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Heat Loss from an Open Cavity

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HEAT LOSS FROM AN OPEN CAVITY

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Sandia Contract 02-5759

ABSTRACT

This report presents the results of an investigation into the heat-loss characteristics of a cavity-type receiver for a parabolic dish concentrating solar collector. The receiver is similar to the type used in the Solar Total Energy Project in Shenandoah, Georgia. This investigation examines the effects of aperture size, orientation, and operating temperature on the heat loss of the receiver. The total receiver heat loss is quantitatively separated into its three modes: radiative, conduction, and convection. The testing was performed in a controlled environment, thereby eliminating any potential wind contribution. It was executed off flux, i.e., with no incident insulation. The receiver was operated in reverse of its typical operating configuration, whereby the heat-transfer fluid was heated externally. Previous heat-loss models or correlations with similar cavity receivers are compared with the experimental results from this study. A convective heat-loss correlation is presented from these experimental results. A theoretical model for the radiative heat loss is developed and compared with two methods used to quantitatively determine the radiative component of total heat loss.

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LIST OF ABBREVIATIONS

ADC	analog to digital converter
AC	alternating current
HTF	heat transfer fluid
N	number of sectioned elements of the receiver cavity internal surface area
STEP	Solar Total Energy Project
TC	thermocouple

I. INTRODUCTION

Cavity type receivers are used extensively in concentrating solar thermal energy collecting systems. The Solar Total Energy Project (STEP) in Shenandoah, Georgia is a large scale field test for the collection of solar thermal energy.⁽¹⁾ The STEP experiment consists of a large field array of solar collectors used to supplement the process steam, cooling and other electrical power requirements of an adjacent knitwear manufacturing facility.

The main components of each collector are the concentrator, the tracking mechanism, and the receiver (Fig. 1). The concentrator is a 7 meter diameter parabolic dish with a highly reflective coating on the inside surface. Each collector has two axes of rotation for tracking the sun all throughout the days of the year. The collectors are subjected to continuous changes in ambient conditions such as wind, solar insulation, and ambient temperature.

Figure 1. Solar Collector⁽¹⁾

These environmental variations, as well as changes in receiver tilt, affect the overall receiver performance. The receiver used in this study is a parabolic collector.

A thorough understanding of receiver heat loss characteristics is essential for future development of solar receivers, and optimization of the STEP system presently in use. The system boundary of the receiver is defined as the outer skin of the receiver and the aperture opening (Fig. 2). The portion of the boundary formed by solid walls are only subject to conductive heat transfer. The aperture, however; is subject to convective, conductive and radiative heat transfer. Mass transfer occurs across the aperture and through the heat transfer fluid lines crossing the system boundary.

Figure 2. Heat transfer system boundary

Analytical methods for predicting the conductive and radiative heat losses from a cavity receiver are fairly straight forward. This, however; is not the case for convective heat loss analysis. The complex geometry of the cavity makes it difficult to use existing analytical models for predicting convective heat loss. Few convective heat loss correlations, for cavity receivers, exist due to the lack of significant empirical data. Correlations for receivers with simple geometry are not considered valid for this receiver.

An extensive search of current literature produced only a few studies on heat loss from cavities. A study was performed by LeQuere, Penot, and Mirenayat in which heat loss characteristics of two different sized cubical cavities were examined.⁽²⁾ They considered variations in receiver operating temperature and angle, in their study. A study performed by Koenig and Marvin, presented by Harris and Lenz, gave an empirically derived correlation for convective heat loss from cylindrical cavity type receivers, including the effects of variation in operating temperature and angle.⁽³⁾ An analytical model for convective heat loss for an open cubical cavity receiver was presented by A. M. Clausing.⁽⁴⁾ The Clausing model was developed for a central receiver operating at much higher temperatures than the receiver studied here. Siebers and Kraabel presented a model for the convective heat loss from a central cylindrical cavity receiver.⁽⁵⁾

There is some experimental data available for this type of receiver from previous tests on off-flux field measurements conducted with limited instrumentation at STEP.⁽⁶⁾ Field measurement experiments, such as the one conducted at STEP, provide no control over environmental conditions such as wind, and ambient temperature. In order to control the environmental conditions, receiver testing for this study, took place indoors.

The purpose of the tests, conducted for this study, was to isolate and quantify the radiative, conductive, and convective components of total heat loss, and to determine the effects of operating temperature, receiver angle, and aperture size on cavity heat loss. An analytical model for radiative heat loss was developed and compared with two other methods used to determine radiative heat loss. A proposed convective heat loss correlation, including effects of aperture size, receiver operating temperature, and receiver angle is presented. The resulting data is a source to evaluate the STEP measurements.

II. APPARATUS

A. Receiver

A drawing of the receiver studied in this work is shown in cross section in Figure 3. The cavity of the receiver is composed of a single tube wound in a conical frustum-cylinder shape with the aperture at the cylindrical end of the tube bundle. The tube bundle is wrapped in a thick blanket of Kaowool® insulation. The outer skin of the receiver is formed by a single cylindrical wrap of sheet metal. The outer skin extends beyond the aperture face to serve as a wind break. The flow lines to and from the receiver are heavily insulated. The inlet and outlet lines for these tests, as shown in Figure 3, are the reverse of those for an on-flux receiver in field operation.

Figure 3. Cavity receiver cross section.

The receiver is cradled in a frame that allows it to rotate 180° (Fig. 4). The receiver can be fixed at 15° increments from -90°, where the aperture is upward, to +90°, where the aperture is downward (Fig. 5). The high pressure flexible lines on the sides of the receiver

test stand allow the receiver to rotate freely for each test position.

Thermocouples were used to measure the receiver inlet and outlet temperatures. Two in-house calibrated K-type thermocouples were immersed in each of the heat transfer fluid (HTF) inlet and outlet lines of the receiver. One of the thermocouples from the inlet and outlet lines measured absolute temperature. The remaining two thermocouples were connected in series to yield a direct measure of the temperature difference between the inlet and the outlet. The receiver was further instrumented with seventeen surface thermocouples and thirteen internal air thermocouples (Figure 6). The surface thermocouples were spot welded in place with the lead ends spaced approximately one-eighth inch apart.

Figure 4. Receiver test stand

TC	SW	TC	SW	TC	SW	TC	SW
ID	#	ID	#	ID	#	ID	#
1A	1	3A	8	5S	15	8A	22
1T	2	3S	9	6A	16	8T	23
1S	3	4A	10	6T	17	8S	24
2A	4	4T	11	6S	18	9A	25
2T	5	4S	12	7A	19	9S	26
2S	6	5A	13	7T	20	10A	27
3T	7	5T	14	7S	21	11A	28
						12A	29
						13A	30

An insulating annulus with a corresponding center plug were fabricated for each of the aperture sizes tested (Fig. 7). The aperture sizes tested were 6 inch diameter, 12 inch diameter, 18 inch diameter, and 26 inch diameter. The 18 inch diameter aperture is the size presently being used for this model of receiver. The 26 inch diameter, the internal diameter of the cavity, aperture leaves no lip to the cavity. The aperture plug and annulus were fabricated of 1 inch thick solid insulation boards. The plug was tapered inward to fit snugly in the respective aperture annulus. The plugs were held in place by two wooden straps extending across the aperture end of the receiver.

Figure 7. Annulus and plug

B. Flow Loop

The heat transfer fluid was heated by a heating and pumping station adjacent to the receiver (Fig 8). The flow system consists of two parallel flow loops- the primary heating loop and the receiver feed loop. The primary heating loop has available two in-line 12 kW electric heaters. A minimum flow rate of 5 gpm was maintained in the heating loop to prevent excessive film temperatures of the HTF in the heaters. The receiver feed loop was throttled for a flow rate through the receiver of 1 gpm. The HTF flow rate through the receiver was measured using three turbine flow meters connected in a series on the inlet line to the receiver. The flow meters are located in a straight section of piping allowing ample upstream and downstream damping lengths. Three flow meters are used for measurement redundancy. One flow meter was factory calibrated. The remaining two flow meters were

calibrated against the factory calibrated flow meter.

Figure 8. Heat transfer fluid heating system

C. Radiometer Setup

One method used to determine the thermal radiative heat loss from the aperture was with a radiometer. The radiometer was mounted on a tripod and placed directly below and centered on the receiver. The radiometer was water cooled and the return water temperature was monitored. The radiometer signal output leads were connected to the computer data acquisition system. A Saran Wrap window assembly was positioned over the radiometer in place of the quartz window bezel. The radiometer window serves to isolate the temperature sensitive thermopile surface from localized convective currents. This is discussed further in radiometer calibration section.

D. Data Acquisition

A computer was used for data acquisition and display. This consisted of an Apple IIe computer with two 16-channel data acquisition cards each connected to a thermocouple cold junction terminal box. The following transducers were connected to the data acquisition system; receiver inlet and outlet thermocouples, two ambient thermocouples, three receiver flow meters; radiometer; radiometer water thermocouple; loop inlet and outlet thermocouples; and the main flow loop flow meter . The surface and air thermocouples on the receiver were connected to a digital display unit via a multi-channel thermocouple switch. The surface and air receiver temperature readings were recorded manually when steady state conditions were obtained for each test point.

III. TEST METHOD

The testing was conducted in two phases. Phase One of the testing examined the effects of receiver operating temperature and receiver angle on the receiver heat loss. Phase Two looked at the effects of receiver aperture size on the receiver heat loss. After Phase One, and before Phase Two, the receiver was overhauled. The overhaul of the receiver included

replacing the insulation in the walls, repainting the tube surfaces, and resealing the seams and ports through the outer skin of the receiver.

A. Temperature and Receiver Angle Effects

The model of the effects of temperature and receiver angle on heat loss developed in this study utilizes results from both Phase One and Phase Two tests. The overlap portion of the Phase One and Phase Two tests were compared for ease of repetition. The four nominal operating temperatures in Phase One testing were 300°F, 400°F, 500°F, and 600°F with the standard 18 inch aperture. The Phase Two study was conducted at operating temperatures of 400°F and 600°F and incorporated 6, 12, 18, and 26 inch apertures. The nominal operating temperature was based on the average of the inlet and outlet temperatures. For each operating temperature the receiver was tested at ten angles from -90° to +90° in Phase One. The receiver angles tested were from 0 to +90°, every 15° and from 0 to -90°, every 30°. Phase Two included receiver angles from 0° to +90°, every 15°. More angles were tested in the positive range, since most cavity receivers operate in this range. The negative angles were tested to provide a clearer understanding of heat loss characteristics, as a function of receiver angle. However, some concentrating solar collector designs operate with inverted cavity receivers.

At the beginning of each test, the receiver was placed in the +90° position with the aperture facing down. The flow system was started and the fluid was heated as close to the operating temperature as possible. Obtaining the nominal HTF temperature at the receiver inlet usually meant setting the heater temperature 25°F to 50°F higher, accounting for heat loss from the connecting line. The flow rate through the receiver was adjusted to approximately one gallon per minute. The one gallon per minute flow rate is typical for these type of receivers at STEP. Thermal stabilization is attained when there is less than 0.1 degree change in the inlet and outlet temperatures over the two minute data sampling

interval. Reaching thermal stabilization often takes several hours depending upon the nominal operating temperature and the ambient laboratory conditions. When thermal stabilization was reached, temperature and flow measurements were recorded.

The convective heat loss from the cavity of the receiver is assumed to be negligible when the receiver is in the $+90^\circ$ position. This assumption is supported in two ways. First, smoke flow visualization techniques revealed negligible air flow across the aperture with the receiver in the $+90^\circ$ position. The second is the minimal variance between experimentally determined radiative heat loss at $+90^\circ$ and the calculated values and radiometer measurements.

Therefore, the total heat loss from the receiver in the $+90^\circ$ position is composed of radiative losses from the aperture and conductive losses through the side, back, and annulus walls of the receiver. The aperture of the receiver was then fitted with an insulated plug to eliminate the radiative component from the total heat loss. With the plug in place, the system was again allowed to reach steady state and again the temperature and flow measurements were recorded. In this manner, the radiative and conductive components of the total heat loss from the receiver for a particular operating temperature were isolated. The radiative and conductive heat losses are assumed constant with receiver angle.

The receiver was then positioned in the $+75^\circ$ attitude and the system allowed to stabilize. The temperature and flow measurements were again recorded. The total heat loss measurements were normalized linearly to the nominal test temperature for comparison purposes. This accounted for the variation in the operating temperature from one test setup to the next. The thermal stabilization procedure was repeated for each receiver angle tested. The entire procedure was repeated for each nominal operating temperature test point.

The total heat loss from the receiver can be expressed as a mathematical relation. The preceding appears as:

$$q_{\text{total}} = \dot{m} C_p (T_{\text{in}} - T_{\text{out}}) \quad (1)$$

where:

T_{in} = temperature of fluid at the inlet to the receiver [K]

T_{out} = temperature of fluid at outlet to receiver [K]

$\dot{m}$ = mass flow rate of the fluid [g/m]

C_p = specific heat of the fluid [K]

The mass flow rate is given by:

$$\dot{m} = \dot{v} \rho \quad (2)$$

where:

$\dot{v}$ = volumetric flow rate

ρ = heat transfer fluid density at the inlet temperature

The conductive heat loss is given by:

$$q_{\text{conductive}} = q_{\text{plugged @} +90^\circ \angle} \quad (3)$$

The radiative heat loss is given by:

$$q_{\text{radiative}} = q_{\text{unplugged @} +90^\circ \angle} - q_{\text{plugged @} +90^\circ \angle} \quad (4)$$

The convective heat loss at any angle, α , is then given by:

$$q_{\text{convective @} \alpha \angle} = q_{\text{total @} \alpha \angle} - q_{\text{conduction}} - q_{\text{radiative}} \quad (5)$$

The HTF volumetric flow rate, inlet temperature, outlet temperature, and temperature difference were all measured with transducers. The density and heat capacity were both calculated as functions of temperature.

B. Aperture Size Effects

The second Phase of the testing examined the effects of receiver aperture size on the

receiver heat loss. This Phase of the testing was performed at two operating temperatures of 400°F and 600°F, and seven receiver angles from 0 to +90° at 15° increments. The four aperture sizes tested were 6 inches, 12 inches, 18 inches, and 26 inches. The 18 inch diameter aperture is the standard size for this receiver. The Phase Two testing followed the same procedure used in Phase One testing with the additional step of changing aperture size. Heat loss values from Phase One were compared with Phase Two.

V RESULTS

A. Temperature and Angle Effects on Total and Convective Heat Losses

The data summary of the receiver operating temperature and receiver angle effects from the Phase One tests are tabulated in Appendix 1. These results were first presented by Stine and McDonald⁽⁸⁾. Total receiver heat loss varies, approximately, linearly with operating temperature (Fig. 9).

Figure 9. Total receiver heat loss versus operating temperature

The total receiver heat loss varies non-linearly with receiver angle (Fig. 10). The total heat loss is at a minimum when the receiver aperture orientation is downward. This supports the assumption of negligible convective heat loss with the receiver in this position. The maximum heat loss occurs when the receiver aperture is oriented at approximately $+45^\circ$ above horizontal. This particular receiver would not normally operate at angles above horizontal as these are negative angles.

Figure 10. Total heat loss versus receiver angle for 18 inch aperture

Results from duplicate test conditions from Phase Two are also presented in Figure 10. As discussed previously, the convective heat loss through the aperture is determined by the difference between the total heat loss at any angle and the total heat loss for the $+90^\circ$ angle (Fig. 11). This requires that the convective heat loss be zero when the receiver is positioned at $+90^\circ$, with the aperture down. The maximum convective heat loss occurred with the receiver in the -45° position. The reduction in total heat loss from Phase One to Phase Two

testing, for receiver angles less than $+60^\circ$, was assumed to be primarily due to the improved insulating properties of the cavity walls. The larger difference in the total receiver heat loss from Phase One to Phase Two for receiver angles greater than $+60^\circ$ resulted from the combined effects of improved insulation in the cavity walls and better sealing of the outer receiver skin. Apparently, sealing of the skin had little effect on heat loss from the receiver for angles less than $+60^\circ$.

Figure 11. Convective heat loss for 18 inch aperture versus receiver angle

B. Aperture Size Effects on Total and Convective Heat Losses

The data summary of the Phase Two aperture size testing are tabulated in Appendix 2.

These results were first presented by Stine and McDonald⁽⁸⁾. The effect of aperture size on the receiver total heat loss is shown (Fig. 12) for an operating temperature of 600°F. At a receiver angle of 0° , the total receiver heat loss increases by a factor of three as the aperture diameter increases from 6 inches to 26 inches. The total heat loss at the $+75^\circ$ and $+90^\circ$

receiver angles are approximately equal. This agrees with a previous study (Stein and McDonald) on the effects of receiver angle⁽⁶⁾. At these positions the total receiver heat loss increases by a factor of two when the aperture diameter increases from 6 inches to 26 inches for a 600°F operating temperature. At +45° the total heat loss increases approximately linearly with increase in aperture size. The receiver angle has less effect on the total heat loss for small apertures. The maximum variation due to receiver angle in the total heat loss is 0.4 kW for the 6 inch diameter aperture as compared to 1.2 kW loss with no aperture (26 inch aperture).

Figure 12. Total Receiver Heat Loss versus Aperture Size for 600°F

The effect of aperture size on the convective component of the total heat loss is shown in Figures 13 and 14. Aperture size has a much greater effect for low receiver angles than high receiver angles. The results also showed the convective loss increased dramatically when the aperture increased from 6 inches to 18 inches. There was little change in the convective loss as the aperture increased beyond 18 inches.

Figure 13. Convective Heat Loss versus Aperture Size for 400°F

Figure 14. Convective Heat Loss versus Aperture Size for 600°F

C. Radiative and Conductive Heat Losses

In these tests, the radiative heat loss was determined from the difference between the plugged and unplugged values of the total heat when the receiver is in the $+90^\circ$ position. The radiative heat loss was assumed constant for all receiver angles. The conductive heat loss, through the receiver walls, was given by the total receiver heat loss when the receiver was in the $+90^\circ$ position with the aperture plugged. The conductive heat loss was also assumed constant for all receiver angles. The radiative and conductive heat losses from Phase One and Two of the testing were compared for repeatability (Fig. 15). Some differences were expected as a result of overhauling the receiver after the Phase One tests.

Figure 15. Radiative and Conductive Heat Losses versus Receiver Temperature

An infrared radiometer was another method used to determine radiative heat loss. The difference between radiometer readings taken with the receiver plugged and unplugged measured the radiative heat loss through the aperture. The two methods for determining the radiative heat loss are compared for operating temperatures of 600°F and 400°F (Figs. 16 and 17). The radiative heat loss increased approximately with the square of the aperture area. For each of the two nominal operating temperatures, the analytical heat loss was slightly higher. The difference between the analytical and experimental data, radiative heat loss, increased positively with aperture size. The disparity was accounted for via the estimated parameters used in analysis. These parameters include surface emissivity, temperature distribution, refractory and non-refractory. For small aperture diameters to cavity volume ratios, the cavity will radiate through the aperture essentially as a black body regardless of the emittances of the internal surfaces. However, as the ratio increases the cavity becomes less of a black body emitter. For large aperture diameter to cavity volume ratios, the emittances of the internal surfaces become critical in determining the cavity emittance. Also, for larger apertures the temperature difference between the inlet and outlet becomes significant. The fixed difference used in the analysis for all aperture sizes could affect the results. Further investigation is required to provide more accurate temperature distributions.

Figure 16 Radiative Heat Loss versus Aperture Size at 400°F

Figure 17 Radiative Heat Loss versus Aperture Size at 600°F

The total heat loss make-up, in terms of the radiative, conductive, and convective components, changes with aperture size. With a 6 inch aperture and the receiver at 45° the conduction loss forms about 65% of the total heat loss. With the receiver at a typical operating angle of 45° and an operating temperature of 600°F , radiative and convective percentages of total heat loss are approximately equal to an aperture of 26 inches (Fig. 18).

Figure 18. Percent Heat Loss Modes versus Aperture Size for 600°F at 45° angle

VI. PREVIOUS CAVITY CONVECTION LOSS MODELS

A. LeQuere, Penot, and Mirenayat Model

LeQuere, Penot and Mirenayat presented an experimental correlation for Nusselt number as a function of Grashof number.⁽⁹⁾ Their study used a cubical cavity typical of those used in central receiver systems. The study investigated varying receiver temperatures and angles. The model was developed for a maximum temperature difference between cavity walls and

the ambient, 230°F. Variation in receiver angles used in the model were from 0°, where the aperture is upward, to 180°, where the aperture is downward.

The cavity used in their testing was modular in design so that each panel could be heated independently. The panels were electrically heated. The electrical power and temperature of each panel were measured. Modular design allowed for local as well as global heat loss analysis. The total heat loss of the cavity was determined from the total electrical power used by all the panels. They determined the radiative component for total heat loss by summing the radiative heat loss of each panel to the cavity aperture.

$$Q_{\text{radiative}} = \sum_i^{N_m} \epsilon \sigma S (T_{\text{panel}}^4 - T_{\text{ambient}}^4) F_{i-o} \quad (6)$$

where:

$\bar{\sigma}$ = Stefan-Boltzmann constant [W/m²-K⁴]

ϵ = emissivity of each panel

S = panel surface area [m²]

T_{panel} = individual panel temperature [K]

T_{ambient} = ambient temperature [K] opening

F_{i-o} = view factor for a panel to cavity opening

N_m = total number of panels that compose the cavity

The conduction heat loss component is determined by the total heat loss of a plugged cavity. By plugging the aperture of the receiver, the radiative and convective components of the total heat loss are eliminated.

The convective heat loss is determined by subtracting the conductive and radiative

components from the total heat loss.

$$q_{\text{convection}} = q_{\text{total}} - q_{\text{conductive}} - q_{\text{radiative}} \quad (7)$$

Their Nusselt number is given by:

$$Nu = \frac{q_{\text{convection}} L}{S k (T_{\text{panel}} - T_{\text{ambient}})} \quad (8)$$

where:

L = dimension of cavity aperture [m]

k = thermal conductivity of air [W/m•K]

S = total interior cavity surface area [m²]

The Grashof number is given by:

$$Gr = \frac{g \beta (T_{\text{panel}} - T_{\text{ambient}}) L^3}{\nu^2} \quad (9)$$

where:

g = local gravitational acceleration [m/s²]

β = thermal expansion coefficient of air [K⁻¹]

ν = kinematic viscosity of air [m²/s]

All fluid properties were evaluated at the ambient temperature. The experimental correlation for Nusselt number as a function of the Grashof number is given by:

$$Nu = a Gr^b \quad (10)$$

The coefficient 'a' and the exponent 'b' are empirically derived and are both a function of receiver angle. The values of 'a' and 'b' are presented in Table 1 for receiver angles of interest in this study. Equation 10 is valid for a Grashof number between 10⁷ and 5 x 10⁹.

Table 1.
Empirical correlation coefficients and exponents

Receiver Angle θ	Coefficient a	Exponent b
-90	0.0570	0.353
-75	0.0470	0.360
-60	0.0545	0.360
-45	0.0465	0.370
-30	0.0480	0.369
-15	0.0465	0.368
0	0.0925	0.330
15	0.0810	0.331
30	0.0640	0.332
45	0.0605	0.316
60	0.0685	0.292
75	0.0330	0.302
90	NA	NA

Consideration must be given to the difference in the cavity geometry from receiver used by LeQuere, Penot and Mirenayat and that used in this study. The receiver used by LeQuere, Penot and Mirenayat was cubical whereas the receiver used in this test was cylindrical and conical. The LeQuere, Penot and Mirenayat receiver aperture is the same as the characteristic interior dimension. They did not study the effect of varying aperture sizes.

LeQuere, Penot and Mirenayat modeled convective heat loss through the aperture is given by:

$$q_{\text{convective}} = h A (T_{\text{cav}} - T_{\text{ambient}}) \quad (11)$$

where:

h = convective heat transfer coefficient [w/m²k]

A = total interior cavity surface area [m²]

T_{cav} = area average cavity surface temperature [K]

T_{ambient} = ambient air temperature [K]

The convective heat transfer coefficient is given by:

$$h = \frac{k \text{ Nu}}{L} \quad (12)$$

where:

L = dimension of cavity aperture [m]

k = thermal conductivity of air [W/m-K]

Nu = Nusselt number

A BASIC computer language program was written to solve for the convective heat loss from the receiver used in this study applying the LeQuere, Penot, and Mirenayat model. For a listing of the computer program see Appendix 3. The results are presented in Appendix 4. The variations in the convective heat loss with receiver angles for operating temperatures from 300°F to 600°F and aperture sizes from 6 inches to 26 inches are presented (Fig. 19).

Figure 19. Convective heat loss for LeQuere, Penot, and Mirenayat model

B. Koenig and Marvin Model

The Koenig and Marvin model for predicting convective heat loss from a cavity receiver is presented by Harris and Lenz.⁽¹⁰⁾ Their model is based on operating temperatures between 550°C(1022°F) and 900°C(1652°F) for an on-flux analysis. The operating temperature range used by Koenig and Marvin is considerably higher than any receiver temperature tested in this study. The Koenig and Marvin receiver was designed to operate at higher temperatures.

For the Koenig and Marvin model the convective heat loss through the cavity aperture is given by:

$$\dot{q}_{cav} = h A_T (T_{cav} - T_{amb}) \quad (13)$$

where:

A_T = area of heat transfer tubing facing inside cavity [m²]

T_{cav} = inside cavity temperature or mean operating temperature [K]

T_{amb} = ambient air temperature [K]

h = cavity convective heat transfer coefficient [W/m²k]

The heat transfer coefficient is given by:

$$h = \frac{k Nu_{cav}}{L} \quad (14)$$

where:

k = thermal conductivity of air [W/m-K]

Nu_{cav} = Nusselt number of the cavity

L = characteristic length of the cavity [m]

The characteristic length of the cavity used by Koenig and Marvin is given by:

$$L = \sqrt{2} R_{\text{cav},i} \quad (15)$$

where:

$R_{\text{cav},i}$ = mean inner cavity radius [m]

The Nusselt number is given by:

$$\text{Nu}_{\text{cav}} = 0.52 P(\phi) \lambda_c^{1.75} (\text{Gr}_L \text{Pr})^{1/4} \quad (16)$$

where:

$P(\phi)$ = is an expression that accounts for the effects of receiver angle

λ_c = is an expression that corrects for aperture size

Gr_L = Grashof number

Pr = Prandtl number

The receiver angle function is given by:

$$P(\phi) = \cos^{3.2}\phi \quad \text{for } 0^\circ \leq \phi \leq 45^\circ \quad (17)$$

$$P(\phi) = 0.707 \cos^{2.2}\phi \quad \text{for } 45^\circ \leq \phi \leq 90^\circ \quad (18)$$

where:

ϕ = angle of cavity axis with the horizontal [degrees]

The aperture size function is given by:

$$\lambda_c = \frac{R_{\text{ap}}}{R_{\text{cav},i}} \quad (19)$$

where:

R_{ap} = cavity aperture radius [m]

The Grashof number is given by:

$$Gr_L = \frac{L^3 g \beta (T_{cav} - T_{amb})}{\nu^2} \quad (20)$$

where:

g = gravitational acceleration [m/sec²]

β = coefficient of volumetric expansion [K⁻¹]

ν = kinematic viscosity [m²/sec]

The volumetric expansion coefficient for air is calculated as:

$$\beta = \frac{1}{T_{prop}} \quad (21)$$

where:

T_{prop} = temperature at which the air properties are evaluated [K]

The Koenig and Marvin air properties temperature is given by:

$$T_{prop} = \frac{11}{16} T_{cav} + \frac{3}{16} T_{amb} \quad (22)$$

The thermal radiative losses through the cavity aperture from the hot interior surface is given by:

$$\dot{q}_{rad} = \pi R_{ap}^2 \epsilon_a \bar{\sigma} (T_{cav}^4 - T_{amb}^4) \quad (23)$$

where:

ϵ_a = emissivity of the aperture

$\bar{\sigma}$ = Stefan-Boltzmann constant [W/m²-K⁴]

$\epsilon_a \approx 0.9$ for these studies

The conduction heat loss through the walls of the cavity is given by:

$$\dot{q}_{\text{cond}} = \frac{k_i A_c (T_{\text{cav}} - T_{\text{amb}})}{t} \quad (24)$$

where:

A_c = area for conduction through the cavity [m²]

k_i = thermal conductivity of the cavity insulation [W/(m - K)]

t = thickness of cavity insulation [m]

The conduction area of the cavity for the receiver considered in this study is given by:

$$A_c = \pi \left(\frac{R_{\text{cav},i} + R_{\text{cav},o}}{2} \right)^2 + 2 \pi \left(\frac{R_{\text{cav},i} + R_{\text{cav},o}}{2} \right) + \pi (R_{\text{cav},i}^2 - R_{\text{ap}}^2) \quad (25)$$

where:

$R_{\text{cav},o}$ = cavity outside radius [m]

Application of the Koenig and Marvin model to the receiver under study here was accomplished using a BASIC computer language program. The program is listed in Appendix 5. The results of the Koenig and Marvin modeling are found in Appendix 6. Figure 20 summarizes the values in Appendix 6.

Figure 20. Convective heat loss for Koenig and Marvin model

C. CLAUSING MODEL

The Clausing model of convective heat loss from cavities was developed for large central receivers as opposed to the small receiver, used in this study.⁽¹¹⁾ The receivers utilized for the development of the Clausing model were simple in geometry with no curved surfaces. The Clausing model has been modified for application to the receiver provided in this study. The model was developed for on-flux mode of operation. For on-flux analysis the refractory surfaces are assumed to have a higher temperature than the active surfaces, whereas, for off-flux analysis the temperature conditions are reversed. Many of the temperature terms used in the Clausing model required modification to work for an off-flux situation.

Clausing's convective heat loss is based on an energy balance between the convective

energy loss within the cavity, q_c , and the energy transported through the aperture of the cavity, q_a (i.e. $q_a = q_c$) (Fig 21).

Figure 21. Convective heat loss balance

The cavity is divided into two zones: a convective zone and a stagnation zone (Fig. 22). The horizontal plane cutting through the upper lip of the cavity aperture divides the convective zone from the stagnation zone. The convective current in the cavity flow over the heated surfaces, the refractory surfaces, and the area of the horizontal plane dividing the stagnation zone from the convective zone. The heated and refractory walls in the stagnation zone do not participate in any convective heat transfer.

Figure 22. Receiver internal cavity zones

1. Convective Energy Loss Through the Aperture

According to Clausing, the convective energy loss through the aperture is given by:

$$q_a = c_p(\rho_\infty V_a A_a) (T_c - T_\infty) \quad (26)$$

where:

ρ_∞ = ambient air density [kg/m³]

V_a = average air flow velocity into the aperture [m/s]

A_a = area of the aperture through which air flows into the aperture [m²]

c_p = specific heat of ambient air [J/kg-K]

T_c = temperature of the exiting air [K]

T_∞ = ambient air temperature [K]

The average exiting velocity is given by⁽¹¹⁾:

$$V_a = \frac{1}{2} \sqrt{[(C_3 V_b)^2 + (C_4 V)^2]} \quad (27)$$

where:

$$C_3 = 1$$

$$C_4 = 1/2$$

V = wind speed [m/s]

V_b = buoyancy induced velocity [m/s]

For the no-wind condition, the interest of study, the equation reduces to:

$$V_a = \frac{1}{2} V_b \quad (28)$$

The buoyancy induced velocity is given by:

$$V_b = \sqrt{g\beta(T_c + T_\infty)L_a} \quad (29)$$

where:

g = local gravitational acceleration [m/s^2]

β = coefficient of volume expansion [K^{-1}]

L_a = projected vertical height of the aperture [m]

For air the temperature coefficient of volume expansion is given by:

$$\beta = \frac{1}{T_b} \quad (30)$$

where:

T_b = bulk air temperature in the convective zone of the cavity [K]

The bulk air temperature is given by:

$$T_b = \frac{T_c + T_\infty}{2} \quad (31)$$

The projected vertical height of the cavity is given by:

$$L_a = D_a \cos \theta \quad (32)$$

where:

D_a = the cavity aperture diameter [m]

θ = receiver angle [degrees]

2. Convective Energy Loss Within the Receiver

The Clausing model for convective heat loss within the cavity is given by:

$$q_c = hA_t(T_t - T_b) + hA_w(T_w - T_b) + hA_s(T_s - T_b) \quad (33)$$

where:

h = average heat transfer coefficient [W/m²-K]

A_t = tube surface area in convective zone [m²]

T_t = average tube surface temperature [K]

A_w = refractory surface area of cavity in convective zone [m²]

T_w = average refractory surface temperature [K]

A_s = area of interface plane between convective zone and stagnation zone [m²]

T_s = average temperature of interface plane [K]

The average heat transfer coefficient is determined from the Nusselt number and is given by:

$$h = \frac{Nu \, k}{L_a} \quad (34)$$

where:

Nu = Nusselt number

k = kinematic viscosity of air at the bulk fluid temperature [W/m-K]

For small receivers with a Grashof number of around 2.6×10^9 the Nusselt number is given by:

$$Nu = 0.10 (Gr \, Pr)^{1/3} \quad (35)$$

where:

Pr = Prandtl number = 0.7 (air)

Gr = Grashof number

The Grashof number is given by:

$$Gr = \frac{g\beta}{\nu^2} (T_w - T_\infty) L_a^3 \quad (36)$$

where:

ν = kinematic viscosity of air at the film temperature [m^2/s]

The film temperature is given by:

$$T_f = \frac{T_w + T_b}{2} \quad (37)$$

For the Grashof number expression the coefficient of expansion is given by:

$$\beta = \frac{1}{T_f} \quad (38)$$

Clausing assumes the temperature of the shear plane to be equal to the tube surface temperature in the convective zone (i.e. $T_s = T_t$). The cavity convective heat loss is then given by:

$$q_c = hA_t(T_t - T_b) + hA_w(T_w - T_b) + hA_s(T_t - T_b) \quad (39)$$

In this work, the refractory surface temperature is assumed to be 100°F cooler than the tube surface temperature. This temperature difference is typical for measured values at the end

plate refractory surface and a heated tube surface near the end plate.

The convective heat transfer areas within the convective zone will vary in size with changes in receiver angle. The expressions for the convective heat transfer areas as a function of receiver angle area are developed in the Zone Area Formulas section.

3. Radiative Energy Loss Through the Aperture

An approximation for the radiative energy loss from the cavity through the aperture, as presented by Clausing, is given by:

$$q_r = A_a \varepsilon \sigma \left[\frac{A_c}{A_c + A_h} (T_w^4 - T_a^4) + \frac{A_h}{A_c + A_h} (T_m^4 - T_a^4) \right] \quad (40)$$

where:

ε = emittance of the cavity

σ = Stefan-Boltzmann constant [W/m²-K⁴]

If the aperture is assumed to radiate as a black body then the emissivity of the cavity is equal to one; especially when the ratio of aperture size to cavity volume is small.

4. Conductive Energy Loss From the Receiver

The Clausing model for the conductive heat loss through the cavity walls is given by:

$$q_k = \frac{k}{t} [A_h (T_m - T_a) + A_w (T_w - T_a)] \quad (41)$$

where:

k = thermal conductivity of the cavity walls [W/mK]

t = thickness of the cavity walls [m]

For this study:

$k = .04756$ [W/mK]

$t = .0889$ [m] = (3.5 [in.])

5. Zone Area Formulas

The receiver cavity is divided into two zones (Fig. 23). The boundary between the zones is formed by a horizontal plane cutting through the cavity at the upper lip of the aperture. The upper zone is assumed stagnant while the lower zone has active convective currents. The area in zone 1 is represented by the internal surface area of the receiver above the horizontal plane. The area in zone 2 is represented by the internal surface area of the receiver below the horizontal plane. The areas of zone 1 and zone 2 vary with receiver angle for a given receiver geometry.

Figure 23. Cavity zones areas

The receiver internal geometry is divided into five sections representing the hot and cold surfaces in the receiver (Fig. 24). The hot surfaces are actively heated. The cold surfaces represent the refractory surfaces. Section 1 is the circular plate at the end of the frustum. Section 2 is the frustum portion of the tube bundle. Section 3 is the cylindrical portion of the tube bundle. Section 4 is the short refractory portion of the cylindrical section. Section 5 is the refractory ring that forms the aperture.

Figure 24. Cavity sections

As the receiver is rotated through various angles, each section of the internal receiver geometry may be divided by the horizontal plane that cuts through the upper inside edge of section 5. The formulas defining the portion of the area of each section that is in zone 1 for a given receiver angle range are derived in Appendix 7.

6. Shear Plane Area

The shear plane area is the area of the horizontal plane within the cavity (Fig. 25). The shear plane area is divided into two sections. The first section is formed by the horizontal plane cutting through the cylindrical portion of the receiver cavity. Not all of the horizontal plane in the cylindrical portion participates in the convective heat loss. The sides of the aperture reduce the effective shear plane area by restricting flow along the horizontal plane at the sides of the cavity near the aperture. The shear plane expands from the upper lip of

the aperture in the horizontal plane. The second section is formed where the horizontal plane cuts the frustum portion of the receiver cavity. The formulas that describe the shear plane area in the specified portion of the cavity for a given receiver angle are derived in Appendix 7.

Figure 25. View looking down showing the effective shear plane area

7. Clausing Model Analysis

A BASIC computer language program was written to solve the convective heat transfer equations (Appendix 8). The mean operating temperature in the program is taken as the tube surface temperature in the convective zone of the receiver. The program calculates the convective energy loss from the receiver cavity for receivers at operating temperatures of 300°F, 400°F, 500°F, and 600°F, receiver angles from 0 to 90° at 15° increments, and aperture diameters of 6 inches, 12 inches, 18 inches, and 26 inches. The results of the Clausing heat loss analysis are presented in Appendix 9. The results of the Clausing model analysis are shown in Figure 26.

Figure 26. Convective heat loss for Clausing model

D. Siebers and Kraabel Model

Siebers and Kraabel present a simple model for the convective heat transfer from a solar cavity receiver.⁽¹²⁾ They emphasize that the model has a large degree of uncertainty due to the lack of sufficient data on cavity receivers. The model was developed for a large central receiver cavity operations on-flux. This model is based primarily on the results of experimental studies from cubical cavities.

The following are the equations used to determine the convective loss from a solar cavity receiver. For natural convection the Nusselt number is given by:

$$Nu_L = 0.088 Gr_L^{1/3} \left[\frac{T_w}{T_\infty} \right]^{0.18} \quad (42)$$

$$\text{for } 10^5 \leq Gr_L \leq 10^2$$

where:

Gr_L = Grashoff number

T_w = average interior cavity wall temperature [K]

T_∞ = ambient temperature [K]

L = the projected vertical height of the receiver aperture [m]

An approximation for the average interior surface area of the cavity is given by:

$$\bar{T}_w = \frac{T_h A_h + T_c A_c}{A_{total}} \quad (43)$$

where:

T_h = average operating temperature of the system [°C]

T_c = average refractory surface temperature in the cavity [°C]

$T_c = T_h - 56^\circ\text{C}$

A_h = heated surface area in the cavity [m²]

A_c = refractory surface area in the cavity [m²]

The 1/3 exponent on the Grashof number results in a heat transfer coefficient that is independent of cavity dimensions. All fluid properties are evaluated at T_∞ . The natural convective heat transfer coefficient is given by:

$$h_{nc,o} = 0.81 (\bar{T}_w - T_\infty)^{0.426} \quad (44)$$

where:

h_{nc} = natural convection

[λ_0] = no lip heat transfer coefficient

The convective heat loss energy is given by:

$$Q_{\text{conv}} = \bar{h}_{\text{nc,o}} A (\bar{T}_w - T_{\infty}) \quad (45)$$

where:

A = the total interior surface area of the cavity receiver [m^2]

$\bar{T}_w$ = the average receiver heated surface temperature [$^{\circ}\text{C}$]

Siebers and Kraabel account for aperture effects by multiplying the natural convective heat transfer coefficient by an area ratio factor. The natural convective heat transfer coefficient including the effects of the aperture lip is given by:

$$\bar{h}_{\text{nc}} = h_{\text{nc,o}} \left[\frac{A_1}{A_2} \right] \left[\frac{A_3}{A_1} \right]^n \quad (46)$$

where:

$n = 0.63$ for $0^{\circ} \leq \phi \leq 30^{\circ}$

$n = 0.8$ for $30^{\circ} \leq \phi \leq 90^{\circ}$

A_1 = total interior cavity surface area [m^2](Fig. 27)

A_3 = interior cavity surface area below the horizontal plane [m^2] (Fig. 27)

A_2 = A_1 minus the area of the lower lip [m^2] (Fig. 27)

Figure 27. Siebers and Kraabel cavity areas

The refractory surfaces are assumed to be 56°C cooler than the mean operating temperature of the receiver. The formulas for areas A1 and A2 are given as follows:

$$A_1 = \pi(R_e + R_c)\sqrt{L_f^2 + (R_c - R_e)^2} + 2\pi R_c L_h + \pi R_c^2 + \pi(R_c^2 - R_a^2) + 2\pi R_c L_c \quad (47)$$

$$A_2 = A_1 - R_c^2 \cos^{-1} \frac{R_a}{R_c} + R_a \sqrt{(R_c^2 - R_a^2)} \quad (48)$$

The formula for A3 depends on the particular receiver angle. The expressions developed for the variation of the cavity internal zone areas as a function of receiver angle can be found in Appendix 7.

The Grashof number is given by:

$$Gr_L = g \beta (\bar{T}_w - T_\infty) \frac{L^3}{\nu^2} \quad (49)$$

where:

g = gravitational constant, 9.81 m/s^2

L = cavity diameter [m]

ν = kinematic viscosity [m^2/s]

β = coefficient of volumetric expansion [K^{-1}]

The uncertainty analysis provided by Siebers and Kraabel is presented in Table 2.

Table 2
Siebers and Kraabel Uncertainty Analysis

<u>Parameters</u>	<u>Uncertainty</u>
A_1	$\pm 10\%$
A_2	$\pm 10\%$
A_3	$\pm 10\%$
A_{ap}	$\pm 5\%$
T_w	$\pm 10\%$
T_∞	$\pm 2\%$
natural convection correlation	$\pm 20\%$

A computer program was used to solve for the Siebers and Kraabel convective heat loss for various aperture diameters, receiver operating temperatures, and receiver angle. A listing of the computer program is in Appendix 10. The results of the convective heat loss analysis using the Siebers and Kraabel model are presented in Appendix 11. The Siebers and Kraabel predictions for the receiver convective heat loss variation with receiver angle are presented in Figure 28.

Figure 28. Convective heat loss for the Siebers and Kraabel model

VII COMPARISON OF CAVITY HEAT LOSS MODELS

With increasing aperture diameter there is a decrease in convective heat loss (Fig. 13 & 14).

The effect of receiver angle on the convective heat loss is more pronounced on larger aperture diameters.

The conduction heat loss forms approximately 65% of the total heat loss for all operating temperatures when the aperture diameter is small and the receiver is placed at a typical operating angle of 45° (Fig. 21).

The percent conduction is reduced and the percent radiative increased with increases in the aperture . With an aperture greater than 12 inches, the percent conduction of the total heat

loss is constant at about 38%. With the 6 inch diameter the percent conduction of the total heat loss is reduced to 25%.

Of primary interest is how well the various models compare with the experimental results. Of the six models examined, only the LeQuere, Penot and Mirenayat model provides for negative receiver angles.

A. Comparison of Previous Models with Experimental Data

The convective heat loss values predicted by the LeQuere, Penot and Mirenayat model are compared with the experimental results of Phase One and Phase Two (Fig. 29). For an ideal correlation, all the data points would fall on the equal value line. An ideal correlation occurs when the predicted results equal the experimental results. All the convective heat loss values predicted by the LeQuere, Penot and Mirenayat model are lower than the experimental results. The large degree of data scattering for higher heat loss values makes it difficult to apply a simple correction factor to the model.

The Koenig and Marvin model for convective heat loss demonstrates more agreement with experimental result than the LeQuere, Penot and Mirenayat model (Fig. 30). The Koenig and Marvin model yields higher convective heat loss values, as compared to the experimental results. The data shows increasing scatter for higher heat loss values. The model only works for positive receiver angles.

Figure 29. LeQuere, Penot, Mirenayat Convective Heat Loss Model Correlation

Figure 30. Koenig and Marvin Convective Heat Loss Model Correlation

The Clausen model provides the best fit of all the previous models examined (Fig. 31). This model predicts only heat loss values for positive receiver angles. The Clausen model is considerably more complicated than any of the other models. The Clausen model overestimates the convective heat loss for lower heat loss conditions and underestimates the convective heat loss for higher heat loss conditions.

Figure 31. Clausing Convective Heat Loss Model Correlation

Figure 32. Siebers and Kraabel Convective Heat Loss Model Correlation

The Siebers and Kraabel model over estimates the convective heat loss as compared with the experimental results (Fig. 32). This model also shows considerable scatter for all heat loss conditions.

B. Stine and McDonald Correlation

The Stine and McDonald model is an extension of the Siebers and Kraabel model to include the effects of varying receiver aperture size and receiver angle ⁽⁸⁾. The complex set of area determinations are not used in the Stine and McDonald model. The Stine and McDonald correlation for the Nusselt number is given as follows:

$$Nu_L = 0.088 Gr_L^{\frac{1}{3}} \left(\frac{T_w}{T_\infty} \right)^{0.18} (\cos \phi)^{2.47} \left(\frac{d}{L} \right)^s \quad (50)$$

and

$$s = 1.12 - 0.98 \left(\frac{d}{L} \right) \quad (51)$$

where:

d = aperture diameter [m]

Gr_L = Grashof number based on length L

L = average internal dimension of cavity [m]

Nu_L = Nusselt number based on length L

T_∞ = ambient temperature [K]

T_w = average internal wall temperature [K]

f = tilt angle of cavity

($f = 90^\circ$ is aperture-down, $f = 0^\circ$ is aperture-sideways)

The aspect ratio term, d/L , accounts for the combined effects of internal surface area and aperture flow area. The effect of the receiver aspect diminishes with increase in aperture size, with the exponent 's'. The Stine and McDonald model predictions compare well with experimental results (Fig. 33). This model can only be applied for positive receiver angles.

Figure 33. Stine and McDonald Convective Heat Loss Model Correlation

The computer program used to generate the Stine and McDonald convective heat loss values is provided in Appendix 12. The data output from the program is presented in Appendix 13.

VIII. ANALYTICAL RADIATIVE HEAT LOSS

In this section the equations used to predict the thermal radiative heat loss through the aperture of the cavity solar receiver are developed. The receiver cavity surfaces are assumed to radiate as gray bodies. The internal geometry is simplified to aid in the formulation of the shape factor expressions.

A. Internal Geometry

The internal receiver surfaces were divided into five main sections (Fig. 34). The sections are defined as either hot or cold. The hot sections were those whose walls were formed by the heat transfer tubing. The hot sections were divided into an integer number of flat, concentric, isothermal bands. The number of bands in each section was determined by the number of turns the heat transfer tubing made in that section. The frustum section has 23 bands and the hot cylindrical section has 15 bands. The width of each band is equal to the surface length of each section divided by the number of bands in each section. The actual spacing between adjacent tubes was not considered significant.

Figure 34. Receiver internal surface sections.

1. Nomenclature

The following list defines the nomenclature used in the thermal radiative heat loss formulas.

- r_e = end plate radius [12.7 cm]
- r_c = cavity radius [33.0 cm]
- r_a = aperture radius [7.6, 15.2, 22.9, 33.0 cm]
- l_c = length of frustum section [29.2 cm]
- l_m = length of hot cylindrical section [25.4 cm]
- l_a = length of cold cylindrical section [14.0 cm]
- l_b = width of hot isothermal bands [1.7 cm]

N_c = number of bands in frustum section (23)

N_m = number of bands in hot cylindrical section (15)

$$l_c \equiv [(l_b N_c)^2 - (r_c - r_e)^2]^{1/2} \quad (54)$$

B. Assumptions

A number of assumptions are necessary to simplify the thermal radiative heat loss calculations. The assumptions made for this analysis are listed as follows:

1. Each band is isothermal based on a linear interpolation between the inlet temperature at the narrow end of the frustum section to the outlet temperature at the bottom end of the hot cylindrical section.
2. Each band is considered as a flat surface.
3. Each tube band is diffuse and gray with emissivity, $\epsilon = 0.85$.
4. The incident and reflected energy flux is uniform over each area.
5. Each band is adjacent to the next (i.e., no gaps between bands).
6. Each refractory surface has an emissivity of 0.70.

C. Shape Factors

All formulas are developed from the basic disc-to-disc shape factor formula.⁽²⁰⁾ The N by N coefficient matrix of the surface energy balance equation (Eqn. 64) requires N^2 shape factors. The equations are solved using a digital computer. Equation 64 is conservation of energy from all the surfaces. Shape factors describe the geometric relationship between surfaces. The derivation of the shape factor formulas used in the coefficient matrix are presented in Appendix 14.

D. Thermal Radiative Heat Loss Equations

The general equation for thermal radiative heat loss from the receiver through the aperture for internal black body surfaces is given by:

$$Q_a = -\sigma T_e^4 A_e F_{A_e - A_a} - \sigma T_s^4 A_s F_{A_s - A_a} - \sigma A_{n_m} \sum_{n_m=1}^{N_m} T_{n_m}^4 F_{n_m - A_a} - \sigma \sum_{n_c=1}^{N_c} T_{n_c}^4 A_{n_c} F_{n_c - A_a}$$

where:

[]_s = annuls

[]_e = end plate

[]_a = aperture

[]_{nm} cylindrical section

[]_{nc} = frustum section

As the aperture size to cavity volume ratio decreases, the radiative characteristics of the receiver cavity approach those of a black body emitter. To account for the various aperture sizes studied, the diffuse gray surface formulas were used. Using the net radiative method, the radiative heat loss for a cavity with diffuse gray surfaces is given by:

$$Q_k = q_k A_k = (q_{o,k} - q_{i,k}) A_k \quad (56)$$

$$q_{o,k} = \epsilon_k \sigma T_k^4 + \rho_k q_{i,k} \quad (57)$$

$$q_{o,k} = \epsilon_k \sigma T_k^4 + (1 - \epsilon_k) q_{i,k} \quad (58)$$

where:

q_o is the outgoing radiant energy flux (radiosity) [W/m²]

q_i is the incoming radiant energy flux [W/m²]

For the aperture:

$$q_{o, \text{opening}} = 0$$

$$T_{\text{opening}} = 0$$

$$\epsilon_{\text{opening}} = 1$$

For the cavity:

$$\sum_{j=1}^N [\delta_{kj} - (1 - \epsilon_k) F_{k-j}] q_{o,j} = \epsilon_k \sigma T_k^4 \quad (59)$$

where

N = total number of surfaces

F_{k-j} = shape factor for surface k to surface j

δ_{kj} = Kronecker delta

$$\delta_{kj} = \begin{cases} 1 & \text{when } k = j \\ 0 & \text{when } k \neq j \end{cases}$$

therefore:

$$Q_k = A_k \frac{\epsilon_k}{(1 - \epsilon_k)} (\sigma T_k^4 - q_{o,k}) \quad (60)$$

and

$$q_{i,k} = \sum_{j=1}^N F_{k-j} q_{o,j} \quad (61)$$

letting

$$a_{kj} = \delta_{kj} - (1 - \epsilon_k) F_{k-j} \quad (62)$$

and

$$C_k = \epsilon_k \sigma T_k^4 \quad (63)$$

then

$$\begin{bmatrix} a_{11} & \dots & a_{1j} & \dots & a_{1N} \\ a_{k1} & \dots & a_{kj} & \dots & a_{kN} \\ a_{N1} & \dots & a_{Nj} & \dots & a_{NN} \end{bmatrix} \begin{bmatrix} q_{o,1} \\ q_{o,k} \\ q_{o,N} \end{bmatrix} = \begin{bmatrix} C_1 \\ C_k \\ C_N \end{bmatrix} \quad (64)$$

The solutions for $q_{o,k}$ are accomplished using a BASIC computer language program (Appendix 15). The heated surfaces are assumed to have an emissivity of 0.85 based on the paint coating specifications. The refractory surfaces are assumed to have a emissivity of 0.70.

E. Assumed Cavity Temperature Distribution

The axial temperature distribution along the heating surface sections is assumed to vary linearly from the top of the frustum section to the bottom of the cylindrical section. The temperature of the top band of the frustum section is equal to the receiver inlet temperature. The temperature of the bottom band of the cylindrical section is equal to the receiver outlet temperature. The inlet and outlet temperature values used in the computer program are assumed to be plus and minus 7.5°F of the operating temperature, respectively.

Table 3
Inlet and Outlet temperatures

Test Phase	Aperture Diameter [in]	Inlet [°F]	Outlet [°F]
1	18	297.7	289.0
1	18	402.4	389.6
1	18	515.6	497.1
1	18	603.9	581.3
2	6	395.2	389.9
2	6	609.3	595.9
2	12	429.4	419.1
2	12	611.3	592.9
2	18	429.3	415.7
2	18	600.3	576.2
2	26*	414.3	399.5
2	26*	602.6	570.4

* There is no annulus therefore the aperture diameter is equal to the cavity diameter.

F. Comparison with Measurements

The radiometer and the analytical methods are compared with the experimental method, $Q_{\text{unplugged}}$ minus Q_{plugged} , for determining the radiative heat loss from the cavity through the aperture. The experimentally determined radiative heat loss was the difference between the open and plugged total receiver heat loss when the receiver aperture was down. A correction was made to account for the heat loss through the aperture plug. The heat loss through the plug must be added to the experimentally determined radiative heat loss data to get the total radiative heat loss from the receiver. The conductive heat loss through the plug is given by:

$$Q_{\text{plug}} = \frac{k_{\text{plug}} \Delta T A_{\text{plug}}}{\Delta x} \quad (65)$$

where:

k_{plug} = thermal conductivity of the plug[W/m-K]

ΔT = temperature difference between the inner and outer surface[K]

A_{plug} = mean surface area of the plug[m]

Δx = distance over which ΔT occurs (the thickness of the plug)[m]

The plugs were fabricated from one inch thick Cera Form[®] boards. The boards have a mean thermal conductivity of 0.32 Btu-in/hr-sq. ft.- $\Delta^\circ\text{F}$ (0.0462 W/m-K).

Log-log scales are used to provide linear constant percent difference lines.

1. Radiometer Method

The radiometer determined heat loss values compared well with the experimentally determined radiative heat loss, $Q_{\text{unplugged}}$ minus Q_{plugged} , with differences within $\pm 20\%$ (Fig. 35).

Figure 35. Experimentally determined radiometer method correlation

2. Analytical Method

The analytical method (Fig. 36) did not compare well with the experimental method for determining the radiative heat loss from the receiver. A number of possible reasons for the discrepancies have been discussed previously.

Figure 36. Analytically determined radiative correlation

IX. INSTRUMENTATION CALIBRATION

A. Flow Meter Calibration

The flow measurement apparatus consists of three basic parts: the turbine flow meter, the inductive pick-off, and the pulse rate counter (Fig. 37). The turbine flow meter rotates at a specific rate for a given fluid type and volumetric fluid flow rate. The rate of rotation is linearly proportional to the fluid flow rate within the specified range. The flow meter must

be calibrated for a specific fluid viscosity, temperature, and flow rate range for accurate measurement.

The inductive pick-off is positioned above the turbine flow meter. When a turbine blade passes the inductive pick-off, an electromagnetically induced pulse signal is sent to the pulse rate converter (PRC). The PRC changes the pulse rate signal to voltage or current outputs. The current or voltage signal is then read by the data acquisition computer. The voltage signal should be used when the distance from the PRC to the computer input terminal is less than ten feet. For distances greater than ten feet the current signal should be used, as long leads result in substantial voltage drops. Voltage drops may significantly skew the voltage signal. The current signal is not affected by the voltage drop. The current signal requires a precision resistor across the computer input terminals. The resistor effectively converts the current signal to a voltage input at the computer terminals. Since precision resistors are expensive, economy requires the voltage signal should be used whenever possible.

Voltage signal output was used during testing for the reasons stated above. The computer displays the equivalent fluid volumetric flow rate based on the voltage input. The slope and offset values of the flow rate versus voltage linear function were inputted into the computer.

Figure 37. Flow measurement system

The heat transfer fluid flow rate is measured with three turbine type flow meters in series. Three flow meters are used for measurement redundancy. One of these flow meters was factory calibrated. The factory calibration specifications sheet is Appendix 16. The calibration curve for the factory calibrated flow meter is presented in Figure 38. The equation of the volumetric flow rate as a function of flow meter output frequency for the factory calibrated flow meter is:

$$\dot{v} = 0.0039578 + 0.001489f \quad (65)$$

where:

f = is the flow meter output frequency [Hz]

$\dot{v}$ = volumetric flow rate [gpm]

Figure 38. Factory calibrated flow meter flow rate versus frequency output

The pulse rate converters (PRCs) were calibrated in-house according to the manufacturer's procedure ⁽¹³⁾. The calibration points for the PRC used with the factory calibrated flow meter are presented in Table 4.

Table 4
Pulse Rate Converter Calibration Points

frequency [Hz]	output voltage [volts]
1600	8.0
2000	10.0

The linear relationship for the frequency as a function of output voltage, as determined by the calibration points, is given as:

$$f = 200 E \quad (66)$$

where:

f = is the frequency input to the PRC [Hz]

E = is the output signal from the PRC [volts]

Substituting the frequency equation of the PRC calibration into the flow rate equation of the factory calibrated flow meter yields an expression for the volumetric flow rate as a function of voltage as follows:

$$\dot{v} = 0.0039578 + 0.001489(200 E) \quad (67)$$

which reduces to:

$$\dot{v} = 0.0039578 + 0.2978E \quad (68)$$

which can be approximated as:

$$\dot{v} = 0.2978E \quad (69)$$

Because $E > 3.36$ volts at typical flow rates the error due to this approximation is less than:

$$\frac{0.0039578}{(0.2978)(3.36)}$$

The remaining two flow meters were calibrated against the factory calibrated flow meter.

Three meters were used for redundancy in the event one meter fails during testing.

1. Flow Meters Calibration

The outputs from the three flow meters were compared for various flow rates. The voltage outputs of the three flow meters were recorded (Appendix 17) (Fig. 39). The heat transfer fluid temperature was maintained at 300°F. Corrective slope and offset values were determined for each of the two uncalibrated flow meters. Applying the linear corrections

will bring the two uncalibrated flow meter voltage outputs into agreement with the factory calibrated flow meter output.

Figure 39. In-house calibrated flow meters correlation curves

The difference between the corrected readings and the factory calibrated readings are compared (Fig. 40). The minimum flow rate for all testing never went below one gallon per minute or 3.36 volts. This flow rate is well within the manufacture specified flow range. The maximum difference between the backup flow meters and the factory calibrated flow meter is ± 0.15 volts or ± 0.045 gallons per minute. Temperature effects are negligible ⁽¹⁴⁾.

Figure 40. In-house calibrated flow meters errors.

Substituting the linear correction expression for the in-house calibrated flow meters into the volumetric flow rate expression of the factory calibrated flow meter yields expressions for the volumetric flow rates as a function of voltage inputs to the computer. The resulting expressions are given as follows:

$$\dot{V}_{\text{flow 1}} = 0.2978(-2.9070 + 2.9616E_{\text{flow 1}}) \quad (70)$$

$$\dot{V}_{\text{flow 2}} = 0.2978(-3.2878 + 3.1808E_{\text{flow 2}}) \quad (71)$$

which reduce to:

$$\dot{V}_{\text{flow 1}} = -0.8657 + 0.88196E_{\text{flow 1}} \quad (72)$$

$$\dot{V}_{\text{flow 2}} = -0.9791 + 0.94724E_{\text{flow 2}} \quad (73)$$

The scale and offset values from these expressions were inputted into the computer. The computer then displays the flow rate for each flow meter in gallons per minute (gpm).

B. Thermocouple Calibration

The total receiver heat loss, Q_T , was given by the product of the mass flow rate, the specific heat of the heat transfer fluid and the temperature difference between the fluid inlet and outlet temperatures (ΔT). Of the three variables, the largest error in the heat loss was due to the measurement of ΔT . Two redundant methods were used to measure ΔT for these experiments. One method of determining ΔT was by subtracting the fluid outlet temperature from the fluid inlet temperature. The other method utilized a direct temperature difference measurement from two thermocouples, one in each of the fluid inlet and outlet lines. This differential thermocouple connection avoids inaccuracies due to reference junction compensation but still requires knowledge of the absolute temperature values. To reduce the error introduced to the total heat loss calculation by the thermocouple readings it was necessary to calibrate the inlet, outlet, and delta temperature thermocouples used in the receiver. Standard thermocouple probes have a maximum error of $\pm 2.2^\circ\text{C}$ or 0.75%, whichever is greater ⁽¹⁵⁾. Using two absolute temperature measurements from standard thermocouple probes would result in a ΔT error of $\pm 3.11^\circ\text{C}$ ($\pm 5.60^\circ\text{F}$) or 1.06% whichever is greater. With temperature differences as low as 2.78°C (5°F) recorded, the standard thermocouples did not yield values within an acceptable error.

A single factory calibrated K-type thermocouple probe was purchased and all other probes were calibrated against it. Only one calibrated probe could be purchased due to budget constraints. The calibrated probe has an accuracy of $\pm 0.2^\circ\text{F}$ after linear correction is applied (Fig. 41). The three point calibration data for the factory calibrated thermocouple is provided in Table 7. The calibration is certified traceable to the U.S. National Bureau of Standards (Appendix 18).

Figure 41 Calibrated thermocouple probe curve

A linear variation of the actual temperature as a function of the indicated temperature is given by:

$$T_{\text{actual}} = -2.4256 + 1.006T_{\text{indicated}} \quad (74)$$

with a correlation coefficient, $R=1.00$

Table 5 shows the error in the calibrated probe after linear correction is applied.

Table 5
Factory Calibrated thermocouple probe error

Indicated Temperature [°F]	Actual Temperature [°F]	Corrected Temperature [°F]	Absolute Error [°F]
300.56	300.06	299.94	0.12
499.39	499.77	499.96	0.19
699.09	701.00	700.86	0.14

1. Thermocouple Calibration Apparatus

A thermocouple calibrating device was fabricated (Fig. 42). The calibrator consisted of a heat source, a heat sink, and an insulated cover. The heat sink was formed from a solid brass cylinder with three holes drilled in one end to accommodate thermocouple probes and a single hole in the other end to accommodate the heat source (Fig. 43). The soldering iron used was an Ungar CI-45, 0.38 A 120 V AC/DC. The soldering iron tip was modified for a snug fit in the heat sink (Fig. 44). The soldering iron was connected to a variable AC power supply. The brass block was insulated to control the rate of heat loss. The thermocouple leads were connected to a data acquisition system.

Figure 42. Thermocouple calibrator

Figure 43. Thermocouple calibrator heat sink

Figure 44. Modified soldering iron heat source

2. Thermocouple Calibration Procedure

Three separate tests were required to accomplish calibration of the two absolute and the two differential thermocouples. In the first test, the absolute inlet and outlet TC probes were inserted in the heat sink along with the calibrated TC probe. The heat source was plugged into a variable AC power supply. The variable AC supply was adjusted until a maximum temperature of approximately 700°F was indicated for the calibrated TC. The power supply was then removed and the system allowed to cool slowly. The temperature time histories for the absolute temperature inlet and outlet thermocouples were recorded. The heat sink was assumed to be isothermal at all TC junctions for any time. Correction factors for the TC's were obtained by comparing the TC outputs to that of the calibrated TC output.

3. Thermocouple Calibration Results

The temperature time history curves for the absolute temperature inlet and outlet thermocouples are presented in Figure 45. The relationship for the inlet thermocouple is quite linear as indicated in Fig. 46. The linear relationship between the inlet TC reading and the calibrated TC reading is given by;

$$T_{cal} = -.2217 + 1.0027 T_{in} \quad (75)$$

The relationship for the outlet thermocouple is quite linear as indicated in Fig. 47. The linear relationship between the outlet TC reading and the calibrated TC reading is given by;

$$T_{cal} = -.1850 + 1.0047 T_{out} \quad (76)$$

Figure 45. Inlet and Outlet thermocouples calibration histories

Figure 46. Factory Calibrated versus inlet thermocouple readings

Figure 47. Factory Calibrated versus outlet thermocouple readings

These equations are used to correct the outlet TC readings to the calibrated TC readings. The difference between the calibrated and inlet TC readings are compared before and after the linearized correction factors were applied (Fig. 48). The maximum difference between the calibrated TC reading and the inlet TC reading before the correction is applied is 2.6°F. After application of the correction factors the maximum difference is 1.02°F. The maximum difference between the calibrated TC readings and the outlet TC readings before the linear correction is applied is 4.2 °F. After the linear correction is applied the maximum difference is 1.44°F (Fig. 49).

Figure 48. Inlet thermocouple errors

Figure 49. Outlet thermocouple errors

Two thermocouples can be arranged to provide a voltage output proportional to the temperature difference of the two junctions (Fig. 50). When both thermocouple junctions are at the same temperature the voltage output is zero.

Figure 50. Differential thermocouple connection

The two thermocouple probes used for the direct temperature difference measurement were inserted in the thermocouple calibrator along with the calibrated thermocouple. The unit was then heated and cooled as per the procedure used for calibrating the inlet and outlet absolute temperature thermocouple probes. Ideally, the net voltage output from the temperature differential connection should be zero regardless of the calibrator temperature. The temperature and micro volt output histories for the calibration procedure are presented in Figure 51. Comparing the differential thermocouple's output with the calibrated thermocouple reading indicates no linear correlation (Fig. 52). The step function of the voltage output is an indication of the minimum computer analog to digital converter (ADC) resolution.

The maximum error in the differential voltage output is $25.45 \mu\text{V}$ which corresponds to a temperature difference error of 1.147°F .

Figure 51. Differential thermocouple readings history

Figure 52. Differential thermocouple errors history

The absolute mean temperature must also be known to convert the millivolt output of the differential thermocouples into an equivalent temperature difference. The voltage to temperature difference conversion factor is determined from a polynomial function of the mean temperature (Fig. 53). The conversion factor polynomial was derived from the voltage-temperature tables for K-type thermocouples.⁽¹⁴⁾

No calibration of the differential thermocouples was performed with a difference in temperature at the junctions.

Figure 53. Differential thermocouple output versus mean temperature

C. Radiometer Calibration

The Hy-Cal[®] Hy-Therm[®] Pyrheliometer P-8400-B was used to measure the thermal radiative heat loss from the receiver cavity (Fig. 54). The spectral range of the radiometer without its quartz window is from 0.2 to 30 microns. The radiometer consists of a thermopile on top of a heat sink. The thermopile converts the temperature gradient across the pile to a proportional current signal. The heat sink is water cooled aluminum base. The exposed end of the thermopile is coated with fused colloidal graphite providing a minimum absorptivity of 0.9. The radiometer outputs 5 mV per solar constant (0.13980 Watts/cm²). The calibration specifications are provided in Appendix 19.

The radiometer was supplied with a bezel mounted quartz window. Because the radiative being measured is in the infra-red wave length region, preliminary testing showed that the

quartz window excessively attenuated the heat flux to the radiometer resulting in an insufficient signal output. When the window was removed, the radiometer became overly sensitive to localized convective heating and cooling which resulted in a fluctuating output signal. For low heat flux level measurements, a window that is virtually transparent to the infrared radiative is desirable. Various window materials were considered and tested for replacement of the quartz window.

Figure 54. Radiometer section view

1. Radiometer Window Evaluations

A bezel was fabricated to accommodate various film windows for testing (Fig. 55). The film was pulled snugly over the bezel. The film was secured in place with a rubber band. The bezel fits over the radiometer. The film window is close enough to the thermopile wafer providing the thermopile with almost 180° of view.

Figure 55. Film window bezel

The test stand consisted of an inverted hot plate positioned concentrically above and facing the radiometer (Fig. 56). A K-type thermocouple probe is immersed in the coolant return catch basin for the radiometer. The base of the radiometer is assumed to be at the same temperature as the water in the catch basin. The hot plate is inverted and positioned above the radiometer to prevent convective heating of the radiometer. The hot plate temperature is controlled using a variable AC power supply. The radiometer can be positioned at various vertical distances from the hot plate. The surface of the hot plate has nine K-type thermocouples welded to it.

Figure 56. Radiometer calibration test stand

The hot plate surface was coated with high emissivity Pyromark[®] paint. The manufacturer's specifications for the Pyromark[®] paint are provided in Appendix 20. The average black-body normal emittance of the painted surface is a function of the surface temperature and can be as low as 0.867 at 600K (Fig. 57). A fifth order polynomial curve fit provides an equation for paint surface emittance as a function of surface temperature.

Figure 57. Pyromark paint emittance

The parameters for the window evaluation test plan are shown in Table 6. At the beginning and end of each test, background measurements were recorded by removing the radiometer from the test stand and placing it above the hot plate on an insulated pad. For each of the plate and background thermal radiative measurements the readings were recorded after a two minute stabilization period. The variable AC power supply was adjusted until the average plate temperature was close to the target temperature. The thermocouples were distributed over the plate surface (Fig. 58).

Table 6
Radiometer window test parameters

Test Window	Target Temperature	Vertical Displacement
Saran Wrap	300°F	0.32r
quartz	"	"
Glad Wrap	"	"
none	"	"
Saran Wrap	400°F	0.75r
quartz	"	"
Glad Wrap	"	"
none	"	"
Saran Wrap	500°F	1.23r
quartz	"	"
Glad Wrap	"	"
none	"	"
Saran Wrap	600°F	1.80r
quartz	"	"
Glad Wrap	"	"
none	"	"
Saran Wrap	700°F	2.5r
quartz	"	"
Glad Wrap	"	"
none	"	"

where r = radius of the hot plate

Figure 58. Hot plate thermocouple distribution

For an average area temperature only thermocouples five through nine were considered.

The average area temperature is given by:

$$T_{\text{average}} = \frac{T_5 + T_6 + T_7 + T_8 + T_9}{5} \quad (77)$$

The window transmittance, τ_{window} , is given by:

$$\tau_{\text{window}} = \frac{q_{\text{radio}}}{q_{\text{radio/plate}}} \quad (78)$$

where

q_{radio} = the thermal radiative heat flux read by the radiometer

$q_{\text{plate/radio}}$ = the thermal radiative heat flux incident on the radiometer from the hot plate

The radiative leaving the hot plate and incident on the radiometer is given by:

$$q_{\text{radio/plate}} = q_{\text{plate}} F_{\text{plate-radio}} \quad (79)$$

where

q_{plate} = the thermal radiative heat flux leaving the hot plate

$F_{\text{plate-radio}}$ = the shape factor from the hot plate to the radiometer

The radiative heat flux leaving the hot plate is given by:

$$q_{\text{plate}} = \sigma \epsilon (\bar{T}_{\text{plate}}^4 - T_{\text{ambient}}^4) \pi r_{\text{plate}}^2 \quad (80)$$

where

$\beta = 5.729 \times 10^{-8} \text{ [W/(m}^2 \cdot \text{K}^4)]$ Stefan-Boltzmann constant

$r_{\text{plate}} = 8.9 \text{ [cm]}$ the radius of the hot plate

ϵ = emissivity of the plate surface.

The shape factor from the hot plate to the radiometer is given by:

$$F_{\text{plate-radio}} = \frac{1}{2} \left\{ 1 + \frac{h^2 + r_{\text{radio}}^2}{r_{\text{plate}}^2} - \sqrt{\left[1 + \frac{h^2 + r_{\text{radio}}^2}{r_{\text{plate}}^2} \right]^2 - 4 \left[\frac{r_{\text{radio}}}{r_{\text{plate}}} \right]^2} \right\} \quad (81)$$

where

h = vertical displacement of the hot plate and radiometer.

r_{radio} = radius of the radiometer = 0.5625 [in.]

When the diameter of the radiometer approaches one inch, as is the case here, a simplified formula may be used. The simplified shape factor formula is given as follows:

$$F_{\text{plate-radio}} = \frac{r_{\text{radio}}^2}{h^2 + r_{\text{plate}}^2} \quad (82)$$

All real gas effects have been ignored (absorption, scattering etc.).

The results of the test are in Appendix 21. The quartz window transmittance varies linearly with source temperature (Fig. 59). The transmittance for the Grad Wrap and Saran Wrap windows are nearly constant over the testing temperature range. The average transmittance for the no window condition is 0.99. Ideally, the transmittance for the no window

condition should be unity. The error in the no window transmittance is well within the instrument's error. Real gas effects may also account for a small loss in the incident flux on the radiometer from the hot plate.

Figure 59. Radiometer windows transmittance

The average transmittance for the Saran Wrap window was determined to be 0.87. The manufacturer specifies a transmittance of 0.88 for the infrared portion of the spectrum. Technical information for Saran Wrap® films is provided in Appendix 22. Although the Glad Wrap had similar transmission characteristics, the Saran Wrap was selected as the radiometer window, since no manufacturer specifications were available for the Glad Wrap. In addition to selecting a radiometer window, it was also necessary to determine effects of radiometer positioning relative to the heat source.

2. Radiometer Positioning

The radiometer positioning sensitivity must be considered for accurate heat flux measurements. The parameters for the radiometer positioning sensitivity test plan are presented in Table 7. At the end of each test the background measurements were taken by removing the radiometer from the test stand and placing it above the hot plate on an insulated pad. For each of the plate and background thermal radiative measurements the radiometer readings were recorded after a two minute stabilization period.

Table 7
Radiometer position sensitivity test parameters

Hot Plate Temp	Offset Distance	Vertical Displacement
400°F	0 to 2r step 0.5r	0.75r
700°F	0 to 6r step 1r	2.5r
400°F	0	1 to 6r step 1r
700°F	0	2 to 12r step 2r

where r = radius of the hot plate

The shape factor from the hot plate to the radiometer is given by:

$$F_{\text{plate-radio}} = \frac{1}{2} \left(1 - \frac{1 + \left(\frac{h}{a}\right)^2 - \left(\frac{r_{\text{plate}}}{a}\right)^2}{\sqrt{\left[1 + \left(\frac{h}{a}\right)^2 - \left(\frac{r_{\text{plate}}}{a}\right)^2\right]^2 - 4\left[\frac{r_{\text{plate}}}{a}\right]^2}} \right) \left(\frac{r_{\text{radio}}}{r_{\text{plate}}} \right)^2 \quad (83)$$

where

h = vertical displacement of the hot plate and radiometer.

r_{radio} = radius of the radiometer = 1.43 cm

r_{plate} = radius of the hot plate = 8.9 cm

h = vertical displacement [in.]

a = horizontal displacement [in.]

The results of the displacement sensitivity test are tabled in Appendix 23. The effects of vertical and horizontal displacement of the radiometer from the heat source are presented in Figure 60. Ideally, all values should be equal to one. The radiometer is especially sensitive to horizontal displacement (i.e. off axis readings).

Figure 60. Radiometer displacement effects

The results indicate that the radiometer should be placed as close as possible and in line

with the heat source. Extreme care was taken to assure the radiometer was centered on the receiver axis during the test phase. An elaborate string and plumb bob arrangement was used to center the radiometer.

X. ERROR ANALYSIS

This error analysis determines error in the results based on test method and instruments used. The error analysis also serves as one form of evaluating the test method. The error analysis does not account for human errors or systematic errors. The general form for the error analysis of a given function, z , where $z=z(x_i)$ is given as follows⁽¹⁶⁾:

$$\sigma_z = \sqrt{\sum_i \left[\left(\frac{\partial z}{\partial x_i} \right) \sigma_{x_i} \right]^2} \quad (84)$$

The general formula for the total heat lost from the cavity is given by:

$$Q_{\text{total}} = \rho \dot{v} c_p \Delta T. \quad (85)$$

The percent error in the total heat loss is given by:

$$\frac{\sigma_{Q_{\text{total}}}}{Q_{\text{total}}} = \sqrt{\left(\frac{\sigma_\rho}{\rho} \right)^2 + \left(\frac{\sigma_{\dot{v}}}{\dot{v}} \right)^2 + \left(\frac{\sigma_{c_p}}{c_p} \right)^2 + \left(\frac{\sigma_{\Delta T}}{\Delta T} \right)^2} \quad (86)$$

The density of the heat transfer fluid is a function of the temperature and is approximated by⁽¹⁷⁾:

$$\rho = 60.6 - 0.0324 T_{\text{inlet}} + 9.84\text{e-}6 T_{\text{inlet}}^2 - 1.79\text{e-}8 T_{\text{inlet}}^3 \text{ [lb/ft}^3\text{]} \quad (87)$$

The error in the heat transfer fluid density is approximated by:

$$\sigma_p = \sqrt{(-0.0324 + 1.968e-5 T_{inlet} - 5.37e-8 T_{inlet}^2)^2 \sigma_{T_{inlet}}^2} \quad (88)$$

The inlet temperature is used for density calculation. The inlet thermocouple used is the one closest to the flow meters.

The heat capacity of the heat transfer fluid is a function of the temperature and is approximated by⁽¹⁷⁾:

$$c_p = 0.3690 + 2.267e-4 T_{mean} \text{ [Btu/lb } ^\circ\text{F]} \quad (89)$$

The error in the heat transfer fluid heat capacity is approximated by:

$$\sigma_{c_p} = 2.267e-4 \sigma_{T_{mean}} \quad (90)$$

A. Flow Measurement Error Analysis

The HTF flow rate is given by:

$$\dot{v} = 0.2978E \quad (91)$$

where:

E = is the output signal from the pulse rate converter (PRC) [volts]

$\dot{v}$ = volumetric flow rate [gpm]

The manufacturer's specified linearity of the PRC is $\pm 0.4\%$ of full scale. The calibrated flow meter is accurate to within $\pm 0.5\%$ of the reading in the flow rate range of 0.8 to 2.5 gallons per minute and with a fluid viscosity in the range of 0.4 to 2.0 centistokes.⁽¹⁸⁾

The output of the PRC to the computer is from 0 to 10 volts. The accuracy of the computer for the 10 volt input range is the larger of $\pm 1\%$ of the reading or $\pm 0.2\%$ of the range (the range is 11 volts for the -1 to 10 volt input).⁽¹⁹⁾ The combined error for the factory calibrated flow meter reading is given by:

$$\sigma_{\text{flow}} = \sqrt{b^2 \sigma_E^2} \quad (92)$$

$$\sigma_E = \sqrt{(\sigma_{\text{PRC}})^2 + (\sigma_{\text{flow meter}})^2 + (\sigma_{\text{computer}})^2} \quad (93)$$

where:

b = the slope of the flow rate versus voltage output for the PRC-flow meter combination

b = 0.2978 [gpm/volt]

β_{PRC} = the error in the pulse rate converter

$\frac{\sigma_{\text{PRC}}}{E_{\text{scale PRC}}} = \pm 0.4\%$ of full scale

$E_{\text{scale PRC}} = 10$ volts

$\beta_{\text{flow meter}}$ = the error in the flow meter

$\frac{\sigma_{\text{flow meter}}}{E_{\text{reading}}} = 0.5\%$ of reading

β_{computer} = the error in the voltage signal ADC

$\frac{\sigma_{\text{computer}}}{E_{\text{reading or } E_{\text{scale computer}}}} = \pm 1.0\%$ of reading or $\pm 0.2\%$ of the range

$E_{\text{scale computer}} = 11$ volts (from -1 to + 10 volts)

The maximum error on flow rate measurement is 1.6 % or 0.0208 gpm.

B. Temperature Measurement Error Analysis

The accuracy of the computer must also be taken into consideration. The specified accuracy of the data acquisition system is given as $\pm 1.44^\circ\text{F}$ ($\pm 0.8^\circ\text{C}$) with a resolution of 0.18°F (0.1°C) for K-type thermocouples. The accuracy of the differential thermocouple connection is specified as $\pm 20\mu\text{V}$ for the $\pm 25\text{mV}$ range setting. This corresponds to a

temperature difference accuracy of $\pm 0.90^\circ\text{F}$ ($\pm 0.5^\circ\text{C}$). Calibration tests indicates an error of $\pm 25.45 \mu\text{V}$ which corresponds to a temperature difference error of $\pm 1.147^\circ\text{F}$.

The error of the temperature readings must include the combined effects of the error of the computer, calibrated probe, the absolute temperature probes, and the computer micro volt readings. The error of the absolute temperature thermocouples is given by:

$$\sigma_{T_{in}} = \sqrt{\sigma_{T_{in}/cal}^2 + \sigma_{cal}^2 + \sigma_{computer\ TC}^2} \quad (94)$$

and

$$\sigma_{T_{out}} = \sqrt{\sigma_{T_{out}/cal}^2 + \sigma_{cal}^2 + \sigma_{computer\ TC}^2} \quad (95)$$

where

$\sigma_{T_{in}/cal}$ = error of the inlet probe as compared with the calibrated probe.

$\sigma_{T_{in}/cal} = \pm 1.02^\circ\text{F}$

$\sigma_{T_{out}/cal}$ = error of the outlet probe as compared with the calibrated probe.

$\sigma_{T_{out}/cal} = \pm 1.44^\circ\text{F}$

$\sigma_{computer\ TC}$ = error of the computer ADC thermocouple channels.

$\sigma_{computer\ TC} = \pm 1.0^\circ\text{F}$

The mean temperature is required in converting the micro volt signal from the differential thermocouple connection to an equivalent temperature difference. The mean temperature is calculated from the absolute temperature readings of the inlet and outlet thermocouples as follows:

$$T_{mean} = \frac{T_{in} + T_{out}}{2} \quad (96)$$

The error in the mean temperature is given by:

$$\sigma_{T_{mean}} = \sqrt{\sigma_{T_{in}}^2 + \sigma_{T_{out}}^2} \quad (97)$$

The temperature difference from the differential thermocouple reading is given by:

$$\Delta T = \frac{\mu V}{k} \quad (98)$$

where k is the micro volt to temperature difference conversion factor.

The conversion factor, k , is a function of the mean temperature (Fig. 49). The error in the measured temperature difference is given by:

$$\sigma_{\Delta T} = \sqrt{\left(\frac{\partial \Delta T}{\partial \mu V} \sigma_{\mu V}\right)^2 + \left(\frac{\partial \Delta T}{\partial k} \sigma_k\right)^2} \quad (99)$$

which reduces to:

$$\sigma_{\Delta T} = \sqrt{\left(\frac{\sigma_{\mu V}}{k}\right)^2 + \left(\frac{\mu V}{k^2} \sigma_k\right)^2} \quad (100)$$

The error in the micro volt reading is dependent on the error in the differential thermocouple output as well as the error in the computer ADC. The error in the micro volt reading is given by:

$$\sigma_{\mu V} = \sqrt{\sigma_{\Delta T \mu V - cal}^2 + \sigma_{computer \mu V}^2} \quad (101)$$

where

$\sigma_{\Delta T \mu V - cal}$ = error in differential thermocouple as compared with the calibrated thermocouple.

$$\sigma_{\Delta T \mu V - cal} = \pm 25.45 \mu V$$

$\sigma_{computer \mu V}$ = error in the computer microvolt reading.

$$\sigma_{computer \mu V} = \pm 20 \mu V$$

The micro volt to temperature difference conversion factor, k , is determined from a ninth order polynomial of the mean temperature at the inlet and outlet junctions. The function for k is given as follows:

$$k = (m0) + (m1)T_{mean} + (m2)T_{mean}^2 + (m3)T_{mean}^3 + (m4)T_{mean}^4 + (m5)T_{mean}^5 + (m6)T_{mean}^6 + (m7)T_{mean}^7 + (m8)T_{mean}^8 + (m9)T_{mean}^9 \quad (102)$$

where

$$m0 = -5.9996574248$$

$$m1 = 0.57623140669$$

$$m2 = -0.0050328211032$$

$$m3 = 2.6366840630e^{-5}$$

$$m4 = -9.2911149803e-8$$

$$m5 = 2.2361762393e-10$$

$$m6 = -3.5624990721e-13$$

$$m7 = 3.5424764505e-16$$

$$m8 = -1.9716587450e-19$$

$$m9 = 4.6528339298e-23$$

The error in k is given by:

$$\sigma_k = \sqrt{\left(\frac{\partial k}{\partial T_{\text{mean}}} \sigma_{T_{\text{mean}}}\right)^2} \quad (103)$$

where:

$$\begin{aligned} \frac{\partial k}{\partial T_{\text{mean}}} = & (m1) + 2(m2)T_{\text{mean}} + 3(m3)T_{\text{mean}}^2 + 4(m4)T_{\text{mean}}^3 + 5(m5)T_{\text{mean}}^4 \\ & + 6(m6)T_{\text{mean}}^5 + 7(m7)T_{\text{mean}}^6 + 8(m8)T_{\text{mean}}^7 + 9(m9)T_{\text{mean}}^8 \end{aligned} \quad (104)$$

C. Normalization Error Analysis

The heat loss is normalized using the following formula:

$$Q_{\text{normalized}} = Q_{\text{measured}} \left(\frac{T_{\text{target}} - T_{\text{ambient standard}}}{T_{\text{measured}} - T_{\text{ambient measured}}} \right) \quad (105)$$

The percent error in the normalized heat loss is given by:

$$\frac{\sigma_{Q_{\text{normalized}}}}{Q_{\text{normalized}}} = \sqrt{\left(\frac{\sigma_{Q_{\text{measured}}}}{Q_{\text{measured}}}\right)^2 + \left(\frac{\sigma_N}{N}\right)^2} \quad (106)$$

where

$$N = \frac{T_{\text{target}} - T_{\text{ambient standard}}}{T_{\text{measured}} - T_{\text{ambient measured}}} \quad (107)$$

and

$$\frac{\sigma_N}{N} = \sqrt{\frac{\sigma_{T_{\text{mean}}}^2 + \sigma_{T_{\text{ambient measured}}}^2}{(T_{\text{mean}} - T_{\text{ambient measured}})^2}} \quad (108)$$

The convective heat loss is given by:

$$\frac{\sigma_N}{N} = \sqrt{\frac{\sigma_{T_{\text{mean}}}^2 + \sigma_{T_{\text{ambient measured}}}^2}{(T_{\text{mean}} - T_{\text{ambient measured}})^2}} \quad (109)$$

The error in the convective heat loss is given by:

$$Q_{\text{convective}} = Q_{\text{total}} - Q_{\text{total}90^\circ} \quad (110)$$

The conductive heat loss is given by:

$$Q_{\text{conductive}} = Q_{\text{total}90^\circ\text{plugged}} \quad (111)$$

The error in the conductive heat loss is given by:

$$\sigma_{Q_{\text{conductive}}} = \sigma_{Q_{\text{total}90^\circ\text{plugged}}} \quad (112)$$

The radiative heat loss is given by:

$$Q_{\text{radiative}} = Q_{\text{total}90^\circ\text{unplugged}} - Q_{\text{conductive}} \quad (113)$$

The error in the radiative heat loss is given by:

$$\sigma_{Q_{\text{radiative}}} = \sqrt{\sigma_{Q_{\text{total}90^\circ\text{unplugged}}}^2 + \sigma_{Q_{\text{conductive}}}^2} \quad (114)$$

The maximum error in the normalized total heat loss is 30.63%. This error occurs with the aperture plugged and the receiver in the +90° position (Fig. 61). The total heat loss with the aperture plugged is equivalent to the conductive heat loss.

Figure 61. Error in total heat loss for various operating temperatures

Figure 62. Error in total heat loss for various aperture diameter operating at 400°F

Figure 63. Error in total heat loss for various aperture diameter operating at 600°F

The errors in the convective and radiative heat losses are higher due to summation variables, each of which contains an error (Equations 110, 111, 113). The maximum error in the convective heat loss is 35.70%. The maximum convective heat loss error occurs at a receiver operating temperature of 400°F with a 6 inch aperture and the receiver in the +90° position (Fig. 64).

Figure 64. Error in convective heat loss for various operating temperatures

Figure 65. Error in convective heat loss for various aperture diameter operating at 400°F

Figure 66. Error in convective heat loss for various aperture diameter operating at 600°F

Figure 67. Error in radiative heat loss from Phase 1 test

Figure 68. Error in radiative heat loss from Phase 2 test

The error in the radiative heat loss measurement increases with decrease in receiver operating temperature and receiver aperture diameter (Fig. 67 & 68). The maximum error in the radiative heat loss is 38.5% with a six inch aperture and a 400°F operating temperature.

XI. CONCLUSIONS:

The results of experimental testing of the heat loss from a solar cavity receiver for various aperture diameters and operating temperatures have been presented. With an increase in aperture size there was an increase in the convective heat loss. The effect of aperture size on the convective heat loss decreased with increases in aperture size. Decreasing the aperture diameter from 18 inches to 6 inches, reduce the convective losses by 60%. The 18 inch aperture presently used for this type of receiver has little or no effect on the free convective heat loss from the receiver.

Conduction was the primary mode of heat loss from the receiver for very small apertures (less than 12 inch diameter).

A low cost radiometer can be used to determine the radiative heat loss from a cavity within $\pm 20\%$ of experimentally determined radiative heat loss.

XII. RECOMMENDATIONS

Further investigation into cavity temperature distribution and internal surface emissivity and how each affects analytically determined radiative heat loss. Inquiries into convective heat loss from a cavity is necessary to consider how various wind condition will effect heat loss characteristics.

APPENDIX 1 Temperature and Angle Test Results																								
Angle	Delta T	Flow SR1	Flow SR1	Flow SR1 error	Flow SR1 error	Flow 1	Flow 2	T amb	T in	T in cal	T out	T out cal	T avg	Delta T (mV)	Density	error Density	Cp	error Cp	Mass Flow	Heat Loss	Heat Loss	error Heat Loss		
300°F	[μV]	[gpm]	[volts]	[±gpm]	[±%]	[gpm]	[gpm]	[°F]	[°F]	[°F]	[°F]	[°F]	[°F]	[°F]	[lbw/lb³]	[±%]	[BTU/lb °F]	[±%]	[lbw/min]	[BTU/min]	[Watts]	[±%]		
90°	105.99	1.42	4.7630	0.0198	1.3983	0.00	0.00	83.7	308	308.0	303.3	303.9	308.0	4.74	51.09	0.09	0.4384	0.1179	9.876	20.12	353.81	30.363		
90°	185.12	1.26	4.2444	0.0185	1.4622	1.10	1.03	78.5	297.8	297.7	288.5	289.0	293.4	8.26	51.35	0.09	0.4355	0.1186	8.877	31.20	348.530	17.341		
75°	185.12	1.27	4.2713	0.0186	1.4384	1.11	1.09	80.3	305	305.0	295.1	295.7	300.3	8.27	51.13	0.09	0.4371	0.1182	8.894	31.44	352.796	17.341		
60°	224.69	1.22	4.0884	0.0181	1.4857	1.05	1.05	80.2	305.1	305.1	294.6	295.1	300.1	10.04	51.12	0.09	0.4370	0.1182	8.321	36.31	642.040	14.478		
45°	264.26	1.17	3.9437	0.0177	1.5096	1.01	1.03	79.1	307.6	307.6	294.2	294.7	301.2	11.81	51.04	0.09	0.4373	0.1182	8.014	41.39	727.870	12.338		
30°	357.53	1.18	3.9467	0.0177	1.5090	1.01	1.03	79.1	308.2	308.2	291.9	292.4	300.3	15.98	51.02	0.09	0.4371	0.1182	8.017	55.99	984.466	9.177		
15°	397.09	1.17	3.9243	0.0177	1.5129	1.01	1.03	78.4	308.8	308.8	289.7	290.2	299.3	17.74	51.00	0.09	0.4369	0.1183	7.968	61.77	1086.103	8.289		
0°	477.64	1.18	3.9687	0.0178	1.5053	1.01	1.04	76.8	309	309.0	287.6	288.1	298.8	21.34	51.00	0.09	0.4367	0.1183	8.057	75.07	1320.023	6.942		
-30°	517.21	1.18	3.9847	0.0178	1.5083	1.00	1.05	75.8	310.2	310.3	286.5	287.0	298.6	23.10	50.96	0.09	0.4367	0.1183	8.051	81.23	1428.363	6.437		
-60°	517.21	1.18	3.9594	0.0178	1.5069	1.00	1.05	74.5	310.4	310.5	286.1	286.6	298.5	23.10	50.95	0.09	0.4367	0.1183	8.031	81.02	1424.721	6.437		
-90°	423.94	1.18	3.9594	0.0178	1.5069	1.01	1.04	73.6	311.3	311.4	291.7	292.2	301.8	18.95	50.93	0.09	0.4374	0.1181	8.027	66.35	1170.200	7.782		
400°F																								
90°	145.55	1.52	5.1035	0.0208	1.3854	1.27	1.23	81.9	406.5	406.3	401.8	403.3	406.9	6.54	47.74	0.10	0.4613	0.1120	9.899	29.18	514.780	22.213		
90°	291.11	1.47	4.9326	0.0203	1.3812	1.27	1.31	76.5	401.5	402.4	388	389.6	396.3	13.11	47.98	0.10	0.4589	0.1126	9.421	56.66	996.372	11.202		
75°	278.39	1.47	4.9381	0.0203	1.3806	1.27	1.31	75.9	402.9	403.8	389.4	391.0	397.9	12.53	47.93	0.10	0.4592	0.1125	9.422	54.22	953.469	11.708		
60°	317.96	1.46	4.9013	0.0202	1.3842	1.27	1.31	76	402.8	403.7	387.3	388.0	396.9	14.31	47.93	0.10	0.4590	0.1126	9.333	61.43	1080.348	10.292		
45°	384.38	1.47	4.9802	0.0203	1.3804	1.26	1.30	76.4	402.5	403.4	384.5	386.0	395.5	17.31	47.94	0.10	0.4586	0.1127	9.429	74.84	1316.094	8.332		
30°	463.51	1.47	4.9326	0.0203	1.3812	1.27	1.31	77.3	402.4	403.3	380.9	382.4	393.4	20.88	47.95	0.10	0.4582	0.1128	9.415	90.06	1583.600	7.118		
15°	539.35	1.47	4.9474	0.0203	1.3797	1.27	1.36	78.1	405.2	406.1	380.2	381.7	394.3	23.87	47.83	0.10	0.4584	0.1127	9.423	103.11	1813.139	6.282		
0°	598.35	1.48	4.9835	0.0204	1.3761	1.17	1.38	79.4	404.4	405.3	377	378.4	392.4	26.86	47.88	0.10	0.4580	0.1128	9.303	116.90	2035.830	5.806		
-30°	662.77	1.49	4.9973	0.0205	1.3730	1.20	1.39	80.9	404.4	405.3	374	375.4	390.9	29.86	47.88	0.10	0.4576	0.1129	9.525	130.15	2288.678	5.074		
-60°	650.05	1.49	5.0038	0.0205	1.3742	1.21	1.30	80.9	404	404.9	373.7	375.1	390.6	29.29	47.89	0.10	0.4575	0.1129	9.544	127.89	2248.875	5.166		
-90°	503.08	1.30	5.0484	0.0206	1.3703	1.21	1.30	80.2	403.2	404.1	379.3	380.8	393.0	22.66	47.92	0.10	0.4581	0.1128	9.627	99.93	1737.180	6.578		
Angle	Delta mV	Flow SR1	Flow SR1	Flow SR1 error	Flow SR1 error	Flow 1	Flow 2	T amb	T in	T in cal	T out	T out cal	T avg	Delta T (mV)	Density	error Density	Cp	error Cp	Mass Flow	Heat Loss	Heat Loss	error Heat Loss		
300°F	[μV]	[gpm]	[volts]	[±gpm]	[±%]	[gpm]	[gpm]	[°F]	[°F]	[°F]	[°F]	[°F]	[°F]	[°F]	[lbw/lb³]	[±%]	[BTU/lb °F]	[±%]	[lbw/min]	[BTU/min]	[Watts]	[±%]		
90°	291.11	1.34	4.4919	0.0191	1.4293	1.19	1.09	83.8	513.4	517.2	503.3	506.3	511.8	12.78	44.00	0.12	0.4850	0.1063	7.868	48.76	857.444	11.268		
90°	450.79	1.35	4.5270	0.0192	1.4250	1.19	1.09	84.3	513.8	515.6	494.4	497.1	506.5	19.81	44.06	0.12	0.4838	0.1068	7.940	76.10	1338.205	7.320		
75°	450.79	1.37	4.3892	0.0194	1.4176	1.22	1.12	84.8	514.6	516.4	495.6	498.3	507.5	19.81	44.03	0.12	0.4840	0.1067	8.044	77.11	1356.009	7.319		
60°	517.21	1.32	4.4448	0.0190	1.4352	1.18	1.08	84.8	515.4	517.2	493.2	495.9	506.7	22.73	44.00	0.12	0.4839	0.1068	7.786	83.62	1505.603	6.421		
45°	603.20	1.32	4.4293	0.0190	1.4372	1.17	1.08	83.8	515.6	517.4	488.2	490.8	504.2	27.40	43.99	0.12	0.4833	0.1069	7.757	102.73	1806.395	5.390		
30°	782.88	1.32	4.4348	0.0190	1.4363	1.17	1.09	84.4	516	517.8	482.5	484.9	501.5	34.44	43.98	0.12	0.4827	0.1070	7.764	129.08	2269.828	4.379		
15°	901.39	1.33	4.4707	0.0191	1.4320	1.18	1.12	84.1	516.4	518.3	477.6	480.1	499.3	39.69	43.96	0.12	0.4822	0.1071	7.824	149.73	2632.958	3.868		
0°	982.14	1.34	4.4937	0.0191	1.4289	1.19	1.13	83.6	516.9	518.8	474.1	476.6	497.8	43.25	43.94	0.12	0.4819	0.1072	7.865	163.90	2881.977	3.395		
-30°	1088.12	1.34	4.4986	0.0191	1.4285	1.18	1.17	83.2	518.3	520.2	470.9	473.3	496.9	47.93	43.89	0.12	0.4816	0.1073	7.861	181.45	3190.663	3.303		
-60°	1127.69	1.34	4.4847	0.0191	1.4302	1.19	1.18	83.1	519.3	521.2	470.7	473.1	497.3	49.66	43.86	0.12	0.4817	0.1072	7.830	187.32	3293.966	3.211		
-90°	888.87	1.34	4.4847	0.0191	1.4302	1.18	1.19	82.5	521	522.9	482.8	485.4	504.2	39.08	43.79	0.12	0.4833	0.1069	7.819	147.88	2598.893	3.913		
600°F																								
90°	330.68	1.49	5.0113	0.0205	1.3737	1.34	1.39	76.5	601.3	603.9	587.9	591.6	597.4	14.31	40.70	0.14	0.5044	0.1024	8.119	51.59	1030.273	9.883		
90°	542.83	1.50	5.0223	0.0205	1.3727	1.34	1.39	77.6	601.3	603.9	577.7	581.3	592.3	23.49	40.70	0.14	0.5033	0.1027	8.137	96.20	1691.828	6.121		
75°	542.83	1.31	5.0808	0.0207	1.3674	1.33	1.39	77.4	601.6	604.2	577.4	581.0	592.3	23.49	40.69	0.14	0.5033	0.1027	8.229	97.29	1710.780	6.120		
60°	633.92	1.48	4.9863	0.0204	1.3761	1.33	1.38	77.2	601.5	604.1	573.4	576.9	590.3	27.54	40.69	0.14	0.5028	0.1028	8.077	111.83	1966.501	5.274		
45°	795.60	1.49	4.9998	0.0205	1.3748	1.33	1.38	77.6	601.7	604.3	567.5	571.0	587.4	34.46	40.68	0.14	0.5022	0.1029	8.097	140.14	2464.250	4.297		
30°	953.29	1.48	4.9749	0.0204	1.3771	1.33	1.38	78.1	600.4	603.0	538.8	562.2	582.4	41.41	40.73	0.14	0.5010	0.1031	8.067	167.38	2943.183	3.681		
15°	1106.84	1.49	4.9982	0.0205	1.3749	1.34	1.38	78.2	598.4	601.0	531.3	554.6	577.6	47.73	40.81	0.14	0.4998	0.1033	8.121	193.87	3409.096	3.230		
0°	1181.39	1.48	4.9842	0.0204	1.3782	1.33	1.35	78.7	594.8	597.1	543.9	547.1	571.9	51.29	40.97	0.14	0.4987	0.1036	8.129	207.89	3653.536	3.070		
-30°	1287.38	1.49	4.9927	0.0205	1.3755	1.34	1.38	80.6	594.7	597.2	539.5	542.7	569.4	55.91	40.96	0.14	0.4982	0.1037	8.142	226.72	3997.206	2.871		
-60°	1300.10	1.50	5.0336	0.0206	1.3699	1.35	1.37	80.6	597.3	600.1	542.4	545.8	572.8	36.43	40.85	0.14	0.4988	0.1036	8.218	231.35	4068.151	2.847		
-90°	1048.36	1.31	5.0391	0.0206	1.3694	1.35	1.37	80.6	601.4	604.0	537	560.4	581.9	45.46	40.69	0.14	0.5009	0.1031	8.196	186.62	3281.530	3.381		

Heat Loss Conv	normalized Heat Loss [Watts]	normalized error Heat Loss [±%]	normalized Heat Loss Conv [Watts]	normalized error Conv [±%]	normalized Heat Loss Cond [Watts]	% Cond	% Cond	% Radiation	alpha	dalpha/dT	error alpha	error ΔT	error ΔT	HTF viscosity
														(centistokes)
0.000	366.084	0.000	0.000	24.997	366.084	0.0	100.0	0.0	22.3429	-0.0007	0.0131	1.4	30.5	1.7685
4.148	377.839	17.669	-9.457	24.992	error Cond	0.0	62.3	37.7	22.4212	-0.0066	0.0152	1.4	19.3	1.8764
93.391	671.439	14.634	84.143	22.947	30.635	-1.6	63.4	38.3	22.3766	-0.0062	0.0141	1.4	17.3	1.7994
179.220	753.799	12.317	166.303	21.659		22.1	48.6	29.3	22.3713	-0.0061	0.0139	1.4	14.4	1.7984
435.816	1023.497	9.417	436.202	20.028	Heat Loss Rad:	42.6	35.8	21.6	22.3766	-0.0062	0.0141	1.4	9.1	1.7665
537.453	1129.722	8.555	542.426	19.637	error Rad	48.0	32.4	19.6	22.3816	-0.0062	0.0142	1.4	8.1	1.7604
771.373	1369.076	7.255	781.781	19.106	221.212	57.1	26.7	16.2	22.3876	-0.0063	0.0143	1.4	6.8	1.7584
878.714	1474.466	6.770	887.170	18.928	error Rad	60.2	24.8	15.0	22.3873	-0.0063	0.0143	1.4	6.3	1.7463
876.072	1462.836	6.767	875.340	18.927	35.368	50.2	25.0	15.1	22.3879	-0.0063	0.0144	1.4	6.3	1.7443
621.350	1179.476	8.047	592.180	19.421	Heat Loss Cond				22.3876	-0.0061	0.0138	1.4	7.6	1.7353
0.000	322.853	22.320	0.000	15.976	322.853	0.0	50.9	49.1	22.2106	0.0027	0.0062	1.3	11.1	1.0718
-42.903	977.075	11.796	-30.370	16.333	error Cond	-5.2	53.5	51.7	22.2143	0.0028	0.0063	1.3	11.6	1.0644
84.178	1111.118	10.374	83.673	13.338	22.2117	7.3	47.0	45.4	22.2117	0.0028	0.0063	1.3	10.2	1.0640
318.722	1362.072	8.857	334.627	14.233	22.2107	25.5	28.8	31.1	22.2072	0.0026	0.0060	1.3	8.4	1.0666
587.228	1633.244	7.270	625.799	13.434	Heat Loss Rad:	37.9	31.6	30.3	22.2025	0.0023	0.0059	1.3	7.0	1.0670
816.767	1891.360	6.434	863.914	13.001	error Rad	45.7	27.6	26.7	22.2051	0.0026	0.0059	1.3	6.1	1.0522
1039.278	2167.021	5.796	1130.376	12.697	504.792	52.8	24.1	23.3	22.2001	0.0024	0.0053	1.3	5.4	1.0564
1292.306	2436.096	5.294	1408.651	12.476	error Rad	57.8	21.5	20.7	22.1966	0.0023	0.0052	1.3	4.9	1.0564
1232.503	2396.448	5.382	1369.003	12.314	25.016	57.1	21.8	21.1	22.1958	0.0023	0.0051	1.3	5.0	1.0585
760.809	1853.833	6.746	826.387	13.158	Heat Loss Cond				22.2015	0.0025	0.0056	1.3	6.4	1.0628
0.000	861.371	11.261	0.000	10.469	861.371	0.0	100.0	58.2	22.7828	0.0051	0.0115	1.4	11.1	0.6323
17.803	1379.549	7.402	16.482	10.469	error Cond	0.0	63.2	36.8	22.7552	0.0052	0.0119	1.4	7.2	0.6367
187.397	1534.687	6.316	171.680	9.862	22.7604	1.2	62.4	36.4	22.7604	0.0052	0.0118	1.4	7.2	0.6345
468.190	1847.466	5.304	484.399	9.225	22.7582	11.2	56.1	32.4	22.7582	0.0052	0.0118	1.4	6.3	0.6323
931.621	2340.183	4.520	977.113	8.674	22.7436	26.2	46.6	27.2	22.7436	0.0053	0.0120	1.4	5.2	0.6318
1224.753	2726.760	4.022	1363.692	8.428	Heat Loss Rad:	41.8	36.8	21.4	22.7290	0.0053	0.0121	1.4	4.1	0.6307
1543.772	2991.930	3.768	1628.863	8.307	error Rad	50.0	31.6	18.4	22.7174	0.0054	0.0122	1.4	3.6	0.6296
1832.457	3316.435	3.492	1953.388	8.185	501.697	54.4	28.8	16.8	22.7093	0.0054	0.0123	1.4	3.3	0.6283
1935.760	3419.686	3.403	2056.618	8.148	error Rad	58.9	26.0	15.1	22.7044	0.0054	0.0123	1.4	3.0	0.6245
1258.690	2647.790	4.069	1284.723	8.448	22.7066	60.1	25.2	14.7	22.7066	0.0054	0.0123	1.4	2.9	0.6218
0.000	1048.173	9.924	0.000	8.732	13.477	48.5	32.5	18.9	22.7436	0.0053	0.0120	1.4	3.6	0.6173
19.152	1760.898	6.187	19.038	8.751	Heat Loss Cond				23.1152	0.0030	0.0067	1.4	9.8	0.4453
274.872	2031.461	5.352	289.600	8.182	1048.173	0.0	60.2	39.8	23.0998	0.0030	0.0069	1.4	6.0	0.4453
772.622	2561.915	4.394	820.115	7.590	error Cond	1.1	59.5	39.4	23.0998	0.0030	0.0069	1.4	6.0	0.4448
1231.355	3093.283	3.776	1381.804	7.236	22.7093	14.3	51.6	34.1	23.0936	0.0030	0.0069	1.4	5.1	0.4449
1717.468	3618.174	3.382	1876.313	7.052	Heat Loss Rad:	9.2	40.9	27.1	23.0848	0.0031	0.0070	1.4	4.1	0.4446
1963.908	3927.963	3.213	2186.103	6.973	error Rad	43.7	33.9	22.4	23.0890	0.0032	0.0072	1.4	3.4	0.4468
2393.378	4319.945	3.026	2578.084	6.889	23.0536	51.9	29.0	19.2	23.0536	0.0033	0.0074	1.4	2.9	0.4503
2376.323	4387.976	3.001	2640.116	6.878	693.687	55.7	26.7	17.7	23.0349	0.0034	0.0077	1.4	2.7	0.4570
1589.902	3469.065	3.507	1727.204	7.113	error Rad	59.7	24.3	16.1	23.0276	0.0034	0.0078	1.4	2.5	0.4569
					23.0373	60.2	23.9	14.8	23.0373	0.0034	0.0077	1.4	2.5	0.4519
					Heat Loss Cond				23.0677	0.0032	0.0073	1.4	3.1	0.4451

Appendix 2: Phase Two; Aperture Size Test Result

[illegible]

Appendix 2: Phase Two; Aperture Size Test Result

[illegible]

Appendix 2: Phase Two; Aperture Size Test Result

[illegible]

Appendix 2: Phase Two; Aperture Size Test Result

System Density [lb/ft ³]	error Density [%]	System Cp [BTU/ft ² -°F]	error Cp [%]	System viscosity [cP]	Total Heat Loss [BTU/min]	Total Heat Loss [Watt]	error Heat Loss [%]	Normalized error Heat Loss [Watt]	Normalized error Heat Loss [%]	Normalized error Conv [%]	Normalized error k [W/m ² -K]	Normalized error h [W/m ² -K]	Normalized error K [%]			
48.41	0.10	0.4573	0.1130	10317	10.43	181.7	4.7	1060.2	1956.6	5.0	1262.7	11.9	0.0072	6.600	610.8	20.5
48.47	0.10	0.4583	0.1127	10317	94.64	1664.2	5.1	935.7	1758.4	5.3	1064.4	12.1	0.0072	5.5976	514.9	16.8
48.12	0.10	0.4593	0.1125	10240	82.34	1473.9	5.7	719.4	1502.9	5.9	808.9	12.4	0.0072	4.2538	391.3	12.5
47.97	0.10	0.4604	0.1122	10240	66.85	1173.3	6.9	471.1	1186.9	7.0	502.9	12.9	0.0072	2.6444	243.3	7.6
47.79	0.10	0.4616	0.1119	9997.6	52.74	874.4	8.6	184.9	965.7	8.7	232.7	13.9	0.0072	1.2237	112.6	1.6
47.49	0.10	0.4628	0.1114	9828.8	42.70	777.4	10.4	22.4	777.4	10.5	31.4	13.1	0.0072	0.1131	1.1	0.0
47.32	0.10	0.4644	0.1112	9340.3	41.43	724.3	10.8	0.0	694.0	10.9	0.0	15.4	0.0072	0.0000	0.0	0.0
47.01	0.10	0.4669	0.1107	8912.7	25.51	444.6	17.3	0.0	413.8	17.3	0.0	0.0	0.0072	0.0000	0.0	0.0
error K	41.90	0.14	0.4989	0.1036	0.4422	19.82	2.7	2180.7	3728.0	2.8	2372.2	6.3	0.0072	7.7673	714.5	12.5
	41.87	0.14	0.4990	0.1033	0.4463	176.84	2.9	1835.3	3340.6	3.0	1944.9	6.8	0.0072	6.4990	597.8	10.1
	41.75	0.14	0.4998	0.1034	0.4479	152.37	2.9	1352.0	2664.8	3.3	1590.0	6.7	0.0072	4.9490	454.5	7.6
	41.55	0.14	0.5009	0.1031	0.4475	123.07	2.9	869.8	2183.6	3.8	971.9	7.0	0.0072	3.0381	279.8	6.0
	41.42	0.14	0.5017	0.1030	0.4491	94.16	4.5	366.5	1714.5	4.6	418.3	7.5	0.0072	1.7111	158.1	1.8
41.31	0.14	0.5023	0.1029	0.4495	63.35	5.6	24.2	1403.8	5.7	18.0	8.2	0.0072	0.1173	14.5	0.0	
41.30	0.14	0.5034	0.1028	0.4515	31.60	728.2	5.8	0.0	728.2	5.9	0.0	8.3	0.0072	0.0000	0.0	0.0
41.04	0.14	0.5038	0.1023	0.4533	7.76	66.1	10.9	0.0	67.8	10.9	0.0	0.0	0.0072	0.0000	0.0	0.0
error K	42.06	0.14	0.4980	0.1038	0.4463	237.6	2.5	2259.0	4515.5	2.7	2484.1	5.4	0.0072	8.1403	744.8	11.2
	42.05	0.14	0.4990	0.1037	0.4481	209.07	2.6	2071.1	4312.9	2.8	2263.5	5.4	0.0072	7.4768	687.8	10.1
	41.94	0.14	0.4986	0.1036	0.4486	207.94	2.8	1899.4	3862.0	2.9	1862.5	5.5	0.0072	6.6985	561.0	7.6
	41.56	0.14	0.4997	0.1034	0.4487	173.92	3.0	1101.3	3232.2	3.3	1193.8	5.7	0.0072	3.9089	359.6	4.5
	41.55	0.14	0.5009	0.1031	0.4487	137.75	3.8	463.3	2528.3	3.9	498.4	6.0	0.0072	1.6332	150.2	1.8
41.41	0.14	0.5017	0.1030	0.4482	116.63	4.4	31.9	2124.9	4.4	9.5	6.4	0.0072	0.3256	30.0	0.0	
41.37	0.14	0.5020	0.1029	0.4479	111.29	1957.9	4.5	0.0	2028.4	4.6	0.0	6.5	0.0072	0.0000	0.0	0.0
41.01	0.14	0.5040	0.1025	0.4444	47.02	84.7	10.2	0.0	84.3	10.2	0.0	0.0	0.0072	0.0000	0.0	0.0

APPENDIX 3: LeQuere, Penot and Mirenayat Model Computer Program Listing

```

REM *****
REM
REM      P. LeQuere, F. Penot, & M. Mirenayat
REM *****
REM  The LeQuere, Penot, & Mirenayat model is used here to predict the convective
losses from
REM  a solar cavity receiver operating at various temperatures and receiver angles.
REM *****
      PRINT " P. LeQuere, F. Penot, & M. Mirenayat Model for Predicting Convective Heat
Loss"
      PRINT
      PRINT
REM *****
REM ***** Receiver Geometry *****
Re=.127      :REM  end plate radius [m]
Rc=.33      :REM  cavity radius [m]
Ro=.45 :REM                      receiver outside radius [m]
Lf=.292      :REM  frustum length [m]
Lh=.254      :REM  cylinder length hot [m]
Lc=.14      :REM  cylinder length cold [m]
REM *****
REM ***** Constants *****
pi=4*ATN(1)
g=9.810001      :REM  gravitational acceleration [m/sec^2]
SB=5.6696E-08      :REM  Stefan Boltzmann const. [W/m^2 K^4]
Cp=1006.86      :REM  specific heat capacity of air at Ta [J/kg K]
Pf=1.19406      :REM  density of air at Ta [kg/m^3]
e=.9      :REM  emittance of cavity
ki=.04756      :REM  insulation conductance [W/m-K] [.33B/h/ft^2/in]
ti=.0889      :REM  thickness of insulation [m] [3.5 in]
Ta=70      :REM  ambient temperature [F]
Ta=(Ta+459.67)/1.8      :REM  ambient temperature [K]
REM *****
REM ***** Angle constants *****
DIM a(13),b(13)
FOR I=1 TO 13
  READ a(I)
  DATA .057,.047,.0545,.0465,.048,.0465,.0925,.0810,.064,.0605,.068 5,.033,0
NEXT I
FOR I=1 TO 13
  READ b(I)
  DATA .353,.36,.36,.37,.369,.368,.33,.331,.332,.316,.292,.302,0
NEXT I
REM *****
REM  open clipboard file for transferring data to spread sheet
OPEN "CLIP:" FOR OUTPUT AS #1
100 :
REM ***** Print Constants *****
REM
CLS
PRINT "End Plate Radius [m] = ";Re
PRINT "Cavity Radius [m] = ";Rc
PRINT "Frustum Length [m] = ";Lf

```

```

PRINT "Hot Cylindrical Section Length [m] = ";Lh
PRINT "Cold Cylindrical Section Length [m] = ";Lc
PRINT "Ambient Temperature [K] = ";
PRINT USING"####.##";Ta
PRINT
REM ***** Write to the clipboard *****
WRITE#1,"","End Plate Radius [m] = ",Re
WRITE#1,"","Cavity Radius [m] = ",Rc
WRITE#1,"","Frustum Length [m] = ",Lf
WRITE#1,"","Hot Cylindrical Section Length [m] = ",Lh
WRITE#1,"","Cold Cylindrical Section Length [m] = ",Lc
WRITE#1,"","Ambient Temperature [K] = ",Ta
WRITE#1,
REM ***** Receiver Aperture Radius Loop *****
FOR I=1 TO 4
CLS
READ Ra
DATA .0762,.1524,.2286,.329
Da=2*Ra :REM aperture diameter [m]
Aa=pi*Ra^2 :REM aperture area [m^2]
REM *****
REM ***** Area Constants *****
REM In the following section Ah and Ar are calculated.
REM Ah is the total interior heated cavity surface area based on the tube bundle
geometry.
REM Ar is the total interior refractory cavity surface.
REM At is the total cavity area.
Ah=pi*(Re+Rc)*(Lf^2+(Rc-Re)^2)^.5+2*pi*Rc*Lh
Ar=pi*Re^2+pi*(Rc^2-Ra^2)+2*pi*Rc*Lc
At=Ah+Ar
Ao=pi*((Rc+Ro)/2)^2+2*pi*((Rc+Ro)/2)+pi*(Rc^2-Ra^2)
REM *****
REM ***** Print Header *****
REM
CLS
PRINT "Aperture Radius [m] = ";Ra
PRINT "Total Cavity Area [m^2] = ";
PRINT USING "####.####";At
PRINT "Total Heated Cavity Area [m^2] = ";
PRINT USING "####.####";Ah
PRINT "Total Refractory Cavity Area [m^2] = ";
PRINT USING "####.####";Ar
REM ***** write header to clipboard *****
WRITE#1,"","Aperture Radius [m] = ",Ra
WRITE#1,"","Total Cavity Area [m^2] = ",At
WRITE#1,"","Total Heated Cavity Area [m^2] = ",Ah
WRITE#1,"","Total Refractory Cavity Area [m^2] = ",Ar
REM ***** Operating Temperature Loop *****
REM
FOR Tmf=300 TO 600 STEP 100
WRITE#1,
REM The operating temperature is converted from F to K
Tm=(Tmf+459.67)/1.8
Twf=Tmf-100 :REM The refractory surfaces are assumed to be 100°F cooler
:REM than the heated tube surfaces.

```

```

Tw=(Twf+459.67)/1.8
CLS
REM *****
REM ***** Print Table Header *****
PRINT "T mean [K] = ";
PRINT USING "####.#";Tm;
PRINT "    [°F] = ";
PRINT USING "####.#";Tmf
PRINT
PRINT ;TAB(3);" Angle";TAB(12);"Q conv";TAB(24);" Nu ";TAB(35);" Gr"
PRINT ;TAB(1);" [degrees]";TAB(13);"[Watts]"
PRINT
REM *****
REM ***** write table header to clipboard *****
WRITE#1,"", "T mean [K] = ",Tm
WRITE#1,"", "    [°F] = ",Tmf
WRITE#1,
WRITE#1," Angle","Q conv"," Nu "," Gr"
WRITE#1," [degrees]","[Watts]"
WRITE#1,
REM ***** Beginning of Angle Loop *****
n=0
FOR phi=-90 TO 90 STEP 15
    z=pi*phi/180 :REM convert angle to radian measure
    REM ***** Angle Function *****
    n=n+1
    REM *****
    Tcav=(Tm*Ah+Tw*Ar)/At :REM area average cavity temperature [K]
    L=2*Ra
    C=1.1547E+19*Ta^-4.4187 :REM gB/v^2.
    k=.0071749261015#+.000064030639041#*Ta
    REM ***** Heat Loss Calculations *****
    Gr=C*(Tcav-Ta)*L^3 :REM Grashof number
    Pr=.7814008749#-.00037306809395#*Ta+5.2131644352D-07*Ta^2-2.
    1272705278D-10*Ta^3
    REM Pr = Prandtl number
    Nu=a(n)*Gr^b(n) :REM Nusselt number
    h=Nu*k/L :REM heat transfer coefficient [W/m^2 K]
    REM *****
    REM ***** heat loss calculations *****
    Qc=h*At*(Tcav-Ta) :REM convective
    REM ***** Output Loop Results *****
    PRINT ;TAB(3);phi;
    PRINT TAB(12);
    PRINT USING "####.#";Qc;
    PRINT TAB(22);
    PRINT USING "###.##";Nu;
    PRINT TAB(32);
    PRINT USING "##.##^";Gr
    REM ***** write to clipboard *****
    WRITE#1,phi,Qc,Nu,Gr
    REM *****
    REM ***** End of Angle Loop *****
NEXT phi
REM *****

```

```

REM          ***** End of Temperature Loop *****
  NEXT Tmf
REM          *****
REM          ***** End of Aperture Radius Loop *****
  NEXT I
REM          *****
CLOSE#1
END

```

Appendix 4 LeQuere, Penot and Mirenayat Model Heat Loss Data
 End Plate Radius [m] 27
 Cavity Radius [m] 33
 Frustum Length [m] 292
 Hot Cylindrical Section Length [m] 0.254
 Cold Cylindrical Section Length [m] 0.254
 Ambient Temperature [K] 261.1

Aperture Radius [m] 0.0762 3
 Total Cavity Area [m²] 2.79
 Total Heated Cavity Area [m²] 2.79
 Total Refractory Cavity Area [m²] 0.62 =

T mean [K] [°F]	422.0 300			477.6 400			533.2 500			588.7 600		
	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr
Angle [degrees]												
-90	939.5	30.5	5.35E+7	1661.0	35.4	8.15E+7	2477.2	39.3	1.10E+8	3371.3	42.5	1.38E+8
-75	877.4	28.5	5.35E+7	1555.8	33.1	8.15E+7	2325.2	36.8	1.10E+8	3169.5	40.0	1.38E+8
-60	1017.4	33.0	5.35E+7	1804.1	38.4	8.15E+7	2696.2	42.7	1.10E+8	3675.3	46.4	1.38E+8
-45	1037.2	33.6	5.35E+7	1846.9	39.3	8.15E+7	2768.3	43.9	1.10E+8	3782.1	47.7	1.38E+8
-30	1051.7	34.1	5.35E+7	1872.0	39.9	8.15E+7	2805.2	44.5	1.10E+8	3831.6	48.3	1.38E+8
-15	1000.9	32.5	5.35E+7	1780.8	37.9	8.15E+7	2667.7	42.3	1.10E+8	3643.0	46.0	1.38E+8
0	1012.5	32.8	5.35E+7	1772.8	37.7	8.15E+7	2626.1	41.6	1.10E+8	3555.3	44.9	1.38E+8
15	902.6	29.3	5.35E+7	1581.0	33.7	8.15E+7	2342.6	37.1	1.10E+8	3172.2	40.0	1.38E+8
30	725.9	23.6	5.35E+7	1272.1	27.1	8.15E+7	1885.5	29.9	1.10E+8	2553.8	32.2	1.38E+8
45	516.2	16.7	5.35E+7	898.5	19.1	8.15E+7	1325.5	21.0	1.10E+8	1788.7	22.6	1.38E+8
60	381.3	12.4	5.35E+7	657.0	14.0	8.15E+7	962.4	15.3	1.10E+8	1291.7	16.3	1.38E+8
75	219.5	7.1	5.35E+7	379.8	8.1	8.15E+7	557.9	8.8	1.10E+8	750.5	9.5	1.38E+8
90	0.0	0.0	5.35E+7	0.0	0.0	8.15E+7	0.0	0.0	1.10E+8	0.0	0.0	1.38E+8

Aperture Radius [m] 0.24 6
 Total Cavity Area [m²] 2.79
 Total Heated Cavity Area [m²] 2.79
 Total Refractory Cavity Area [m²] 0.62 =

T mean [K] [°F]	422.0 300			477.6 400			533.2 500			588.7 600		
	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr
Angle [degrees]												
-90	960.8	63.7	4.33E+8	1690.5	73.9	6.57E+8	2515.1	81.9	8.81E+8	3418.1	88.8	1.11E+9
-75	910.6	60.4	4.33E+8	1606.8	70.2	6.57E+8	2395.5	78.0	8.81E+8	3260.7	84.7	1.11E+9
-60	1055.9	70.0	4.33E+8	1863.1	81.4	6.57E+8	2777.8	90.5	8.81E+8	3781.0	98.2	1.11E+9
-45	1099.1	72.9	4.33E+8	1947.5	85.1	6.57E+8	2912.1	94.9	8.81E+8	3972.8	103.2	1.11E+9
-30	1112.2	73.8	4.33E+8	1969.9	86.1	6.57E+8	2944.8	95.9	8.81E+8	4016.5	104.3	1.11E+9
-15	1056.3	70.1	4.33E+8	1870.0	81.7	6.57E+8	2794.6	91.0	8.81E+8	3810.8	99.0	1.11E+9
0	986.9	65.5	4.33E+8	1719.8	75.1	6.57E+8	2541.5	82.8	8.81E+8	3436.0	89.2	1.11E+9
15	881.6	58.5	4.33E+8	1536.8	67.2	6.57E+8	2271.9	74.0	8.81E+8	3072.1	79.8	1.11E+9
30	710.6	47.1	4.33E+8	1239.2	54.1	6.57E+8	1832.4	59.7	8.81E+8	2478.4	64.4	1.11E+9
45	488.6	32.4	4.33E+8	846.5	37.0	6.57E+8	1245.9	40.6	8.81E+8	1679.0	43.6	1.11E+9
60	343.3	22.8	4.33E+8	588.8	25.7	6.57E+8	860.5	28.0	8.81E+8	1153.3	29.9	1.11E+9
75	201.8	13.4	4.33E+8	347.5	15.2	6.57E+8	509.3	16.6	8.81E+8	684.2	17.8	1.11E+9
90	0.0	0.0	4.33E+8	0.0	0.0	6.57E+8	0.0	0.0	8.81E+8	0.0	0.0	1.11E+9

Aperture Radius [m] = 0.2286 9
 Total Cavity Area [m²] = 1.556
 Total Heated Cavity Area [m²] = 1.037
 Total Refractory Cavity Area [m²] = 0.519

T mean [K]	422.0			477.6			533.2			588.7		
[°F]	300			400			500			600		
Angle [degrees]	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr
-90	953.8	98.6	1.49E+9	1663.5	114.0	2.24E+9	2464.4	126.3	3.00E+9	3340.5	136.7	3.76E+9
-75	911.7	94.2	1.49E+9	1594.8	109.3	2.24E+9	2367.4	121.3	3.00E+9	3214.1	131.5	3.76E+9
-60	1057.2	109.3	1.49E+9	1849.2	126.7	2.24E+9	2745.2	140.7	3.00E+9	3727.0	152.5	3.76E+9
-45	1114.2	115.2	1.49E+9	1956.9	134.1	2.24E+9	2913.4	149.3	3.00E+9	3964.3	162.3	3.76E+9
-30	1126.1	116.4	1.49E+9	1977.0	135.5	2.24E+9	2942.5	150.8	3.00E+9	4003.0	163.8	3.76E+9
-15	1068.1	110.4	1.49E+9	1874.4	128.4	2.24E+9	2789.0	142.9	3.00E+9	3793.3	155.3	3.76E+9
0	952.2	98.4	1.49E+9	1645.1	112.7	2.24E+9	2421.0	124.1	3.00E+9	3264.8	133.6	3.76E+9
15	851.6	88.0	1.49E+9	1472.0	100.9	2.24E+9	2166.8	111.0	3.00E+9	2922.7	119.6	3.76E+9
30	687.3	71.0	1.49E+9	1188.3	81.4	2.24E+9	1749.8	89.7	3.00E+9	2360.7	96.6	3.76E+9
45	463.4	47.9	1.49E+9	796.0	54.5	2.24E+9	1166.6	59.8	3.00E+9	1568.3	64.2	3.76E+9
60	316.0	32.7	1.49E+9	537.5	36.8	2.24E+9	782.4	40.1	3.00E+9	1046.1	42.8	3.76E+9
75	188.0	19.4	1.49E+9	321.2	22.0	2.24E+9	468.8	24.0	3.00E+9	628.3	25.7	3.76E+9
90	0.0	0.0	1.49E+9	0.0	0.0	2.24E+9	0.0	0.0	3.00E+9	0.0	0.0	3.76E+9

Aperture Radius [m]/[in] = 0.329 13
 Total Cavity Area [m²] = 1.380
 Total Heated Cavity Area [m²] = 1.037
 Total Refractory Cavity Area [m²] = 0.343

T mean [K]	422.0			477.6			533.2			588.7		
[°F]	300			400			500			600		
Angle [degrees]	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr	Q conv [Watts]	Nu	Gr
-90	915.2	147.1	4.63E+9	1566.2	169.3	6.88E+9	2298.3	187.1	9.14E+9	3097.6	202.3	1.14E+10
-75	881.9	141.8	4.63E+9	1513.3	163.6	6.88E+9	2225.1	181.1	9.14E+9	3003.6	196.1	1.14E+10
-60	1022.6	164.4	4.63E+9	1754.8	189.7	6.88E+9	2580.2	210.0	9.14E+9	3482.9	227.4	1.14E+10
-45	1090.0	175.2	4.63E+9	1877.9	203.0	6.88E+9	2768.9	225.4	9.14E+9	3746.0	244.6	1.14E+10
-30	1100.4	176.9	4.63E+9	1895.0	204.8	6.88E+9	2793.4	227.4	9.14E+9	3778.3	246.7	1.14E+10
-15	1042.5	167.6	4.63E+9	1794.7	194.0	6.88E+9	2644.8	215.3	9.14E+9	3576.5	233.5	1.14E+10
0	890.2	143.1	4.63E+9	1509.5	163.2	6.88E+9	2200.7	179.2	9.14E+9	2951.1	192.7	1.14E+10
15	797.1	128.1	4.63E+9	1352.1	146.1	6.88E+9	1971.8	160.5	9.14E+9	2644.8	172.7	1.14E+10
30	644.0	103.5	4.63E+9	1092.8	118.1	6.88E+9	1594.1	129.8	9.14E+9	2138.6	139.6	1.14E+10
45	426.4	68.5	4.63E+9	719.0	77.7	6.88E+9	1044.1	85.0	9.14E+9	1395.7	91.1	1.14E+10
60	283.0	45.5	4.63E+9	472.7	51.1	6.88E+9	681.7	55.5	9.14E+9	906.5	59.2	1.14E+10
75	170.3	27.4	4.63E+9	285.6	30.9	6.88E+9	413.1	33.6	9.14E+9	550.5	35.9	1.14E+10
90	0.0	0.0	4.63E+9	0.0	0.0	6.88E+9	0.0	0.0	9.14E+9	0.0	0.0	1.14E+10

APPENDIX 5: Koenig and Marvin Model Computer Program Listing

```

REM *****
REM
REM                                     Koenig and Marvin Model
REM *****
REM   The Koenig and Marvin method is used here to predict the convective losses from
REM   a cavity solar receiver operating at various temperatures and receiver angles.
REM *****
PRINT " Koenig and Marvin Model for Predicting Convective Heat Loss"
PRINT
PRINT
REM *****
REM ***** Receiver Geometry *****
Re=.127      :REM end plate radius [m]
Rc=.33       :REM cavity radius [m]
Ro=.45 :REM receiver outside radius [m]
Lf=.292      :REM frustum length [m]
Lh=.254      :REM cylinder length hot [m]
Lc=.14       :REM cylinder length cold [m]
REM *****
REM ***** Constants *****
pi=4*ATN(1)
g=9.810001   :REM gravitational acceleration [m/sec^2]
SB=5.6696E-08 :REM Stefan Boltzmann const. [W/m^2 K^4]
Cp=1006.86   :REM specific heat capacity of air at Ta [J/kg K]
Pf=1.19406   :REM density of air at Ta [kg/m^3]
e=.9         :REM emittance of cavity
ki=.04756    :REM insulation conductance [W/m-K] [.33B/h/ft^2/in]
t=.0889      :REM thickness of insulation [m] [3.5 in]
Ta=70        :REM ambient temperature [F]
Ta=(Ta+459.67)/1.8 :REM ambient temperature [K]
REM *****
REM open clipboard file for transferring data to spread sheet
OPEN "CLIP:" FOR OUTPUT AS #1
100 :
REM ***** Print Constants *****
REM
CLS
PRINT "End Plate Radius [m] = ";Re
PRINT "Cavity Radius [m] = ";Rc
PRINT "Frustum Length [m] = ";Lf
PRINT "Hot Cylindrical Section Length [m] = ";Lh
PRINT "Cold Cylindrical Section Length [m] = ";Lc
PRINT "Ambient Temperature [K] = ";
PRINT USING"####.#";Ta
PRINT
REM ***** Write to the clipboard *****
WRITE#1,"","End Plate Radius [m] = ",Re
WRITE#1,"","Cavity Radius [m] = ",Rc
WRITE#1,"","Frustum Length [m] = ",Lf
WRITE#1,"","Hot Cylindrical Section Length [m] = ",Lh
WRITE#1,"","Cold Cylindrical Section Length [m] = ",Lc
WRITE#1,"","Ambient Temperature [K] = ",Ta
WRITE#1,

```



```

REM ***** Receiver Aperture Radius Loop *****
FOR I=1 TO 4
CLS
  READ Ra
  DATA .0762,.1524,.2286,.329
  Da=2*Ra :REM aperture diameter [m]
  Aa=pi*Ra^2 :REM aperture area [m^2]
REM *****
REM ***** Area Constants *****
REM In the following section Ah and Ar are calculated.
REM Ah is the total interior heated cavity surface area based on the tube bundle
geometry.
REM Ar is the total interior refractory cavity surface.
REM At is the total cavity area.
  Ah=pi*(Re+Rc)*(Lf^2+(Rc-Re)^2)^.5+2 *pi*Rc*Lh
  Ar=pi*Re^2+pi*(Rc^2-Ra^2)+2*pi*Rc*Lc
  At=Ah+Ar
  Ao=pi*((Rc+Ro)/2)^2+2*pi*((Rc+Ro)/2)+pi*(Rc^2-Ra^2)
REM *****
REM ***** Print Header *****
REM
CLS
  PRINT "Aperture Radius [m] = ";Ra
  PRINT " Total Cavity Area [m^2] = ";
  PRINT USING "###.###";At
  PRINT " Total Heated Cavity Area [m^2] = ";
  PRINT USING "###.###";Ah
  PRINT " Total Refractory Cavity Area [m^2] = ";
  PRINT USING "###.###";Ar
REM ***** write header to clipboard *****
  WRITE#1, ",", "Aperture Radius [m] = ",Ra
  WRITE#1, ",", " Total Cavity Area [m^2] = ",At
  WRITE#1, ",", " Total Heated Cavity Area [m^2] = ",Ah
  WRITE#1, ",", " Total Refractory Cavity Area [m^2] = ",Ar
REM ***** Operating Temperature Loop *****
REM
  FOR Tmf=300 TO 600 STEP 100
  WRITE#1,
  REM The operating temperature is converted from F to K
  Tm=(Tmf+459.67)/1.8
  Twf=Tmf-100 :REM The refractory surfaces are assumed to be 100°F cooler
               :REM than the heated tube surfaces.
  Tw=(Twf+459.67)/1.8
  CLS
REM *****
REM ***** Print Table Header *****
  PRINT "T mean [K] = ";
  PRINT USING "###.##";Tm;
  PRINT " [°F] = ";
  PRINT USING "###.##";Tmf
PRINT
PRINT ;TAB(3);" Angle";TAB(12);"Q conv";TAB(24);"Q total";TAB(34);"% Conv";
PRINT TAB(45);" Nu ";TAB(56);"
Gr";TAB(66);"P(ø)";TAB(76);"k";TAB(86);"gB/v^2";TAB(96);"Pr
";TAB(106);"Tp"

```

```

PRINT ;TAB(1);" [degrees]";TAB(13);"[Watts]";TAB(24);"[Watts]";TAB(36);"%
PRINT
REM *****
REM ***** write table header to clipboard *****
WRITE#1,"", "T mean [K] = ",Tm
WRITE#1,"", " [°F] = ",Tmf
WRITE#1,
WRITE#1," Angle","Q conv","Q total","% Conv"," Nu "," Gr","P(ø)"
WRITE#1," [degrees]","[Watts]","[Watts]","%","","",""
WRITE#1,
REM ***** Beginning of Angle Loop *****
FOR a=0 TO 90 STEP 15
    z=pi*a/180 :REM convert angle to radian measure
    REM ***** Angle Function *****
    IF a>45 THEN 121
    P=(COS(z))^3.2
    GOTO 124
121 :
    IF a=90 THEN 122
    P=.707*(COS(z))^2.2
    GOTO 124
122 :
    P=0
124 :
    REM *****
    Tcav=(Tm*Ah+Tw*Ar)/At :REM area average cavity temperature [K]
    Lcc=Ra/Rc
    L=2^.5*Rc
    Tp=(11*Tcav+3*Ta)/16 :REM air properties temperature [K]
    C=1.1547E+19*Tp^-4.4187 :REM gB/v^2.
    k=.0071749261015#+.000064030639041#*Tp
    REM ***** Heat Loss Calculations *****
    Gr=C*(Tcav-Ta)*L^3 :REM Grashof number
    Pr=.7814008749#-.00037306809395#*Tp+5.2131644352D-07*Tp^2-2.
    1272705278D-10*Tp^3
    REM Pr = Prandtl number
    C1=.52
    a1=1.75
    Nu=C1*P*Lcc^a1*(Gr*Pr)^.25 :REM Nusselt number
    h=Nu*k/L :REM heat transfer coefficient [W/m^2 K]
    REM *****
    REM ***** heat loss calculations *****
    Qr=pi*Ra^2*e*SB*(Tcav^4-Ta^4) :REM radiative
    Qc=h*At*(Tcav-Ta) :REM convective
    Qk=ki*Ao*(Tcav-Ta)/t :REM conductive
    Qt=Qr+Qc+Qk
    PQc=Qc/Qt*100
    REM ***** Output Loop Results *****
    PRINT ;TAB(3);a;
    PRINT TAB(12);
    PRINT USING "####.#";Qc;
    PRINT;TAB(24);
    PRINT USING "####.#";Qt;
    PRINT TAB(34);
    PRINT USING "###.#";PQc;

```

```

PRINT TAB(44);
PRINT USING "###.##";Nu;
PRINT TAB(54);
PRINT USING "##.##^";Gr;
PRINT TAB(64);
PRINT USING "#.####";P;
PRINT TAB(74);
PRINT USING "#.####";k;
PRINT TAB(84);
PRINT USING "###.##^";C;
PRINT TAB(94);
PRINT USING "#.####";Pr;
PRINT TAB(104);
PRINT USING "####.#";Tp
REM ***** write to clipboard *****
WRITE#1,a,Qc,Qt,PQc,Nu,Gr,P
REM *****
REM ***** End of Angle Loop *****
NEXT a
REM *****
REM ***** Output Radiation & Conduction *****
PRINT"Radiation (Watts) = ";Qr
PRINT"Conduction (Watts) = ";Qk
REM ***** Write radiation & conduction to clipboard **
WRITE#1,"","Radiation (Watts) = ",Qr
WRITE#1,"","Conduction (Watts) = ",Qk
REM *****
REM ***** End of Temperature Loop *****
NEXT Tmf
REM *****
REM ***** End of Aperture Radius Loop *****
NEXT I
REM *****
CLOSE#1
END

```

Appendix 6: Koenig and Marvin Model Heat Loss

Appendix 6 Koenig and Marvin Heat Loss Data						
End Plate Radius [m] = 0.127						
Cavity Radius [m] = 0.33						
Frustum Length [m] = 0.292						
Hot Cylindrical Section Length [m] = 0.254						
Cold Cylindrical Section Length [m] = 0.14						
Ambient Temperature [K] = 294.3						
Aperture Radius [m] = 0.0762						
Total Cavity Area [m ²] = 1.7021						
Total Heated Cavity Area [m ²] = 1.0372						
Total Refractory Cavity Area [m ²] = 0.6648						
T mean [K] = 422.0						
[°F] = 790						
Angle [degrees]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	P(φ)
0	70.0	271.3	25.8	6.39	9.21E+8	1
15	62.7	264.2	23.7	5.72	9.21E+8	0.8949939
30	44.2	245.7	18.0	4.09	9.21E+8	0.6310997
45	23.1	224.6	10.3	2.11	9.21E+8	0.3298769
60	10.8	212.3	5.1	0.98	9.21E+8	0.1538698
75	2.3	204.0	1.2	0.23	9.21E+8	3.61E-02
90	0.0	201.3	0.0	0.00	9.21E+8	0
Radiation (Watts) = 16.9						
Conduction (Watts) = 184.6						
T mean [K] = 477.6						
[°F] = 890						
Angle [degrees]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	P(φ)
0	114.0	428.5	26.6	6.28	8.65E+8	1
15	102.0	416.5	24.5	5.62	8.65E+8	0.8949939
30	72.0	386.4	18.6	3.97	8.65E+8	0.6310997
45	37.6	352.1	10.7	2.07	8.65E+8	0.3298769
60	17.5	332.0	5.3	0.97	8.65E+8	0.1538698
75	4.1	318.6	1.3	0.23	8.65E+8	3.61E-02
90	0.0	314.4	0.0	0.00	8.65E+8	0
Radiation (Watts) = 33.2						
Conduction (Watts) = 281.2						
T mean [K] = 533.2						
[°F] = 990						
Angle [degrees]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	P(φ)
0	159.3	594.1	26.9	6.06	7.52E+8	1
15	142.8	577.4	24.7	5.43	7.52E+8	0.8949939
30	100.7	535.3	18.8	3.83	7.52E+8	0.6310997
45	52.6	487.2	10.8	2.00	7.52E+8	0.3298769
60	24.5	459.1	5.3	0.93	7.52E+8	0.1538698
75	5.8	448.4	1.3	0.22	7.52E+8	3.61E-02
90	0.0	434.6	0.0	0.00	7.52E+8	0
Radiation (Watts) = 56.7						
Conduction (Watts) = 377.9						
T mean [K] = 588.7						
[°F] = 1090						
Angle [degrees]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	P(φ)
0	206.1	769.8	26.8	5.81	6.35E+8	1
15	184.4	748.2	24.7	5.20	6.35E+8	0.8949939
30	130.1	693.8	18.7	3.67	6.35E+8	0.6310997
45	68.0	631.7	10.8	1.92	6.35E+8	0.3298769
60	31.7	595.5	5.3	0.89	6.35E+8	0.1538698
75	7.4	571.2	1.3	0.21	6.35E+8	3.61E-02
90	0.0	563.8	0.0	0.00	6.35E+8	0
Radiation (Watts) = 89.2						
Conduction (Watts) = 474.5						

Appendix 6: Koenig and Marvin Model Heat Loss

Average Radps [W] = 81373						
Total Cavity Area [m ²] = 1.50372						
Total Heated Cavity Area [m ²] = 1.50372						
Total Refractory Cavity Area [m ²] = 0.6101						
T _{mean} [K] = 422.0						
[°F] = 300						
Angle	Q _{conv}	Q _{total}	% Conv	Nu	Gr	P(e)
[degrees]	[Watts]	[Watts]	%			
0	230.8	483.0	47.8	31.49	9.21E+8	1
15	206.6	458.8	45.0	32.4	9.21E+8	8949039
30	145.7	397.9	36.6	35.6	9.21E+8	6310997
45	76.1	328.3	23.2	7.00	9.21E+8	3298769
60	35.5	287.7	12.3	3.31	9.21E+8	1538698
75	8.3	260.5	3.2	0.78	9.21E+8	6.61E-02
90	0.0	252.2	0.0	0.00	9.21E+8	0
Radiation (Watts) = 68.8						
Conduction (Watts) = 183.4						
T _{mean} [K] = 477.6						
[°F] = 400						
Angle	Q _{conv}	Q _{total}	% Conv	Nu	Gr	P(e)
[degrees]	[Watts]	[Watts]	%			
0	374.1	787.0	47.5	21.12	8.63E+8	1
15	334.8	747.7	44.8	28.91	8.63E+8	8949039
30	236.1	649.6	36.4	33.3	8.63E+8	6310997
45	123.4	536.3	23.0	6.97	8.63E+8	3298769
60	57.6	470.5	12.3	3.25	8.63E+8	1538698
75	13.5	426.4	3.2	0.76	8.63E+8	6.61E-02
90	0.0	412.9	0.0	0.00	8.63E+8	0
Radiation (Watts) = 194.5						
Conduction (Watts) = 278.4						
T _{mean} [K] = 523.2						
[°F] = 500						
Angle	Q _{conv}	Q _{total}	% Conv	Nu	Gr	P(e)
[degrees]	[Watts]	[Watts]	%			
0	522.4	1124.9	46.4	30.37	7.50E+8	1
15	467.5	1070.1	43.7	22.3	7.50E+8	8949039
30	329.7	932.2	35.4	28.6	7.50E+8	6310997
45	172.3	774.9	22.2	6.72	7.50E+8	3298769
60	80.4	682.9	11.8	3.13	7.50E+8	1538698
75	18.9	631.4	3.0	0.74	7.50E+8	6.61E-02
90	0.0	603.6	0.0	0.00	7.50E+8	0
Radiation (Watts) = 229.1						
Conduction (Watts) = 373.4						
T _{mean} [K] = 588.7						
[°F] = 600						
Angle	Q _{conv}	Q _{total}	% Conv	Nu	Gr	P(e)
[degrees]	[Watts]	[Watts]	%			
0	674.0	1502.4	44.9	35.2	6.33E+8	1
15	603.2	1431.6	42.1	24.7	6.33E+8	8949039
30	425.3	1253.8	33.9	23.2	6.33E+8	6310997
45	222.3	1050.8	21.2	6.44	6.33E+8	3298769
60	103.7	932.1	11.1	3.00	6.33E+8	1538698
75	24.4	852.8	2.9	0.71	6.33E+8	6.61E-02
90	0.0	828.4	0.0	0.00	6.33E+8	0
Radiation (Watts) = 350.0						
Conduction (Watts) = 458.5						

Appendix 6: Koenig and Marvin Model Heat Loss

Aperture Radius (m) = 1286						
Total Cavity Area (m ²) = 15361						
Total Heated Cavity Area (m ²) = 10372						
Total Refractory Cavity Area (m ²) = 1589						
T _{mean} [K] = 4220						
[°F] = 300						
Angle (degrees)	Q _{conv} (Watt)	Q _{total} (Watt)	% Conv	Nu	Gr	P(θ)
0	4532	7941	57.1	8.70	8.21E+8	1
13	4056	7483	54.3	8.11	8.21E+8	0.8949939
30	2860	6269	46.6	7.38	8.21E+8	0.6310997
45	1495	4983	30.5	6.42	8.21E+8	0.3298769
60	697	4106	17.0	6.72	8.21E+8	0.158698
75	164	357.2	4.6	1.58	8.21E+8	3.61E-02
90	0.0	340.8	0.0	0.00	8.21E+8	0
Radiation (Watt) = 3593						
Conduction (Watt) = 2818						
T _{mean} [K] = 4776						
[°F] = 400						
Angle (degrees)	Q _{conv} (Watt)	Q _{total} (Watt)	% Conv	Nu	Gr	P(θ)
0	7289	13720	53.6	12.30	8.60E+8	1
13	6323	12384	51.8	11.40	8.60E+8	0.8949939
30	4600	10461	44.1	10.07	8.60E+8	0.6310997
45	2404	8236	29.2	9.15	8.60E+8	0.3298769
60	1121	6953	16.1	6.60	8.60E+8	0.158698
75	263	6083	4.3	1.35	8.60E+8	3.61E-02
90	0.0	583.1	0.0	0.00	8.60E+8	0
Radiation (Watt) = 6592						
Conduction (Watt) = 2739						
T _{mean} [K] = 5332						
[°F] = 500						
Angle (degrees)	Q _{conv} (Watt)	Q _{total} (Watt)	% Conv	Nu	Gr	P(θ)
0	1013.9	1904.9	53.2	11.35	2.43E+8	1
13	907.4	1798.4	50.5	10.02	2.43E+8	0.8949939
30	639.9	1330.8	48.8	8.60	2.43E+8	0.6310997
45	334.3	1225.4	27.3	8.64	2.43E+8	0.3298769
60	156.0	1040.0	14.9	6.36	2.43E+8	0.158698
75	36.6	927.6	4.0	1.49	2.43E+8	3.61E-02
90	0.0	891.0	0.0	0.00	2.43E+8	0
Radiation (Watt) = 8248						
Conduction (Watt) = 3662						
T _{mean} [K] = 5887						
[°F] = 500						
Angle (degrees)	Q _{conv} (Watt)	Q _{total} (Watt)	% Conv	Nu	Gr	P(θ)
0	1305.2	2585.3	50.5	10.62	5.29E+8	1
13	1168.2	2449.3	47.7	10.46	5.29E+8	0.8949939
30	823.7	2104.8	39.1	9.00	5.29E+8	0.6310997
45	430.6	1711.7	25.2	8.09	5.29E+8	0.3298769
60	200.8	1482.0	13.6	6.10	5.29E+8	0.158698
75	47.2	1328.3	3.6	1.43	5.29E+8	3.61E-02
90	0.0	1281.1	0.0	0.00	5.29E+8	0
Radiation (Watt) = 822.6						
Conduction (Watt) = 583						

Appendix 6: Koenig and Marvin Model Heat Loss

Aperture Radius (m) = 0.329						
Total Cavity Area (m ²) = 1.3803						
Total Heated Cavity Area (m ²) = 1.0372						
Total Refractory Cavity Area (m ²) = 0.3430						
T _{mean} [K] = 1422.0						
[°F] = 2600						
Angle (degrees)	Q _{conv} (Watts)	Q _{total} (Watts)	% Conv %	Nu	Gr	P(σ)
0	798.6	1329.1	60.1	82.62	9.21E+8	1
15	714.8	1245.3	57.4	73.94	9.21E+8	0.8949939
30	504.0	1034.5	48.7	52.14	9.21E+8	0.6310997
45	263.5	793.9	33.2	27.25	9.21E+8	0.3298769
60	122.9	653.4	18.8	12.71	9.21E+8	0.1538698
75	28.9	530.5	5.2	2.39	9.21E+8	3.61E-02
90	0.0	530.5	0.0	0.00	9.21E+8	0
Radiation (Watts) = 351.8						
Conduction (Watts) = 178.7						
T _{mean} [K] = 1477.6						
[°F] = 2690						
Angle (degrees)	Q _{conv} (Watts)	Q _{total} (Watts)	% Conv %	Nu	Gr	P(σ)
0	1262.6	2201.1	57.4	80.91	8.51E+8	1
15	1130.1	2068.5	54.6	72.42	8.51E+8	0.8949939
30	796.9	1735.3	45.9	51.06	8.51E+8	0.6310997
45	416.5	1355.0	30.7	26.69	8.51E+8	0.3298769
60	194.3	1132.8	17.2	12.43	8.51E+8	0.1538698
75	45.6	984.1	4.6	2.32	8.51E+8	3.61E-02
90	0.0	984.1	0.0	0.00	8.51E+8	0
Radiation (Watts) = 672.7						
Conduction (Watts) = 265.8						
T _{mean} [K] = 1543.2						
[°F] = 2800						
Angle (degrees)	Q _{conv} (Watts)	Q _{total} (Watts)	% Conv %	Nu	Gr	P(σ)
0	1741.8	3226.8	54.0	77.94	7.35E+8	1
15	1538.9	2843.9	51.2	69.78	7.35E+8	0.8949939
30	1099.3	2584.3	42.5	49.19	7.35E+8	0.6310997
45	574.6	2059.6	27.9	25.71	7.35E+8	0.3298769
60	268.0	1753.0	15.3	11.99	7.35E+8	0.1538698
75	63.0	1548.0	4.1	2.82	7.35E+8	3.61E-02
90	0.0	1485.0	0.0	0.00	7.35E+8	0
Radiation (Watts) = 1132.2						
Conduction (Watts) = 352.9						
T _{mean} [K] = 1588.7						
[°F] = 2880						
Angle (degrees)	Q _{conv} (Watts)	Q _{total} (Watts)	% Conv %	Nu	Gr	P(σ)
0	2231.2	4436.4	50.3	74.64	6.20E+8	1
15	1998.9	4202.1	47.5	66.80	6.20E+8	0.8949939
30	1408.1	3613.4	39.0	47.10	6.20E+8	0.6310997
45	736.0	2941.3	25.0	24.62	6.20E+8	0.3298769
60	343.3	2548.6	13.5	11.48	6.20E+8	0.1538698
75	80.6	2283.9	3.5	2.70	6.20E+8	3.61E-02
90	0.0	2205.3	0.0	0.00	6.20E+8	0
Radiation (Watts) = 1765.3						
Conduction (Watts) = 440.0						

Appendix 7: Zone and Shear Plane Area Formulas

1. Zone Area Formulas

The receiver cavity is divided into two zones (Fig. 23). The boundary between the zones is formed by a horizontal plane cutting through the cavity at the upper lip of the aperture. The upper zone is assumed stagnate while the lower zone has active convective currents. Zone 1 area represents the internal surface area of the receiver above the horizontal plane. The zone 2 area represents the internal surface area of the receiver below the horizontal plane. The zone 1 and zone 2 areas vary with receiver angle for a given receiver geometry. The following formulas describe the zone 1 and zone 2 surface areas of the receiver cavity

Figure 23. Cavity zones areas.

The receiver internal geometry is divided into five sections representing the hot and cold surfaces in the receiver (Fig. 24). The hot surfaces are actively heated. The cold surfaces represent the refractory surfaces. Section 1 is the circular plate at the end of the frustum. Section 2 is the frustum portion of the tube bundle. Section 3 is the cylindrical portion of the tube bundle. Section 4 is the short refractory portion of the cylindrical section. Section 5 is the refractory ring that forms the aperture.

Figure 24. Cavity sections.

As the receiver is rotated through various angles, each section of the internal receiver geometry may be divided by the horizontal plane that cuts through the upper inside edge of section 5. The critical angles represent limits for the various algebraic expression of the zone areas (Fig. 69). The following formulas define the portion of the area of each section that is in zone 1 for a given receiver angle range. The remaining surface area of each section in zone 2 is determined by subtracting the zone 1 area from the total surface area for that section.

Figure 69. Critical angles.

where:

$$\varnothing_1 = \tan^{-1} \left[\frac{R_a - R_e}{l_{cc} + l_{hc} + l_f} \right] \quad (115)$$

$$\varnothing_2 = \tan^{-1} \left[\frac{R_a + R_e}{l_{cc} + l_{hc} + l_f} \right] \quad (116)$$

$$\varnothing_3 = \tan^{-1} \left[\frac{R_a + R_c}{l_{cc} + l_{hc}} \right] \quad (117)$$

$$\varnothing_4 = \tan^{-1} \left[\frac{R_a + R_c}{l_{cc}} \right] \quad (118)$$

where:

R_e = radius of the end plate

(a) section 1

Range $0 \leq \emptyset \leq \emptyset_1$

$$\text{Area} = 0$$

Range $\emptyset_1 \leq \emptyset \leq \emptyset_2$

$$\text{Area} = R_e^2 \cos^{-1} \left[\frac{R_a - (\ell_{cc} + \ell_{hc} + \ell_f) \tan \emptyset}{R_e} \right] + [(\ell_{cc} + \ell_{hc} + \ell_f) \tan \emptyset - R_a]$$

$$\left\{ 2R_e [(\ell_{cc} + \ell_{hc} + \ell_f) \tan \emptyset - R_a + R_e] - [(\ell_{cc} + \ell_{hc} + \ell_f) \tan \emptyset - R_a + R_e]^2 \right\}^{1/2} \quad (119)$$

Range $\emptyset_2 \leq \emptyset \leq \frac{\pi}{2}$

$$\text{Area} = \pi R_e^2 \quad (120)$$

(b) section 2

Range $0 \leq \emptyset \leq \emptyset_1$

$$\text{Area} = \left\{ \frac{\left[\left(\frac{R_c - R_e}{\ell_f} \right) (R_c - R_a) + (\ell_{cc} + \ell_{hc}) \right] \sin \emptyset}{\sin \left[\frac{\pi}{2} - \emptyset - \tan^{-1} \left(\frac{R_c - R_e}{\ell_f} \right) \right]} + \frac{(R_c - R_a)}{\sin \left[\tan^{-1} \left(\frac{R_c - R_e}{\ell_f} \right) \right]} \right\}$$

$$R_c \cos^{-1} \left[\frac{R_a - (\ell_{cc} + \ell_{hc}) \tan \emptyset}{R_c} \right] \quad (121)$$

$$\text{Range } \emptyset_1 \leq \emptyset \leq \emptyset_2$$

$$\begin{aligned} \text{Area} = & \sqrt{\ell_f^2 + (R_c - R_e)^2} \left\{ R_e \cos^{-1} \left[\frac{R_a - (\ell_{cc} + \ell_{hc} + \ell_f) \tan \emptyset}{R_e} \right] \right. \\ & \left. + R_c \cos^{-1} \left[\frac{R_a - (\ell_{cc} + \ell_{hc}) \tan \emptyset}{R_c} \right] \right\} \end{aligned} \quad (122)$$

$$\text{Range } \emptyset_2 \leq \emptyset \leq \emptyset_3$$

$$\begin{aligned} \text{Area} = & \left\{ \pi R_e + \pi \left\{ R_e + a \sin \left[\tan^{-1} \left(\frac{R_c - R_e}{\ell_f} \right) \right] \right\} \right\} a \\ & + \left\{ R_c \cos^{-1} \left[\frac{R_a - (\ell_{cc} + \ell_{hc}) \tan \emptyset}{R_c} \right] + \pi \left\{ R_e + a \sin \left[\tan^{-1} \left(\frac{R_c - R_e}{\ell_f} \right) \right] \right\} \right\} \\ & \left[\sqrt{(R_c - R_e)^2 + \ell_f^2} - a \right] \end{aligned} \quad (123)$$

where:

$$a = \left\{ \frac{\sqrt{(R_e + R_a)^2 + (\ell_{cc} + \ell_{hc} + \ell_f)^2} \sin \left[\emptyset - \tan^{-1} \left(\frac{R_a + R_e}{\ell_{cc} + \ell_{hc} + \ell_f} \right) \right]}{\sin \left[\pi - \emptyset - \tan^{-1} \left(\frac{R_c - R_e}{\ell_f} \right) \right]} \right\} \quad (124)$$

$$\text{Range } \emptyset_3 \leq \emptyset \leq \frac{\pi}{2}$$

$$\text{Area} = \pi (R_c + R_e) \sqrt{(R_c - R_e)^2 + \ell_f^2} \quad (125)$$

(c) section 3

$$\text{Range } 0 \leq \emptyset \leq \emptyset_3$$

$$\text{Area} = R_c \ell_{hc} \left\{ \cos^{-1} \left[\frac{R_a - \ell_{cc} \tan \varnothing}{R_c} \right] + \cos^{-1} \left[\frac{R_a - (\ell_{cc} + \ell_{hc}) \tan \varnothing}{R_c} \right] \right\} \quad (126)$$

$$\text{Range} \quad \varnothing_3 \leq \varnothing \leq \varnothing_4$$

$$\begin{aligned} \text{Area} &= 2 \pi R_c \left[\ell_{cc} + \ell_{hc} - \frac{(R_a + R_c)}{\tan \varnothing} \right] \\ &+ R_c \left[\frac{(R_a + R_c)}{\tan \varnothing} - \ell_{cc} \right] \left\{ \pi + \cos^{-1} \left[\frac{R_a - \ell_{cc} \tan \varnothing}{R_c} \right] \right\} \end{aligned} \quad (127)$$

$$\text{Range} \quad \varnothing_4 \leq \varnothing \leq \frac{\pi}{2}$$

$$\text{Area} = 2 \pi R_c \ell_{hc} \quad (128)$$

(d) section 4

$$\text{Range} \quad 0 \leq \varnothing \leq \varnothing_4$$

$$\text{Area} = R_c \ell_{cc} \left\{ \cos^{-1} \left[\frac{R_a}{R_c} \right] + \cos^{-1} \left[\frac{R_a - \ell_{cc} \tan \varnothing}{R_c} \right] \right\} \quad (129)$$

$$\text{Range} \quad \varnothing_4 \leq \varnothing \leq \frac{\pi}{2}$$

$$\text{Area} = 2 \pi R_c \left[\ell_{cc} - \frac{(R_a + R_c)}{\tan \varnothing} \right] + R_c \left\{ \pi + \cos^{-1} \left[\frac{R_a}{R_c} \right] \right\} \frac{(R_a + R_c)}{\tan \varnothing} \quad (130)$$

(e) section 5

$$\text{Range} \quad 0 \leq \varnothing \leq \frac{\pi}{2}$$

$$\text{Area} = R_c^2 \cos^{-1} \left[\frac{R_a}{R_c} \right] - R_a \sqrt{R_c^2 - R_a^2} \quad (131)$$

$$\text{Range} \quad \varnothing = \frac{\pi}{2}$$

$$\text{Area} = \pi (R_c^2 - R_a^2) \quad (132)$$

2. Shear Plane Area

The shear plane area is the area of the horizontal plane within the cavity (Fig. 25). The shear plane area is divided into two sections. The first section is formed by the horizontal plane cutting through the cylindrical portion of the receiver cavity. Not all of the horizontal plane in the cylindrical portion participates in the convective heat loss. The sides of the aperture reduce the effective shear plane area by restricting flow along the horizontal plane at the sides of the cavity near the aperture. The shear plane expands parabolically from the upper lip of the aperture in the horizontal plane. The second section is formed where the horizontal plane cuts the frustum portion of the receiver cavity. The following formulas describe the shear plane area in the specified portion of the cavity for a given receiver angle

Figure 25. View looking down showing the effective shear plane area.

(a) Shear Plane Area -cylindrical section

Figure 70. Cylindrical section shear plane angles.

The angles in figure 70 are defined as follows:

$$\varnothing_1 = \tan^{-1} \left[\frac{R_a}{l_{cc} + l_{hc}} \right] \quad (133)$$

$$\varnothing_2 = \tan^{-1} \left[\frac{R_a + R_c}{l_{cc} + l_{hc}} \right] \quad (134)$$

Range $0 \leq \varnothing \leq \varnothing_1$

$$D = \frac{(l_{cc} + l_{hc})}{\cos \varnothing} \quad (135)$$

$$L = 2\sqrt{R_c^2 - R_a^2} \quad (136)$$

$$L_e = 2\sqrt{R_c^2 - [R_a - (l_{cc} + l_{hc}) \tan \varnothing]^2} \quad (137)$$

- (151) $Area_{shear} = \frac{3}{2D} [L^2 + L L_e + L_e^2] + \frac{3}{2D^*} [L^{*2} + L^* L_e^* + L_e^{*2}]$
- (150) $D^* = \frac{R_c}{\sin \emptyset}$
- (149) $L_e^* = 0$
- (148) $L^* = 2R_c$
- (147) $D = \frac{R_a}{\sin \emptyset}$
- (146) $L_e = 2R_c$
- (145) $L = 2\sqrt{R_a^2 - R_c^2}$
- Range $\emptyset_2 \leq \emptyset \leq \frac{\pi}{2}$
- (144) $Area_{shear} = \frac{3}{2D} [L^2 + L L_e + L_e^2] + \frac{3}{2D^*} [L^{*2} + L^* L_e^* + L_e^{*2}]$
- (143) $D^* = \frac{\sin \emptyset}{(\lambda_{cc} + \lambda_{hc}) \tan \emptyset - R_a}$
- (142) $L_e^* = \frac{2\sqrt{R_a^2 - [R_a - (\lambda_{cc} + \lambda_{hc}) \tan \emptyset]^2}}{2}$
- (141) $D = \frac{R_a}{\sin \emptyset}$
- (140) $L_e = 2R_c$
- (139) $L = 2\sqrt{R_a^2 - R_c^2}$
- Range $\emptyset_1 \leq \emptyset \leq \emptyset_2$
- (138) $Area_{shear} = \frac{3}{2D} [L^2 + L L_e + L_e^2]$

Shear Plane Area -frustum section

Figure 71. Frustum section shear plane angles.

The angles in figure 71 are defined as follows:

$$\varnothing_1 = \tan^{-1} \left[\frac{R_a - R_e}{l_{cc} + l_{hc} + l_f} \right] \quad (152)$$

$$\varnothing_2 = \tan^{-1} \left[\frac{R_a + R_e}{l_{cc} + l_{hc} + l_f} \right] \quad (153)$$

$$\varnothing_3 = \tan^{-1} \left[\frac{R_a + R_c}{l_{cc} + l_{hc}} \right] \quad (154)$$

Range $0 \leq \varnothing \leq \varnothing_1$

$$L = 2\sqrt{R_c^2 - [R_a - (l_{cc} + l_{hc}) \tan \varnothing]^2} \quad (155)$$

$L_e = 0$

$$D = \frac{l_f [R_c + (l_{cc} + l_{hc}) \tan \varnothing - R_a]}{(R_c - R_e) \cos \varnothing - l_f \sin \varnothing} \quad (156)$$

$$\text{Area}_{\text{shear}} = \frac{2D}{3} \left[\frac{L^2 + LL_e + L_e^2}{L + L_e} \right] \quad (157)$$

$$\text{Range } \emptyset_1 \leq \emptyset \leq \emptyset_2$$

$$L = 2\sqrt{R_c^2 - [R_a - (\ell_{cc} + \ell_{hc}) \tan \emptyset]^2} \quad (158)$$

$$L_e = 2\sqrt{R_e^2 - [R_a - (\ell_{cc} + \ell_{hc} + \ell_f) \tan \emptyset]^2} \quad (159)$$

$$D = \frac{\ell_f}{\cos \emptyset} \quad (160)$$

$$\text{Area}_{\text{shear}} = \frac{2D}{3} \left[\frac{L^2 + LL_e + L_e^2}{L + L_e} \right] \quad (161)$$

$$\text{Range } \emptyset_2 \leq \emptyset \leq \emptyset_3$$

$$L = 2\sqrt{R_c^2 - [R_a - (\ell_{cc} + \ell_{hc}) \tan \emptyset]^2} \quad (162)$$

$$L_e = 0$$

$$D = \frac{\ell_f [R_c - (\ell_{cc} + \ell_{hc}) \tan \emptyset + R_a]}{(R_c - R_e) \cos \emptyset + \ell_f \sin \emptyset} \quad (163)$$

$$\text{Area}_{\text{shear}} = \frac{2D}{3} \left[\frac{L^2 + LL_e + L_e^2}{L + L_e} \right] \quad (164)$$

$$\text{Range } \emptyset_3 \leq \emptyset \leq \frac{\pi}{2}$$

$$\text{Area}_{\text{shear}} = 0 \quad (165)$$

The total shear area in the cavity at any one angle is the sum of the shear areas of the cylindrical section and the frustum section.

Appendix 8: Clausings's Model Computer Program Listing

```

REM                                     *****
REM
REM                                     Clausings's Method
REM      5 sections program w/ shear plane area
REM                                     *****
REM      The Clausings method is used here to predict the convective, radiative,
REM      and conductive losses from a cavity solar receiver operating at various
REM      temperatures and receiver angles.
REM                                     *****
      PRINT " Clausings's Method of Predicting Heat Losses"
      PRINT
      PRINT
REM                                     *****
REM      The program allows some variations in receiver geometry. These
REM      variables are inputted in this section of the program.
REM                                     *****
REM      ***** Receiver Geometry *****
Re=.127          :REM end plate radius [m]
Rc=.33           :REM cavity radius [m]
Lf=.292          :REM frustum length [m]
Lh=.254          :REM cylinder length hot [m]
Lc=.14           :REM cylinder length cold [m]
REM                                     *****
REM      ***** Constants *****
pi=4*ATN(1)
g=9.810001       :REM gravitational acceleration [m/sec^2]
SB=5.6696E-08    :REM Stefan Boltzmann const. [W/m^2 K^4]
Cp=1006.86       :REM specific heat capacity of air at Ta [J/kg K]
Pf=1.19406       :REM density of air at Ta [kg/m^3]
e=1              :REM emittance of cavity
ki=.04756        :REM insulation conductance [W/m-K] [.33B/h/ft^2/in]
ti=.0889         :REM thickness of insulation [m] [3.5 in]
Ta=70            :REM ambient temperature [F]
Ta=(Ta+459.67)/1.8 :REM ambient temperature [K]
REM                                     *****
Pflag=0
INPUT "Do you want a hard copy ";Q$
IF LEFT$(Q$,1)="y" THEN 50
IF LEFT$(Q$,1)="Y" THEN 50
Pflag=1
50 :
REM      open clipboard file for transferring data to spread sheet
OPEN "CLIP:" FOR OUTPUT AS #1
100 :
IF Pflag=1 THEN 55
REM      ***** Print Constants *****
REM
CLS
LPRINT "End Plate Radius [m] = ";Re
LPRINT "Cavity Radius [m] = ";Rc
LPRINT "Frustum Length [m] = ";Lf
LPRINT "Hot Cylindrical Section Length [m] = ";Lh
LPRINT "Cold Cylindrical Section Length [m] = ";Lc

```

```

LPRINT "Ambient Temperature [K] = ";
LPRINT USING"####.##";Ta
LPRINT
55 :
REM ***** Write to the clipboard *****
WRITE#1,"","End Plate Radius [m] = ",Re
WRITE#1,"","Cavity Radius [m] = ",Rc
WRITE#1,"","Frustum Length [m] = ",Lf
WRITE#1,"","Hot Cylindrical Section Length [m] = ",Lh
WRITE#1,"","Cold Cylindrical Section Length [m] = ",Lc
WRITE#1,"","Ambient Temperature [K] = ",Ta
WRITE#1,
REM ***** Receiver Aperture Radius Loop *****
FOR I=1 TO 4
IF Pflag=1 THEN 58
LPRINT CHR$(12)
58 :
READ Ra
DATA .0762,.1524,.2286,.329
Da=2*Ra :REM aperture diameter [m]
Aa=pi*Ra^2 :REM aperture area [m^2]
REM *****
REM ***** Angle Limits *****
REM In this section the 3 angle limits, z1, z2, z3, and z4 are calculated.
z1=ATN((Ra-Re)/(Lf+Lc+Lh)) :p1=z1*180/pi
z2=ATN((Ra+Re)/(Lf+Lc+Lh)) :p2=z2*180/pi
z3=ATN((Ra+Rc)/(Lc+Lh)) :p3=z3*180/pi
z4=ATN((Ra+Rc)/Lc) :p4=z4*180/pi
z5=ATN(Ra/(Lc+Lh)) :p5=z5*180/pi
REM *****
REM ***** Area Constants *****
REM In the following section Ah and Ac are calculated.
REM Ah is the total interior heated cavity surface area based on the tube bundle
geometry.
REM Ar is the total interior refractory cavity surface.
REM Aha is the interior heated cavity surface area is zone 2, the convective zone.
REM Ara is the interior refractory cavity surface area is zone 2, the convective zone.
REM AT is the total cavity area.
Ah=pi*(Re+Rc)*(Lf^2+(Rc-Re)^2)^.5+2 *pi*Rc*Lh
Ar=pi*Re^2+pi*(Rc^2-Ra^2)+2*pi*Rc*Lc
AT=Ah+Ar
REM Aha and Aca are functions of the receiver angle and are determined by
REM calculating the heated and refractory areas in zone 1, above the
REM horizontal plane, and then subtracting these values from their
REM respective total areas.
REM *****
IF Pflag=1 THEN 60
REM ***** Print Header *****
REM
CLS
LPRINT "Aperture Radius [m] = ";Ra
LPRINT " Total Cavity Area [m^2] = ";
LPRINT USING "####.####";AT
LPRINT " Total Heated Cavity Area [m^2] = ";
LPRINT USING "####.####";Ah

```

```

LPRINT " Total Refractory Cavity Area [m^2] = ";
LPRINT USING "###.###";Ar
60 :
REM ***** write header to clipboard *****
WRITE#1, "", "Aperture Radius [m] = ", Ra
WRITE#1, "", " Total Cavity Area [m^2] = ", AT
WRITE#1, "", " Total Heated Cavity Area [m^2] = ", Ah
WRITE#1, "", " Total Refractory Cavity Area [m^2] = ", Ar
REM ***** Operating Temperature Loop *****
REM
FOR Tmf=300 TO 600 STEP 100
WRITE#1,
REM The operating temperature is converted from F to K
Tm=(Tmf+459.67)/1.8
Twf=Tmf-100 :REM The refractory surfaces are assumed to be 100°F cooler
:REM than the heated tube surfaces.
Tw=(Twf+459.67)/1.8
CLS
REM *****
IF Pflag=1 THEN 62
REM ***** Print Table Header *****
LPRINT "T mean [K] = ";
LPRINT USING "###.##";Tm;
LPRINT " [°F] = ";
LPRINT USING "###.##";Tmf
LPRINT
LPRINT ;TAB(3);" Angle";TAB(12);"Tube Area";TAB(22);"Refrac. Area";TAB(34);"Q
conv";
LPRINT;TAB(44);"Q total";TAB(54);"% Conv";TAB(65);" Nu ";TAB(76);"
Gr";TAB(87);" Ashear"
LPRINT ;TAB(1);"
[degrees]";TAB(13);"[m^2]";TAB(23);"[m^2]";TAB(34);"[Watts]" ;
LPRINT;TAB(44);"[Watts]";TAB(56);"%";TAB(88);"[m^2]"
LPRINT
REM *****
62 :
REM ***** write table header to clipboard *****
WRITE#1, "", "T mean [K] = ", Tm
WRITE#1, "", " [°F] = ", Tmf
WRITE#1,
WRITE#1, " Angle", "Tube Area", "Refrac. Area", "Q conv", "Q total", "% Conv", " Nu ",
Gr, "Ashear"
WRITE#1, " [degrees]", "[m^2]", "[m^2]", "[Watts]", "[Watts]", "%", "", "[m ^2]"
WRITE#1,
REM ***** Beginning of Angle Loop *****
FOR A=0 TO 90 STEP 15
z=pi*A/180
REM ***** Zone Areas *****
REM The receiver cavity is divided into 5 sections to accommodate the
REM zone area calculations. The sections are defined as follows;
REM section 1 = end plate
REM section 2 = frustum
REM section 3 = hot cylinder
REM section 4 = cold cylinder
REM section 5 = ring

```

```

REM      AZ1 = area of section 1 in zone 1
REM      AZ2 = area of section 2 in zone 1
REM      AZ3 = area of section 3 in zone 1
REM      AZ4 = area of section 4 in zone 1
REM      AZ5 = area of section 5 in zone 1
REM      *****SECTION 1*****
      IF z>z1 THEN 101
      AZ1=0
      GOTO 201
101 :
      IF z>z2 THEN 102
      x=(Ra-(Lf+Lc+Lh)*TAN(z))/Rc
      cx=-ATN(x/SQR(-x*x+1))+1.5708
      m=(Lf+Lc+Lh)*TAN(z)-Ra+Re
      AZ1=Re^2*cx+((Lf+Lc+Lh)*TAN(z)-Ra)*SQR(2*Re*m-m^2)
      GOTO 201
102 :
      AZ1=pi*Re^2
201 :
      *****SECTION 2*****
      IF z>z1 THEN 202
      x=(Ra-(Lc+Lh)*TAN(z))/Rc
      cx=-ATN(x/SQR(-x*x+1))+1.5708
      m=ATN((Rc-Re)/Lf)
      AZ2=((Rc-Re)/Lf)*(Rc-Ra)+Lc+Lh)*SIN(z)/SIN(pi/2-z-m)
      AZ2=(AZ2+(Rc-Ra)/SIN(m))*Rc*cx
      GOTO 251
202 :
      IF z>z2 THEN 203
      x1=(Ra-(Lc+Lf+Lh)*TAN(z))/Re
      cx1=-ATN(x1/SQR(-x1*x1+1))+1.5708
      x2=(Ra-(Lc+Lh)*TAN(z))/Rc
      cx2=-ATN(x2/SQR(-x2*x2+1))+1.5708
      AZ2=SQR(Lf^2+(Rc-Re)^2)*(Re*cx1+Rc*cx2)
      GOTO 251
203 :
      IF z>z3 THEN 204
      m=ATN((Rc-Re)/Lf)
      n=ATN((Ra+Re)/(Lc+Lf+Lh))
      l=SQR((Lc+Lf+Lh)^2+(Ra+Re)^2)*SIN(z-n)/SIN(pi-z-m)
      x=(Ra-(Lc+Lh)*TAN(z))/Rc
      cx=-ATN(x/SQR(-x*x+1))+1.5708
      AZ2=(pi*Re+pi*(Re+l*SIN(m)))*l
      AZ2=AZ2+(Rc*cx+pi*(Re+l*SIN(m)))*(SQR(Lf^2+(Rc-Re)^2)-l)
      GOTO 251
204 :
      AZ2=pi*(Re+Rc)*SQR(Lf^2+(Rc-Re)^2)
251 :
      *****SECTION 3*****
      IF z>z4 THEN 253
      IF z>z3 THEN 252
      x1=(Ra-Lc*TAN(z))/Rc
      x2=(Ra-(Lc+Lh)*TAN(z))/Rc
      cx1=-ATN(x1/SQR(-x1*x1+1))+1.5708
      cx2=-ATN(x2/SQR(-x2*x2+1))+1.5708

```

```

    AZ3=Rc*(cx1+cx2)*Lh
GOTO 301
252 :
    m=(Ra+Rc)/TAN(z)
    x=(Ra-Lc*TAN(z))/Rc
    cx=-ATN(x/SQR(-x*x+1))+1.5708
    AZ3=2*pi*Rc*(Lh+Lc-m)+Rc*(m-Lc)*(pi+cx)
    GOTO 301
253 :
    AZ3=2*pi*Rc*Lh
301 :
REM      ***** SECTION 4 *****
    IF z>z4 THEN 302
    x1=Ra/Rc
    x2=(Ra-Lc*TAN(z))/Rc
    cx1=-ATN(x1/SQR(-x1*x1+1))+1.5708
    cx2=-ATN(x2/SQR(-x2*x2+1))+1.5708
    AZ4=Rc*(cx1+cx2)*Lc
    GOTO 401
302 :
    x=Ra/Rc
    cx=-ATN(x/SQR(-x*x+1))+1.5708
    m=(Ra+Rc)/TAN(z)
    AZ4=2*pi*Rc*(Lc-m)+Rc*m*(pi+cx)
401 :
REM      ***** SECTION 5 *****
    zm=pi/2
    IF z<zm THEN 402
    AZ5=pi*(Rc^2-Ra^2)
    GOTO 500
402 :
    x=Ra/Rc
    cx=-ATN(x/SQR(-x*x+1))+1.5708
    AZ5=Rc^2*cx-Ra*SQR(Rc^2-Ra^2)
500 :
REM  Aha and Aca are calculated here.
    Aha=Ah-AZ2-AZ3
    Ara=Ar-AZ1-AZ4-AZ5
REM      ***** Shear Area Calculations *****
REM      ***** Cylindrical Shear Area Section *****
800 :
    IF z>z5 THEN 810
    L1=0
    Le=2*(Rc^2-(Ra-(Lc+Lh)*TAN(z))^2)^.5
    D=(Lc+Lh)/COS(pi*A/180)
    Acshear=2*D*(L1^2 +L1*Le+Le^2)/(3*(L1+Le))
    GOTO 850
810 :
    IF z>z3 THEN 820
    L1=0
    Le=2*Rc
    D=Ra/SIN(z)
    L2=2*Rc
    Le2=2*(Rc^2-(Ra-(Lc+Lh)*TAN(z))^2)^.5
    D2=((Lc+Lh)*TAN(z)-Ra)/SIN(z)

```

```

Acshear=2*D*(L1^2 +L1*Le+Le^2)/(3*(L1+Le))+2*D2*(L2^2
+L2*Le2+Le2^2)/(3*(L2+Le2))
GOTO 850
820 :
L1=0
Le=2*Rc
D=Ra/SIN(z)
L2=2*Rc
Le2=0
D2=Rc/SIN(z)
Acshear=2*D*(L1^2 +L1*Le+Le^2)/(3*(L1+Le))+2*D*(L2^2
+L2*Le2+Le2^2)/(3*(L2+Le2))
850 :
REM ***** Frustum Shear Area Section *****
IF z>z1 THEN 860
L1=2*(Rc^2-(Ra-(Lc+Lh)*TAN(z))^2)^.5
Le=0
D=Lf*(Rc+(Lc+Lh)*TAN(z)-Ra)/((Rc-Re)*COS(z)-Lf*SIN(z))
Afshear=2*D*(L1^2 +L1*Le+Le^2)/(3*(L1+Le))
GOTO 890
860 :
IF z>z2 THEN 870
L1=2*(Rc^2-(Ra-(Lc+Lh)*TAN(z))^2)^.5
Le=2*(Re^2-(Ra-(Lc+Lh+Lf)*TAN(z))^2)^.5
D=Lf/COS(z)
Afshear=2*D*(L1^2 +L1*Le+Le^2)/(3*(L1+Le))
GOTO 890
870 :
IF z>z3 THEN 880
L1=2*(Rc^2-(Ra-(Lc+Lh)*TAN(z))^2)^.5
Le=0
D=Lf*(Rc-(Lc+Lh)*TAN(z)+Ra)/(COS(z)*(Rc-Re)+Lf*SIN(z))
Afshear=2*D*(L1^2 +L1*Le+Le^2)/(3*(L1+Le))
GOTO 890
880 :
Afshear=0
890 :Ashear=Acshear+Afshear
REM *****
REM ***** Heat Loss Calculations *****
La=Da*COS(z) :REM projected length of aperture [m]
IF La<0 THEN La=0
T1=.08*(Tm-Ta)+273 :REM first guess temp of air leaving the aperture
XP=200 :REM
350 :
Tc=T1
GOTO Temp
370 :
Q1=DQ
380 :
Tc=XP
GOTO Temp
400 :
Q2=DQ
Tx=(T1*Q2-XP*Q1)/(Q2-Q1)
Tc=Tx

```



```

Temp:
Tb=(Tc+Ta)/2          :REM bulk temp inside cavity [K]
B1=1/Tb                :REM coefficient of volume expansion [1/K]
Tf=(Tm+Tb)/2          :REM film temp [K]
B2=1/Tf                :REM coefficient of volume expansion [1/K]
U=1.462E-06*Tf^1.5/(1+112/Tf) :REM absolute viscosity [kg/m-sec]
Pa=352.95/Tf           :REM density of air [kg/m^3]
V=U/Pa                 :REM kinematic viscosity [m^2/sec]
Tff=Tf*1.8             :REM film temp from [K] to [°R]
k=.00679+3.5353E-05*Tff :REM thermal conductivity [W/m-K]
Tv=ABS(Tc-Ta)
Vb=SQR(g*B1*Tv*La)     :REM characteristic velocity due to buoyancy [m/sec]
Va=.5*Vb               :REM average velocity [m/sec]
Qc=(Pf*.5*Aa*Va)*Cp*(Tc-Ta) :REM heat transfer through aperture [W]
Gr=g*B2*(Tm-Tb)*La^3/V^2 :REM Grashof number
Pr=.7                  :REM Prandtl number
Nu=.1*(Gr*Pr)^.333     :REM Nusselt number
h=Nu*k/Da              :REM heat transfer coefficient [W/m^2 K]
Qi=h*Aha*(Tm-Tb)+h*Ara*(Tw-Tb)+h*Ashear*(Tm-Tb) :REM heat transfer within
the aperture [W]
DQ=Qi-Qc
IF Tc=T1 THEN 370
IF Tc=XP THEN 400
IF ABS(DQ)<.1 THEN 740
IF DQ<0 THEN GOTO 720
XP=Tx
GOTO 380
720 :
T1=Tx
GOTO 350
740 :
Qr=Aa*e*SB*((Ac/(Ah+Ac))*(Tw^4-Ta^4)+(Ah/(Ah+Ac))*(Tm^4-Ta^4)) :REM
radiative loss [W]
Qk=(ki/t)*(Ah*(Tm-Ta)+Ar*(Tw-Ta))
QT=Qc+Qr+Qk            :REM total heat loss from receiver
PQc=100*Qc/QT           :REM %convective
REM *****
IF Pflag=1 THEN 66
REM ***** Output Loop Results *****
LPRINT ;TAB(3);A;
LPRINT TAB(12);
LPRINT USING "###.###";Aha;
LPRINT TAB(22);
LPRINT USING "###.###";Ara;
LPRINT TAB(32);
LPRINT USING "####.##";Qc;
LPRINT;TAB(42);
LPRINT USING "####.##";QT;
LPRINT TAB(54);
LPRINT USING "###.##";PQc;
LPRINT TAB(64);
LPRINT USING "####.##";Nu;
LPRINT TAB(74);
LPRINT USING "###.##^";Gr;
LPRINT TAB(88);

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```

LPRINT USING "##.##";Ashear
66 :
REM ***** write to clipboard *****
WRITE#1,A,Aha,Ara,Qc,QT,PQc,Nu,Gr,Ashear
REM *****
REM ***** End of Angle Loop *****
NEXT A
REM *****
IF Pflag=1 THEN 68
REM ***** Output Radiation & Conduction *****
LPRINT"Radiation (Watts) = ";Qr
LPRINT"Conduction (Watts) = ";Qk
68 :
REM ***** Write radiative & conduction to clipboard **
WRITE#1,"","Radiation (Watts) = ",Qr
WRITE#1,"","Conduction (Watts) = ",Qk
REM *****
REM ***** End of Temperature Loop *****
NEXT Tmf
REM *****
REM ***** End of Aperture Radius Loop *****
NEXT I
REM *****
CLOSE#1
END

```

Appendix 9: Clausing Model Heat Loss Data

Appendix 9 Clausing Model Heat Loss Data								
	End Plate Radius [m] =		0.127					
	Cavity Radius [m] =		0.330					
	Plenum Length [m] =		0.292					
	Hot Cylindrical Section Length [m] =		0.254					
	Cold Cylindrical Section Length [m] =		0.140					
	Ambient Temperature [K] =		294.261					
	Aperture Radius [m] =		0.076					
	Total Cavity Area [m ²] =		1.702					
	Total Heated Cavity Area [m ²] =		1.037					
	Total Refractory Cavity Area [m ²] =		0.665					
	T mean [K] =		422.0					
	[°F] =		300.0					
Angle [degrees]	Tube Area [m ²]	Refr. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.614	0.406	345.5	467.1	74.0	20.5	1.26E+07	0.30
15	0.465	0.377	312.5	434.2	72.0	20.2	1.19E+07	0.34
30	0.284	0.358	244.1	365.7	66.7	18.7	9.48E+06	0.32
45	0.139	0.350	164.7	286.4	57.5	15.9	5.84E+06	0.26
60	0.033	0.334	69.4	191.1	36.3	12.0	2.51E+06	0.08
75	0.000	0.267	29.5	151.2	19.5	6.4	3.82E+05	0.07
90	0.000	0.000	0.0	121.6	0.0	0.0	0.00E+00	0.07
	Radiation (Watts) =		25.1					
	Conduction (Watts) =		96.6					
	T mean [K] =		477.6					
	[°F] =		400.0					
Angle [degrees]	Tube Area [m ²]	Refr. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.614	0.406	570.7	763.9	74.7	20.1	1.19E+07	0.30
15	0.465	0.377	516.7	709.9	72.8	19.8	1.13E+07	0.34
30	0.284	0.358	406.5	599.8	67.8	18.4	9.07E+06	0.32
45	0.139	0.350	278.6	471.8	59.0	15.7	5.63E+06	0.26
60	0.033	0.334	124.6	317.8	39.2	11.9	2.45E+06	0.08
75	0.000	0.267	53.4	246.6	21.6	6.4	3.78E+05	0.07
90	0.000	0.000	0.0	193.2	0.0	0.0	0.00E+00	0.07
	Radiation (Watts) =		46.1					
	Conduction (Watts) =		147.2					
	T mean [K] =		533.2					
	[°F] =		500.0					
Angle [degrees]	Tube Area [m ²]	Refr. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.614	0.406	808.9	1082.4	74.7	19.5	1.07E+07	0.30
15	0.465	0.377	732.4	1006.0	72.8	19.2	1.02E+07	0.34
30	0.284	0.358	578.0	851.6	67.9	17.8	8.25E+06	0.32
45	0.139	0.350	398.8	672.3	59.3	15.3	5.15E+06	0.26
60	0.033	0.334	182.9	456.5	40.1	11.6	2.26E+06	0.08
75	0.000	0.267	78.4	352.0	22.3	6.2	3.53E+05	0.07
90	0.000	0.000	0.0	273.6	0.0	0.0	0.00E+00	0.07
	Radiation (Watts) =		75.8					
	Conduction (Watts) =		197.8					
	T mean [K] =		588.7					
	[°F] =		600.0					
Angle [degrees]	Tube Area [m ²]	Refr. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.614	0.406	1085.1	1419.9	74.3	18.7	9.45E+06	0.30
15	0.465	0.377	955.3	1320.1	72.4	18.4	9.05E+06	0.34
30	0.284	0.358	755.0	1119.8	67.4	17.2	7.34E+06	0.32
45	0.139	0.350	522.6	887.5	58.9	14.7	4.61E+06	0.26
60	0.033	0.334	243.0	607.9	40.0	11.2	2.04E+06	0.08
75	0.000	0.267	104.2	469.1	22.2	6.1	3.21E+05	0.07
90	0.000	0.000	0.0	364.8	0.0	0.0	0.00E+00	0.07
	Radiation (Watts) =		116.5					
	Conduction (Watts) =		248.4					

Appendix 9 Clausing Model Heat Loss Data

Aperture Radius [m] = 0.132								
Total Cavity Area [m ²] = 1.647								
Total Heated Cavity Area [m ²] = 1.037								
Total Refractory Cavity Area [m ²] = 0.610								
T mean [K] = 422.0								
[°F] = 300.0								
Angle [degrees]	Tube Area [m ²]	Refrac. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.742	0.435	605.0	799.7	75.7	47.7	1.58E+08	0.25
15	0.566	0.399	535.8	730.3	73.3	46.4	1.45E+08	0.32
30	0.370	0.372	408.4	603.1	67.7	42.2	1.09E+08	0.33
45	0.213	0.364	277.0	471.7	58.7	35.0	6.23E+07	0.31
60	0.059	0.350	118.2	312.9	37.8	25.4	2.38E+07	0.15
75	0.000	0.282	46.4	241.1	19.2	13.3	3.45E+06	0.14
90	0.000	0.000	0.0	194.7	0.0	0.0	0.00E+00	0.13
Radiation (Watts) = 100.2								
Conduction (Watts) = 94.5								
T mean [K] = 477.6								
[°F] = 400.0								
Angle [degrees]	Tube Area [m ²]	Refrac. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.742	0.435	984.4	1312.0	75.0	47.6	1.57E+08	0.25
15	0.566	0.399	871.9	1199.6	72.7	46.4	1.45E+08	0.32
30	0.370	0.372	667.8	995.5	67.1	42.2	1.09E+08	0.33
45	0.213	0.364	457.6	785.3	58.3	35.0	6.26E+07	0.31
60	0.059	0.350	203.2	530.8	38.3	25.5	2.40E+07	0.15
75	0.000	0.282	80.5	408.2	19.7	13.4	3.50E+06	0.14
90	0.000	0.000	0.0	327.7	0.0	0.0	0.00E+00	0.13
Radiation (Watts) = 184.2								
Conduction (Watts) = 143.4								
T mean [K] = 533.2								
[°F] = 500.0								
Angle [degrees]	Tube Area [m ²]	Refrac. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.742	0.435	1380.6	1876.2	73.6	46.6	1.47E+08	0.25
15	0.566	0.399	1222.7	1718.3	71.2	45.4	1.36E+08	0.32
30	0.370	0.372	938.5	1434.1	65.4	41.3	1.03E+08	0.33
45	0.213	0.364	645.9	1141.6	56.6	34.4	5.89E+07	0.31
60	0.059	0.350	292.1	787.7	37.1	25.0	2.27E+07	0.15
75	0.000	0.282	116.2	611.8	19.0	13.2	3.32E+06	0.14
90	0.000	0.000	0.0	495.6	0.0	0.0	0.00E+00	0.13
Radiation (Watts) = 303.2								
Conduction (Watts) = 192.4								
T mean [K] = 588.7								
[°F] = 600.0								
Angle [degrees]	Tube Area [m ²]	Refrac. Area [m ²]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m ²]
0	0.742	0.435	1786.1	2493.3	71.6	45.1	1.34E+08	0.25
15	0.566	0.399	1581.5	2288.8	69.1	44.0	1.24E+08	0.32
30	0.370	0.372	1215.1	1922.4	63.2	40.1	9.38E+07	0.33
45	0.213	0.364	838.3	1545.5	54.2	33.3	5.39E+07	0.31
60	0.059	0.350	382.9	1090.1	35.1	24.3	2.08E+07	0.15
75	0.000	0.282	152.5	859.8	17.7	12.8	3.05E+06	0.14
90	0.000	0.000	0.0	707.2	0.0	0.0	0.00E+00	0.13
Radiation (Watts) = 465.9								
Conduction (Watts) = 241.4								

Appendix 9 Clausing Model Heat Loss Data

Aperture Radius [m] = 0.229								
Total Cavity Area [m^2] = 1.556								
Total Heated Cavity Area [m^2] = 1.037								
Total Refractory Cavity Area [m^2] = 0.519								
T mean [K] = 422.0								
[°F] = 300.0								
Angle [degrees]	Tube Area [m^2]	Refrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	0.855	0.411	705.4	1021.9	69.0	75.0	6.15E+08	0.17
15	0.664	0.387	646.6	983.1	67.1	72.6	5.59E+08	0.30
30	0.467	0.347	496.7	813.2	61.1	65.6	4.12E+08	0.33
45	0.283	0.338	338.3	654.8	51.7	54.0	2.30E+08	0.34
60	0.092	0.323	154.4	470.9	32.8	38.7	8.46E+07	0.23
75	0.002	0.274	59.0	375.3	15.7	20.2	1.21E+07	0.21
90	0.000	0.000	0.0	316.5	0.0	0.0	0.00E+00	0.20
Radiation (Watts) =			225.5					
Conduction (Watts) =			91.0					
T mean [K] = 477.6								
[°F] = 400.0								
Angle [degrees]	Tube Area [m^2]	Refrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	0.855	0.411	1137.7	1689.4	67.3	75.3	6.22E+08	0.17
15	0.664	0.387	1042.5	1594.2	65.4	72.9	5.65E+08	0.30
30	0.467	0.347	802.4	1354.1	59.3	65.9	4.17E+08	0.33
45	0.283	0.338	550.6	1102.3	50.0	54.3	2.33E+08	0.34
60	0.092	0.323	257.8	809.5	31.9	39.0	8.61E+07	0.23
75	0.002	0.274	99.8	651.5	15.3	20.4	1.23E+07	0.21
90	0.000	0.000	0.0	551.7	0.0	0.0	0.00E+00	0.20
Radiation (Watts) =			414.5					
Conduction (Watts) =			137.2					
T mean [K] = 533.2								
[°F] = 500.0								
Angle [degrees]	Tube Area [m^2]	Refrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	0.855	0.411	1586.6	2452.3	64.7	73.9	5.88E+08	0.17
15	0.664	0.387	1453.4	2319.1	62.7	71.6	5.35E+08	0.30
30	0.467	0.347	1119.4	1985.1	56.4	64.8	3.96E+08	0.33
45	0.283	0.338	770.9	1636.6	47.1	53.4	2.22E+08	0.34
60	0.092	0.323	365.5	1231.2	29.7	38.3	8.19E+07	0.23
75	0.002	0.274	142.2	1007.9	14.1	20.1	1.17E+07	0.21
90	0.000	0.000	0.0	865.7	0.0	0.0	0.00E+00	0.20
Radiation (Watts) =			682.3					
Conduction (Watts) =			183.5					
T mean [K] = 588.7								
[°F] = 600.0								
Angle [degrees]	Tube Area [m^2]	Refrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	0.855	0.411	2043.8	3321.7	61.5	71.8	5.40E+08	0.17
15	0.664	0.387	1871.8	3149.7	59.4	69.6	4.91E+08	0.30
30	0.467	0.347	1442.1	2720.0	53.0	63.0	3.64E+08	0.33
45	0.283	0.338	995.0	2273.0	43.8	51.9	2.04E+08	0.34
60	0.092	0.323	475.0	1752.9	27.1	37.3	7.54E+07	0.23
75	0.002	0.274	185.4	1463.4	12.7	19.5	1.08E+07	0.21
90	0.000	0.000	0.0	1277.9	0.0	0.0	0.00E+00	0.20
Radiation (Watts) =			1048.2					
Conduction (Watts) =			229.7					

Appendix 9 Clausing Model Heat Loss Data

Aperture Radius [m] = 0.329								
Total Cavity Area [m^2] = 1.380								
Total Heated Cavity Area [m^2] = 1.037								
Total Refractory Cavity Area [m^2] = 0.343								
T mean [K] = 422.0								
[°F] = 300.0								
Angle [degrees]	Tube Area [m^2]	efrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	1.024	0.336	740.0	1291.2	57.3	110.7	1.98E+09	0.01
15	0.883	0.317	743.7	1295.0	57.4	106.9	1.78E+09	0.22
30	0.628	0.270	592.6	1143.8	51.8	96.2	1.30E+09	0.34
45	0.384	0.244	385.3	936.6	41.1	79.0	7.19E+08	0.36
60	0.146	0.228	191.5	742.7	25.8	56.3	2.60E+08	0.33
75	0.011	0.187	69.0	620.2	11.1	29.3	3.67E+07	0.30
90	0.000	0.000	0.0	551.3	0.0	0.0	0.00E+00	0.29
Radiation (Watts) =			467.1					
Conduction (Watts) =			84.2					
T mean [K] = 477.6								
[°F] = 400.0								
Angle [degrees]	Tube Area [m^2]	efrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	1.024	0.336	1181.3	2165.0	54.6	111.4	2.02E+09	0.01
15	0.883	0.317	1183.5	2167.2	54.6	107.6	1.82E+09	0.22
30	0.628	0.270	941.6	1925.3	48.9	96.8	1.32E+09	0.34
45	0.384	0.244	614.8	1398.5	38.5	79.6	7.35E+08	0.36
60	0.146	0.228	309.0	1292.7	23.9	56.7	2.66E+08	0.33
75	0.011	0.187	112.3	1096.0	10.2	29.6	3.76E+07	0.30
90	0.000	0.000	0.0	983.7	0.0	0.0	0.00E+00	0.29
Radiation (Watts) =			858.5					
Conduction (Watts) =			125.2					
T mean [K] = 533.2								
[°F] = 500.0								
Angle [degrees]	Tube Area [m^2]	efrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	1.024	0.336	1637.7	3217.1	50.9	109.6	1.92E+09	0.01
15	0.883	0.317	1638.0	3217.4	50.9	105.8	1.73E+09	0.22
30	0.628	0.270	1302.1	2881.4	45.2	95.3	1.26E+09	0.34
45	0.384	0.244	851.7	2431.1	35.0	78.3	7.00E+08	0.36
60	0.146	0.228	430.5	2009.9	21.4	55.8	2.53E+08	0.33
75	0.011	0.187	157.0	1736.4	9.0	29.1	3.59E+07	0.30
90	0.000	0.000	0.0	1579.4	0.0	0.0	0.00E+00	0.29
Radiation (Watts) =			1413.2					
Conduction (Watts) =			166.2					
T mean [K] = 588.7								
[°F] = 600.0								
Angle [degrees]	Tube Area [m^2]	efrac. Area [m^2]	Q conv [Watts]	Q total [Watts]	% Conv %	Nu	Gr	Ashear [m^2]
0	1.024	0.336	2101.1	4479.5	46.9	106.6	1.77E+09	0.01
15	0.883	0.317	2099.4	4477.8	46.9	103.0	1.59E+09	0.22
30	0.628	0.270	1667.9	4046.3	41.2	92.7	1.16E+09	0.34
45	0.384	0.244	1092.1	3470.4	31.5	76.2	6.46E+08	0.36
60	0.146	0.228	553.7	2932.1	18.9	54.4	2.34E+08	0.33
75	0.011	0.187	202.5	2580.9	7.8	28.4	3.31E+07	0.30
90	0.000	0.000	0.0	2378.4	0.0	0.0	0.00E+00	0.29
Radiation (Watts) =			2171.2					
Conduction (Watts) =			207.2					

Appendix 10 Siebers and Kraabel Computer Program Listing

```

REM *****
REM
REM                               Siebers & Kraabel Method
REM
REM *****
REM   The Siebers & Kraabel method is used here to predict the convective
REM   from a solar cavity receiver operating at various temperatures and
REM   receiver angles.
REM *****
PRINT " Siebers & Kraabel Method of Predicting Convective Losses"
PRINT
PRINT
REM *****
REM   The program allows some variations in receiver geometry. These
REM   variables are inputted in this section of the program. The characteristic
REM   length, as called for in the reference, is simply the cavity diameter
REM   given here as 'Cl'.
REM *****
REM                               Receiver Geometry *****
Re=.127                :REM end plate radius [m]
Rc=.33                :REM cavity radius [m]
Lf=.292               :REM frustum length [m]
Lh=.254               :REM cylinder length hot [m]
Lc=.14                :REM cylinder length cold [m]
Cl=2*Rc               :REM characteristic length [m]
REM *****
REM                               Constants *****
pi=4*ATN(1)
Ta=70                 :REM ambient temperature [°F]
REM *****
OPEN "CLIP:" FOR OUTPUT AS #1
REM ***** write header to clipboard *****
WRITE#1, " Siebers & Kraabel Method"
WRITE#1,
  WRITE#1,"","End Plate Radius [m] = ",Re
  WRITE#1,"","Cavity Radius [m] = ",Rc
  WRITE#1,"","Frustum Length [m] = ",Lf
  WRITE#1,"","Hot Cylindrical Section Length [m] = ",Lh
  WRITE#1,"","Cold Cylindrical Section Length [m] = ",Lc
  WRITE#1,"","T amb [°F] = ",Ta
WRITE#1,
REM ***** Receiver Aperture Radius Loop *****
FOR rad=1 TO 4
  READ Ra
  DATA .0762, .1524, .2286, .329
  Da=2*Ra
REM *****
REM                               Angle Limits *****
REM   In this section the 4 angle limits, z1, z2, z3, and z4 are calculated.
  z1=ATN((Ra-Re)/(Lf+Lc+Lh)) :p1=z1*180/pi
  z2=ATN((Ra+Re)/(Lf+Lc+Lh)) :p2=z2*180/pi
  z3=ATN((Ra+Rc)/(Lc+Lh))    :p3=z3*180/pi
  z4=ATN((Ra+Rc)/Lc)         :p4=z4*180/pi

```



```

REM *****
REM ***** Area Constants *****
REM In the following section area 1, area 2, and area 3 are calculated.
REM A1 is the total interior cavity surface area.
REM A2 is the total interior cavity surface area minus the lower lip.
REM A3 is the interior cavity surface area below the horizontal plane
REM cutting through the receiver at the top of the aperture.
REM
  Ah=pi*(Re+Rc)*(Lf^2+(Rc-Re)^2)^.5+2*pi*Rc*Lh
  Ar=pi*Re^2+pi*(Rc^2-Ra^2)+2*pi*Rc*Lc
  A1=Ah+Ar
  A2=A1-Rc^2*(-ATN((Ra/Rc)/SQR(-(Ra/Rc)*(Ra/Rc)+1))+1.5708)+Ra
  *SQR(Rc^2-Ra^2)
REM Area 3 is a function of the receiver angle and is determined by
REM calculating the total area in zone 1, above the horizontal
REM plane, and then subtracting this value from the total area.
REM *****
REM ***** Print Header *****
PRINT " Siebers & Kraabel Method"
PRINT
  PRINT "End Plate Radius [m] = ";Re
  PRINT "Cavity Radius [m] = ";Rc
  PRINT "Aperture Radius [m] = ";Ra
  PRINT "Frustum Length [m] = ";Lf
  PRINT "Hot Cylindrical Section Length [m] = ";Lh
  PRINT "Cold Cylindrical Section Length [m] = ";Lc
  PRINT "T amb = ";Ta
  PRINT " Total Area [m^2] = ";A1
PRINT
REM *****
REM ***** write header to clipboard *****
WRITE#1,
  WRITE#1,"","Aperture Radius [m] = ",Ra
  WRITE#1,""," Total Area [m^2] = ",A1
REM ***** Operating Temperature Loop *****
REM
  FOR Th=300 TO 600 STEP 100
    REM mean system operating temperature of receiver [°F]
    Tr=Th-100
    Tw=(Th*Ah+Tr*Ar)/A1
    CLS
  REM *****
  REM ***** Air Properties *****
  REM The value of 'k' calculated here is the product of the gravitational
  REM constant times the coefficient of volumetric expansion divided by
  REM the kinematic viscosity squared. (i.e..  $g \beta / \nu^2$  [1/K-m^3]) The
  REM equation for 'k' is based on data from Table A-1, p. 388, Kays & Crawford,
  REM " Convective Heat and Mass Transfer ", second edition, McGraw-Hill.
  PRINT
    k=2.651E+08-2186000!*Ta+7935.4726#*Ta^2-13.3076*Ta^3+.0082*T a^4
    Gr=k*(Tw-Ta)/1.8*Cl^3 :REM Grashoff number
    Nu=.088*Gr^(1/3)*((Tw+459.67)/(Ta+459.67))^1.8 :REM Nusselt number
    hc=.81*((Tw-Ta)/1.8)^.426
    REM hc=natural convection no lip heat transfer coefficient
  REM *****

```



```

REM          ***** Print Table Header *****
PRINT "Nusselt Number =";Nu
PRINT "Grashoff Number =";Gr
PRINT "T mean [°F] = ";Th
PRINT ;TAB(3);" Angle";TAB(11);"Sec 1";TAB(19);"Sec 2";TAB(27);"Sec 3";
PRINT;TAB(35);"Sec 4";TAB(43);"Sec 5";TAB(50);"Heat Loss";TAB(61);" h ";
PRINT;TAB(72);"Total Zone 1"
PRINT ;TAB(1);" [degrees]";TAB(11);"[m^2]";TAB(19);"[m^2]";TAB(27);"[m^2]";
PRINT;TAB(35);"[m^2]";TAB(43);"[m^2]";TAB(51);"[Watts]";TAB(
60);"[Watts/K-m^2]";
PRINT;TAB(73);"[m^2]"
PRINT
REM          *****
REM          ***** WRITE HEADER TO CLIPBOARD *****
WRITE#1,"","Nusselt Number =",Nu
WRITE#1,"","Grashoff Number =",Gr
WRITE#1,"T mean = ",Th
WRITE#1,
WRITE#1,"Angle","Sec 1","Sec 2","Sec 3","Sec 4","Sec 5","Heat Loss","h","Total Zone
1 "
WRITE#1,"[degrees]","[m^2]","[m^2]","[m^2]","[m^2]","[m^2]","[m^2]",
"[Watts]","[Watts/K-m^2]","[m^2]"
WRITE#1,
REM          ***** Beginning of Angle Loop *****
FOR A=0 TO 90 STEP 15
    z=pi*A/180
    REM          *****
    REM          ***** Zone Areas *****
    REM The receiver cavity is divided into 5 section to accommodate the
    REM zone area calculations. The sections are defined as follows;
    REM section 1 = end plate
    REM section 2 = frustum
    REM section 3 = hot cylinder
    REM section 4 = cold cylinder
    REM section 5 = ring
    REM AZ1 = area of section 1 in zone 1
    REM AZ2 = area of section 2 in zone 1
    REM AZ3 = area of section 3 in zone 1
    REM AZ4 = area of section 4 in zone 1
    REM AZ5 = area of section 5 in zone 1
    REM          *****SECTION 1*****
    IF z>z1 THEN 101
        AZ1=0
        GOTO 201
    101 :
        IF z>z2 THEN 102
            x=(Ra-(Lf+Lc+Lh)*TAN(z))/Rc
            cx=-ATN(x/SQR(-x*x+1))+1.5708
            m=(Lf+Lc+Lh)*TAN(z)-Ra+Re
            AZ1=Re^2*cx+((Lf+Lc+Lh)*TAN(z)-Ra)*SQR(2*Re*m-m^2)
            GOTO 201
        102 :
            AZ1=pi*Re^2
    201 :

```

```

REM          *****SECTION  2*****
IF z>z1 THEN 202
  x=(Ra-(Lc+Lh)*TAN(z))/Rc
  cx=-ATN(x/SQR(-x*x+1))+1.5708
  m=ATN((Rc-Re)/Lf)
  AZ2=((Rc-Re)/Lf)*(Rc-Ra)+Lc+Lh)*SIN(z)/SIN(pi/2-z-m)
  AZ2=(AZ2+(Rc-Ra)/SIN(m))*Rc*cx
  GOTO 301
202 :
IF z>z2 THEN 203
  x1=(Ra-(Lc+Lf+Lh)*TAN(z))/Re
  cx1=-ATN(x1/SQR(-x1*x1+1))+1.5708
  x2=(Ra-(Lc+Lh)*TAN(z))/Rc
  cx2=-ATN(x2/SQR(-x2*x2+1))+1.5708
  AZ2=SQR(Lf^2+(Rc-Re)^2)*(Re*cx1+Rc*cx2)
  GOTO 301
203 :
IF z>z3 THEN 204
  m=ATN((Rc-Re)/Lf)
  n=ATN((Ra+Re)/(Lc+Lf+Lh))
  l=SQR((Lc+Lf+Lh)^2+(Ra+Re)^2)*SIN(z-n)/SIN(pi-z-m)
  x=(Ra-(Lc+Lh)*TAN(z))/Rc
  cx=-ATN(x/SQR(-x*x+1))+1.5708
  AZ2=(pi*Re+pi*(Re+l*SIN(m)))*l
  AZ2=AZ2+(Rc*cx+pi*(Re+l*SIN(m)))*(SQR(Lf^2+(Rc-Re)^2)-l)
  GOTO 301
204 :
  AZ2=pi*(Re+Rc)*SQR(Lf^2+(Rc-Re)^2)
301 :
REM          *****SECTION  3 *****
IF z>z3 THEN 302
  x1=(Ra-Lc*TAN(z))/Rc
  x2=(Ra-(Lc+Lh)*TAN(z))/Rc
  cx1=-ATN(x1/SQR(-x1*x1+1))+1.5708
  cx2=-ATN(x2/SQR(-x2*x2+1))+1.5708
  AZ3=Rc*(cx1+cx2)*Lh
  GOTO 401
302 :
IF z>z4 THEN 303
  m=(Ra+Rc)/TAN(z)
  x=(Ra-Lc*TAN(z))/Rc
  cx=-ATN(x/SQR(-x*x+1))+1.5708
  AZ3=2*pi*Rc*(Lh+Lc-m)+Rc*(m-Lc)*(pi+cx)
  GOTO 401
303 :
  AZ3=2*pi*Rc*Lh
401 :
REM          *****SECTION  4 *****
IF z>z4 THEN 402
  x1=Ra/Rc
  x2=(Ra-Lc*TAN(z))/Rc
  cx1=-ATN(x1/SQR(-x1*x1+1))+1.5708
  cx2=-ATN(x2/SQR(-x2*x2+1))+1.5708
  AZ4=Rc*(cx1+cx2)*Lc
  GOTO 501

```

```

402 :
    x=Ra/Rc
    cx=-ATN(x/SQR(-x*x+1))+1.5708
    m=(Ra+Rc)/TAN(z)
    AZ4=2*pi*Rc*(Lc-m)+Rc*m*(pi+cx)
501 :
REM      ***** SECTION 5 *****
    zm=pi/2
    IF z<zm THEN 502
    AZ5=pi*(Rc^2-Ra^2)
    GOTO 600
502 :
    x=Ra/Rc
    cx=-ATN(x/SQR(-x*x+1))+1.5708
    AZ5=Rc^2*cx-Ra*SQR(Rc^2-Ra^2)
600 :
REM      ***** Calculate Area 3 *****
    AZT=AZ1+AZ2+AZ3+AZ4+AZ5
    A3=A1-AZT
REM      *****
REM      ***** Heat Loss Calculation *****
    zz=pi*30/180
    IF z>zz THEN 601
    n=.63
    GOTO 700
601 :
    n=.8
700 :
    h=hc*(A1/A2)*(A3/A1)^n
    q=h*A1*(Tw-Ta)/1.8
REM      ***** PRINTER Output *****
REM
PRINT;TAB(4);
PRINT USING"###.";A;
PRINT;TAB(9);
PRINT USING "###.###";AZ1;
PRINT;TAB(17);
PRINT USING "###.###";AZ2;
PRINT;TAB(25);
PRINT USING "###.###";AZ3;
PRINT;TAB(33);
PRINT USING "###.###";AZ4;
PRINT;TAB(41);
PRINT USING "###.###";AZ5;
PRINT;TAB(50);
PRINT USING "#####.";q;
PRINT;TAB(60);
PRINT USING "###.###";h;
PRINT;TAB(70);
PRINT USING "###.###";AZT
REM      ***** OUTPUT TO CLIPBOARD *****
WRITE #1,A,AZ1,AZ2,AZ3,AZ4,AZ5,q,h,AZT
NEXT A
NEXT Th
NEXT rad

```

```
PRINT "bye!"  
CLOSE #1  
END
```

Appendix 11 Siebers and Kraabel Model Heat Loss

Appendix 11 Siebers & Kraabel Model Heat Loss Data									
End Plate Radius (m) = 0.127									
Cavity Radius (m) = 0.33									
Prism Length (m) = 0.292									
Hot Cylindrical Section Length (m) = 0.254									
Cold Cylindrical Section Length (m) = 0.14									
T amb (°F) = 70									
Aperture Radius (m) = 0.076									
Total Area (m²) = 1.702									
Nusselt Number = 153.25									
Grashof Number = 4.47E+9									
T mean = 300									
Angle (degrees)	Sec 1 (m²)	Sec 2 (m²)	Sec 3 (m²)	Sec 4 (m²)	Sec 5 (m²)	Heat Loss (Watts)	h (Watts/K-m²)	Total Zone 1 (m²)	
0	0.014	0.199	0.224	0.124	0.121	831.9	4.807	0.682	
15	0.038	0.311	0.261	0.129	0.121	736.9	4.081	0.860	
30	0.051	0.449	0.304	0.135	0.121	621.3	3.441	1.060	
45	0.051	0.510	0.388	0.143	0.121	423.1	2.343	1.213	
60	0.051	0.511	0.494	0.159	0.121	358.3	1.863	1.335	
75	0.051	0.511	0.527	0.225	0.121	261.3	1.447	1.435	
90	0.051	0.511	0.527	0.290	0.324	0.0	0.000	1.702	
Nusselt Number = 180.50									
Grashof Number = 6.81E+9									
T mean = 400									
Angle (degrees)	Sec 1 (m²)	Sec 2 (m²)	Sec 3 (m²)	Sec 4 (m²)	Sec 5 (m²)	Heat Loss (Watts)	h (Watts/K-m²)	Total Zone 1 (m²)	
0	0.014	0.199	0.224	0.124	0.121	1516.6	5.513	0.682	
15	0.038	0.311	0.261	0.129	0.121	1343.4	4.883	0.860	
30	0.051	0.449	0.304	0.135	0.121	1132.7	4.117	1.060	
45	0.051	0.510	0.388	0.143	0.121	771.4	2.804	1.213	
60	0.051	0.511	0.494	0.159	0.121	613.2	2.229	1.335	
75	0.051	0.511	0.527	0.225	0.121	476.3	1.731	1.435	
90	0.051	0.511	0.527	0.290	0.324	0.0	0.000	1.702	
Nusselt Number = 208.34									
Grashof Number = 9.15E+9									
T mean = 500									
Angle (degrees)	Sec 1 (m²)	Sec 2 (m²)	Sec 3 (m²)	Sec 4 (m²)	Sec 5 (m²)	Heat Loss (Watts)	h (Watts/K-m²)	Total Zone 1 (m²)	
0	0.014	0.199	0.224	0.124	0.121	2311.3	6.252	0.682	
15	0.038	0.311	0.261	0.129	0.121	2047.3	5.538	0.860	
30	0.051	0.449	0.304	0.135	0.121	1726.2	4.669	1.060	
45	0.051	0.510	0.388	0.143	0.121	1175.6	3.180	1.213	
60	0.051	0.511	0.494	0.159	0.121	934.4	2.328	1.335	
75	0.051	0.511	0.527	0.225	0.121	725.9	1.964	1.435	
90	0.051	0.511	0.527	0.290	0.324	0.0	0.000	1.702	
Nusselt Number = 223.49									
Grashof Number = 1.13E+10									
T mean = 600									
Angle (degrees)	Sec 1 (m²)	Sec 2 (m²)	Sec 3 (m²)	Sec 4 (m²)	Sec 5 (m²)	Heat Loss (Watts)	h (Watts/K-m²)	Total Zone 1 (m²)	
0	0.014	0.199	0.224	0.124	0.121	3198.2	6.889	0.682	
15	0.038	0.311	0.261	0.129	0.121	2832.9	6.102	0.860	
30	0.051	0.449	0.304	0.135	0.121	2388.6	5.145	1.060	
45	0.051	0.510	0.388	0.143	0.121	1628.7	3.504	1.213	
60	0.051	0.511	0.494	0.159	0.121	1293.0	2.785	1.335	
75	0.051	0.511	0.527	0.225	0.121	1064.3	2.164	1.435	
90	0.051	0.511	0.527	0.290	0.324	0.0	0.000	1.702	

Appendix 11 Siebers and Kraabel Model Heat Loss

Average K _{area} [W/m ²] =		0.152							
Total Area [m ²] =		1.647							
Nusselt Number = 153.85									
Grashoff Number = 4.52E+09									
T _{mean} = 300									
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]	
0	0.000	0.112	0.183	0.101	0.074	888.2	5.029	0.470	
15	0.031	0.250	0.222	0.107	0.074	783.2	4.435	0.683	
30	0.051	0.403	0.264	0.113	0.074	664.4	3.782	0.905	
45	0.051	0.495	0.329	0.121	0.074	474.3	2.686	1.070	
60	0.051	0.511	0.467	0.136	0.074	339.8	2.037	1.239	
75	0.051	0.511	0.527	0.203	0.074	267.7	1.518	1.365	
90	0.051	0.511	0.527	0.290	0.269	0.0	0.000	1.647	
Nusselt Number = 180.99									
Grashoff Number = 6.82E+09									
T _{mean} = 400									
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]	
0	0.000	0.112	0.183	0.101	0.074	1610.9	6.008	0.470	
15	0.031	0.250	0.222	0.107	0.074	1420.5	5.296	0.683	
30	0.051	0.403	0.264	0.113	0.074	1205.1	4.485	0.905	
45	0.051	0.495	0.329	0.121	0.074	860.3	3.209	1.070	
60	0.051	0.511	0.467	0.136	0.074	632.6	2.434	1.239	
75	0.051	0.511	0.527	0.203	0.074	485.6	1.811	1.365	
90	0.051	0.511	0.527	0.290	0.269	0.0	0.000	1.647	
Nusselt Number = 203.77									
Grashoff Number = 9.20E+09									
T _{mean} = 500									
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]	
0	0.000	0.112	0.183	0.101	0.074	2448.8	6.809	0.470	
15	0.031	0.250	0.222	0.107	0.074	2159.4	6.004	0.683	
30	0.051	0.403	0.264	0.113	0.074	1831.8	5.094	0.905	
45	0.051	0.495	0.329	0.121	0.074	1307.8	3.636	1.070	
60	0.051	0.511	0.467	0.136	0.074	992.0	2.738	1.239	
75	0.051	0.511	0.527	0.203	0.074	738.1	2.052	1.365	
90	0.051	0.511	0.527	0.290	0.269	0.0	0.000	1.647	
Nusselt Number = 223.88									
Grashoff Number = 1.15E+10									
T _{mean} = 600									
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]	
0	0.000	0.112	0.183	0.101	0.074	3383.4	7.499	0.470	
15	0.031	0.250	0.222	0.107	0.074	2983.5	6.613	0.683	
30	0.051	0.403	0.264	0.113	0.074	2551.0	5.610	0.905	
45	0.051	0.495	0.329	0.121	0.074	1807.0	4.005	1.070	
60	0.051	0.511	0.467	0.136	0.074	1370.6	3.038	1.239	
75	0.051	0.511	0.527	0.203	0.074	1019.9	2.261	1.365	
90	0.051	0.511	0.527	0.290	0.269	0.0	0.000	1.647	

Appendix 11 Siebers and Kraabel Model Heat Loss

Aperture Ratio [in] = 0.229								
Total Area [m ²] = 1.556								
Nusselt Number = 154.56								
Grashoff Number = 4.60E+09								
T mean = 900								
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]
0	0.000	0.047	0.135	0.074	0.033	912.7	5.368	0.290
15	0.018	0.194	0.180	0.081	0.033	811.2	4.771	0.506
30	0.031	0.346	0.224	0.088	0.033	690.8	4.083	0.742
45	0.051	0.470	0.285	0.097	0.033	498.1	2.930	0.936
60	0.051	0.511	0.435	0.112	0.033	361.2	2.125	1.141
75	0.051	0.511	0.525	0.161	0.033	260.4	1.532	1.280
90	0.031	0.511	0.527	0.290	0.178	0.0	0.000	1.356
Nusselt Number = 181.90								
Grashoff Number = 6.95E+09								
T mean = 400								
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]
0	0.000	0.047	0.135	0.074	0.033	1640.3	6.396	0.290
15	0.018	0.194	0.180	0.081	0.033	1457.8	5.684	0.506
30	0.031	0.346	0.224	0.088	0.033	1241.5	4.841	0.742
45	0.051	0.470	0.285	0.097	0.033	895.3	3.491	0.936
60	0.051	0.511	0.435	0.112	0.033	648.2	2.531	1.141
75	0.051	0.511	0.525	0.161	0.033	468.0	1.825	1.280
90	0.031	0.511	0.527	0.290	0.178	0.0	0.000	1.356
Nusselt Number = 204.56								
Grashoff Number = 9.29E+09								
T mean = 900								
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]
0	0.000	0.047	0.135	0.074	0.033	2482.1	7.238	0.290
15	0.018	0.194	0.180	0.081	0.033	2206.1	6.433	0.506
30	0.031	0.346	0.224	0.088	0.033	1878.7	5.479	0.742
45	0.051	0.470	0.285	0.097	0.033	1354.8	3.951	0.936
60	0.051	0.511	0.435	0.112	0.033	982.3	2.865	1.141
75	0.051	0.511	0.525	0.161	0.033	708.2	2.065	1.280
90	0.031	0.511	0.527	0.290	0.178	0.0	0.000	1.356
Nusselt Number = 224.58								
Grashoff Number = 1.16E+10								
T mean = 600								
Angle [degrees]	Sec 1 [m ²]	Sec 2 [m ²]	Sec 3 [m ²]	Sec 4 [m ²]	Sec 5 [m ²]	Heat Loss [Watts]	h [Watts/K-m ²]	Total Zone 1 [m ²]
0	0.000	0.047	0.135	0.074	0.033	3420.3	7.966	0.290
15	0.018	0.194	0.180	0.081	0.033	3039.9	7.080	0.506
30	0.031	0.346	0.224	0.088	0.033	2588.8	6.029	0.742
45	0.051	0.470	0.285	0.097	0.033	1868.8	4.348	0.936
60	0.051	0.511	0.435	0.112	0.033	1353.6	3.153	1.141
75	0.051	0.511	0.525	0.161	0.033	975.9	2.275	1.280
90	0.031	0.511	0.527	0.290	0.178	0.0	0.000	1.356

Appendix 11 Siebers and Kraabel Model Heat Loss

Aperture Radius [m] = 0.329									
Total Area [m²] = 1.380									
Nusselt Number = 157.19									
Grashof Number = 4.80E+09									
T mean = 300									
Angle [degrees]	Sec 1 [m²]	Sec 2 [m²]	Sec 3 [m²]	Sec 4 [m²]	Sec 5 [m²]	Heat Loss [Watts]	h [Watts/K-m²]	Total Zone 1 [m²]	
0	0.000	0.000	0.013	0.007	0.000	949.3	6.034	0.020	
15	0.000	0.044	0.110	0.026	0.000	877.4	5.378	0.180	
30	0.036	0.244	0.166	0.037	0.000	750.9	4.646	0.482	
45	0.051	0.424	0.229	0.048	0.000	510.5	3.246	0.752	
60	0.051	0.511	0.381	0.064	0.000	337.2	2.143	1.006	
75	0.051	0.511	0.515	0.105	0.000	203.2	1.292	1.182	
90	0.051	0.511	0.527	0.290	0.002	0.0	0.000	1.380	
Nusselt Number = 183.96									
Grashof Number = 7.14E+09									
T mean = 400									
Angle [degrees]	Sec 1 [m²]	Sec 2 [m²]	Sec 3 [m²]	Sec 4 [m²]	Sec 5 [m²]	Heat Loss [Watts]	h [Watts/K-m²]	Total Zone 1 [m²]	
0	0.000	0.000	0.013	0.007	0.000	1672.2	7.146	0.020	
15	0.000	0.044	0.110	0.026	0.000	1343.5	6.605	0.180	
30	0.036	0.244	0.166	0.037	0.000	1287.3	5.302	0.482	
45	0.051	0.424	0.229	0.048	0.000	899.4	3.844	0.752	
60	0.051	0.511	0.381	0.064	0.000	594.0	2.339	1.006	
75	0.051	0.511	0.515	0.105	0.000	357.9	1.530	1.182	
90	0.051	0.511	0.527	0.290	0.002	0.0	0.000	1.380	
Nusselt Number = 206.34									
Grashof Number = 9.49E+09									
T mean = 500									
Angle [degrees]	Sec 1 [m²]	Sec 2 [m²]	Sec 3 [m²]	Sec 4 [m²]	Sec 5 [m²]	Heat Loss [Watts]	h [Watts/K-m²]	Total Zone 1 [m²]	
0	0.000	0.000	0.013	0.007	0.000	2305.2	8.064	0.020	
15	0.000	0.044	0.110	0.026	0.000	2313.3	7.233	0.180	
30	0.036	0.244	0.166	0.037	0.000	1928.8	6.209	0.482	
45	0.051	0.424	0.229	0.048	0.000	1347.4	4.537	0.752	
60	0.051	0.511	0.381	0.064	0.000	889.9	2.864	1.006	
75	0.051	0.511	0.515	0.105	0.000	536.2	1.726	1.182	
90	0.051	0.511	0.527	0.290	0.002	0.0	0.000	1.380	
Nusselt Number = 226.19									
Grashof Number = 1.18E+10									
T mean = 600									
Angle [degrees]	Sec 1 [m²]	Sec 2 [m²]	Sec 3 [m²]	Sec 4 [m²]	Sec 5 [m²]	Heat Loss [Watts]	h [Watts/K-m²]	Total Zone 1 [m²]	
0	0.000	0.000	0.013	0.007	0.000	3431.3	8.858	0.020	
15	0.000	0.044	0.110	0.026	0.000	3171.5	8.188	0.180	
30	0.036	0.244	0.166	0.037	0.000	2641.9	6.820	0.482	
45	0.051	0.424	0.229	0.048	0.000	1845.5	4.764	0.752	
60	0.051	0.511	0.381	0.064	0.000	1218.8	3.147	1.006	
75	0.051	0.511	0.515	0.105	0.000	734.4	1.896	1.182	
90	0.051	0.511	0.527	0.290	0.002	0.0	0.000	1.380	

APPENDIX 12: Stine and McDonald Model Computer Program Listing

```

REM *****
REM
REM                               Stine & McDonald Method
REM
REM *****
REM *****
PRINT " Stine & McDonald Method of Predicting Convective Losses"
PRINT
PRINT
REM *****
REM *****
REM ***** Receiver Geometry *****
Re=.127          :REM end plate radius [m]
Rc=.33           :REM cavity radius [m]
Lf=.292          :REM frustum length [m]
Lh=.254          :REM cylinder length hot [m]
Lc=.14           :REM cylinder length cold [m]
L=2*Rc           :REM characteristic length [m]
REM *****
REM ***** Constants *****
pi=4*ATN(1)
Ta=70 :Tak=(Ta+459.67)/1.8          :REM ambient temperature [°F]
REM *****
OPEN "CLIP:" FOR OUTPUT AS #1
REM ***** write header to clipboard *****
WRITE#1, " Stine & McDonald Method"
WRITE#1,
WRITE#1,"","","End Plate Radius [m] = ",Re
WRITE#1,"","","Cavity Radius [m] = ",Rc
WRITE#1,"","","Frustum Length [m] = ",Lf
WRITE#1,"","","Hot Cylindrical Section Length [m] = ",Lh
WRITE#1,"","","Cold Cylindrical Section Length [m] = ",Lc
WRITE#1,"","","T amb [°F] = ",Ta
WRITE#1,
REM ***** Receiver Aperture Radius Loop *****
FOR rad=1 TO 4
READ Ra
DATA .0762, .1524, .2286, .329
Da=2*Ra
REM *****
REM ***** Area Constants *****
REM In the following section area 1, area 2, and area 3 are calculated.
REM At is the total interior cavity surface area.
REM Ah is the simplified cavity tube surface area
REM Ar is the simplified refractory cavity surface area.
Ah=pi*(Re+Rc)*(Lf^2+(Rc-Re)^2)^.5+2*pi*Rc*Lh
Ar=pi*Re^2+pi*(Rc^2-Ra^2)+2*pi*Rc*Lc
At=Ah+Ar
REM *****
REM ***** Print Header *****
PRINT " Stine & McDonald Method"
PRINT
PRINT "End Plate Radius [m] = ";Re

```

```

PRINT "Cavity Radius [m] = ";Rc
PRINT "Aperture Radius [m] = ";Ra
PRINT "Frustum Length [m] = ";Lf
PRINT "Hot Cylindrical Section Length [m] = ";Lh
PRINT "Cold Cylindrical Section Length [m] = ";Lc
PRINT "T amb [°F] = ";Ta; " [k] = ";Tak
PRINT " Total Area [m^2] = ";At
PRINT
REM *****
REM ***** write header to clipboard *****
WRITE#1,
  WRITE#1,"","Aperture Radius [m] = ",Ra
  WRITE#1,""," Total Area [m^2] = ",At
REM ***** Operating Temperature Loop *****
REM
  FOR Th=300 TO 600 STEP 100
    REM mean system operating temperature of receiver [°F]
    Tr=Th-100
    Tw=(Th*Ah+Tr*Ar)/At
    CLS
    REM *****
    REM ***** Air Properties *****
    REM The value of 'k' calculated here is the product of the gravitational
    REM constant times the coefficient of volumetric expansion divided by
    REM the kinematic viscosity squared. (i.e..  $g \beta / \nu^2$  [1/K-m^3]) The
    REM equation for 'k' is based on data from Table A-1, p. 388, Kays & Crawford,
    REM " Convective Heat and Mass Transfer ", second edition, McGraw-Hill.
    PRINT
    gBv=1.1547E+19*Tak^-4.4187
    Gr=gBv*(Th-Ta)/1.8*L^3 :REM Grashoff number
    k=.0071749261015#+.000064030639041#*Tak :REM thermal conductivity of air
    REM *****
    REM ***** Print Table Header *****
    PRINT "Grashoff Number =",Gr
    PRINT "T mean [°F] = ";Th
    PRINT ";TAB(3);" Angle";TAB(11);"Nu";TAB(19);"Heat Loss";TAB(27);" h "
    PRINT ";TAB(1);" [degrees]";TAB(11);"";TAB(19);"[Watts]";TAB(27);"[Watts/K-m^2]"
    PRINT
    REM *****
    REM ***** WRITE HEADER TO CLIPBOARD *****
    WRITE#1,"","Grashoff Number =",Gr
    WRITE#1,"T mean = ",Th
    WRITE#1,
    WRITE#1,"Angle","Nu","Heat Loss","h"
    WRITE#1,"[degrees]","", "[Watts]","[Watts/K-m^2]"
    REM ***** Beginning of Angle Loop *****
    FOR a=-90 TO 90 STEP 15
      z=pi*a/180
      REM *****
      REM ***** Heat Loss Calculation *****
      s=-.982*(Da/L)+1.12
      IF a=90 THEN 200
      Nu=.088*Gr^(1/3)*((Tw+459.67)/(Ta+459.67))^1.8*(COS(z))^2.47 *(Da/L)^s
      GOTO 300

```

```

200 :
Nu=0
300 :
:REM Nusselt number
h=Nu*k/L
q=h*At*(Tw-Ta)/1.8
REM ***** PRINTER Output *****
REM
PRINT;TAB(4);
PRINT USING"###.";a;
PRINT;TAB(9);
PRINT USING "###.##";Nu;
PRINT;TAB(17);
PRINT USING "#####.##";q;
PRINT;TAB(25);
PRINT USING "###.####";h
REM ***** OUTPUT TO CLIPBOARD *****
WRITE #1,a,Nu,q,h
NEXT a
NEXT Th
NEXT rad
PRINT "bye!"
CLOSE #1
END

```

Appendix 13: Stein and McDonald Model Heat Loss

Stine & McDonald Method .			
	End Plate Radius [m] =	0.127	
	Cavity Radius [m] =	0.33	
	Frustum Length [m] =	0.292	
	Hot Cylindrical Section Length [m] =	0.254	
	Cold Cylindrical Section Length [m] =	0.14	
	T amb [°F] =	70	
	Aperture Radius [m] =	0.0762	
	Total Area [m^2] =	1.70207	
	Grashoff Number =	5.24E+9	
	T mean =	300	
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	44.0	230.0	1.736
15	40.4	211.1	1.593
30	30.9	161.2	1.217
45	18.7	97.7	0.737
60	7.9	41.5	0.313
75	1.6	8.2	0.062
90	0.0	0.0	0.000
	Grashoff Number =	7.51E+9	
	T mean =	400	
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	50.8	380.6	2.002
15	46.6	349.4	1.837
30	35.6	266.8	1.403
45	21.6	161.7	0.850
60	9.2	68.7	0.361
75	1.8	13.5	0.071
90	0.0	0.0	0.000
	Grashoff Number =	9.79E+9	
	T mean =	500	
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	56.6	552.5	2.230
15	51.9	507.2	2.047
30	39.7	387.3	1.563
45	24.0	234.7	0.947
60	10.2	99.7	0.402
75	2.0	19.6	0.079
90	0.0	0.0	0.000
	Grashoff Number =	1.21E+10	
	T mean =	600	
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	61.7	743.3	2.434
15	56.7	682.3	2.234
30	43.3	521.1	1.706
45	26.2	315.8	1.034
60	11.1	134.2	0.439
75	2.2	26.4	0.086
90	0.0	0.0	0.000

Appendix 13: Stein and McDonald Model Heat Loss

Aperture Radius [m] = 0.1524			
Total Area [m^2] = 1.647346			
Grashoff Number = 5.24E+9			
T mean = 300			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	97.4	509.0	3.841
15	89.4	467.3	3.525
30	68.3	356.8	2.692
45	41.4	216.3	1.632
60	17.6	91.9	0.693
75	3.5	18.1	0.136
90	0.0	0.0	0.000
Grashoff Number = 7.51E+9			
T mean = 400			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	112.4	842.3	4.429
15	103.1	773.2	4.066
30	78.8	590.4	3.105
45	47.7	357.8	1.882
60	20.3	152.0	0.799
75	4.0	29.9	0.157
90	0.0	0.0	0.000
Grashoff Number = 9.79E+9			
T mean = 500			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	125.2	1222.7	4.935
15	114.9	1122.4	4.530
30	87.8	857.1	3.459
45	53.2	519.5	2.096
60	22.6	220.7	0.891
75	4.4	43.4	0.175
90	0.0	0.0	0.000
Grashoff Number = 1.21E+10			
T mean = 600			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	136.6	1645.0	5.386
15	125.4	1510.0	4.944
30	95.8	1153.1	3.776
45	58.0	698.9	2.288
60	24.7	296.9	0.972
75	4.8	58.4	0.191
90	0.0	0.0	0.000

Appendix 13: Stein and McDonald Model Heat Loss

Aperture Radius [m] = 0.2286			
Total Area [m^2] = 1.556138			
Grashoff Number = 5.24E+9			
T mean = 300			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	138.7	724.9	5.469
15	127.4	665.4	5.020
30	97.3	508.1	3.834
45	58.9	308.0	2.324
60	25.0	130.8	0.987
75	4.9	25.7	0.194
90	0.0	0.0	0.000
Grashoff Number = 7.51E+9			
T mean = 400			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	160.0	1199.4	6.307
15	146.9	1101.0	5.790
30	112.2	840.8	4.421
45	68.0	509.6	2.680
60	28.9	216.5	1.138
75	5.7	42.6	0.224
90	0.0	0.0	0.000
Grashoff Number = 9.79E+9			
T mean = 500			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	178.3	1741.2	7.027
15	163.6	1598.3	6.450
30	125.0	1220.5	4.926
45	75.7	739.7	2.985
60	32.2	314.3	1.268
75	6.3	61.8	0.249
90	0.0	0.0	0.000
Grashoff Number = 1.21E+10			
T mean = 600			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	194.6	2342.5	7.670
15	178.6	2150.2	7.041
30	136.4	1642.0	5.376
45	82.7	995.2	3.259
60	35.1	422.8	1.384
75	6.9	83.1	0.272
90	0.0	0.0	0.000

Appendix 13: Stein and McDonald Model Heat Loss

Aperture Radius [m] = 0.329			
Total Area [m^2] = 1.380262			
Grashoff Number = 5.24E+9			
T mean = 300			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	163.0	851.5	6.425
15	149.6	781.6	5.897
30	114.2	596.9	4.504
45	69.2	361.8	2.729
60	29.4	153.7	1.160
75	5.8	30.2	0.228
90	0.0	0.0	0.000
Grashoff Number = 7.51E+9			
T mean = 400			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	188.0	1409.0	7.409
15	172.5	1293.3	6.801
30	131.8	987.6	5.194
45	79.9	598.6	3.148
60	33.9	254.3	1.337
75	6.7	50.0	0.263
90	0.0	0.0	0.000
Grashoff Number = 9.79E+9			
T mean = 500			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	209.4	2045.4	8.255
15	192.2	1877.5	7.577
30	146.8	1433.8	5.786
45	89.0	869.0	3.507
60	37.8	369.2	1.490
75	7.4	72.6	0.293
90	0.0	0.0	0.000
Grashoff Number = 1.21E+10			
T mean = 600			
Angle	Nu	Heat Loss	h
[degrees]		[Watts]	[Watts/K-m^2]
0	228.6	2751.7	9.010
15	209.8	2525.9	8.270
30	160.2	1928.9	6.316
45	97.1	1169.0	3.828
60	41.3	496.7	1.626
75	8.1	97.7	0.320
90	0.0	0.0	0.000

Appendix 14: Shape Factors Formulas

All formulas are developed from the basic disc-to-disc shape factor formula ⁽²⁰⁾. The N by N coefficient matrix of the heat loss equation requires N² shape factor equations (Eqn. 1). The shape factor equations are solved using a digital computer. The following section shows the development of the shape factor formulas used in the coefficient matrix.

(a) End Plate (section 1 ↔ aperture):

$$\text{let } R_e = \frac{r_e}{L}, \quad R_a = \frac{r_a}{L}, \quad \text{and } X = 1 + \frac{1 + R_e^2}{R_a^2}$$

$$F_{A_e - A_a} = \frac{A_a}{A_e} F_{A_a - A_e}$$

$$F_{A_e - A_a} = \frac{A_a}{2A_e} \left[X - \sqrt{X^2 - 4 \left(\frac{R_e}{R_a} \right)^2} \right]$$

$$F_{A_e - A_a} = \frac{r_a^2}{2r_e^2} \left[1 + \frac{L^2 + r_e^2}{r_a^2} - \sqrt{\left(1 + \frac{L^2 + r_e^2}{r_a^2} \right)^2 - 4 \left(\frac{r_e}{r_a} \right)^2} \right]$$

$$F_{A_e - A_a} = \frac{1}{2r_e^2} \left\{ (l_c + l_m + l_a)^2 + r_a^2 + r_e^2 - \sqrt{\left[(l_c + l_m + l_a)^2 + r_a^2 + r_e^2 \right]^2 - 4 (r_e r_a)^2} \right\}$$

(b) Center Cylinder (section 3 ↔ aperture):

$$F_{A_a - A_{\text{section}}} = F_{A_a - x\text{-section}_1} - F_{A_a - x\text{-section}_2}$$

$$A_a F_{A_a - A_{\text{section}}} = A_{\text{section}} F_{A_{\text{section}} - A_a}$$

$$F_{A_{\text{section}} - A_a} = \frac{A_a}{A_{\text{section}}} F_{A_a - A_{\text{section}}}$$

$$F_{A_{\text{section}} - A_a} = \frac{A_a}{A_{\text{section}}} [F_{A_a - x\text{-section}_1} - F_{A_a - x\text{-section}_2}]$$

$$F_{A_{\text{section}} - A_a} = \frac{A_a}{A_{\text{section}}} \left[\frac{A_c}{A_a} F_{x\text{-section}_1 - A_a} - \frac{A_c}{A_a} F_{x\text{-section}_2 - A_a} \right]$$

$$F_{A_{\text{section}} - A_a} = \frac{A_c}{A_{\text{section}}} [F_{x\text{-section}_1 - A_a} - F_{x\text{-section}_2 - A_a}]$$

$$F_{A_{\text{section}} - A_a} = \frac{r_c}{2l_b} [F_{x\text{-section}_1 - A_a} - F_{x\text{-section}_2 - A_a}]$$

$$\text{let } R_1 = \frac{r_c}{y}, \quad R_2 = \frac{r_a}{y}, \quad X = 1 + \frac{1 + R_2^2}{R_1^2}$$

$$\text{then } F_{A_{x\text{-section}} - A_a} = \frac{1}{2} \left[X - \sqrt{X^2 - 4 \left(\frac{R_2}{R_1} \right)^2} \right]$$

$$F_{A_{x\text{-section}} - A_a} = \frac{1}{2} \left[1 + \frac{1 + R_2^2}{R_1^2} - \sqrt{\left(1 + \frac{1 + R_2^2}{R_1^2} \right)^2 - 4 \left(\frac{R_2}{R_1} \right)^2} \right]$$

$$F_{A_{x\text{-section}_2} - A_a} = \frac{1}{2} \left[1 + \frac{1 + \frac{r_a^2}{y_2^2}}{\frac{r_c^2}{y_2^2}} - \sqrt{\left(1 + \frac{1 + \frac{r_a^2}{y_2^2}}{\frac{r_c^2}{y_2^2}} \right)^2 - 4 \left(\frac{r_a}{r_c} \right)^2} \right]$$

$$F_{A_{x\text{-section}_2} - A_a} = \frac{1}{2} \left[1 + \frac{y_2^2 + r_a^2}{r_c^2} - \sqrt{\left(1 + \frac{y_2^2 + r_a^2}{r_c^2} \right)^2 - 4 \left(\frac{r_a}{r_c} \right)^2} \right]$$

and similarly:

$$F_{A_{x\text{-section}_1} - A_a} = \frac{1}{2} \left[1 + \frac{y_1^2 + r_a^2}{r_c^2} - \sqrt{\left(1 + \frac{y_1^2 + r_a^2}{r_c^2} \right)^2 - 4 \left(\frac{r_a}{r_c} \right)^2} \right]$$

$$F_{A_{\text{section}} - A_a} = \frac{r_c}{4l_b} \left[\frac{y_1^2 + r_a^2}{r_c^2} - \sqrt{\left(1 + \frac{y_1^2 + r_a^2}{r_c^2} \right)^2 - 4 \left(\frac{r_a}{r_c} \right)^2} - \frac{y_2^2 + r_a^2}{r_c^2} \right. \\ \left. + \sqrt{\left(1 + \frac{y_2^2 + r_a^2}{r_c^2} \right)^2 - 4 \left(\frac{r_a}{r_c} \right)^2} \right]$$

$$F_{A_{\text{section}} - A_a} = \frac{1}{4r_c l_b} \left[y_1^2 - y_2^2 - \sqrt{(r_a^2 + y_1^2 + r_c^2)^2 - 4(r_c r_a)^2} + \sqrt{(r_a^2 + y_2^2 + r_c^2)^2 - 4(r_c r_a)^2} \right]$$

$$F_{A_{\text{section}} - A_a} = \frac{1}{4r_c l_b} \left[(l_a + (n_m - 1)l_b)^2 - (l_a + n_m l_b)^2 - \sqrt{[(l_a + (n_m - 1)l_b)^2 + r_a^2 + r_c^2]^2 - 4(r_c r_a)^2} \right. \\ \left. + \sqrt{[(l_a + n_m l_b)^2 + r_a^2 + r_c^2]^2 - 4(r_c r_a)^2} \right]$$

(c) Frustum (section 2 ↔ aperture):

The view factor for a section of the frustum from A_a is equal to the view factor from A_a to the circular cross-sectional area on the bottom of the frustum section minus the view factor from A_a to the circular cross-section on the top of the frustum section.

$$F_{A_a - A_{section}} = F_{A_a - x-section_1} - F_{A_a - x-section_2}$$

$$A_a F_{A_a - A_{section}} = A_{section} F_{A_{section} - A_a}$$

$$F_{A_{section} - A_a} = \frac{A_a}{A_{section}} F_{A_a - A_{section}}$$

$$F_{A_{section} - A_a} = \frac{A_a}{A_c} [F_{A_a - x-section_1} - F_{A_a - x-section_2}]$$

$$F_{A_{section} - A_a} = \frac{A_a}{A_{section}} \left[\frac{A_{x-section_1}}{A_a} F_{x-section_1 - A_a} - \frac{A_{x-section_2}}{A_a} F_{x-section_2 - A_a} \right]$$

$$F_{A_{section} - A_a} = \frac{1}{A_{section}} [A_{x-section_1} F_{x-section_1 - A_a} - A_{x-section_2} F_{x-section_2 - A_a}]$$

$$F_{A_{section} - A_a} = \frac{1}{(r_1 + r_2)l_b} [r_1^2 F_{x-section_1 - A_a} - r_2^2 F_{x-section_2 - A_a}]$$

$$\text{let } R_1 = \frac{r_{x-section}}{y}, \quad R_2 = \frac{r_a}{y}, \quad X = 1 + \frac{1 + R_2^2}{R_1^2}$$

$$\text{then } F_{A_{X\text{-section}} - A_a} = \frac{1}{2} \left[X - \sqrt{X^2 - 4 \left(\frac{R_2}{R_1} \right)^2} \right]$$

$$F_{A_{X\text{-section}} - A_a} = \frac{1}{2} \left[1 + \frac{1 + R_2^2}{R_1^2} - \sqrt{\left(1 + \frac{1 + R_2^2}{R_1^2} \right)^2 - 4 \left(\frac{R_2}{R_1} \right)^2} \right]$$

$$F_{A_{X\text{-section}_2} - A_a} = \frac{1}{2} \left[1 + \frac{1 + \frac{r_a^2}{h_2^2}}{\frac{r_2^2}{h_2^2}} - \sqrt{\left(1 + \frac{1 + \frac{r_a^2}{h_2^2}}{\frac{r_2^2}{h_2^2}} \right)^2 - 4 \left(\frac{r_a}{r_2} \right)^2} \right]$$

$$F_{A_{X\text{-section}_2} - A_a} = \frac{1}{2} \left[1 + \frac{h_2^2 + r_a^2}{r_2^2} - \sqrt{\left(1 + \frac{h_2^2 + r_a^2}{r_2^2} \right)^2 - 4 \left(\frac{r_a}{r_2} \right)^2} \right]$$

and similarly:

$$F_{A_{X\text{-section}_1} - A_a} = \frac{1}{2} \left[1 + \frac{h_1^2 + r_a^2}{r_1^2} - \sqrt{\left(1 + \frac{h_1^2 + r_a^2}{r_1^2} \right)^2 - 4 \left(\frac{r_a}{r_1} \right)^2} \right]$$

$$F_{A_{\text{section}} - A_a} = \frac{1}{2l_b(r_1 + r_2)} \left[r_1^2 - r_2^2 + h_1^2 - h_2^2 - \sqrt{(r_1^2 + h_1^2 + r_a^2)^2 - 4(r_1 r_a)^2} \right. \\ \left. + \sqrt{(r_2^2 + h_2^2 + r_a^2)^2 - 4(r_2 r_a)^2} \right]$$

$$h_1 = l_a + l_m + (n_m - 1) \frac{l_c}{N_c}$$

$$h_2 = l_a + l_m + n_m \frac{l_c}{N_c}$$

$$r_2 = r_c - n_m \frac{r_c - r_e}{N_c} \quad r_1 = r_c - (n_m - 1) \frac{r_c - r_e}{N_c}$$

$$F_{n_m - A_a} = \frac{1}{2l_b \left[2r_c - (2n_m - 1) \frac{(r_c - r_e)}{N_c} \right]} \left\{ \left[r_c - (n_m - 1) \frac{(r_c - r_e)}{N_c} \right]^2 - \left[r_c - n_m \frac{(r_c - r_e)}{N_c} \right]^2 \right. \\ \left. + \left[l_a + l_m + (n_m - 1) \frac{l_c}{N_c} \right]^2 - \left[l_a + l_m + n_m \frac{l_c}{N_c} \right]^2 \right. \\ \left. - \sqrt{\left\{ \left[r_c - (n_m - 1) \frac{(r_c - r_e)}{N_c} \right]^2 + \left(l_a + l_m + (n_m - 1) \frac{l_c}{N_c} \right)^2 + r_a^2 \right\}^2 - 4 \left\{ \left[r_c - (n_m - 1) \frac{(r_c - r_e)}{N_c} \right] r_a \right\}^2} \right. \\ \left. + \sqrt{\left\{ \left[r_c - n_m \frac{(r_c - r_e)}{N_c} \right]^2 + \left(l_a + l_m + n_m \frac{l_c}{N_c} \right)^2 + r_a^2 \right\}^2 - 4 \left\{ \left[r_c - n_m \frac{(r_c - r_e)}{N_c} \right] r_a \right\}^2} \right\}$$

(d) Spacer Ring (section 4 ↔ aperture):

$$F_{A_a - A_s} = 1 - F_{A_a - A_{x-section}}$$

$$F_{A_s - A_a} = \frac{A_a}{A_s} F_{A_a - A_s}$$

$$F_{A_a - A_{x-section}} = \frac{A_{x-section}}{A_a} F_{A_{x-section} - A_a}$$

$$F_{A_s - A_a} = \frac{A_a}{A_s} \left[1 - \frac{A_{x-section}}{A_a} F_{A_{x-section} - A_a} \right]$$

$$F_{A_{x-section} - A_a} = \frac{1}{2} \left[X - \sqrt{X^2 - 4 \left(\frac{R_a}{R_c} \right)^2} \right]$$

$$F_{A_s - A_a} = \frac{r_a^2}{2r_c l_a} \left\{ 1 - \frac{r_c^2}{2r_a^2} \left[X - \sqrt{X^2 - 4 \left(\frac{R_a}{R_c} \right)^2} \right] \right\}$$

$$\text{where } R_a = \frac{r_a}{l_a}, \quad R_c = \frac{r_c}{l_a}$$

$$X = 1 + \frac{1 + \left(\frac{r_a}{l_a}\right)^2}{\left(\frac{r_c}{l_a}\right)^2}$$

$$X = 1 + \frac{l_a^2 + r_a^2}{r_c^2}$$

therefore:

$$F_{A_{x\text{-section}} - A_a} = \frac{1}{2} \left[1 + \frac{l_a^2 + r_a^2}{r_c^2} - \sqrt{\left(1 + \frac{l_a^2 + r_a^2}{r_c^2}\right)^2 - 4 \left(\frac{r_a}{r_c}\right)^2} \right]$$

$$F_{A_s - A_a} = \frac{r_a^2}{2r_c l_a} \left\{ 1 - \frac{r_c^2}{2r_a^2} \left[1 + \frac{l_a^2 + r_a^2}{r_c^2} - \sqrt{\left(1 + \frac{l_a^2 + r_a^2}{r_c^2}\right)^2 - 4 \left(\frac{r_a}{r_c}\right)^2} \right] \right\}$$

$$F_{A_s - A_a} = \frac{r_a^2}{2r_c l_a} \left\{ 1 - \frac{1}{2r_a^2} [(r_c^2 + l_a^2 + r_a^2) - \sqrt{(r_c^2 + l_a^2 + r_a^2)^2 - 4(r_a r_c)^2}] \right\}$$

(e)(section i and j ↔ section i and j): Shape Factors from a Surface Onto Itself

For the flat surfaces (aperture, annulus, and end plate) $F_{i-i} = 0$

For the cylindrical and frustum sections:

$$F_{i-i} = 1 - F_{i-x1} - F_{i-x2}$$

$$F_{i-x1} = \frac{A_{x1}}{A_i} F_{x1-i} \quad \text{and} \quad F_{i-x2} = \frac{A_{x2}}{A_i} F_{x2-i}$$

therefore

$$F_{i-x1} = \frac{A_{x1}}{A_i} F_{x1-i} \quad \text{and} \quad F_{i-x2} = \frac{A_{x2}}{A_i} F_{x2-i}$$

and

$$F_{x1-i} = 1 - F_{x1-x2} \quad \text{and} \quad F_{x2-i} = 1 - F_{x2-x1}$$

$$F_{x2-x1} = \frac{A_{x1}}{A_{x2}} F_{x1-x2}$$

$$F_{i-i} = 1 - \frac{A_{x1}}{A_i} [1 - F_{x1-x2}] - \frac{A_{x2}}{A_i} \left[1 - \frac{A_{x1}}{A_{x2}} F_{x1-x2} \right]$$

$$F_{i-i} = 1 - \frac{A_{x1}}{A_i} - \frac{A_{x2}}{A_i} + 2 \frac{A_{x1}}{A_i} F_{x1-x2}$$

$$F_{x1-x2} = \frac{1}{2} \left[X - \sqrt{X^2 - 4 \left[\frac{R_2}{R_1} \right]^2} \right]$$

$$\text{where } R_1 = \frac{r_1}{h}, \quad R_2 = \frac{r_2}{h}, \quad \text{and } X = 1 + \frac{h^2 + r_2^2}{r_1^2}$$

$$F_{x1-x2} = \frac{1}{2} \left[1 + \frac{h^2 + r_2^2}{r_1^2} - \sqrt{\left[1 + \frac{h^2 + r_2^2}{r_1^2} \right]^2 - 4 \left[\frac{r_2}{r_1} \right]^2} \right]$$

$$F_{i-i} = 1 - \frac{A_{x1}}{A_i} - \frac{A_{x2}}{A_i} + \frac{A_{x1}}{A_i} \left[1 + \frac{h^2 + r_2^2}{r_1^2} - \sqrt{\left[1 + \frac{h^2 + r_2^2}{r_1^2} \right]^2 - 4 \left[\frac{r_2}{r_1} \right]^2} \right]$$

$$F_{i-i} = 1 - \frac{r_2^2}{(r_1 + r_2)l_b} + \frac{r_1^2}{(r_1 + r_2)l_b} \left[\frac{h^2 + r_2^2}{r_1^2} - \sqrt{\left[1 + \frac{h^2 + r_2^2}{r_1^2} \right]^2 - 4 \left[\frac{r_2}{r_1} \right]^2} \right]$$

For the spacer ring (section 4 ↔ section 4):

$$r_1 = r_2 = r_c \quad \text{and} \quad h = l_a$$

For the hot cylinder (section 3_{band i} ↔ section 3_{band i}):

$$r_1 = r_2 = r_c \quad \text{and} \quad h = l_b$$

For the frustum (section 2_{band i} ↔ section 2_{band j}):

$$r_1 = r_c - (r_c - r_e) \frac{(n_c - 1)}{N_c}, \quad r_2 = r_c - (r_c - r_e) \frac{n_c}{N_c}, \quad \text{and } h = \frac{l_{cb}}{\sqrt{l_c^2 + (r_c - r_e)^2}}$$

Shape Factors from Bands of the Cylindrical and Frustum Sections to other Bands of the Cylindrical and Frustum Sections (section i_{band j} ↔ section i_{band k}):

The following shape factor formulas are used between different bands of the frustum section, between different bands of the hot cylindrical section, between bands of the hot cylindrical section and bands of the frustum section, between the spacer ring and bands of the hot cylindrical section, and between the spacer ring and bands of the frustum section.

$$F_{i-j} = F_{i-x2} - F_{i-x1}$$

$$F_{x1-i} = F_{xi-x3} - F_{x1-x4}$$

$$F_{x2-i} = F_{x2-x3} - F_{x2-x4}$$

$$F_{i-x1} = \frac{A_{x1}}{A_i} F_{x1-i} \quad \text{and} \quad F_{i-x2} = \frac{A_{x2}}{A_i} F_{x2-i}$$

$$F_{i-j} = \frac{A_{x2}}{A_i} [F_{x2-x3} - F_{x2-x4}] - \frac{A_{x1}}{A_i} [F_{x1-x3} - F_{x1-x4}]$$

$$F_{i-j} = \frac{r_2^2}{(r_3 + r_4)l_b} [F_{x2-x3} - F_{x2-x4}] - \frac{r_1^2}{(r_3 + r_4)l_b} [F_{x1-x3} - F_{x1-x4}]$$

$$F_{xn-xm} = \frac{1}{2} \left[1 + \frac{h_{nm}^2 + r_m^2}{r_n^2} - \sqrt{\left[1 + \frac{h_{nm}^2 + r_m^2}{r_n^2} \right]^2 - 4 \left[\frac{r_m}{r_n} \right]^2} \right]$$

between different bands of the frustum section (section 2_{band i} ↔ section 2_{band j}):

$$r_1 = r_c - (r_c - r_e) \frac{n_j}{N_c}$$

$$r_2 = r_c - (r_c - r_e) \frac{(n_j - 1)}{N_c}$$

$$r_3 = r_c - (r_c - r_e) \frac{n_i}{N_c}$$

$$r_4 = r_c - (r_c - r_e) \frac{(n_i - 1)}{N_c}$$

$$h = \frac{l_c l_b}{\sqrt{l_c^2 + (r_c - r_e)^2}}$$

$$h_{13} = h_{24} = (n_j - n_i)h$$

$$h_{14} = (n_j - n_i + 1)h$$

$$h_{23} = (n_j - n_i - 1)h$$

between different bands of the hot cylindrical section (section 3_{band i} ↔ section 3_{band j}) :

$$r_1 = r_2 = r_3 = r_4 = r_c$$

$$h_{13} = h_{24} = (n_j - n_i)l_b$$

$$h_{14} = (n_j - n_i + 1)l_b$$

$$h_{23} = (n_j - n_i - 1)l_b$$

between bands of the hot cylindrical section and bands of the frustum section
(section 2_{band i} ↔ section 3_{band j}):

$$r_1 = r_c - (r_c - r_o) \frac{n_j}{N_c}$$

$$r_2 = r_c - (r_c - r_o) \frac{(n_j - 1)}{N_c}$$

$$r_3 = r_4 = r_c$$

$$h = \frac{l_c l_b}{\sqrt{l_c^2 + (r_c - r_o)^2}}$$

$$h_{13} = h_{24} = l_m - n_i l_b + n_j h$$

$$h_{14} = l_m - (n_i - 1) l_b + n_j h$$

$$h_{23} = l_m - n_i l_b + (n_j - 1) h$$

between the spacer ring and bands of the hot cylindrical section
(section 4 ↔ section 3_{band i}):

$$F_{\text{spacer} - j} = \frac{r_2^2}{(r_3 + r_4) l_a} [F_{x2 - x3} - F_{x21 - x4}] - \frac{r_1^2}{(r_3 + r_4) l_a} [F_{x1 - x3} - F_{x1 - x4}]$$

$$F_{x_n - x_m} = \frac{1}{2} \left[1 + \frac{h_{nm}^2 + r_m^2}{r_n^2} - \sqrt{\left[1 + \frac{h_{nm}^2 + r_m^2}{r_n^2} \right]^2 - 4 \left[\frac{r_m}{r_n} \right]^2} \right]$$

$$r_1 = r_2 = r_3 = r_4 = r_c$$

$$h_{13} = n_j l_b$$

$$h_{14} = n_j l_b + l_a$$

$$h_{23} = (n_j - 1) l_b$$

$$h_{24} = (n_j - 1) l_b + l_a$$

between the spacer ring and bands of the frustum section
(section 4 ↔ section 2_{band i}):

$$r_1 = r_c - (r_c - r_e) \frac{n_j}{N_c}$$

$$r_2 = r_c - (r_c - r_e) \frac{(n_j - 1)}{N_c}$$

$$r_3 = r_4 = r_c$$

$$h = \frac{l_c l_b}{\sqrt{l_c^2 + (r_c - r_e)^2}}$$

$$h_{13} = l_m + n_j h$$

$$h_{14} = l_m + n_j h + l_a$$

$$h_{23} = l_m + (n_j - 1) h$$

$$h_{24} = l_m + (n_j - 1) h + l_a$$

Shape Factors from Circular Sections to Bands of the Cylindrical and Frustum Sections:

The following shape factor formulas are used between the end plate and bands of the hot cylindrical section, bands of the frustum section, and the spacer section, between the aperture and the bands of the hot cylindrical section, bands of the frustum section, and the spacer section, and between the annulus and aperture combined and bands of the hot cylindrical section, bands of the frustum section, and the spacer section.

$$F_{i-j} = F_{i-x2} - F_{i-x1}$$

$$F_{i-x1} = \frac{1}{2} \left[1 + \frac{h_{13}^2 + r_1^2}{r_3^2} - \sqrt{\left[1 + \frac{h_{13}^2 + r_1^2}{r_3^2} \right]^2 - 4 \left[\frac{r_1}{r_3} \right]^2} \right]$$

$$F_{i-x2} = \frac{1}{2} \left[1 + \frac{h_{23}^2 + r_2^2}{r_3^2} - \sqrt{\left[1 + \frac{h_{23}^2 + r_2^2}{r_3^2} \right]^2 - 4 \left[\frac{r_2}{r_3} \right]^2} \right]$$

$$F_{i-j} = \frac{1}{2} \left[\frac{h_{23}^2 + r_2^2}{r_3^2} - \sqrt{\left[1 + \frac{h_{23}^2 + r_2^2}{r_3^2} \right]^2 - 4 \left[\frac{r_2}{r_3} \right]^2} \right] - \frac{1}{2} \left[\frac{h_{13}^2 + r_1^2}{r_3^2} - \sqrt{\left[1 + \frac{h_{13}^2 + r_1^2}{r_3^2} \right]^2 - 4 \left[\frac{r_1}{r_3} \right]^2} \right]$$

between the end plate and bands of the hot cylindrical section
(section 1 ↔ section 3_{band i}):

$$r_1 = r_2 = r_c$$

$$r_3 = r_e$$

$$h_{23} = l_c + (N_m - n_j) l_b$$

$$h_{13} = l_c + (N_m - n_j + 1) l_b$$

between the end plate and bands of the frustum section
(section 1 ↔ section 2_{band i}):

$$r_1 = r_e + (r_c - r_e) \left[1 - \frac{n_j - 1}{N_c} \right]$$

$$r_2 = r_e + (r_c - r_e) \left[1 - \frac{n_j}{N_c} \right]$$

$$r_3 = r_e$$

$$h = \frac{l_c l_b}{\sqrt{l_c^2 + (r_c - r_e)^2}}$$

$$h_{23} = (N_c - n_j) h$$

$$h_{13} = (N_c - n_j + 1) h$$

between the end plate and the spacer section
(section 1 ↔ section 4):

$$r_1 = r_2 = r_c$$

$$r_3 = r_e$$

$$h_{23} = l_c + l_m$$

$$h_{13} = l_c + l_m + l_a$$

between the annulus and aperture combined and bands of the hot cylindrical section
(section 5+ aperture ↔ section 3_{band i}):

$$r_1 = r_2 = r_3 = r_c$$

$$h_{23} = l_a + (n_j - 1) l_b$$

$$h_{13} = l_a + n_j l_b$$

between the annulus and aperture combined and bands of the frustum section
(section 5+ aperture ↔ section 2_{band i}):

$$r_1 = r_c - n_j \frac{(r_c - r_e)}{N_c}$$

$$r_2 = r_c - (n_j - 1) \frac{(r_c - r_e)}{N_c}$$

$$r_3 = r_c$$

$$h = \frac{l_c l_b}{\sqrt{l_c^2 + (r_c - r_e)^2}}$$

$$h_{23} = l_a + l_m + (n_j - 1) h$$

$$h_{13} = l_a + l_m + n_j h$$

between the annulus and aperture combined and the spacer section
(section 5+ aperture ↔ section 4):

$$r_1 = r_2 = r_3 = r_c$$

$$h_{23} = 0$$

$$h_{13} = l_a$$

between the aperture and bands of the hot cylindrical section
(aperture $\leftrightarrow$ section 3bands i):

$$r_1 = r_2 = r_c$$

$$r_3 = r_a$$

$$h_{23} = l_a + (n_j - 1) l_b$$

$$h_{13} = l_a + n_j l_b$$

between the aperture and bands of the frustum section
(aperture $\leftrightarrow$ section 2bands i):

$$r_1 = r_c - n_j \frac{(r_c - r_e)}{N_c}$$

$$r_2 = r_c - (n_j - 1) \frac{(r_c - r_e)}{N_c}$$

$$r_3 = r_a$$

$$h = \frac{l_c l_b}{\sqrt{l_c^2 + (r_c - r_e)^2}}$$

$$h_{23} = l_a + l_m + (n_j - 1) h$$

$$h_{13} = l_a + l_m + n_j h$$

between the aperture and the spacer section
(aperture $\leftrightarrow$ section 4):

$$r_1 = r_2 = r_c$$

$$r_3 = r_a$$

$$h_{23} = 0$$

$$h_{13} = l_a$$

Shape Factors from Circular Sections to Other Circular Sections:

The following shape factor formulas are used between the end plate and the aperture: and between the end plate and the aperture and annulus combined.

$$F_{i-j} = \frac{1}{2} \left[1 + \frac{h^2 + r_j^2}{r_i^2} - \sqrt{\left[1 + \frac{h^2 + r_j^2}{r_i^2} \right]^2 - 4 \left[\frac{r_j}{r_i} \right]^2} \right]$$

between the end plate and the aperture
(section 1 ↔ aperture):

$$r_i = r_e$$

$$r_j = r_a$$

$$h = l_a + l_m + l_c$$

between the end plate and the aperture and annulus combined
(section 1 ↔ aperture + section 5):

$$r_i = r_e$$

$$r_j = r_c$$

$$h = l_a + l_m + l_c$$

For shape factors from the spacer section, bands of the hot cylindrical section, and bands of the frustum section to the annulus section the following relationship is used:

$$F_{i - \text{annulus}} = F_{i - (\text{annulus} + \text{aperture})} - F_{i - \text{aperture}}$$

Appendix 15: Analytical Thermal Radiation Heat Loss Program Listing

```

REM
REM
REM *****
REM THEORETICAL THERMAL RADIATION HEAT LOSS PROGRAM
REM *****
REM This program predicts the thermal radiative heat loss from
REM the cavity solar receiver using the net radiation method.
REM
REM DIFFUSE GRAY BODY VERSION
REM This section of the program is used to verify the thermal radiation
REM shape factor formulas of the solar cavity receiver.
REM
REM *****
REM
OPEN "Ther Rad Program Output" FOR OUTPUT AS #1
WRITE#1,"aperture","operating","radiative"
WRITE#1,"diameter","temperature","heat loss"
WRITE#1,"[in]","[°F]","[Watts]"
REM *****
REM nomenclature
REM *****
REM re = end plate radius
REM rc = cavity radius
REM ra = aperture radius
REM lc = length of frustum section
REM lm = length of hot cylindrical section
REM la = length of cold cylindrical section
REM lbc = width of hot isothermal bands in frustum section
REM lbm = width of hot isothermal bands in hot cylindrical section
REM Nc = number of bands in frustum section
REM Nm = number of bands in hot cylindrical section
REM
REM constants
REM *****
S=5.729*10^-8 :REM Stephan-Boltzmann constant W/(m^2 K^4)
pi=3.14
REM *****
REM CAVITY GEOMETRY
REM *****
re=.254/2
rc=.33
lc=.292
la=.14
lm=.686-lc-la
Nm=15!
lbm=lm/Nm
Nc=23!
lbc=SQR((rc-re)^2+lc^2)/Nc
hc=lc*lbc/SQR((rc-re)^2+lc^2)
DIM rad(12),Top(12)
FOR n=1 TO 12
READ rad(n)
DATA 0.2286,0.2286,0.2286,0.2286,.0762,.0762,.1524,.1524,.2286,.2

```

```

286,.3302,.3302
NEXT n
FOR n=1 TO 12
READ Top(n)
DATA 300,400,500,600,400,600,400,600,400,600,400,600
NEXT n
Tdiff=20 :REM assumed temperature difference between inlet and outlet
REM *****
REM This section determines the total number of elements that make
REM up the internal surface of the cavity receiver.
REM *****
NT=Nc+Nm+4
DIM F(NT,NT),sum(NT),A(NT,NT),E(NT),T(NT),C(NT),q(NT),G(NT,NT+1)
,M(NT+1)
REM F(I,J) is the shape factor matrix
REM sum(NT) is a shape factor verification array
REM A(NT,NT) is the coefficient matrix
REM E(NT) is the emissivity array
REM T(NT) is the temperature array
REM C(NT) is the constant array
REM G(NT,NT+1) is the augmented Gaussian matrix
REM q(NT) is the outgoing radiant energy flux ( radiosity )
REM *****
REM This section defines the numbering of elements that make
REM up the internal surface of the cavity receiver.
REM *****
REM aperture = 1
REM annulus = 2
REM spacer ring = 3
REM end plate = 4
REM hot cylindrical section is numbered 5 thru Nm+4
REM frustum section is numbered Nm+5 thru Nc + 6
REM *****
REM EMISSIVITY ARRAY INPUT SECTION
REM *****
E(1)=0 :REM emissivity of the aperture
E(2)=.7 :REM emissivity of the annulus
E(3)=.7 :REM emissivity of the spacer section
E(4)=.7 :REM emissivity of the end plate
FOR n=5 TO NT
E(n)=.85
NEXT n
REM *****
REM BEGINNING OF APERTURE RADIUS VARIATION LOOP
REM *****
numT=4
FOR samp=1 TO 12
ra=rad(samp)
REM *****
REM SHAPE FACTORS CALCULATION SECTION
REM *****
REM ***** Shape factors for each element onto itself *****
REM *****
REM ***** For flat surfaces  $F_{i-i} = 0$  *****

```

```

F(1,1)=0
F(2,2)=0
F(4,4)=0 :REM aperture, annulus , and end plate
REM      ***** spacer section *****
ri=rc
rj=rc
h=la
GOSUB shape
F(3,3)=1-ri^2/((ri+rj)*la)*(1-FF)-rj^2/((ri+rj)*la)*(1-rj^2/ri^2*FF)
REM      ***** hot cylindrical section *****
ri=rc
rj=rc
h=lbm
GOSUB shape
FOR n=1 TO Nm
k=n+4
F(k,k)=1-ri^2/((ri+rj)*lbm)*(1-FF)-rj^2/((ri+rj)*lbm)*(1-rj^2/ri^2*FF)
NEXT n
REM      ***** frustum section *****
h=hc
FOR n=1 TO Nc
ri=rc-(rc-re)*n/Nc
rj=rc-(rc-re)*(n-1)/Nc
GOSUB shape
k=Nm+4+n
F(k,k)=1-ri^2/((ri+rj)*lbc)*(1-FF)-rj^2/((ri+rj)*lbc)*(1-ri^2/rj^2*FF)
NEXT n
REM      *****
REM      Shape factor from elements of the cylindrical and frustum sections
REM      to other elements of the cylindrical and frustum sections
REM      *****
REM      ***** between different elements of the frustum section *****
FOR M=1 TO Nc-1
FOR n=M+1 TO Nc
r1=rc-(rc-re)*n/Nc
r2=rc-(rc-re)*(n-1)/Nc
r3=rc-(rc-re)*M/Nc
r4=rc-(rc-re)*(M-1)/Nc
h13=(n-M)*hc
h24=h13
h14=(n-M+1)*hc
h23=(n-M-1)*hc
h=h13
ri=r1
rj=r3
GOSUB shape
F13=FF
h=h23
ri=r2
rj=r3
GOSUB shape
F23=FF
h=h14
ri=r1
rj=r4

```

```

GOSUB shape
F14=FF
h=h24
ri=r2
rj=r4
GOSUB shape
F24=FF
i=Nm+4+M
j=Nm+4+n

$$F(i,j)=r2^2/((r3+r4)*lbc)*(F23-F24)-r1^2/((r3+r4)*lbc)*(F13-F14)$$


$$F(j,i)=(r3+r4)/(r1+r2)*F(i,j)$$

NEXT n
NEXT M
REM *** between different elements of the hot cylindrical section ****
FOR M=1 TO Nm-1
FOR n=M+1 TO Nm
r1=rc
r2=rc
r3=rc
r4=rc
h13=(n-M)*lbc
h24=h13
h14=(n-M+1)*lbc
h23=(n-M-1)*lbc
h=h13
ri=r1
rj=r3
GOSUB shape
F13=FF
h=h23
ri=r2
rj=r3
GOSUB shape
F23=FF
h=h14
ri=r1
rj=r4
GOSUB shape
F14=FF
h=h24
ri=r2
rj=r4
GOSUB shape
F24=FF
i=4+M
j=4+n

$$F(i,j)=r2^2/((r3+r4)*lbc)*(F23-F24)-r1^2/((r3+r4)*lbc)*(F13-F14)$$


$$F(j,i)=(r3+r4)/(r1+r2)*F(i,j)$$

NEXT n
NEXT M
REM *****
REM *** Shape factors between elements of the hot cylindrical ***
REM *** section and elements of the frustum section ****
REM *****
FOR M=1 TO Nm

```

```

FOR n=1 TO Nc
r1=rc-(rc-re)*n/Nc
r2=rc-(rc-re)*(n-1)/Nc
r3=rc
r4=rc
h13=lm-M*lbm+n*hc
h24=lm-(M-1)*lbm+(n-1)*hc
h14=lm-(M-1)*lbm+n*hc
h23=lm-M*lbm+(n-1)*hc
h=h13
ri=r1
rj=r3
GOSUB shape
F13=FF
h=h23
ri=r2
rj=r3
GOSUB shape
F23=FF
h=h14
ri=r1
rj=r4
GOSUB shape
F14=FF
h=h24
ri=r2
rj=r4
GOSUB shape
F24=FF
i=M+4
j=n+4+Nm
F(i,j)=r2^2/((r3+r4)*lbm)*(F23-F24)-r1^2/((r3+r4)*lbm)*(F13-F14)
F(j,i)=(r3+r4)*lbm/((r1+r2)*lbc)*F(i,j)
NEXT n
NEXT M
REM *****
REM *** Shape factors between the spacer section and elements ****
REM *** of the hot cylindrical section*****
REM *****
FOR n=1 TO Nm
r1=rc
r2=rc
r3=rc
r4=rc
h13=n*lbm
h24=(n-1)*lbm+la
h14=n*lbm+la
h23=(n-1)*lbm
h=h13
ri=r1
rj=r3
GOSUB shape
F13=FF
h=h23
ri=r2

```

```

rj=r3
GOSUB shape
F23=FF
h=h14
ri=r1
rj=r4
GOSUB shape
F14=FF
h=h24
ri=r2
rj=r4
GOSUB shape
F24=FF
i=3
j=n+4
F(i,j)=r2^2/((r3+r4)*la)*(F23-F24)-r1^2/((r3+r4)*la)*(F13-F1  4)
F(j,i)=(r3+r4)*la/((r1+r2)*lbm)*F(i,j)
NEXT n
REM *****
REM *** Shape factors between the spacer section and elements ***
REM *** of the frustum section ***
REM *****
FOR n=1 TO Nc
r1=rc-(rc-re)*n/Nc
r2=rc-(rc-re)*(n-1)/Nc
r3=rc
r4=rc
h13=lm+n*hc
h24=lm+la+(n-1)*hc
h14=lm+la+n*hc
h23=lm+(n-1)*hc
h=h13
ri=r1
rj=r3
GOSUB shape
F13=FF
h=h23
ri=r2
rj=r3
GOSUB shape
F23=FF
h=h14
ri=r1
rj=r4
GOSUB shape
F14=FF
h=h24
ri=r2
rj=r4
GOSUB shape
F24=FF
i=3
j=n+4+Nm
F(i,j)=r2^2/((r3+r4)*la)*(F23-F24)-r1^2/((r3+r4)*la)*(F13-F1  4)
F(j,i)=(r3+r4)*la/((r1+r2)*lbc)*F(i,j)

```

```

NEXT n
REM *****
REM Shape factors between circular sections and the spacer section,
REM elements of the hot cylindrical section, and elements of the
REM frustum section.
REM *****
REM **between the end plate and elements of the hot cylindrical section *
r3=re
r1=rc
r2=rc
FOR n=1 TO Nm
h23=lc+lm-n*lbm
h13=lc+lm-(n-1)*lbm
ri=r3
rj=r1
h=h13
GOSUB shape
F31=FF
ri=r3
rj=r2
h=h23
GOSUB shape
F32=FF
i=4
j=4+n
F(i,j)=F32-F31
F(j,i)=r3^2/((r1+r2)*lbm)*F(i,j)
NEXT n
REM **between the end plate and elements of the frustum section **
r3=re
FOR n=1 TO Nc
r1=re+(rc-re)*(1-(n-1)/Nc)
r2=re+(rc-re)*(1-n/Nc)
h23=lc-n*hc
h13=lc-(n-1)*hc
ri=r3
rj=r1
h=h13
GOSUB shape
F31=FF
ri=r3
rj=r2
h=h23
GOSUB shape
F32=FF
i=4
j=4+Nm+n
F(i,j)=F32-F31
F(j,i)=r3^2/((r1+r2)*lbc)*F(i,j)
NEXT n
REM **between the end plate and the spacer section **
r3=re
r1=rc
r2=rc
h23=lc+lm

```

```

h13=lc+lm+la
ri=r3
rj=r1
h=h13
GOSUB shape
F31=FF
ri=r3
rj=r2
h=h23
GOSUB shape
F32=FF
i=4
j=3
F(i,j)=F32-F31
F(j,i)=r3^2/((r1+r2)*la)*F(i,j)
REM  **between the aperture and elements of the hot cylindrical section **
r3=ra
r1=rc
r2=rc
FOR n=1 TO Nm
h23=la+(n-1)*lbm
h13=la+n*lbm
ri=r3
rj=r1
h=h13
GOSUB shape
F31=FF
ri=r3
rj=r2
h=h23
GOSUB shape
F32=FF
i=1
j=4+n
F(i,j)=F32-F31
F(j,i)=r3^2/((r1+r2)*lbm)*F(i,j)
NEXT n
REM  **between the aperture and elements of the frustum section **
r3=ra
FOR n=1 TO Nc
r1=rc-n*(rc-re)/Nc
r2=rc-(n-1)*(rc-re)/Nc
h23=la+lm+(n-1)*hc
h13=la+lm+n*hc
ri=r3
rj=r1
h=h13
GOSUB shape
F31=FF
ri=r3
rj=r2
h=h23
GOSUB shape
F32=FF
i=1

```



```

j=4+n+Nm
F(i,j)=F32-F31
F(j,i)=r3^2/((r1+r2)*lbc)*F(i,j)
NEXT n
REM   **between the aperture and the spacer section **
ri=ra
rj=rc
h=la
GOSUB shape
i=1
j=3
F(i,j)=1-FF
F(j,i)=ri^2/(2*rj*la)*F(i,j)
REM   *****
REM   Shape factors for the annulus section are determined by the differences
REM   between shape factors of the annulus and aperture combined with
REM   an element and the aperture with an element.
REM   *****
REM   **between the annulus and elements of the hot cylindrical section **
r3=rc
r1=rc
r2=rc
FOR n=1 TO Nm
h23=la+(n-1)*lbm
h13=la+n*lbm
ri=r3
rj=r1
h=h13
GOSUB shape
F31=FF
ri=r3
rj=r2
h=h23
GOSUB shape
F32=FF
i=2
j=4+n
F(i,j)=(rc^2*(F32-F31)-ra^2*F(1,j))/(rc^2-ra^2)
F(j,i)=(rc^2-ra^2)/((r1+r2)*lbm)*F(i,j)
NEXT n
REM   **between the annulus and elements of the frustum section **
r3=rc
FOR n=1 TO Nc
r1=rc-n*(rc-re)/Nc
r2=rc-(n-1)*(rc-re)/Nc
h23=la+lm+(n-1)*hc
h13=la+lm+n*hc
ri=r3
rj=r1
h=h13
GOSUB shape
F31=FF
ri=r3
rj=r2
h=h23

```

```

GOSUB shape
F32=FF
i=2
j=4+n+Nm
F(i,j)=(rc^2*(F32-F31)-ra^2*F(1,j))/(rc^2-ra^2)
F(j,i)=(rc^2-ra^2)/((r1+r2)*lbc)*F(i,j)
NEXT n
REM    **between the annulus and the spacer section **
r1=rc
r2=rc
r3=ra
ri=r1
rj=r2
h=la
GOSUB shape
F12=FF
ri=r1
rj=r3
GOSUB shape
F13=FF
i=2
j=3
F(i,j)=1-rc^2/(rc^2-ra^2)*(F12-F13)
F(j,i)=(rc^2-ra^2)/((r1+r2)*la)*F(i,j)
REM
REM    Shape factors from circular section to other circular sections
REM
REM    ***** between the end plate and the aperture *****
ri=re
rj=ra
h=la+lm+lc
GOSUB shape
i=4
j=1
F(i,j)=FF
F(j,i)=re^2/ra^2*F(i,j)
REM    ***** between the end plate and the annulus *****
ri=re
rj=rc
h=la+lm+lc
GOSUB shape
i=4
j=2
F(i,j)=FF-F(i,1)
F(j,i)=re^2/(rc^2-ra^2)*F(i,j)
REM
REM    Shape factors matrix output
REM
FOR i=1 TO NT
FOR j=1 TO NT-1
PRINT USING "#.###";F(i,j);
PRINT SPC(1);
NEXT j
PRINT USING "#.###";F(i,NT)
PRINT

```

```

NEXT i
111 :
REM *****
REM The sum of the shape factors for one element to all the elements
REM of the enclosure is equal to one. This property is used to verify
REM the shape factors previously calculated. For an enclosure of N
REM elements the sum of all the shape factors should equal N.
REM *****
FOR i=1 TO NT
FOR j=1 TO NT
sum(i)=0
NEXT j
NEXT i
SUMT=0
FOR i=1 TO NT
FOR j=1 TO NT
sum(i)=sum(i)+F(i,j)
SUMT=SUMT+sum(i)
NEXT j
NEXT i
PRINT *****
FOR i=1 TO NT-1
PRINT " SUM ";i;" = ";
PRINT USING "##.####";sum(i)
NEXT i
i=NT
PRINT "SUM ";i;" = ";
PRINT USING "##.####";sum(i)
PRINT *****
222 :
REM *****
REM END OF SHAPE FACTOR SECTION
REM *****
REM *****
REM *****
REM COEFFICIENTS MATRIX CALCULATIONS SECTION
REM *****
FOR i=1 TO NT
FOR j=1 TO NT
KD=1
IF i=j THEN 400
KD=0
400 :
A(i,j)=KD-(1-E(i))*F(i,j)
NEXT j
NEXT i
REM *****
REM coefficient matrix output
REM *****
FOR i=1 TO NT
FOR j=1 TO NT-1
PRINT USING "##.####";A(i,j);
PRINT SPC(1);
NEXT j
PRINT USING "##.####";A(i,NT)

```

```

PRINT
NEXT i
333 :
REM *****
REM BEGINNING OF TEMPERATURE
REM *****
REM *****
REM TEMPERATURE ARRAY INPUT SECTION
REM *****
Tmean=Top(samp)
Tin=Top(samp)+Tdiff/2:Tout=Top(samp)-Tdiff/2
PRINT Tin,Tout,Tmean
REM
REM Each element is assumed to be isothermal. Angular temperature
REM measurements for the hot cylindrical section and the frustum
REM section are averaged to give one temperature for each band. The
REM axial temperature values are determined from linear extrapolation
REM from band with temperature measurements. Temperature values
REM are in Kelvin.
T(1)=0 :REM temperature of the aperture opening
FOR n=2 TO 4 :REM temperature of the refractory surfaces
T(n)=((Tmean-40)-32)*5/9+273.15
NEXT n
FOR n=5 TO NT
T(n)=((Tout+(Tin-Tout)*(n-5)/(NT-5))-32)*5/9+273.15
NEXT n
REM ***** OUTPUT THE TEMPERATURE DISTRIBUTION *****
FOR n=1 TO NT
PRINT "T(;"n;"= ";T(n)
NEXT n
REM *****
REM CONSTANT ARRAY CALCULATION SECTION
REM *****
FOR n=1 TO NT
C(n)=E(n)*S*T(n)^4
NEXT n
REM *****
REM HEAT FLUX SOLUTIONS
REM *****
REM
REM Gaussian Elimination method is used to solve for the heat output
REM of each surface, including the total heat lost from the receiver
REM through the aperture.
REM ***** augmented matrix *****
FOR i=1 TO NT
FOR j=1 TO NT
G(i,j)=A(i,j)
NEXT j
G(i,NT+1)=C(i)
NEXT i
GOSUB Gauss
REM *****
REM OUTPUT OF HEAT LOSS THROUGH APERTURE AND HEAT
REM RADIATED FROM ALL OTHER ELEMENTS

```

[illegible]

```

M(j)=G(1,j)
NEXT j
FOR i=1 TO NT-1
FOR j=1 TO NT+1
G(i,j)=G(i+1,j)
NEXT j
NEXT i
FOR j=1 TO NT+1
G(NT,j)=M(j)
NEXT j
GOTO 444
REM ***** PRINT CYCLE *****
CLS
FOR M=1 TO NT
FOR n=1 TO NT
PRINT G(M,n);SPC(5);
NEXT n
PRINT G(M,NT+1)
NEXT M
REM *****
444 :
GOTO Gauss
Elimination:
REM ***** Gaussian Elimination. *****
FOR k=1 TO NT
ss=G(k,k)
FOR j=1 TO NT+1
G(k,j)=G(k,j)/ss
NEXT j
FOR i=k+1 TO NT
ss=G(i,k)
FOR j=1 TO NT+1
G(i,j)=G(i,j)-ss*G(k,j)
NEXT j
NEXT i
NEXT k
REM
FOR k=1 TO NT-1
FOR i=1 TO NT-k
ss=G(i,NT-k+1)
FOR j=1 TO NT+1
G(i,j)=G(i,j)-ss*G(NT-k+1,j)
NEXT j
NEXT i
NEXT k
GOTO 555
REM ***** PRINT CYCLE *****
CLS
FOR M=1 TO NT
FOR n=1 TO NT
PRINT G(M,n);SPC(5);
NEXT n
PRINT G(M,NT+1)
NEXT M
REM *****

```

```
555 :  
FOR i=1 TO NT  
q(i)=G(i,NT+1)  
NEXT i  
IF Flag=0 GOTO 600  
FOR k=1 TO Flag  
qq=q(NT)  
FOR i=2 TO NT  
q(i)=q(i-1)  
NEXT i  
q(1)=qq  
NEXT k  
600 :  
RETURN
```

Appendix 16: Flow Meter Factory Calibration Specifications

FLOW TECHNOLOGY, INC. MECHANICAL DATASHEET 7412

Customer: CAL POLY KELLOG UNIT
Meter Model #: FT4-BAEXB-LAD-G
Meter Serial #: 8407412
End Fitting: MG-32556-B
Bearing Type: CARBIDE
Pickoff Type: HI-TEMP MAG
Pickoff P/N: 80666-104

Job #: 23194
Tap #:
Size: 1/2"
Cal. Media: FREON TE
Viscosity: 0.83 CTS
Temperature: 75.00 °F
Density: 12.18 #/

Meter Freq (Hz)	Meter Flow Rate (GAL/Min)	Meter K Factor (P/GAL)	Freq / Viscosity (Hz/CTS)
2052.7	3.0718	40094.49	2464.262
1472.5	2.1931	40285.28	1767.664
1066.1	1.5824	40424.25	1279.887
777.27	1.1515	40501.43	933.099
559.29	0.8308	40391.61	671.420
408.40	0.6096	40198.27	490.281
286.39	0.4313	39845.83	343.811
205.55	0.3158	39056.52	246.761
151.03	0.2351	38542.37	181.309
113.86	0.1797	38012.29	136.690

Calibrated by: R. GAYAGAN

Calib Inv #: 51092

Certified by:

Calib Recal Date: 10/1/87

Date: 4/10/87

Signal Output: 7 Mv @ 113 Hz

Appendix 17: Flow Meters Voltage Output

Factory Flow	Flow 1	Flow 2	cor Flow	cor Flow 2	ΔFlow 1	ΔFlow 2
[volts]	[volts]	[volts]	[volts]	[volts]	[volts]	[volts]
-0.0017	0.9092	1.0031	-0.214859	-0.08714	-0.2131588	-0.0954395
-0.0017	0.9088	1.0022	-0.214843	-0.100002	-0.2143432	-0.0983022
-0.0017	0.9122	1.0022	-0.205876	-0.100002	-0.2042758	-0.0983022
-0.0017	0.9147	1.0022	-0.198573	-0.100002	-0.1968733	-0.0983022
-0.0017	0.9184	1.0022	-0.19354	-0.100002	-0.1918996	-0.0983022
1.7420	1.6329	1.6224	1.9280169	1.8727299	0.1860169	0.13072992
1.8092	1.6321	1.6240	1.9256481	1.8778192	0.1164481	0.0686192
1.8396	1.6329	1.6262	1.9280169	1.884817	0.0884189	0.04521898
1.8527	1.6359	1.6274	1.9368999	1.8886339	0.0841999	0.0359392
2.5587	1.8756	1.8519	2.6466516	2.6027285	0.0879516	0.04402352
2.5667	1.8751	1.8472	2.6451711	2.5877738	0.0784711	0.02107376
2.5768	1.8785	1.8536	2.6552885	2.6061808	0.0784885	0.03138088
2.5844	1.8764	1.8493	2.6490204	2.5944534	0.0646204	0.01005344
2.7988	1.9715	1.9318	2.9806115	2.8568994	0.1878115	0.08356944
2.8626	1.9846	1.9478	2.9694006	2.9077622	0.1068006	0.04516224
2.8841	1.9939	1.9529	2.996879	2.9239843	0.1128379	0.03988432
3.3314	2.1343	2.0831	3.4126623	3.381245	0.0812623	0.00672448
3.3360	2.1419	2.0852	3.4351859	3.3448042	0.0999859	0.00880416
3.3369	2.1490	2.0886	3.456189	3.3556189	0.119289	0.01871888
3.3411	2.1469	2.0886	3.4499709	3.3556189	0.1088709	0.01451888
3.3478	2.1440	2.0852	3.441384	3.3448042	0.099584	-0.0025958
3.3508	2.1465	2.0918	3.4487885	3.3651619	0.0878885	0.01436128
3.7837	2.3059	2.2382	3.9207699	3.8314666	0.1370899	0.04776856
3.8225	2.2805	2.2458	3.8455605	3.8556406	0.0230605	0.03314064
3.8310	2.2808	2.2458	3.8455605	3.8556406	0.0145605	0.02484064
3.8310	2.2805	2.2442	3.8455605	3.8505514	0.0145605	0.01955136
4.1404	2.3722	2.3333	4.1170842	4.1339606	-0.0233158	-0.0064394
4.1472	2.3786	2.3363	4.1360846	4.1453503	-0.0111784	-0.003697
4.6016	2.5413	2.4855	4.6177893	4.6180784	0.0161893	0.0164784
4.6181	2.5422	2.4888	4.6204542	4.612671	0.0023542	-0.005429
4.6223	2.5434	2.4859	4.6240074	4.6193507	0.0017074	-0.0029493
4.6270	2.5434	2.4881	4.6240074	4.6269485	-0.0029485	-0.0006515
4.9616	2.6508	2.6018	4.9420188	4.9880054	-0.0395812	0.00640544
4.9629	2.6673	2.6018	4.9908753	4.9880054	0.0079753	0.00510544
4.9884	2.6491	2.6030	4.9369851	4.9918224	-0.0514149	0.0034224
4.9888	2.6504	2.6030	4.9408344	4.9918224	-0.0479656	0.0030224
4.9888	2.6538	2.6018	4.9503018	4.9880054	0.0578962	-0.0007946
5.0484	2.6893	2.6195	5.0560173	5.0443056	0.00796173	-0.0040944
5.3942	2.7992	2.7332	5.3814312	5.4059826	-0.0127688	0.01176256
5.4022	2.7945	2.7320	5.3675145	5.4021456	-0.0346355	-0.44405
5.4098	2.7992	2.7345	5.3814312	5.4100876	-0.0286564	0.0000876
5.7831	2.9302	2.8541	5.7693222	5.7905213	-0.0137778	0.00742128
5.7987	2.9378	2.8579	5.7918258	5.8026083	-0.0068742	0.00390832
5.8004	2.9357	2.8579	5.7858077	5.8026083	-0.0147985	0.00220832
5.8025	2.9370	2.8609	5.789457	5.8121507	-0.013043	0.00365072
6.0485	3.0211	2.9349	6.0384771	6.0475299	-0.0100229	-0.0008701
6.1305	3.0431	2.9645	6.1036191	6.1416816	-0.0268809	0.0111816
6.1305	3.0456	2.9653	6.1110216	6.1442262	-0.0194784	0.01378224
6.1365	3.0465	2.9670	6.1136865	6.1496336	-0.0228135	0.0131336
6.1398	3.0473	2.9683	6.1160853	6.1537886	-0.0237447	0.01398664
6.1462	3.0509	2.9683	6.1248888	6.1537886	-0.0212617	0.00758164
6.1470	3.0494	2.9670	6.1222734	6.1496336	-0.0247266	0.0026336
6.1504	3.0494	2.9691	6.1222734	6.1563133	-0.0281266	0.00591328
6.1517	3.0515	2.9670	6.1284915	6.1496336	-0.0232085	-0.0020664
6.1580	3.0538	2.9718	6.1347098	6.1642653	-0.02332504	0.00626528
6.1635	3.0570	2.9733	6.144777	6.1696726	-0.018723	0.00617264
6.1643	3.0536	2.9689	6.1347098	6.1557886	-0.0295994	-0.0105314
6.1658	3.0604	2.9725	6.1548444	6.167128	-0.0107856	0.001528
6.5718	3.1952	3.1018	6.5539872	6.5784054	-0.0178128	0.00680544
6.5718	3.1919	3.0984	6.5442159	6.5675807	-0.0275841	-0.0042093
6.5773	3.1978	3.1023	6.5616858	6.5799598	-0.0156142	0.00269584
6.5778	3.1957	3.1027	6.5554677	6.5812682	-0.0218428	0.0039816
6.5921	3.1969	3.1031	6.5590209	6.5825405	-0.0330791	-0.0095395
7.0178	3.3610	3.2510	7.044821	7.0529808	0.0027121	0.0051808
7.0224	3.3483	3.2422	7.0073163	7.0249898	-0.0150837	0.00258976
7.0351	3.3529	3.2450	7.0209869	7.0275344	-0.0141631	-0.0075656
7.0364	3.3529	3.2481	7.0209869	7.0437585	-0.0154681	0.00735848
7.0410	3.3517	3.2608	7.0173837	7.0841526	-0.0236163	0.04315264
7.0487	3.3719	3.2468	7.0771959	7.0898214	0.0284959	-0.0090786
7.3386	3.4556	3.3449	7.3250816	7.3516579	-0.0135884	0.01306792
7.3496	3.4535	3.3446	7.3188135	7.3487952	-0.0307865	-0.0088048
7.3627	3.4632	3.3462	7.3475352	7.355793	-0.0151648	-0.006907
7.3636	3.4556	3.3428	7.3250816	7.3449782	-0.0385884	-0.0186218
7.3830	3.4641	3.3432	7.3508001	7.3462808	-0.0082798	-0.0087464
7.3856	3.4586	3.3432	7.3339146	7.3462506	-0.0516854	-0.0393464
7.4320	3.4869	3.3491	7.4177109	7.3650173	-0.0142861	-0.0669827
7.4456	3.4709	3.3554	7.3703349	7.3850563	-0.0752651	-0.0605437
7.7782	3.6118	3.4788	7.788476	7.791574	0.0137476	0.0036744
7.7766	3.6027	3.4911	7.7605947	7.8166909	-0.0160053	0.0400088
7.7968	3.6031	3.4772	7.798451	7.7724778	-0.0172348	-0.0243222
7.7998	3.6125	3.4780	7.7896125	7.7750224	-0.0101875	-0.0247776
7.8911	3.6463	3.4869	7.8896843	7.8033515	-0.0014057	-0.0877685
7.8924	3.6442	3.5106	7.8834762	7.8787165	-0.0089238	-0.0136835
7.8945	3.6442	3.4878	7.8834762	7.8061942	-0.0110238	-0.0883068

Appendix 18 Calibrated Thermocouple Probe Specification

CALIBRATION REPORT

CUSTOMER: CALIFORNIA POLYTECH STATE UNIVERSITY FOUNDATION
MECH ENGR DEPT
3801 W TEMPLE AVENUE
PIMONA CA 91768

REPORT NO: OM-70609592
TEST ITEM: KQSS-18G
TEST DATE: JUNE 9, 1987

PURCHASE ORDER NO: CPF66026ADD2

OMEGA ENGINEERING certifies that the above item has been calibrated and that its calibration is certified as traceable to the U.S. National Bureau of Standards. Traceability of these measurements is derived from the included NBS test numbers.

<u>Probe No.</u>	<u>Nominal Temperature</u>	<u>Actual Test Temperature</u>	<u>Indicated Temperature</u>	<u>Deviation</u>
1	300 DEG F	300.06	300.56	.50
1	500	499.77	499.39	.38
1	700	701.0	699.09	1.91

Reference: NATIONAL BUREAU OF STANDARDS TEST NO(s): 236495-37778

Tony D. Inverno
Supervisor, Instrumentation

CAL-4

OMEGA ENGINEERING, INC.

OMEGA PRESS

OMEGA INTERNATIONAL CORP.

BIOMEGA

One Omega Drive, Box 4047, Stamford, CT 06907-0047 (203) 359-1800 Telex 908404 Cable OMEGA FAX (203) 359-7700

CERTIFICATE OF CALIBRATION

HY-CAL Engineering
A Unit of Goodrich Supply
9650 Brookhurst Avenue • El Monte, CA 91734-3078

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Appendix 20: Pyromark® Paint Specifications

PYRO/INCOLOY;540C CURE; AS RECVD. EMITT

Appendix 20: Pyromark® Paint Specifications

PYROMARK/INCOLOY;540-1;540C CURE;AS RECD

Constants ϵ (hot plate) [in] = 3.5 radiometer response [S.C./mV] = 0.171 ϵ (radiometer) [in] = 0.5625 Stefan-Boltzmann [W/(m²·K⁴)] = 57.308-9 Point emittance poly. coeff.

Window	vertical ϵ (plate)	0.32	0.32	0.75	1.73	1.73	m0	m1	m2	m3	m4	m5
	Shape Factor	0.0234	0.0234	0.0163	0.0103	0.0089	1.033983	-6E-04	6.44E-07	-1.44E-11	-2.49E-13	1.07E-16
	T mean	amb	300°F	400°F	500°F	600°F						
	position	background	plate	background	plate	background	background	plate	background	background	plate	background
saran	T1 [°F]	74.1	74.2	74.3	298.1	299.2	301.3	372.3	394.3	396.8	406.3	408.3
	T2 [°F]	74	74	74.2	312	313.6	316	414.4	418.2	419.4	493.5	496.3
	T3 [°F]	73.8	73.9	74.1	305.1	307.2	309.3	404.3	408.6	409.9	482.2	483.7
	T4 [°F]	74.2	74.4	74.4	313.2	315.3	317	415.5	418.9	420.2	496.2	496.9
	T5 [°F]	74	74	74.1	313.6	315.8	317.9	417	421	422.5	497.1	499
	T6 [°F]	74	74	74.2	317.2	319.3	321.4	424.4	427.7	429	506.1	509.6
	T7 [°F]	73.8	73.9	73.8	316.4	318.3	320.6	423	427.1	428.5	506.5	508.2
	T8 [°F]	74.2	74.4	74.6	319.4	321.4	324	426.9	431	432.3	511.4	513.2
	T9 [°F]	75.1	75.2	75.3	313.4	315.1	317	417.2	420.5	422.2	498.3	500.8
	T amb [°F]	74.8	75.2	74.8	72.3	72.3	72.3	69	68.9	69.2	71.5	71.7
	T water [°F]	83.8	84.5	85.1	76.2	76.5	76	68.1	68.5	68.5	69.3	69.6
	T avg [°F]	74.22	74.3	74.4	316	317.98	320.18	421.7	425.46	426.9	504.28	506.16
	Radiometer [mV]	-0.1177	-0.181	-0.1349	0.0029	4.3487	-0.0029	0.0632	6.1284	0.0431	0.089	5.6806
	Radiometer [Watts]		-0.0081			0.6452			0.9014			0.8277
	HP emittance		0.9034			0.8779			0.8720			0.8693
quartz	Hot Plate [Watts]		-0.0011			0.7962			1.0465			0.9372
	window transmittance		7.3636			0.8103			0.8613			0.8647
	T1 [°F]	73.7	74	74.1	288.5	292.4	295.5	379.5	385.4	389.8	470.4	470.5
	T2 [°F]	73.6	74	74	302.9	306.8	309.3	403.1	408.3	411.8	499.8	499.2
	T3 [°F]	73.4	73.9	73.9	296	299.7	302.4	392	397.8	401.4	487.8	487
	T4 [°F]	73.8	74.1	74.3	303.9	307.8	311.1	403.2	408.6	412.7	501.5	500.7
	T5 [°F]	73.4	73.9	73.9	303.7	307.7	311.1	402.7	409.5	413.6	503.7	503.2
	T6 [°F]	73.6	73.9	74	308	312	315.2	412.2	417.4	421.3	513	512.9
	T7 [°F]	73.4	73.7	73.9	307.1	310.9	313.5	411	416.5	419.9	512.2	511.4
	T8 [°F]	73.8	74.2	74.3	310.4	313.9	316.8	415.1	420	424	517.4	516.7
	T9 [°F]	74.8	75.1	75.1	303.6	307.7	310.9	404.9	410.3	414.7	503.4	503.7
	T amb [°F]	76	75.7	75.7	72.7	72.5	72.5	68.3	68.5	68.8	72.1	72.3
	T water [°F]	81	82.1	83.1	77	76.8	76.4	67.3	67.8	67.9	69.2	69.5
	T avg [°F]	73.8	74.16	74.34	306.56	310.44	313.5	409.18	414.74	418.7	509.94	509.58
	Radiometer [mV]	-0.0459	-0.066	-0.0374	0	1.197	-0.0086	0.0144	1.8715	0.0144	0.0316	2.0897
	Radiometer [Watts]		-0.0021			0.1782			0.2735			0.3049
	HP emittance		0.9034			0.8784			0.8724			0.8692
	Hot Plate [Watts]		-0.0029			0.7572			0.9904			0.9716
	window transmittance		0.7241			0.2353			0.2782			0.3138

Appendix 21 Radiometer Window Test Data

glad	T1 [°F]	74.3	74.3	74.4	305.3	305.8	305.6	398	397.7	399.3	468.8	468.8	469.2	572.3	573.8	573.4	609.5	673.2	674
	T2 [°F]	74.2	74	74.1	317.4	319.5	321.2	421.2	421	421.3	497.6	498.9	500.3	611.2	610	612.6	712.9	715.7	716
	T3 [°F]	74	73.9	74	310.7	312.5	313.8	411.6	412.2	412.4	485.6	486.4	487.6	597	595	596	698.4	700.3	701.4
	T4 [°F]	74.6	74.6	74.6	318.8	321.4	322.5	421.5	422.7	424.1	498.5	499.5	501	613	614.5	615	723.1	726.5	727.4
	T5 [°F]	74.2	74	74.1	319.5	321.8	323.7	424	425	425.9	500.9	502.3	503.2	615.6	615.8	616.2	721.3	723.9	725.3
	T6 [°F]	74.2	74	74.1	323.1	325.6	327	430.3	430.9	432.1	511	512.6	513.1	632.7	634.1	634.4	731.7	734.4	735.3
	T7 [°F]	74	73.9	74	322.1	324	325.4	429.9	430.5	430.8	509.8	510.9	512.3	632	630.5	631.6	747	749.9	750.2
	T8 [°F]	74.6	74.6	74.6	325.3	327.2	329.1	434.2	434.9	435.3	514.3	516	517.2	638.6	637.1	638.5	755.8	758.3	759.3
	T9 [°F]	75.3	75.4	75.4	319.2	321.6	322.7	423.3	423.8	425.1	501.9	502.6	503.1	619	620.9	620	732.8	736	737
	T amb [°F]	74.6	74.7	74.4	72.1	71.9	71.7	69.5	69.6	69.7	72	72	72.1	73.2	73.3	73.2	69.6	69.6	69.7
	T water [°F]	86.2	88	77.5	76	76.2	75.8	68.7	70.1	70.4	68.5	68.8	69.1	69.6	69.9	69.9	73.1	73.2	73.2
	T avg [°F]	74.46	74.58	74.44	321.84	324.04	325.54	428.34	429.02	429.88	507.58	508.88	509.78	627.58	627.68	628.14	741.72	744.5	745.42
	Radiometer [mV]	-0.1607	-0.287	0	0.0086	4.5439	-0.0201	0.0402	6.2575	0.0258	0.1349	5.7581	0.0947	0.155	5.7724	0.1292	0	5.2156	0.0144
	Radiometer [Watts]		-0.0307			0.6751			0.9236			0.8373			0.8354			0.7728	
	HP emittance		0.9034			0.8775			0.8718			0.8692			0.8676			0.8684	
	Hot Plate [Watts]		-0.0003			0.8287			1.0630			0.9687			0.9435			0.8487	
	window transmittance		#####			0.8146			0.8672			0.8644			0.8854			0.9106	
no window	T1 [°F]	74.2	74.2	74.2	278.4	278.8	281.1	399.8	399.8	400.4	488.4	488.5	488.8	575.8	575.4	575.1	608.2	670.5	674.9
	T2 [°F]	74.2	74.2	74.2	287.9	292.3	294.7	422.7	422.5	423.3	482.4	488.6	492.6	612.9	613.8	612.6	709.4	708.7	709.1
	T3 [°F]	74	74.1	74	281.5	286.2	288.2	413.5	413.4	414.2	475.2	477.8	480.6	597.1	597.3	597.2	695.7	694.4	694.7
	T4 [°F]	74.6	74.6	74.6	289.1	293.1	295.2	423.9	424	424.2	479.4	488.2	493	614.4	615	615.9	720.3	720	721.2
	T5 [°F]	74.1	74.1	74.1	289.1	293.8	296.2	426.3	426.3	427.2	491.9	491.5	495	616.4	616.8	617.4	719.6	718.2	718.3
	T6 [°F]	74.1	74.1	74.1	292.5	296.8	299.2	432.1	432.6	433.2	493.7	501.1	505.2	634.3	634.9	635.2	748.3	747.1	748.6
	T7 [°F]	74	74.1	74	291.7	296.3	298.4	432	431.8	432.7	501.9	502.4	505.1	632.2	633.1	632.5	743.4	742.5	743.4
	T8 [°F]	74.6	74.7	74.7	295	299.2	301.7	436.3	436	437	502.7	506.6	510	638.8	639.2	639.1	751.9	751.2	752.2
	T9 [°F]	75.3	75.3	75.2	288.6	293.1	295.3	425.3	425.9	426	476.7	489.8	494.4	620.7	620.8	622	729.7	729.1	730.8
	T amb [°F]	74.5	73.9	73.8	72.8	72.6	72.5	70	69.9	70.1	71.8	71.7	71.8	73.5	73.4	73.4	69.1	69.2	69.4
	T water [°F]	75.3	76.2	76.9	77	77.1	77	70.4	70.4	70.4	68.4	68.9	69.1	70.1	70.4	70.4	72.9	73.5	73.1
	T avg [°F]	74.42	74.46	74.42	291.38	295.84	298.16	430.4	430.52	431.22	493.38	498.28	501.94	628.48	628.96	629.24	738.58	737.62	738.66
	Radiometer [mV]	-0.0373	-0.066	-0.0316	-0.0373	4.2569	-0.0345	0.0144	7.1101	0.0201	0.1177	6.1485	0.1062	0.1722	6.4384	0.178	-0.0431	5.6992	-0.0115
	Radiometer [Watts]		-0.0047			0.6369			1.0524			0.8957			0.9293			0.8482	
	HP emittance		0.9034			0.8795			0.8717			0.8695			0.8676			0.8683	
	Hot Plate [Watts]		0.0007			0.6857			1.0726			0.9234			0.9482			0.8287	
	window transmittance		-67143			0.9288			0.9812			0.9700			0.9801			1.0235	

Appendix 22: Saran Wrap® Specifications

Table 2 —
Properties of Various
SARAN WRAP Films

Property	Test Method	Remarks	Units	3	8	16	18	560
General								
Specific Gravity	ASTM D 1505 (4176)	Static — film to film		1.46	1.71	1.71	1.71	1.65
Coefficient of Friction	ASTM D 1694 (78)	Static — film to metal Kinetic — film to film Kinetic — film to metal		—	—	0.36	0.39	0.36
				—	—	0.33	0.33	0.24
				—	—	0.56	0.56	0.32
Barrier								
Water Absorption	ASTM D 570 (77)							
Water Vapor Transmission Rate	Perma-Trans W		g m ² /100 m ² (g m/m ²)					
Gas Transmission Rate	ASTM D 2655 (81) and ASTM D 1434 (75)		cc m ² /100 m ² (cc m/m ²)					
Optical								
Visible Light Transmission								
Ultraviolet Cut Off								
Infrared Light Transmission								
Resistance to Sunlight								
Clarity	ASTM D 1146 (70) (78)							
Gloss	ASTM D 2457 (77) (77)	45° Specular Gloss						
Haze	ASTM D 1600 (61) (77)							
Mechanical								
(Minute) Tensile Strength	ASTM D 882 (81)	Values determined on 100 gr film except 560 600 gr	lb/in ² (kg/cm ²)	7000 (3100)	—	8000 (3600)	—	14,500 (6500)
Elongation	ASTM D 882 (81)		%	30	—	50 for these types	—	—
Thermal								
Heat Seal Temperature								
Shrink								
Electrical								
Insulative Strength	ASTM D 1149 (81)							
Dielectric Properties	ASTM D 1125 (78)

NOTE: The values presented are a guideline
of the values and are not to be used for
specification purposes.
SARAN WRAP films are not mutually
compatible for use in contact with
certain foods.
SARAN WRAP films are not mutually
compatible for use in contact with
certain foods.

Appendix 22: Saran Wrap® Specifications

Light Transmission Characteristics

SARAN WRAP films offer good resistance to sunlight under glass. Such properties as tensile strength, elongation, flexibility, and impermeability to water vapor and gases decrease only slightly. Outdoor exposure to direct sunlight, however, is not recommended. Figure 2 below shows typical light transmission values for SARAN WRAP films.

FDA and USDA Status

SARAN WRAP films, when used unmodified and according to good manufacturing practices — when used for food contact applications — can comply with the U.S. Food, Drug and Cosmetic Act as amended.

Many of these films also have been accepted by the U.S. Department of Agriculture for packaging of meat and meat

food products, and poultry and poultry products, prepared in Federally inspected plants.

Government regulations are subject to change. While it is the responsibility of users of SARAN WRAP to check the suitability of their intended use with regulatory agencies, resources of The Dow Chemical Company are available to assist customers with pertinent data and other information.

Shrink Characteristics

SARAN WRAP plastic films become highly oriented during manufacture. This orientation makes the film susceptible to shrinkage on exposure to elevated temperatures — a property very desirable in applications such as overwraps. Further, by control of the shrink-inducing temperature, the film user can control the degree of shrinkage obtained.

For use in laminates where shrink is undesirable, preshrunk SARAN WRAP 18L film is available. Differences in the shrinkage rates of 18L and other films are shown in Figures 3 and 4.

Figure 2 — Light Transmission vs Wave Length for 100 Gauge SARAN WRAP 3, 8, 18, 18L, and 19 Films

$$Q = T T^4$$

$$T \leq K$$

$$\mu m = 1$$

$$A = 1 \mu m \times 10^{-3}$$

$$1 A = .0001 \mu m$$

$$U = 0.1712 E-8 \frac{RT^4}{(n_r)^2 R^4}$$

$$U = 5.6696 E-8 \frac{W}{m^2 \cdot K^4}$$

Appendix 23 Radiometer Displacement Sensitivity Test Data

[illegible]

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