Solubility of Anthracene in Binary Diisopropyl Ether + Alkane Solvent Mixtures at 298.15 K

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Experimental solubilities are reported for anthracene in six binary diisopropyl ether + alkane solvent mixtures at 298.15 K. The alkane solvents studied were hexane, heptane, octane, cyclohexane, methylcyclohexane, and 2,2,4-trimethylpentane. Results of these measurements were used to test a mathematical representation based on the combined nearly ideal binary solvent (NIBS)/Redlich–Kister equation. For the six systems studied, the combined NIBS/Redlich–Kister equation was found to accurately describe the experimental data, with an average absolute deviation between measured and back-calculated values being approximately $\pm 0.3\%$.

Introduction

Solid–liquid equilibrium data for crystalline polycyclic aromatic hydrocarbons dissolved in organic solvents are becoming increasingly important in the petroleum industry, particularly in light of present trends toward heavier feedstocks and the known (or suspected) carcinogenicity/mutagenicity of many larger polycyclic aromatic hydrocarbons. Over the past 20 years, we have reported experimental solubility data for anthracene and pyrene dissolved in numerous binary solvents and have developed a fairly simple predictive method for estimating the solubility of crystalline organic compounds in ternary^{1–4}

$$\ln x_A^{\text{sat}} = x_B^0 \ln(x_A^{\text{sat}})_B + x_C^0 \ln(x_A^{\text{sat}})_C + x_D^0 \ln(x_A^{\text{sat}})_D + x_B^0 x_C^0 \sum_{i=0}^r S_{BC,i} (x_B^0 - x_C^0)^i + x_B^0 x_D^0 \sum_{j=0}^s S_{BD,j} (x_B^0 - x_D^0)^j + x_C^0 x_D^0 \sum_{k=0}^t S_{CD,k} (x_C^0 - x_D^0)^k \quad (1)$$

and higher-order multicomponent solvent mixtures⁵

$$\ln x_A^{\text{sat}} = \sum_I x_I^0 \ln(x_A^{\text{sat}})_I + \sum_I \sum_{J>I} (x_I^0 x_J^0 \sum_{i=0}^r S_{IJ,i} (x_I^0 - x_J^0)^i) \quad (2)$$

based on the extended form Combined Nearly Ideal Binary Solvent (NIBS)/Redlich–Kister solution model. Predictions are based on the measured solubility data in all of the contributing sub-binary solvent mixtures. In eqs 1 and 2 x_i^0 values refer to the initial mole fraction solvent composition of component i calculated as if the solute were not present, and $(x_A^{\text{sat}})_I$ denotes the measured solute solubility in pure solvent i . The various $S_{IJ,i}$ parameters can be evaluated with a least-squares regression analysis.

In the present study, we extend our solubility measurements to binary solvent mixtures containing diisopropyl ether. Experimental solubilities are reported for anthracene dissolved in six binary mixtures containing diisopropyl ether with hexane, heptane, octane, cyclohexane, methylcyclohexane, and 2,2,4-trimethylpentane at 298.15 K. Results of these measurements

are used to calculate the $S_{IJ,i}$ curve-fit coefficients. To date, the solubility behavior of anthracene in binary solvent mixtures containing diisopropyl ether has not been studied.

Experimental Methods

Materials. Anthracene (Aldrich, 99+ %) was recrystallized several times from 2-propanone to yield a purified sample having a melting point temperature of $T/K = 489$. Diisopropyl ether (Aldrich, 99 %, anhydrous), hexane (Aldrich, 99 %), heptane (Aldrich, 99 %, anhydrous), octane (Aldrich, 99+ %, anhydrous), cyclohexane (Aldrich, HPLC grade, 99.9+ %), methylcyclohexane (Aldrich, 99+ %, anhydrous), and 2,2,4-trimethylpentane (Aldrich, HPLC Grade, 99.7 %) were stored over molecular sieves and distilled shortly before use. Gas chromatographic analysis showed the solvent mole fraction purities to be 99.7 % or better. Binary solvent mixtures were prepared by mass so that composition could be calculated to 0.0001 mole fraction.

Apparatus and Procedure. Excess solute and solvent were placed in amber glass bottles and allowed to equilibrate in a constant temperature water bath at $T/K = 298.15 \pm 0.05$ for at least 3 days (often longer) with periodic shaking in order to facilitate dissolution of the solid. Attainment of equilibrium was verified by repetitive measurements after a minimum of 3 additional days and by approaching equilibrium from supersaturation by pre-equilibrating the solutions at a slightly higher temperature. Aliquots of saturated anthracene solutions were transferred through a coarse filter into a tared volumetric flask to determine the amount of sample and then diluted quantitatively with methanol for spectrophotometric analysis at 356 nm on a Bausch and Lomb Spectronic 2000. Concentrations of the dilute solutions were determined from a Beer–Lambert law absorbance versus concentration working curve. Molar absorptivities of the nine standard solutions systematically with molar concentration and ranged from $\epsilon/(\text{L} \cdot \text{mol}^{-1} \cdot \text{cm}^{-1}) = 7450$ to $\epsilon/(\text{L} \cdot \text{mol}^{-1} \cdot \text{cm}^{-1}) = 7150$ for anthracene compositions ranging from $C/(\text{mol} \cdot \text{L}^{-1}) = 6.75 \times 10^{-5}$ to $C/(\text{mol} \cdot \text{L}^{-1}) = 2.25 \times 10^{-4}$. Identical molar absorptivities were obtained for select anthracene standard solutions that contained volume fractions up to 5 % of the neat diisopropyl ether and alkane cosolvents. Experimental molar concentrations were converted to mass fraction solubility by multiplying by the molar mass of

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Table 1. Experimental Mole Fraction Solubilities (x_A^{sat}) of Anthracene in Binary Diisopropyl Ether (B) + Alkane (C) Solvent Mixtures at 298.15 K

x_B^0	x_A^{sat}	x_B^0	x_A^{sat}
Diisopropyl Ether (B) + Hexane (C)			
0.0000	0.001274	0.5841	0.001980
0.1098	0.001463	0.7732	0.002238
0.2022	0.001570	0.8892	0.002419
0.3817	0.001756	1.0000	0.002515
0.4835	0.001877		
Diisopropyl Ether (B) + Heptane (C)			
0.0000	0.001576	0.6102	0.002180
0.1357	0.001711	0.7970	0.002337
0.2247	0.001799	0.8930	0.002430
0.4129	0.001981		
0.5041	0.002074		
Diisopropyl Ether (B) + Octane (C)			
0.0000	0.001838	0.6317	0.002383
0.1401	0.001991	0.8188	0.002504
0.2374	0.002064	0.8840	0.002533
0.4258	0.002202		
0.5378	0.002311		
Diisopropyl Ether (B) + Cyclohexane (C)			
0.0000	0.001553	0.4356	0.002213
0.1004	0.001768	0.5831	0.002313
0.1502	0.001867	0.7577	0.002435
0.3444	0.002145	0.8688	0.002480
0.4344	0.002202		
Diisopropyl Ether (B) + Methylcyclohexane (C)			
0.0000	0.001649	0.4754	0.002296
0.0990	0.001860	0.7635	0.002496
0.1945	0.002020	0.8924	0.002520
0.2898	0.002121		
0.3721	0.002182		
Diisopropyl Ether (B) + 2,2,4-Trimethylpentane (C)			
0.0000	0.001074	0.6343	0.001897
0.1349	0.001229	0.8184	0.002219
0.2408	0.001356	0.9086	0.002380
0.4530	0.001627		
0.5410	0.001752		

anthracene, volume(s) of the volumetric flask(s) used, and any dilutions required to place the measured absorbances on the Beer–Lambert law absorbance versus concentration working curve and then dividing by the mass of the saturated solution analyzed. Mole fraction solubilities were computed from mass fraction solubility using the binary solvent initial mole fraction compositions and molar masses of the solute and both cosolvents. Experimental anthracene solubilities in the six binary diisopropyl ether + alkane mixtures studied are listed in Table 1. Numerical values represent the average of between four and eight independent determinations, with the measured mole fraction solubilities being reproducible to within $\pm 1.5\%$. Calculated standard deviations ranged from $\sigma_{n-1} = 0.000020$ to $\sigma_{n-1} = 0.000035$ mole fraction.

Results and Discussion

For a binary solvent mixture, eq 2 takes the mathematical form of

$$\ln x_A^{\text{sat}} = x_B^0 \ln(x_A^{\text{sat}})_B + x_C^0 \ln(x_A^{\text{sat}})_C + x_B^0 x_C^0 \sum_{i=0}^r S_{BC,i} (x_B^0 - x_C^0)^i \quad (3)$$

The ability of eq 3 to represent mathematically the experimental solubility of anthracene in the six binary diisopropyl ether + alkane solvent mixtures is summarized in Table 2 in the form of the “curve-fit” parameters and the average absolute percent

Table 2. Mathematical Representation of Anthracene Solubilities in Several Binary Diisopropyl Ether (B) + Alkane (C) Solvent Mixtures Based on Equation 3

solvent (B) + solvent (C)	S_1^a	$100 \times \text{dev}^b$
diisopropyl ether + hexane	0.195 −0.177 0.490	0.3
diisopropyl ether + heptane	0.153 ^c	0.2
diisopropyl ether + octane	0.216 0.084 0.258	0.3
diisopropyl ether + cyclohexane	0.546 −0.303 0.205	0.3
diisopropyl ether + methylcyclohexane	0.494 −0.219 0.325	0.4
diisopropyl ether + 2,2,4-trimethylpentane	0.113 0.036 0.177	0.1

^a Curve-fit coefficients are ordered as S_0 , S_1 , and S_2 . ^b Deviation = $\sum |[(x_A^{\text{sat}})^{\text{calc}} - (x_A^{\text{sat}})^{\text{exp}}] / (x_A^{\text{sat}})^{\text{exp}}| / N$. ^c Only a single curve-fit coefficient was needed.

deviations in back-calculated solubilities. The parameters S were computed from a polynomial least-squares analysis of

$$[\ln x_A^{\text{sat}} - x_B^0 \ln(x_A^{\text{sat}})_B - x_C^0 \ln(x_A^{\text{sat}})_C] / (x_B^0 x_C^0) = S_0 + S_1(x_B^0 - x_C^0) + S_2(x_B^0 - x_C^0)^2 \quad (4)$$

using the commercial software TableCurve (Janel Scientific, Corte Madera, CA). Careful examination of the Table 2 reveals that eq 3 does provide an accurate mathematical representation for how the solubility of anthracene varies with solvent composition. The overall average absolute deviation between back-calculated and experimental values is $\pm 0.3\%$, which is less than the uncertainty associated with the measured mole fraction solubilities.

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