Engineering Development of Advanced Coal-Fired
Low-Emissions Boiler Systems

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P.O. Box 880
Morgantown, West Virginia 26507-0880

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By
Babcock & Wilcox Company
1562 Beeson Street
Alliance, Ohio 44601

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I. Project Management

I.1 Summary of Activities

I.1.1 Period of April 1997 through June 1997

The detailed test and operations plan to operate, demonstrate, and evaluate the POC test facility was completed. The test plan was written to meet the objectives as set forth in the SOW. The POC test plan is being incorporated into the Phase III final report. The POC schedule and Phase IV cost estimate were also completed.

The Phase II final report draft was completed. Topical reports addressing the areas identified in the report outlines are essentially completed. A draft version of the final report was distributed for internal review. Comments received during the internal review are being incorporated into the final report.

Work on the Phase III final report continued. Suggestions received from an internal review are being incorporated into the final report.

I.1.1 Technical Papers Submitted or Presented


I.1.2 Phase IV Funding

Efforts continue to develop support in North Dakota with hopes of obtaining funding. Utility contacts are in progress to identify and obtain tailored collaboration funds to support Phase IV where available.
II. NO\textsubscript{x} Subsystem

The goal of the NO\textsubscript{x} Subsystem is to achieve continuous operation of the Low-Emissions Boiler System (LEBS) at NO\textsubscript{x} emissions at or below 0.20 lb/MBtu through combustion techniques only, with a further target of 0.1 lb NO\textsubscript{x}/MBtu using supplementary advanced flue gas cleanup technologies if necessary. These goals places practical constraints that must be considered on the NO\textsubscript{x} Subsystem design. Not only must the boiler be designed to achieve time-temperature mixing histories that minimize NO\textsubscript{x}, but it must also be designed to operate that way throughout its working lifetime. Therefore, NO\textsubscript{x} minimization strategies must be integrated into the control systems for every boiler component from the pulverizers to the stack. Furthermore, these goals must be met without increases in carbon loss and CO emissions from the levels achieved with current low-NO\textsubscript{x} combustion systems. Therefore, the NO\textsubscript{x} Subsystem requires not only sound mechanical designs of burners, furnace surface, and staging air/fuel injectors, but also sensors and software to allow control of their operation. Through engineering analysis, experimental testing, and numerical modeling in Phase II, an advanced low-NO\textsubscript{x} control system is being developed. The progress of these activities is presented in this report.

II.1 Summary of Activities

II.1.1 Period of April 1997 through June 1997

Work on the final reports is in full swing. Drafts of all Phase II and Phase III final reports were completed for internal review by month's end.

II.2 Key Accomplishments

II.2.1 Final Reports

All contributions to the final reports have been drafted for internal review. Topical reports addressing the areas identified in the report outlines and the Design Deficiency table from Phase I are essentially completed.

II.2.2 POC Test Plan

The detailed test and operations plan to operate, demonstrate, and evaluate the POC test facility was completed. The test plan was written to meet the objectives set forth in the SOW. The POC test plan is being incorporated into the Phase III Final Report.
III. SO₂/Particulate/Air Toxics/Solid By-Product Subsystem

The scope of the SO₂ subsystem comprises the control of SO₂, particulate matter, hazardous air pollutants (commonly called "air toxics"), and solid byproducts from the B&W LEBS plant. The specific minimum performance requirements for the SO₂ subsystem are:

- SO₂ — Less than 0.20 lb (SO₂ equivalent)/MBtu for coals with sulfur levels of 3 lb of sulfur per MBtu and no more than 0.067 times the sulfur content (lb/MBtu) for coals with less than 3 lb of sulfur per MBtu.
- Particulate — Less than 0.015 lb particulate/MBtu
- Potential to comply with possible emissions control regulations for targeted air toxics.
- Produce environmentally benign solid byproduct.
- Integrate with other plant subsystems to yield optimal overall performance and cost.

In addition, the following performance targets have been established:

- SO₂ — Less than 0.10 lb (SO₂ equivalent)/MBtu for coals with sulfur levels of 3 lb of sulfur per MBtu and no more than 0.0333 times the sulfur content (lb/MBtu) for coals with less than 3 lb of sulfur per MBtu.
- Particulate — Less than 0.01 lb particulate/MBtu (B&W plans to achieve 0.005 lb/MBtu)

On the basis of the results compiled during the concept selection process completed in Phase I, the Limestone Injection Dry Scrubbing (LIDS) process was selected for further development and evaluation in B&W's LEBS project. The LIDS process is a cost-effective integration of three commercially proven flue gas cleanup technologies: furnace limestone injection, dry scrubbing, and pulse-jet fabric filtration. As a result of Phase I testing, the initial LIDS process was enhanced by the addition of a particulate collector before the dry scrubber and the new process was named E-LIDS™. Through engineering analysis, experimental testing, and numerical modeling, an E-LIDS™ process is being developed that is capable of ultra-high SO₂ removal and superior particulate control while addressing the potential issues of air toxic emissions and solid byproduct utilization. The progress of the E-LIDS™ activities follows.

III.1 Summary of Activities

III.1.1 Period of April 1997 through June 1997

Drafts of all Phase II and Phase III final reports were completed for internal review by month's end.
III.2 Key Accomplishments

III.2.1 Final Reports

All contributions to the final reports were drafted for internal review. Topical reports addressing the areas identified in the report outlines and the Design Deficiency table from Phase I are essentially completed.

III.2.2 POC Test Plan

The detailed test and operations plan to operate, demonstrate, and evaluate the POC test facility was completed. The test plan was written to meet the objectives set forth in the SOW. The POC test plan is being incorporated into the Phase III Final Report.
IV. Boiler Subsystem

At the heart of the LEBS is the boiler. Within this advanced B&W boiler, all of the low emission technologies are integrated. To meet the net plant efficiency goal of 42%, the boiler must be designed not only to achieve the proper conditions for low NOx combustion with air staging and accommodate the in-furnace injection of the limestone for the LIDS process, but it must also efficiently capture the heat to produce high temperature steam at well above critical pressure. The steam conditions selected for the boiler are 4500 psi, 1100°F/1100°F/1100°F.

Since the steam-side pressure and main and reheat steam temperatures are higher than conventional cycles and operation of low NOx burners creates sub-stoichiometric conditions in portions the furnace, additional challenges are presented. Higher alloy materials must be used in the outlet portions of the superheater and re heater banks to obtain acceptable surface metal temperatures. In addition, materials must be selected that will resist corrosion since the surface of these outlet tubes will operate at temperatures which will allow the coal ash to remain molten on their surfaces. Consideration must also be given to furnace wall corrosion in the combustion zone. Thus, boiler design work has been identified to address the integration of the NOx and SO2 subsystems while applying B&W’s advanced supercritical boiler technology.

IV.1 Summary of Activities

IV.1.1 Period of April 1997 through June 1997

All design, drafting and cost estimating work was completed. Essentially all of the Phase III Volume 2 report has been drafted for internal reviews.

IV.2 Key Accomplishments

IV.2.1 CGU Boiler Development

Activities this quarter centered around completion of the CGU boiler design and drawings, providing final cost estimates to Raytheon and completion of volume 2 of the Phase III final report describing the Commercial Generating Unit.

CGU Boiler Design - The boiler design effort was completed.

Cost Estimation - The boiler island cost for both the conventional 2400 psi 1000°F/1000°F and LEBS designs were completed and provided to Raytheon.

Plant Efficiency - Total plant auxiliary power was finalized with Raytheon and final net plant efficiency determined.
V. Balance of Plant Subsystem

In order to develop an overall plant design and to evaluate plant efficiency and cost, B&W subcontracted with Raytheon Engineers and Constructors of Denver, Colorado. Together a Phase I concept was developed that achieved the initial LEBS goal of 38% net plant efficiency. That design resulted in identification of a number of potential improvements to the turbine cycle and auxiliary equipment needed to meet the Phase II goal of 42% net plant efficiency.

V.1 Summary of Activities

V.1.1 Period of April 1997 through June 1997

All design, drafting and cost estimating work was completed. Essentially all of the Phase III Volume 2 report has been drafted for internal reviews.

Final plant arrangement and P&ID drawings were completed. Balance of plant equipment costs were developed and the economic analysis for the total plant was completed. Auxiliary power requirements were completed and the net plant efficiency was established at 42.27%. The cost analysis/evaluation section for Volume 2 of the Phase III final report was completed and submitted to B&W completing all Raytheon deliverables.

V.2 Key Accomplishments

Plant Arrangement - Plant layout drawings and P&ID's were finalized, completed and submitted to B&W for incorporation into the final reports.

Plant Costs - Balance of plant costs for the conventional and LEBS designs were completed and the cost analysis including levelized busbar costs were completed.

Net Plant Efficiency - The steam cycle heat and mass balances and auxiliary power summary were finalized and the final net plant efficiency is an outstanding 42.27%.

Final Reporting - All Final report contributions were completed to B&W's satisfaction and received for incorporation.
VI. Controls & Sensors Subsystem

In order to maintain low stack emissions and optimum boiler performance throughout the operating range and lifetime of the LEBS, a state-of-the-art integrated control system must be developed. This control system must include new sensors as well as old sensors used in new ways. It must make sense out of the data provided while initiating or directing the operator to take appropriate action. The control system that will help assure that the LEBS will meet its stack emission, efficiency, availability, and cost of electricity goals.

The overall philosophy of the LEBS control system is to use conventional, state-of-the-art solutions to satisfy new control requirements. Existing sensors, hardware, and software are specified whenever possible and new measurements or advanced equipment are recommended for development only where necessary to assure the success of the project. The progress of the Controls & Sensors Subsystem is contained in this report.

VI.1 Summary of Activities

VI.1.1 Period of April 1997 through June 1997

Final report writing was completed. In addition, the POC DCS was revised to incorporate the full complement of controls and sensors on both burner groups and to include additional interposing logic and control loops on the E-LIDSTM system to reduce operating manpower requirements.

VI.2 Key Accomplishments

POC Control System - The POC DCS was revised to incorporate the full complement of controls and sensors on both burner groups and to include additional interposing logic and control loops on the E-LIDSTM system to reduce operating manpower requirements.

Final Reporting - All contributions by the Controls and Sensors subsystem for the Phases II and III final reports were completed.