perform the following steps, as required, to verify that the Port Controller is not stuck (i.e., due to ice or debris buildup or other damage) or to verify that it travels freely between its current position and its resting position.

2.2.4 Close the inlet air control station's 12-in. isolation butterfly valve (physically labeled VTP-V-154A for tank 241-AN-101 through -154G for tank 241-AN-107) (ref. TO-060-101) while observing that the Port Controller drops freely to its resting position.

2.2.5 Open the 12-in. isolation butterfly valve that was closed in the previous step while observing that the Port Controller raises freely to its initial position.

2.3 VAPOR MONITORING AND EQUIPMENT BONDING

NOTE

OSD's require vapor sampling prior to initiating intrusive work such as contained in this OTP. In addition, OSD-T-151-00030 requires continuous vapor monitoring for the duration of the intrusive work in the case of WATCHLIST TANKS AN-103, AN-104, AN-105, and AN-107. Initial vapor sample for each tank is taken from the ventilation line in the corresponding vent pit, or a Standard Hydrogen Monitoring System (SHMS) reading may be used if available. Subsequent monitoring may be performed at the location of work (i.e., at the inlet air control station).

NOTE

IF the flammable gas concentration is less than or equal to 10% of the lower flammability limit (LFL), then work may continue. Also, IF the flammable gas concentration is less than or equal to 10% of the LFL, AND IF the tank is not on the flammable gas watchlist, the bonding and grounding requirements may be removed from that tank (APPLIES TO NON-WATCHLIST TANKS AN-101, AN-102, & AN-106 ONLY).

NOTE

IF at any time the flammable gas concentration for any tank is GREATER THAN 10% of the LFL, BUT LESS THAN OR EQUAL TO 25% (OSD-00007 & OSD-00030):

- a. STOP WORK.
- b. Notify Shift Operations, Tank Farm Transition Project Engineering, Waste Tank Process Engineering, and Nuclear Safety for evaluation in compliance with the OSD's.
- c. Continue work only upon approval of a written plan describing how to proceed; see OSD-00007 and OSD-00030 for current approval requirements.

NOTE

If at any time the flammable gas concentration is GREATER THAN 25% of the LFL (OSD-00007 & OSD-00030):

- a. STOP WORK.
- b. Notify Shift Operations, Tank Farm Transition Project Engineering, Waste Tank Process Engineering, and Nuclear Safety in compliance with the Flammable Gas Control Limits and other OSD requirements.

- 2.3.1 If a pit entry is required to perform ventilation line vapor monitoring, open hinged ventilation pit cover in preparation for entry.

VENT PIT-101	≈	TANKS AN-102 & AN-103
VENT PIT-102	≈	TANKS AN-101 & AN-104
VENT PIT-103	≈	TANKS AN-105 & AN-106
VENT PIT-104	≈	TANK AN-107

- 2.3.2 If a pit entry is required, monitor for toxic gases, flammable gases and oxygen deficiencies before pit entry. Confined Space Entry Permit shall be required for all pit entries.

- 2.3.3 As required by OSD-T-151-00007 or OSD-T-151-00030, bond the inlet air control station test port plugs or caps, vapor sample tubes, and any test equipment required to support the OTP. Bond per drawing H-2-73450, Rev. 4, Sht. 3, Note 10, Assembly E; verify bonding assembly passes required one megohm (1 MΩ) resistance check after installation.

- 2.3.4 Monitor vapor (i.e., sample from the ventilation line located in the ventilation pit or use an available SHMS reading, corresponding to the tank being tested) for baseline reading for flammable gases. Continuous monitoring (i.e., at ≤ 15-minute intervals) is required for AN-103, AN-104, AN-105, and AN-107 (WATCHLIST TANKS). Record flammable gas concentrations.

- 2.3.5 Remove required test port cover plugs and wait 5 minutes before performing the next step.

- 2.3.6 Monitor vapor at the inlet air control station, or use a reading from the ventilation pit or SHMS if available, corresponding to the tank being tested, after obtaining a baseline reading for flammable gases. Continuous monitoring (i.e., at ≤ 15 minute intervals) is required for AN-103, AN-104, AN-105, or AN-107 (WATCHLIST TANKS). Record flammable gas concentration.

2.4 AEROSOL PENETRATION TEST

NOTE

Visual inspection identifies potential ventilation system problems or conditions which may affect test activities. No pass/fail inspection criteria are used. The following list may be used as a guide for items to be inspected for adequacy, deficiency, or other concerns:

- Filter housing access
- Damage to instrumentation
- Test port access
- Labels on pressure gauges
- Light level in work area
- Damage to filter housing or ductwork
- Damage to housing door or seal
- Labels on test ports
- Current calibration labels
- General housekeeping & tripping hazards

2.4.1 Perform visual inspection of equipment and work area, and perform aerosol penetration test per procedure 6-TF-156 (including Appendix TV thereof).

2.5 RESTORATION

- 2.5.1 Verify aerosol test equipment has been removed and test port plugs or caps are restored.
- 2.5.2 If directed by the Test Director, perform flow adjustments (ref. TO-060-101). If any orifice plates have been changed, record final installed ID size and corresponding nominal flow rate; ref. drawing H-2-85647.
- 2.5.3 If no more tests are to be immediately performed, but there are still remaining filters to be tested, then close and perform lock and tag on valves opened in Step 2.1.6 which correspond to units not yet tested.

2.6 POST TESTING

- 2.6.1 Test Director to review data sheets for completeness and legibility.
- 2.6.2 Quality Assurance (QA) to review Data Sheets for completeness and legibility. This can be done after completion of all testing.
- 2.6.3 Subsequent operational tests will start at Step 2.1.6, with a new set of test data sheets.
- 2.6.4 Survey all equipment before removal from work area, as required.

3.0 BIBLIOGRAPHY

ACGIH, *Industrial Ventilation*, Section 9, "Testing of Ventilation Systems."

ASME N510-1989, *Testing of Nuclear Air Treatment Systems.*

Drawing H-2-71991, *Piping Plan Tank 101.*

Drawing H-2-71992, *Piping Plan Tank 102.*

Drawing H-2-71993, *Piping Plan Tank 103.*

Drawing H-2-71994, *Piping Plan Tank 104.*

Drawing H-2-71995, *Piping Plan Tank 105.*

Drawing H-2-71996, *Piping Plan Tank 106.*

Drawing H-2-72039, *Piping Plan Tank 107.*

Drawing H-2-73450, *Piping Isolation Details Pipe & Riser Closures.*

Drawing H-2-85646, *Air Control Station.*

Drawing H-2-85647, *Airflow Controller.*

Drawing H-14-020101, *Ventilation Tank Primary System (VTP) O & M System P&ID.*

ERDA 76-21, *Nuclear Air Cleaning Handbook.*

OSD-T-151-00007, *Operating Specifications for the 241-AN, AP, AW, AY, AZ, and SY Tank Farms.*

OSD-T-151-00030, *Operating Specifications Watch List Tanks.*

Procedure 7-GN-056, *Airflow Capacity and Distribution Tests.*

Procedure TO-060-101, *Operate 241-AN Primary and Annulus Vent Systems.*

Procedure 6-TF-156, *HEPA Filter In-Place Leak Test (Aerosol Test), including Appendix TV, 241-AN Tank Inlet Filter Aerosol Test Data Sheets.*

WHC-CM-1-10, *Safety Manual*, Standard WKS-6, "Pre-Job Safety Planning," Standard WKS-21, "Ladders," Standard WKS-8.1, "Operations Lock and Tag Program," Standard WKS-22, "Scaffolding," Standard WKS-10, "Personal Protection," and Standard WKS-12, "Hand and Portable Power Tools."

WHC-CM-6-1, *Standard Engineering Practices*, EP-4.2, "Testing Requirements."

WHC-CM-7-5, *Environmental Compliance Manual*, Section 2.5.5.2, "Testing and Performance Criteria."

WHC-SD-WM-ATP-177, *Acceptance Test Procedure, Air Inlet Filter and Control Station Pressure Decay Test.*

WHC-SD-WM-HSP-002, *Tank Farm Health and Safety Plan (HASP).*

TEST	PORT	HEPA FILTER VTP-FLT 101B THRU 107B
BASELINE	INJECT	A
	SAMPLE	B
PENETRATION	INJECT	A
	SAMPLE	C

FIGURE 1. INLET FILTER TEST PORTS (TYPICAL).

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TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.1.1 - 2.1.4		
2.1.5 - 2.1.8		
2.2.1 - 2.2.5		
2.3.1 & 2.3.2		
2.3.3		
2.3.4		ELECTRICAL RESISTANCE IN Q: CALIBRATION DUE DATE: LESS THAN ONE MEGOHM (1 MQ)?: Q.C. SIGNATURE & DATE:

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6		
2.4.1		
2.5.1 - 2.5.3		
2.6.1 - 2.6.4		

* ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Test Execution Data Sheet reviewed By:

(Cognizant Engineer, printed name, signature, & date)

(Quality Assurance, printed name, signature, & date)

RECORD OF TEST EXCEPTION

TANK NUMBER: 241-AN-

TEST EXCEPTION NUMBER:

EXCEPTION		
DATE:	REFERENCE OTP STEP NUMBER:	
DESCRIPTION OF PROBLEM:		
ACTION TAKEN:		
RESOLUTION		
<u>RESPONSIBILITY/ORGANIZATION</u>	SIGNATURE:	DATE:
TEST DIRECTOR:		
COGNIZANT ENGINEER:		
OTHER:		

Record of Test Exception reviewed By:

(Quality Assurance, printed name, signature, & date)

[MAKE ADDITIONAL COPIES AS REQUIRED; ONE EXCEPTION PER SHEET]

APPENDIX B: TEST DATA SHEETS AND PARTICIPANTS LIST

ST 2/11/98

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-101

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
		#6
2.1.1 - 2.1.4	DJM 1-28-97	Note: dP gages have been calibrated (1.5.5) and pressure decay test has been completed (1.5.6), Vent pit cover open, Pit monitoring complete - measured gas and O ₂ levels are acceptable, Vent valve(s) open, Tank Vacuum, AN-101-107 (IN WG): 1.5, 1.8, 1.6, 1.8, 2.0, 1.7, 2.2
2.1.5 - 2.1.8	DJM 1-28-97	Lock and tag removed, Station isolation valve open, N/A for 2.1.7 and 2.1.8 (other stations will be brought on-line as tested)
2.2.1 - 2.2.5	DJM 1-28-97	125 scfm orifice plate installed per WHC-SD-WM-ATR-178 (verified again if changed out per step 2.5.2), Port controller is levitated, and drops and raises freely, Flow controller PASSES simple/final functional test
2.3.1 & 2.3.2	DJM 1-28-97	Pit entry for monitoring is not required
2.3.3	DJM 1-28-97	Bonding of applicable plugs/instruments complete, Resistance check verified < 1 MΩ
2.3.4	DJM 1-28-97	ELECTRICAL RESISTANCE IN Ω: N/A CALIBRATION DUE DATE: N/A LESS THAN ONE MEGOHM (1 MΩ): N/A O.C. SIGNATURE & DATE: N/A Flammable gas concentration: 0% LEL Location: Dome

ST 2/11/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-101

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6	DJM 1-28-97	Plugs removed for 5 minutes, Flammable gas concentration: 0% LEL Location: Dome
2.4.1	DJM 1-28-97	Filter PASSES aerosol testing, see attached Vent + Balance test data sheets
2.5.1 - 2.5.3	DJM 1-28-97	Equipment restored, Final installed orifice size (inches): 2-7/16 (60 cfm)
2.6.1 - 2.6.4	DJM 1-28-97	Data sheets are complete and ready for QA review

* ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Robert S. Nicholson

Test Execution Data Sheet reviewed By:

Robert S. Nicholson 1-28-97
(Cognizant Engineer, printed name, signature, & date)

W. Adams 1/29/97
(Quality Assurance, printed name, signature, & date)

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-102

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
		# 7
2.1.1 - 2.1.4	DJM 1-28-97	Note: dP gages have been calibrated (1.5.5) and pressure decay test has been completed (1.5.6), Vent pit cover open, Pit monitoring complete - measured gas and O ₂ levels are acceptable, Vent valve(s) open, Tank vacuum, AN-101-107 (IN WG): 2.4, 2.7, 2.8, 2.7, 2.9, 2.5, 3.0
2.1.5 - 2.1.8	DJM 1-28-97	Lock and tag removed, Station isolation valve open, N/A for 2.1.7 and 2.1.8 (other stations will be brought on-line as tested)
2.2.1 - 2.2.5	DJM 1-28-97	125 scfm orifice plate installed per WHC-SD-WM-ATR-178 (verified again if changed out per step 2.5.2), Port controller is levitated, and drops and raises freely, Flow controller PASSES simple/final functional test
2.3.1 & 2.3.2	DJM 1-28-97	Pit entry for monitoring is not required
2.3.3	DJM 1-28-97	Bonding of applicable plugs/instruments complete, Resistance check verified < 1 MΩ
2.3.4	DJM 1-28-97	ELECTRICAL RESISTANCE IN Ω: N/A LESS THAN ONE MEGOHM (1 MΩ): N/A FLAMMABLE GAS CONCENTRATION: 0% LEL LOCATION: Dome CALIBRATION DUE DATE: N/A O.C. SIGNATURE & DATE: N/A

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-102

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6	DJM 1-28-97	Plugs removed for 5 minutes, Flammable gas concentration: 0% LEL Location: Dome
2.4.1	DJM 1-28-97	Filter PASSES aerosol testing, see attached Vent + Balance test data sheets
2.5.1 - 2.5.3	DJM 1-28-97	Equipment restored, Final installed orifice size (inches): 2-7/16 (60 cfm)
2.6.1 - 2.6.4	DJM 1-28-97	Data sheets are complete and ready for QA review

* ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Robert S. Nicholson *Robert Nicholson*
(Cognizant Engineer, printed name, signature, & date) 1-28-97

Test Execution Data Sheet reviewed By:

W. Adams *W. Adams* 1/29/97
(Quality Assurance, printed name, signature, & date)

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-103

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
		#3
2.1.1 - 2.1.4	DJM 1-28-97	Note: dP gages have been calibrated (1.5.5) and pressure decay test has been completed (1.5.6), Vent pit cover open, Pit monitoring complete - measured gas and O ₂ levels are acceptable, Vent valve(s) open, Tank vacuum, AN-101-107 (IN WG): NR, 2.0, 1.8, 2.0, 2.3, 2.0, 2.5
2.1.5 - 2.1.8	DJM 1-28-97	Lock and tag removed, -1.5 IN WG Station isolation valve open, N/A for 2.1.7 and 2.1.8 (other stations will be brought on-line as tested)
2.2.1 - 2.2.5	DJM 1-28-97	125 scfm orifice plate installed per WHC-SD-WM-ATR-178 (verified again if changed out per step 2.5.2), Port controller is levitated, and drops and raises freely, Flow controller PASSES simple/final functional test
2.3.1 & 2.3.2	DJM 1-28-97	Pit entry for monitoring is not required
2.3.3	DJM 1-28-97	Bonding of applicable plugs/instruments complete, Resistance check verified < 1 MΩ
2.3.4	DJM 1-28-97	ELECTRICAL RESISTANCE IN IN: N/A CALIBRATION DUE DATE: N/A LESS THAN ONE MEGOHM (< 1 MΩ): N/A E.C. SIGNATURE & DATE: N/A Flammable gas concentration: 0% LEL Location: Dome

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-103

HNF-SD-WM-OTR-215 Rev. 1
5/21/97

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6	DSM 1-28-97	Plugs removed for 5 minutes, Flammable gas concentration: 00% LEL Location: Dome
2.4.1	DSM 1-28-97	Filter PASSES aerosol testing, see attached Vent + Balance test data sheets
2.5.1 - 2.5.3	DSM 1-28-97	Equipment restored, Final installed orifice size (inches): 3-3/32 (100 cfm)
2.6.1 - 2.6.4	DSM 1-28-97	Data sheets are complete and ready for QA review

* ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Test Execution Data Sheet reviewed By:

Robert S. Nicholson
(Cognizant Engineer, printed name, signature, & date)Robert S. Nicholson
1-28-97W.L. Adams
(Quality Assurance, printed name, signature, & date)W.L. Adams
1/29/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-104

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
		#2
2.1.1 - 2.1.4	DJM 1-28-97	Note: dP gages have been calibrated (1.5.5) and pressure decay test has been completed (1.5.6), Vent pit cover open. Pit monitoring complete - measured gas and O ₂ levels are acceptable, Vent valve(s) open, Tank vacuum, AN-101-107 (IN WG): NR, 2.0, 1.6, 2.0, 2.0, 1.8, 2.4
2.1.5 - 2.1.8	DJM 1-28-97	Lock and tag removed, -1.8"wg Station isolation valve open, N/A for 2.1.7 and 2.1.8 (other stations will be brought on-line as tested)
2.2.1 - 2.2.5	DJM 1-28-97	125 scfm orifice plate installed per WHC-SD-WM-ATR-178 (verified again if changed out per step 2.5.2), Port controller is levitated, and drops and raises freely, Flow controller PASSES simple/final functional test
2.3.1 & 2.3.2	DJM 1-28-97	Pit entry for monitoring is not required
2.3.3	DJM 1-28-97	Bonding of applicable plugs/instruments complete, Resistance check verified < 1 MΩ
2.3.4	DJM 1-28-97	ELECTRICAL RESISTANCE IN R: N/A CALIBRATION DUE DATE: N/A LESS THAN ONE MEGOHM (1 MΩ): N/A G.C. SIGNATURE & DATE: N/A Flammable gas concentration: 0% LEL Location: Dome

JT 2/11/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN- 104

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6	DSM 1-28-97	Plugs removed for 5 minutes, Flammable gas concentration: 0% LEL Location: Dome
2.4.1	DSM 1-28-97	Filter PASSES aerosol testing, see attached Vent + Balance test data sheets
2.5.1 - 2.5.3	DSM 1-28-97	Equipment restored, Final installed orifice size (inches): 3-3/32 (100 cfm)
2.6.1 - 2.6.4	DSM 1-28-97	Data sheets are complete and ready for QA review

*

ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Robert Nicholson Robert Nicholson 1-28-97
(Cognizant Engineer, printed name, signature, & date)

Test Execution Data Sheet reviewed By:

Wk Adams Wk Adams 1/29/97
(Quality Assurance, printed name, signature, & date)

ST 2/11/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-105

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
		#1
2.1.1 - 2.1.4	DJM 1-28-97	Note: dP gages have been calibrated (1.5.5) and pressure decay test has been completed (1.5.6), Vent pit cover open, Pit monitoring complete - measured gas and O ₂ levels are acceptable, Vent valve(s) open, Tank vacuum, AN-101-107 (IN WG): 2.0, 2.2, 2.0, 2.3, 2.4, 2.1, 2.5
2.1.5 - 2.1.8	DJM 1-28-97	Lock and tag removed, 1.7 IN WG Vac. Station isolation valve open, N/A for 2.1.7 and 2.1.8 (other stations will be brought on-line as tested)
2.2.1 - 2.2.5	DJM 1-28-97	125 scfm orifice plate installed per WHC-SD-WM-ATR-178 (verified again if changed out per step 2.5.2), Port controller is levitated, and drops and raises freely, Flow controller PASSES simple/final functional test
2.3.1 & 2.3.2	DJM 1-28-97	Pit entry for monitoring is not required
2.3.3	DJM 1-28-97	Bonding of applicable plugs/instruments complete, Resistance check verified < 1 MΩ
2.3.4	DJM 1-28-97	ELECTRICAL RESISTANCE IN Ω: N/A CALIBRATION DUE DATE: N/A LESS THAN ONE MEGOHM (1 MΩ): N/A O.C. SIGNATURE & DATE: N/A Flammable gas concentration: 0% LEL Location: Dome

JT 2/11/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-105

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6	DJM 1-28-97	Plugs removed for 5 minutes, Flammable gas concentration: 0% LEL Location: Dome
2.4.1	DJM 1-28-97	Filter PASSES aerosol testing, see attached Vent + Balance test data sheets
2.5.1 - 2.5.3	DJM 1-28-97	Equipment restored, Final installed orifice size (inches): 3-3/32 (100 cfm) -2.0 IN WG
2.6.1 - 2.6.4	DJM 1-28-97	Data sheets are complete and ready for QA review

* ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Robert Nicholson *Robert Nicholson* 1-28-97
(Cognizant Engineer, printed name, signature, & date)

Test Execution Data Sheet reviewed By:

Wk Adams *Wk Adams* 1/29/97
(Quality Assurance, printed name, signature, & date)

ST 2/1/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-106

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
		#4
2.1.1 - 2.1.4	DJM 1-28-97	Note: dPgages have been calibrated (1.5.5) and pressure decay test has been completed (1.5.6), Vent pit cover open, Pit monitoring complete - measured gas and O ₂ levels are acceptable, Vent valve(s) open, Tank vacuum, AN-101-107 (1N WG): 2.0, 2.2, 1.9, 2.2, 2.4, 2.1, 2.5
2.1.5 - 2.1.8	DJM 1-28-97	Lock and tag removed, -2.2 IN WG Station isolation valve open, N/A for 2.1.7 and 2.1.8 (other stations will be brought on-line as tested)
2.2.1 - 2.2.5	DJM 1-28-97	125 scfm orifice plate installed per WHC-SD-WM-ATR-178 (verified again if changed out per step 2.5.2), Port controller is levitated, and drops and raises freely, Flow controller PASSES simple/final functional test
2.3.1 & 2.3.2	DJM 1-28-97	pit entry for monitoring is not required
2.3.3	DJM 1-28-97	Bonding of applicable plugs/instruments complete, Resistance check verified < 1 MΩ
2.3.4	DJM 1-28-97	ELECTRICAL RESISTANCE IN Ω: N/A CALIBRATION DUE DATE: N/A LESS THAN ONE MEGOHM (1 MΩ): N/A G.C. SIGNATURE & DATE: N/A Flammable gas concentration: 0% LEL Location: Dome

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HNF-SD-WM-OTR-215 Rev. 0

ST 2/11/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-106

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6	DSM 1-28-97	Plugs removed for 5 minutes, Flammable gas concentration: 0% LEL Location: Dome
2.4.1	DSM 1-28-97	Filter PASSES aerosol testing, see attached Vent + Balance test data sheets
2.5.1 - 2.5.3	DSM 1-28-97	Equipment restored, Final installed orifice size (inches): 2-7/16 (60 cfm)
2.6.1 - 2.6.4	DSM 1-28-97	Data sheets are complete and ready for QA review

*

ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Robert Nicholson Robert Nicholson 1-28-97
(Cognizant Engineer, printed name, signature, & date)

Test Execution Data Sheet reviewed By:

W.H. Adams W.H. Adams 1/29/97
(Quality Assurance, printed name, signature, & date)

JT 2/1/97

TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-107

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
		#5
2.1.1 - 2.1.4	DJM 1-28-97	Note: dPgages have been calibrated (1.5.5) and pressure decay test has been completed (1.5.6), Vent pit cover open, Pit monitoring complete - measured gas and O ₂ levels are acceptable, Vent valve(s) open, Tank vacuum, AN-101-107 (1NWG): 1.9, 2.1, 2.0, 2.1, 2.2, 2.0, 2.5
2.1.5 - 2.1.8	DJM 1-28-97	Lock and tag removed, Station isolation valve open, N/A for 2.1.7 and 2.1.8 (other stations will be brought on-line as tested)
2.2.1 - 2.2.5	DJM 1-28-97	125 scfm orifice plate installed per WMC-SD-WM-ATR-178 (verified again if changed out per step 2.5.2), Port controller is levitated, and drops and raises freely, Flow controller PASSES simple/final functional test
2.3.1 & 2.3.2	DJM 1-28-97	Pit entry for monitoring is not required, pit cover open, monitoring complete, measured gas + O ₂ levels acceptable
2.3.3	DJM 1-28-97	Bonding of applicable plugs/instruments complete, Resistance check verified < 1 MΩ
2.3.4	DJM 1-28-97	ELECTRICAL RESISTANCE IN G: N/A LESS THAN ONE MEGOHM (1 MΩ): N/A Flammable gas concentration: 0% LEL Location: Vent pit CALIBRATION DUE DATE: N/A O.C. SIGNATURE & DATE: N/A

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TEST EXECUTION DATA SHEET

TANK NUMBER: 241-AN-107

REFERENCE STEP	ACCEPT/REJECT* (TEST DIRECTOR OR DESIGNEE TO INITIAL AND DATE)	RECORDED VALUES (INCLUDE UNITS), OBSERVATIONS, OTHER DATA
2.3.5 & 2.3.6	DJM 1-28-97	Plugs removed for 5 minutes, Flammable gas concentration: 0% LEL Location: Vent pit
2.4.1	DJM 1-28-97	Filter PASSES aerosol testing, see attached Vent + Balance test data sheets
2.5.1 - 2.5.3	DJM 1-28-97	Equipment restored, Final installed orifice size (inches): 2-7/16 (60 cfm)
2.6.1 - 2.6.4	DJM 1-28-97	Data sheets are complete and ready for QA review

*

ACCEPTANCE INDICATED BY TEST DIRECTOR'S OR DESIGNEE'S INITIALS AND DATE. IF RESULTS ARE REJECTED, INDICATE AS SUCH AND DESCRIBE CIRCUMSTANCES IN THE OBSERVATIONS COLUMN.

Results Accepted By:

Robert Nicholson, Robert Nicholson 1-28-97
 (Cognizant Engineer, printed name, signature, & date)

Test Execution Data Sheet reviewed By:

W.K. Adams, W.K. Adams 1/29/97
 (Quality Assurance, printed name, signature, & date)

TEST PARTICIPANTS IDENTIFICATION LIST

INITIALS	PRINTED NAME	RESPONSIBILITY
DJM	Dan Minter	Engr. support
JJT	JACK F THOMPSON	COG. ENG.
DAM	D.A. McCAWETT	VAR
RLW	Robert L. Ward	V+D
SVC	Steven V. Carrick	WB
JPH	Josh Herrick	NO
VM	Vicki Miller	NPO
MWA	Greg Hanson	Test Director
RSS	RANDY SWIFT	ELEC.
K	KASEY G. JUNT	IHS
TEW	VERONICA E WATSON	Nuclear Operator
RSN	RS Nicholson	241-AN Cap Eng
JJR	JAMES T ROSS	P.I.C. <i>[Signature]</i>

WTP MAINTENANCE PROCEDURE DATA SHEET
241-AN TANK INLET FILTER
AEROSOL TEST DATA SHEETS

PROC. NO. 6-TF-156-TV
REV. 0, CHG. 0
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DATA SHEET 1

7.1	INSTRUMENT CALIBRATION DATA	
7.1.1	AIR FLOW INSTRUMENT	PHOTOMETER
	Flow Instrument Type	Equipment Number 6476
	WHSL Code Number	WHSL Code Number 702-23-10-012
	WHSL Cal Due Date	WHSL Cal Due Date 1-16-98
		WHC Cal Due Date 7-22-97
	AEROSOL GENERATOR	
	Model Number TDA-6A	Model Number TDA-6A
	Equipment Number 10957	Equipment Number 10376
	Functional Test Due Date 6-12-97	Functional Test Due Date 5-1-97
	Aerosol Type Emery 3004	Aerosol Type Emery 3004
7.1.2	ADDITIONAL INSTRUMENT CALIBRATION DATA	
	COMMENTS: used Generator 10376 for all tests 10957 would not work.	

Initials/Date *luc* 1-28-98
guc
 1-28-97

WTP MAINTENANCE PROCEDURE DATA SHEET
241-AN TANK INLET FILTER
AEROSOL TEST DATA SHEETS

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DATA SHEET 2

STEP 7.2	VISUAL INSPECTION CHECKLIST	YES	NO	N/A
7.2.1	Filter housing access adequate?	X		
	Housekeeping adequate?	X		
	Lighting levels adequate?	X		
	Housing or ductwork damaged?		X	
	Test ports available (Figures 1 & 2)?	X		
	Test ports labeled?	X		
	Housing door or seal damaged or leaking?		X	
	Installed pressure gauges labeled?	X		
	Calibration labels current?	X		
	Instrumentation damaged (broken, disconnected)?		X	
	Filter damaged (tears, holes, frame separation)?		X	
	Evidence of moisture in housing (stains, water)?		X	
7.2.2	COMMENTS: _____ _____ _____ _____ _____ _____ _____ _____ _____ _____			

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AEROSOL TEST DATA SHEETS

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DATA SHEET 3 (Sheet 1 of 2)

STEP 7.3		DIFFERENTIAL PRESSURE READINGS				
7.3.1	FILTER*	DP GAUGE*	LOCATION	READING (in. wg)	LIMITS (in. wg)	RESULTS
	241-AN-101 TANK INLET					
	Prefilter FLT-101A	PDI-113A	Inlet Filter	.30	0.01 min 1.00 max	PASS FAIL
	HEPA FLT-101B	PDI-114A		0	0.10 min 2.00 max	PASS FAIL
	241-AN-102 TANK INLET					
	Prefilter FLT-102A	PDI-113B	Inlet Filter	.02	0.01 min 1.00 max	PASS FAIL
	HEPA FLT-102B	PDI-114B		.19	0.10 min 2.00 max	PASS FAIL
	241-AN-103 TANK INLET					
	Prefilter FLT-103A	PDI-113C	Inlet Filter	.10	0.01 min 1.00 max	PASS FAIL
	HEPA FLT-103B	PDI-114C		.20	0.10 min 2.00 max	PASS FAIL
	241-AN-104 TANK INLET					
	Prefilter FLT-104A	PDI-113D	Inlet Filter	0	0.01 min 1.00 max	PASS FAIL
	HEPA FLT-104B	PDI-114D		.16	0.10 min 2.00 max	PASS FAIL
	241-AN-105 TANK INLET					
	Prefilter FLT-105A	PDI-113E	Inlet Filter	.03	0.01 min 1.00 max	PASS FAIL
	HEPA FLT-105B	PDI-114E		.19	0.10 min 2.00 max	PASS FAIL

* Equipment designations as labeled in field are prefixed by "VTP-".

Initials/Date SM 1-28-97
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WTP MAINTENANCE PROCEDURE DATA SHEET
241-AN TANK INLET FILTER
AEROSOL TEST DATA SHEETS

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DATA SHEET 3 (Sheet 2 of 2)

STEP 7.3	DIFFERENTIAL PRESSURE READINGS*					
	FILTER*	DP GAUGE*	LOCATION	READING (in. wg)	LIMITS (in. wg)	RESULTS
7.3.1	241-AN-106 TANK INLET					
	Prefilter FLT-106A	PDI-113F	Inlet Filter	0	0.01 min 1.00 max	PASS FAIL
	HEPA FLT-106B	PDI-114F		.15	0.10 min 2.00 max	PASS FAIL
	241-AN-107 TANK INLET					
	Prefilter FLT-107A	PDI-113G	Inlet Filter	0	0.01 min 1.00 max	PASS FAIL
	HEPA FLT-107B	PDI-114G		.16	0.10 min 2.00 max	PASS FAIL
7.3.2	Authorization to Proceed: If <u>any</u> DP reading is NOT within operating limits, then authorization to continue testing is <u>required</u> . Fac. PIC: <u>[Signature]</u> Date: <u>1-28-97</u>					
	COMMENTS: <u>per filter 106, 104, 107</u> <u>Primary Hepta 101 pressure transducer gauge wrong</u> <u>> Needs to start @ 0" to 1" or < 1"</u> <u>[Signature]</u>					

* Equipment designations as labeled in field are prefixed by "VTP-".

Initials/Date [Signature] 1-28-97

WTP MAINTENANCE PROCEDURE DATA SHEET
 241-AN TANK INLET FILTER
 AEROSOL TEST DATA SHEETS

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241-AN TANK INLET	
MEASUREMENT	TEST PORT
Velocity Pressure	C, D
Duct Diameter:	12 in. (i.d.)
Duct Area:	0.79 sq ft

NOTE:

PITOT TRAVERSES ARE NOT TAKEN
 UNLESS DIRECTED BY COG ENGINEER.
 INLET AIR FLOW IS DETERMINED BY
 FLOW CONTROLLER ORIFICE PLATE
 SIZE (SEE H-2-85647-3).

H-2-85646
 TF156TV1.00

Figure 1. 241-AN Tank Inlet Air Flow Test Ports (Typical).

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241-AN TANK INLET FILTER
AEROSOL TEST DATA SHEETS

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DATA SHEET 4 (Sheet 1 of 7)

241-AN-101 TANK INLET

STEP 7.4	SYSTEM AIR FLOW READINGS				
--	STEPS 7.4.1 THRU 7.4.6 DO NOT APPLY UNLESS DIRECTED BY THE COGNIZANT ENGINEER. ENTER ORIFICE PLATE NUMBER AND NOMINAL FLOW FROM SCHEDULE SHOWN ON H-2-85647, SHEET 3.				
	PLATE #	16	NOMINAL AIR FLOW (CFM)		125
	Traverse Points* (in.)	PORT C		PORT D	
		VP (in. wg)	Velocity** (fpm)	VP (in. wg)	Velocity** (fpm)
7.4.1 7.4.2 7.4.3	1/2				
	1				
	1 3/4				
	2 3/4				
	4 1/8				
	7 7/8				
	9 1/4				
	10 1/4				
	11				
	11 1/2				
7.4.4	Port Totals (fpm)				
	Total fpm = Total Port C + Total Port D				
7.4.5	Average fpm = Total fpm ÷ 20				
7.4.6	Air flow (cfm) = Average fpm x 0.79 sq ft				

* Ten-point traverse per ACGIH 9 measured relative to internal diameter (i.d.); no points to be located within 0.5 in. of stack walls (40 CFR 60, App. A).

** FPM = 4005 $\sqrt{VP}$

Initials/Date

See 1-28-97

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AEROSOL TEST DATA SHEETS

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241-AN-102 TANK INLET

STEP 7.4		SYSTEM AIR FLOW READINGS			
STEPS 7.4.1 THRU 7.4.6 DO NOT APPLY UNLESS DIRECTED BY THE COGNIZANT ENGINEER. ENTER ORIFICE PLATE NUMBER AND NOMINAL FLOW FROM SCHEDULE SHOWN ON H-2-85647, SHEET 3.					
PLATE #		16		NOMINAL AIR FLOW (CFM)	
				125	
Traverse Points* (in.)		PORT C		PORT D	
		VP (in. wg)	Velocity** (fpm)	VP (in. wg)	Velocity** (fpm)
7.4.1 7.4.2 7.4.3	1/2				
	1				
	1 3/4				
	2 3/4				
	4 1/8				
	7 7/8				
	9 1/4				
	10 1/4				
	11				
	11 1/2				
7.4.4	Port Totals (fpm)				
	Total fpm = Total Port C + Total Port D				
7.4.5	Average fpm = Total fpm ÷ 20				
7.4.6	Air flow (cfm) = Average fpm x 0.79 sq ft				

* Ten-point traverse per ACGIH 9 measured relative to internal diameter (i.d.); no points to be located within 0.5 in. of stack walls (40 CFR 60, App. A).

** FPM = 4005 $\sqrt{VP}$

Initials/Date lu 1-28-97

WTP MAINTENANCE PROCEDURE DATA SHEET
241-AN TANK INLET FILTER
AEROSOL TEST DATA SHEETS
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DATA SHEET 4 (Sheet 3 of 7)**241-AN-103 TANK INLET**

STEP 7.4		SYSTEM AIR FLOW READINGS			
STEPS 7.4.1 THRU 7.4.6 DO NOT APPLY UNLESS DIRECTED BY THE COGNIZANT ENGINEER. ENTER ORIFICE PLATE NUMBER AND NOMINAL FLOW FROM SCHEDULE SHOWN ON H-2-85647, SHEET 3.					
PLATE #		16		NOMINAL AIR FLOW (CFM)	
				125	
7.4.1 7.4.2 7.4.3	Traverse Points* (in.)	PORT C		PORT D	
		VP (in. wg)	Velocity** (fpm)	VP (in. wg)	Velocity** (fpm)
	1/2				
	1				
	1 3/4				
	2 3/4				
	4 1/8				
	7 7/8				
	9 1/4				
	10 1/4				
	11				
	11 1/2				
7.4.4	Port Totals (fpm)				
	Total fpm = Total Port C + Total Port D				
7.4.5	Average fpm = Total fpm ÷ 20				
7.4.6	Air flow (cfm) = Average fpm x 0.79 sq ft				

* Ten-point traverse per ACGIH 9 measured relative to internal diameter (i.d.); no points to be located within 0.5 in. of stack walls (40 CFR 60, App. A).

** FPM = 4005 $\sqrt{VP}$

Initials/Date sr 1-28-97

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241-AN-104 TANK INLET

STEP 7.4		SYSTEM AIR FLOW READINGS			
STEPS 7.4.1 THRU 7.4.6 DO NOT APPLY UNLESS DIRECTED BY THE COGNIZANT ENGINEER. ENTER ORIFICE PLATE NUMBER AND NOMINAL FLOW FROM SCHEDULE SHOWN ON H-2-85647, SHEET 3.					
PLATE #		16		NOMINAL AIR FLOW (CFM)	
				125	
Traverse Points* (in.)		PORT C		PORT D	
		VP (in. wg)	Velocity** (fpm)	VP (in. wg)	Velocity** (fpm)
7.4.1 7.4.2 7.4.3	1/2				
	1				
	1 3/4				
	2 3/4				
	4 1/8				
	7 7/8				
	9 1/4				
	10 1/4				
	11				
	11 1/2				
	7.4.4	Port Totals (fpm)			
Total fpm = Total Port C + Total Port D					
7.4.5	Average fpm = Total fpm + 20				
7.4.6	Air flow (cfm) = Average fpm x 0.79 sq ft				

* Ten-point traverse per ACGIH 9 measured relative to internal diameter (i.d.); no points to be located within 0.5 in. of stack walls (40 CFR 60, App. A).

** FPM = 4005 $\sqrt{VP}$

Initials/Date luc 1-28-97

WTP MAINTENANCE PROCEDURE DATA SHEET
241-AN TANK INLET FILTER
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DATA SHEET 4 (Sheet 5 of 7)**241-AN-105 TANK INLET**

STEP 7.4		SYSTEM AIR FLOW READINGS			
STEPS 7.4.1 THRU 7.4.6 DO NOT APPLY UNLESS DIRECTED BY THE COGNIZANT ENGINEER. ENTER ORIFICE PLATE NUMBER AND NOMINAL FLOW FROM SCHEDULE SHOWN ON H-2-85647, SHEET 3.					
PLATE #		16		NOMINAL AIR FLOW (CFM)	
				125	
Traverse Points* (in.)		PORT C		PORT D	
		VP (in. wg)	Velocity** (fpm)	VP (in. wg)	Velocity** (fpm)
7.4.1 7.4.2 7.4.3	1/2				
	1				
	1 3/4				
	2 3/4				
	4 1/8				
	7 7/8				
	9 1/4				
	10 1/4				
	11				
	11 1/2				
7.4.4	Port Totals (fpm)				
	Total fpm = Total Port C + Total Port D				
7.4.5	Average fpm = Total fpm ÷ 20				
7.4.6	Air flow (cfm) = Average fpm x 0.79 sq ft				

* Ten-point traverse per ACGIH 9 measured relative to internal diameter (i.d.); no points to be located within 0.5 in. of stack walls (40 CFR 60, App. A).

** FPM = 4005 $\sqrt{VP}$

Initials/Date mc 1-28-97

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241-AN-106 TANK INLET

STEP 7.4		SYSTEM AIR FLOW READINGS			
STEPS 7.4.1 THRU 7.4.6 DO NOT APPLY UNLESS DIRECTED BY THE COGNIZANT ENGINEER. ENTER ORIFICE PLATE NUMBER AND NOMINAL FLOW FROM SCHEDULE SHOWN ON H-2-85647, SHEET 3.					
--		PLATE #	16	NOMINAL AIR FLOW (CFM)	125
7.4.1 7.4.2 7.4.3	Traverse Points* (in.)	PORT C		PORT D	
		VP (in. wg)	Velocity** (fpm)	VP (in. wg)	Velocity** (fpm)
	1/2				
	1				
	1 3/4				
	2 3/4				
	4 1/8				
	7 7/8				
	9 1/4				
	10 1/4				
	11				
	11 1/2				
7.4.4	Port Totals (fpm)				
	Total fpm = Total Port C + Total Port D				
7.4.5	Average fpm = Total fpm + 20				
7.4.6	Air flow (cfm) = Average fpm x 0.79 sq ft				

* Ten-point traverse per ACGIH 9 measured relative to internal diameter (i.d.); no points to be located within 0.5 in. of stack walls (40 CFR 60, App. A).

** FPM = 4005 $\sqrt{VP}$

Initials/Date Luc 1-28-97

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DATA SHEET 4 (Sheet 7 of 7)**241-AN-107 TANK INLET**

STEP 7.4		SYSTEM AIR FLOW READINGS			
STEPS 7.4.1 THRU 7.4.6 DO NOT APPLY UNLESS DIRECTED BY THE COGNIZANT ENGINEER. ENTER ORIFICE PLATE NUMBER AND NOMINAL FLOW FROM SCHEDULE SHOWN ON H-2-85647, SHEET 3.					
PLATE #		/6		NOMINAL AIR FLOW (CFM)	
				125	
7.4.1 7.4.2 7.4.3	Traverse Points* (in.)	PORT C		PORT D	
		VP (in. wg)	Velocity** (fpm)	VP (in. wg)	Velocity** (fpm)
	1/2				
	1				
	1 3/4				
	2 3/4				
	4 1/8				
	7 7/8				
	9 1/4				
	10 1/4				
	11				
	11 1/2				
7.4.4	Port Totals (fpm)				
	Total fpm = Total Port C + Total Port D				
7.4.5	Average fpm = Total fpm ÷ 20				
7.4.6	Air flow (cfm) = Average fpm x 0.79 sq ft				

* Ten-point traverse per ACGIH 9 measured relative to internal diameter (i.d.); no points to be located within 0.5 in. of stack walls (40 CFR 60, App. A).

** FPM = 4005 $\sqrt{VP}$

Initials/Date LM 1-28-97

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TEST	PORT	HEPA FILTER VTP-FLT 101B THRU 107B
BASELINE	INJECT	A
	SAMPLE	B
PENETRATION	INJECT	A
	SAMPLE	C

Figure 2. 241-AN Tank Inlet Filter Test Ports (Typical).

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241-AN TANK INLET FILTER
AEROSOL TEST DATA SHEETS

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DATA SHEET 5 (Sheet 1 of 7)

241-AN-101 TANK INLET FILTER VTP-FLT-101B

STEP 7.5	AEROSOL TEST READINGS		
	TRIAL 1	TRIAL 2	TRIAL 3
7.5.1	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi
7.5.2	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b
7.5.3	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p
7.5.4	<u>.1</u> x <u>2</u> = <u>.2</u> c_p	<u>.1</u> x <u>2</u> = <u>.2</u> c_p	<u>.1</u> x <u>2</u> = <u>.2</u> c_p
STEP 7.8	AEROSOL PENETRATION CALCULATIONS*		
7.8.1	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$
7.8.2	PASS = $P < 0.05\%$ FAIL = $P \geq 0.05\%$		
	<u>PASS</u> FAIL	<u>PASS</u> FAIL	<u>PASS</u> FAIL
7.8.3	Fac. PIC signature required if <u>ANY</u> trial fails: Fac. PIC _____ Date: _____		

* Background concentrations (B_b , B_p) are for information only and are not part of percent penetration calculation.

Initials/Date Joe 1-28-97

WTP MAINTENANCE PROCEDURE DATA SHEET
241-AN TANK INLET FILTER
AEROSOL TEST DATA SHEETS

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DATA SHEET 5 (Sheet 2 of 7)

241-AN-102 TANK INLET FILTER VTP-FLT-102B

STEP 7.5	AEROSOL TEST READINGS		
	TRIAL 1	TRIAL 2	TRIAL 3
7.5.1	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi
7.5.2	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b
7.5.3	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p
7.5.4	<u>.1</u> x <u>2</u> = <u>.2</u> c_p	<u>.1</u> x <u>2</u> = <u>.2</u> c_p	<u>.1</u> x <u>2</u> = <u>.2</u> c_p
STEP 7.8	AEROSOL PENETRATION CALCULATIONS*		
7.8.1	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$
7.8.2	PASS = $P < 0.05\%$ FAIL = $P \geq 0.05\%$		
	<u>PASS</u> / FAIL	<u>PASS</u> / FAIL	<u>PASS</u> / FAIL
7.8.3	Fac. PIC signature required if <u>ANY</u> trial fails: Fac. PIC _____ Date: _____		

* Background concentrations (B_b , B_p) are for information only and are not part of percent penetration calculation.

Initials/Date SLC 1-28-87

WTP MAINTENANCE
241-AN TANK INLET
AEROSOL TEST DATA

Post-It* Fax Note	7671	Date	1-29-97	# of pages	1
To	JACK T.	From	RSSC		
Co./Dept	Eng	Co.			
Phone #		Phone #			
Fax #	3-2240	Fax #			

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O, CHG. O
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241-AN-103 TANK INLET FILTER VTP-FLT-103B

STEP 7.5	AEROSOL TEST READINGS		
	TRIAL 1	TRIAL 2	TRIAL 3
7.5.1	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi
7.5.2	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C _o	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C _b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C _b
7.5.3	<u>100</u> x <u>0</u> = <u>0</u> B _b <u>.1</u> x <u>0</u> = <u>0</u> B _p	<u>100</u> x <u>0</u> = <u>0</u> B _b <u>.1</u> x <u>0</u> = <u>0</u> B _p	<u>100</u> x <u>0</u> = <u>0</u> B _b <u>.1</u> x <u>0</u> = <u>0</u> B _p
7.5.4	<u>.1</u> x <u>2</u> = <u>.2</u> C _p	<u>.1</u> x <u>2</u> = <u>.2</u> C _p	<u>.1</u> x <u>2</u> = <u>.2</u> C _p
STEP 7.8	AEROSOL PENETRATION CALCULATIONS*		
7.8.1	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = \underline{.002} \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = \underline{.002} \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = \underline{.002} \%$
7.8.2	PASS = P < 0.05% FAIL = P ≥ 0.05% <div style="display: flex; justify-content: space-around;"> <u>PASS</u> / FAIL <u>PASS</u> / FAIL <u>PASS</u> / FAIL </div>		
7.8.3	Fac. PIC signature required if <u>ANY</u> trial fails: Fac. PIC _____ Date: _____		

* Background concentrations (B_b, B_p) are for information only and are not part of percent penetration calculation.

 Initials/Date JM 1-28-97

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241-AN TANK INLET FILTER
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DATA SHEET 5 (Sheet 4 of 7)
241-AN-104 TANK INLET FILTER VTP-FLT-104B

STEP 7.5	AEROSOL TEST READINGS		
	TRIAL 1	TRIAL 2	TRIAL 3
7.5.1	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi
7.5.2	(Scale X Reading = Eq. Input) <u>100</u> X <u>100</u> = <u>10000</u> C_b	(Scale X Reading = Eq. Input) <u>100</u> X <u>100</u> = <u>10000</u> C_b	(Scale X Reading = Eq. Input) <u>100</u> X <u>100</u> = <u>10000</u> C_b
7.5.3	<u>100</u> X <u>0</u> = <u>0</u> B_b <u>.1</u> X <u>0</u> = <u>0</u> B_p	<u>100</u> X <u>0</u> = <u>0</u> B_b <u>.1</u> X <u>0</u> = <u>0</u> B_p	<u>100</u> X <u>0</u> = <u>0</u> B_b <u>.1</u> X <u>0</u> = <u>0</u> B_p
7.5.4	<u>.1</u> X <u>2</u> = <u>.2</u> C_p	<u>.1</u> X <u>2</u> = <u>.2</u> C_p	<u>.1</u> X <u>2</u> = <u>.2</u> C_p
STEP 7.8	AEROSOL PENETRATION CALCULATIONS*		
7.8.1	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$
7.8.2	PASS = $P < 0.05\%$ FAIL = $P \geq 0.05\%$		
	PASS FAIL	PASS / FAIL	PASS / FAIL
7.8.3	Fac. PIC signature required if <u>ANY</u> trial fails: Fac. PIC _____ Date: _____		

* Background concentrations (B_b , B_p) are for information only and are not part of percent penetration calculation.

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WTP MAINTENANCE PROCEDURE DATA SHEET
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241-AN-105 TANK INLET FILTER VTP-FLT-105B

STEP 7.5	AEROSOL TEST READINGS		
	TRIAL 1	TRIAL 2	TRIAL 3
7.5.1	Generator: <u>1/1A</u> psi	Generator: <u>1/1A</u> psi	Generator: <u>1/1A</u> psi
7.5.2	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> c_b
7.5.3	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p
7.5.4	<u>.1</u> x <u>2</u> = <u>.2</u> c_p	<u>.1</u> x <u>2</u> = <u>.2</u> c_p	<u>.1</u> x <u>2</u> = <u>.2</u> c_p
STEP 7.8	AEROSOL PENETRATION CALCULATIONS*		
7.8.1	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = \underline{.002} \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = \underline{.002} \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = \underline{.002} \%$
7.8.2	PASS = $P < 0.05\%$ FAIL = $P \geq 0.05\%$		
	PASS / FAIL	PASS / FAIL	PASS / FAIL
7.8.3	Fac. PIC signature required if <u>ANY</u> trial fails: Fac. PIC _____ Date: _____		

* Background concentrations (B_b , B_p) are for information only and are not part of percent penetration calculation.

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AEROSOL TEST DATA SHEETS

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DATA SHEET 5 (Sheet 6 of 7)

241-AN-106 TANK INLET FILTER VTP-FLT-106B

STEP 7.5	AEROSOL TEST READINGS		
	TRIAL 1	TRIAL 2	TRIAL 3
7.5.1	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi
7.5.2	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C_b
7.5.3	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p
7.5.4	<u>.1</u> x <u>2</u> = <u>12</u> C_p	<u>.1</u> x <u>2</u> = <u>12</u> C_p	<u>.1</u> x <u>2</u> = <u>12</u> C_p
STEP 7.8	AEROSOL PENETRATION CALCULATIONS*		
7.8.1	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.12}{10000} \right)$ $P = \underline{.002} \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.12}{10000} \right)$ $P = \underline{.002} \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.12}{10000} \right)$ $P = \underline{.002} \%$
7.8.2	PASS = $P < 0.05\%$ FAIL = $P \geq 0.05\%$ <div style="display: flex; justify-content: space-around;"> <u>PASS</u> / FAIL <u>PASS</u> / FAIL <u>PASS</u> / FAIL </div>		
7.8.3	Fac. PIC signature required if <u>ANY</u> trial fails: Fac. PIC _____ Date: _____		

* Background concentrations (B_b , B_p) are for information only and are not part of percent penetration calculation.

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241-AN TANK INLET FILTER
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DATA SHEET 5 (Sheet 7 of 7)

241-AN-107 TANK INLET FILTER VTP-FLT-107B

STEP 7.5	AEROSOL TEST READINGS		
	TRIAL 1	TRIAL 2	TRIAL 3
7.5.1	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi	Generator: <u>N/A</u> psi
7.5.2	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C_b	(Scale X Reading = Eq. Input) <u>100</u> x <u>100</u> = <u>10000</u> C_b
7.5.3	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p	<u>100</u> x <u>0</u> = <u>0</u> B_b <u>.1</u> x <u>0</u> = <u>0</u> B_p
7.5.4	<u>.1</u> x <u>2</u> = <u>.2</u> C_p	<u>.1</u> x <u>2</u> = <u>.2</u> C_p	<u>.1</u> x <u>2</u> = <u>.2</u> C_p
STEP 7.8	AEROSOL PENETRATION CALCULATIONS*		
7.8.1	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$	$P = 100 \left(\frac{C_p}{C_b} \right)$ $P = 100 \left(\frac{.2}{10000} \right)$ $P = .002 \%$
7.8.2	PASS = $P < 0.05\%$ FAIL = $P \geq 0.05\%$ PASS / FAIL PASS / FAIL PASS / FAIL		
7.8.3	Fac. PIC signature required if <u>ANY</u> trial fails: Fac. PIC _____ Date: _____		

* Background concentrations (B_b , B_p) are for information only and are not part of percent penetration calculation.

Initials/Date SK 1-28-97

DISTRIBUTION SHEET

To	From	Page 1 of 1
Distribution	JA Tuck, 373-5755, S2-03	Date 5 February 1997
Project Title/Work Order		EDT No. 617371
241-AN Ventilation Upgrades; HNF-SD-WM-OTR-215 Rev. 0		ECN No. n/a

Name	MSIN	Text With All Attach.	Text Only	Attach./ Appendix Only	EDT/ECN Only
WL Adams	S5-13				X
RE Bauer	S7-14				X
RA Dodd	S5-07				X
CE Hanson	S7-12	X			
GN Hanson	S5-05	X			
GD Johnson	S7-14				X
JR Kriskovich	R1-56				X
J Lohrasbi	S5-05	X			
DJ Minter	S2-24	X			
RS Nicholson	S5-05	X			
WE Ross	S5-07				X
RJ Shupe	R2-82				X
DL Sparks	S5-03				X
JF Thompson	S5-57	X			
JA Tuck	S2-03	X			