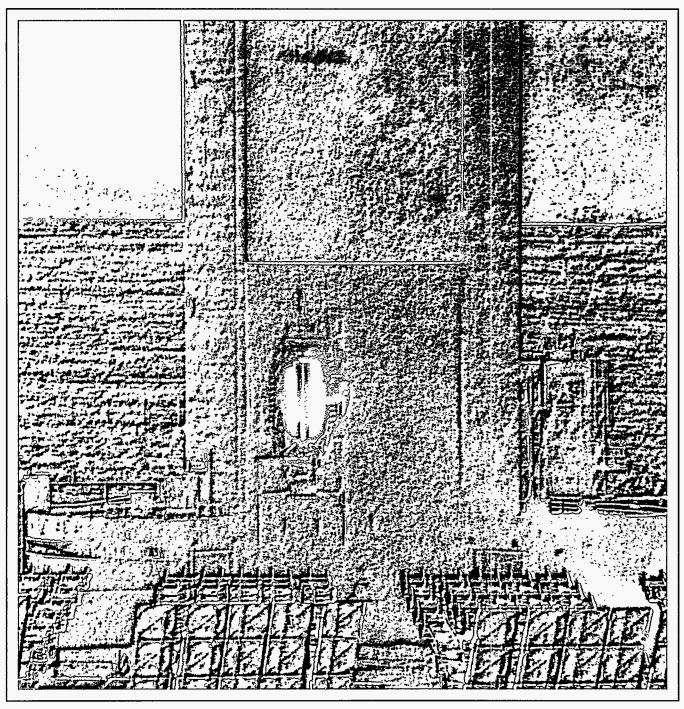
Results of Molten Salt Panel and Component Experiments for Solar Central Receivers:

Cold Fill, Freeze/Thaw, Thermal Cycling and Shock, and Instrumentation Tests

James E. Pacheco, Mark E. Ralph, James M. Chavez, Sam R. Dunkin, Earl E. Rush, Cheryl M. Ghanbari and Matt W. Matthews Solar Thermal Technology and Test Departments

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RESULTS OF MOLTEN SALT PANEL AND COMPONENT EXPERIMENTS FOR SOLAR CENTRAL RECEIVERS: COLD FILL, FREEZE/THAW, THERMAL CYCLING AND SHOCK, AND INSTRUMENTATION TESTS

James E. Pacheco, Mark E. Ralph, James M. Chavez, Sam R. Dunkin, Earl E. Rush, Cheryl M. Ghanbari and Matt W. Matthews Solar Thermal Technology and Test Departments

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Abstract

Experiments have been conducted with a molten salt loop at Sandia National Laboratories in Albuquerque, NM to resolve issues associated with the operation of the 10MW_e Solar Two Central Receiver Power Plant located near Barstow, CA. The salt loop contained two receiver panels, components such as flanges and a check valve, vortex shedding and ultrasonic flow meters, and an impedance pressure transducer. Tests were conducted on procedures for filling and thawing a panel, and assessing components and instrumentation in a molten salt environment. categories of experiments were conducted: 1) cold filling procedures, 2) freeze/thaw procedures, 3) component tests, and 4) instrumentation tests. Cold-panel and -piping fill experiments are described, in which the panels and piping were preheated to temperatures below the salt freezing point prior to initiating flow, to determine the feasibility of cold filling the receiver and piping. The transient thermal response was measured, and heat transfer coefficients and transient stresses were calculated from the data. Analysis is presented which quantifies the thermal stresses in a pipe undergoing thermal shock. In addition, penetration depths were calculated to determine the distances salt could flow in cold pipes prior to freezing shut and validated with panel tests. Freeze/thaw experiments were conducted with the panels, in which the salt was intentionally allowed to freeze in the receiver tubes, then thawed with heliostat beams to assess permanent deformation in the tubes, and to develop procedures to thaw a panel so minimal damage occurs. Slow thermal cycling tests were conducted to measure both how well various designs of flanges (e.g., tapered flanges or clamp type flanges) hold a seal under thermal conditions typical of nightly shut down, and the practicality of using these flanges on high maintenance components. In addition, the flanges were thermally shocked to simulate cold starting the system. Instrumentation such as vortex shedding and ultrasonic flow meters were tested alongside each other, and compared with flow measurements from calibration tanks in the flow loop. MASTER

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Nomenclature

v = Poisson's ratio

Bi = Biot number Cp_s = specific heat of solid Cpm = specific heat of liquid D = diameter of pipeE = modulus of elasticityFo = Fourier number h = heat transfer coefficient $h_c = heat of fusion$ k =thermal conductivity of pipe (Eq. 5) L = wall thicknessNu = Nusselt numberPr = Prandtl number r = radial coordinate of pipe $r_1 = inner radius of pipe$ r_o = outer radius of pipe r* = nondimensional pipe radius R = radial coordinate of inner radius of pipe R_0 = radial coordinate of frozen layer Re = Reynolds number T = temperature $T_f =$ freezing point $T_i = initial$ wall temperature $T_o = inlet liquid temperature$ T_w = wall temperature T_{∞} = fluid temperature x^* = nondimensional distance from insulated surface z = distance to freeze closed α = thermal diffusivity (Eq. 3) or coefficient of thermal expansion (Eq. 9) α_m = thermal diffusivity of liquid α_s = thermal diffusivity of solid $\delta = 1 - r_1^* = \text{nondimensional wall thickness}$ λ_n = characteristic values of transient conduction equation γ = parameter measuring the relative importance of sensible to latent heat, assumed to be 0.7 (water) θ^* = nondimensional temperature θ_0^* = nondimensional temperature at the insulated surface σ_{θ} = circumferential stress σ_r = radial stress $\sigma_z = axial stress$ σ^* = nondimensional thermal stress

Executive Summary

This report summarizes experiments we conducted with a molten salt flow loop, located at the Central Receiver Test Facility at Sandia National Laboratories in Albuquerque, New Mexico, under the US DOE Central Receiver Development Program. Experiments were conducted to test hardware and instrumentation in a molten salt environment and to develop procedures that support the design and operation Solar Two. Solar Two is a 10 MW_e Solar Central Receiver Pilot plant in Daggett, California, which is undergoing retrofit with a receiver and storage system which use molten salt as the heat transfer fluid. The major conclusions and recommendations from our experiments with the molten salt loop are summarized below.

Cold Fill Tests

We successfully showed that molten salt can flow through ambient temperature piping without freezing shut provided the flow rate is high enough. These results were scaled to the riser and down comer of the Solar Two and a 100 MW_e molten salt power plant using a correlation. These large diameter pipes should not freeze closed during the cold filling procedure (e.g., at morning startup). The thermal stresses during this thermal shock were calculated to be lower than the material's endurance limit for vertical runs of the piping. We recommend testing the cold filling method in the riser and downcomer of Solar Two and if it proves favorable, implemented as a mode of operation in commercial plants to reduced parasitic power consumption and increase availability.

We found every region of the receiver does not have to be above the salt freezing point before flow is initiated. The minimum temperature to avoid freezing during startup for the Solar Two receiver is estimated to be 200°F (93°C). We found the best method for preheating a panel was to use moving heliostats to avoid hot or cold spots.

Freeze/Thaw Tests

A receiver panel which becomes frozen with salt could require hours to thaw and could damage the tubes. We measured permanent strains as high as 4% after two freeze/thaw cycles. Monitoring the temperatures during the thawing process was also difficult with a limited number of thermocouples, but an infrared camera would simplify the monitoring.

Component Tests

We found that check valves work well in a molten salt environment after repeated pressure cycling and recommend their use. Flanges held up well to slow thermal cycling and to thermal shocking without major failures. All the flanges tested, though, began to leak slowly. Flanges should be minimized in a molten salt loop. Hot torquing the flanges, periodically, may help reduce the leaks.

Instrumentation Tests

Vortex shedding flow meters worked exceedingly well with molten salt and are the preferred flow meter for this application. Overall flow rate uncertainties of less than $\pm 5\%$ can be obtained with a proper calibration. The impedance-type pressure transducer we tested was responsive and performed well. It could replace hard to find NaK filled pressure transducers. The impedance type is relatively expensive, though.

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I. Background

In a molten salt central receiver power plant, the parasitic electrical power consumption can be a significant percentage of the total power production if it is not properly managed. Good management also involves careful assessment of operating strategies to minimize the parasitics. Since the nitrate salt, which serves as the heat transfer medium between the receiver and the steam generator, has a freezing point of 430°F (221°C), the associated piping, valves, instrumentation, and tanks must be kept above this temperature (typically at 550°F, 288°C) to assure the salt will not freeze. During inclement weather and during the night the plant does not operate, but the heat trace is kept energized to maintain the temperature of the empty lines at 550°F (288°C). This operating strategy is not an economically advantageous method of conditioning a highly cyclic power plant. One strategy of reducing the nightly parasitic power consumption is to turn off the heat trace at night, allowing the piping to cool down to ambient, then fill the piping cold at start up the next morning.

There has been very little data collected on cold starting the receiver and piping at temperatures below the molten salt freezing point. The Molten Salt Electric Experiment receiver in the external configuration was cold started at temperatures below the freezing point. In one of three cases, the receiver partially froze [1]. No detailed analysis was done on the transient freezing phenomenon. In this report we describe experiments where we cold started receiver panels and piping.

Due to the nitrate salt's high freezing point and the fact that the salt expands upon melting, we were concern with the damage that could occur in receiver tubes if the salt were to freeze in the receiver and then thaw out. This situation could occur during shut down of the receiver. If one of the drain valves failed to open and went undetected during the drain process, molten salt would be trapped in the associated panel, and the salt would subsequently freeze. Upon thawing, the expanding salt could damage the tube. In previous experiments, detailed assessments of the freezing and thawing of the panel tubes were not conducted. The Martin Marietta molten salt receiver became frozen with salt and was successfully thawed, though no data on tube deformation was available.

Three molten salt receivers and large-scale pump and valve loops have been tested at Sandia National Laboratories to determine the viability of molten salt as a heat transport fluid and storage medium for central receiver solar power plants. The Category B receiver was a 5 MWt cavity molten nitrate salt receiver. The testing of this receiver in 1988 [2] showed the feasibility of fabricating and operating a molten salt receiver consisting of serpentine flow panels. However, there are some components and instrumentation that need further evaluation.

Check valves have not previously been used in molten salt. Check valves are required when pumps are connected in series to a common manifold, or to the base of a riser to prevent back spin and damage to a pump during a sudden shut off of one pump while the others are flowing. Experiments with flanges in the Pump and Valve Loop show that they were a significant source of leaks.

The purpose of the current molten salt experiments is to verify the operation and reliability of components, instrumentation, and procedures proposed for implementation in the Solar Two project. Many of the components have been proven in a molten salt environment, but additional information is required. Other components were not tested sufficiently or at all in previous molten

salt experiments. The goal of these tests was to reduce uncertainties concerning the performance of untested components and operating procedures (e.g., cold filling the receiver or piping, and thawing a frozen panel.)

We conducted these tests to address concerns by the Solar Two Technical Advisory Committee - a committee of utilities, industries, the U.S. Department of Energy, and Sandia National Laboratories overseeing the technical issue of the Solar Two Project. The technical needs and concerns were prioritized, and a test program was developed. Consequently, some issues, such as thermal cycling of full scale valves, could not be implemented. However, this test program did address all the high priority issues.

II. System Description

The experiments were conducted with an existing molten salt loop initially built for a direct absorption receiver [3]. It was modified to accommodate two wing panels (fabricated by Foster Wheeler Corporation) removed from a salt-in-tube receiver (the Category B receiver) to evaluate a cold receiver startup procedure and conduct freeze/thaw experiments. Each panel consists of two serpentine flow passes which have six 1 inch (2.5 cm) OD 304 stainless steel tubes with 0.065 inch (1.65 mm) thick walls. The two passes are connected to a common 6 inch (15 cm) diameter manifold (schedule 80 piping) at the top of the panel. Each panel vent connects to a common 1 inch vent line, in which a hand valve is located to vary the venting flow rate. The experiment was located at the base of the Solar Tower at the National Solar Thermal Test Facility in Albuquerque, NM. Figure 1 is a schematic of the system and the wing panels. Figure 2 is a photograph of the panels and flow loop.

In this flow loop, salt is pumped from the salt sump, through the components, then either returned to the sump or diverted up the riser. At the top of the riser is the pressurized accumulator (surge) tank. The flow goes through the down comer, and can either be diverted to the panel or a manifold. The outlet of the panel flows into the manifold. The manifold drains into two calibration tanks. Flow from the calibration tanks returns to the sump. The pump can flow salt at 100 gallons per minute (380 liters/min) through the 2 inch (5.1 cm) piping.

We added flanges, a check valve, flow meters, and pressure transducers to test their performance. Three types of flanges were tested: 1) clamped, compressive metal-seal type flanges made by Reflange (R-CON) and by Grayloc, 2) bolted, compressive metal-seal flanges (E-CON) also made by Reflange, and 3) a standard ANSI ring-joint flange. The check valve, manufactured by Reflange (V-CON), was a spring-loaded, swing-type check valve. Two types of flow meters were tested: 1) vortex shedding flow meters made by Engineering Measurements Company, and 2) ultrasonic flow meters (wetted type and clamp on type transducers) manufactured by Panametrics. In addition, we installed pieces of performed fiberglass insulation to determine their viability as another insulation material. This insulation is easier to install than the wool blanket or calcium silicate insulation previously used. Its upper temperature limit is approximately 850°F. Table 1 lists the components we tested.

Although we were not able operate the flow loop at the pressures expected to be encountered in the cold side of a typical molten salt system, we were able to simulate operational and thermal cycling expected on the cold side of the system where the thermal ramp rates and stresses are typical of nightly conditioning. The ramp rates on the hot side of a molten salt system (down stream of a receiver) are very difficult to simulate with the existing loop, and therefore were not simulated with this test setup.

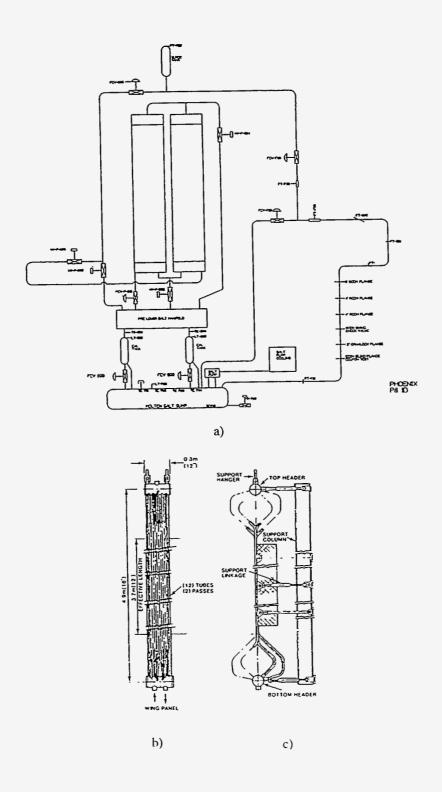


Figure 1. Flow schematic of the system (a) and a wing panel front (b) and side view (c).

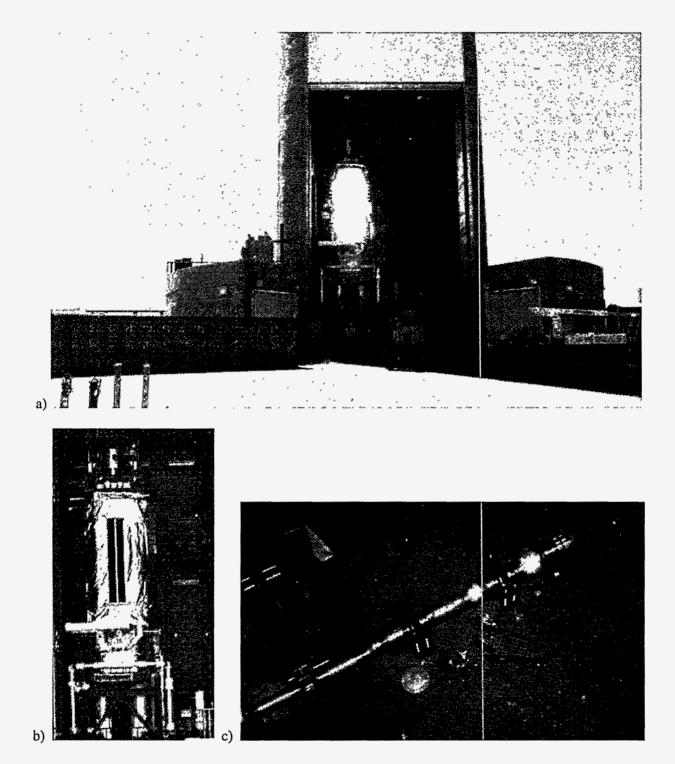


Figure 2. Photographs of molten salt panels (a and b) and flow loop test section (c) at the base of the Central Receiver Test Facility at Sandia National Laboratories.

Table 1. Components and instrumentation tested in molten salt loop.

Component or instrumentation	Туре	Size	Manufacturer
Flange	Clamped, compressive metal seal type	2 inch and two 4 inch	Reflange (R-CON) and Grayloc (2 inch)
Flange	Bolted, compressive metal seal type	6 inch	Reflange (R-CON)
Flange	ANSI ring type flange	4 inch	standard
Check valve	Spring loaded swing	3 inch	Reflange (V-CON)
Flow meter	Vortex shedding	2 inch	Engineering Measurements Co.
Flow meter	Ultrasonic - wetted transducer	2 inch	Panametrics
Flow meter	Ultrasonic - clamp on transducer	any sized pipe up to 10 feet dia.	Panametrics
Pressure transducer	High temperature Impedance	0-250 psi range	Kaman

III. Test Results

Cold Fill Tests

Cold filling involves flowing molten salt through piping or the receiver when all or part is below the salt freezing point. Cold filling has several advantages in the operation of a plant that experiences cyclic operation. If the molten salt can flow through parts of the system which are below the freezing point, parasitics could be reduced, since the heat trace would not have to be used on those lines. In addition, the operation of the plant could be more flexible if the plant could be brought on line faster by not having to wait for the heat trace to heat the lines to operating temperatures resulting in increased availability. Also, during morning startup, it is difficult to uniformly preheat the entire receiver. Some spots will experience much more heating than others due to non-uniform flux profiles from heliostats. This is a particular concern for the east side of a cylindrical receiver during morning start up. Localized convection will add to the problem. A roving aiming strategy, where the heliostat aim points are periodically changed, could provide more uniform heating of the receiver panels, thus avoiding severe hot or cold spots. Also, if the receiver can be filled with molten salt when areas of the receiver are below the salt freezing point, the receiver start up procedure would be much simpler, and could occur sooner. These strategies will boost performance and reduce operating expenses, resulting in lower energy costs. There are two major concerns with cold filling components and piping: freezing of the flowing salt, and transient thermal stresses.

We conducted cold fill experiments on the panels and on a section of piping. We measured the thermal response as the panel or piping underwent the rapid change in temperature, and estimated the heat transfer coefficients during this transition. We also derived expressions describing the transient stresses a pipe or tube will experience during a thermal shock. Using a correlation which describes the penetration distance of a liquid as a function of the fluid properties and flow conditions, we estimated the distance salt could flow through cold piping before freezing shut.

Results of Cold Fill Panel, Manifold, and Piping Tests. We conducted tests varying the initial panel temperature to determine whether salt could flow through all four passes of the panel before freezing shut. The flow velocity was approximately the same for each test, 2 ft/s (0.6 m/s). The purposes of these tests were to 1) determine if salt flow could be established in "cold" manifolds, panels, and piping, 2) measure the thermal responses of the tubes and manifolds undergoing thermal shock, and 3) estimate the corresponding stresses in the materials.

We conducted a series of tests trying lower and lower panel preheat temperatures ranging from 550 °F (288°C) to ambient before initiating salt flow. Next, we tried flowing salt through cold (near ambient) manifolds (heat trace off) with the panels preheated to 550°F. Then we tried flowing through cold manifolds and cold panels. Each scenario was repeated several times.

We found we were able to consistently flow through ambient temperature manifolds and panels without freezing salt or blocking tubes. In our test loop, we were able to fill the panels only in a serpentine fashion. To prevent entrapment of air, we had to fill the panel slowly (~2 ft/s, 0.6 m/s). Figure 3 shows the temperature response of the tubes and upper manifold as they are filled with 550°F (288°C) salt. The receiver tubes were initially at 50°F (10°C). The header was

Temperatures During Cold Fill

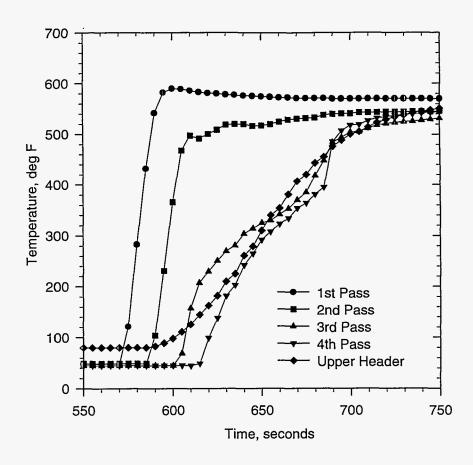


Figure 3. Temperature response of the cold receiver tubes and upper header as they are filled with 550°F (288°C) salt.

initially hotter than the panels, since an adjacent heat trace zone conducted heat to the header. The header and first pass receiver tubes experienced the greatest thermal shock. As the salt continued through the other passes, the temperature of the initial slug of salt decreased, resulting in the deposition of a frozen layer of salt on the tube wall, which reduced the shock, then melted away. This can be inferred from the change in slope of the fourth pass tube temperature and the upper header temperature. Figure 4 shows the temperature ramp rates of first, second, third, and fourth pass tubes. Note how the third and fourth passes show lower peak ramp rates. A frozen layer of salt is likely responsible for the reduced peak ramp rates, since as the initial slug of salt comes in contact with the cold tube surface, a frozen layer develops which limits the rate at which the temperature can rise, and provides some thermal capacitance. The outside tube temperature corresponding to the peak ramp rate in the fourth pass is approximately 395°F (202°C).

A thermal analysis was conducted on a receiver tube and header during this thermal shock, and is described in the Thermal Analysis section. The estimated heat transfer coefficients were calculated. In addition, calculations on the penetration depths—the distance a fluid flows through cold piping before freezing shut— are also discussed in the Calculation of Penetration Distances section.

Ramp Rates

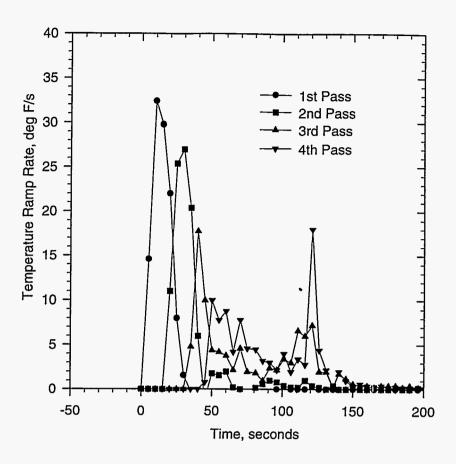


Figure 4. Temperature ramp rates of first, second, third, and fourth pass tubes.

The stresses in the receiver tube were calculated using the heat transfer coefficients obtained from the experiment. A stress model is described in the Transient Stress Analysis section. Stresses in the tube-to-header junction are more complicated, and are dictated by the temperature gradients at the transition.

In addition to cold filling the panels and manifolds, we conducted similar tests on a section of piping. We turned off the heat trace to a section of piping and let it cool to ambient, then initiated salt flow to determine its thermal response and estimate heat transfer coefficients and stresses. We measured the thermal response of an insulated 40 foot (12 m) long, 2 inch (5.1 cm) diameter 316 SS, schedule 40 pipe undergoing thermal shock. The piping was part of the riser. We turned off the heat trace, and allowed it to cool to ambient. When the piping was cold (at ambient), we pumped salt through it at approximately 9.5 ft/s (2.9 m/s) and measured the temperature outside of the pipe. Figure 5 is a plot of the outside wall temperature as a function of time. With this data, we calculated the heat transfer coefficient at the inner wall using a first eigenvalue approximation to an analytical solution of plane wall conduction. These procedures are discussed in the next section.

2" sch40 Pipe

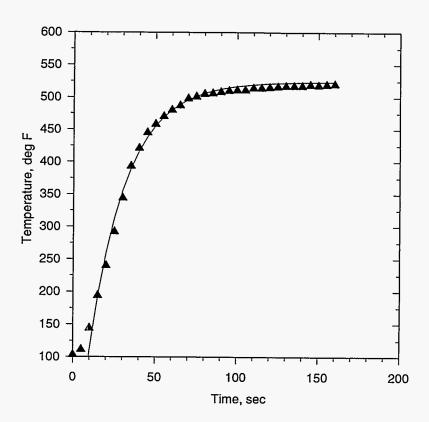


Figure 5. Outside wall temperature as a function of time of a 2 inch schedule 40 pipe undergoing thermal shock. The symbols are actual data points. The solid line is a fit of the data using the thermal model for Bi = 0.444.

Thermal Analysis During Cold Fill. In the cold-fill experiment on the panel, manifolds, and piping, we measured the outside wall temperatures as they are thermally shocked. From that data we wanted to obtain the inside wall temperature and the average heat transfer coefficient. The heat transfer coefficient allowed us to calculate the stresses developing in the wall of the pipe or tube as it rapidly heats up.

Assuming that the tube or pipe wall can be approximated as a plane wall, we can use an analytical solution to estimate the inside wall temperature and heat transfer coefficient. Since the receiver tube and piping have relatively thin walls, the plane wall assumption is a good approximation. In our tests, the outside of the pipe, manifolds, and the receiver tubes were insulated. (In actuality, only half of the receiver tube is insulated and the other side is exposed, but this should have minor bearing on the result, since initially the outside natural convective heat transfer to the air is relatively small, and the time scales are short for thermal shock.)

The solution to the energy equation for a plane wall suddenly subjected to a convection boundary condition describes the temperature distribution in the wall as a function of time [4]. Its form is:

$$\theta^*(x^*, t^*) = \frac{T(x, t) - T_{\infty}}{T_i - T_{\infty}} = \sum_{n=1}^{\infty} C_n \exp(-\lambda_n F_0) \cos(\lambda_n x^*)$$
 (1)

where the coefficient C_n :

$$C_n = \frac{4\sin(\lambda_n)}{2\lambda_n + \sin(2\lambda_n)},\tag{2}$$

Fo (the Fourier number) is the nondimensional time and x^* is referenced from the insulated surface:

$$Fo = \frac{\alpha t}{L^2}, \ x^* = \frac{x}{L}. \tag{3,4}$$

The discrete characteristic values (eigenvalues) of λ_n are the positive roots of the transcendental equation:

$$\lambda_n \tan(\lambda_n) = Bi = \frac{hL}{k}. \tag{5}$$

The length, L, is half the thickness of the plane wall since convection occurs on both faces, but in the case of a pipe or tube wall it is equal to the wall thickness, since one face has convection and the other is insulated. Note the midplane of a plane wall behaves like an insulated surface. The infinite series solution can be approximated by the first term in the series for values of $Fo \ge 0.2$. The solution becomes:

$$\theta^* = C_1 \exp(-\lambda_1^2 F_0) \cos(\lambda_1 x^*) \tag{6}$$

or

$$\theta^* = \theta_a^* \cos(\lambda_1 x^*) \tag{7}$$

where θ_o^* is the temperature at the midplane, $x^*=0$ (the insulated boundary, in our case the outside tube wall). The coefficients C_I and λ_I are determined from the equations 2 and 5. Since we measured the outside wall temperature (insulated surface) as a function of time and we knew the approximate salt bulk-fluid-temperature (initial salt temperature), we calculated measured values for θ_o^* and Fo. By iterating on λ_I until the calculated value of θ_o^* converged on the measured value of θ_o^* , we obtained the Biot number, Bi. From the Biot number we obtained the heat transfer coefficient.

The average heat transfer coefficients determined during the thermal shock for each pass, for the upper header, and for a 2 inch pipe are shown in Table 2. The solid line in Figure 5 is a fit of the data to the model for a constant heat transfer coefficient. Note that initially the temperature changes gradually (the first three data points). In order to get a good fit of the data with the model, the initial starting time of the model had to be adjusted, since the actual heat transfer coefficient is not constant with time. Assuming a constant heat transfer coefficient will yield higher stresses than one which gradually increases to its final value, and thus will be conservative. Stress analyses for an insulated circular pipe undergoing thermal shock are discussed in the next section.

For heat transfer in fully developed pipe flow when applied to freezing with turbulent flow, the following correlation has been suggested to estimate heat transfer coefficients between the fluid and the frozen layer [5]:

$$Nu = 0.0155 \text{ Re}^{0.83} \text{Pr}^{0.5} (R_{\circ}/R)^{0.83}$$
(8)

Table 2. Biot numbers and heat transfer coefficients during cold fill experiments.

Location	Approx. Velocity m/s	Bi (from data using the model)	h (from Bi) W/m ² K
2" sch40 Pipe	2.9	0.444	1700
6" sch80 Header	0.11	0.881	1200
First Pass Tube	0.67	0.296	2700
Second Pass Tube	0.67	0.243	2200
Third Pass Tube	0.67	0.124	1100
Fourth Pass Tube	0.67	0.114	1000

where R_o is the inner pipe radius and R is the radial coordinate of the frozen layer. This correlation is applicable beyond the thermal entrance length (approximately 10 tube diameters), and provides a conservative estimate of the heat transfer to the pipe, since the frozen layer will act as an insulator.

It should be noted that the heat transfer that occurs when the receiver is under high flux is quite different for a cold start scenario. A description of the heat transfer under high flux is presented in Appendix C.

Transient Stress Analysis of Piping and Tubes Undergoing Thermal Shock - Nondimensional Analysis. The stress calculations are important in determining the material behavior in a severe transient condition. For an insulated pipe, we can use the temperature distribution from the thermal analysis to calculate the circumferential, radial, and axial stresses. These thermal stresses should be superimposed on existing pipe loads due to structural factors. If the temperature is a function of the radial component only, then each component of stress is [6,11]:

$$\sigma_{\theta}(r) = \frac{E\alpha}{(1-\nu)r^2} \left(\frac{r^2 + r_i^2}{r_o^2 - r_i^2} \int_{r_i}^{r_o} T(r)rdr + \int_{r_i}^{r} T(r)rdr - T(r)r^2 \right)$$
(9)

$$\sigma_{r}(r) = \frac{E\alpha}{(1-\nu)r^{2}} \left(\frac{r^{2} - r_{i}^{2}}{r_{o}^{2} - r_{i}^{2}} \int_{r_{i}}^{r_{o}} T(r)rdr - \int_{r_{i}}^{r} T(r)rdr \right)$$
(10)

$$\sigma_{z}(r) = \frac{E\alpha}{(1-\nu)} \left(\frac{2}{r_o^2 - r_i^2} \int_{r_i}^{r_o} T(r) r dr - T(r) \right)$$
(11)

The temperature profile at a given time, Fo, can be found from Equation 7:

$$T(r) = \theta^*_{o}(T_i - T_{\infty})\cos(\lambda_I x^*) + T_{\infty}$$
(12)

The nondimensional length x^* is referenced from the insulated surface (the outside radius) and can be transformed into the nondimensional radial coordinates, $r^*=r/r_0$ and $r^*_1=r_1/r_0$, from:

$$x^*=(1-r^*)/(1-r^*)=(1-r^*)/\delta$$
.

In carrying out the integration, the stress components can be expressed in a nondimensional thermal stress format:

$$\sigma^*(r^*) = \frac{\sigma(r)(1-\nu)}{E\alpha(T_r - T_{co})} \tag{13}$$

Which for the three stress components are:

$$\sigma_{\theta}^{*}(r^{*}) = \frac{r^{*2} + r_{i}^{*2}}{1 - r_{i}^{*2}} \frac{\partial_{\sigma}^{*}}{2r^{*2}} \left\{ \frac{\delta^{2}}{\lambda_{1}^{2}} \left[1 - \cos(\lambda_{1}) \right] + \frac{\delta r_{i}^{*}}{\lambda_{1}} \sin(\lambda_{1}) \right\}$$

$$+ \frac{\delta^{2} \theta_{\sigma}^{*}}{\lambda_{1}^{2} r^{*2}} \left\{ \cos(A) - \cos(\lambda_{1}) \right\}$$

$$- \frac{\delta \theta_{\sigma}^{*}}{\lambda_{1} r^{*2}} \left\{ r^{*} \sin(A) - r_{i}^{*} \sin(\lambda_{1}) \right\} - \theta_{\sigma}^{*} \cos(A)$$

$$\sigma_{r}^{*}(r^{*}) = \frac{r^{*2} - r_{i}^{*2}}{1 - r_{i}^{*2}} \frac{\partial_{\sigma}^{*}}{r^{*2}} \left\{ \frac{\delta^{2}}{\lambda_{1}^{2}} \left[1 - \cos(\lambda_{1}) \right] + \frac{\delta r_{i}^{*}}{\lambda_{1}} \sin(\lambda_{1}) \right\}$$

$$- \frac{\delta^{2} \theta_{\sigma}^{*}}{\lambda_{1}^{2} r^{*2}} \left\{ \cos(A) - \cos(\lambda_{1}) \right\}$$

$$+ \frac{\delta \theta_{\sigma}^{*}}{\lambda_{1} r^{*2}} \left\{ r^{*} \sin(A) - r_{i}^{*} \sin(\lambda_{1}) \right\}$$

$$+ \frac{\delta \theta_{\sigma}^{*}}{\lambda_{1} r^{*2}} \left\{ r^{*} \sin(A) - r_{i}^{*} \sin(\lambda_{1}) \right\}$$

$$- \theta_{\sigma}^{*} \cos(A)$$

$$A = \frac{\lambda_{1}}{2} (1 - r^{*})$$

$$(17)$$

 $A = \frac{\lambda_1}{s} (1 - r^*)$ (17)

The characteristic value, λ_1 , is found from the solution to Equation 5 and is a function of the Biot number, Bi, which indicates the relative importance of surface heat transfer to conduction. Equations 14 to 16 are valid for $Fo \ge 0.2$. For smaller times (Fo <0.2), several terms in the series in Equation 1 must be used to calculate the temperature distribution. The temperature distribution is then used in Equations 9-11 to calculate the stresses. These equations can be used to calculate the transient stresses as a function of the Biot number and the pipe geometry. Figures 6, 7, and 8 show the nondimensional circumferential, radial, and axial thermal stresses as function of the nondimensional radius for several times (Fo) for a specific geometry. Note that in Figure 6 a skin stress develops at the inner surface. When the pipe is cold relative to the fluid—"up shock"—the stresses at the inner surface are compressive and tensile on the outer surface during the thermal shock. When it is hot relative to the fluid-"down shock"-the stresses are tensile on the inner surface. Figure 9 shows the effect of the Biot number on the stress distribution for a specific time. Figure 10 shows the nondimensional thermal (circumferential or axial) stress at the inner surface of the pipe as a function of time (Fo) for several Biot numbers using 30 terms of the series in Equation 1. When the heat transfer coefficient is large relative to the pipe thermal conductivity (large Bi numbers), there will be significant temperature gradients across the pipe wall and larger thermal stresses will develop during a thermal shock. At small Biot numbers, conductivity dominates relative to surface heat transfer and there are small thermal gradients across the wall

Circum. Stress vs Radius

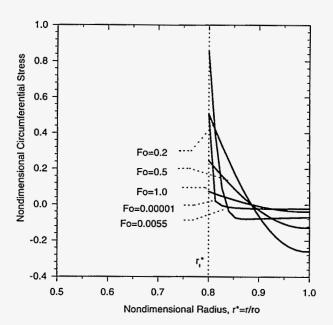


Figure 6. Nondimensional circumferential thermal stresses in pipe undergoing thermal shock as function of the nondimensional radius for several times (Fo) using thirty terms in of the nondimensional temperature equation (Eq. 1) for $r_i/r_o=0.8$ and Bi=100.



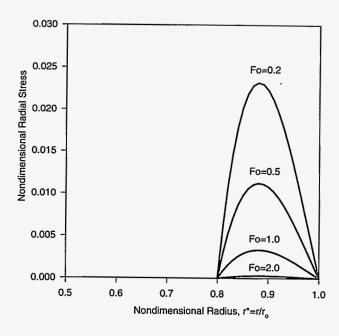


Figure 7. Nondimensional radial thermal stresses in pipe undergoing thermal shock as function of the nondimensional radius for several times (Fo) using thirty terms in of the nondimensional temperature equation (Eq. 1) for r_i/r_o =0.8 and Bi=100.

Axial Stress

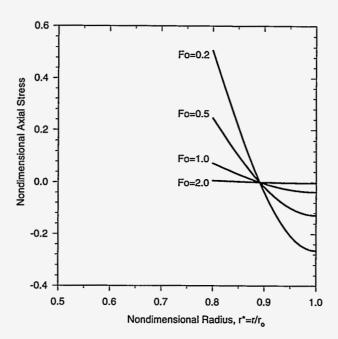


Figure 8. Nondimensional axial thermal stresses in pipe undergoing thermal shock as function of the nondimensional radius for several times (Fo) using thirty terms in the nondimensional transient temperature equation (Eq. 1) for $r_i/r_o = 0.8$ and Bi=100.

Effect of Bi

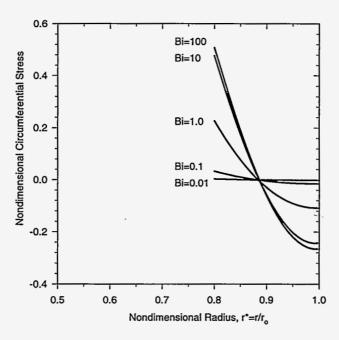


Figure 9. Effect of the Biot number on the nondimensional circumferential thermal stress distribution for a specific time (Fo=0.2) and $r_i/r_o = 0.8$.

Stress vs Time (Fo)

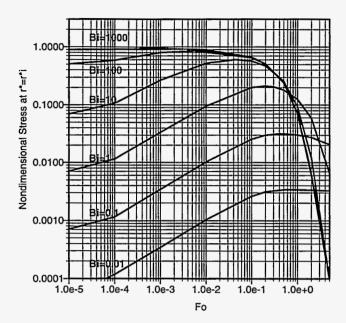


Figure 10. Nondimensional thermal (circumferential or axial) stress at the inner surface of the pipe undergoing thermal shock as a function of time (Fo) for several Biot numbers using 30 terms of the series in the nondimensional transient temperature equation (Eq. 1) for $r_i/r_o=0.8$.

resulting in small thermal stresses. The stresses build with time, reaching a peak, then finally drop as the wall reaches a uniform temperature. Each curve has a maximum thermal stress. These maximum stresses are shown in Figure 11 as a function of the Biot number. Figure 12 shows the time (Fo) when the maximum stress occurs as a function of Biot number.

From the data we gathered during the shock tests, we determined the Biot numbers are relatively small. We used these Biot numbers to calculate the stresses in piping or tubes we thermally shocked: a 2-inch schedule 40 316SS pipe, a 6-in schedule 40 304SS header and a 1-inch 0.065 inch wall 304SS receiver tube. Table 3 shows the maximum equivalent stress based on the maximum energy distortion theory of failure [7], sometimes referred to as the von Mises stress, for each case. In each case the stresses were calculated to be lower than the endurance limit of the material ($\sigma_e \approx 270$ MPa for stainless steel [8]) for these tests indicating that for the test conditions the piping itself can handle these stresses over the life of the system. It is likely these stresses are conservative, since the heat transfer coefficients are not constant, but gradually increase to the equilibrium value.

Maximum Stress vs Bi

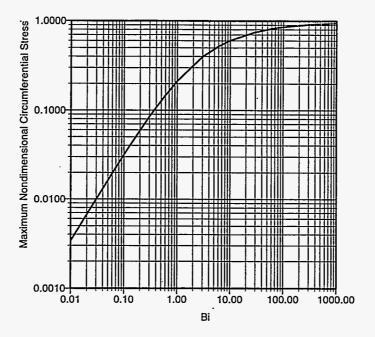


Figure 11. The maximum nondimensional thermal stress as a function of the Biot number for a pipe undergoing thermal shock for $r_i/r_o = 0.8$. These are the maxima of Figure 10.

Time When Max. Stress Occurs

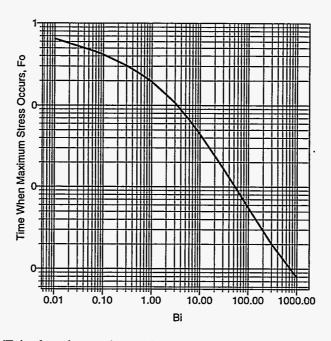


Figure 12. The time (Fo) when the maximum thermal stress occurs as a function of the Biot number.

Table 3. Calculated Maximum Stresses at the Inner Wall of Piping or Tubes Initially at 25°C Undergoing Thermal Shock with Molten Salt at 290°C based on the Biot Numbers from Experiments.

Pipe or Tube Size	σ _{Equivalent} , MPa
1 inch receiver tube, 0.065 inch wall,	-100
304 SS	
2 inch schedule 40, 316 SS	-140
6 inch schedule 80 header, 304 SS	-240

Using Equation 9, a conservative estimate of the peak circumferential stresses at the inner surface of a pipe or tube can be calculated as a function of salt velocity. Plots of these relations are shown in Figures 13 and 14 for 6 inch and 16 inch piping proposed for handling molten salt in the Solar Two and Commercial scale systems, respectively. There is a critical velocity at which the stresses exceed the endurance limit of the material. These velocities are listed in Table 4 for several pipe schedules and materials proposed for handling molten salt. Carbon steel is able to handle thermal stresses better than stainless steel, because carbon steel has a much lower coefficient of thermal expansion, even though its endurance limit is lower.

Thermal Stresses in 6" Pipe (Stainless Steel)

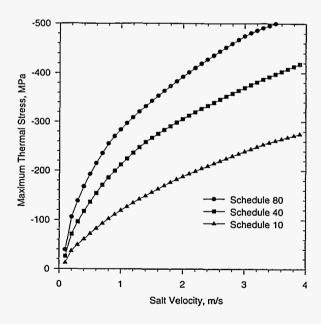


Figure 13. Maximum stress at the inside wall as a function of velocity for 6 inch piping.

Thermal Stresses in Stainless Steel 16 inch Pipe

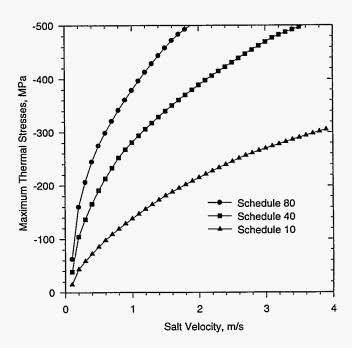


Figure 14. Maximum stress at the inside wall as a function of velocity for 16 inch piping.

Table 4. Maximum Velocities During Cold Fill Where Maximum Thermal Stresses are Below Endurance Limit of the Material for $T_{wall} = 25^{\circ}\text{C}$ and $T_{salt} = 288^{\circ}\text{C}$.

Pipe Size	Schedule	Material	Maximum Velocity, m/s
6 inch	80	Stainless 316	0.9
6 inch	80	Carbon	3.7
6 inch	40	Stainless 316	1.5
6 inch	40	Carbon	6.3
6 inch	10	Stainless 316	3.8
16 inch	80	Carbon	1.9
16 inch	40	Carbon	3.7
16 inch	10	Carbon	12.2
16 inch	10	Stainless 316	5.7

Even though the stresses in the walls of piping or tubes were low when thermally shocked in our tests, high stresses could develop where there are large loads already existing in the piping due to structural considerations, where there is a sudden change in wall thickness, or where there is abrupt changes in contour resulting stress concentrations. It should be noted this analysis applies only to vertical runs of piping or tubes where the temperature gradient is a function of the radial coordinate. In horizontal pipes, the leading edge of the fluid could have a sloped profile resulting in circumferential temperature gradient, in addition to the radial gradient. This would result in stress condition. Most of the piping in the risers and downcomers of molten-salt central-receiver solar power plants is in vertical runs.

For a receiver illuminated with high flux, the stresses are quite different from the stresses during thermal shock. In addition to a through-wall stress, there is a front-to-back tube stress. Appendix D shows the strain equations applicable to receiver tubes under high flux.

Calculations of Penetration Distances - Transient Freezing in Pipes. Another issue pertaining to cold starting piping is how far the molten salt can flow through a cold pipe before freezing shut. This length is known as the penetration distance. There are several models which describe transient freezing in pipes, but one model correlates data from several experiments and a variety of fluids into a single equation that describes the penetration depth as a function of the fluid properties, the Reynolds number, the wall temperature, and fluid temperature [9]. The correlation, Equation 18, describes the axial distance a fluid will flow through a cold pipe whose temperature is held below the fluid's freezing point before the pipe freezes shut. The wall temperature is held constant.

$$\frac{z}{D} = 0.23 \,\mathrm{Pr}^{1/2} \,\mathrm{Re}^{3/4} (\alpha_m / \alpha_s)^{1/9} [h_f / (Cp_s (T_f - T_w))]^{1/3} [1 + \gamma Cp_m (T_o - T_f) / h_f]$$
 (18)

The penetration depths were calculated for molten salt properties at several pipe diameters and flow velocities. These results are shown in Table 5 and in Figure 15. For large diameter piping, such as used with the riser or downcomer in the Solar Two central receiver power plant, we could theoretically flow through hundreds or thousands of feet of piping. In a commercial scale plant, we may be able to flow through *miles* of cold piping. We expect these values to be conservative, since the correlation was developed for a constant wall temperature.

Table 5. Penetration depths for molten salt for various pipe diameters, velocities, and salt inlet temperatures for a wall temperature $T_w = 68^{\circ}F$ (20°C).

Diameter	Flow Velocity	Salt Inlet Temperature	Penetration Depth
0.75 in	3 m/s (9.8 ft/s)	288°C (550°F)	39 m (129 ft)
0.75	1 m/s (3.3 ft/s)	288°C (550°F)	17 m (57 ft)
0.75	l m/s	371°C (700°F)	27 m (87 ft)
1.5 in	3 m/s	288°C (550°F)	132 m (435 ft)
1.5	l m/s	288°C (550°F)	58 m (191 ft)
1.5	1 m/s	371°C (700°F)	90 m (294 ft)
6 in	3 m/s	288°C (550°F)	1498 m (4920 ft)
6	l m/s	288°C (550°F)	657 m (2160 ft)
16 in	3 m/s	288°C (550°F)	8340 m (27400 ft)
16	1 m/s	288°C (550°F)	3660 m (12000 ft)

For the panel experiments described previously, we were able to flow through four passes and the associated headers and jumper tubes all at ambient temperature with a salt velocity of 2 ft/s (0.6 m/s). The total length of tubing is about 60 feet (18 m). The correlation predicts the fluid should freeze in about 50 feet (15 m). This means we were probably on the border of freezing.

Penetration Depths vs Salt Flow Rate

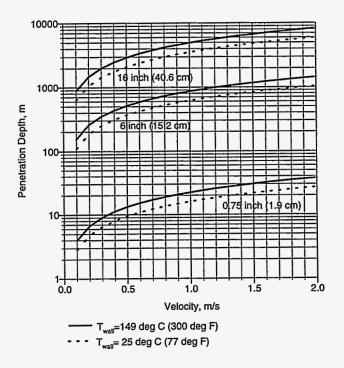


Figure 15. The penetration depths for several pipe diameters as a function flow velocity.

In addition, we were able to flow through over 155 feet (47 m) of ambient temperature (<100°F) 2 in piping without freezing the pipe shut. The correlation predicted we would be able flow at least twice that distance. It should be noted that the correlation was developed for piping that was submerged in a bath of fluid to hold the pipe outer surface at a constant temperature. In the cold fill tests described in the previous section, the piping or receiver tubing was not held at a constant temperature, but allowed to heat up. The correlation may be conservative, because an insulated pipe has a finite heat capacitance.

When tried filling the panels at lower velocities (0.4 m/s), we were not able to flow through all the passes. We detected salt in the second and part of the third pass, but it is unclearly whether the flow stopped in third pass due to freezing, or a systematic problem. The correlation predicted we should have frozen in the third pass. Unfortunately, we could not the verify the accuracy of the correlation very well with the panels, because they are connected with a common vent line which allows the flow to bypass the second and third pass and enter the fourth pass. We postulate that when the flow through the tubes in the second and third pass becomes restricted due to a buildup of a frozen layer of salt, the preferential path of least resistance is the bypass line. This could effectively cut off the venting of air through the second and third passes, resulting the panel becoming air bound.

In a report on the Molten Salt Electric Experiment of a receiver in the external configuration [1], experiments are described in which the receiver was started cold in a flood fill mode (all the panels in a receiver are filled from the bottom up). In two cases they succeeded in filling the panel, but in one case they froze part of it. For this case, the correlation predicts that salt would have barely made it through the 11.5 foot (3.5 m) high panel, which is consistent with the results.

The data are summarized in Table 6. (The flow rate was not given in the report, but was calculated from information about the system. The fact that third test in the series has a higher penetration distance than the second one may be attributed the uncertainty in the flow assumption and average panel temperature measurement.)

Table 6. Results for cold start experiments with the MSEE external receiver along with the correlation results. The panel height is 11.5 feet (3.5 m), tube diameter 0.62 inches (1.6 cm), salt flow rate approximately 0.4 ft/s (0.1 m/s).

Wall Temp	Salt Temp	Penetration Distance	MSEE Result
325°F (163°C)	700°F (371°C)	19.0 ft (5.8 m)	Fill OK
240°F (116°C)	650°F (343°C)	13.6 ft (4.2 m)	Fill OK
210°F (99°C)	700°F (371°C)	14.7 ft (4.5 m)	Partially frozen panel

For the Solar Two receiver designed by Rockwell, in order to prevent freezing, the receiver panels should be heated (with heliostats) to temperatures above 200°F (93°C) with headers and jumper tubes preheated with heat trace to the salt temperature, assuming the panels are flood filled at the design flow rate. The panels should be heated to at least 390°F (199°C) with jumper tubes initially at ambient temperature. These results are shown in Table 7.

Table 7. Estimated penetration depths for Rockwell's Solar Two receiver. Panel height is approximately 21 feet (6.4 m), jumper tube length: approximately 10 ft (3.0 m), tube inside diameter: 0.7145 inches (1.81 cm), salt velocity during flood fill: 0.87 ft/s (0.27 m/s).

Tube Temp	Penetration depth
10°F (-12°C)	18.35 ft (5.6 m)
100°F (38°C)	19.9 ft (6.1 m)
200°F (93°C)	22.4 ft (6.8 m)
400°F (204°C)	44.3 ft (13.5 m)

Summary of Cold Fill Tests

The following conclusions can be made about the cold fill tests:

- Cold filling the panel and/or manifolds is feasible. In normal operation it would not be necessary to cold fill the panel. As a minimum, our results show that the entire panel does not have to be above the salt freezing temperature before salt flow is established.
- Results from the stress analysis show that the stresses in the header and receiver tubes were below the endurance limit during a thermal shock. Analysis should be done for a particular design of the tube-to-header junction and transitions in piping cross section to make sure there are not any localized stress concentrations, and to estimate the life based on fatigue of these areas.
- The best combination of reduced parasitics and increased availability might be partial preheating (e.g., preheating to 300°F).

- We recommend that even if the piping is cold started, valves, flanges, and instrumentation should be kept near the salt temperature to minimize reliability issues that could arise if these components were thermally stressed.
- Our experience has shown that the most successful method for uniformly preheating the panels
 is to use a roving aiming pattern where the heliostat aim points change every few seconds to
 avoid localized under- and overheating.
- Although our results show that we can successfully flow through cold piping and tubes, care
 must be taken to avoid freezing of salt past slow leaking valves in unheated piping.

Freeze/Thaw Experiments

In a molten salt receiver, there are multiple drain valves. During the nightly shut down of the receiver, a drain valve might fail to actuate. If a valve fails to actuate once in a thousand times, a receiver—which has 14 drain valves—will fail to drain approximately once every two and a half months. That does not necessarily mean a panel will freeze that often. Only if this failure is not detected in time and corrective action (such as manually opening the valve) is not taken will the salt trapped in the associated panels freeze. Since the volume of salt increase when it goes from the solid to the liquid state for a fixed mass, damage can occur to the panel if the salt is thawed in a section of tubing or piping which is constrained at both ends.

The objectives of these tests were to determine the procedure required to thaw a receiver panel if it became frozen with salt, and to determine what amount of damage were done to the receiver tubes during the thawing process. A total of five freeze/thaw cycles were conducted. Prior to installation of the panels, all the tubes' outside diameters were measured at various locations along its length, so we could determine the permanent strain induced during the freeze/thaw tests. The freeze/thaw test procedures we used are described below.

First, we established flow in all tubes of the panels to allow the panels to reach thermal equilibrium. After flowing salt through the panels for several minutes, we shut off all drain and outlet valves to prevent salt from draining out of the panel. We then allowed the panels to cool so their temperatures' dropped below salt the freezing point. Figure 16 shows panel and header temperatures as they cool. Note how the slopes of the curves change at the salt freezing temperature, 430°F (221°C). When the salt becomes solid, the slopes change again. The header temperature is maintained above 460°F (238°C) by heat trace. The panels cooled to the salt's freezing point only 25 minutes after the pump stopped in the shielded environment of the solar tower. An exposed external central receiver (e.g., the Solar Two receiver) will cool much faster.

After the average panel temperature was less than 280°F (138°C), we opened the drain and panel outlet valves to empty the lower header of salt. Heat trace was kept on in the headers and on the jumper tubes to maintain the temperature above the freezing point. Once the headers had drained, we initiated thawing with heliostats. The only way for salt to leave the panel as it thaws is through the drain. Therefore, we started thawing from the bottom by putting on one heliostat and allowing it to heat that area of the panel to > 500°F (260°C). We continued to add heliostats, one at a time above the previous one, raising the panel temperature. One test was interrupted by weather and had to be continued the next sunny day. Once all thermocouple readings on the panel were above the salt freezing point, we tried to establish flow through the panel. On the first attempt, we were

Panel Freeze Test: 01/04/94

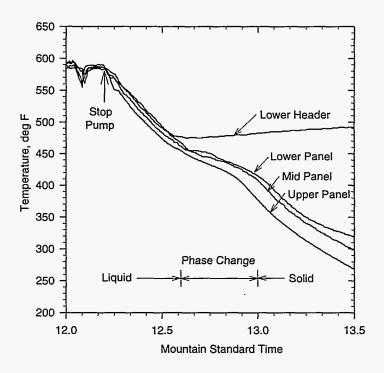


Figure 16. Temperatures receiver panels and header as they cool when filled with molten salt which freezes in the panel at approximately 430°F (221°C).

unable to flow though the majority of the panel because there were sections of tubes under the insulation where the heat trace could not heat it up enough, and we could not heat it with solar. In these regions we had to rely on conduction to melt the salt. Once we achieved flow through part of the panel we continued to flow salt, which helped thaw the frozen areas. After several hours we were able clear all tubes.

After two freeze/thaw cycles we measured the tube diameters. Plots of the permanent (plastic) strain as a function of the panel height are shown in Figure 17 for the east panel and 18 for the west panel. There did not seem to be any pattern to the damage. The maximum permanent strain induced in the tubes was over 4%. Figures 19 and 20 show the plastic permanent strain as a function of the horizontal location (tube number). The values of tube deformations are also shown in Table 8. Tubes 3, 4, and 5 in the east panel have much lower permanent strains than the other tubes in the panel. The west panel does not show this behavior. These results indicate the freezing phenomenon is complex, and requires further study.

Some observations and conclusions can be made regarding these tests:

- Thawing a frozen panel can require several hours, and could result in significant down time.
- The major problem with thawing the panel was a lack of sufficient heat under the insulation, particularly in the upper header where beneficial natural convection within the header oven cavity is not significant. It may be necessary to install additional heat trace in the regions where the insulation meets the panel to assure those areas can heat up to above the salt melting point.

East Panel Deformation

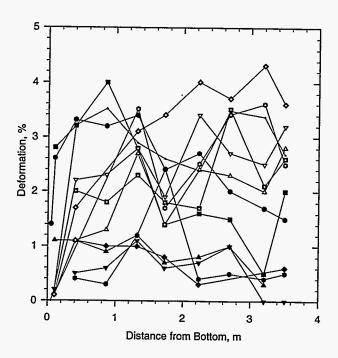


Figure 17. Permanent strain induced in the east panel tubes as a function of the panel height after two freeze/thaw cycles.

West Panel Deformation

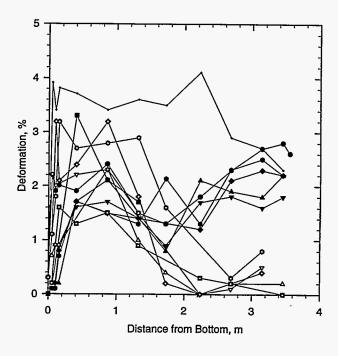


Figure 18. Permanent strain induced in the west panel tubes as a function of the panel height after two freeze/thaw cycles.

Side View: East Panel Deform.

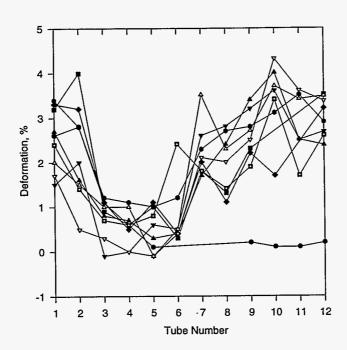


Figure 19. Permanent strain as a function of the width (tube number) for the east panel.

Side View: West Panel Deformation

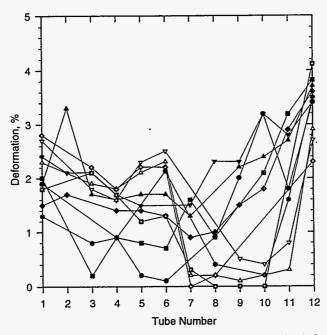


Figure 20. Permanent strain as a function of the width (tube number) for the west panel.

Table 8. Pre- and Post-Measurements of Tube Diameters in East and West Panel after 2 Freeze/Thaw Cycles.

Motten Salt Panel Deformation Measurements Pretest Measurements: 02/02/93 Post Measurements: 02/07/94-02/08/94

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1,321	11	52	1.001	1.035		1.000	1.028		0.997			0.998	1.009			1,010	1,000	1.000	1.012	1,200	1.002			0.999		2,703	1,001			0,997	1.028		0 997					
1.727	12	68	1,000	1.024	2.400	1.001	1,015	1.399	0.998	1,005	0.701		1,007	0.599	1.001	1,009	0.799	0 996		2.410	1.001		1.798	0.996		1,406		1.020	1,898	0.998	1.032	3.407	1,000			0.999		
1.727 2.235 2.692	12	88	0.999	1.026	2.703	0.999	1.015	1.602	0.997	1.005	0 802		1,007	0.700	0.999	1,002	0.300	1,000		0.400				0 998		2.405	1.000	1.034	3.400	0.998	1.038	4.008	0.997	1.022	2.508	1.007	1.031	2.383
2.692	14	106	0.998	1.018	2,004	0.999	1.014	1,502	0.999	1.009	1,001	1.000	1.010	1,000	1.001	1.000	-0.100	1,000	1.005	0.500	0.997	1.032	3 511	1,000	1.023	2.300	0.997	1.024	2.708	0.998	1.035	3,707	0.996	1.030	3.414	1,005	1.040	3 483
3,15	14 15	124	0 999		1	0,998			1.000			0.998			1.001			1,001			0.998			0.997			0.999			0,997			0.998	3		1.005		
3.2	16	126	1.001	1.018	1.698		1.005	0,500	0.999	1.002	0.300	0.998	0.998	0.000	1,001	1.000	-0,100	1.001	1.005	0.400	0,998	1.019	2,104	0.998	1.018	2.004	1,001	1.024	2,503	0,996	1.039	4.317	0.998	1.034	3.607	1.008	1.042	3,373
3.251			1,000			1,000			0.999			0,998			1,001			1.001			0.998			1,000			1,001			0.999			0.998			1.007		
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3.505	22	138	1,002	1.017	1,497			2 002	1,001	1.000	-0.100	1.000	1.000	0.000		1.005	0.601		1,003	0.501		1,025	2 603		1.025	2 808	1.000		3.200		1.035	3 604		1.026	2.498		1.033	2.684
3.556		140	1,002		11.407	0.998			1.000	- 11.000	-0.100	0 996	- 11000	0.000	0.999	-11000	0.001	0 999	11000		1.000	-1,020	2.000	0.997	11020		0.998			0.997	11000		1,000			1,003	- 111-1	
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Average Std De	<u> </u>		0.002								0.779	0.002	0.004			0.005			0.006	0.722							0.999							0.012				
Sid De	ř ·						1.041		1,001			1,002	1.010							2.410				1,000										1.034				
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	<u> </u>				1.401	0 997	1,005	1 0 500	1.0 997	1,000	•0.100	0.896	0,998	0.000	0.998	1.000	-0.100	0.996	1,003	0.299	0.997	1.0181	1,698	0 996	1,010	1.101	0.997	0,999	0.201	0.996	0.338	0.100	0.990	0.999	0.100	0.990	1.000	0 000
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bottom	Ь	ottom	W1 1	W1	W1	W2 inches	W2	W2	W3 inches	W3	W3	W4	W4	W4												W8				W10	W10					W12 \		
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0.051	2	2	1.001	1.023	2.198	1,000	1,001	0.100	0.999			0 998			1,000	0.999	-0.100	1,003	1,002	-0.100	1.001	1,003	0.200	0.993	1.000	0.705	0,996	1,018	2.209	1.000	1.011	1,100	0.998	1.009	1.102	0.996	1.035	3.916
0.051	3	4	1,000	1.019	1.900	1,000			1,000	0.999	-0.100	0.999	1.008	0.901	1,000	1.002	0.200	1.001	1.002	0.100	1.002		-0.200		1.002	0.906	1.000	1.020	2.000	1.003	1.035	3,190	1.001	1.019	1.798	0,998	1.032	3.407
0.152	4		0.998	1.018	2.004	0,999	0,998	-0.100	0.999 1.000 1.000	1.002	0.200	0.999		0.901	1.001	1.009	0.799	1,000	1.007	0.700	1.000	1.016	1.600	0,997	1.006	0.903	0.998			1.004	1.025	2.092	1.004	1.036	3.187	0.996	1.034	3.815
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0.406	9	16	1,000	1.019	1.900		1.032	3.303		1.014	1.705	0.996	1.012		0,997			0 998	1.015	1.703	1.001						0.999	1.021	2.202	1.003	1.027						1.034	
0.864	10 11 12 13		0.997	1.021	2.407				0.996	1.017	2.108	0.998		1.703			1.493				0 999				1.019				2.305		1.034				2.797			
1,321	11	52	1.001	1.016	1.499	0.999		1.702	0.995			0.997		1.404		1.013	1.401		1.013	1.300		1.008	0.901			1.000	1,000	1.015	1.500		1,019		1.001		2.897			
1.727	12	68	1.002	1.015	1.297	1,000			0,999	1.007		1.001	1.010	0.899	0.997			0.985		2.132			-0.100			0.400	1,000				1.004				1.600		1.036	
2.235	13	88	1.000	1.018	1.800	0.998			0,999	1.020	2,102		1.019	1.697	1.001	1.013	1,199	1.001		1.299		1.001	0 301			0,000				1.001	1.001				-0.100		1.038	
1,321 1,727 2,235 2,692 3,15 3,2	14		1.001	1.018 1.024 1.027	1.297 1.800 2.298 2.700	0.998 1.001 0.999			0.999	1.018			1.015	1.805	0.998		2.104	0.996	1.019		0,999				0.999		0.999	1.000				-0.100						
3.15	15		1,000	1.027	2.700	0.999			1.001	1,019	1.798	1.001	1.017	1.598		1,025	2,295		1.023	2.505	1.000	0.998	-0.200		1.017	-0.196	1.001	1.006	0.500		1,004	0.400			0.800		1.025	2.705
3.2	16		1,000			0.999			1.000			1.000			0.998			1.012			1.001		-	1.004			0.999			1.004			1.000		 	0.998		
3 251	17	128	0,999			1,001			1.000			0.999			0.998			1.015			1.002			0.999			1.000			1.003			0.999	'	 '	1,019		
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3.454	21	136	0.999	1.027	2.803	1.001 1.001 1.001			0.998	1.020	2.204	1,000	1.018	1,800		1.019	2.207	0.998	1.020	2.204		0.999	0.000		1.000	0 200	1,001	1.000	-0.100		1,000	-0.100		1.000	-0.100		1.021	2.305
3.505	22	138	1.000 0.998			1.001			0.996	. 1		1.001	- 1		0.998			1.001 0.998	!	-	0,999		!	0.998			0.999			1,000			1.000		 	0.996		
3 556	23	140	0,998	1.024	2.605	1.001			0.999			1.000	!		0.997			0.998		-	1.000			0.996			1.000			1.000			1.003	<u> </u>	<u> </u>	0 997		
					<u> </u>																																	
Average			1.000	1.020 0.006	1.978		1,011	1.185		1.013	1.413	0.999	1.013	1.432	1.000	1.013		1.001	1,012	1.415					1.006								1.001					
Std Dev		1.	0.001	0 006	0.676	0.001	0.014	1.402	0.002	0.008	0.880	0.002	0.004	0.384	0.002	0.008	0.823	0.006 1.015	0.008 1.023	0.929	0,001	0.007	0.694	0.006	0.007	0.716	0.002						0.001					
Average Std Dev Max Min	1		1.002	1.027	2,803	1.002	1.032	3 303	1.001	1.020	2 204	1.002	1.019	1.805	1.005	1.025	2.295	1.015	1.023	2.505	1.003	1.016	1.600	1.019	1.019	2.309	1.003	1.021	2.305	1,005	1,035	3,194	1.004	1,036	3,187	1.019		
Min	i		0.997		0 300	0 998	0.998	-0.100	0.995	0.999	-0.100	0 996	1.008	0 899	0.997	0.999	-0.100	0.985	1.002	-0.100	0.998	0 998	-0.200	0.993	0.999	-0.196	0 996	0.999	-0.100	0.998	0,997	-0.100	0.998	0 999	-0.100	0.996	0 999	0.100
Max ch	ange %=		4 112																																			

- Although we had over 41 thermocouples on the 24 receiver tubes and 4 headers, we were unable to determine where the blockages were. Even when all the thermocouples indicated that the temperatures were above the salt melting point, we still had plugs of salt. In the Solar Two and commercial receivers there will be even less instrumentation. If a panel becomes frozen, temporary thermocouples should be installed to monitor the panel temperatures more thoroughly. They could be mounted on the outside of the tubes. Another option is to monitor the temperatures with an IR camera.
- The heat trace should be designed to heat the headers and jumper tubes above 500°F within 10 hours when they are *full* of salt.

Component Tests

The main objectives of the component tests were to test unproven hardware and determine how well they perform in a molten salt environment, and to reduce uncertainties of the performance of untested components and operating procedures. Many of the flanges were tested in a molten salt environment, but additional information is required. Check valves were not tested previously in molten salt. The component tests were broken down into three areas: 1) check valve cycling, 2) slow thermal cycling of flanges, and 3) thermal shocking of flanges.

Check valves are needed at the pump outlet to prevent damage to the pump from the static "head" of salt when the pump stops, or to prevent pressure surges caused by redundant pumps on a common header when one pump stops. Serious damage to the pump can result if it is not protected from the strong inertial forces of the salt coming from the other pump and from the salt head in the riser.

It is desirable to use flanges that facilitate service of certain high maintenance components in molten salt loops. The flanges used in the molten salt pump and valve test loops were a constant source of salt leaks. The purpose of these tests was to test various other designs of flanges (e.g., tapered flanges or clamp type flanges) to measure how well they held a seal under thermal cycling, and to determine if it is practical to use flanges around the high maintenance components. We tested five flanges: a 2 inch Grayloc, two 4 inch R-CONs, a 6 inch E-CON, and a 4 inch ANSI ring type.

Check Valve Cycling. The purpose of the experiments with the check valve were to test their operation in a molten salt environment and to determine how to drain the salt from the check valve. A 3 inch spring loaded swing check valve was tested in a section of piping between flanges in the loop. Although we could not simulate the pressures expected to be encountered in cold side of a molten salt loop, we did simulate the flow velocities and the temperature cycles on the cold loop.

Figure 21 is a photograph of the check valve we tested (V-CON model manufactured by Reflange, Inc.). A drain hole was drilled in the flapper to allow a short section of piping downstream of the check valve to drain.

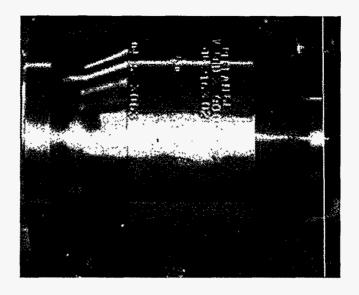


Figure 21. Photograph of the 3 inch check valve (V-CON model manufactured by Reflange, Inc.) tested in the salt loop.

In these tests we pressure cycled the check valve by flowing salt at the maximum flow rate approximately 100 gallons/min (380 l/min) and establishing pressure in the accumulator to 30 psi, then shutting a bypass valve (FCV 720) and turning off the pump. Shutting the valve before turning off the pump caused a momentary spike in the pressure, but assured the check valve would receive positive pressure on the downstream side of the flapper. We monitored the pressure decay in the accumulator tank. After waiting approximately 30 minutes to allow the pump motor to cool, we repeated the cycling. Figure 22 shows the pressure and flow as a function of time for several cycles. There were no problems with its operation after over 300 cycles (approximately 1 year of operation). The flapper was inspected after the 300 cycles, and found to be in good condition with no signs of wear.

Slow Thermal Cycling of Flanges. Flanges in a molten salt environment have been known to leak significantly after being thermally cycled [12]. It is desirable to use flanges to facilitate service of high maintenance components, such as the pumps, in molten salt loops. The flanges used in the molten salt pump and valve experiments were a constant source of salt leaks. We tested various flanges to determine how well they hold a seal under the slow thermal cycling expected during nightly shut down of the plant followed by morning preheat with heat trace. We slow cycled four flanges: a Grayloc 2 inch with clamp type connectors, two 4 inch R-CON flanges with clamp type connectors manufactured by Reflange, and one 6 inch E-CON bolted flange also manufactured by Reflange. The Reflange flanges have a unique metal gasket that is radially compressed (elastically) when the two faces are brought together, providing a tight seal.

Checkvalve Cycling

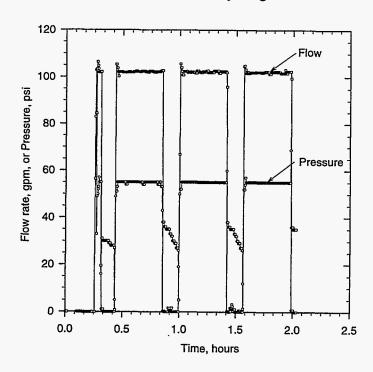


Figure 22. Pressure and flow as a function of time during a typical check valve cycle.

In these tests we simulated the nightly shut down and cooling of the components (assuming the heat trace were turned off) by using a fan and removing some of the insulation to enhance the cooling and match the temperature profiles we had expected to see in service at Solar Two. We cycled between 200 and 500°F. Each cycle took between six and eight hours. Figure 23 shows a typical slow thermal cycle. After approximately 180 slow thermal cycles, one of the 4 inch flanges started leaking very slightly. (We realized the torque on the bolts for the first 180 cycles was lower than the recommended value for the size of bolts we were using, and may have resulted in a less than optimum compression on the gasket.) We inspected all the flanges (we disassembled the two 4 inch flanges) and noticed they had all leaked to some extent, except the bolted 6 inch E-CON which showed no visible signs of salt. The bolted flange may provide a more uniform compression on the faces of the flange and gasket as compared to the clamp type flanges. See Figure 24. Since the salt is very wetting, it tends to get into cracks and seeps past gaskets, soaking and degrading the insulation. The continuous thermal cycling adds to its migration. Even though the flanges leaked a small amount (approximately 1 drop per hour), they would not likely fail catastrophically, since the gaskets are metal.

We retorqued the bolts to their recommended torque and continued the slow thermal cycling for an additional 120 cycles (a total of 300 cycles -- approximately one year of service) without any failures.

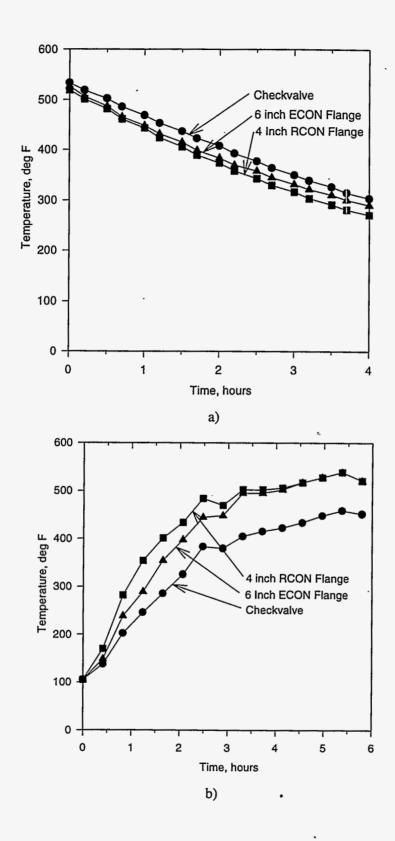


Figure 23. Typical slow thermal cycle of flanges simulating nightly cool down of components followed by slow heatup with heat trace.

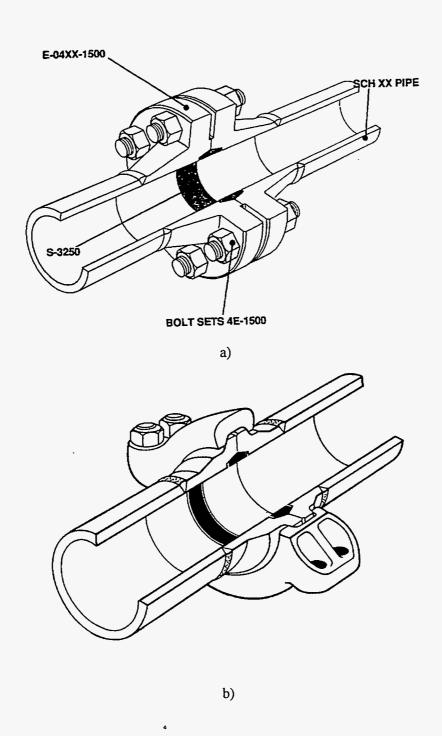


Figure 24. Schematic of a) ECON and b) RCON flanges.

Thermal Shocking of Flanges. The most severe thermal cycling a flange could experience in a molten salt system would be a thermal shock where the flange is at one temperature and it is suddenly subjected to salt at a different temperature. This situation could occur in one of two ways: 1) when the salt temperature at the outlet of the receiver suddenly drops due to a cloud transient, or 2) at startup if the flanges were at a temperature below the salt temperature. In the first case, the salt temperature transient could be from 1050 to 550°F (566 to 288°C) in approximately five minutes. In the second case, the flange could be as cold as ambient with the salt at approximately 550°F (288°C). This situation could arise if the parasitic power consumption were being minimized at nightly shut down by turning off the heat trace followed by cold filling of the piping. In our test loop we only simulated the second thermal shock case, since it would be very difficult to simulate the transient salt temperature at the receiver outlet. We conducted these tests at two initial flange temperatures either: 300°F or ambient (~100°F) with the salt at 550°F.

Prior to the start of the thermal shock tests we installed a 4 inch ring-type flange to test alongside the other flanges. In these tests we allowed the flanges to cool for several hours or overnight by lowering set point temperature of the heat trace or by turning off the heat trace completely. After the flanges had cooled to the desired temperature, we shock them by pumping 550°F salt through them. Figure 25 shows a typical temperature profile of the flanges and check valve during a shock.

Thermal Shock of Components

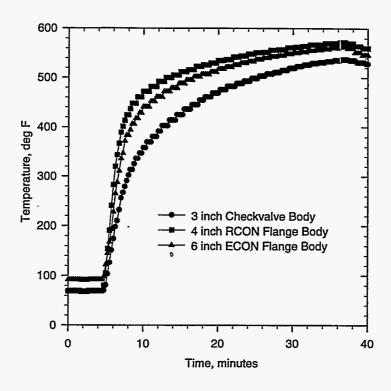


Figure 25. Typical temperature transient of the flanges during a shock.

After 25 cycles at 300°F, we inspected the flanges. There did not appear to be any visible breaches of integrity. We continued the thermal shocks with the flanges at ambient temperature. The flanges experienced 146 shocks without failure, although the flanges continued to leak at a very slight rate. After all these thermal shocks, none of the flanges failed catastrophically. With continuous operation and exposure to pressurized salt, all except one of the flanges showed only minor leaking (wetting between the interfaces of the flange faces or actually dripping of salt at a rate of approximately one drop per hour). The exception is the Grayloc flange which leaked significantly, enough to form a stalagmite of salt on the floor. Leaks over a long period of time can soak the insulation and increase the thermal losses. Exposure of salt to heat trace can also cause an electrical short in the heat trace.

A finite element analysis was done on the 6 inch E-CON flange to determine the stresses that developed in this flange undergoing thermal shock with salt a 550°F and the flange either initially at 77°F (25°C) or at 300°F (149°C). The details of this analysis are included in the appendix. There were two areas of concern in the flange where the stresses reached a maximum: 1) at the interface of the two flange faces at the outer most radius, and 2) on the inner surface of the flange adjacent to the gasket. The stresses developed at the interface between the two flange faces during either initial condition (77 or 300°F) were highly localized and were in excess of the yield for the material, but a chamfer exists at this location. The actual stress should be much lower with the chamfer, so that region is not a concern. On the other hand, the stresses in second region are in excess of the yield when the flange is shocked from an initial temperature of 77°F (25°C) but not in excess when shocked at 300°F (149°C). Based on this analysis, we recommend that flanges are preheated at least to 300°F (149°C) prior to initiating salt flow.

These flanges are an improvement over the flanges used in the pump and valve test loops which were raised-faced flanges with a Flexitalic type gasket. Those flanges tended to leak severely under cyclic conditions.

Our observations and recommendations regarding these flanges are:

- The flanges held up remarkably well to the conditions to which we subjected them. There were no severe failures. The majority of the salt leaks were very slight.
- Flanges should be minimized in a salt system. They should be used only for removal of high
 maintenance equipment such as the pumps, if at all. All welded construction is preferred,
 especially on hot loops.
- If the piping is cold started, the flanges should be preheated to at least 300°F (149°C) prior to flowing salt through them.
- The flanges tend to seal better if they are not thermally cycled.
- Hot retorquing the bolts periodically may reduce the leaks.
- Heat trace zones should be designed so that flanges and valves are not part of the same heat trace circuit as the rest of the riser or down comer, so that cold starting the rest of the piping can be done.

Instrumentation Tests: Flowmeters and Pressure Transducer

Flowmeters. Flowmeters were a considerable source of problems in previous molten salt experiments [2]. For example, the Category B receiver used venturi type flowmeters with differential pressure transducers using silicone oil as an intermediate fluid to measure flow. The

pressure transducers had problems with silicone oil volatilizing at the cold salt temperature. In addition, venturi flowmeters only have a range of about 4:1. Because of the limited range and silicone oil problems, we investigated other designs of flow meters that could be more reliable, provide higher accuracy, and have a greater range.

We chose to test two types of flowmeters: vortex shedding and ultrasonic. These flowmeters were selected because they are common, commercially available products which can withstand the temperatures we expected to encounter in the cold side of a salt system. The vortex shedding flowmeter has wedge in the flow field and senses oscillations of the vortices which are shed from the wedge. The frequency of the oscillations is proportional to the flow rate. The ultrasonic flowmeter sends a sound wave through the moving fluid from one transducer to the other, with and against the flow. It measures the time difference between the traverses. We tested two types of ultrasonic flowmeters: a wetted type where the transducers actually send the sound wave directly into the fluid, and a clamp-on type where the transducers simply mount on the outside of the pipe and propagate the sound wave through the pipe wall. The vortex shedding flowmeter we tested was manufactured by Engineering Measurement Company, and the ultrasonics by Panametrics. Both have temperature limitations and are only rated for the cold side of a molten salt system. The ultrasonic flowmeters were calibrated with water at the factory prior to installation in the salt loop. The vortex shedding flowmeters had been calibrated under the Direct Absorption Receiver Program.

We have operated the flowmeters since the beginning of this test program. The first clamp-on transducers were not made for the cold salt temperatures and their bodies (made of a "high" temperature phenolic material) melted. The manufacturer replaced them with all metal transducers. We also experienced some problems with the cables to the wetted transducers. Once we worked through the bugs in the hardware and programming, the ultrasonic flow meters worked reasonably well. The clamp-on flowmeter uses a petroleum couplant between the transducer and the pipe wall which allows the sound wave to penetrate through the pipe and into the fluid. After approximately a week or two of intermittent service at the cold salt temperatures (above 500°F), the couplant dried out and caused inaccuracies in its readings. A new application of couplant restored the contact between the transducer and the pipe wall.

A comparison between the flowmeters is shown in Figure 26 during a varying flow condition. The vortex shedding responds much faster and stabilizes better to changes in flow rate. For control purposes, the vortex shedding would be the preferred flowmeter. The ultrasonic flowmeter took some time to tune and to get operating properly, partly due to the faulty cable. By changing the parameters (such as the number of samples it averages for a reading) in the software of the electronics for the ultrasonic flowmeters, we were able to change its response.

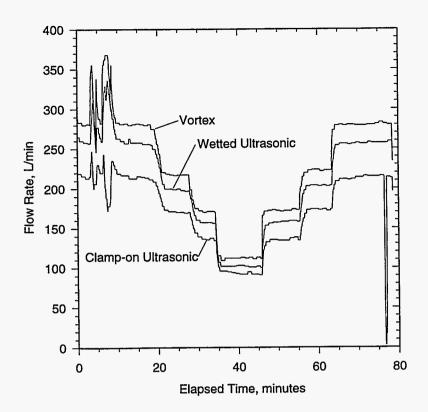


Figure 26. Response of vortex and ultrasonic flowmeters during a varying flow condition.

The flowmeters were compared with calibration tanks in the salt loop. Since the volumes of the calibration tanks are essentially constant with time, and the accuracy of the bubbler level measurement devices is good (\pm 3.8%), we chose to compare the flowmeters with the calibration tank flow.

The uncertainty of the flow measurement has two components: the bias (also called systematic) errors and the random errors [10]. The bias errors affect each measurement the same amount (at a given condition) and represent the offset from the "true" value. Random errors are the errors that change in a random fashion with repeated measurement. The random errors are not correlated with each other, and their limit can be measured if several data points are taken. Since the true bias and random errors are not known, their estimates are approximated by limits of each. The bias limit equals the square root of the sum of squares of each elemental bias limit (b_i) :

$$B = [\Sigma b_i^2]^{1/2} \tag{19}$$

The random limit equals:

$$S = \left(\frac{t_{95}S_x}{\sqrt{N}}\right) \tag{20}$$

where t_{95} is the Student's t statistic at 95% confidence, S_x is the standard deviation of the data set, and N is the number of data points [10]. For the root-sum-square uncertainty model, the uncertainty is found by combining the bias and random limits as follows:

$$U_{RSS} = \pm \left[B^2 + S^2 \right]^{1/2} \tag{21}$$

This model provides an interval around the test average that will contain the true value ≈95% of the time. In the flow tests, the flowmeter readings were compared with a reference—the calibration tanks. The bias errors relative to the reference can be measured. However, the reference (the calibration tanks) also has bias errors which we could not measure.

Table 9 lists each bias error source and estimated magnitude for the calibration tank flow measurement. The calibration tanks use bubblers to sense level. The amount of time to fill between two levels in each tank is measured and the flow rate calculated. Since the volumes of calibration tanks were not measured when the Panel Research Experiment was fabricated, exact volumes are not known. However, the dimensions were determined from drawings of the tanks. The volume was calculated, accounting for an overflow standpipe. Even if the tanks have significant amounts of eccentricity (5% change in the diameter) causing the tank to become elliptical, the volume of each is not significantly affected (it changes by less than 0.5%). Other bias sources of errors are thermal expansion of the tank volume between ambient and 550°F, salt density variations due to temperature, and the bubbler calibration.

Table 9. Bias Limit Sources for Calibration Tank Flow Measurement.

Error Source	Magnitude
1. Tank Eccentricity (tank cross section is elliptical: minor axis is 95% tank radius, major axis 105% radius).	0.5%
2. Tank Thermal Expansion (change in tank volume from	1.5%
ambient to 550°F).	1.370
3. Salt Property Variations (change in density and thus level between 550 and 650°F).	1.8%
4. Bubbler Calibration (approximately 0.5 inch in 18 inches).	<u>3.0%</u>
Total Bias Limit Calibration Tank Flow (Root Sum Square)	3.8%

The flowmeters were compared with the calibration tanks at several flow rates. Starting at 100% flow, we allowed the flow to stabilize, then closed the drain valves to the calibration tanks. The bubblers measured the level in each tank as a function of time. The elapsed time for the salt to fill the tank between the lower and upper level settings is measured in each tank to calculate the flowrate. The total flowrate is the sum of the two calibration tank flows.

Figure 27 shows the results of the comparison of the flowmeters against the calibration tank flowrate. Each data point represents the average of several readings during the calibration run. Figure 28 shows the measured bias errors (relative to the calibration tank flowrate) for each flowmeter as a function of flow. The bias errors represent the systematic errors in the measurements. Note how the bias errors are a function of the flow rate. The implication of this dependency is that calibration constant for each flow meter is off by a fixed percentage. The random errors are shown in Figure 29. The random errors were calculated from the data using Equation 20. The random errors are quite small, indicating the flowmeters give consistent readings over the range of the flows tested. The root-sum-square uncertainties, U_{RSS} , for each flow meter as a function of flow rate are shown in Table 10. The U_{RSS} accounts for the bias errors of the reference source—the calibration tanks.

Flowmeter Calibration

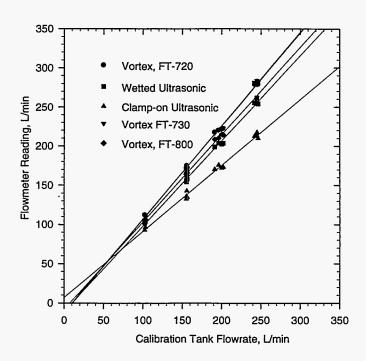


Figure 27. Comparison of the vortex and ultrasonic flowmeters against the calibration tank flowrate.

Bias Errors for Flowmeters

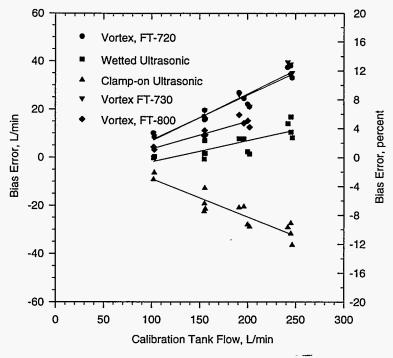


Figure 28. Measured bias errors (relative to the calibration tank flowrate) for each flowmeter as a function of flow.

Random Errors for Flowmeters

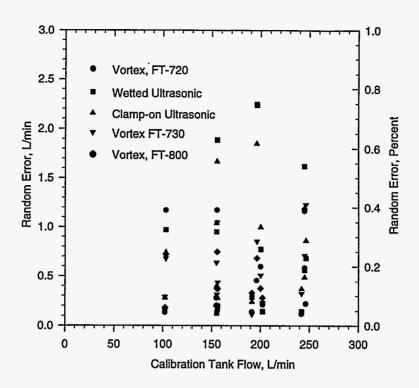


Figure 29. Measured random errors for each flowmeter as a function of flow.

Table 10. Root-sum-square Uncertainty (U_{RSS}) for Each Flowmeter.

Flowrate, L/min	Vortex, FT-720	Wetted Ultrasonic, PF-001	Clamp-on Ultrasonic, PF-002	Vortex, FT-730	Vortex, FT-800
102.6	± 9.8%	±3.9%	± 8.5%	± 9.9%	± 5.3%
155.4	11.6	4.2	12.8	11.6	7.3
197.4	12.6	4.6	13.0	12.5	8.5
244.6	15.1	6.4	13.3	15.6	

The large uncertainties observed are primarily due to the large bias errors. By periodically calibrating the flowmeters against a calibrated reference (such as calibration tanks or the cold surge tank of receiver with a *calibrated* bubbler - this is important), the majority of bias error limits can be calibrated out resulting in a root-sum-square uncertainty with a magnitude of the uncertainty equal to the calibrated reference. Overall uncertainties (U_{RSS}) of less than $\pm 5\%$ can be obtained with these flowmeters. The random error limits were much smaller and did not contribute significantly to the overall uncertainty under steady conditions.

Other observations and recommendations regarding flowmeters:

The vortex shedding flowmeter worked exceedingly well (very reliable) in the molten salt
environment and should be used whenever possible. The ultrasonic flowmeters were less
reliable.

- It is essential that provisions to calibrate the flowmeters in situ are designed into a molten salt system (e.g., <u>calibrated</u> level indicators in the cold tanks).
- For calibration purposes, the tank volume should be measured before installation and the bubbler must be calibrated.
- The clamp-on ultrasonic flowmeters are useful for temporarily (< 1 week) measuring flow in areas where there is no flow measurement or to verify flow measurement of an existing flowmeter and where the effort or expense and down time does not justify installation of a welded in flowmeter. During the check out phase of the receiver and salt system or during performance monitoring may be the time when clamp-on ultrasonic flowmeters could be useful on a very temporary basis or as a temporary backup if one of the permanent flowmeters were to fail and the plant was ready to run.
- The flow rate only needs to be measured on the cold side. There should be no need to measure flow on the hot side.

Pressure Transducer. We have tested an impedance-type pressure transducer and a NaK-filled pressure transducer in the salt loop to determine how well they work in molten salt. The silicone oil used in pressure transducers in previous molten salt tests tended to volatilize. The NaK-filled pressure transducers made by Taylor worked well in the pump and valve loop once snubbers were used to eliminate pressure pulsations which fatigued the membrane. Unfortunately, NaK-filled pressure transducers are difficult to find anymore. The impedance-type pressure transducer we tested in our loop is made by Kaman, and is good for temperatures up to 1200°F. It senses small displacements in its membrane and correlates them to pressure. It is self temperature compensating. Although we don't have any method to calibrate the pressure transducers in our system, the impedance-type pressure transducer was calibrated at the factory at 550, 750, and 1050°F. The impedance-type pressure transducer in our loop experienced the same thermal cycling and shock as the flanges, and did not fail or give erroneous readings. The pressure measurement in Figure 22 was from the impedance-type pressure transducer.

Comments regarding pressure transducers:

- The impedance-type pressure transducers work well but are expensive (~\$5k each).
- NaK-filled pressure transducers are hard to find.
- To keep instrumentation costs down, minimize the number of salt pressure measurements needed.
- The pressure transducers should be oriented so the salt can drain from them. Experience from previous molten salt experiments has shown, that if salt is allowed to freeze on the membrane, then thawed, the thawing process causes the membrane to rupture.

IV. Ongoing and Further Research

The work conducted so far has answered many of the questions regarding how far salt can flow through cold pipes during a cold fill scenario and the thermal stresses that develop when components and piping are thermally shocked, and some of the effects of freezing and thawing. We have also tested instrumentation that are an improvement over previous instruments. Ongoing and further research is directed towards understanding the freeze/thaw phenomenon, validating transient freezing models, and testing improved components and instrumentation. A description of each of these follows.

Simple Element Freeze/Thaw Tests (Ongoing)

A two-chamber oven was built to investigate the salt freeze/thaw phenomenon in typical receiver tubes. The purpose of the simple-element freeze/thaw experiments is to quantitatively measure in a controlled setup the permanent deformation inflicted to samples of receiver tubes undergoing freezing and thawing. When nitrate salt changes from the solid to the liquid phase the volume increases, causing an expansion of a given mass of salt. During the expansion process, the tube material can yield resulting in a plastic deformation of the tube material. In these tests, several receiver tubes of various diameters and wall thicknesses filled with nitrate salt undergo several freeze/thaw cycles to measure the deformation of tubes. Preliminary results indicate under the most severe case (freezing the lower half of a tube, then freezing the upper half, followed by thawing the lower part with a stop in the upper half to prevent sliding of the solid salt) the tubes will rupture after 12 cycles.

Ball Valves Test

Ball valves are desirable for use as drain and fill valves because they are relatively compact and in the fully opened position the flow restriction is small relative to other types of valves, such as globe valves. We have pressure cycled a 2 inch Mogas ball valve to assess its functionality and leak rate in a molten salt environment. The valve was closed and pressurized to 60 psi (410 kPa) for five minutes followed by flow for five minutes. After each 50 cycles, the leak rate was measured with the valve in the closed position and pressure on the valve. The amount of salt that leaks by was measured every 0.5 hour. After 300 cycles the leak rate was measured to be approximately 15 grams of salt per half hour.

Transient Freezing Experiments

The correlation for transient freezing in pipes used to calculate penetration depths is based on experiments where the pipe wall is cooled externally to maintain a constant wall temperature. In reality, pipes have a finite heat capacitance. The effects of the pipe heat capacitance on the penetration depths for molten salt penetration depths is an area that could be investigated further.

Impedance Heating System

For long runs of piping, impedance heating could have advantages over mineral insulated (MI) cable. With impedance heating, the pipe wall becomes the heater by passing a low A-C voltage (<80 volts) through it. One lead of the electrical cables is connected to the electrical midpoint of the pipe, and the other is divided in two, with each of these connected to an end of the pipe that is to be heated. The cables run on the outside of the pipe and are easy to access. We plan to test an impedance heating system in our salt loop.

Multiport Valve

A multiport valve allows flow from one line to be distributed to several lines. It has a single actuator to control the valve. A multiport valve could be used in place of several drain and fill valves, thus reducing the complexity associated with controlling and maintaining several valves. Although this valve is not a commercial product, a small company in Colorado (TedCo) has designed such a valve for molten salt applications. This type of valve should be investigated further.

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Appendix A. Finite Element Analysis of Flange Undergoing Thermal Shock

The following is memo written by Scott Rawlinson describing a finite element analysis of an ECON type 6 inch flange undergoing thermal shock at two different initial conditions: 25 and 149°C.

Sandia National Laboratories

Albuquerque, New Mexico 87185-1127

date: July 27, 1994

to: Jim Pacheco, MS-0703

Org. 6216

ocit Routin

from: Scott Rawlinson, MS-1127

Org. 6215 5-3137

subject: Finite Element Results for Salt Flange

To ensure the reliability of some aspects of Solar Two, you are concerned about stresses in several critical components, one of which is the flange coupling. As an alternate method of thermal conditioning at night, some of the salt line may be drained and allowed to cool. At startup these lines will be at ambient temperature or they will be preheated to a temperature below the salt freezing point and will undergo a significant thermal shock. The purpose of this memo is to document the finite element analysis (FEA) results on the flanges undergoing thermal shock that will be used in these molten salt loops.

I used the COSMOS/M finite element program to model the pipe flange. This program can be used on a PC and according to a survey done by our analysis group about three years ago, is one of the better FEA programs. The program has been continuously updated and improved since that time. I used the latest version, 1.70. The developers of this code, Structural Research and Analysis Corporation (SRAC), verify its results using numerous test case models.

The system being modeled is two E-CON flanges that are bolted together at 45 degree intervals. A step is machined into each of the mating flanges. A gasket is placed in this notch that is formed from these steps. The model was developed to determine: (1) stresses at steady-state conditions; (2) stresses that would occur if 290 °C salt suddenly flowed through this pipe connection without any heat trace (at ambient temperature); and (3) stresses that would occur if 290 °C salt suddenly flowed through this pipe connection after the flanges are preheated to 149 °C (300 °F). Therefore a transient solution is required for (2) and (3).

The envelope of the FEA model was developed from the sketch you supplied, using data from Reflange. Several iterations of the model were developed. The first model was developed in an older version, 1.65A. Then the newer version arrived, and although it did not contain any changes that should affect this particular model, I developed the model in the newer version. In addition, after knowing what loading would occur, I decided that gap elements should be placed between the flange and the gasket. Otherwise, the gasket would appear to be part of the flange, adding to its strength -- this would not be realistic. Only the results using the gap elements, separating the gasket from the flanges, will be presented.

A summary of the parameters in the FEA model is given below:

- Element type (for flanges and gasket): 4-node planar, "PLANE2D", axisymmetric
- Average element size: 2-mm
- Element type (gap between flange and gasket): 2-node "GAP"
- Force/pressure boundary conditions: 28,300 N at bolt hole location
- Flux/Temperature boundary conditions:
 - Convection along entire length of inner pipe
 - Convection coeff = 550 W/m²-K
 - Bulk fluid temp: 290 °C
- Displacement boundary conditions: Zero displacement in y direction at midpoint of gasket
- Flange material properties (SS316) [1,2]:
 - Modulus of elasticity: 193 GPa
- Poisson's ratio: 0.3
 - Coefficient of thermal expansion: 17.5 x 10⁻⁶ m/m-K
 - Density: 8000 kg/m³
 - Specific Heat at Constant Pressure: 505 J/kg-K
 - Thermal conductivity: 15.6 W/m-K
- Gasket material properties (17-4PH) [3]:
 - Modulus of elasticity: 193 GPa
 - Poisson's ratio: 0.3
 - Coefficient of thermal expansion: 12.1 x 10⁻⁶ m/m-K
 - Density: 7832 kg/m³
 - Specific Heat at Constant Pressure: 505 J/kg-K
 - Thermal conductivity: 12.1 W/m-K

Note: Material properties were taken as constant and were calculated at the average between an ambient temperature of 25 °C and the operating temperature of 290 °C.

The boundary conditions stated above require some explanation. Since the pipe flange is modeled axisymmetrically, the proper bolt load must be calculated. COSMOS/M assumes axisymmetric problems are based on one radian. Therefore the proper bolt load is:

$$F = F_b \frac{\#bolts}{2\pi}$$

The force in the bolt was given as 4000-5000 lb. from Bob Lathan at Reflange, Inc.. I used 5000 lb. = 22,242N, or an equivalent load of about 28,300N, using the above equation.

When I first developed the thermal model, I placed 290 °C boundary conditions (salt temperature) along the inside of the pipe. The resultant stresses were extremely high in this region. However, I realized that was not the proper boundary condition. The inside of the pipe will not instantaneously reach 290 °C -- it will reach that temperature much more slowly through the boundary layer. Therefore I re-analyzed the problem using convective boundary conditions.

The correlation I used to determine the convection coefficient is based on turbulent flow in circular tubes and is given as [4]:

$$\overline{h} = .023 \frac{k}{D} \operatorname{Re}_{D}^{4/5} \operatorname{Pr}^{0.3}$$

for

 $0.7 \le Pr \le 160$ $ReD \ge 10,000$ $L/D \ge 60$

where

k = thermal conductivity

D = pipe diameter L = pipe length

 $Re_D = Reynolds number$ Pr = Prandtl number

Using your stated flowrate of 100 gpm and using the properties of salt at 290 °C from [5], I calculated a convection coefficient of 552 W/m²-K

550 W/m²-K (the above assumptions were met). This number is very close to your calculated valve based on experimental results from the smaller pipe flange at time \geq 90 seconds.

Since the problem is transient in nature, a timestep is needed. The critical timestep is calculated as (information supplied by SRAC):

$$\Delta t_{cr} \leq \frac{2}{1-2\theta} \frac{\Delta x^2 \rho c_p}{k}$$

where

 $\Delta x = \text{smallest mesh size}$

 ρ = density

 c_p = specific heat at constant pressure θ = stability parameter

Using the values of material properties and stability factor to give the smallest possible stable timestep, I calculated a critical timestep of 0.86 seconds. I used a 0.5 second timestep in the analysis.

My assumptions in the analysis were as follows:

- Constant material properties (linear problem) (1)
- (2) Constant convection coefficient
- No external thermal losses (insulated)
- Bolt load does not change with time or temperature
- No friction at gasket/flange interface (it will become apparent later that this value is irrelevant)
- Flowrate = 100 gpm (6)

Steady-State Results (Ambient Temperature):

The results of the steady-state analysis for 25 °C are shown in Figures 1a through 1d. All stresses discussed below are Von-Mises stresses, a common stress criterion used to predict failure. Figure 1a illustrates the model's element mesh, force, and displacement boundary conditions. Two areas, regions A and B are also illustrated -- these will be referred to later. Figures 1b and 1c are exaggerated displacement plots. The pipe flanges tend to be clamped together due to the bolt loads. This plot appears to show that the gasket is separating from the lower pipe flange. However, remember that this is an exaggerated plot on a scale on the order of several hundred. I was concerned that the apparent non-symmetry indicated a problem, so I consulted personnel at SRAC -- they said that sometimes this happens in a deformed plot when the displacements are very small, resulting in a very distorted plot with the huge scale factor. This is what happened in this case. In fact, he checked the entire model and found no problems. Figure 1d is a Von-Mises stress plot of the center of the bolted connection. The maximum stress is 175 MPa, and occurs where the two flange bodies contact due to the bolt forces (region A). This stress is well below the yield point of SS316 at ambient temperature.

Transient Results for No Preheat:

Next, the convective boundary condition was applied along the inside of the pipe wall. Since the temperature distribution changes with time, the resultant stresses will also change. I examined the results at t = 0.5, 1, 5, 10, 20, 30, 60, 120, 180, and 240 seconds. To observe how the stress patterns develop with time, I included the results at t = 0.5, 5, 10, 30, 60, 120, and 240 seconds in Figures 2 through 8.

The maximum stress occurs at the same location as the steady-state results, but is higher due to the additive effect of the temperature or convective boundary conditions. Because the pipe is being heated from the inside of the pipe, this inner region expands faster than the outer region, which tends to compress the contact line even greater than with only bolt loads.

The following table summarizes the stresses in the two areas of concern:

Table I - FEA Results for Case Without Preheat

Time (seconds)	Von-Mises Stress, Region A (MPa)	Corresponding Temperature, Region A (°C)	Yield Strength, Region A (MPa)	Von-Mises Stress, Region B (MPa)	Corresponding Temperature, Region B (°C)	Yield Strength, Region B (MPa)
0.0	175	25	240	35	25	240
0.5	180	25	240	90	37	240
1.0	171	25	240	90	44	240
5.0	178	25	240	142	69	240
10.0	214	25	240	172	81	240
20.0	279	25	240	196	98	240
30.0	341	25	240	239	107	240
60.0	527	25	240	265	128	240
120.0	537	50	240	323	161	240
180.0	542	58	240	325	178	240
240.0	547	67	240	328	187	240

These results at the contact point (region A) indicate that the yield strength is easily exceeded. However, I asked if this was actually chamfered at this point. It turns out that it is, which would eliminate this high stress point. More of a concern is the stresses along the inner pipe adjacent to the gasket. For times > 30 seconds, stresses exceed the yield point in this region (the yield point is constant from 25-200 °C). Based on this, it is apparent that local yielding may occur if you thermally shock this bolted connection.

Notice that maximum stresses are nearly level at 240 seconds. As the temperature distribution evens out, the stresses will decrease and eventually return to the stresses with bolt loading only (since the expansion will be equal throughout the flange assembly). Therefore, the stresses at t= 240 seconds are about as high as can be expected.

Finally, I looked at any gap that may occur between the flange and gasket surfaces. There is a slight gap at t=240 seconds but is nearly undetectable -- less than $\cong 0.1$ -mm. Because of the effect of the bolt force and thermal loading, the gasket is never compressed. Any stresses in the gasket are only due to the thermal gradient. Because the gasket is never constrained, the coefficient of friction used is not relevant.

Transient Results with Preheat:

I re-ran the model assuming the entire flange was preheated to a uniform temperature of $149 \,^{\circ}\text{C}$ (300 °F). I examined the results at t = 0.5, 30, 60, 120, 180, and 240 seconds. The results are displayed in Figures 9 through 14. The following table summarizes the Von-Mises stresses in regions A and B.

Time (seconds)	Von-Mises Stress, Region A (MPa)	Corresponding Temperature, Region A (°C)	Yield Strength, Region A (MPa)	Von-Mises Stress, Region B (MPa)	Corresponding Temperature, Region B (°C)	Yield Strength, Region B (MPa)
0.5	177	150	240	18	150	240
30.0	266	150	240	133	193	240
60.0	361	150	240	145	204	240
120.0	454	162	240	182	221	≅ 240
180.0	495	170	240	198	230	≅ 240
240.0	504	180	240	202	235	≅ 240

Table I - FEA Results for Case Without Preheat to 149 °C

As with the case with no preheat, the highest stresses occurred at the point of contact between the two flange bodies. Again, this point was ignored because there is actually a chamfer at this location. The other area of concern, region B, has much more acceptable stresses. A maximum Von-Mises stress of 202 MPa occurs at t=240 seconds. The corresponding temperature at that point and time is approximately 235 °C. The yield strength of SS316 at this temperature point is nearly 240 MPa, therefore the stress level is acceptable. Note that as with the case with no preheat, the stresses have very nearly peaked and would begin to decrease with time to the levels of that in the steady-state condition.

Conclusions:

Based on these results of this model, it appears that local yielding may occur (without preheat) along the inner pipe adjacent to the gasket. It is possible that a full 3-D model may indicate otherwise, but it is not likely since the region in question is far from the bolts. Therefore, it is not recommended that this flange connection be thermally shocked from ambient conditions. However if heat trace is used to preheat the flanges to 149 °C (300 °F), the stresses would remain below the yield point of the material..

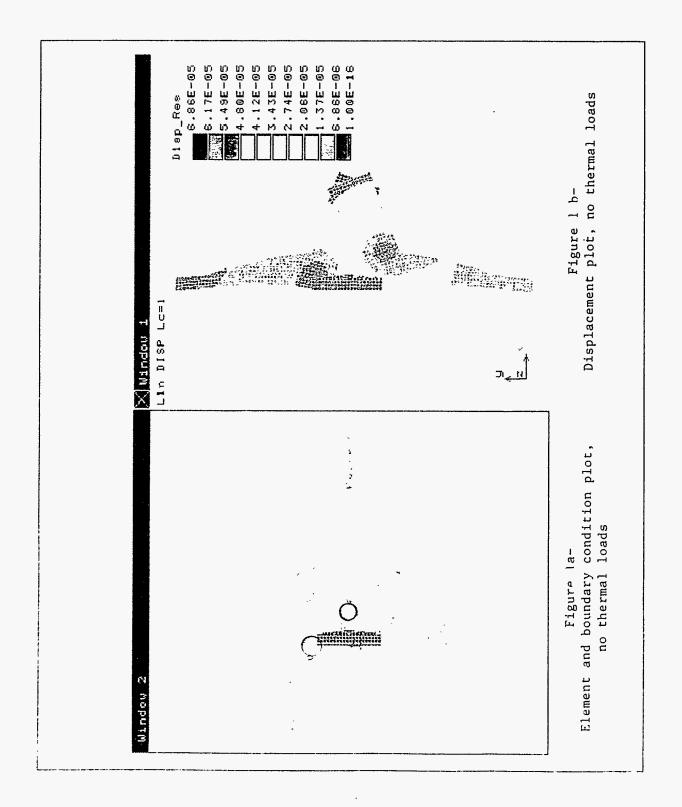
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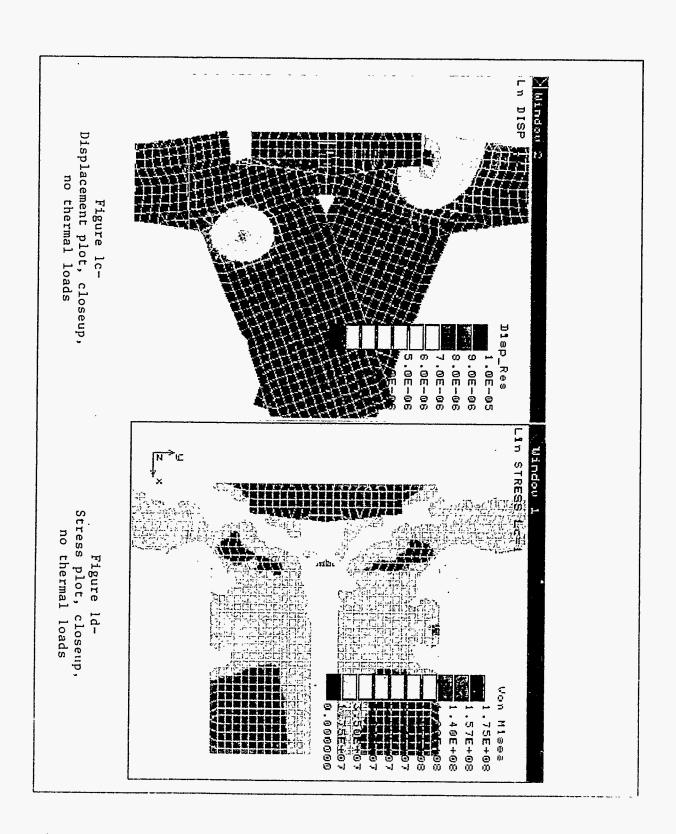
- 1. American Society for Metals, Engineering Properties of Steel, pp. 292-296, ASM, 1982.
- 2. Incropera, F. P., and DeWitt, D.P., <u>Fundamentals of Heat Transfer</u>, p765, Wiley, New York, 1981.
- 3. Kattus, J.R., Aerospace Structural Metals Handbook, code 1501, March, 1978.
- 4. Incropera, F. P., and DeWitt, D.P., <u>Fundamentals of Heat Transfer</u>, p406-407, Wiley, New York, 1981.
- 5. Smith, David C., Chavez, James M., <u>Final Report on Phase I Testing of a Molten Salt Cavity Receiver</u>, Vol II The Main Report, Table 2-II, p 2-4, SAND 87-2290, May 1992.

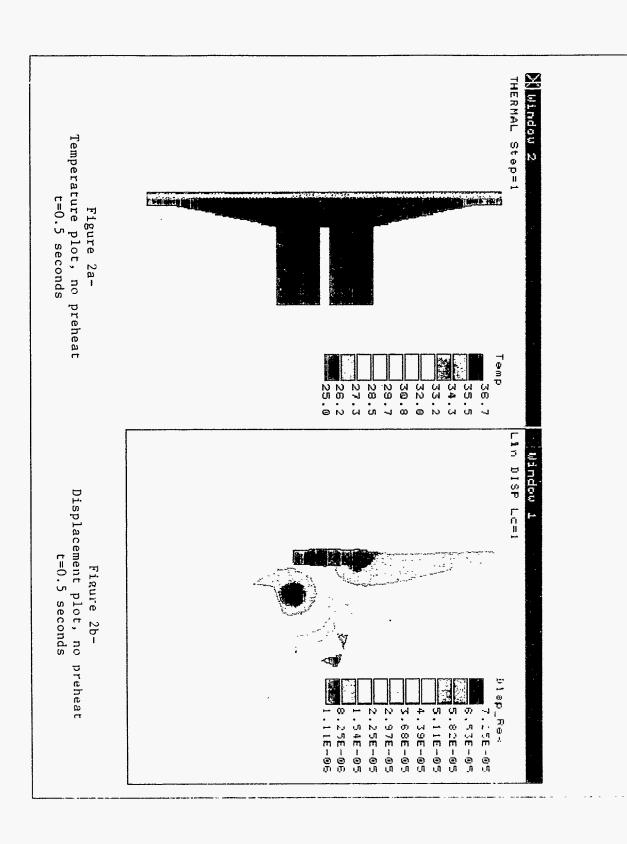
Attachments with all copies: Figures 1 through 14

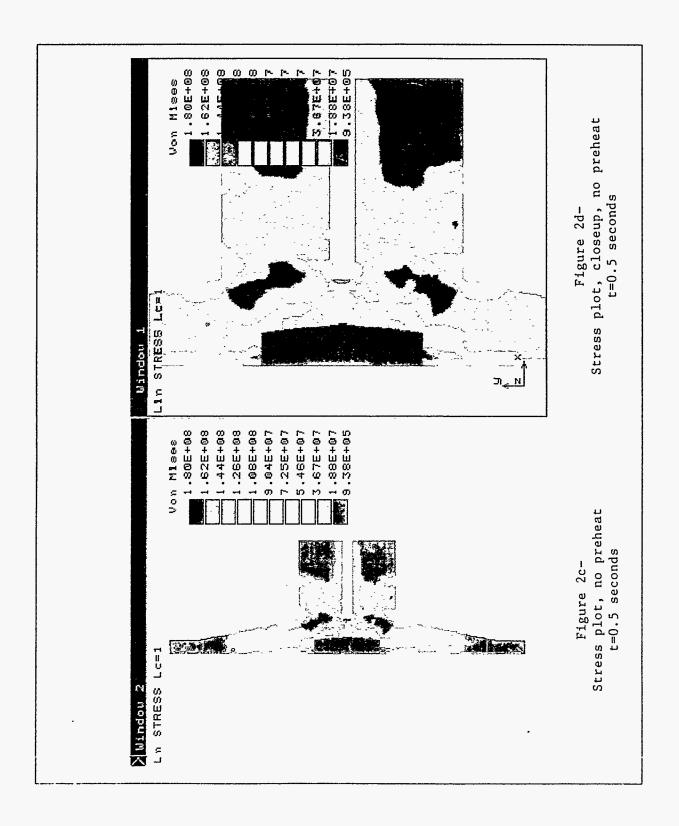
Copy to:
Chuck Lopez, SCE
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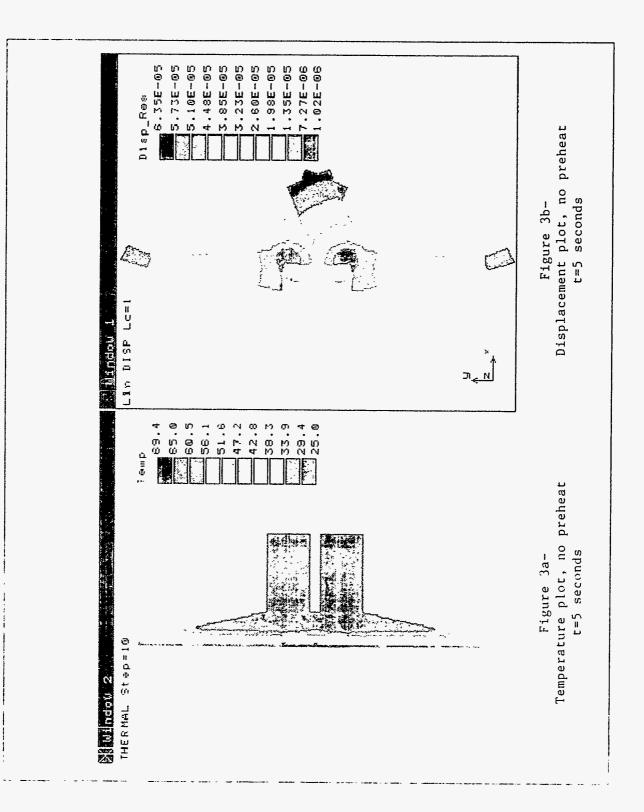
MS-0703 Jim Chavez, 6216 MS-0703 Craig Tyner, 6216 MS-0703 Greg Kolb, 6216 MS-0704 Paul Klimas, 6201 MS-1127 Chris Cameron, 6215 MS-1127 Scott Rawlinson, 6215 (2) File K.3, 6215

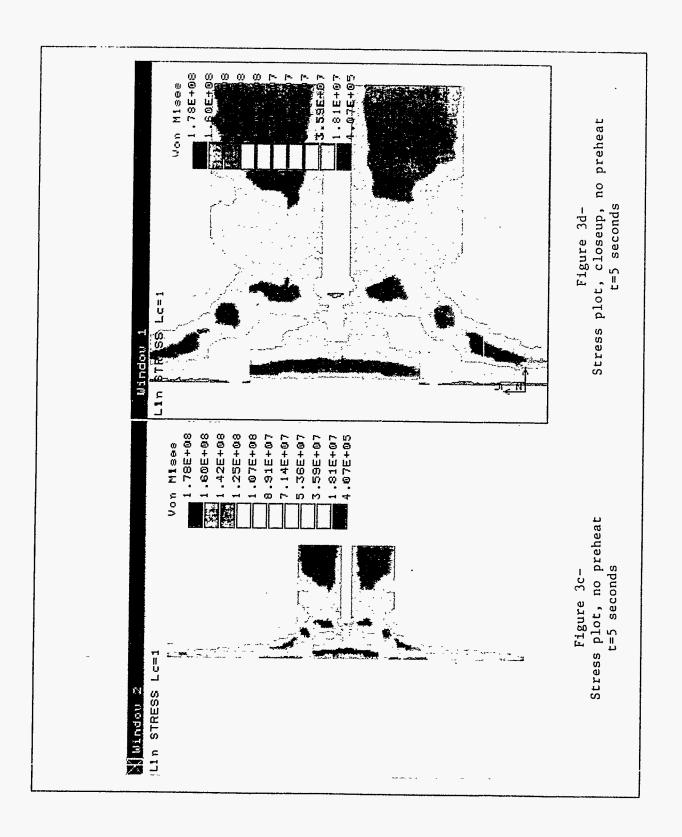


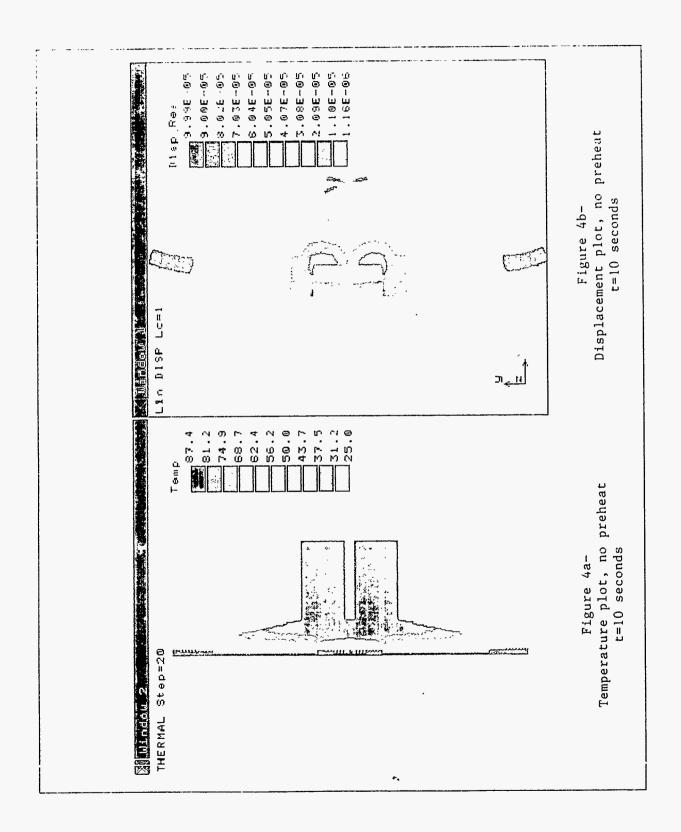


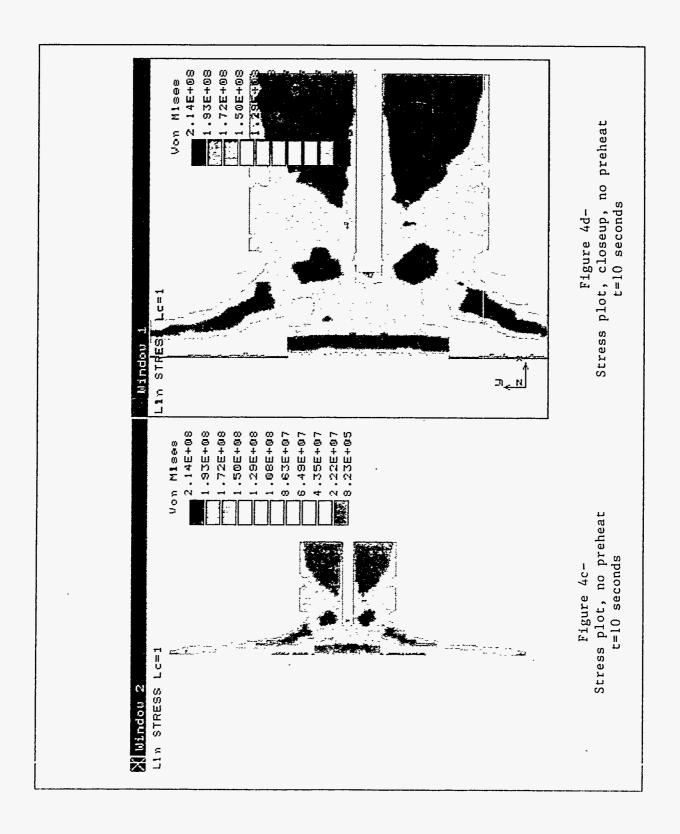


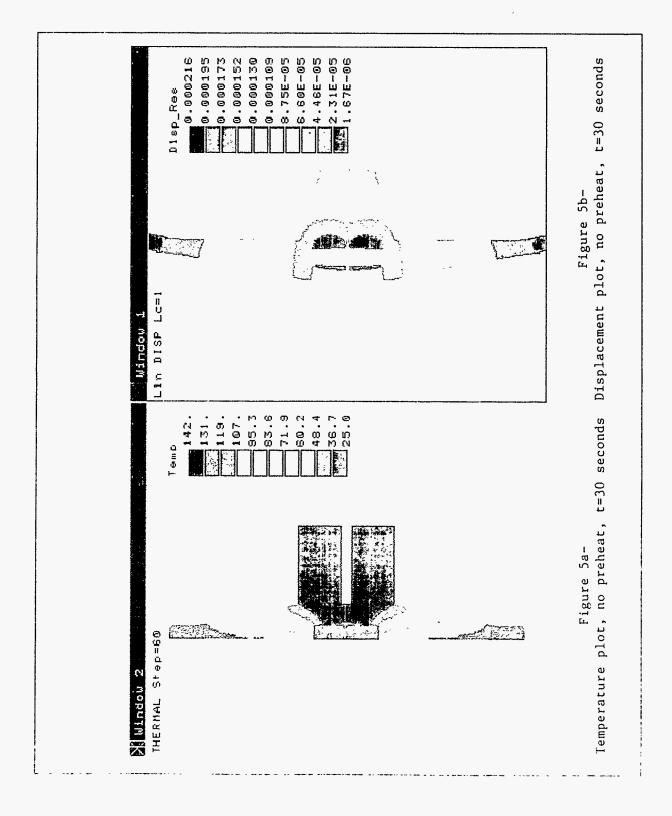


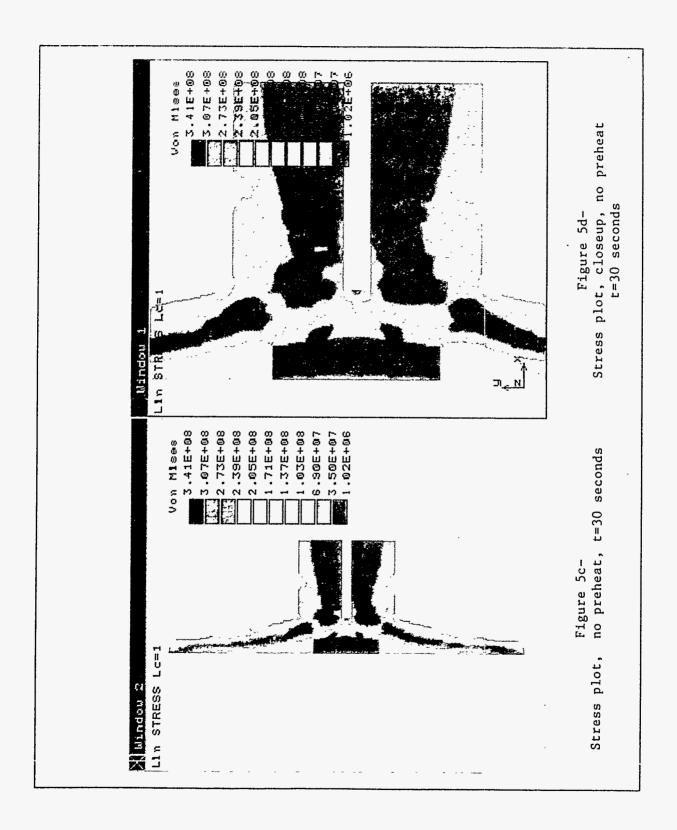


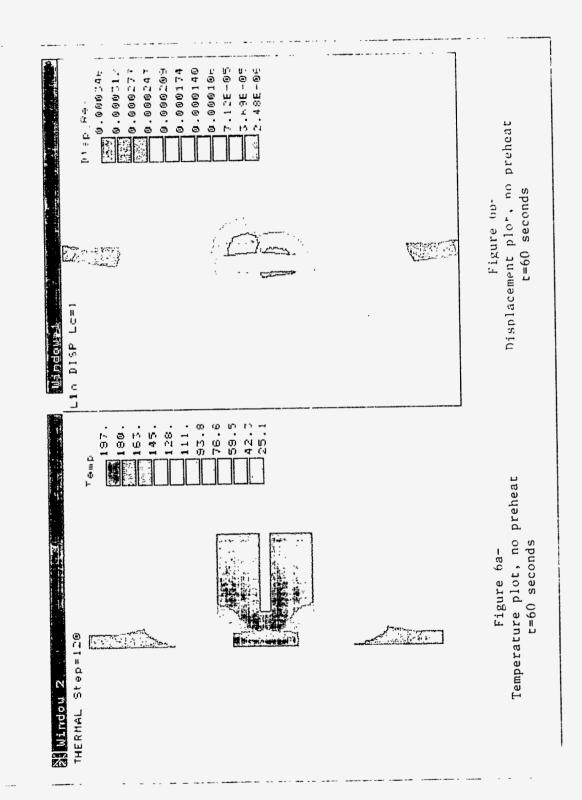


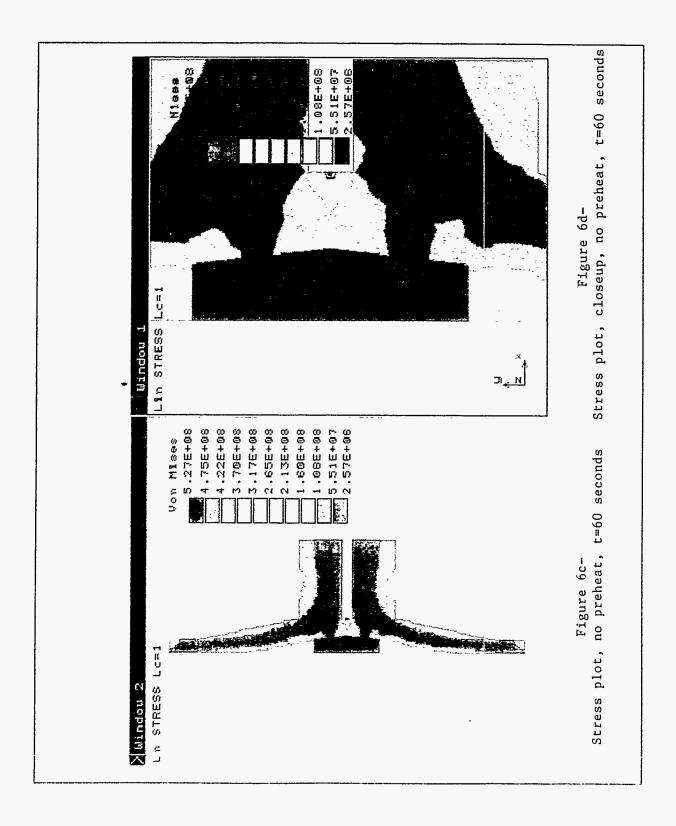


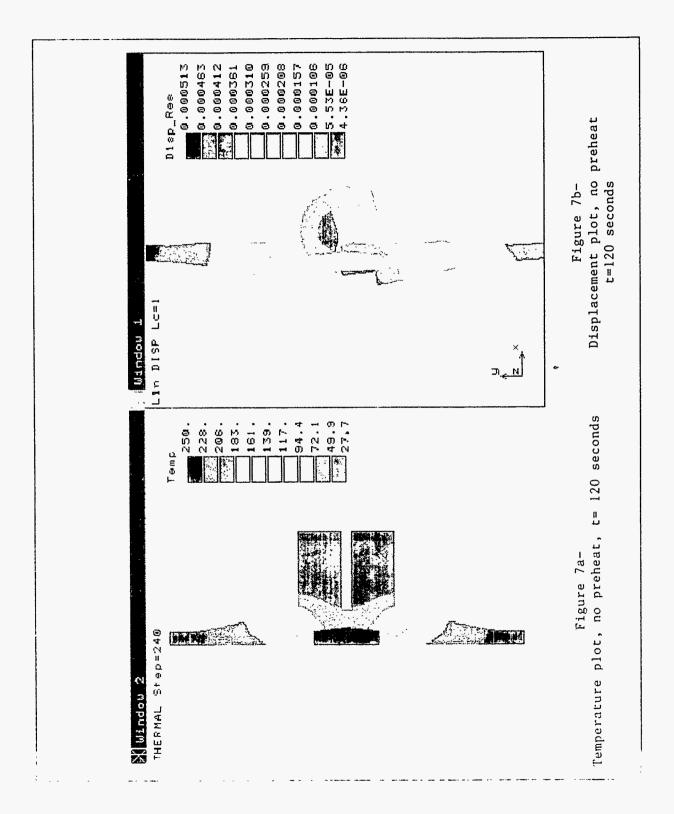


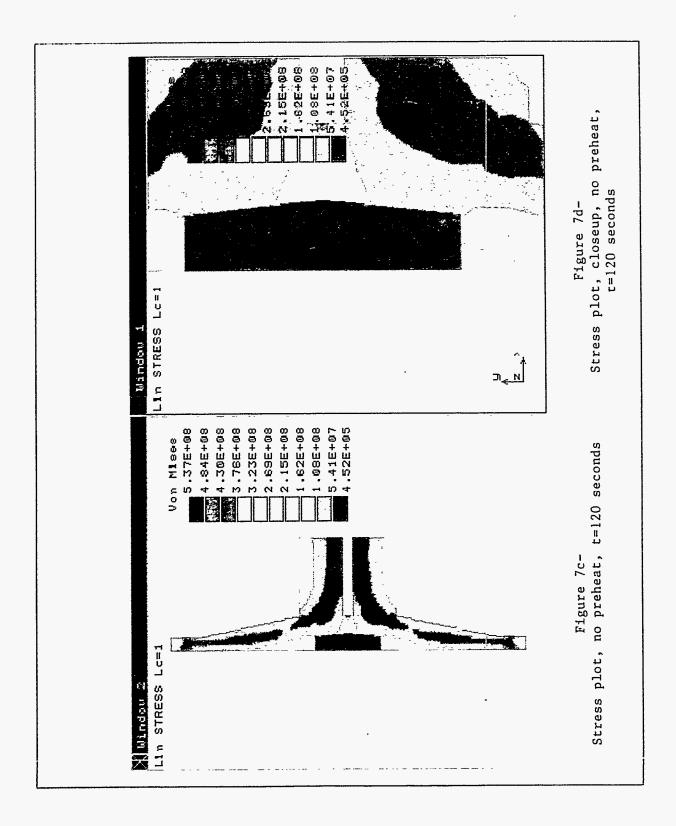


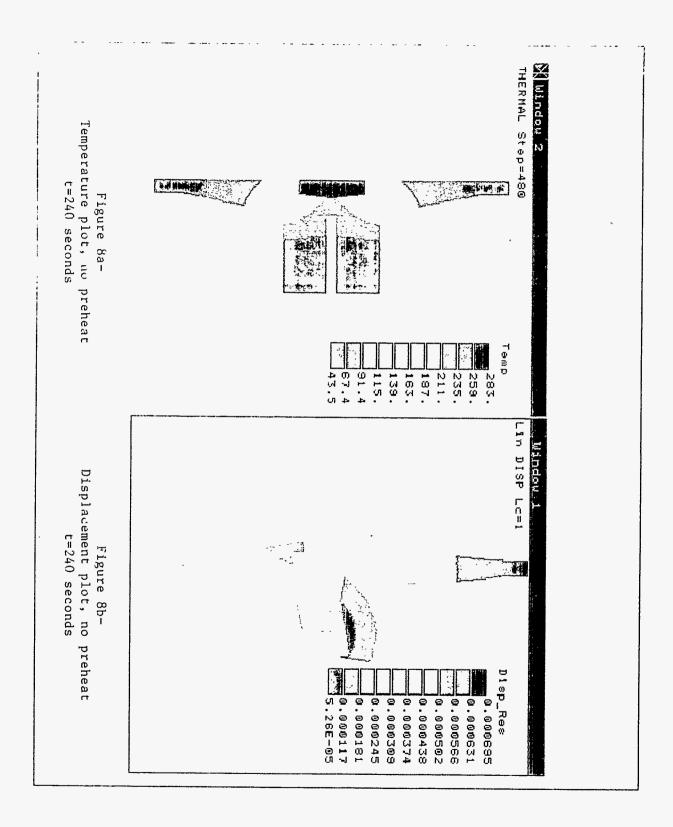


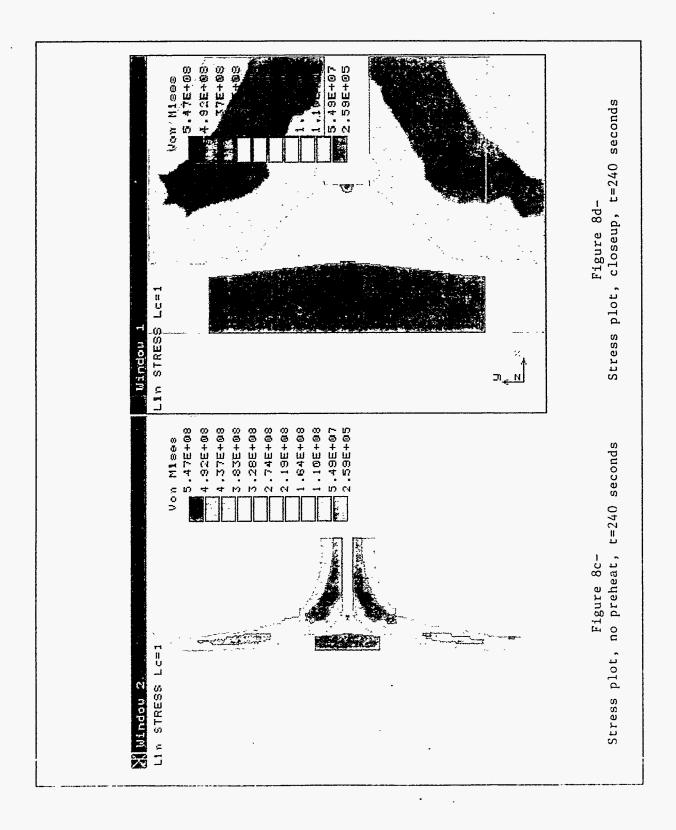


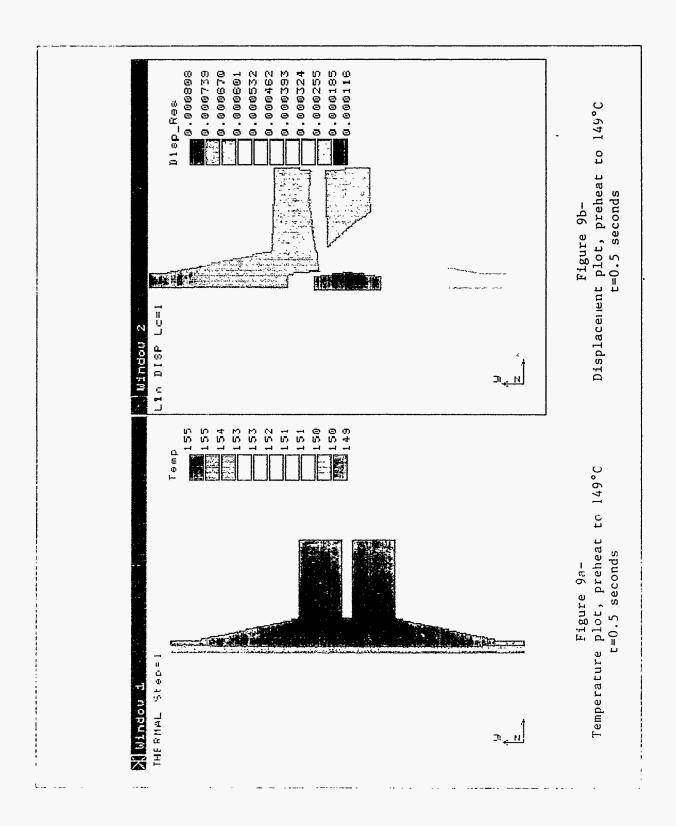


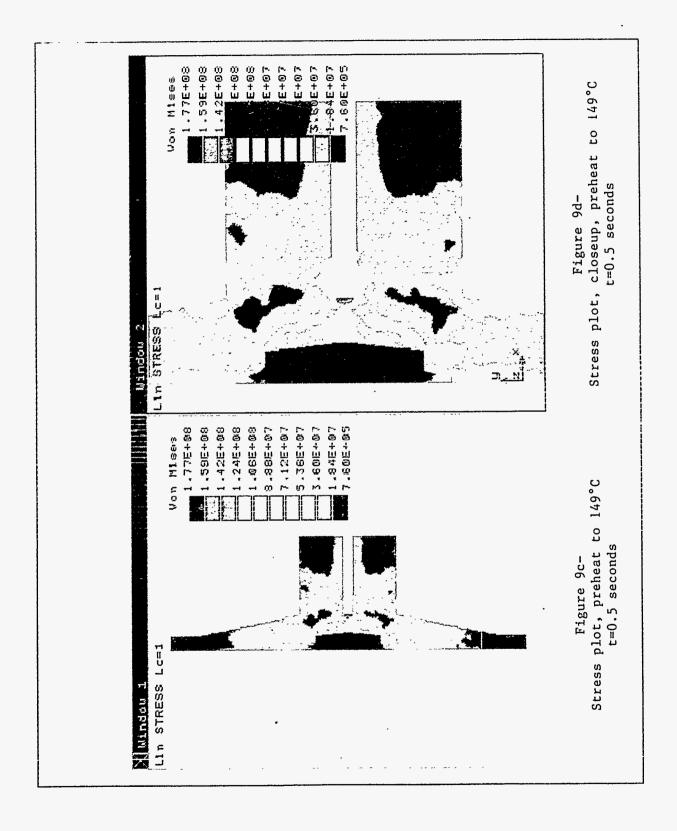


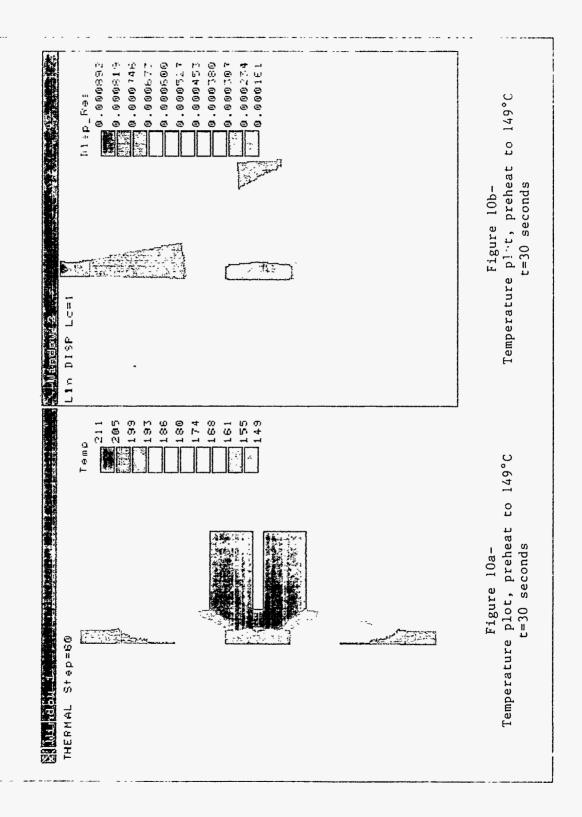


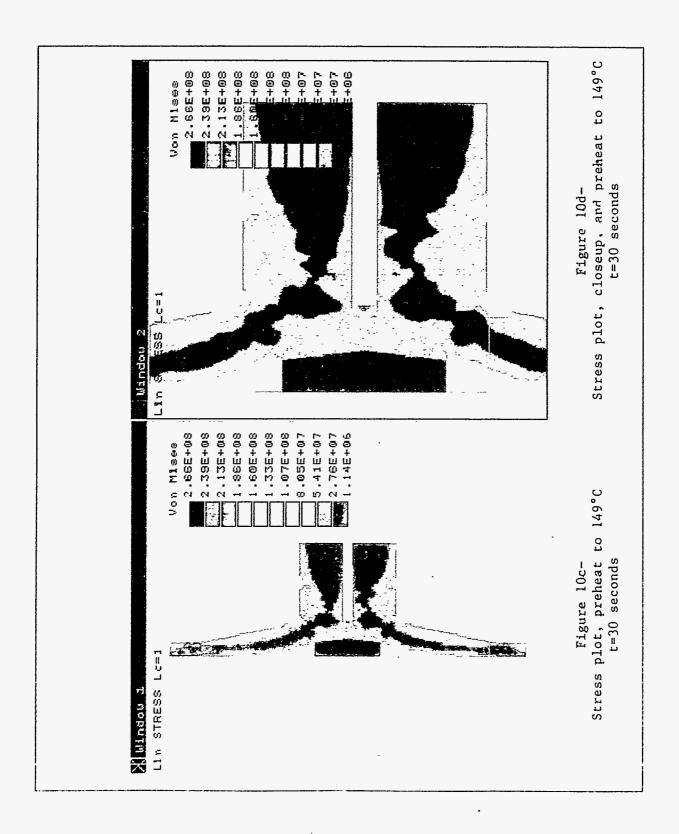


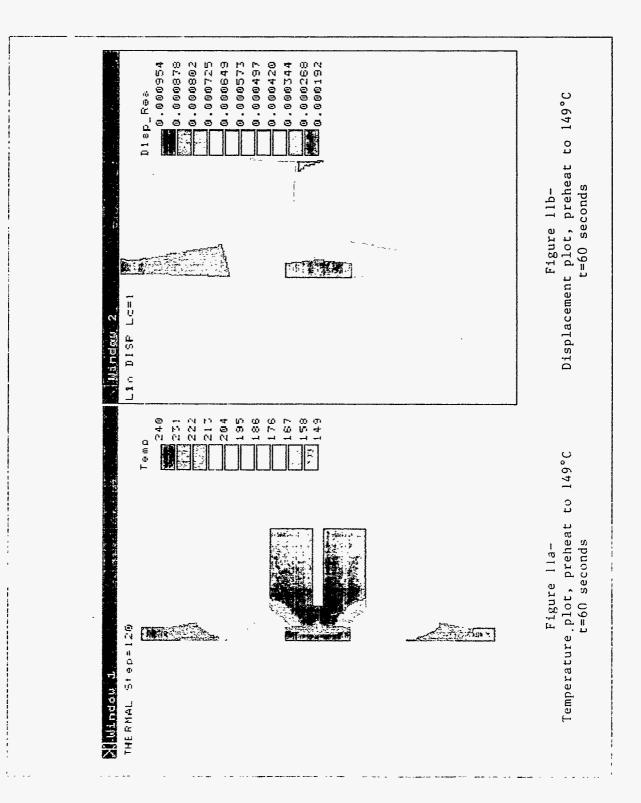


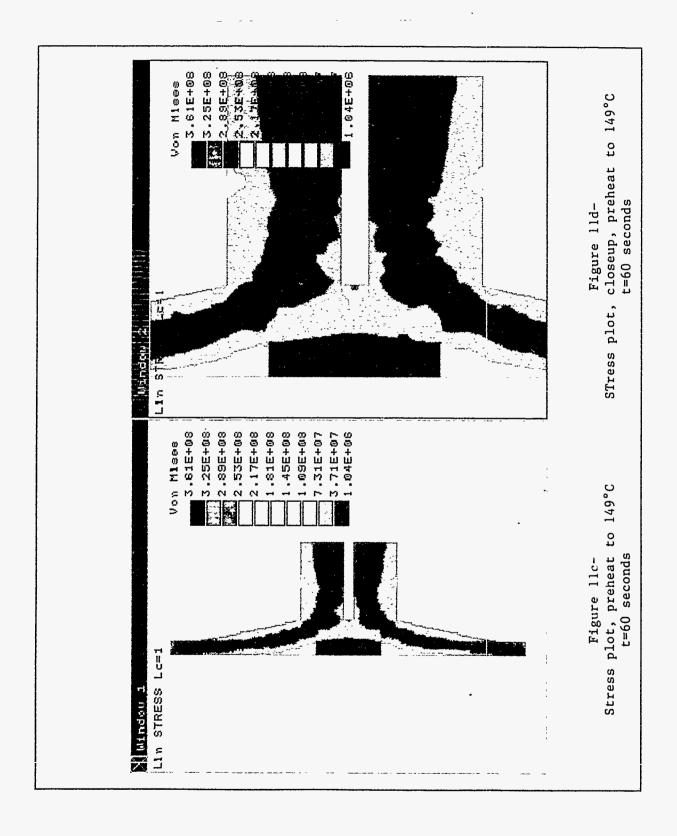


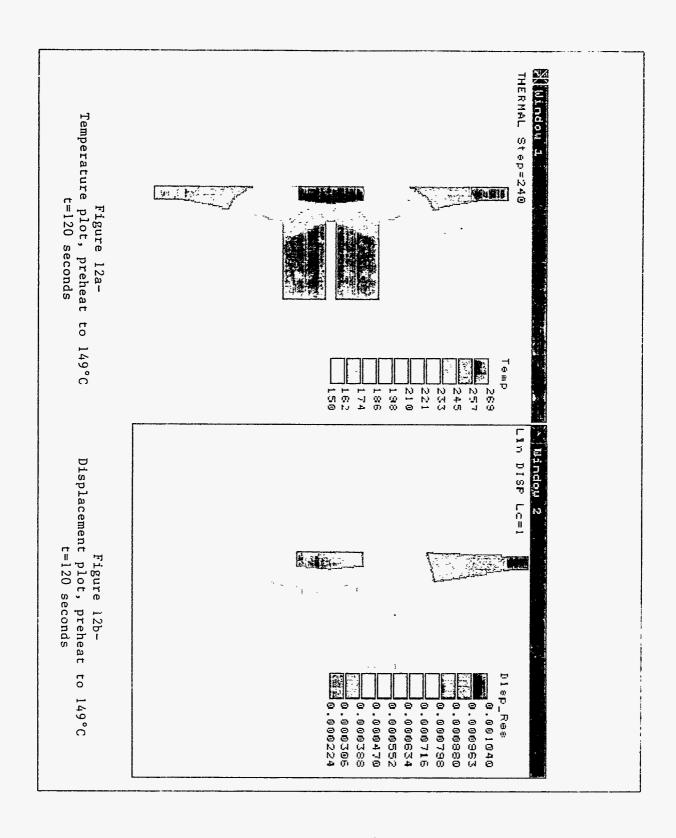


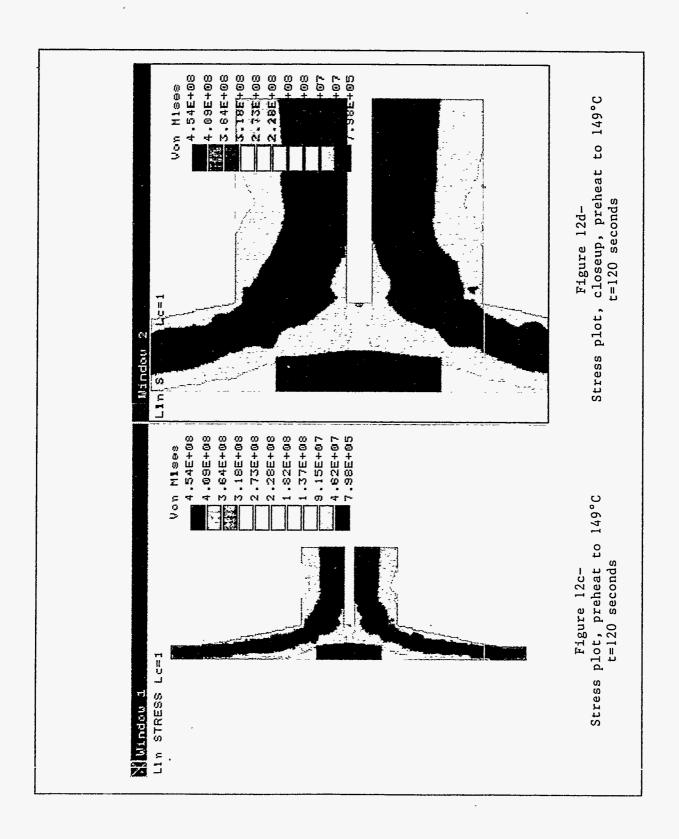


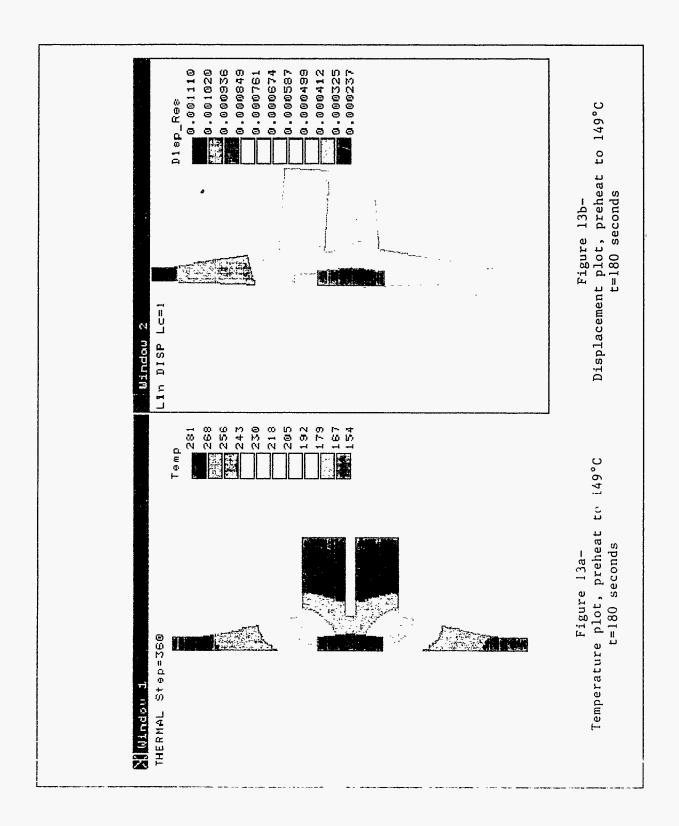


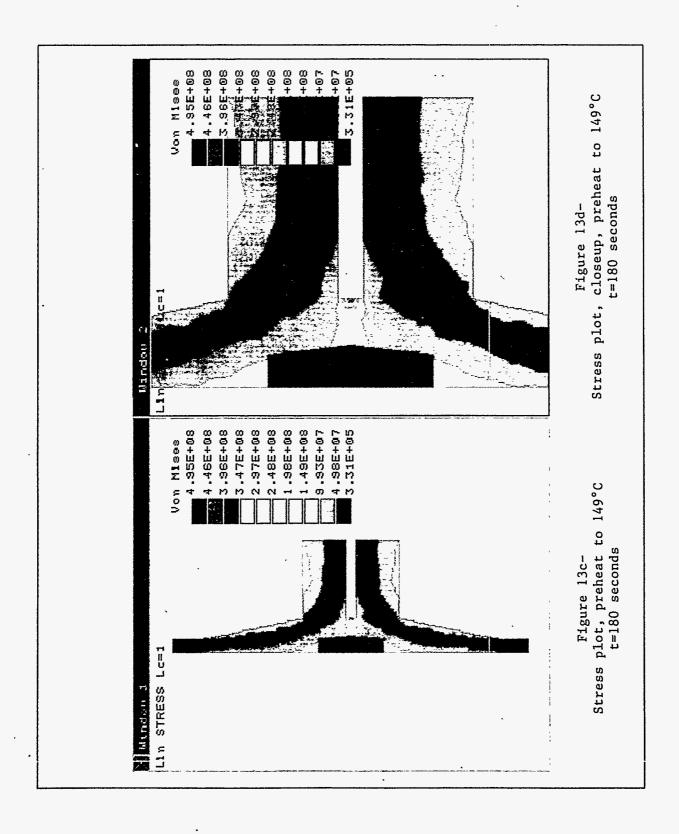


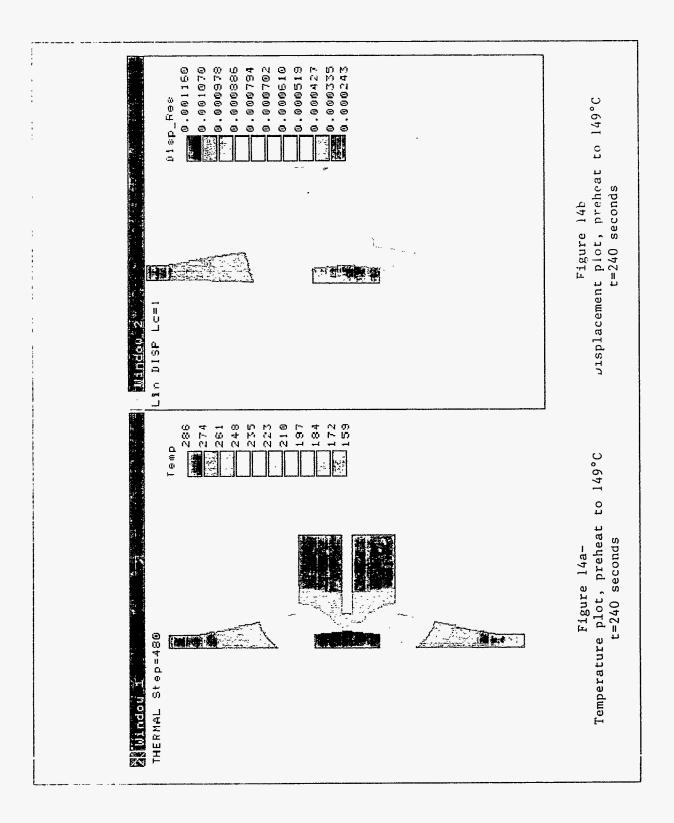


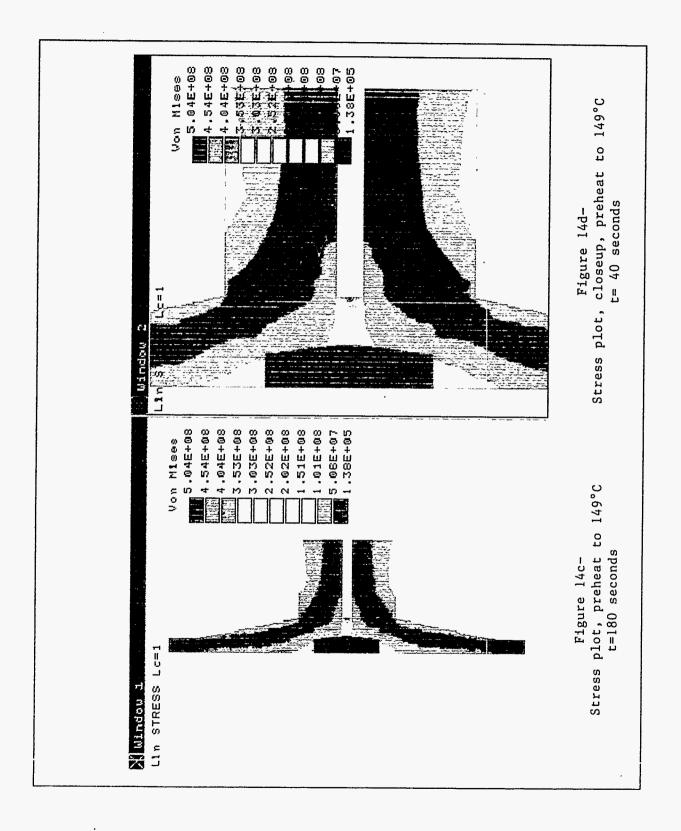












Appendix B. Fabrication of Heat Trace Circuits

The heat trace for large systems is usually designed by the supplier. Each zone is sized based on the heating load and the piping diagrams. The length and power rating of a heat trace cable are sized based on the power required to maintain a pipe at given temperature and the power supply voltage. For a given voltage and heat trace cable length, the MI cable resistance density can be selected to provided the desired power. As a rule of thumb, we try to limit the power wattage density to less than 50 W/ft of MI cable length. Figures B-1 through B-4 are photographs of heat trace installed on a section of piping, a valve body, the header of a receiver panel, and above the jumper tubes in a receiver panel.

To maintain the integrity of the electrical circuit, only, tube benders should be used to bend the heat trace cable. See Figure B-5. After the heat trace is installed, it is covered with metal foil to prevent insulation from getting between the heater and the pipe causing the heater to overheat. The metal foil also helps to direct the radiant heat from the heat trace to the pipe or component. The metal foil can either be wrapped around the pipe and heat trace or tack welded over the heat trace to the pipe.

A critical area in heat trace circuit fabrication is the hot to cold junction. This junction makes a transition from the power lead (copper cable) to the heater (NiCr cable). Most of the failures of heat trace circuits can be attributed to a failure at the hot to cold junction. Below is an outline of the fabrication of hot-to-cold junctions.

- 1. First, a splice is drilled out to fit over the MI cable. See Figure B-6.
- 2. Cut the MI cable by scoring it three times, but not cutting it all the way through because it may cause a short of the conductor wire. Snap off the cut piece.
- 3. Remove 3/8 inch of the sheath to expose the inner wire of the MI cable. Peel the sheath to expose the Magnesium Oxide (MgO) and conductor wire (Figure B-7.)
- 4. File the inner conductor wire flat. Everything must be kept clean to make sure the silver solder adheres. Clean with emery cloth (Figure B-8).
- 5. Test (Meger Test) the insulation quality of each MgO MI cable by measuring the resistance between the conductor and the sheath. The resistance should be at least 5 M Ω preferably 20 M Ω .
- 6. Clean everything that has to be brazed: the conductors and sheath.
- 7. Check the splice and stress fitting for fit.
- 8. Slip the stress fitting and splice over the MI cable.
- 9. Put flux on the conductor of the cold lead (copper wire) to help the brazing process.
- 10. Put solder on with a torch.
- 11. Check the resistance again to make sure there are no shorts.
- 12. Line up the hot (NiCr) and cold (Cu) leads (Figure B-9).
- 13. Melt the solder from the cold (Cu) side and let it flow towards the hot (NiCr) side.
- 14. Remove flux residue with pliers. Check integrity of joint. Buff with emery cloth.
- 15. Check resistance again for shorts.
- 16. Clean any outgassing of flux residue on the surface of the MgO by taking out the top surface of the MgO. The MgO is very hydroscopic.
- 17. Slide the splice over the junction until the junction can be seen through the breather hole.



Figure B-1. Heat trace installed on 2 inch pipe before metal foil was installed. It is snaked to allow for thermal expansion.

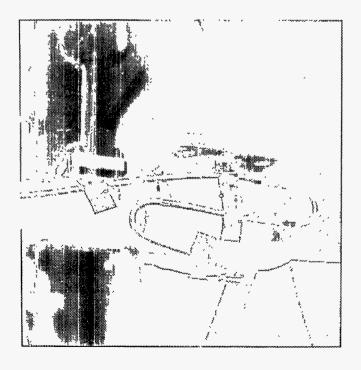


Figure B-2. Heat trace installed on valve body prior to being covered with metal foil.

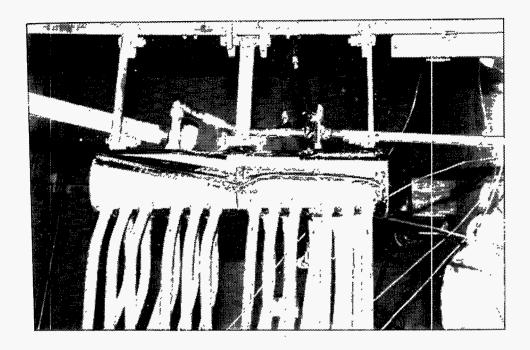


Figure B-3. Heat trace on receiver panel header with metal foil covering the cable.

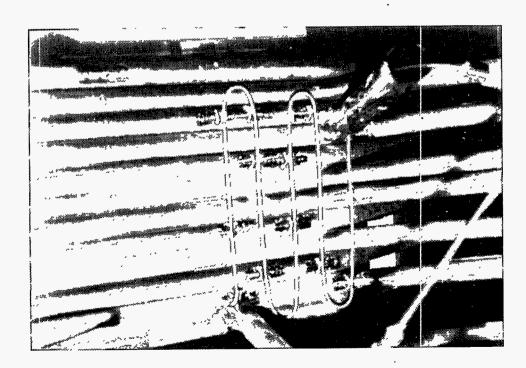


Figure B-4. Heat trace on jumper tubes in receiver panel.

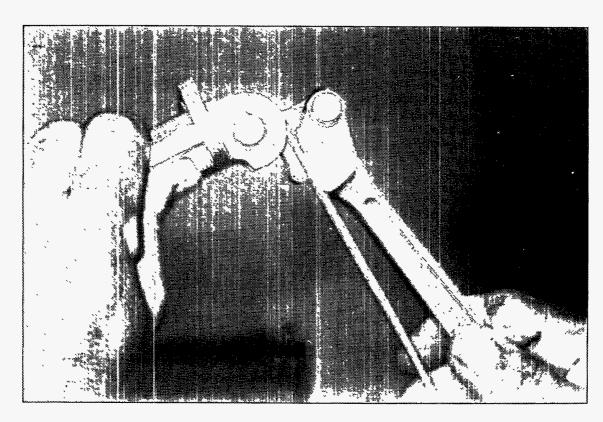


Figure B-5. Tube bender used for bending MI cable.

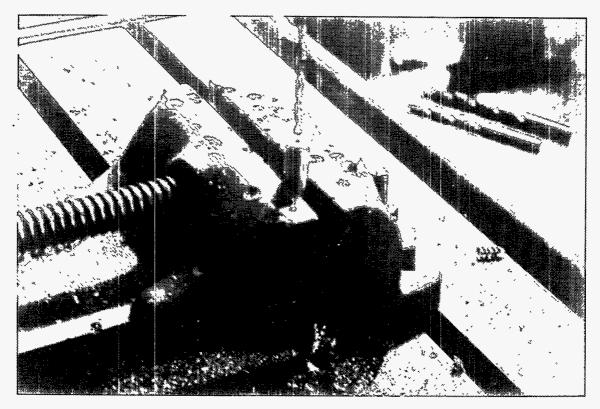


Figure B-6. Splice is drilled to fit over MI cable.

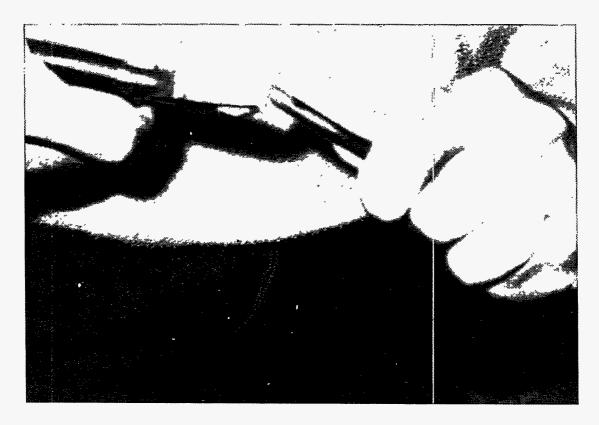


Figure B-7. Sheath is peeled away to expose magnesium oxide (MO) and the conductor wire.

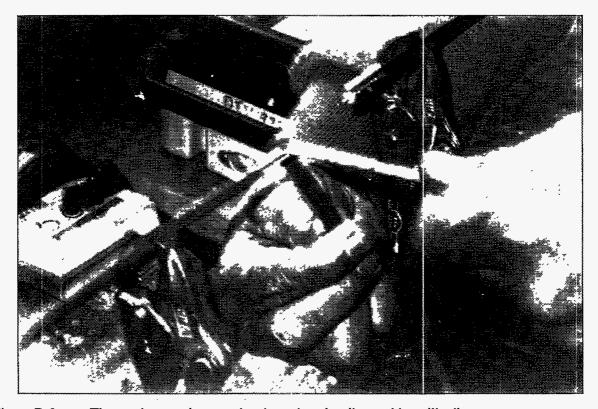


Figure B-8. The conductor wire must be cleaned so the silver solder will adhere.

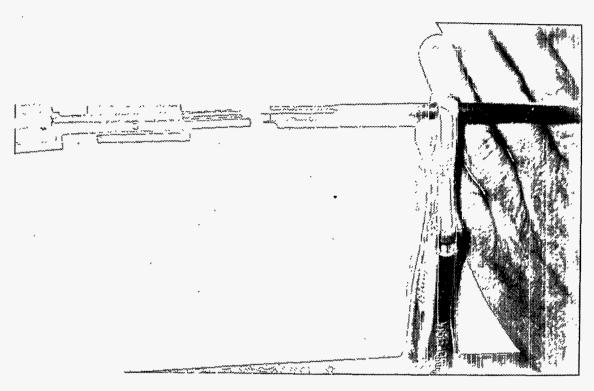


Figure B-9. The heater wire - NiCr, (on the left) and cold lead - Cu (on the right) are lined up.

- 18. Braze the heater side of the splice to the sheath first. Don't have both sides of the MI cable clamped tight otherwise stress will build in the joint. Allow the junction to grow. Braze the hot side by first heating the splice because it has more thermal mass than the sheath, then heating the surrounding cable to bring all parts to temperature at once. Flow solder around the splice. Repeat for cold side (Figure B-10).
- 19. Check resistance again.
- 20. Use a screw to cap off the breather hole in the slice by first putting a kink in the threads two or three threads up to prevent the screw from going in too far and screwing it in the breather hole. Clip of the screw flush with the surface of the splice. File it down. Use a round tail file to make groves in splice for solder to adhere.
- 22. Flux area. Seal vent hole with solder.
- 22. Use a wet rag (Figure B-11) to determine if junction is sealed by measuring resistance. If water penetrated the seal, the resistance would decrease.

Don'ts with Heat Trace:

- 1. Don't weld near heat trace. Weld splatter could burn a hole in the sheath.
- 2. Don't hammer heat trace to fit it in tight spots (Figure B-12).
- 3. Don't use pliers or files to bend the MI cable (Figures B-13 and B-14). Use a tube bender (Figure B-5).

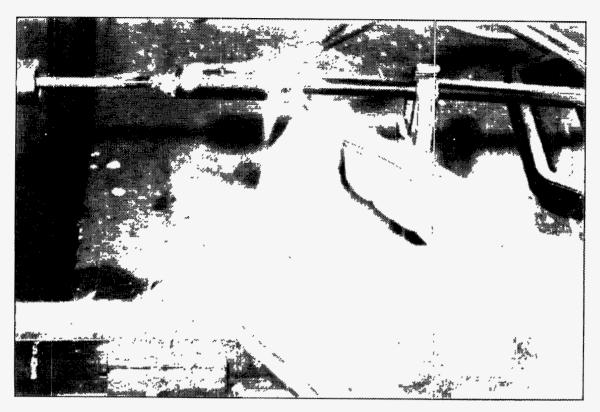


Figure B-10. The spice is brazed to the cable sheath.



Figure B-11. Use a wet rag to determine if the junction is sealed.

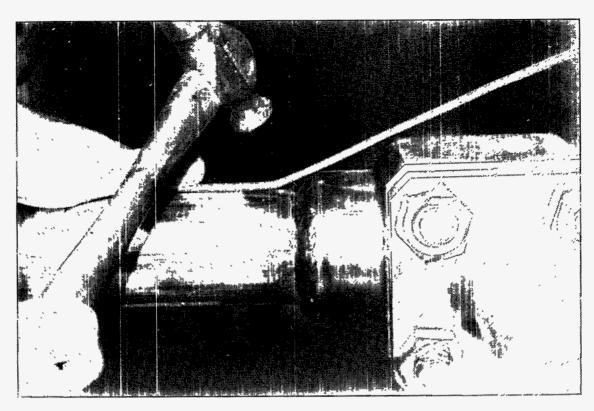


Figure B-12. Do not hammer heat trace.

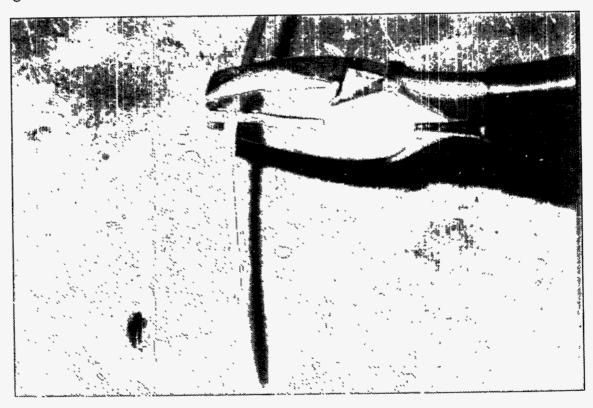


Figure B-13. Do not use pliers to bend heat trace.

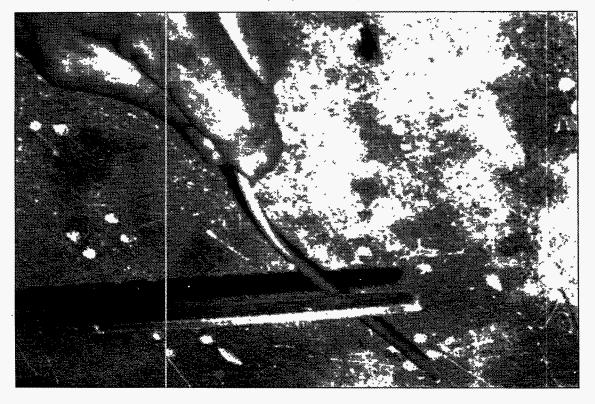


Figure B-14. Do not use a file on the heat trace sheath.

Appendix C. Heat Transfer Coefficient for Circumferentially Varying Heat Flux

The impetus behind establishing a method to estimate accurately heat transfer coefficients is so that the flux limitations on receiver tubes can be set using thermal fatigue data based on the maximum temperature the tube material will experience during normal operation. Since the receiver tubes in a central receiver are heated on one side and insulated on the other, asymmetric heating will affect the heat transfer and thus the tube-temperature distribution. In the Handbook of Heat Transfer Fundamentals there is a description of the effects of circumferentially varying heat flux distribution on the Nusselt number (the nondimensional heat transfer coefficient, Nu=hD/k) for a specific flux distribution, but not a general case. In the journal article referenced by the handbook¹, the methodology to estimate the Nusselt number for an arbitrarily varying flux distribution is described. Basically, the authors describe an analytical derivation where they solve the energy equation by breaking the arbitrary flux distribution into the average flux around the tube plus the variation from the average. The authors claim the theoretical results are within 10% of experimental data for $0.7 \le Pr \le 75$. The model accounts for variations in the radial and circumferential thermal eddy diffusivities for turbulent flow ($\epsilon_{H\rho}$ and $\epsilon_{H\theta}$) which are based on experimental data. The local Nusselt number, $Nu(\theta)$, can be calculated if the flux variation can be expressed in terms of a Fourier series.

In the case of a receiver tube, the flux distribution varies approximately with cosine of the angle from the tube crown assuming the flux is specular (parallel rays). See Figure C-la). Normalizing the flux distribution by the average flux, $q''_0 = q''_{net}/\pi$, the distribution can be represented as $q''(\theta)/q''_0 = 1 + F(\theta)$ where:

$$F(\theta) = 0 \qquad 0^{\circ} \le \theta \le 90^{\circ}$$

$$0 \qquad 90^{\circ} \le \theta \le 270^{\circ}$$

$$\pi \cos(\theta) \qquad 270^{\circ} \le \theta \le 360^{\circ}.$$

 $F(\theta)$ is represented by the Fourier series:

$$F(\theta) = \sum_{n=1}^{\infty} F_n(\theta) = \sum_{n=1}^{\infty} a_n \cos(n\theta)$$

where

$$a_1 = \pi/2$$

$$a_n = \frac{\sin((1-n)\pi/2)}{1-n} + \frac{\sin((1+n)\pi/2)}{1+n}.$$

Figure C-1b) shows the comparison of the flux distribution to Fourier series representation (n=0 to 6). Once the Fourier series representation is known, the fully developed, local Nusselt number is calculated from:

$$Nu_{\omega}(\theta) = \frac{2(q''(\theta)/q''_{o})}{G_{o} + \sum_{n=1}^{\omega} G_{n}F_{n}(\theta)} = h(\theta)D/k$$

¹"Turbulent Heat Transfer in a Circular Tube with Circumferentially varying Thermal Boundary Conditions," *J. Heat. Mass. Transfer*, Vol. 17, pp 1003-1018, (1974).

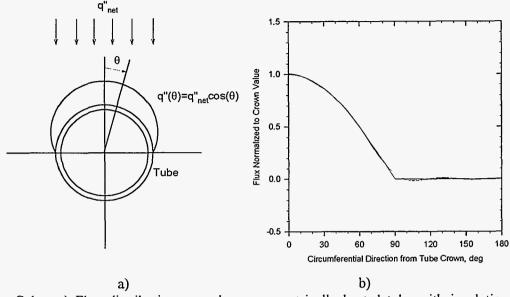


Figure C-1. a) Flux distribution around an asymmetrically heated tube with insulation on the unilluminated side, and b) comparison of flux distribution to Fourier series representation (six terms).

where G_o and G_n are found from solutions to the energy equation and are functions of the Prandtl, Pr, and Reynolds, Re, numbers. They are tabulated in the referenced article.

Figure C-2 shows a comparison of the Nusselt number computed by the above method to that computed by the Dittus Boelter equation - a commonly used correlation for uniformly heat tubes $(Nu=0.023Re^{0.8}Pr^{0.4})$. As can be seen, the analytical estimate of the heat transfer coefficient is greater in value. The authors also state for Pr=8, the dependence of the Nusselt number upon Reynolds number exceeds the power of 0.8 and thus the Dittus-Boelter equation tends to gives more conservative results the higher the Reynolds number. This has been cited by other researchers. According to the referenced article, the deviations between the derivation and experimental data do not exceed 10% and are generally much less. Note, the Pr and Re number for nitrate salts vary from approximately 3.2 and 100,000, respectively, at 1050°F to 10.2 and 30,000, respectively, at 550°F.

This method will give an accurate estimate of localized heat transfer coefficients for a non-uniformly heated tube.

Nu(θ), Pr=10, Re=30,000

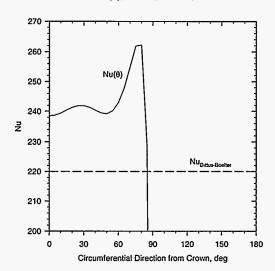


Figure C-2. Comparison of analytical calculation of Nusselt number which accounts for variations in flux to that determined by the Dittus-Boelter equation for Pr=10 and Re=30,000. $Nu(\theta)$ drops to zero between 90° to 180°.

Appendix D. Strain Equations for a Receiver Tube Under High Flux

Assuming a flux profile on the tube that follows a cosine function (Eq. D-1), a relation can be found between the tube strain and flux, tube material properties, and heat transfer coefficient. The plane strain in the tube is the sum of the strain in the tube wall due to the temperature difference across the wall and the strain due to the tube front-to-back temperature difference (Eq. D-2). The flux profile, strain equation, ε , and the tube inside and outside crown temperatures are defined below (assuming thin walled tubes):

$$q''(\theta) = q''_{net}\cos(\theta)$$
 (D-1)

$$\varepsilon = \alpha \left[\left(\frac{T_{o,c} - T_{i,c}}{2(1 - \upsilon)} \right) + \left(\frac{T_{o,c} + T_{i,c}}{2} - T_{avg} \right) \right]$$
 (D-2)

$$T_{o,c} = \frac{q''_{nel} t_{wall}}{k} + T_{i,c}$$
 (D-3)

$$T_{i,c} = T_s + \frac{q''_{net}}{h_c} \tag{D-4}$$

The average tube temperature can be approximated by:

$$T_{avg} = \frac{q''_{net}}{\pi h_c} + \frac{q''_{net} t_{wall}}{2 \pi k} + T_s$$
 (D-5)

Substituting these into the strain equation yields:

$$\varepsilon = \frac{\alpha q''_{net}}{\pi} \left[\frac{t_{wall}}{2k} \left(\frac{\pi (2 - \upsilon) - (1 - \upsilon)}{(1 - \upsilon)} \right) + \frac{(\pi + 1)}{h_c} \right]$$
 (D-6)

Eq. D-6 shows how the flux, tube thickness, material properties and heat transfer coefficient at the crown affect the strain. Also note that the heat transfer coefficient is a function of the salt velocity and temperature. Assuming the control system has anticipatory capabilities, the flow rate and thus the heat transfer coefficient will be tied to the incident flux. At nominal operating conditions, a deviation in the heat transfer coefficient of 10% will only result in a 5% change in strain.

Appendix E. Molten and Solid Nitrate Salt Properties

The following properties are for molten and solid nitrate salt. Table E-1 shows the density, heat capacity, thermal conductivity, absolute and kinematic viscosities, Prandtl number, and thermal diffusivity as a function of temperature for molten salt. These data were compiled from various sources. Many properties were obtained for an equimolar ratio of sodium nitrate (46% by weight) and potassium nitrate (54% by weight). We have assumed the difference is not significant. For further details on salt properties please refer to A Review of the Chemical and Physical Properties of Molten Alkali Nitrate Salts and Their Effect on Materials Used for Solar Central Receivers, R.W. Bradshaw and R.W. Carling, SAND87-8005, printed April 1987.

Molten Nitrate Salt

Composition:

Sodium Nitrate NaNO₃ 60% by weight Potassium Nitrate KNO₃ 40% by weight

Physical Properties (300-600°C, T is in °C):

Density (kg/m³):

 $\rho = 2090 - 0.636 \text{ T}$

Heat Capacity (J/kg•K):

Cp = 1443 + 0.172 T

Thermal Conductivity (W/m•K):

 $k = 0.443 + 1.9 \times 10^{-4} \text{ T}$

Absolute Viscosity (mPa·s):

 $\mu = 22.714 - 0.120 \text{ T} + 2.281 \text{x} 10^4 \text{ T}^2 - 1.474 \text{x} 10^{-7} \text{ T}^3$

Other Molten Salt Properties:

Isotropic Compressibility (NaNO₃) at the melting point:

 $2x 10^{-10} \text{ m}^2/\text{N}$

Speed of Sound:

NaNO₃:

1763.3 m/s (5785.1 ft/s) at 336°C (637°F)

KNO₃:

1740.1 m/s (5709 ft/s) at 352°C (666°F)

Change in Sound Speed with Temperature:

NaNO₃:

0.74 m/s•K

KNO₃:

1.1 m/s•K

Phase Change Nitrate Salt Properties

Freezing Point:

Solidifies at 221°C (430°F)

Start to crystallize at 238°C (460°F)

Heat of Fusion - (based on molecular average of heat of fusion of each component):

$$h_{sl} = 161 \text{ kJ/kg}$$

Change in Density Upon Melting:

$$\Delta V/V_{solid}$$
=4.6% $\Rightarrow V_{liquid}$ = 1.046 V_{solid}

Solid Salt

Density, p:

NaNO₃:

2260 kg/m³ at room temperature

KNO₃:

2190 kg/m³ at room temperature

Heat Capacitance, Cp:

NaNO₃:

37.0 cal/K·mol = 1820 J/kg·K near melting point

KNO₃:

28.0 cal/K•mol = 1160 J/kg•K near melting point

Thermal Conductivity, k:

KNO₃:

2.1 W/m•K

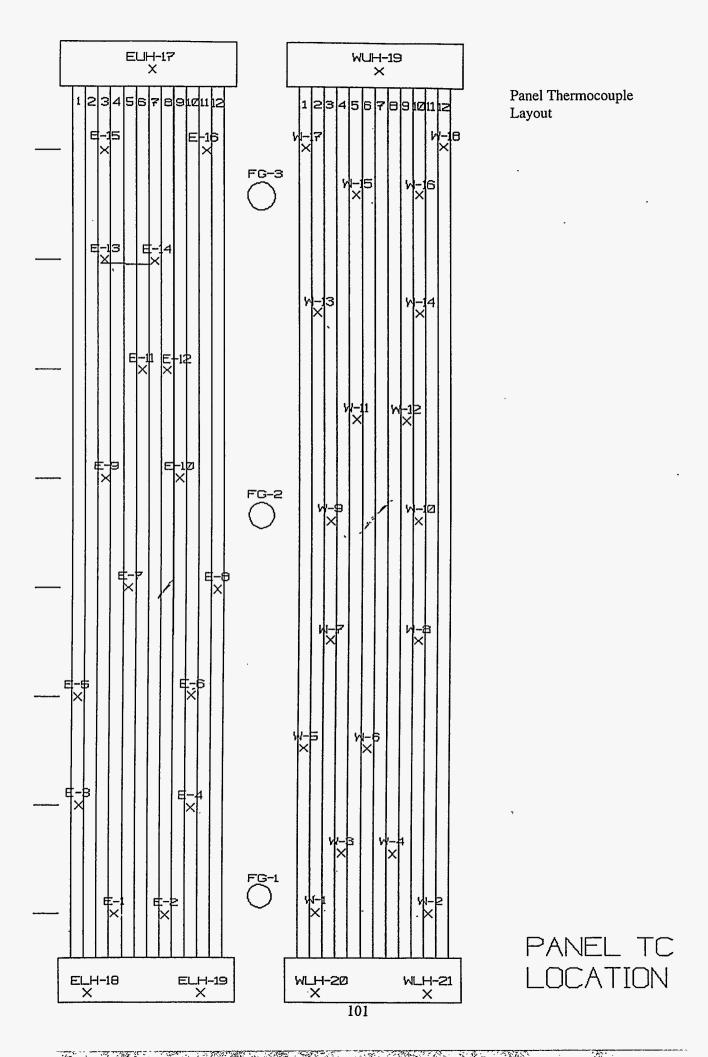
Table E-1. Molten Nitrate Salt Properties: 60% NaNO₃, 40% KNO₃.

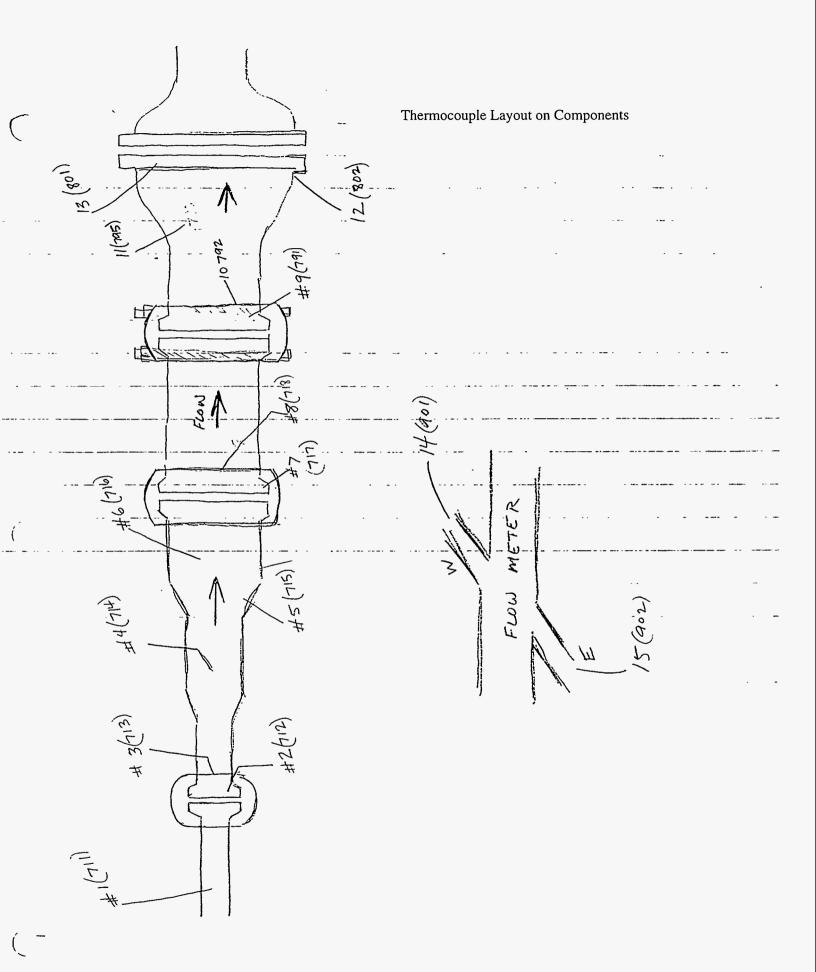
Γ	Ţ		ρ		Ср		k		μ		ν		Pr	α	
	Temperat	ure	Den	sity	Heat Ca	pacity	Thermal Co	nductivity	Absolute \	/iscosity	Kinematic \	/iscosity	Prandtl	Thermal D	oiffusivity
	С	F	Kg/m^3	lbm/ft^3	J/kg/K	3tu/lbm/F	W/m/K	Btu/h/ft/F	Pa s	lbm/ft/h	m^2/s	ft^2/h		m^2/s	ft^2/h
Γ	270	518	1918	119.8	1489	0.3558	0.493	0.2850	0.00404	9.78	2.11E-06	0.082	12.20	1.73E-07	0.00669
1	280	536	1912	119.4	1491	0.3562	0.495	0.2861	0.00376	9.10	1.97E-06	0.076	11.33	1.74E-07	0.00673
ı	290	554	1906	119.0	1493	0.3566	0.497	0.2872	0.00350	8.47	1.84E-06	0.071	10.52	1.75E-07	0.00677
ı	300	572	1899	118.6	1495	0.3570	0.499	0.2883	0.00326	7.89	1.72E-06	0.067	9.77	1.76E-07	0.00681
ı	310	590	1893	118.2	1496	0.3574	0.501	0.2894	0.00304	7.36	1.61E-06	0.062	9.09	1.77E-07	0.00685
ı	320	608	1886	117.8	1498	0.3578	0.503	0.2905	0.00284	6.87	1.51E-06	0.058	8.47	1.78E-07	0.00689
ı	330	626	1880	117.4	1500	0.3582	0.505	0.2916	0.00266	6.43	1.41E-06	0.055	7.90	1.79E-07	0.00694
ı	340	644	1874	117.0	1501	0.3586	0.507	0.2927	0.00249	6.02	1.33E-06	0.051	7.38	1.80E-07	0.00698
ı	350	662	1867	116.6	1503	0.3591	0.509	0.2938	0.00234	5.65	1.25E-06	0.048	6.91	1.81E-07	0.00702
ı	360	680	1861	116.2	1505	0.3595	0.510	0.2949	0.00220	5.32	1.18E-06	0.046	6.48	1.82E-07	0.00706
ı	370	698	1855	115.8	1507	0.3599	0.512	0.2960	0.00207	5.02	1.12E-06	0.043	6,10	1.83E-07	0.00710
ı	380	716	1848	115.4	1508	0.3603	0.514	0.2971	0.00196	4.75	1.06E-06	0.041	5.76	1.84E-07	0.00715
ı	390	734	1842	115.0	1510	0.3607	0.516	0.2982	0.00186	4.51	1.01E-06	0.039	5.46	1.86E-07	0.00719
1	400	752	1836	114.6	1512	0.3611	0.518	0.2993	0.00178	4.30	9.68E-07	0.038	5.18	1.87E-07	0.00723
١	410	770	1829	114.2	1514	0.3615	0.520	0.3004	0.00170	4.11	9.29E-07	0.036	4.95	1.88E-07	0.00728
3	420	788	1823	113.8	1515	0.3619	0.522	0.3015	0.00163	3.94	8.94E-07	0.035	4.73	1.89E-07	0.00732
1	430	806	1817	113.4	1517	0.3623	0.524	0.3026	0.00157	3.80	8.64E-07	0.033	4.55	1.90E-07	0.00736
ı	440	824	1810	113.0	1519	0.3628	0.526	0.3037	0.00152	3.67	8.39E-07	0.032	4.39	1.91E-07	0.00741
ı	450	842	1804	112.6	1520	0.3632	0.528	0.3048	0.00147	3.56	8.16E-07	0.032	4.24	1.92E-07	0.00745
١	460	860	1797	112.2	1522	0.3636	0.529	0.3059	0.00143	3.47	7.97E-07	0.031	4.12	1.93E-07	0.00750
ı	470	878	1791	111.8	1524	0.3640	0.531	0.3070	0.00140	3.38	7.80E-07	0.030	4.01	1.95E-07	0.00754
ı	480	896	1785	1,11.4	1526	0.3644	0.533	0.3081	0.00137	3.31	7.66E-07	0.030	3.91	1.96E-07	0.00759
ı	490	914	1778	111.0	1527	0.3648	0.535	0.3092	0.00134	3.24	7.53E-07	0.029	3.82	1.97E-07	0.00763
ı	500	932	1772	110.6	1529	0.3652	0.537	0.3103	0.00131	3.18	7.42E-07	0.029	3.74	1.98E-07	0.00768
ı	510	950	1766	110.2	1531	0.3656	0.539	0.3114	0.00129	3.12	7.31E-07	0.028	3.66	1.99E-07	0.00773
ı	520	968	1759	109.8	1532	0.3660	0.541	0.3125	0.00127	3.06	7.20E-07	0.028	3.59	2.01E-07	0.00777
ı	530	986	1753	109.4	1534	0.3664	0.543	0.3136	0.00124	3.01	7.09E-07	0.027	3.51	2.02E-07	0.00782
	540	1004	1747	109.0	1536	0.3669	0.545	0.3147	0.00122	2.95	6.97E-07	0.027	3.43	2.03E-07	0.00787
	550	1022	1740	108.6	1538	0.3673	0.547	0.3158	0.00119	2.88	6.84E-07	0.027	3.35	2.04E-07	0.00791
	560	1040	1734	108.2	1539	0.3677	0.548	0.3169	0.00116	2.81	6.69E-07	0.026	3.26	2.05E-07	0.00796
ı	570	1058	1727	107.8	1541	0.3681	0.550	0.3180	0.00113	2.72	6.52E-07	0.025	3.15	2.07E-07	0.00801
	580	1076	1721	107.4	1543	0.3685	l .	0.3191	0.00109	2.63	6.32E-07	0.024	3.04	2.08E-07	0.00806
	590	1094	1715	107.0	1544	0.3689	0.554	0.3202	0.00104	2.52	6.08E-07	0.024	2.91	2.09E-07	0.00811
	600	1112	1708	106.7	1546	0.3693	0,556	0.3213	0.00099	2.40	5.80E-07	0.022	2.76	2.10E-07	0.00816

9

Appendix F. Selected Sets of Data and Other Information

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SETUP INFORMATION FOR THE PANAMETRICS ULTRASONIC FLOWMETER

PROMPT SETTING

System Units METRIC

Volumetric Units liters

Time Units . minutes

Decimal Digits 2

Totalizer Units liters

Decimal Digits 2

Analog Out Units Volumetric

Analog Out Zero 0.0 liters/min (4 mA)

Full Scale 500.0 liters/min (20 mA)

Error Handling Force Low

Response Time 30 readings

Fluid Type Other (for Molten Sodium Nitrate-60% and Potassium

Nitrate-40%)

Fluid Sound Speed 1800.0 m/s (nitrate salt, 1812 m/s was measured when

clamp on flowmeter was work)

Reynolds Correction Active

Kin. Viscosity 1.863 E-6 m^2/s @ 288 C (550F) nitrate salt

Meter Factor K 1.000

Transducer # 91 for the wetted flow cell (Channel 1)

116 for the clamp on transducer (Channel 2)

The setup for each type of transducer is different and continues on the next page.

The Following Apply to the CLAMP ON TRANSDUCERS. (Note the clamp on transducer temperature should not exceed 288 C (550 F). It should be removed before operating at higher temperatures.)

Pipe Temperature 93 C (Wedge Temperature - measured half way up wedge)

Wall Thickness 3.91 mm (0.154 in for 2" dia SCH 40 SS

piping)

Pipe I.D. 52.50 mm (2.067 in)

Traverses 2

Pipe Material Stainless Steel

Pipe Type Round

Zero Cutoff 0.3 m/s

Xducer Spacing S 58.00 mm (enter actual dimension)

This is the space needed for the clamp on transducers as computed from the parameters entered into the computer. If the actual spacing doesn't match this value, the value can be overwritten to match the actual physical spacing.

The Following Apply to the WETTED TRANSDUCERS. (Note the wetted transducer temperature should be monitored and the sensor itself - which is out of the fluid - should not exceed 288 C (550 F). It should be removed before operating at higher temperatures.)

Path Length P 256.4816 mm (10.0977 in from Panametrics)

Axial Dimension L 157.5054 mm (6.2010 in from Panametrics)

Pipe I.D. 52.50 mm (2.067 in)

Pipe Type Round

Zero Cutoff 0.3 m/s

Type Parameter 909 to enter parameters for wetted transducer 91:

Transducer Number 91
Transducer type Wetted
Tranducer Frequency 1.0 MHz

Transducer Tw (delay) 36 µsec (or 36.7 per Mike Pouglia of Panametrics)

Transducer THETA 1 N/A

Transducer Wedge Soundspeed N/A m/sec (ft/sec)

Metal Clamp-on Flow transducers Numbers:

. CTS-1.0-HT CTS-1.0-HT 1192256 CTS. 1.0 MHz S/N 693286 XDCR#21 XDCR #21

on elbow: 2R0308

Part Numbers on Components in Molten Salt Experiments

Tee and cap for Corrosion Experiments:

E-CON E0204-300 S-2063 316 ISZ E-CON E0204-300 S-2063 316 ISZ

2" Flange:

Clamp:

GRAYLOC 2

182F304 GNS0218 CANADA SN48302

Body (2 of these):

PN115405 GRAYLOC® 2GR20 BW 2SCH40 SA182-F316L G1316 S07037700

Checkvalve:

REFLANGE V-CON 3-900

316 216302

(Clamp side): F04 S-3063

4" Flange (on checkvalve):

(Clamp):

REFLANGE C-04

(Body):

R-CON F04-0304 S-3063 316 216302

4" Flange:

(Clamp):

REFLANGE C-04

(Body, 2):

R-CON S4063 316 91461

6" Flange (8 bolt):

(Body, 2):

E-CON E0604-300 S-6065 316 AJM E-CON E0604-300 S-6065 316 LDI

Panametrics Flow Meter - Electronics

Model 6468-22-1000-0 Serial Number 791 Software Version 4.D

Weight of Components

31 lbs: from elbow to blind flange for corrosion coupons to first half of 2" grayloc flange

14.5 lbs: 2" grayloc clamp

39 lbs: 2nd half of 2" grayloc flange + 2x3 reducer + 3" V-CON checkvalve + half of 3" inner 4" outer R₂-CON flange

27 lbs: 2nd half of 3" inner, 4" outer R-CON flange to 1st half of 4" R-CON flange

27 lbs: 1st R-CON 4" clamp

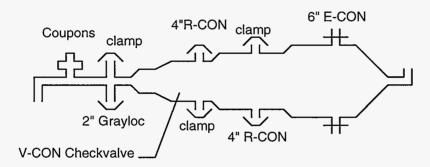
29lbs: 2nd R-CON 4" clamp

42 lbs: 2nd half of 4" R-CON flange + 4x6 reducer + 1st half of 6" E-CON flange.

42 lbs: 2nd half of 6" E-CON flange + 6"x2" reducer + elbow

Total weight: 251 lbs

Total length outer edge of elbow to outer edge of elbow: 100"



Added 2-1-94

4" ANSI Ring Type flange, 300#, oval grove, oval ring, stainless steel





Ring Type Flange

added between 4" R-CON Flanges

43.1 lbs: 2nd half of 3" inner, 4" outer R-CON flange to 1st half of 4" Ring-type flange

36.5 lbs: 2nd half of 4" Ring-type flange to 1st half of 4" R-CON flange

New Total Weight: 303.6 lbs

Panel Cold Fill Test: 12/01/93

CRTF	Panel Col	d Fill Test, 1	12/01/93	-		
TEST		1st pass		3rd pass	4th pass	Upper he
Time		TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	DEG F	DEG F	DEG F	DEG F
9.4494	475	48	48	46	46	80
9.4508	480	48	48	46	46	80
9.4522	·	48	48	46	46	80
9.4536	490	48	48	46	46	80
9.455		48	48	46	46	80
9.4564	·	48	48	46	46	80
9.4581	505	48	48	46	46	80
9.4594	 	48	48	46	46	80
9.4608	·	48	48	45	46	80
9.4622		48	48	45	45	80
9.4636	 	48	48	45	45	80
9.465		48	48	45	45	80
9.4664	+	48	49			80
9,4678	÷	ļ. <u>. </u>	49			80
9.4692	·		49		 	
9.4706	+		 		45	80
9.4717			49		45	80
9.4731	+		49	45	45	80
9,4744	····					80
9.4758	***		49	45	45	80
9,4772		121	49	45	45	80
9.4786	580	283	49	45		
9.48	585	432	49	45		·
9.4814	590	542	104			
9.4828	595	582	231	45		
9.4842	600	590	366	45	45	98
9.4856	605					
9.4869	610	586				
9.4883						
9.4897	620			 		
9.4911	625	····	,			
9.4925				 		
9,4939						
9.4953	640	576	520			
9.4967						
9,4983		· · · · · · · · · · · · · · · · · · ·				
9.4997						
9,5011						
9.5025	·	,				
9.5039	+	·	531			
9.5053	675	571	532			
9.5067	+	·	533			·
9.5081	685				···	
9.5094	690					
9.5108	695	570	541	494	507	488

Panel Cold Fill Test: 12/01/93

CR	RTF	Panel Col	d Fill Test, 1		· · · · · · · · · · · · · · · · · · ·		
TES	ST		1st pass	2nd pass	3rd pass	4th pass	Upper he
Tim	ne 📑		TEW4	TEW17	TEE12	TEE9	TEWUH19
họ	ur	Time	DEG F	DEG F	DEG F	DEG F	DEG F
	9.5122	700	570	541	504	518	500
	9.5136	705	570	543	505	519	505
	9.5147	710	570	543	512	527	514
	9.5161	715	570	543	518	532	523
	9.5175	720	570	544	521	534	529
	9.5189	725	570	544	523	537	534
	9.5203	730	570	544	525	539	538
	9.5217	735	570	545	526	540	543
	9.5231	740	570	545	528	542	545
	9.5244	745	570	545	530	543	548
	9.5258	750	570	546	532	544	551
	9.5272	755	570	546	533	545	553
	9.5286	760	570	546	535	546	555
	9.5303	765	570	547	536	547	557
[-	9.5317	770	570	547	537	549	558
	9.5331	775	569	547	538	550	559
[9.5344	780	569	547	538	550	559
	9.5358	785	569	548	539	551	561
	9.5372	790	569	548	540	551	562
	9.5386	795	569	548	540	551	562
Ī	9.54	800	569	548	542	552	563
	9.5414	805	569	548	542	552	563
Ī	9.5425	810	569	550	543	553	564
	9.5439	815	569	550	543	553	564
	9.5453	820	569	550	543	553	564
[-	9.5467	825	569	550	544	553	564
	9.5481	830	569	550	544	555	564
	9.5494	835	569	550	544	555	566
	9.5508	840	569	550	545	555	566
	9.5522	845	569	550	545	555	566
	9.5536	850	569	550	545	555	566
	9.555	855	569	550	545	555	566
	9.5564	860	569	550	545	556	566
	9.5581	865	569	550	546	556	566
	9.5594	870	568	550	546	556	566
	9.5608	875	568	550	546	556	566
	9.5622	880	568	550	546	556	566
	9.5636	885	568	550	546	556	566
	9.565	890	568	550	546	556	566
	9.5664	895	567	550	548	556	567
	9.5678	900	567	550	-		567
	9.5689	905	567	550			567
	9.5703	910	567	550	-	557	567
	9.5717	915	•	550		557	567
1	9.5731	920	567	550	•- •	•	567

Panel Cold Fill Test: 12/01/93

CRTF	Panel Col	d Fill Test,		<u> </u>	l	
TEST		1st pass	2nd pass			Upper he
Time		TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	DEG F	DEG F	DEG F	DEG F
9.5744	925	567	550	548	557	567
9.5758	930	567	550	548	557	567
9.5772	935	567	550	548	556	567
9.5786	940	567	550	548	554	567
9.58	945	567	550	548	552	567
9.5814	950	567	550	548	549	567
9.5831	955	567	550	548	548	567
9.5844	960	567	550	548	547	567
9.5858	965	567	550	548	546	567
9.5872	970	567	550	548	546	567
9.5886	975	. 567	550	548	545	567
9.59	980	566	550	548	545	567
9.5914	985	566	550	548	545	
9.5928	990	566	550	550	545	
9.5942	995	565	550		•	· · · · · · · · · · · · · · · · · · ·
9,5953		565	550	·	543	
9.5967		565	550	550		
9.5981	1010	· · - · · · · · · · · · · · · · · · · ·	550			
9.5994	1015	· ·	550			567
9.6008			550			566
9.6022		564	550	· · · · · · · · · · · · · · · · · · ·		
9.6036	1030		550	550		566
9.605	1035	564	550	550	557	566
9.6064	1040	564	550	550	557	566
9.6078	1045	564	550	550		566
9.6092	1050	564	550	549		
9.6106	1055	564	550	549		566
9.6122	1060	564	550	549	557	566
9.6136	1065	564	550	549	557	566
9.615	1070	564	550	549	557	
9.6164	1075	564	550			566
9.6178	1080	564	550	549	557	565
9.6192	1085	564	550	549	557	565
9.6206	1090	564	550	549	557	565
9.6219	1095	564	550	549	557	565
9.6233	1100	564	550	549	557	565
9.6244	1105	564	550	549	557	565
9.6258	1110	564	550	550	557	565
9.6272	1115	564	549	550	557	565
9.6286		564	549	550	557	565
9.63		564	549	550	557	565
9.6314		564	549	550	557	565
9.6328		564	549	550	558	565
9.6342	·	564	549	550	558	566
9.6356	·		550		558	566

Panel Cold Fill Test: 12/01/93

CRTF	Panel Col	d Fill Test,			4.1.	
TEST		1st pass	2nd pass		4th pass	Upper he
Time	<u>+</u>	TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	·	DEG F	DEG F	DEG F
9.6369		·	550	550	·	566
9.6383			550		558	566
9.64			550		558	566
9.6414			550		558	566
9.6428			550		558	. 566
9.6442			550		558	566
9.645				551	558	566
9.6469				551	· · · · · · · · · · · · · · · · · · ·	566
9.6483			550	551	558	566
9.6497			550	551	559	·
9.651		·	550		559	
9.6522		·	550	551		
9.653			550	551		•
9.655	•		550			
9.656						
9.6578			551	551		
9.659	2 1230	574	555	551		
9.660	5 1235	576	557	551		·
9.6619	9 1240	577	559	551	560	567
9.663	3 1245	578	561	554	561	568
9.664	7 1250	579	562	555	562	570
9.666	1 1255	579	562	558	563	571
9.667	5 1260	580	563	558	566	572
9.668	9 1265	580	563	559	566	573
9.670	3 1270	580	565	560	567	574
9.671	7 1275	580	565	560	568	574
9.673	1 1280	580	565	561	568	575
9.674	4 1285	580	565	561	570	576
9.676	1 1290	580	565	563	570	578
9.677	5 1295	580	565	563	571	578
9.678		580	566	563	571	578
9.680	3 1305	580	566	564	571	579
9.681	7 1310	577	566	564	571	579
9.683				·	571	579
9.684		•				579
9.685		+		•		579
9.687						579
9.688			·	·		- L
9.6			•			
9.691		•				
9.692			•			
9.693		·				
9.695		+				
9.696					•	
9.698						

Panel Cold Fill Test: 12/01/93

CRTF	Panel Col	d Fill Test,	12/01/93			
TEST		1st pass	2nd pass	3rd pass	4th pass	Upper he
Time		TEW4	TEW17	TEE12	TEE9	TEWUH19
hour	Time	DEG F	DEG F	DEG F	DEG F	DEG F
9.6994	1375	564	550	553	560	570
9.7008	1380	564	550	553	560	569
9.7022	1385	564	550	552	559	569
9.7036	1390	564	550	552	559	568
9.705	1395	564	550	552	559	568
9.7064	1400	564	550	552	559	568

Cold Fill Test of 2 inch Pipe

_	Cold Pipe Test Schedule 40, 2in pipe									
	pt. 24, 19						, 524 F	:		
	pi. 24, 17	Outsic					leg F			
 -	hannel	439				443		445		
	s:Min:Sec	407	140	771	772	440	777	-1-10		
 '''	9:16:55	367	262	103	99	96	126	613		
-	9:17:00		263	103	99			613		
	9:17:05	363			99	96		613		
-		362	263	103	99			613		
-	9:17:10	362	263	103	98	96 96		613		
-	9:17:15 9:17:20	362 361		103						
	9:17:25	363	263 263	104						
-	9:17:23				99		126			
·		363	262	103	99					
-	9:17:35	361	262	103						
	9:17:40									
}	9:17:45		281	144						
	9:17:50	444	302			124				
	9:17:55	462	320	240	191	152		592		
	9:18:00	475	341	292	230					
	9:18:05	~~	358	344		•				
	9:18:10	493	377	393		•				
-	9:18:15	496	391	421						
	9:18:20	_496	405	445	416					
1	9:18:25	499	415	458			420			
ļ	9:18:30	500	425				451			
	9:18:35	+				•				
	9:18:40									
L	9:18:50	507	455			·				
.	9:18:55	507	460	501	501		•			
	9:19:00	_508_	465			•	·	•		
	9:19:05		468					•		
	9:19:10	508	472				· ·			
	9:19:15	509	475		512					
	9:19:20	509	478	511	513	_515	512	532		
	9:19:25	511	480	511	513	515	512	_532		
	9:19:30	511	483	514	515	517	514	532		
	9:19:35	511	485	514	517	518	515	532		
	9:19:40	511	487	515	517	519	516	532		
	9:19:45	510	488	516	519	519	515	532		
	9:19:50	513	490	517	519	519	·	•		
-	9:19:55	511	491	517	518	·	·	·		
	9:20:00	513	493	517	519			·		
	9:20:05	513	495					·- ·		
-	9:20:10	515	495	518	521			•		
	9:20:15	514	497	519				•		
	9:20:20	514	497	520		·	+	•		
-	9:20:25	516	498	519	+	522	· · · · · · · · · · · · · · · · · · ·			
	9:20:30	514			522	·		•		
	9:20:35				•	•	· · · · · · · · · · · · · · · · · · ·	•-		
	7.20.00	010	7//	<u> </u>		<u> </u>	520			

Cold Fill Test of 2 inch Pipe

Cold Pipe	Test		Sche	dule 4	0, 2in	pipe			
Sept. 24, 1	993		Salt Te	empe	rature	, 524 [-		
	Outsid	ide Pipe Temperature, deg F							
Channel	439	440	441	442	443	444	445		
Hrs:Min:Sec									
9:20:40	516	501	520	522	523	521	532		
9:20:45	517	502	520	523	523	522	532		
9:20:50	516	503	521	524	523	521	533		
9:20:55	516	503	520	524	524	522	533		
9:21:00	517	503	521	524	524	523	533		
9:21:05	516	504	521	524	524	523	533		
9:21:10	519	504	522	525	524	523	533		
9:21:15	518	505	522	524	524	522	533		
9:21:20	516	505	522	525	524	523	533		
9:21:25	517	505	522	525	525	523	533		
9:21:30	517	507	523	526	525	523	533		
9:21:35	517	507	523	526	525	524	533		
9:21:40	518	507	523	525	525	524	533		
9:21:45	517	507	523	525	526	524	534		
9:21:50	516	507	523	526	525	524	533		
9:21:55	518	508	523	526	525	525	533		
9:22:00	517	508	523	526	525	524	533		
9:22:05	519	508	523	526	526	525	533		
9:22:10	518	509	523	527	526	525	533		
9:22:15	519	507	523	526	525	523	532		
9:22:20	519	509	524	526	527	525	533		
9:22:25	518	510	524	527	527	525	533		
9:22:30	518	509	523	526	525	524	533		

	Total Bias	and Rando	m Uncertai	nty Percent	s and Urss	Uncertainti	ies			
Flow	FT-720 Vo	rtex Flow	PF-001 W	etted Ultra	PF-002 Cla	l ampon Ultr	FT-730 Vo	rtex	FT-800 Vo	intex
L/min	4-22	Random t95S/N^.5	Bias Bi	Random t95S/N^.5	i		Bias Bi	Random t95S/N^.5	Bias Bi	Random t95S/N^.5
Average			Ì				-	į		
Flow, It/mir	%	%	%	%	%	%	%	%	%	%
102.58	9.76	0.63				0.50	9.90	0.47	5.29	0.44
155.40	11.58	0.29	4.14	0.51	12.78	0.55	11.55		7.29	0.27
197.41	12.56	0.18	4.56	0.44	12.97	0.42	12.50	0.22	8.48	0.21
244.65	15.09	0.21	6.35	0.31	13.27	0.30	15.62			
Flow	Urss		Urss		Urss		Urss		Urss	
102.5759	9.77976		3.878089	_	8.485958		9.91473		5.310453	
155.3991	11.58529		4.168351		12.79488		11.55541		7.295545	
197.4063	12.55799		4.581304		12.97705		12.49935		8.48723	
244.6471	15.08722		6.358041		13.27571		15.62751			

	Bias and R	landom Un	certainty Pe	rcents Rela	ative to Bub	bler Refere	ence			
ľ									-	
Flow	FT-720 Vo	rtex Flow	PF-001 We	etted Ultra	PF-002 Cla	ampon Ultr	FT-730 Vo	rtex	FT-800 Vo	rtex
L/min	Bias	Random	Bias	Random	Bias	Random	Bias	Random	Bias	Random
	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5
Lt/min	%	%	%	%	%	%	%	%	%	%
245.07	15.52159	0.475089	6.862377	0.662462	-11.1397	0.488859	15.82366	0.481864		
245.07	13.99688	0.239153	4.261886	0.230269	-12.9097	0.200013	14.08849	0.290354		
196.22	12.42478	0.232202	3.896936	1.145752	-10.4407	0.944796	12.56068	0.435271	7.226531	0.348303
191.20	13.99572	0.071855	4.027049	0.149455	-10.8986	0.125255	13.66786	0.060468	9.22606	0.171739
155.47	12.56275	0.753997	4.490394	1.213737	-8.18096	1.074611	12.56275	0.674396	7.159739	0.480827
155.19	10.07565	0.12859	1.012406	0.081947	-12.3653	0.25961	10.29978	0.201509	5.663095	0.24198
102.99	8.110337	1.133905	0.300727	0.940323	-6.15803	0.721195	8.490264	0.658884	3.086858	0.699224
102.16	9.834467	0.130553	-0.22997	0.152059	-8.94488	0.272782	9.767941	0.282077	4.198763	0.17449
154.91	10.90267	0.179409	-0.45872	0.614047	-14.4883	0.671667	10.51535	0.412473	5.932066	0.129107
156.03	10.16607	0.099755	1.122052	0.125268	-13.7377	0.177755	10.1898	0.27912	6.035729	0.236388
200.13	11.02	0.299602	1.208081	0.386784	-13.964	0.498647	10.88372	0.25495	7.597939	0.187905
202.08	10.38117	0.10355	0.711803	0.070636	-14.2525	0.116727	10.46034	0.114129	6.214532	0.137835
246.46	13.39638	0.089405	3.323362	0.277316	-14.7587	0.349742	14.27843	0.499605		
242.00	15.44113	0.048174	5.7871	0.059108	-12.0118	0.152921	16.38737	0.134167		

	Bias and R	andom Un	certainty Le	vels Relativ	ve to Bubble	er Referenc	e			
Flow	FT-720 Vo	rtex Flow	PF-001 We	etted Ultra			FT-730 Vo	rtex	FT-800 Vo	rtex
L/min	Bias	Random	Bias	Random	Bias	Random	Bias	Random	Bias	Random
	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5	Bi	t95S/N^.5
Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min	Lt/min
245.07	38.04	1.164281	16.82	1.623467	-27.30	1.198025	38.78	1.180883		
245.07	34.30	0.586083	10.44	0.564311	-31.64	0.490163	34.53	0.711559		
196.22	24.38	0.455627	7.65	2.248196	-20.49	1.853879	24.65	0.85409	14.18	0.68344
191.20	26.76	0.137384	7.70	0.285752	-20.84	0.239483	26.13	0.115611	17.64	0.328358
155.47	19.53	1.172231	6.98	1.886982	-12.72	1.670686	19.53	1.048475	11.13	0.747537
155.19	15.64	0.199558	1.57	0.127173	-19.19	0.402888	15.98	0.312721	8.79	0.375527
102.99	8.35	1.167861	0.31	0.968482	-6.34	0.742792	8.74	0.678615	3.18	0.720163
102.16	10.05	0.133369	-0.23	0.15534	-9.14	0.278667	9.98	0.288162	4.29	0.178255
154.91	16.89	0.277923	-0.71	0.951224	-22.44	1.040483	16.29	0.638965	9.19	0.2
156.03	15.86	0.155645	1.75	0.195453	-21.43	0.277347	15.90	0.435503	9.42	0.36883
200.13	22.05	0.599587	2.42	0.774063	-27.95	0.997932	21.78	0.510226	15.21	0.376051
202.08	20.98	0.209255	1.44	0.142743	-28.80	0.235883	21.14	0.230634	12.56	0.278538
246.46	33.02	0.220348	8.19	0.683476	-36.37	0.86198	35.19	1.231332		
242.00	37.37	0.11658	14.00	0.14304	-29.07	0.370062	39.66	0.324677		

Percent	FT-720 Vo	rtex Flow	PF-001 W	etted Ultra	PF-002 Cla	ampon Ultr	FT-730 Vo	rtex	FT-800 Vo	rtex	East Cal	West Cal	Total Cal	Num of pts	t95
Flow							Ave	Std	Ave	Std				N	
	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min	L/min		
														T -1	
100	283.10	5.11	261.88	7.12	217.77	5.26	283.84	5.18			103.55	141.51	245.07	77.00	2
100	279.37	2.57	255.51	2.48	213.43	2.15	279.59	3.12			103.55	141.51	245.07	77.00	2
80	220.60	0.83		4.09	175.73	3.37	220.87	1.55	210.40	1.24	89.88	106.34	196.22	15.00	2.131
80	217.96	0.56		1.17	170.36	0.98	217.33	0.47	208.84	1.34	91.55	99.65	191.20	67.00	2
60	175.00	2.51	162.45	4.05		3.58	175.00	2.25	166.60	1.60	84.01	71.45	155.47	20.00	2.086
60	170.83	0.68		0.43	136.00	1.37	171.17	1.06	163.98	1.27	84.01	71.18	155.19	46.00	2
40	111.35	2.71	103.30	2.24	96.65	1.72	111.74		106.17	1.67	77.87	25.12	102.99	23.00	2.069
40	112.20	0.68		0.79	93.02	1.41	112.14	1.46	106.45	0.90	77.87	24.28	102.16	103.00	2
60	171.80			2.61	132.47	2.85	171.20		164.10	0.55	84.29	70.62	154.91	30.00	2
60	171.89	0.57	157.78	0.72	134.59	1.02	171.93	1.60	165.44	1.36	84.29	71.73	156.03	54.00	2
80	222.18	1.72	202.55	2.22	172.18	2.87	221.91	1.47	215.33	1.08	90.71	109.41	200.13	33.00	2
80	223.06	0.74		0.50	173.28	0.83	223.22	0.82	214.64	0.98	91.27	110.81	202.08	50.00	
100	279.48	0.51	254.65	1.58	210.09	2.00	281.65	2.85			104.95	141.51	246.46	23.00	2.069
100	279.36	0.48	256.00	0.59	212.93	1.54	281.65	1.35			100.48	141.51	242.00	69.00	2
														Bias Errors	:
														Tank Dim:	0.5
														Therm.Exp	1.5
														Bubble Ca	3
														Prop. Vary	1.8
							-								
				,										Bias RMS	3.839271

Flow meter calibration data.

	CRTF	NET-		99 P	lay	DATA	FILE; 1994	11:28:4	12 am;						
me	Time	Time	Time		T720	PF-001	PF-002	FT730	FT800	PT72	0 C/	LE.FLOCALW.	FL(FCV80	00 LT700	LT899
ST	hour	min	sec		/min	Lt/min	Lt/min	Lt/min	Lt/min	PSIG			Lt/min	inch	Inch
.5341		11	32	3	288					57	56		_ 0	55	22
.5355		11	32	8:	288					60	56		.0).	55	22
.5369		11	32	13	288					57	56		0	_ 55 _	22
1.5383		11	32	18	283				38	64	56	0	0	61	22. –
.5397		11.	32	23	283				32	56	57	0	0	61	22.
.5411		11.	32	28	283				32	62	57		0	61	22
1.542		11	32	33	283					62	57 57	0	0	61	22
.5438		11	32	38:	283				32	62 ⁱ			0	55	22
1.5452		11.	32	43	283				32	56	57		0.	62	21
1.5466		11.	32	48.	283				32	59	<u>57</u>		- 0;	62	21.
5480		11	32	53	283				32	63		<u>0</u>	0	62	21
1 5494	-	11	32	58	283				82	63	<u>57</u> 57	- -0	0	62	20
1.5508		11.	33	3	283			⊸	B2 B2	59	<u>57</u> . 57	0	<u>o</u> ,	62	20
1.5522		11.	33	8.	283				82 	61	- <u>57</u> .	. <u>v</u> .	ö.	62	20
1.5536		.11.	33	13.	283				82		57	- 0	<u>o</u>	55	19
11.55		11	33	18	280				82 82	57 62	- 57		· 👸	62.	19
1 5563		11.	33	23	280				81	59'	57	0	− 0	62	19.
1.5577		11	33	33	280 280				B1	57	57	0	0 -	62	18
1.5591		11	33	38					81 B1	62	57	0	Ö,	62	18
1.5605		11.	33	43	280 280		<u> </u>		81 81	65	- 57 -		- 6	62	18
1.5619		. <u>11</u>	33	48	280	•			81 81	61	. <u>57</u> .	- <u>o</u> .	Ŏ.	62	18
1.5633						·			81 <u>.</u>	60	57		. 0	62 62	18
1.5647		11	33	53	280				81	59	57	0	<u>0</u>	56	18
1.5661		11	33	58	280				81	63	57		- 0	63	18
11.567		11	34.	<u>3</u> 8	280				81 81	60	57		- 0	57	18
1 5688		11.	$\frac{34}{24}$.						81	62	57		<u></u>	62	18
1.5702		<u>.11</u>	34	13	280				81	53	57		0 -	53	18
1.5719			_34	19 24	28				82	66	57			66	18
1.5733		11	34		28				82 82	64	57		- 0	66	19
1.5747		11.	34	29	28				82	61	57	0	- 0 -	66,	19.
1.5761		11.	34	34	28				82		57		0	57 	20
11.577		11	34	39	28					61	57	<u>o</u>	· · · · · · · · · · · · · · · · · · ·	63	20
1.5788		11.	34	44.	28				82	61.	57	0	- 0	57	20
1.5802		.11	34	49	28				82	61	57		- 0	57	21
1.5816		11	34	54	28				82! 82'	60	57			63	21
1.5830		11,	34	59	_ 28				82		57	0	- ö	63	21
1.5844		11.	35	4	28				82	60	57	0 ;	0	63	21
11.5858		11,	35 35	- 9	28				82	61	- 57 -	0	- <u>0</u> .	63	21
1.5872		11	35	14	280				43	61	56		0	63	22
1.5886	_+		·	24	33				29	61	43,	0	0	57	22
<u>11.5</u> 11.5913		. <u>11.</u> 11	35 35	29	34				51	52	38		o,	57	22
1.5913			35	34	34				57	57	34	5	<u>0</u> ;	57	22
		11				•			63	57.	32	0,	0	50	23
1.5941		11.	<u>35</u> 35	39_ 44	349	·			63	47	30		0	50	23
1.5955			35	44-	35				69	47	31	0,	0.	24	23
1.5969		· 11							44	- 1 /2	41			5	23
1.5983		11	35	54	34				26	2	48	Ö	0.	5	23
1.5997		11.	35 36	<u>59</u>	_ 32 31				99	2	57	0	- 0-	5	23
1.6011					· -				82		64		0	5	23
11.602		11.	36 36	14	<u>30</u>				59	2	71	0	- <u>ō</u>	5	23
1.6052		-11	36	19	27	·			46	- 2	/ 		0	5 5	23
1.6052		11	36	24	27				21	- 2	80	—— 0 ·-·	0	5	23
1.6080		- 11	36	29	26				11	2	82		.0.	5 5	23
1.6094		11.	36	34	26				5.	2	85:	0	- 0 -	5	23
1.6108		11	36	39		···			16	-2	86		. 0	5 5	24
1.6122		11	36	44	26				32	26	66		0	44	24
1 6136		11	36	49	32	- 			16:	63	50		· -0 1 · -	63	24
11.61		11.	36	54	33				39	58	41.		· 0	57	23
1.6163		11	36	59	31				100	54	43		0	- 51	23
1.6177		11	37	⁵⁹	30				100	54 ·	48	<u>o</u>	0,	57	23
1.6177		11	37	9	29				93	57	50		0	57 57	23
										62	53	0	0	65	23
1.6205		11.	37	. 14	29				88				0	58	22
1.6219			37	19	28				88	63	54	0	0	63	22
1 6233		11.	37	24	28				88	63	55 _.		-		
1.6247		_11_	37	29	28				88	59	55	- 0	0	63 _.	22
1.6261		<u> 11</u>	37	34	28				82	66	56	<u>-</u> 0.	0.		22
11.627		11	37	39	28				182	62	57	<mark>0</mark> .		63	22
1.6288		11	37	-44	28				82	62.	57 	_ 0	_ 0	63	22.
1.6302		11.	37	49	28				82	62	57	0:	0	63	22
11.6316		11	37	. 54_	28				82	65	. 57	0	0	63	22
1.6330			37	59	28				82	59	_ 57	· <u>0</u>	0_	63	22.
1.6344		11	38	4	28	· ·	59 22		82	63 _.	57	0	0,	63	22
	83	11	38	9	28	2 25	9 22	20 2	282	63	57	0	0	63	22

Flow meter calibration data.

44.00700	441	001	4.41	0001	orol	0001	0001	59]	57	Ol	0	63	22	16
11.63722	11	38	14	282	259	220	282		56	- 0	0	68	22	17
11.63861	11	38	19	303	259	220	235	67			0	60	22	17
11,64	11	38	24	342	277	220	103	58	40	0				18
11.64139	11	38	29	350	288	237	121	54	35	0	0	53	22	
11.64278	11	38	34	356	295	243	135	53	31	0	0	53	22	18
11.64417	11	38	39	356	306	243	141	53	29	0	0	53	22	19
11.64556	11	38	.44	356	311	234	146	49	27	0	0	47	22	19
11.64694	11	38	49	362	323	214	146	46	26	0	0	47	22	20
					323	201	152	46	24	0	0	47	22	20
11.64833	11	38	54	362										21
11.64972	11	38	59	362	323	201	152	42	24	0	0	41	23	
11.65111	11	39	4	362	329	196	158	34	23	0	0	35	23	21
11.6525	11	39	9	368	317	188	158	50	22	0	0	47	23	20
11.65389	11	39	14	368	312	188	164	45	22	0	0	47	23	19
11.65528	11	39	19	368	312	188	164	41	21	0	0	40	23	17
			24	368	312	178	164	44	20	0	0	40	23	15
11.65667	11	39									0	46	23	14
11.65806	11	39	29	368	331	172	164	47	20	0				
11.65944	11	39	34	368	331	172	169	48	20	0	0	46	24	11
11.66083	11	39	39	368	336	178	169	66	20	0	0	63	24	10
11.66222	11	39	44	368	329	178	162	5	23	0	0	4	24	8
11.66361	11	39	49	362	329	178	148	1	28	0	0	4	24	4
11,665	11	39	54	362	319	178	135	1	32	0	0	4	24	0
								- i -	38	0	0	4	24	0
11.66639	11	39	59	349	319	178	120					4	24	0
11.66778	11	40	4	343	319	178	106	1	42	0	0			
11.66917	11	40	9	338	319	183	94	1	47	0	0	4	24	0
11.67056	11	40	14	330	312	183	82	1	51	0	0	4	24	0
11.67194	11	40	19	316	309	196	68	1	56	0	0	0	24	0
11.67333	11	40	24	325	303	213	74	36	50	0	0	39	24	0
11.67472	11	40	29	348	298	221	118	42	38	0	0	42	24	ō
The state of the s										0	0	48	24	
11.67611	11	40	34	355	298	230	131	47	34					
11.6775	11	40	39	328	300	235	291	51	32	0	0	48	24	0
11.67889	11	40	44	322	294	235	313	54	36	0	0	54	23	0
11.68028	11	40	49	314	288	235	313	51	41	0	0	54	23	
11.68167	11	40	54	308	288	235	307	54	43	0	0	54	23	0
11.68306	11	40	59	301	288	235	307	54	46	0	0	54	23	0
	11	41	4	301	288	230	301	54	49	ō	0	55:	23	0
11.68444			9		282	230	295	57	50	0	0	55	23	
11.68583	11	41		295										0
11.68722	11	41	14	295	275	230	295	57	52	0	0 -	56	23	
11.68861	11	41	19	290	275	230	289	57	53	0	0	56	23	
11,69	11	41	24	290	275	225	289	60	54	0	0	56	23	0
11.69139	11	41	29	290	269	225	289	60	54	0	0	62	23	0
11.69278	11	41	34	290	269	225	289	60	55	0	0	62	23	O
11.69417	11	41	39	283	269	225	289	60	55	0	0	62	22	C
	11	41	44	283	263	225	283	63	56	0	0	62	22	<u> </u>
11.69556									56	0	0	62	22	0
11.69694	11	41	49	283	263	225	283	601						
11.69833	11	41	54	283	263	219	283	62	56	0	0	62	22	
11.69972	11	41	59	283	263	219	283	65	56	0	0	62	22	
11.70111	11	42	4	283	263	219	283	63	56	0	0	62	22	C
11,7025	11	42	9	283	263	219	283	63	56	0	0	62	22	C
11.70389	11	42	14	283	263	219	283	59	57	0	0.	62	22	C
11.70528	11	42	19	283	263	219	283	66	57	0	0	62	22	C
11.70667	11	42	24	283	263	219	283	62	57	0	0	62	22	
									57			59	22	<u>c</u>
11.70806	11	42	29	283	263	219	283	59		0				
11.70944	11	42	34	283	263	219	283	66	57	0	0	67	22	
11.71083	11	42	39	281	263	219	283	63	57	01	0	60	22	
11.71222	11	42	44	281	263	219	282	59	57	0	0	60	22	0
11.71361	11	42	49	281	260	219	282	62	58	0)	O ¹	66	22	C
11.715	11	42	54	281	260	217	282	61	58	0	0	58	22	<u> </u>
11.71639	11	42	59	281	260	217	282	56	581	0	0	58	22	C
11.71778	11	43	41	281	260	217	282	63	58	0	0	58	22	C
11.71917	11	43	9	281	260	217	282	63	58	0.	0.	65	22	C
		43	14	281	260	217	282	66	58	0	0:	65.	22	
11.72056	11							~	581	0	0	65.	22	
11.72194	11	43	19	281	260	217	282	64						
11.72333	11'	43	24	281	260	217	282	64	58	0!	0	65	22	C
11.72472	11	43	29	281	260	217	282	64	58	0:	0	65	22	C
11.72583	11	43	33	281	260	217	282	61	58	0	0	65	22	
11.72722	11	43	38	281	260	217	282	64	58	0;	0	65	22	
11.72861	11	43	43	282	260	217	282	60	58	0,	0	59	22	
11.73	11	43	48	282	257	217	282	60	58	0)	0	59.	22	
								57	58	0		59	22	
11.73139	111	43	53	282	257	217	282							
11.73278	11	43	58	282	257	217	282	61!	58	<u>0</u> ;	0,	65	22	
11.73417	11	441	31	282	257	217	282	60:	58	0	0,	59	21	
11.73556	11	44	8	282	257	217	282	64	58	Ο,	0	59	21	(
11.73694	11	44	13	282	257	217	282	57	58	0	0	59	20	8
11.73833	11	44	18	282	257	217	282	59	58	0,	0:	59	20	10
					257			62	58	0	0	66	20	13
11.73972	11	44	23	282		217.	282					59	19	15
11.74111	11	44	28	282	257	217	282	58	58	0	<u>0</u> ;			
11.7425	11	44	33	282	257	217	282	60	58	0,	0;	59	19,	15
11.74389	11	44	38	282	257	217	282	67	58	0	0	66	19	20
	11	441	431	280	257	217	284	62	58	0:	0;	60	18.	22
11.74528				-501										

Flow meter calibration data.

11.74667	11	44	48	280	257	217	284	64	57	0	0	60	18	24
11.74806	11	44	53	280	263	213	284	61	57	0	0	60	18	27
11.74944	11	44	58	280	263	213	284	57	57	0	0	60	18	27
11.75083	11	45	3	280	263	213	284	61	57	0	0,	60	18	27
11.75222	11	45	8	280	263	213	284	66	57	0	0	66	19	25
11.75361	11	45	13	280	263	213	284	66	57	0	00	66	19	21
11.755	11	45	18	280	258	213	284	62	57	0	0	60	19	18
11.75639	11	45	23	280	258	213	284	62	57	0	0	60	20	13
11.75778	11	45	28	280	258	213	284	62	57	0	0,	60	20	10
11.75917	11	45	33	280	258	213	284	58	57	0	0	60	21	7
11.76056	11.	45	38	280	258	213	284	59	57	0	0.	60	21	
11.76194	11	45	43	281	258	213	280	59	57	0	0	60	21	
11.76333	11	45	48	281	258	213	280	59	58	0	0	60	21	
11.76472	11	45	53	281	258	213	280	63	58	0	0	60	22	- (
11.76611	11	45	58	281	258	213	280	62	58	0	0	60	22	— - `
11.7675	11	46	3	281	258	213	280	59	58	0	0	60	22	
11.76889	''	46	8	281	258	213	280	59	58	0	0	60	22	`
11.77028		46		281	258				58	0	0		22	
	11,		13			213	280	60				60		
11.77167	11	46	18	281	258	213	280	55	58	0	0	58	22	
11.77306	11.	46	23	281	258	213	280	59	58	0	0	58	22	
11.77444	11	46	28	281	258	213	280	63	58	0	0'	65	22	
11.77583	11	46	33	281	258	213	280	60	58	0	0	58	22	9
11.77722	111	46	38	281	258	213	280	60	58	0	0	58	22	(
11.77861	11	46	43	282	258	213	282	60	58	0	0	58	22	_ (
11.78	11	46	48	282	258	213	282	65	58	0	0	65	22	(
11.78139	11	46	53	282	258	216	282	60	58	0	0	59	22	(
11.78278	11	46	58	282	258	216	282	57	58	0	0	59	22	(
11.78417	11	47	3	282	258	216	282	62	58	0	0	59	22	
11.78556	11	47	8	282	258	216	282	58	58	0	0	59	22	(
11.78694	11	47	13	282	258	216	282	62	58	0	0	65	22	
11.78833	11	47	18	282	258	216	282	61	58	0		65	22	
11.78972	11	47	23	282	258	216	282	61	58	0	0	65	22	
11.79111	11	47	28	282	258	216	282	62	58	0	0;	58	22	
11.79278	11	47	34	282	258	216	282	63	58	0	<u> </u>	58	22	
11.79417	11	47	39	281	258	216	282	60	58	0	0	58	<u></u> .	
11.79556	11	47	44	281	258	216	282	59	58	0	0:	58	21	
11.79694	11	47	49	281	258	216		56	58	0	0,	58		
							282						21	5
11.79833	11	47	54	281	258	215	282	63	58	0	0.	64	_21	}
11.79972	11.	47	59	281	258	215	282	57	58	0	0	_57	20	
11.80111	11	48	4	281	258	215	282	57	58	0	0	_ 57	20	_ 12
11.8025	11	48	9	281	258	215	282	60	. 58	0:	0	. 57	19	14
11.80389	11	48	14:	281	258	215	282	59	58	0	0	62	19	16
11.80528	11	48	19	281	256	215	282	57	58	0	0	62	19	18
11.80667	11	48	24,	281	256	215	282	60'	58	0	0	62	18	20
11.80806	11	48	29	281	256	215	282	63	58	0	0	62	18	23
11.80944	11	48	34	281	256	215	282	59	58	0	0	62	18	25
11.81083	11	48	39	280	256	215	282	64	58	0	0,	62	18	27
11.81222	11	48	44	280	256	215	281	64	58	0	· · · · ·	62	18	28
11.81361	11	48	49	280	256	215	281	64	57	0	0;	62	18	26
11.815	11	48	54	280	256	214	281	59	57	0	0	62	18	27
11.81639	11	48	59	280	256	214	281	63	57	0	0	61	19	24
11.81778	11	49	4	280	256	214.	281	60	57	 0'	0	59	19	2
11.81917	11	49	9	280	256	214	281	57	57	0		59	19	17
11.82056		49	14	280	256	214	281	60	57	0	0	60	20	14
													~	
11.82194	11	49	19,	280	256	214	281	60	57	0:	0.	60		}
11.82333	11.	49	24	280	256	214	281	98	57	0		98.	21	:
11.82472	11	49	29	280	256	214	281	123	57	0	0.	123	21	3
11.82611		49	34	280	256	214	281	127	57	0	0,	127	21	
11.8275	11	49	39	281	256	214	281	125	58	0	0.	121	21	(
11.82889		49	44	281	256	214	280	120	58	0	0,	121	22_	0
11.83028	11	49	49	281	256	214	280	211	58	0	0	188	22	
11.83167	11	49	54	281	256	212	280	226	59	0	0	223	22	
11.83306	11	49	59	281	256	212	280	236	59	0	0	231	22	Ţ,
11.83444	11	50	4	281	256	212	280	236	59	0	o	236	22	(
11.83583	11	50	9	281	256	212	280	239	59	0	0	236	22	- (
11.83722.	11	50	14	281	256	212	280	237	59	0	0	242	22	Č
11.83861	11	50	19,	281,	255	212	280	260	60	0		254	22	Ö
	11	50	24	275	255	212	280	270	61	0	0	270	22	- 6
11.84	11	50	29	275	255	212	274	270	61	0	0	270	22	`
		50	34	275	255	212	274	272	62		0	270	22	
11.84139	11		39	275	255	212	274	272	62	0	0	270		
11.84139 11.84278	11	50	051		255						·		22	
11.84139 11.84278 11.84417	11	50	44		(33	212	274	272	62	0	. 0	270	22	(
11.84139 11.84278 11.84417 11.84556	11	50	44	275		010	0741	070			^	070		
11.84139 11.84278 11.84417 11.84556 11.84694	11 11 11	50 50	49	275	250	212,	274	272	62	0	0	270	22	
11.84139 11.84278 11.84417 11.84556 11.84694 11.84833	11 11 11 11	50 50 50	49 54	275 275	250 250	209	274	272	62	0	0	270	22	. (
11.84139 11.84278 11.84417 11.84556 11.84694 11.84833 11.84972	11 11 11 11 11	50 50 50 50	49 54 59	275 275 275	250 250 250	209 209	274 274	272 272	62 62	0	0	270 270	22 22	(
11.84139 11.84278 11.84417 11.84556 11.84694 11.84833 11.84972 11.85111	11 11 11 11 11	50 50 50 50 51	49 54 59 4	275 275 275 275	250 250 250 250	209 209 209	274 274 274	272 272 268	62 62 63	0 0 0	0 0 0	270 270 268	22 22 22	· · · · · (
11.84139 11.84278 11.84417 11.84556 11.84694 11.846833 11.84972 11.85111 11.8525	11 11 11 11 11 11	50 50 50 50 51 51	49 54 59 4 9	275 275 275 275 275 275	250 250 250 250 250 250	209 209 209 209	274 274 274 274	272 272 268 257	62 62 63 63	0 0 0	0 0 0 0	270 270 268 257	22 22 22 22	((
11.84139 11.84278 11.84417 11.84556 11.84694 11.84833 11.84972 11.85111	11 11 11 11 11	50 50 50 50 51	49 54 59 4	275 275 275 275	250 250 250 250	209 209 209	274 274 274	272 272 268	62 62 63	0 0 0	0 0 0	270 270 268	22 22 22	· · · · · (

Flow meter calibration data.

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11.85667	11:	51	24	268	250	209	268	244	66	0	0	244	22	0
11.85806	11	51	29	268	250	209	268	244	67	0	0	244	22	0
11.85944	11	51	34	263	244	209	268	244	68	0	0;	245	22	0
11.86083	11	51	39	263	244	204	262	239	70	0	0)	238	22	0
11.86222	11	51	44	263	244	204	262	239	71)	0	0	238	22	
11.86361	11,	51	49	256	244	204	256 256	239	72 73	0	0	238	22	0
11.865	11	51	54	256		204		242	73	0	0	238	22	- 0
11.86639	11	51	59	256	239	204	256 256	239	74	0	0	236	22	- 0
11.86778	11	52	4	256	239	199	250	228	76	0	0	228	22;	0
11.86917	11	52	9	251				228	78	ol	0	228	22	 0
11.87056	11	52	14	251	233	199 194	250 243	228	79	0	0	228	22	- 6
11.87194	11	52	19	244	233	194	243	228	80	-0	0	228	22	
	11	52	24	244	227	194	243	228	80	0	ŏ	228	22	-
11.87472		52	34	244	227	194	243	228	81	0	0	223	22	 6
11.87611	11	52 52	39	238	227	189	243	218	83	0	0	216	22	- 6
11.87889	11	52	44	232	222	189	238	216	85	0	0	216	22	<u>ō</u>
11.88028	111	52	49	232	222	189	231	213	87	01	0	209	22	0
11.88167	11	52	54	226	216	184	225	208	89	0	Ö	209	22	ō
11.88306	11	52	59	226	216	184	225	208	90	0	0	209	22	0
11.88444	11	53	4	221	211	184	225	208	90	0	0	209	22	0
11.88583	11	53	9	221	211	178	221	208	91	0	0	209	22	0
11.88722	11	53	14	221	206	178	221	208	91	0	0	209	22	0
11.88861	11,	53	19	221	206	178	221	211	91	0)	0	209	22	. 0
11,89	11	53	24	221	206	178	221	211	91	0	0	209	22	0
11.89139	11	53	29	221	206	178	221	211	91	0;	O _i	209	22	0
11.89278	11.	53	34	221	206	178	221	211	91	0	0;	212	22	0
11.89417	11,	53	39	221	206	173	221	211	91	0	0	212	22	0
11.89556	11	53	44	221	200	173	221	211	91	0	0	212,	221	0
11.89694	11	53	49	221	200	173	221	211	91	0	0	212	22	0
11.89833	11	53	54	221	200	173	221	211	91	0	0	212	22	0
11.89972	11	53	59	221	200	173	221	211	92	0	0,	212	22	0
11.90111	11	54	4	219	200	173	221	211	92	0	0,	212	22	0
11.9025	11	54	9	219	200	173	218	211 ⁱ	92	0	O;	212	22	0
11.90361	11	54	13	219	200	173	218	211	92	0	0	212,	22	0
11,905	11	54	18	219	200	173	218	211	92	0	0	212	22	0
11.90639	11	54	23	219	200	173	218	211	92	0]	0	212	22	0
11.90778	11	54	28	219	200	173	218	211	92	0	0	212	22	0
11.90917	11	54	33	219	200	173	218	211	92	0	0	210	22	0
11.91056	11	54	38	219	200	171	218	211	92	0	0	210	22	0
11.91194	11	54	43	219	200	171	218	211	92	0	0	210	22	0
11.91333	11	54	48	219	200	171	218	211	92	0	0	210	22	0
11.91472	11	54	53	. 219	200	171	218	211	92	0	0	210	22	0
11.91611	11	54	58	219	200	171	218	211	92 92	0	0	210	21	2
11.9175	11	55	3	218	200	171	218	211	92	0	0	210	211	7
11.91889	11	55	8	218	200	171	218	210	92	0	0	210	20	8
11.92028	11	55 55	13 18	218	200	171	218	210	92	0	0	210	20	11
11.92167	11	551	23	218	200	171	218	210	92	0	0	210	20	12
11.92444	11	55	28	218	200	171	218	210	92	 	ol	210	20	15
11.92583	11	55	33	218	200	171	218	210	92	ol ol	ol	209	19	16
11.92722	11	55	38	218	200	171	218	210	92	0	0	209,	19	18
11.92861	111	55	43	218	200	171	218	210	92	0	0	209	19	20
11.93	11	55	48	218	199	171	218	210	92	0	ol o	209	191	23
11.93139	11	55	53	218	199	171	218	210	92	ol ol	o	209	18	25
11.93278	11	55	58	218	199	171	218	210	92	0	o o	209	18	27
11.93417	11	56	3	217	199	171	218	207	92	o	O	209	18	27
11.93556	11	56	8	217	199	171	217	207	92	0	0	209	18	26
11.93694	11	56	13	217	199	171	217	210	92	O	0	209	19	21
11.93833	11	56	18	217	199	171	217	210	92	0	0	209	19	17
11.93972	11	56	23	217	199	171	217	207	92	0	0	209	20	13
11.94111	11	56	28	217	199	171	217	207	92	0	0	209	20	8
11.9425	11	56	33	217	199	171	217	207	92	0	0	207	21	5
11.94389	11	56	38	217	199	170	217	207	92	0	0	207	21	1
11.94528	11	56	43	217	199	170	217	207	92	0	0	207	21	
11.94667	11	56	48	217	200	170	217	210	92	0	0	207	22	
11.94806	11	56	53	217	200	170	217	210	92	0	0	207	22	1
11.94944	11	56	58	217	200	170	217	208	92	0	0	207	22	1
11.95083	11	57	3	218	200	170	217	208	92	0	0	207	22	1
11.95222	11	57	8	218	200	170	217	208	92	0	0	207	22	1
11.95361	11	57	13	218	200	170	217	208	92	0	0	207	22	1
11,955	11	57	18	218	200	170	217	208	92	0	0	207	22	1
11.95639	11	57	23	218	200	170	217	208	92	0	0	207	22	1
11.95778	11	57	28	218	200	170	217	208	92	01	0	207	22	1
11.95917	11	57	33	218	200	170	217	208	92	0)	0	209	221	1
11.96056	11	57	38	218	200	170	217	208	92 92	0	0	209	22	C
					200	1701	047		091	an i				- (
11.96194	11	57	43	218	200	170	217	208						
	11 11 11	57 57	43 48 53	218 218 218	198 198	170	217	208 211	92	0	0	209	22	- 0

Flow meter calibration data.

11.96611	11	57	58	218	198	170	217	208	93	0	0	209	22.	(
11.9675 1.96889	11.	58	3	218	198	170	217	208	93		0	209	22	
.96889	11	. <u>58</u> 58	<u>8</u>	218' 218	198	170 170	217	208	93	0	_0_	209 209	22 22	Ċ
97167	11	58	18	218	198:	170	217			0	- 0.	~ -		Ċ
.97306	11	58	23	218	198	170	217	208	93	0.	<u>.0</u> , _	209 209	22 22	Ċ
.97444	11	58	28	218	198	170	217	208	93		<u>0</u> .	209	22	,
.97583	11	58	33	218	198	170	217	208	93	0	0	209	21	
.97722		58	38	218	198	169	217	208	93	0		209	21	-
.97861	11	58	43	218	198	169	217	208	93	0	0	209	21.	- 6
11.98	- 11	58	48	218	197	169	217	208	93	0:-		209	20	ě
.98139	11	58	53	218	197	169	217	208	92	0.		209	20	10
.98278	11	58	58	218	197	169	217	208	92	0	0	209	20	12
1.98417	11	59	3	218	197	169	217	208	92	· 0 -	0	209	20	14
.98556	11 *	59	<u>_</u>	218	197	169	217	208	92	<u>0</u> -	0	209	19	16
.98694	11	59	13	218	197	169	217	208	92	_ <u>v</u> .	o.	209	19	18
.98833	11	59	18	218	197	169	217	208	92	0	. 0	209	19	20
.98972	11	59	23	218	197	169	217	208	92	0	0	209	19	23
.99111	11	59	28	218	197	169	217	208	92	0	0	209	18	24
1.9925	11	59	33	218	197	169	217	208	92		0	209	18	27
.99389	11	59	38	218	197	170	217	208	92	0	0	209	18	27
.99528	11	59	43	218	197	170	217	208	92	0	0	209	18	27
1.99667	11	59	48	218	198	170	217	208	92	0	o [.]	208	19	25
1.99806	11	59	53	211	198	170	210	187	96	0	0	187	19	19
1.99944	11	59	58	206	198	170	204	187	98	0	0	187	20	15
2.00083	12	0	3	199	192	170	204	187	99	0	0	187	20	10
2.00222	12	0	8	199	192	164	198	187	100	0	0	187	21	ē
2.00361	12	0	13	199	187	164	198	187	101	0	0	187	21	2
12.005	12	0	18	199	187	164	198	189	101	0	0	187	21	Ç
2.00639	12	0	23	199'	187	160	198	189	101	0	0	187	22	(
2.00778	12	0	28	199	187	160	198	180	102	0	0	176	22	(
2.00917	12	0	33	186	182	160	192	174	105	_0_	0	176	22	2
2.01056	12	0	38	186	182	154	186	176	105	0_	. 0	176	22	C
2.01194	12	0	43	186	176	154	186	176	105	0	_ 0_	176	22	_(
2.01333	12	0	48	186	176	154	186	174	106	0	0,	176	22	C
2.01472	12	0	53	186	171	149	181	174	106	0	0	176	_ 22	C
2.01611	12	0	58	180	171	149	181	171	107	0	0,	168	22	0
12.0175 2.01889	12.		3	180	171	149	181	167	108	0	. 0	168	22	0
2.02028	12 12	1	8	180	166	149	175_	167	108	0	.0	168	22.	0
2.02028	12		13	175	166	144	175	167	108	0	0	168.	22.	C
2.02306	12	1 -	<u>18</u> 23	175	166	144	175	167	109	0.	. 0.	168	22	0
2.02444	12.		28	175 175	166 166	144	<u> 175</u> -	167	109	. 0,	0	168	22	0
2.02583	12	1 -	33	175			175 175		109	0.	0	168	22	0
2.02722	12	- i	38	175	160 160	144	175	167 167	109	-0-	0.	168	22	0
2.02861	12:	1	43	175	160	144	175	167	109	0.		168	22	- 0
12.03	12	:	48	175	160	144	175	164	109		0	168 168	22	0
2.03139	12	- i -	53	175	160	144	175	167	109		0	168	22	0
2.03278	12		<u>55</u>	175	160	139	175	167	109	0	. 0.	166	22 22	0
2.03417	12	2	3	175	160	139	175	167	109	<u>0</u> .	0	166	22	0
2.03556	12		8	175	160	139	173	167	109	0 ;	0.	166	22	0
2.03694	12	<u>~</u> .	13	172	160	139	173	167	109		0	166	21	2
2.03833	12	2	18	172	160	139	173	167	109	<u>0</u>	0.	166	21	3
2.03972	12	2	23	172	160	139	173	164	109	<u>0</u>	0	166	21	
2.04111	12	2	28	172	160	139	173	164	109	<u>0</u> .	. 0	166	21	7
2.0425	12	-	33	172	157	139	173	164	109		0	166	21	g
2.04389	12	2	38	172	157	139	173	164	109	ö	- 0	166	20	11
.04528	12	2	43	172	157	139	173	164	109	0'	0,-	166	20	13
.04667	12	2	48	172	157	139	173	164	109	0	ŏ	166	20	15
2.04833	12	2	54	172	157	139	173	164	109	<u>o</u> _		166	20	18
2.04972	12	2	59	172	157	136	173	164	109	0	0	162	19	19
2.05111	12	3	4	172	157	136	173	164	109	0	0	162	19	21
2.0525	12	3	9	172	157	136	171	164	109	0	0	162	19	23
2.05389	12	3	14.	170	157	136	171	164	109	0	0	162	19	25
.05528	12	_3	19	170	157	136	171	164	109	0	0	162	19	27
2.05667	12	3	24	170	157	136	171	165	109	0	_0,	162	18	29
2.05806	12	3	29	170	157	136	171	165	109	0	0	162	18	29
2.05944	12	3	34	170	157	136	171	165	109	0	0	162	19	27
.06083	12	3.	39	170	157	136	171	165	109	0	0	162	20	21
2.06222	12	3	44	170	157	136	171	165	109	0	0	162	20	16
2.06361	12	3	49	170	157	136	171	165	109	0	0	162	20	10
12.065	12	3	54	170	157	136	171	165	109	0	0	162	21	4
2.06639	12	3	59	170	157	135	171	165	109	0	0	165	21	1
2.06778	12	4	4	170	157	135	171	165	109	0	0	165	22	(
.06917	12	4	9	170	157	135	172	162	109	0	0	165	22	
	12	4	14	171	157	135	172	165	109	0	0	165	22	0
2.07056														-
2.07194	12	4	19:	171	157	135	172	165	109	0	0	165	22	0
		4	19: 24	171 171	157 157	135	172	165	109	0	. <u>0</u>	165 165	22 22	0

Flow meter calibration data.

12.07575 12	12.07611	12	4	34	171	157	135	172	165	109	0	0	165	22	(
20.07889 12															
20,00000 72												0			
12.08556						157	135		163	109	0	0	165	22	(
12,08464 12 5 6 717 157 177 172 168 1090 0 0 161 21	12.08167	12	4	54	171	157	135	172	163	109	0	O)	165		2
12,0055 12 8 9 171 157 137 170 168 108 0 0 161 21 12,00872 12 5 14 771 157 137 170 163 108 0 0 161 21 12 12,00881 12 5 2 171 157 137 170 163 108 0 0 0 161 22 12,00881 12 5 2 171 157 137 170 163 108 0 0 0 161 20 12 12 12 12 12 12 1	12.08306	12	4	59	171	157	137	172	163	109	0	0,			
12,09572 12 12 13 14 17 17 17 17 17 17 17	12.08444	12	· 5	4	171	157	137	172	163	109					
12.08691 12 8 19 1711 157 137 170 163 109 0 0 161 20	12.08583	12	5	9	171		137	170							
12,093 12 5	12.08722	12													9
12,0919 12	12.08861														. 11
12 12 12 13 14 17 15 15 15 17 17 17 16 16 10 10 10 16 16 18 18 18 18 18 18															13
	12.09139														15
12,005 12															17
12.05954															19
12,008572 12															21
12.0987 12 5 50 171 156 134 170 168 109 0 0 168 191 12.0082 12 6 3 171 156 134 170 168 109 0 0 158 181 12.0082 12 6 3 171 156 134 170 168 109 0 0 165 181 12.0081 12 6 13 170 156 134 170 168 109 0 0 165 181 12.0081 12 6 13 170 156 134 170 168 109 0 0 165 181 12.0081 12 6 13 170 156 134 170 168 109 0 0 0 165 181 12.0081 12 6 13 170 156 134 170 168 109 0 0 0 185 191 12.0089 12 6 23 170 156 134 170 168 109 0 0 0 185 191 12.0089 12 6 23 170 156 134 170 168 109 0 0 0 185 191 12.0089 12 6 23 170 156 134 170 168 109 0 0 0 150 191 12.0089 12 6 23 170 156 134 170 168 109 0 0 0 150 191 12.0089 12 6 23 170 156 134 170 168 109 109 0 0 0 150 191 12.0089 12 6 23 170 146 134 170 168 109 109 0 0 0 150 191 12.0089 12 6 23 170 146 134 170 168 140 100 0 0 120 21 12.0089 12 6 38 127 146 134 170 180 180 109 0 0 120 21 12.1194 12 6 38 127 148 170 170 170 170 180 180 0 0 120 22 12.1195 12 6 38 127 148 170															22 25
12.10083															26
12,10222 12															28
12.10361 12 e															29
12.105															29
12,10636															25
12 17 12 6															20
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1211156															10
															
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															(
	12.11611														
					115	113	101	110	105	120	0	0	108	22	
	12.11889		7	8	115	107	101	110	105	120	0	0		22	
12 12 12 12 13 15 10 10 10 10 10 10 10	12.12028	12	7	13	115	107	101	110	107	120					
	12.12167	12;	7	18	115	107	101	110							
12.12593	12.12306														
12.12722 12 7 38 115 102 96 1110 104 120 0 0 105 22	12.12444														
															(
T2,13 12 7 48 109 102 96 110 104 120 0 0 0 105 22 12,133 12 7 53 103 102 96 110 104 120 0 0 0 105 22 12,133 12 7 58 109 102 96 113 108 120 0 0 105 22 12,134 17 12 8 3 109 102 96 113 108 120 0 0 0 105 22 12,134 17 12 8 3 109 102 96 113 108 120 0 0 0 105 22 12,134 17 12 8 8 8 109 102 96 113 108 120 0 0 0 105 22 12,139 12 8 8 8 109 102 96 113 108 120 0 0 0 106 22 12,139 12 8 8 8 109 102 96 113 105 120 0 0 0 106 22 12,139 12 8 23 109 102 96 113 105 120 0 0 0 106 22 12,139 12 8 28 109 102 96 113 105 120 0 0 0 106 22 12,141 12 8 28 109 102 96 113 105 120 0 0 0 106 22 12,149 12 8 33 109 102 96 113 105 120 0 0 0 106 22 12,149 12 8 38 109 102 96 113 105 120 0 0 0 106 22 12,149 12 8 38 109 102 96 113 105 120 0 0 0 106 22 12,149 12 8 38 109 102 96 113 105 120 0 0 0 106 22 12,149 12 8 38 109 102 96 113 108 120 0 0 0 106 22 12,149 12 8 8 43 112 102 96 113 108 120 0 0 0 106 22 12,149 12 8 8 43 112 102 96 113 108 120 0 0 0 106 22 12,149 12 8 8 58 112 102 96 113 108 120 0 0 0 106 22 12,149 12 8 58 112 102 96 113 108 119 0 0 0 106 22 12,149 12 8 58 112 102 96 113 108 119 0 0 0 106 22 12,149 12 8 58 112 102 96 114 108 119 0 0 0 106 22 12,149 12 8 58 112 102 96 114 108 119 0 0 0 106 22 12,149 12 8 58 112 102 96 114 108 119 0 0 0 106 22 12,159 12 9 3 112 102 96 114 108 119 0 0 0 106 22 12,159 12 9 3 112 102 96 114 108 119 0 0 0 106 21 12,159 12 9 3 112 102 96 114 108 119 0 0 0 108 21 12,159 12 9 38 112 102 95 114 108 119 0 0 0 108 21 12,159 12 9 38 112 102 95 114 108 119 0 0 0 108 21 12,159 12 9 38 112 102 95 114 108 119 0 0 0 108 19 12,179 12 10 38 112 102 94 114 108 11							· · · · · · · · · · · · · · · · ·								(
12.15199 12															
12.13278 12															}
12.15556 12															
12,13694 12															
12,13833															
12,13972 12															
12.14111												0.	106		(
12,1425 12						102	96	113	105	120	0	0	106	22	(
12.14528 12			8	33	109	102	96	113	105	120	0	0	106	22	
12.14667	12.14389	12	8	38	109	102	96	113	108	120	0				
12.14806	12.14528	12	8	43	112			113							1
12.14944 12	12.14667														
12.15083 12 9 3 112 102 96 114 108 119 0 0 106 21 12.15222 12 9 8 112 102 96 114 108 119 0 0 108 21 12.1555 12 9 18 112 102 96 114 108 119 0 0 108 21 12.1556 12 9 23 112 102 96 114 108 119 0 0 108 21 12.1557 12 9 28 112 102 95 114 108 119 0 0 108 21 12.15778 12 9 33 112 102 95 114 108 119 0 0 108 21 12.15917 12 9 33 112 102 95 114 108 119 0 0 108 20 12.16916 12 9 38 112 102 95 114 108 119 0 0 108 20 12.16778 12 10 4 112 102 95 114 106 119 0 0 108 20 12.16917 12 10 9 112 102 95 112 106 119 0 0 108 20 12.16917 12 10 9 112 102 95 112 106 119 0 0 108 20 12.17056 12 10 14 112 102 95 112 106 119 0 0 108 19 12.17333 12 10 24 112 102 95 112 106 119 0 0 108 19 12.173531 12 10 28 112 102 94 112 106 119 0 0 108 19 12.17656 12 10 33 112 102 94 112 106 119 0 0 108 19 12.17361 12 10 28 112 102 94 112 106 119 0 0 108 19 12.173631 12 10 33 112 102 94 112 106 119 0 0 108 19 12.17661 12 10 38 112 102 94 112 106 119 0 0 108 19 12.17681 12 10 48 112 102 94 112 106 119 0 0 108 19 12.17681 12 10 48 112 102 94 112 106 119 0 0 108 19 12.17681 12 10 48 112 102 94 112 106 119 0 0 108 19 12.17681 12 10 48 112 102 94 112 107 119 0 0 108 19 12.18391 12 10 48 112 102 94 112 107 119 0 0 108 19 12.18656 12 11 8 112 102 94 111 107 120 0 0 108 19 12.18633 12 11 18 112 102 94 111 107 120 0 0 107 19	12.14806	12	8	53											
12.1522 12	12.14944														
12.15361 12															10
12.155 12 9 18 112 102 96 114 108 119 0 0 108 21 12.15639 12 9 23 112 102 95 114 108 119 0 0 108 21 12.15778 12 9 28 112 102 95 114 108 119 0 0 108 21 12.16056 12 9 38 112 102 95 114 108 119 0 0 108 20 12.16078 12 10 4 112 102 95 112 106 119 0 0 108 20 12.16917 12 10 9 112 102 95 112 106 119 0 0 108 19 12.17696 12 10 14 112 102 95 112 106															11
12.15639 12	·														14
12.15778 12 9 28 112 102 95 114 108 119 0 0 108 21 12.15917 12 9 33 112 102 95 114 108 119 0 0 108 20 12.16056 12 9 38 112 102 95 114 106 119 0 0 108 20 12.16778 12 10 4 112 102 95 112 106 119 0 0 108 20 12.16917 12 10 9 112 102 95 112 106 119 0 0 108 19 12.17956 12 10 14 112 102 95 112 106 119 0 0 108 19 12.1794 12 10 24 112 102 94 112 106 <td></td> <td>15</td>															15
12.15917															17
12.16056 12 9 38 112 102 95 114 106 119 0 0 108 20 12.16778 12 10 4 112 102 95 112 106 119 0 0 108 20 12.16917 12 10 9 112 102 95 112 106 119 0 0 108 19 12.17056 12 10 14 112 102 95 112 106 119 0 0 108 19 12.17194 12 10 19 112 102 95 112 106 119 0 0 108 19 12.17333 12 10 24 112 102 94 112 106 119 0 0 108 19 12.17444 12 10 28 112 102 94 112 106															18
12.16778 12 10 4 112 102 95 112 106 119 0 0; 108 20 12.16917 12 10 9 112 102 95 112 106 119 0 0 108 19 12.17055 12 10 14 112 102 95 112 106 119 0 0 108 19 12.17194 12 10 19 112 102 95 112 106 119 0 0 108 19 12.17333 12 10 24 112 102 94 112 106 119 0 0 108 19 12.17444 12 10 28 112 102 94 112 106 119 0 0 108 19 12.17583 12 10 33 112 102 94 112 1															20
12.16917 12 10 9 112 102 95 112 106 119 0 0 108 19 12.17056 12 10 14 112 102 95 112 106 119 0 0 108 19 12.17194 12 10 19 112 102 95 112 106 119 0 0 108 19 12.17333 12 10 24 112 102 94 112 106 119 0 0 108 19 12.17363 12 10 28 112 102 94 112 106 119 0 0 108 19 12.17583 12 10 33 112 102 94 112 106 119 0 0 108 19 12.17861 12 10 38 112 102 94 112 1	12.16778														30
12.17056 12 10 14 112 102 95 112 106 119 0 0 108 19 12.17194 12 10 19 112 102 95 112 106 119 0 0 108 19 12.17333 12 10 24 112 102 94 112 106 119 0 0 108 19 12.17444 12 10 28 112 102 94 112 106 119 0 0 108 19 12.17583 12 10 33 112 102 94 112 106 119 0 0 108 19 12.17583 12 10 38 112 102 94 112 106 119 0 0 108 19 12.17522 12 10 38 112 102 94 112 107 119 0 0 108 19 12.17861 12 10 <td>12.16917</td> <td></td> <td>108</td> <td></td> <td>31</td>	12.16917												108		31
12.17194 12 10 19 112 102 95 112 106 119 0 0 108 19 12.17333 12 10 24 112 102 94 112 106 119 0 0 108 19 12.17444 12 10 28 112 102 94 112 106 119 0 0 108 19 12.17583 12 10 33 112 102 94 112 106 119 0 0 108 19 12.17583 12 10 38 112 102 94 112 107 119 0 0 108 19 12.17722 12 10 38 112 102 94 112 107 119 0 0 108 19 12.17861 12 10 43 112 102 94 112 107 119 0 0 108 19 12.18139 12 10 <td>12.17056</td> <td></td> <td></td> <td>14</td> <td></td> <td>102</td> <td></td> <td></td> <td>106</td> <td>119</td> <td></td> <td></td> <td></td> <td></td> <td>3.</td>	12.17056			14		102			106	119					3.
12.17444 12 10 28 112 102 94 112 106 119 0 0 108 19 12.17583 12 10 33 112 102 94 112 106 119 0 0 108 19 12.17722 12 10 38 112 102 94 112 107 119 0 0 108 19 12.17861 12 10 43 112 102 94 112 107 119 0 0 108 19 12.18 12 10 48 112 102 94 112 107 119 0 0 108 19 12.18139 12 10 53 112 102 94 112 107 120 0 0 108 19 12.18276 12 10 58 112 102 94 111 107	12.17194		10	19	112			112							32
12.17583 12 10 33 112 102 94 112 106 119 0 0 108 19 12.17722 12 10 38 112 102 94 112 107 119 0 0 108 19 12.17861 12 10 43 112 102 94 112 107 119 0 0 108 19 12.18 12 10 48 112 102 94 112 107 119 0 0 108 19 12.18139 12 10 53 112 102 94 112 107 120 0 0 108 19 12.18278 12 10 58 112 102 94 111 107 120 0 0 108 19 12.18477 12 11 3 112 102 94 111 107 120 0 0 108 19 12.18566 12 11 8 112 102 94 111 107 120 0 0 107 19 12.18694 12 11 </td <td>12.17333</td> <td></td> <td>32</td>	12.17333														32
12.17722 12 10 38 112 102 94 112 107 119 0 0 108 19 12.17861 12 10 43 112 102 94 112 107 119 0 0 108 19 12.18 12 10 48 112 102 94 112 107 119 0 0 108 19 12.18139 12 10 53 112 102 94 112 107 120 0 0 108 19 12.18278 12 10 58 112 102 94 111 107 120 0 0 108 19 12.18477 12 11 3 112 102 94 111 107 120 0 0 108 19 12.18556 12 11 8 112 102 94 111 107 120 0 0 107 19 12.18694 12 11 13 112 102 94 111 107 120 0 0 107 19 12.18833 12 11 </td <td>12.17444</td> <td></td> <td>32</td>	12.17444														32
12.17861 12 10 43 112 102 94 112 107 119 0: 0 108: 19 12.18 12 10 48: 112 102 94 112 107 119 0: 0 108: 19 12.18139 12 10 53 112 102 94 112: 107 120 0 0 108: 19 12.18278 12 10 58 112 102 94 111: 107 120 0 0 0 108: 19 12.18417 12 11 3 112 102 94 111: 107 120 0 0 108: 19 12.18556 12 11 8 112 102 94 111: 107 120 0 0 107: 19 12.18694 12 11 13 112 102 94 111 107 120 0 0 107: 19 12.18833 12 11 18 112 102 94 111 107 120 0 0 107: 19	12.17583														32
12,18 12 10 48 112 102 94 112 107 119 0! 0 108 19 12.18139 12 10 53 112 102 94 112 107 120 0 0 108 19 12.18278 12 10 58 112 102 94 111 107 120 0 0 108 19 12.18477 12 11 3 112 102 94 111 107 120 0 0 0 108 19 12.18556 12 11 8 112 102 94 111 107 120 0 0 0 107 19 12.18694 12 11 18 112 102 94 111 107 120 0 0 107 19 12.18833 12 11 18 112 102 94	12.17722														3:
12.18139 12 10 53 112 102 94 112 107 120 0 0 108 19 12.18278 12 10 58 112 102 94 111 107 120 0 0 108 19 12.18417 12 11 3 112 102 94 111 107 120 0 0 0 108 19 12.18556 12 11 8 112 102 94 111 107 120 0 0 107 19 12.18694 12 11 13 112 102 94 111 107 120 0 0 107 19 12.18833 12 11 18 112 102 94 111 107 120 0 0 107 19	12.17861														3:
12.18278 12 10 58 112 102 94 111 107 120 0 0 108 19 12.18417 12 11 3 112 102 94 111 107 120 0 0 108 19 12.18556 12 11 8 112 102 94 111 107 120 0 0 107 19 12.18694 12 11 13 112 102 94 111 107 120 0 0 107 19 12.18833 12 11 18 112 102 94 111 107 120 0 0 107 19															3
12.18417 12 11 3 112 102 94 111 107 120 0 0 108 19 12.18556 12 11 8 112 102 94 111 107 120 0 0 107 19 12.18694 12 11 13 112 102 94 111 107 120 0 0 107 19 12.18833 12 11 18 112 102 94 111 107 120 0 0 107 19															3
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12.18833 12 11 18 112 102 94 111 107 120 0 0 107 19															3:
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Flow meter calibration data.

12.19111	12	11	28	112	102	93	111	107	120	0	O;	107	19	32
12.1925	12	11	33	112	102	93	111	107	120	0	o;	107	19	32
12.19389	12	11;	38	112	103	93	111	105	120	0	0	107	19	32
12.19528	12	11	43 .	112	103	93	111	109	119	0	0	107	19	32
12.19667	12	11	48	112	103	93	111	109	119	0	0	107	19	32
12.19806	12	11	531	112	103	93	111	109	119	0	oʻ	107	19	32
12.19944	12	11	58	112	103	93	113	106	119	0	0	107	19	32
12.20083	12	12	3	112	103	93	113	106	119	0	0	107	19:	32
12.20222	12	12	8	112	103	93	113	106	119	0	0	108	19	32
12.20361	12	12	13	112	103	93	113	106	119	0	0	108	19	32
12.205	12	12	18	112	103	93	113	106	119	0		108	· — 19	32 31
12.20639	12	12	23	112	103	92	113	106	119	0	0	108	- 19 -	29
12.20778	12	12	28	112	103	92	113	106	119	0				
12.20917	12.										0;	108	<u>19</u> .	25
		12	33	112	103	92	113	106	119	0		108		18
12.21056	12	12	38	112	103	92	113	106	119	0	0	108	21	13
12.21194	12	12	43	113	103	92	113	106	120	0	0	108	21	7
12.21333	12	12	48	113	103	92	113	106	120	0	0 į	108	22	3
12.21472	12	12	53	113	103	92	113	106	120	0	0	108	22,	0
12.21611	12	12	58	113	103	92	112	106	120	0	0	108	22	0
12.2175	12	13	3	113	103	92	112	106	120	O.	0	108	22	ő
12.21889	12	13	8	113	103	92	112	106	120	0	0	107	22	ō
12.22028	12	13:	13	113	103	92	112	106	120	0	0	107	22	— · š
12.22167	12	13	18	113	103	92	112	106	120			107	22	ŏ
12.22306	12	13	23	113	103	92	112	106	120		-0.	107	- 22	ŏ
12.22444	12	13	28	113	103	92	112	106	120			107	22	0
12.22583	12	13	33	113	103	92		106						
12.22722							112		120	0		107	22.	0
	12	13	38	113	102	92	112	106	120	0	0	107	22	의
12.22861	12	13	43	112	102	92	112	106	120	0	0	107	22	<u>o</u>
12.23	12	13	48	112	102	92	112	106	120	0,	0	107	22	0
12.23139	12	13	53	112	102	92	112	106	120	0	0	107	22	1
12.23278	12	13	58	112	102	92	114	107	120	0	0	107	22	2
12.23417	12	14	3	112	102	92	114	107;	120	0,	0	107	22	4
12.23556	12	14	8	112	102	92	114	107	120	0	0	108	21	- <u>6</u>
12.23694	12	14	13	112	102	92	114	107	120	0	0	108	21	_ 8
12.23833	12	14	18	112	102	92	114	107	120	0	0	108	21	9
12.23972	12	14.	23	112	102	95	114	107	120	- ō	o ;	108	21	11
12.24111	12	141	28	112	102	95	114	107	120		0	108	21	13
12.2425	12	14:	33	112	102	95:	114	107	120	0:				- !3
12.24389	12	14	38	112	102							108	21	15
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12.24528	12	14!	43	113	101	95	114	107	120	0	0	108	21	18
12.24667	12	14	48	113	101	95	114	107	120	0	<u>0;</u>	108	20	20
12.24806	12	14	53	113	101	95	109	107	120	0	0	108	20	22
12.24944	12	14	58	113	101	95	109	106	120	<u> </u>	0,	108	20	23
12.25083	12	15	3	113	101	95	109	106	120	o j	0	108	20	25
12.25222	12	15	8	113	101	95	109	106	120	0	0.	104	20	27
12.25361	12	15	13	113	101	95	109	106	120	0	0'	104	20	29
12.255	12	15	18	113	101	95	109	106	120	0	0	104	20	30
12.25639	12	15	23	113	101	92	109	106	120	0	0	104	19	31
12.25778	12	15	28	113	101	92	109	106	120		0	104	19	32
12.25917	12	15	33	113	101	92	109	106	120	o ;	0	104	19	32
12.26056	12	15	38	113	101	92	109	106	120	0 -	0	104	19	32
12.26194	12	15	43	111	101	92								32
12.26333	12	15	48	111	101	92	109	106	120	0	0	104	19.	
12.26472	12	15	53	111			109	106	120	0	0	104	19	32
12.26472	····				101	92	112	106	120,	0	0	104	- 19	32
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12.2675	12	16	3	111	101	92	112	107	120	0	0	104	19	32
12.26889	12	16.	8	111	101	92	112	107	120	0	0,	106	19	32
12.27028	12	16	13	111	101	92	112	107	120	0	0	106	19	32
12.27167	12	16	18	111	101	92	112	107	120	0	0	106	19	32
12.27306	12	16	23	111	101	92	112	107	120	0.	0	106	19	32
12.27444	12	16	28	111	101	92	112	107	120	01	0:	106	19	32
12.27611	12	16	34	111	101	92	112	107	120	0	0	106	19	32
12.2775	12	16	39	113	102	92	112	107	120	0,	0:	106	19	32
12.27889	12	16	44	113	102	92	112	107	120	0	0	106	19	32
12.28028	12	16	49	113	102	92	112	107	120	<u>ŏ</u>		106	19	32
12.28167	12	16:	54	113	102	92	113	107	120	0	_	106	19	32
12.28306	12	16	59	113	102	92	113	105	120	0		~	19	32
12.28444	12.	17	4	113	102						0	106		
12.28583						92	113	105	120		0	106	19	32
	12	17	9	113	102	92	113	105	120	0	0	106	19	32
12.28722	12	17	14	113	102	92	113	105	120	0,	0	106	19	32
12.28861	12	17	19	113	102	92	113	105	120	0	0	106	19	32
12.29	12	17	24	113	102	91	113	105	120	0	0_	106	19	32
12.29139	12	17	29	113	102	91	113	105	120	0	0	106	19	32
12.29278	12	17	34	113	102	91	113	105	120	0	0	106	19	32
12.29417	12	17	39	111	100	91	113	105	120	0	0	106	19	31
12.29556	12	17	44.	111	100	91	113	105,	120	0	0	106	19	26
12.29694	12	17:	49	111	100	91.	113	105	120	0	0	106	20	22
12.29833	12	17:	54	111	100	91	112	105	120	0.	0	104	20	15
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Flow meter calibration data.

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12.36778	12.365	12	21	54	172	157	135	171	164	108	0	0	164	20	1
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12.3925 12 23 33 172 158 134 173 167 109 0 0 165 22 12.39369 12 23 38 172 158 134 173 167 109 0 0 165 22 12.39528 12 23 43 172 158 134 172 164 109 0 0 165 22 12.39667 12 23 48 172 158 134 172 164 109 0 0 165 22 12.39906 12 23 53 172 158 134 172 164 109 0 0 165 22 12.39944 12 23 58 172 158 134 172 164 109 0 0 165 22 12.40083 12 24 3 172 158 134 172															
12.39389 12 23 38 172 158 134 173 167 109 0 0 165 22 12.39528 12 23 43 172 158 134 172 164 109 0 0 165 22 12.39667 12 23 48 172 158 134 172 164 109 0 0 165 22 12.39806 12 23 53 172 158 134 172 164 109 0 0 165 22 12.39944 12 23 58 172 158 134 172 164 109 0 0 165 22 12.40083 12 24 3 172 158 134 172 164 109 0 0 165 22 12.40222 12 24 8 172 158 134 172															
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12.39944 12 23 58 172 158 134 172 164 109 0 0 165 22 12.40083 12 24 3 172 158 134 172 164 109 0 0 165 22 12.40222 12 24 8 172 158 134 172 164 109 0 0 165 22 12.40361 12 24 13 172 158 134 172 164 109 0 0 165 22 12.405 12 24 18 172 158 134 172 164 109 0 0 165 22 12.40639 12 24 23 172 158 134 172 164 109 0 0 165 22 12.40778 12 24 28 172 158 134 172 164 109 0 0 165 22	12.39667		23	48	172	158	134	172	164	109	0	0	165	22	(
12.39944 12 23 58 172 158 134 172 164 109 0 0 165 22 12.40083 12 24 3 172 158 134 172 164 109 0 0 165 22 12.40222 12 24 8 172 158 134 172 164 109 0 0 165 22 12.40361 12 24 13 172 158 134 172 164 109 0 0 165 22 12.405 12 24 18 172 158 134 172 164 109 0 0 165 22 12.40639 12 24 23 172 158 134 172 164 109 0 0 165 22 12.40778 12 24 28 172 158 134 172 164 109 0 0 165 22	12.39806	12	23	53	172	158	134	172	164	. 109	0	0	165	22	
12.40083 12 24 3 172 158 134 172 164 109 0 0 165 22 12.40222 12 24 8 172 158 134 172 164 109 0 0 165 22 12.40361 12 24 13 172 158 134 172 164 109 0 0 165 22 12.405 12 24 18 172 158 134 172 164 109 0 0 165 22 12.40639 12 24 23 172 158 134 172 164 109 0 0 165 22 12.40778 12 24 28 172 158 134 172 167 109 0 0 166 22											0				
12.40222 12 24 8 172 158 134 172 164 109 0 0 165 22 12.40361 12 24 13 172 158 134 172 164 109 0 0 165 22 12.405 12 24 18 172 158 134 172 164 109 0 0 165 22 12.40639 12 24 23 172 158 134 172 164 109 0 0 165 22 12.40778 12 24 28 172 158 134 172 167 109 0 0 166 22															
12.40361 12 24 13 172 158 134 172 164 109 • 0 0 165 22 12.405 12 24 18 172 158 134 172 164 109 0 0 165 22 12.40639 12 24 23 172 158 134 172 164 109 0 0 165 22 12.40778 12 24 28 172 158 134 172 167 109 0 0 166 22															
12.405 12 24 18 172 158 134 172 164 109 0 0 165 22 12.40639 12 24 23 172 158 134 172 164 109 0 0 165 22 12.40778 12 24 28 172 158 134 172 167 109 0 0 166 22															
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12.40778 12 24 28 172 158 134 172 167 109 0 0 166 22															
															
	14.70110														

Flow meter calibration data.

12.41056	12	24	38	172	158	134	172	167	109	0	0	166	22	
12.41194	12	24	43	172	158	134	174	167	109	00	0	166	22	1
12.41333	12	24	48	172	159	1341	174	167	109	0	0	166	_ 21	_ 3
12.41472	12	24'	53	172	159	134	174	167	109	0	0	166	21	
12.41611	12	24	58	172	159	137	174	167	108	0	0	166	21	6
12.4175	12	25	3	172	159	137	174	167	108	0	0	166	21	_ ;
12.41889	12	25	8	172	159	137	174	167	108	0	0	166	20	10
12.42028	12	25	13	172	159	137	174	167	108	01	0	166	20	1
12.42167	12	25	18	172	159	137	174	167	108	0	0	166	20	- 14
12.42306	12	25	23	172	159	137	174	167	108	0	0	166	20	16
12.42444	12	25	28	172	159	137	174	167	108	<u>o</u>	0	166	20	18
12.42583	12	25	33	174	159	137	174	167	108	- 😽	0	166	19	20
12.42722	12	25	38	174	159	137	174	167	108	0;	. 0	166	19	22
12.42861	12	25	43	174	159	137	173	167	108	0 ;	0	166		24
													- 19 _.	
12.43	12	25	48.	174	159	137	173	167	. 108	0	0	166	_ 19.	20
12.43139	12	25	53	174	159	137	173	167	108	<u> </u>	0	166	18,	28
12.43278	12	25	58	174	159	137	173	167	108	0	0	166	18	29
12.43417	12	26	3	174	159	138	173	167	108	0	0	166	18	30
12.43556	12	26	8	174	159	138	173	167	108	0	0	166	18.	3
12.43694	12	26	13	174	159	138	173	167	108'	0	0	166	18	3.
12.43833	12	26	18	174	159	138	173	167	108	0	0	166	18	32
12.43972	12	26	23	174	159	138	173	167	108	0	0	166	18	30
12.44111	12	26	28	174	159	138	173	164	108	0,	0	166	19	2
12.4425	12	26	33	174	159	138	173	164	108	0′	0	164	19	19
12.44389	12	26	38	173	159	138	173	167	108		<u>-</u>	164	20	1
12.44528	12	26	43,	173	159	138	172	167	108	- 0	· ·	164	21	- 7
12.44667	12	26	48	173	158	138	172	167	108		0	164	21	
12,44806	12	26	53	173	158	138	172	163	108		0	164	22	
12.44944	12	26	58	173	158	138	172	163	109	- 0 -	0	164	22	-
12.45083	12	27	3	173	158	134	172	163	109		. 0	164	22	
12.45222	12	27	8	173	158	134	172	166	109	0	o ·	164	22	-
12.45361	12	27	13	173	158	134	172	166	109		0	164	22	
12.45528	12		19											
		27		173	158	134	172	166	109	0.	0	164	22.	-
12.45667	12	27	24	173	158	134	172	166	109	0	0_	169	22	
12.45806	12	27	29	181	158	134	187	199	103	0	0	199	22	1
12.45944	12	27	34	195	164	140	195	199	100	0	0.	199	22	1
12.46083	12	27	39	195	170	140	195	199	99	0	0	199	22	
12.46222	12	27	44	202	170	146	202	199	98!	0	_ 0.	199	22	1
12.46361	12	27	49:	202	176	151	202	199	98	0	0	199	22	1
12.465	12	27	54	202	176	151	202	199	98	0	0	198	22	C
12.46639	12	27	59	202	181	151	208	211	95	0	0	209	22	C
12.46778	12	28'	4	209	181	157	208	211	94	0	0	209	22	
12.46917	12	28	9	209	188	157	208	211	93	0	0	209	22	(
12.47056	12	28	14	215	188	157	215	211	93	0	0	209	22	. (
12.47194	12	28	19	215	193	162	215	211	93	0	0	209	22	. (
12.47333	12	28	24	215	193	162	215	211	93	0	0	209	22	- (
12.47472	12	28	29	215	193	162	215	208	93	0	0 · · -	210	22	- 3
12.47611	12	28	34	215	193	162	215	216	91,	0;	0	216	22	ì
12,4775	12	28	39	220	198	162	220	216	91	0		216	22	
12.47889	12	28	44	220	198	168	220	216	90	0				,
12.48028	12	28	49	220	198							216	22.)
						168	220	216	90	0′	0,	216	22.	-9
12.48167	12	281	54,	220	198	168	220	216	90	0	ō;	216	22	
12.48306	12	28	59	220	198	168	220	216	90	0	. 0	216	22	(
12.48444	12	29	4	220	198	168	220	216	90	0	0	216	22	(
12.48583	12	29	9	220	203	168	220	216	90!	0	0	216	22	(
12.48722	12	29	14	220	203	173	220	216	90	0	_ 0	216	22	(
12.48861	12	29	19	220	203	173	220	216	90	0	0	216	22	(
12.49	12	29	24	220	203	173	220	213	90	0	0	216	22	(
12.49139	12	29	29	220	203	173	220	213	90	0	0	216	22	
12.49278	12	29	34	220	203	173	220	213	90	0	0	215	22	
12.49417	12	29	39	223	203	173	223	213	90	0	0	215	22	Ċ
12.49556	12	29	44	223	203	173	223	213	90	0	ō	215	22	
12.49694	12	29	49	223	203	173	223	216	90	0	0	215	22	(
12.49833	12	29	54	223	203	173	223	216	90		0	215	22.	Ò
12.49972	12	29	59	223	203	173	223	216	89	0	6	215	22	Č
12.50111	12	30	4	223	203	173	223	216	89	<u> </u>	0.		22. 22	į
12.5025	12	30	9	223	203							215		
12.50389	12					173	223	216	89	0.	0	215	22	9
12.50528		30	14	223	204	174	223	216	89	0	0	215	22	
	12	30	19	223	204	174	223	216	89	0:	0	215	22_	(
12.50667	12	30	24	223	204	174	223	216	89	0	_0	215	_ 22	(
12.50806	12	30	29	223	204	174	223	216	89	0	_0	215	22	
12.50944	12	30	34	223	204	174	223	216	89	0	0	214	22	. (
12.51083	12	30	39	224	204	174	223	216	89	0	0	214	22	- (
12.51222	12	30	44	224	204	174	223	216	89	0	0	214	22	(
12.51361	12	30	49	224	204	174	223	215	89	0	0	214	22	i
12.515	12	30	54	224	204	174	223	215	89	0.	<u>o</u> ,	214	22	-
12.51639	12	301	59	224	204	174	223	215	e 89	0		214	22	}
12.51778	12													
12.51778	12	31	4	224	204	174	223	215	89	0	0	214	22	
		41	9	224	204	174	223	215)	89	0	0.	214	22	

Flow meter calibration data.

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12.52056	12	31	14	224	204	174	223	215	89	0			22	0
12.52194	12	31	19	224	204	174	223	215	89	0			22	0
12.52333	12	31	24	224	204	174	223	215		0			22	0
12.52472	12	31	29	224	204	174	223	215	89	0		214	22	0
12.52611	12	31	34	224	204	174	223	215	89	0		214	22	0
12.5275	12	31	39	224	204	174	223	215	89	0			22	0
12.52889	12	31	44	224	204	174	223	215	89	0			22	1
12,53028	12	31	49	224	204	174	223	215	89	0	0		21	3
12.53167	12	31	54	224	204	174	223	215	89	0	0	214	21	5
12.53306	12	31	59	224	204	174	223	215	89	0	0	214	21	7
12.53444	12	32	4	224	204	174	223	215	89	0	0	214	20	9
12.53583	12	32	9	224	203	174	223	215	89	0	0	214	20	11
12.53694	12	32	13	224	203	173	223	215	89	0	0	214	20	13
12.53833	12	32	18	224	203	173	223	215	89	0	0	214	19	15
12.53972	12	32	23	224	203	173	223	215	89	0	0	214	19	17
12.54111	12	32	28	224	203	173	223	215	89	0			19	19
12.5425	12	32	33	224	203	173	223	215	89	0			19	22
12.54389	12	32	38	222	203	173	222	215	89	0			18	23
12.54528	12	32	43	222	203	173	222	215	89	0			18	26
12.54667	12	32	48	222	203	173	222	215	89	0			18	27
		32	53	222	203	173	222	215	89	0			18	26
12.54806	12								89	ő			19	23
12.54944	12	32	58	222	203	173	222	212		0			19	19
12.55083	12	33	3	222	203	173	222	212	89					
12.55222	12	33	8	222	204	173	222	212	89	0			20	
12.55361	12	33	13	222	204	174	222	212	89	0			20	11
12.555	12	33	18	222	204	174	222	215	89	0			20	
12.55639	12	33	23	222	204	174	222	215	89	0			21	2
12.55778	12	33	28	222	204	174	222	215	89	0			21	1
12.55917	12	33	33	222	204	174	222	215	89	0			21	1
12.56056	12	33	38	223	204	174	224	215	89	0			22	1
12.56194	12	33	43	223	204	174	224	215		0			22	1
12.56333	12	33	48	223	204	174	224	215	89	0			22	1
12.56472	12	33	53	223	204	174	224	215	89	0	0		22	1
12.56611	12	33	58	223	204	174	224	215	89	0	0	214	22	1
12.5675	12	34	3	223	204	174	224	215	89	0	0	214	22	1
12.56889	12	34	8	223	203	174	224	215	89	0	0	214	22	1
12.57028	12	34	13	223	203	172	224	212	89	0	0	214	22	1
12.57167	12	34	18	223	203	172	224	215	89	0	0	214	21	1
12.57306	12	34	23	223	203	172	224	215	89	0	0	214	21	3
12.57444	12	34	28	223	203	172	224	215	89	0	0	214	21	5
12.57583	12	34	33	223	203	172	224	215	89	0	0	215	21	7
12.57722	12	34	38	223	203	172	224	215	89		0	215	20	9
12.57861	12	34	43	223	203	172	224	215	89	0	0	215	20	11
12.58	12	34	48	223	203	172	224	215	89	0	0	215	20	14
12.58139	12	34	53	223	203	172	224	215	89	0	0	215	19	15
12.58278	12	34	58	223	203	172	224	215	89	0	0	215	19	18
12.58417	12	35	3	223	203	172	224	215	89	0	0	215	19	20
12.58556	12	35	8	223	204	172	224	215	89	0	0	215	19	
12.58694	12	35	13	223	204	174	224	215	89	0		215	18	24
12.58833	12	35	18	223	204	174	224	213	89	0		215		
12.58972	12	35	23	223	204	174	224	213	89	0				
12.59111	12	35	28	223	204	174	224	216	87	0				
12.5925	12	35	33	250	204	174	252	71	72	0				
12.59389	12	35	38	261	211	179	258	71	67	0				
12.59528	12	35	43	267	225	187	265	62		0				
12.59667	12	35	48	273	231	192	272		63	0				
12.59806	12	35	53	273	236	198	277	64		0				
12.59944	12	35	58	273	236	198	277	61		0				
12.60083	12	36	3	273	243	198	277	60		0				
12.60222	12	36	8	273	243	204	277	60						
	12	36	13	273	249	204	277	63					 	
12.60361				273	249	204	277	60						
12,605	12	36	18			204		58						
12.60639	12	36	23	279	249		277							
12.60806	12	36	29	279	254	209	277	57						
12.60944	12	36	34	279	254	209	277	63					22	
12.61083	121	36	39	279	254	209	277	57						
12.61222	12	36	44	279	254	209	277							
12.61361	12	36	49	279	254	209	277	63						
12.615	12	36	54	279	254	209	283							
12.61639	12	36	59	279	254	209	283							
12.61778	12	37	4	279	254	209	283							
12.61917	12	37	9	279	.254	209	283							
12.62056	12	37	14	279	254	209	283							
12.62194	12	37	19	279	254	209	283	59	59					
12.62333	12	37	24	280	254	209	283		59		0	59	22	
12.62472	12	37	29	280	256	212	283	,			0	59	22	
12.62611	12	37	34	280	256	212	283				0	59	22	0
12.6275	12	37	39	280	256	212	283						22	0
		37	44	280	256	212					0			
12,62889	12													

Flow meter calibration data.

2.63028	12	37	49	280	256	212	283	62	58	0	0	58	22	
2.63167	12	37	54	280	256	212	284	63	58	0	0	62	22	
2.63306	12	37	59	280	256	212	284	59	58	0	0	62	22	
2.63444	12	38	4	280	256	212	284	59	58	0	0	56	22	
2.63583	12	38	9	280	256	212	284	63	58	0	0	63	22	
2.63722		38												
	12		14	280	256	212	284	59	58	0	0	63	22	
2.63861	12	38	19	280	256	212	284	64	58	0	0 ′	63	22	
12.64	12	38	24	279	256	212	284	64	58	0	01	63	21	
2.64139	12	38	29	279	256	212	284	58	58	0	0	57	21	
2.64278	12	38	34	279	256	212	284	59	58	0	0	57	21	
2.64417	12	38	39	279	256	212	284	59	58	0		57	20	
2.64556	12	38	44	279	256	212		59			0			
							284		58	0		57	20	
2.64694	12	38	49	279	256	212	284	63	58	0	O _↓	63_	20	
2.64833	12,	38	54	279	256	212	282	58	58	0	0'	57	19	
2.64972	12	38	59	279	256	212	282	58	58	0	0	62	19	
2.65111	12	39	4	279	256	212	282	58	58	0	0	62	19	
12.6525	12.	39	9	279	256	212	282	58	58	0	0	57	18	
2.65389	12	39	14	279	256	212	282	58	58	0	0	57	18	
2.65528	12.	39	19	279	256	212	282							
2.65667	12:	391						60	58	0	<u>o</u>	57	18	
			24	280	256	212	282	60	58	0	0	57	18	
2.65806	12	39	29	280	256	211	282	60	58	0	0	57	19	
2.65944	12	39	34	280	255	211	282	60	57	0	01	57	19	
2.66083	12	39	39	280	255	211	282	56	57	0	0	53	19	
2.66222.	12	39	44	280	255	211	282	59	57	0	0	59	20	
2.66333	12	39	48	280	255	211	282	62	57	0	0	59	20	
2.66472	12	39	53	280	255	211	281	67	57	0	0	67	21	
2.66611	12	39	58	280										
					255	211	281	64	57	0	0:	67	21	-
12.6675	12	40	3	280	255	211	281	56	57	0	0	60	21	
2.66889	12!	40!	8	280	255	211	281	56	57	0	0	56	21	
2.67028	12	40	13	280	255	211	281	60	57	0	0	62	22	
2.67167	12	40	18	280	255	211	281	65	57	01	0	62	22	
2.67306	12.	40	23	280	255	211	281	61	57	0	0	62	22	-
2.67444	12	40	28	280	255	212	281	62	57	0	0	62		
2.67611	12	40	34	280									22	
					256	212	281	61	58	0	0	62	22.	
12.6775	12	40	39	280	256	212	281	61	58	0	0	62	22	
2.67889	12	40	44	280	256	212	281	64	58	0	0	62	22	
2.68028	12	40	49	280	256	212	281	60	58	0	0	62	22	
2.68167	12	40	54	280	256	212	281	63	58	0	0	62	22	
2.68306	12	40	59	280	256	212	281	60	58	0	<u> </u>	62	22	
2.68444	12	41	4	280	256	212	281	67	58					
2.68583	12	41	9							0	0'	62	22	
				280	256	212	281	63	58	0	0	63	22	
2.68722	12	411	14	280	256	212	281	58	58	0	0:	63	22	
2.68861	12	41'	19	280	256	212	281	61	58	0	0	63	22	
12.69	12	41	24	279	256	212	281	581	58	0	0	63	22	-
2.69139	12	41	29	279	256	214	281	63	58	0	0	63	22	-
2.69278	12	411	34	279	257	214	281	63	58	0 :	·- o	63	22	
2.69417	12	41	39	279	257									
						214	281	64	58	0	0	63	21	
2.69556	12	41	44	279	257	214	281	61	58	0	0	63	21	
2.69694	12	41	49	279	257	214	281	61	58	0	0 j	63	21	
2.69833	12	41	54	279	257	214	283	65	58	0	0	63.	20	
2.69944	12	41	58:	279	257	214	283	60	58	0	0	63	20	
2.70083	12	42	3	279	257	214	283	60	58	0	0	63	20.	-
2.70222	12.	42	8	279	257	214	283							-
								60	58	0,		63.	19	
2.70361	12:	42	13	279	257	214	283	60	58	<u> 0</u>	00	61	19	
12.705	12	42	18	279	257	214	283	60	58	O	0	61	19	
2.70639	12	42	23	279	257	214	283	58	58	0	0	61	18	
.70778	12	42	28	279	257	214	283	58	58	0	0	61	18	
.70917	12	42	33	279	256	214	283	54	57	0	0	55	18	
.71056	12	42	38	279	256	214	283	61	57	0	0	61	18	
.71194	12	42	43	279	256	214	283	63	57	0,	0-	61		-
.71333	12	42	48	279	256								18_	
.71472	12					214	283	59	57	0 .	0	61	18	_
		42	53	279	256	214	280	58	57	0	0	61	18	
.71611	12	42	58,	279	256	214	280	58	57	0	0	61	18	
2.7175	12	43	3	279	256	214	280	61	57	0	0	61	18	
71889	12	43	8	279	256	214	280	59	57	0	0	61	18	
72028	12	43	13	279	256	214	280	63	57	0	0	61	18	
72167	12	43.	18	279	256			59						
						214.	280		57	0	0	61	18	
72306	12:	43	23	279	256	214	280	62	57	0	0	61	18	
72444	12	43)	28	279	256	216	280,	59	57	0	0	55	18	
.72583	12	43	33	279	256	216	280	59	57	0 -	0	55	18	
.72722	12	43	38	279	256	216	280	57	57	0		55	18	
72861	12	43	43	279	256	216	280	56	57	0				
12.73	12	43	48	279							*	62	_ 18_	-
					256	216	280	61	57	0	0	60	18	
.73139	12	43	53	279	256	216	278	60	57	0	0	60	18	
.73278	12	43	58	279	256	216	284	65	57	0		65	18	
.73417	12	44	3	279	256	216	284	61	57	0	0	57	19	
.73556	12	44.	8	279	256	216	284	60:	57	- 0	0	57	19	
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73694	12	44	13'	279	256!	216	284	62:	57	0	0	63	20	

Flow meter calibration data.

12.73972	12	44	23	280)	256	216	284	57	57	0	0	57	20:	10
12.74111	12	44	28	280	256	215	284	57	57	0	Oi Oi	57	21	6
12.7425	12	44	33	280	258	215	284	60	57	O	0	57	21	3
12.74389	12	44	38	280	258	215	278	60	57	0	01	57	21	1
12.74528	12	44	43	280	258	215	278	60	57	0	01	63	21	1
12.74667	12	44	48	280	· 258	215	278	58	57	0	0	63	22	1
12.74806	12	44	53	280	258	215	278	62	57	0	0	61	22	1
12.74944	12	44	58	280	258	215	284	62	57	0	0,	61	22	1
12.75083	12	45	3	280	258	215	284	56	57	0	0)	541	22	
12.75222	12	45	8	280	258	215	284	56	57	0	0	54	22	_ !
12.75361	12	45	13	280	258	215	284	63	57	0	0	63	22.	
12.755	12	45	18	280	258!	215	284	62	57	0!	0	63;	22	;
12.75667	12	45	24	280	258	215	284	59i	57 58	0	0	57	22	
12.75806	12	45 45	34	280	257 257	215	284	62	58	0;	0	57	22	-
12.75944	12	45	39	280	257	215	284	591	58	0	01	57	22	
12.76083	12	45	44	280	257	215	284	59	58	0	0	57	22,	1
12.76361	12	45	49	280	257	215	284	67	58	0	0	66	22	1
12.765	12	45	54	280	257	215	284	64	58	01	0	66	221	1
12.76639	12	45	59	280	257	215	283	60)	58	0	0	58	22	1
12.76778	12	46	4	280	257	215	283	60	58	0	0	58	22	1
12.76917	12	46	9	280	257	215	283	59	58	0	0	58	22	1
12.77056	12	46	14	280	257	215	283	59	58	01	0	58	22	1
12.77194	12	46	19	280	257	215	283	66	58	0	0	66	22	1
12.77333	12	46	24	281	257	215	283	66	58	0	0	66	22	1
12.77472	12	46	29	281	257	215	283	70	58	0	0	66	22	1
12.77611	12	46	34	281	257	215	283	66	58	0	0	66	22	
12.7775	12	46	39	281	257	215	283	62	58	0	0]	60	22	
12.77889	12	46	44	281	257	215	283	65	58	0	0	60	22	
12.78028	12	46	49	281	257	215	283	61	58	0	0	60,	22	
12.78167	12	46	54	281	257	215	283	64	58 58	0,	0,	60	22	
12.78306	12	47	4	281	257	215	280	60	581	0,	0,	60:	22	- i
12.78583	12	47	9	281	257	215	280	65	58	01	0	60	22	
12.78722	12	47	14	281	257	215	280	62	58	O	0	60	22,	1
12.78861	12	47	19	281	257	215	280	58	58	0	0	60	22	1
12.79	12	47	24	283	257	215	280	63	58	0	0	67	22	1
12.79139	12	47	29	283	257	216	280	61	58	0	0)	61	22	1
12.79278	12	47	34	283	257	216	280	62	58	0	0!	61	22	1
12.79417	12	47	39	283	257	216	280	62	58)	0	0	61	22	1
12.79556	12	47	44	283	257	216	280	58	58	0	0	61	22	
12.79694	12	47	49	283	257	216	280	62	58	0	0	61	22	
12.79833	12	47	54	283	257	216	280	58	58 58	0	0	61	221	
12.79972	12	47	59	283	257 257	216	280	58 61	58	0	0	61	22	
12.80111	12	48	9	283	257	216	280	66	58	0	0	68	22	
12.80389	12	481	141	283	257	216	280	63	58	0	0	60	22	- 1
12.80528	12	48	19	283	257	216	280	59	58	0	Ō	60	22	1
12.80667	12	48	24	281	257	216	280	62	58	0	Ō	60	22	1
12.80806	12	48	29	281	257	215	280	61	58	0	0	60	22	1
12.80917	12	48	33	281	257	215	280	59	58	0	0	59	22	1
12.81056	12	48	38	281	257	35	280	63	58	0	0	59	22	1
12.81194	12	48	43	281	257	3	280	60	58	0	0	59	22	1
12.81333	12	48	48	281	257	3	280	63	58	0	0	59	22	
12.81472	12	48	53	281	257	3	280	57	58	0	0	59	22	
12.81611	12	48	58	281	257	40	281	64	58	0	0	59 65	22	$-\frac{1}{1}$
12.8175	12	49 -	8	281	257	214	281	60	58	0	0	65	22	
12.81889	12	49	13	281	257	214	281	64	58	0	0	65	22	<u>'</u>
12.82167	12	49	18	281	257	214	281	61	58	0	0	59	22	1
12.82306	12	49	23	280	257	214	281	58	58	0	0	59	22	1
12.82444	12	49	28	280	257	214	281	61	58	o	0	59	22	1
12.82583	12	49	33	280	259	214	281	61	58	0	0	59	22	1
12.82722	12	49	38	280	259	214	281	61	58	0	0	59	22	1
12.82861	12	49	43	280	259	214	281	61	58	01	0	57	22	1
12.83	12	49	48	280	259	214	281	60	58	0	0	60	22	1
12.83139	12	49	53	280	259	214	281	55	58	0	0	54	22	1
12.83278	12	49	58	280	259	214	280	58	58	0	0	60	22	
12,83417	12	50	3	280	259	214	280	61	58	0	0	61)	22	_ 1
12.83556	12	50	8	280	259	213	280	61	58	0	0	61	22	
12.83694	12	50	13	280	259	213	280	65	58 58	0	0	66) 58	22	1
12,83833	12	50	18	280	259	213	280	62 58	58	0	0	58	22	—
12.83972	12	50	23	280	259 259	213	280	69	58	0	0	63	22	
12.84111	12	50	33	260	259	213	261	111	73	0	0	115	22	1
12.84389	12	50	38	234	234	196	233	119	88	0	0	122	22	<u></u>
12.04303	12	501	30	2341	234	1301	2001	1131	001					:

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Time	Time	Time F	720 PF-00		FT730 GPM	FT800 GPM	TEE16 DEG F	TEE15 TEE1	DEG F	TEE12 DEG F	TEE11 DEG F		DEG F		TEE7 DEG F	DEG F	TEE5 DEG F	TEE4 DEG F	TEE3 DEG F 590	TEE2 DEG F	TEE1 DEG F	DEG F 590	DEG F	DEG F
	12 0	4 19	369 374	412 2	89 72 90 8		590 594	592	592 59 592 59	1 591 1 591	60	8 592	591 592 593	595 597	592 593	591 591 592	582 584 585	591	591	590 590 590	593 594		591	584 585
1	12 0 12 0 12 0	34 49	360 331	341 2	97 26 62 32	196	594 594 594 592	593 593 596	593 59 596 59 602 59	3 60	0 60 0 60 7 60	8 592	597	598 598 595	593 594 594 592	591 590	584 582	591 589	591 590	588	593 592	594 594	592 592	585 585
	12 1 12 1	1 <u>9</u>	367 380	336 2	77 8 79 8	154	594 592 592	594	597 59 594 59	0 59	9 60	8 589	602 597	595 597 598	592	1 590	582 584	589 590 591	590 590	588	592 593	594 594	592 592	5 <u>84</u> 584
	12 12 1	33 49	380 380 380	346 2	99 11 85 14 97 16	144	592	591 593 597	594 59 597 59 596 59	3 60	1 62	2 591	593	598 598	593 594	591 591	584 584	591	591 592	590	594 595	594 594	592 592 593	2 585 2 585
	12 2 12 2	19	376	346 2			594 594	595 594	504 50	3 60 4 59 4 59	8 61 3 61	4 593	595 592	597	594	591 592	580 572	591 591	591 589	590 590	594 593	594 595	593 593	3 585 3 585
-	12 2	33 49 4 19 34 48 3	382	344 2	93 86	2 2	594 594	593	592 59 589 58	1 58 9 58	8 60 3 60 9 59	5 590 2 588	591 587	593 590 584	590	590	560 560	589 585	586 582	584 584 581	590 588	595	593	3 586 3 586
-	12 1 1 12 1 1 12 2 12 12 2 12 12 12 12 1		382 388	333 2 363 3	75 02	5 0	587	589 588	586 <u>58</u> 583 58	6 57 2 57	9 59 4 59	7 584 3 581	592 591 587 585 582 579	580 574	587 583	588 584 580 578	582 584 584 580 572 566 560 554 542 533	583 579	580 576	581 578 578	580	595 595 595	593	3 586 3 586
1 -	12 3	48	376 382 382 382 388 388 388 388 387 387 387 387 387 387	393 2 386 2	95 1- 69 93 93 95 96 97 97 97 97 97 97 97 97 97 97 97 97 97	0 0 0 0 0 0	587 587	585	579 58 576 57	4 59 1 58 9 58 6 57 2 57 0 56 6 56 3 56 9 55 7 55	59 59 5 5 5 6 5 5 5 5 5 5 5 5 5 5 5 6 5 7	6 577 6 575	579 577	584 580 574 571 566 562	580 578	574	537 532	591 591 589 585 583 579 577 573 571 567	592 591 589 586 580 576 572 569 568 559 559 559 568 568 568 568 568 568 568 568 568 568	572 568	576	si 595	5 593	3 585 3 585
	12 4 12 4 12 4	18 33	388 387	353 3	06	0		583 580	576 57 572 57 568 56 566 56	9 55	1 58 6 57 3 57	9 569	577 573 569 566 566 567 561	557 552	572	568 565	526 521	567 565	563 559	566 564 567	571 566	594	593	3 585 3 584
	12 5	48	387 387	389 3	75 2	9 132 6 104	581	581	566 56 571 56 571 56 564 56	7 55 3 54 9 56	9 57	5 564	566 567	550 564	567 570	564	524	565 565	559 568	567 568	561 569	594	592	2 584 7 583
-	12 5 12 5	33	376	382	93 17 87 17	8 127 6 136 6 145	569 569	565 561	564 56 561 57	7 56 6 56	0 56 8 56	5 569 4 577	561 561	565 574	_ 565 572	571 578	524 557 554 557	570 578	565 568	570 57	566 57	578	578	2 579 8 575
	12 5 12 6	3	376 376 378	336	187 17 105 16 199 15 189 15	3 148 7 151	580	566	568 58	1 57	2 56 5 56	8 582 3 584	568 574	578 581	578	583	563	582 584	579	582 581	576 58	57	576	7 575 6 577
-	12 6	33	378	360 2 360 2 285 2	89 15 86 15	0 151 0 154	580	573 583	573 58 583 58	5 <u>57</u> 6 <u>57</u>	8 56	0 <u>585</u> 2 <u>585</u>	575 580	583 583 584	58 582 584 584	587 587 588	57	585	581	586	584	579 4 580	57 57 3 58	8 579 0 590
-	12 7	3	378 378 378	366 269	98 <u>16</u> 303 16	0 1 <u>54</u> 0 154	580 586	585 585	585 58	6 57 6 57 7 57	9 56 9 57	6 <u>587</u>	580 584 584	584	584 581 581	588 588	573	587	5 582 7 582 7 582 7 582	58	58	584	582	2 581
. -	12 7 12 7 12 7 12 8 12 8	33 48	376 376	338 2 289 3	97 16 308 16	0 154 0 154	586 586	585 585	585 58 587 58	7 57	9 57	6 587 8 587	585 585	584 584	58 58 58	588 588 588	573	587	582	58	58:	5 58	5 58 5 58	2 583 4 583
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	12 12 10	19 34	375 375 375 375	305 298	94 15 303 16	8 156 4 156	588 588	587 587	587 58	18 58 18 58	50 5	8 588	586 586	585	58 58 58	589	57	3 58	7 584	58	8 58 8 58	6 58 6 58 6 58	7 <u>58</u> 7 58	35 584 35 584
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-	12 11 12 11	33	375 377 377	374	301 15 278 15 307 13	9 156	58	586 586	587 58 587 58	18 58 18 57	5 5	75 589	586 586	585 584	58 58	6 589 6 589	57 56	58	7 582	4 58 2 58	8 58 8 58	6 58 6 58	7 58 7 58 7 58	35 583 35 583
	12 12 12 12	- 40 3 - 18	377 55	318	301 2 4 9	9 1	58 58	585 583	585 58 582 58	57 57 57	76 <u>5</u>	74 587 74 586	585 582	583 579	58 58	587 2 586	56 55	2 58 5 58	580 5 570	58 58	8 58 8 58 8 58 6 58 3 58	5 3 58	7 58 7 58 7 58	35 584 35 584
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hour		sec	GPM	Lt/min	LVmin	GPM	GPM				DEG F	DEG F			DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F				DEG F DEG I	
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hour		min	Sec	<u> </u>	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F		DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	
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1	12		39	34	455 455 452	437	471	456		454	400	460	465	444	460	441	452	430	456	446	432	442	493	473	481	469	572
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	12		43	19	438	424	465	445			375	451	460		458	433	443	418	455	439	422	435	493	474	483	461	570
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-	12		45	33	430	414	457	441		440	357	446	457	431	452 451	430	439	410	454	435	413	431	494	475	483	457	560
1-	12		45	48	430	413	457	440		440 440	355	446	456		450	430	439	409		434	412	431	495	475	484	456	569
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	12		46	18	428 427	412	455	439	457	439	350	445	455	430	449	430 429 429 428	438 438	407	452	433	410	431	495	475	484	456	570
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	12		47	10	425	410	453	437 437		438	343	444	453 452			428	436	403	448	432 431	407	429	496	476 476	485	454	- 569
	12		47	33	422	408 407	452	436	454	437	338	443	451	427	440	427	436	402 400	445	431	407 405	428 428	496 497	476	485 485	452 452	508
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1	12		48	19	420	403	449 448	435	452	435	330	441	448	426	443	424	434 434	396	442	429	403	426	497	476	487	450	566
1.	12		48	34	419	402	448	434	452	435	328	441	447	425	442	424	434	395	442	428	400	425 425	498	476	487	450	565
-	12		48	49	417	402	448 446 446 445	434	451	435	324	440	447	425	4421	423	433 433 432 432 432 431 431 430	395 393 392 391	441 440	428	399 398 396 396 394 393 392	425	498	477	487	449	565
	12		49	10	416	401	446	433 432	451	434	322	440 440	446		- 441	423	433	392	440	427	398	424	499	477	488	448	565
	- 12		49	34	415	300	446	433	450 449	434	310	439	445 444	424	4 <u>41</u> 440	422	432	391	439 439 438 438 437 437	426 426	396	424	500	477	488 489	448 447	565
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	12	7	50	4	414 413	397 396 395 394	444 444 443 443	431	449 448	432	315	438	443	422	439	419	431	386	438	426 425	393	423 422	501	478	491	446	566
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	12		50	48	409	392 391	443]	430	446	431	308	437	441 440	419	437	417	430	382	436	423	389 388	421	503	478	493	446	567
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	12		52	33	402	384 383 382 379	439	427	443	427	296	434	436	414	433	410	427	368	431	416	377	414 413	505	479	495	442	563
	12		52	48	400	382	437	427 426 425	442	427	294	434	435	413	433	409	426	368 366	431	415	375	412	505	479	496	441	563
	12		53	4	398	379	436	425	442	426	292	434	435	412	432	408	426	364 362	430	414	374	411	505	479	496	441	562
1	12		53	19	397	377	436	425	441	426	291	433	434	412	432	407	425	362	429	414	372	410	506	479	497	440	562

Time	Time	- 1	ime ec	TEW18 DEG F	TEW17 DEG F	TEW16 DEG F	TEW15	TEW14	TEW13 DEG F	TEW12	TEW11	TEW10 DEG F	TEW9	TEW8	TEW7	TEW6	TEW5	TEW4	TEW3 DEG F	TEW2	TEW1	TEWUHI	TEWLH20	TEWLH21	TE970 TE99	90
1			34	396	376	435	424	440	425	290	433	433	DEG F	DEG F 431	DEG F 406	DEG F 424	DEG F	DEG F	DEG F	DEG F 370	DEG F 410	DEG F	DEG F	DEG F		F
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	2	54	19		372 370	434 434	423	440	424 423			432 432	409		403	423	357	428	411	367	407	507	480	498	439	56
	2	54	34	390	368	433	421	439	423					430 429	402 401	423 422	356 354		410 409	365	406 405	508 508	480 480	499 500	438	<u>56</u>
	2	54	49	389	367	433	421	438	422	281	431	431	406	429	400	422	353	426	408	363	404	509	481		438	56
	2	55	19	388 386	366 364	431 431	420 420		421 420	280 279	431 430	430 429	404 403	428	398	421	351		407	361)	403	509	481	501	438	56
	2	55	33	385	362	431		437	419		430	429	403	427 427	396 395	420 419	349 347	425 424	405 404	360 358	402 401	510 510	481 481	501 501	437	_56
	2	55	19 33 48 3	384	361	430	418	436	419	276	430	428	400	426	393	418	345	423	403	356	398	511	481	502	438 438 438 438 437 437 437 437 437 436 436	56
	2	56	18	381 380	359 357	430 429	417	436 435	418 417		429 429	427 427	399 398	425	392	418	344	422	401	355	397	511	481	502	437	56
1	2	56			355	429	416	435	416	271	428	426	396	424 424	390 389	417 416	342 341	421	400 398	352 351	396 395	511 511	481 481	502	436	56
1	2	56	48	377	354	429 428 427	415	435	416	270	428	426	396 394	423	387	415	340	420 419	397	349	393	512	482	502	435	- 56
	2	57 57 57 57	18	377 373	351 350	427 427	414	434 434	415 414		427 427	425 424	393 392 390 389 387	422	386	415	338	419	396	348	391	512	482 482	503	434	56
1	2	57	33	372	349	425	412	434	413	265	427	424	390	421 421	384 382	414	337 335	417	394 392 391	347 345	390 388	513 513	482 482	503	434	55
	2	57	48	372	348	425	412	433	412	265	426	423 422	389	420	381	412	334	415	391	343	387	513	482	503	433	55
1	2	58 58	10	371 368	347 345	424 423	410 410	433	411	263	426	422	387	419	379	411	333	415	390	-341	386	513	482	503	433	55
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1	2	59	34	361	339 338	419	404		406 405		423 423	418 417		414	371 371	405 404	326 325	410 409		335 334	381 380	516 516	484 484	506 506	431	560
1		59	49	360	336	418	402	429	404	254	422	416	377	413	369	403	324		381	334	379	517	484	506	431	56
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13	3	0	49	355	332	414	200	428	399	250	420 420 419	413	372	408	363	397	319	403	376	329	375	517	484	507 508	428	55/
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13		2	48	345	322	406	386	424	389	241	414	404	362	398	353	386	310		366	320 319	368 368	520 521	485 485	509 509	425	55/
15		킑	3 18	344 343	321 319	404 403	384 383	423	387	240	413	403	361	397	352 351 350 349 347 346 345	385	310	391	365	319	367	521	485	509	424	550
13		3	33	341	318	402	381	421	386 384	239	413 412	402 401	360 359	395 394	351	383 382	308	390 388	364 363	318 318	366	522	486 486	510	423	556
13		3	48	340	317	401	380	421	383	238 237 235 235 233 233 232 230	411	399	358	392	349	381	307 307	387	362	317	366 365	522 522	486	510 511	423	55°
15		4	3 18	339 339	317 316	400 397	379 377	420 419	381 380	235	410 409	398	356	391	347	379	306	385		315	365 365	522 523	486	511	423	557
13	3	4	33	337	315	396	376	419	378	233	409	397 395	355 354	389	346	378 377	306 304 304 303	384 383	359 358	314 313	364 363	523 523	487 487	511	422 422	555
15		4	48		313	395	375	418	377	233	408	395 393 392 390	354 353	386	344	375	303	381	357	312	362	524	487	511 512	421	560 567
10		5	3 18		312 311	392 391	373 372	417 416	375 374	232	406 406	392	351	385	342	374	301	380	356	311	362	524 524 524 524	487	512	421	570
10		5	33		310	390	371	416	373	228	405	389	349	383	341	372 371	300 299	378 376	355 353	310 309	360 359	524	487 487	512	422 422	574
10		5	48	333	310	389	370	415	372	228	404	387	348	380	339	370	298	375	352	308	359	524	487	512	423	576 577
10		6	3 18	330	309	386 385	369 367	414 413	370 369	226 226	402 401	385 384	351 349 348 347 346 345 343 342 341 340 339 338 336 335 334 333 334 333	378 377	344 342 341 340 339 338 337 336 335 334 332 331 332 322 329 328	369	297	373	352	308	358	524	487	512 512 512 512 512 512 512 512 512	423	579
13	3	6	34 49	329	306	384	366	412	368	224	400	382	345	376	336	367 366	296 295	372 370	350 348	306 305	357 357	524 525	487 487	512	424 424	580 581 582 583 584 584 585 586 586 586 586 586 586 585 585 586 586
13		6	49		305	381	365	411	366	223	399	380	344	374	335	365	294	368	348	304	356	525	487	512	425	581
15		-/-	19	326 326	305 304	380 379	364 362	410 409	365 364	222	397 397	379 377	343	373 371	334	363 362 361 360 358 357 356	292	367	347	303	356	526	488	512	425	582
13	3	7	34	325	303	378	361	408	362	221	395	376	341	370	332	361	292 291	366 365	346 345	302 301	354 354	526 527	488 488	512 513	426 426	582
13		7	49	324	302	375	360	407	361	220	394	374	340	369	331	360	290	364	344	301	353	527	488	513	426	584
13			19	323	300	374 373	359 358	406 404	359 358	220 219	393 392	373 371	339	367 366	330	358	289	363	343	300	353 352	527	488	513	426	584
13	3	8	34	322	299	373 372	356	403	357	218	390	370	337	365	328	356	288 287	361 360	342 341	299 298	352 352	527 528	488 489	513 514	427 428	585
13		8	49	321	298	370	355	402	356	217	389	368	336	365 363 362 361 360 358	327	355	286	359	341	298	352	528	489	514	428	58£
13		9	19	319	297 297	369	354 353	401 400	354 353	216 215	388 386	366 365	335	362	326	355 354 352 351	285	358	340	297	352	529	489	514	428	586
13	3	9	34	318	295	366	352	398	352	214	385	363	333	360	325 324	352	284 283	356 355	339 338	296 296	350 350	529 529	489 489	514 514	428 428	586
13		9	49	315	294	365	351	397	351	213	384	362	332	358	323	350	282	354	337	294	349	529	489	514	428	586
13	3	10 10	19	315 314	294 293	363	350 349	396 394	350 349	212 211	383	360 359	331	357 356	323 322 321	349	281	352	335	293	348	529	489	514	428	586
13	31	10	33	313	292	367 366 365 363 362 361 360 358 356	348	393	349	210	384 383 382 380 379 378	359	330 329	356	321	350 349 348 347 346 345	280 279 278 277	351 349	334 333	292 291	347 347	530 530	489 490	514 515	428 428	585
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	ក្រែម	Time min 3 11 3 11		TEW18	TEW17 DEG F	TEW16	TEW15	TEW14 DEG F	TEW13 DEG F	TEW12 DEG F	TEW11 DEG F	TEW10 DEG F	TEW9 DEG F	TEW8 DEG F	TEW7 DEG F	TEW6	TEW5 DEG F	TEW4 TI	EW3 EG F	TEW2	TEW1	TEWUH19	TEWLH20	TEWLH21	TE970	TE990
լը	our	min	SOC .	DEG F		DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F	DEG F D	EG F		DEG F	DEG F	DEG F	DEG F	DEG F	DEG F
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l.	13	11	48	309	287	354	342	385	342	206	374	350	325	349	31	5 34	274	344	329	289	344	532	490	515	429	586
- 1_	18	12	3	308	287	352	341	384	341	205	373	349	324	347	31	5 34	273	343	328	287	344	4 532	490	515	429	586
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l.	13	3 12	48	305	284	349	338	380 378 377	337	202	369	345	321	344	31:	2 33	18 271	339	326	286	343	534	490	515	430	588
	13	13	3	305	284	347	337	378	336	201	368	344	320	343	31	1 33	270	338	325	285	343	3 534	490	515	430	588
l i	13	3 13	18	305	282	346	336	377	335	201	367	342	319	341	31	0 33	269	.337	324	284	34	1 534	491	516	430	589
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i i	13	13 14 3 14	48	303	281	344	334	374	333	200	365	340	318	339	30	33	4 267	334	322	284	34	535	491	516	430	589
r	13	14	3	302	280	343	333	373	332	199	363	338	317	338	30	7 33	3 265	333	321	283	339	535	491	516	430	589
r	13	14	18	301	280	342	332	371	331	198	363	337	316	337	30	33	264	332	320	283	339	535	491	515	430	589
-	13	14	33	300	279	340	332	370	330	197	361	336	315	336	30	33	264	331	319	281	33	535	491	515	430	589
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I-	13	10	49	294	212	200	324	359	323	100	353	320	308	327	293	32	3 257	322	312	277	333	537	492	510	429	590
		15	49	294	2/2	230	323	358	322	190	352	325	308	326	291	32	256	321	312	276	33	538	492	516	429	590
	13	H 17	4	293	2/1	329	322	357	321	190	351	324	307	325	29	32	256	320	311	276	334	538	492	516	429	591
[13	17	18	300 299 298 297 296 296 295 294 294 293 292 291	270	328	321	355	320	189	350	322	306	324	29	32	255	319	311	276	334	539	493	516	430	591
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	13	17	48	291	268	325	319	353	318	188	348	320	304	322	29	31	9 254	317	309	275	334	540	493	517	430	592
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- 1-	13	18	33	288	265	323	317	349	315	185	344	317	302	319	292	2 31	6 252	315	307	274	332	2 540	493	517	430	592
	13	18	48	287	265	322	316	348	314	185	344	316	301	318	29	31	6 251	314	306	273	332	2 541	493	517	430	592
I.	13	19	3	287	264	320	315	347	314	185	343	315	300	317	290	31	5 250	313	305	272	331	541	493	517	429	592
- 1	13	19	18	286	264	319	314	346	313	184	342	314	300	316	290	31	4 249	312	304	273	331	541	493	517	429	591
l'	13	19	- <u>33</u> 48	283	263	318	314	345	312	182	341	313	299	315	289	31	3 248	311	303	272	330	541	493	517	429	591
ı	13	19	48	283	263	317	313	344	311	181	340	312	298	314	28	31	2 247	309	303	272	330	541	493	517	429	591
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- 1-	13	20	49	281	259	314	310	339	308	180	336	308	295	310	289	30	9 244	305	299	270	329	542	493	517	429	591
- 1-	13	- 21	4	280	259	312	309	338	307	179	335	306	294	309	28	30	8 243	305	299	270	320	543	493	517	429	592
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- 1-	13	22		278	257	309	306	334	303	177	332	303	291	306	28	30	5 240	302	296	269	325	544	494	518	430	505
-	13	22	18	277	256	308	305	333	302	177	331	302	291	305	280	30	4 240	300	206	260	326	544	494	518	430	505
- !-	13	22	33	277	255	308	304	332	302	176	330	301	290	304	276	30	230	200	295	260	325	545	494	518 518 518	420	505
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-	13	25	18	200		297	296	321	293	170	321	291	282	294	27	29	231	290	287	267	326	547	495	518	429	594
	. 13	- 25	_ 33	268	247	296	295	_ 320	_ 292	169	320	290	281	294	2/0	29	4 231	290	287	267	325	548	495	518	429	594
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l_	13	26	49	265	244	292	291	316	288	166	316	285	277	289	266	29	0 227	285	284	267	325	550	496	519	429	596
	_ 13	27	4	264	244	291	291	315	287	165	315	285	277 276 276	288	266	29	0 227	284	283	266	325	550	496	519	429	589
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[]	13	27	48	262 262	241	289	289	312	285	163	313	282	274	286 285 284 283 282 281	264	28	7 225	281	281	265	324	550	496	519	430	573
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	_ 13	28	33	260	239	287	286	310	283	162	311 310 309 308	279	272	283	261	28	5 223	279	278	266	323	551	497	519	431	566
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	13	29	3	259	238	284 283	285	308	281	160	309	278	271	281	260	28	4 222	277	277	265	322	551	498	519	431	564
L	13	29	18	258	238	283	284	308	281	159	308	277	270	281	259	28 28 28 28 28 28	3 221	276	276	265	322	552	498	519 519 519 519 519	432	564

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illous.	13	29				283	283	307		160	307			279					276					519		
	13	29			236	282	283	306	279	160	307	276		279	258	281	220	274	275	265 265	322 322	552 552	499 499	518	433 433	563 563 563 564 564 564 564 563 563
	13	30				281	282	305	278	159	306	275	268	278		281			275	265	322	552	499	518	433	563
	13	30			235	279	281	304	278	158	305	274	267	277		280	218		274	265	322 322	553	499	518	433	563
	13	30	34	254	234	279	280	303	277	158	304	273	267	276	256	279	218		273		321	553	500	518	434	564
	13	30	48		234	279	280	302	276	158	304	272	266	276		280 279 278	218	272	273	265	321	554	500	519	434	564
	13	31	4	254	233	277	279	301	275	157	303	271		275		278	217		272			554	500 500	519	434	564
	13	31			233	276	278	300	274	156	302	270		274		277			272		321	555	500	519	434	564
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ļ	13	32			230	274	276	297	272	153	299	267		270		274						555	500	519	434	562
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	13	32			229	271	274	296	270	153	298	265	260	269					267		318	556	500		434	560
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	13	34				268	271			151	295	262		265							315	557 557	501 502			560
	13	34				266	270	291	266	151	293	261		264	245	268		260	264 264		315	557	502	520 521	434	560 ECO
	13	34				265	270	290		151	292	260		263		268			264		315	557	502	521	434	561
<u> </u>	13	34				265	269	290		151	292	259		263	244	267			263		315	558	503	521	435	
-	13	35				264	268	289		151	291	258	255	262	243				263		314	558	503	521	435	562
	13	35				264	267	288		150	290	258	254	261	243				262		314	559	503	522	435	564
	13	35			223	263	267	287		150	290	257	254	261	242	265			262		313	559	505	522	435	564
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	13	36	3	244		262	266	286	261	149	289	256	253	259	241			256	260		313	559	505	523	435	564
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	13	36				259	264	284	259	149	287	254	252	259	242	264	208	256	262	257	313	560	506	523	434	563
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	13	37			219	258	263	283		149	286	254				266			266		316	560	507	523	434	563 563 562
	13	37			219	257	262	282	257	149	285	254	252	262	249	267			268		317	560	507	523	434	563
.	13	37			219	257	261	281	257	149	284	254	252	264		269			270		318	561	508	524	434	562
	13	38			218	256	261	280	256	148	284	254	252	265		271		265	273		319	561	509	524	434	562
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	13	38			216	255 254	259	279		148	283	254	252		262	275			278		323	562	509	525	434	563
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 	13	39		237	215 215	253 251	258 258	277 276		148	282	255	253 254	272 274		279			282		325	562	511	525	434	565
	13	39				251	258	275		148	281 280	255 255		274	271 274	281 283		275 277	284 287		328 329	562 563	511 513	525 526	434	565 566
	13]	39	34	236	214	251	200	2/5	252	14/	280	255	253	2/6	2/4	283	246	2//	287	266	329	563	513	526	434	566

EOIF	TAC	E: Wed De	c 15 19	93 7:39:18	3 am						<u> </u>
ime		Time			PF-001	FT730	FT			PP-001	PT720
our		min	sec	Lt/min	Lt/min	Lt/min	Lt/	/min	PSIG	PSIG	PSIG
	7	40	3	0	56	4	1	0	-2	-2	
	7		18	0		4	ı	0	-2	-2	
	7		33	0	67	3		0	-2	-2	
	7	40	48	0	61	3		Oi	-2	-2	
	7		3	0		5		0	-2		
	7	46	6	0	58		1	0	-2		
		46	10	0	58	5		0	-2	-2	
	7		13	0	58	5	:-	0	-2	-2	
	7	46	16			5		0	-2	-2	
								0	-2	-2	
	7	46		0			-			-2	
	7	46	22	0			-	0	-2		
	7	46	25	0		5		. 0	-2	-2	
	7	46	28	0				0	-2	-2	
	7	46	31	0				0			
	7	46	34	0	56	5		0		-2	
	7	46	38	0	56		5	0	-2		
	7		41	0		5	5	0	-2		
	7	46	44	0	61	5		0	-2		
	7	46	47	0	61	5	5	0	-2	-2	
	7	46		0		5	5	0	-2		
	7	46	53	0			1	0			
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	 7	47	2	0				0			
	-	47	6					0			
	7	47	9	0				0	-2		
	7			0	·		-	0	-2		
	- ' 7	47	15	0	•		-	0			
											
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	7	47						0			
	7							0	-2		
	7							0			
	7		•				5	0			
	7							0			
	7	48	34	0	71			0			
	7	48	49	0			1	0			
	7	49	4	0	53	7	7	0	-2		
	7	49	19	0	50	7	7	0	-2	-2	2
	7	49	34	0	61	2	2	0	-2	-2	2
	7	49	49	0	56	2	2	0	-2	-2	2
	7	50		0			2	0		+	2
	 7		·				2	0			
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	7						2	<u>ö</u>			
	7	51					1	- 0			
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	$-\frac{7}{3}$						7'	- 0		-2	
		51	48)	0			
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	7					ļ	2	0			
	7	52					7	0			
	7	52	48	0			7	0		-2	2
	7						5	0			
	_ 7						5	0			
	7		34	0		:	5	0			
	7					!	5	0		-2	2
	7				52		1	0	-2	-2	2
	7						5	0			
	7						5	0	-2	-2	
	-						5	0		-2	
	- 					,	5	0	-2		
	- ' 7						1				
	7	55					2	0			
	7	55						0			
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	7	56	48	397	379	18	6	0	64	50)

Time	Time		FT720	PF-001		FT800	PT710		PT720
hour 7	min 57		Lt/min	Lt/min	Lt/min 162	Lt/min	PSIG	PSIG	PSIG
7		18 33	386 386	361 373	148	0	68 71	53 57	10
		48	387	302	5		68	55	15
7		3	387	289	5		68	55	
7		18	387	336	5	0	68	55	
7		34	387	352	5		68	55	15
7		49	74	335	77	0	-3	16	
7		4	4	-4	4	Ö	-6	31	10
7		19	4	-4	4		-6	31	9
7		34	4	-4	4		-6	30	9
7		49	4	-4	4		-6	30	8
8		4	0	-5	0		-6	30	9 8 8
8		19	ō	•5	1	0	•6	30	8
8		33	0	-5	6	0	-6	30	7
8	0	48	0	-5	6	0	-6	30	7
8	1	3	0	-5	1	0	-6	30	7 6
8	1	18	0	-5	2	0	-6	30	6
8	1	33	0	-5	7	0	-6	30	6
8	1	48	0	-5	7	0	-6	30	6 5
8	2	3	0	5	1	0	-6	30	5
8		18	0	-5	0	0	-6	30	5
8	2	33	0	-5	0	0	Ģ	30	5 4
8	2	48	0	-5	1		-6	29	4
8	3	3	0	-5	1	0	-6	29	4
8		18	0	• 5	1	0	-6	29	4
8		34	0	-5	0	0	-6	29	3
8		49	0	-5	6	0	-6	28	3
8		4	0	-5	7	0	-6	28	3 3 2 2 2
8		19	0	•5	1	0	-6	28	3
8		34	0	-5	7	0	-6	28	2
8		49	0	-5	7	0	-6	28	2
8		4	0	-5	1		-6	28	2
8		19	0	-5	1	0	-6	28	2
8		33	0	-5	0	0	-6	28	2
8		48	0	-5	0	0	-6	27	1
8		3	3	-5	6	0	-6	5	0
8		18	399	-5	221	0	56	49	0
8		33	399	388	188	0	63	51	2 5
8		48	393	359	183	0	64	51	5
8		3 18	393	366	171	0	66	53	8
8		33	387 380	367	159 30	0	69	55	12
8		48		358		0	67	55	16
8		48	387 387	361 382	4	0	68 68	55 55	15
8		19	387	382	4	0	68	55 55	15 15
8		34	387	347	4	0	68	55 55	15
8	 	49	387	320	6	0	68	55	15
8		4	387	359	5	0	68	55 55	15
8		19	387	371	5	0	68		
8		34	387	309	5	Ö	68	55 55	15 15
8		49	386	361	5	0	68	55	15
8		4	386	352	6	0	68	55	15
8	10	19	386	370	6	0	68	55	15
8		34	386	352	2	0	68	55	15
8		49	386	361	1	0	68	55	15
8		4	386	364	1		68	55	15
8		19	386	349	1	ō	68	55	15
8		33	386	355	1	0	68	54	15
8	11	48	386	384	1	0	68	54	15
8	12	3	386	383	. 0	0	68	54	15
8		18	386	381	2	0	68	54	15
8	12	33	386	373	6	0	68	55	15
8		48	387	352	1	. 0	68	55	15
8	13	3	387	411	1	0	68	55	15
8		18	387	399	1	0	68	55	15
8		33	387	360	1	0	68	55	15
8		48	386	401	0	0	68	55	15
8		4	386	359	0	0	68	55	15
8		19	386	355	2	0	68	55	15
8		34	386	385	1	0	68	55	15
. 8	14	49	386	383	2	0	68	55	15

Time hour	Time min		Time sec	FT720 Lt/min	PF-001 Lt/min	FT730 Lt/min	FT800 Lt/min	PT710 PSIG	PP-001 PSIG	PT720 PSIG
	8	15	4	386	362	6	0		55	15
	B	15	19	386	390	2	0	68	55	15
	B!	15	34	387	378	2 5	0	68 68	55 55	15 15
	Bi B	15 16	49 4	387 387	383 370	0	0	68	55	15
		16	19	387	398	1	0	68	55	
		16	33	387	349	1	0	68	55	
	8:	16	48	388	351	1	0	68	55	15
	8:	17	3	388	353	1	0	68	55	15
	8	17	18	388	364	1	0		55	15
	В	17			364	1	0		55	15
	8	17	48	387	360	2	0	68	55	
		18	3	387	352	2	0	68	55 55	
	8	18 18	18 33	387 387	358 325	1	0	68	55	
	8	18	48	387	360	1				15
	8	19	4		378	1	0		55	
	8	19			342	1	0		55	15
	8	19			340	7			55	15
	8 -	19			342	7	0		55	15
	81	20			365	6	0		55	15
	8 8	20 20	19 34		314 322	7	0		55 54	15
	8	20	49			2	0			
	8	21	49		364		0			15
	8	21	19			2	Ö			15
	8	21	34	388	386	1	0	68	55	
		21	48							15
	8	22	3			1				
	81	22	18		398				55	15
	8 8	22 22			354 357	6	0		55 55	
	8	23			378		0			15
	8	23					0			
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	8	23					0	68	55	15
	8	24							·	
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	8	26								15
	8	26								15
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	8:	26								
	8 ¹	27 27	<u> </u>				<u> </u>			
	8	27								
	8;	27								
	8	28					O			15
	8	28	18	387	335	5	0	68	55	15
	8	28		387	375	5			54	15
	8	28					0			15
	8	29				2	0			15
	8 [;]	29 29							•	15
	81	29								
	8:	30								i 15
	8	30		388	401					15
	8i	30	34	389	357	7				15
	8	30		389	363	2	C			3 15
	8	31								
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	8:	31								
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	8	32				6				3 13
	8	32								

Time	Time	Time	FT720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour	min	sec	Lt/min	Lt/min		Lt/min	PSIG	PSIG	PSIG
	· · · · · · · · · · · · · · · · · · ·	48	0	-5	2	0		36	11
8		3	0	-5	6	Ŏ	-6	35	11
		18	0	-5	7	Ö	-6	35	10
		33	0	-5	0	0	-6	35	10
8		48	0	-5	7	0	-6	35	9
		3	0		1	0		35	9
8		18		-5			-6		
			6	-5	1	0	-6	35	8
		34	6	-5	2	0		35	8
		49	1	-5	7	0		35	7
		4	1	-5	1			33	7
8		19	6	-5	2	0		33	6
8	35	34	1	-5	2	0	-6	33	6
8	35	49	1	-5	2	0	-6	32	5
8			6	-5	1	0	-6	32	5
8	36	19	0	-5	1	. 0	-6	32	5
8	36	34	0	-5	2	0	-6	30	5
8		49	0	-5	8	0	-6	30	4
		3	0	-5	0	0	-6	30	4
8		18	ō	-5	1	0	-6	30	4
		33	Ö	-5	1	ō	-6	29	3
8		48	0	-5	Ö	0	-6	29	3
	+	3	0	-5	1	0	-6	29	3
		18	0	-5 -5		0	-6 -6	29	3
					2				3
8		33	0	-5	2	0		27	2
8		48	0	-5	2	0	-6	27	2
		3	0	-5	1	0		27	
		18	0	-5	2	0	-6	27	2
8		34	0	-5	2	0	-6	26	2
		49	19	- 5	9	0	-6	19	1
		4	253	-5		0	58	50	0
8		19	400	358	195	0	62	52	2
		34	394	380	184	0	65	52	5
8		49	394	348	172	0	67	52	8
8	41	4	388	355	160	0	69	55	12
8	41	19	382	351	45	0	68	55	16
8	41	34	382	365	7	0	68	55	16
٤	41	49	382	365	1	0	68	55	15
		4	388	367	1	0		55	15
8		19	388	354	2	0	68	55	15
8		34	388	364	2	ō	68	55	15
		48	388	380	2	ō	68	55	15
8		3	388	350	2	Ö	68	55	15
		18	388	373	2	0		55	15
		33	388	349	1	0		55	15
		48	388	352	2	0		55	15
	 	3		355	7			55	15
			386			0			
		18	386	399	5	0		55	15
	·			307		0			
8		48	386			0		55	15
		3	387	379		0		55	15
		19	387	376		0		55	15
		34		386		0		55	15
8		49	387	354	2	0		55	15
		4		335		0		55	15
8		19	386	393	2	0		55	15
ε	46	34	386	333		0	68	55	15
8		49	386	333		0	68	55	15
	47	4	387	344		0	68	55	15
8		19		397	2	0		55	15
		33	387	340		0	68	55	15
8		48	387	366		0		55	15
		3	385	374		0	68	55	15
<u>-</u>		18		336		ő		55	15
		33	385	353		0		55	15
				394		0		55	15
8		3		381	4	0		55	15
		18	389	343		0	68	55	15
		33		361		0		55	15
		48	389	376				55	15
				355		0			15
	50	18	387	338	2	0	68	55	15

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Time	Time	Time		FT720	PF-001		FT800	PT710	PP-001	PT720
hour	min	sec		Lt/min	Lt/min			PSIG		PSIG
	8	50	34		301	2	0			15
	8	50	49	387	386	2	0	68	55	
	8!	51:	4	386	347	2	0	68	55	15
	8	51	19	386	366	. 1	0	68	55	
	8	51	34	386	303	2	0	68	55	15
	8:	51	49	386	359	2	0	68	_ 55	15
	8	52	4		341	7	0	68	55	15
	8	52	19		347	2	0	68	55	
	8	52,	33	388	370	2	0	68	55	
	8.	52	48		343	1	0		55	15
	8	53	3		369	1	0	68	55	15
	8	53	18		337	6	0	68	55	
	8	53	33		365	2	0	68	55	15
	8	53	48 3			5 0		68	55	15
	8	54 54	18				0	68	55	15
	8.				353	7	0			•
	<u>8.</u> 8.	54 54	33 48		343 337	1.	0	68	5 <u>5</u> 55	10
						1	0	68		15 15
	8: 8:	55 55	19	386	356 372	7	0	68	<u>55</u> 55	15
	8:	55	34		372	7	0		55	15
	8i	55	49		405	6	0	68	55 55	15
	8	56	49	,	368	0			55	
	<u>8</u>	56,	19		-	4	0		55	15
	<u>8</u> 8	56	34		388	4	0		55	
	8	56	48		377	4	0		55	
	8	57	3			4	<u></u>	68	55	
	8	57	18	 	349	0	0	68	55	
	8	57	33			0	0		55	
	8	57	48				0	• — —		•
	8	58	3			2	0	68	55	
	8	58	18			0	0		55	4
	8	58	33		359	2	0		55	
	8	58	48			0	0	•	55	
	8.	59	3			2	0			
	8.	59	18			2	0			
	8.	59	33				0			
	8	591	49			6	0	68	55	15
	9	0	4	389	379	2	0	68	55	
	9	0.	19	389	395	1	0	68	55	
	9	0:	34	385	354	6	0	68	55	
	9	0.	49	385	370	6	0	68	55	15
	9	1	4	385	356	7	0	68	55	
	9	1	19	385	367	4	0	68	55	
	9	1	33	388	373	4	0	68	55	15
	9	1	48		·	4	0		55	15
	9	2	3	•			0		55	
	9	2	18				0	68	55	15
	9	2	33		329		0		55	
	9	2	48		365					
	9	3	5		376					
	9	3	18		345	2	0			
	9:	3	33				0	•		
	9	3	48							
	9	4	3				0		55	
	9	4	18							
	9	4	34				0		55	
	9.	4!	49							
	9'	5	4		•	54		•		
	9	5	19				0	•	,	
	9.	5	34				0			
	9	5	49		-3					
	9	6	4							
	9	6	19							1
	9	6	33			2		•		
	9	6!	48					4		
	9	7	3							
	9.	7	18							
	9	7	33							1
	9	7	48							
	9	8	3	12	-5	6	0	-6	35	.1

Time						-T730				PT720 PSIG
hour	_			Lt/min		_t/min			PSIG	
	9	. 8	18	9	-5	0	0	-6	35	
	9	8	33	4	-5	0	0	-6	35 35	
	9	8	48	4	-5	0	0	-6 -6	33	
	9	9	4	4	- 5	0	0	-6	33	
	9	9	19	4	-5	0	0	-6	33	
	9	9	34	4	-5	0	0	- <u>-</u> -6	32	
	9	9	49	0	-5	1	0	-6	32	
	9	10	4	0	-5	1	0	-6	32	
	9	10	19	0	-5	2	0	-6	30	
	9	10	34	0	-5	2	0	-6	30	
	9	10	49	0	-5			-6	30	
	9	11	4	0	-5 -5	1 	0	-6 -6	29	
	9	11	18		-5 -5	2		-6	29	
	9	11	34 48	2	-5 -5	6			29	
	9	11 12				6			29	
	9	12	3 18	2		7			27	
	9	12	33			1			27	
	9	12	48	- 0	-5	1			27	
		13	3			4			27	
	9	13	18			4			26	
	9	13	33			4			26	
	9	13	48			10			12	
	9	14	3			194			52	
	91	14	18			189			52	
	9	14				177			- 52	2 6
	9	14				165				
	9	15				153	1			
	9	15				4	}		55	
	9	15				4				
	9	15				4		. 68	55	5 15
	9	16				4	C	68	55	15
	9	16				5		68	55	5 15
	9	16				C		68		
	9	16		385	406	4	1 (
	9	17		385	355	4	(
	9	17	18	386	326	4	(
	9	17	33	386		4				
	9	17	48	386		2	? (
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	9			386				68		
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	9	21		387				0) 68 0) 68	-	
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	9							68		
	9			38				0 68		
	9							0 68		
	9	2:						0) 68		5 1
	9			38 38 38 38 38 38 38 38 38 38 38 38 38 3				0 68		
	9	2:						68		
	9							0 68		
	9						2	0 67		5 1
	9						6	0 68		5 1
	9			3 38				0 68		5 1
	9	2.						0 68		5 1
	9							0 68		5 1
	9							0 68		55 1
	9							0 68		55 1
	9			8 38				0 68		55 1
	9			4 38 9 38				0 6		55 1

Time	•	Time	Time	F1720	PF-001	FT730	FT800	PT710	PP-001	PT720
hour			sec	Lt/min	Lt/min	Lt/min	Lt/min		PSIG	PSIG
	9	26	4	388	336	4	0	68	55	15
	9	26	19	387	372	4	0	68	55	15
	9	26	34	387	362	4	0	68	55	15
	9	26	49	387	392	4	0	68	55	15
l	9	27	3	387	371	8	0	68	55	15
	9	27	18	384	296	1	0	68	55	15
	9	27	33	384	320	6	0	68	55	15
	9	27	48	384	369	1	0	68	55	15
	9	28	3	384	370	2	0	68	55	15
	9	28	18	387	372	0	0	68		15
	9	28	33	387	353	6	0	68	55	15
	9	28	48	387	342	7	0	68	55	15
	9:	29	3	387	354	1	0	68	55	
	9	29	18	388	366	1	0	68		
	9	29	33	388	360	1	Ö	68	55	15
	91	29	48	388	374	6	0	68		15
	9	30	4	388	330	0	0			
	9	30	19	387	345	2	0			
	9	30	34	387	380	7	ō	·	55	
	9	30	49	387	349	1	0			
	9	31	4	387	371	1			55	
-	-9	31	19	388	385	2	Ö			
	9,	31	34	388	352	7	ő			
·	9	31	49	388	351	Ö	0			
	9	32	4	388	325	1	0			
	9	32		387	359		ō	 		
	9	32	34	387	365	2	ŏ			
	9	32			354		Ö			
	-9	33	3		343		0			*
	9	33	18	385	316	2	Ö		55	
	9	33	33	385	344		0			
	9	33	48	385	287	1	0		55	
	9	34	3		334		0			
	9	34	18	385			0		55	
-	9.	34	33	385		6	0			
	9	34	48			7			55	
	9	35	4	385						·
	9	35	19			2	0			
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Thermal Shock Data for Components

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	9	5	4	361	568	492	461
	9	5 5	19	361	568	492	461
	9	5	34	361	568	492	461
	9	5	49	359	568	492	472
	9	6	4	359	572	500	472
	9	6	19	359	572	500	
	9	6	34	359	572	500	
	9	6	48	358	572	500	479
	9	6. 7	3	358	575	505	479
	9	7	18	358	575	505	479
	9	7	33	358		505	
	9	7	48	358	575	505	488
	9 9 9 9		3	358	575	512	488
	9	. 8 8	18	358	578	512	488
-	9	8	33	358	578	512	488
	9	8	48	359	578	512	495
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	9	9	19	359	579	516	495
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	9	9	49	360	579	516	502
-	9	10	4	360	579		502
	9	10	19	360	581	523	502
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	9	10	49	359	581	523	507
	9	11	3	359	581	526	507
	9	11	18	359	581	526	507
	9	11	33	359	581	526	507
	9	11	48	358	581	526	507
	9	12	3	358	581	530	512
	9	12	18	358	583	530	512
	9	12	33	358	583	530	512
	9	12	48	358	583	530	512
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Thermal Shock Data for Components

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Data for Slow Cool Down of Components with Fan Simulating Nightly Cool Down.

			Check	4"flg	6"flg	
	Time Z				Z 524	Z 525
OCT20,1993 12:28:20 12 28 20	12.5	583	585	585	582	575 DEG F
OCT20,1993 12:43:20 12 43 20	12.7	586	588		586	581 DEG F
OCT20,1993 12:58:20 12 58 20	13.0	592	594	594	591	586 DEG F
OCT20,1993 13:13:20 13 13 20	13.2	574	582	579	581	575 DEG F
OCT20,1993 13:28:20 13 28 20	13.5	572	566	559		560 DEG F
OCT20,1993 13:43:20 13 43 20	13.7	584	550		-	546 DEG F
OCT20,1993 13:58:20 13 58 20	14.0	586	533	519		-
OCT20,1993 14:13:20 14 13 20	14.2	579	518	501	506	
OCT20,1993 14:28:20 14 28 20		589	502	482		505 DEG F
OCT20,1993 14:43:20 14 43 20	14.7	570	486	462	466	
OCT20,1993 14:58:20 14 58 20	15.0	591	469	444	449	
OCT20,1993 15:13:20 15 13 20	15.2	567	454	424	432	456 DEG F
OCT20,1993 15:28:20 15 28 20	15.5	585	437	406		
OCT20,1993 15:43:20 15 43 20	15.7	569	423	390		
OCT20,1993 15:58:20 15 58 20	16.0	575.	408	374	384	412 DEG F
OCT20,1993 16:13:20 16 13 20	16.2	572	393	358	370	396 DEG F
OCT20,1993 16:28:20 16 28 20	16.5	564	378	343		
OCT20,1993 16:43:20 16 43 20	16.7	575	364	330	345	372 DEG F
OCT20,1993 16:58:20 16 58 20	17.0	565	350	317	332	360 DEG F
OCT20,1993 17:13:20 17 13 20	17.2	573	339	304	322	355 DEG F
OCT20,1993 17:28:20 17 28 20	17.5	554	327	292	311	339 DEG F
OCT20,1993 17:43:20 17 43 20	17.7	575	315	282	301	334 DEG F
OCT20,1993 17:58:20 17 58 20	18.0	553	304	272		323 DEG F
OCT20,1993 18:13:20 18 13 20		572	294 294	261	282	310 DEG F
OCT20,1993 18:28:20 18 28 20	18.5	551	283	252	273	308 DEG F
OCT20,1993 18:43:20 18 43 20	18.7	571	273	243	265	296 DEG F
OCT20,1993 18:58:20 18 58 20	19.0	549	264	235	256	287 DEG F
OCT20,1993 19:13:20 19 13 20	19.2	570	255	227	248	284 DEG F
OCT20,1993 19:28:20 19 28 20	19.5	547	247	218	241	271 DEG F
OCT20,1993 19:43:20 19 43 20	19.7	569	239	212		269 DEG F
OCT20,1993 19:58:20 19 58 20	20.0	547	232	205	227	261 DEG F
OCT20,1993 20:13:20 20 13 20	20.0	568	224	198	221	250 DEG F
OCT20,1993 20:28:20 20 28 20	20.5	546	218	192	215	250 DEG F
OCT20,1993 20:43:20 20 43 20	20.7	567	211	186	209	242 DEG F
OCT20,1993 20:58:20 20 58 20	21.0	545	205	181	209	
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OCT20,1993 21:28:20 21 28 20					- •	
OCT20,1993 21:28:20 21 28 20 OCT20,1993 21:43:20 21 43 20	21.5	542	194	171	194	224 DEG F
	21.7	563	188	166	189	223 DEG F
	22.0	547	183	162	185	217 DEG F
OCT20,1993 22:13:20 22 13 20	22.2	562	179	157	181	208 DEG F
OCT20,1993 22:28:20 22 28 20	22.5	544	174	153	177	211 DEG F
OCT20,1993 22:43:20 22 43 20	_22.7	567	170	149	172	203 DEG F
OCT20,1993 22:58:20 22 58 20	23.0	541	_ 165	144	168	_ 198 DEG F
OCT20,1993 23:13:20 23 13 20	23.2	564	162	142	166	199 DEG F
OCT20,1993 23:28:20 23 28 20	23.5	538	159	139	162	190 DEG F
OCT20,1993 23:43:20 23 43 20	23.7	563	155	135	159	192 DEG F
OCT20,1993 23:58:20 23 58 20	24.0	539	151	132	156	187 DEG F

Data for Slow Heat Up of Components with Two Heat Trace Circuits.

	Heatup Wit	h Two Circ	uits
	CheckV	4"Flange	6"flange
Time,hr	TEPL-4	TEPL-8	TEPL-10
0	104.8205	104.8205	104.8205
0.4135	137.351	169.8815	148.1945
0.827	202.412	281.931	238.557
1.2405	245.786	354.221	289.16
1.654	285.5455	401.2095	354.221
2.0675	325.305	433.74	397.595
2.481	383.137	484.343	444.5835
2.8945	379.5225	469.885	448.198
3.308	404.824	502.4155	495.1865
3.7215	415.6675	502.4155	495.1865
4.135	422.8965	506.03	502.4155
4.5485	433.74	516.8735	516.8735
4.962	448.198	527.717	527.717
5.3755	459.0415	538.5605	538.5605
5.789	451.8125	520.488	520.488

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