Activity Coefficients at Infinite Dilution of Organic Compounds in Four New Imidazolium-Based Ionic Liquids

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ABSTRACT: Activity coefficients of 42 to 54 organic compounds in the four ionic liquids (ILs) 1-hexyl-3-methylimidazolium tris(pentafluoroethyl)trifluorophosphate, 1-butyl-3-methylimidazolium bis(pentafluoroethylsulfonyle)imide, 1,3-didecyl-2-methylimidazolium bis(trifluoromethylsulfonyle)imide, and 1-ethyl-3-methylimidazolium methanesulfonate were measured using inverse gas chromatography from (312 to 353) K. The retention data were also converted to gas-to-IL and water-to-IL partition coefficients using the corresponding gas-to-water partition coefficients. Both sets of partition coefficients were analyzed using the modified Abraham solvation parameter model. The derived equations correlated the experimental gas-to-IL and water-to-IL partition coefficient data to within average standard deviations of 0.113 and 0.143 log units, respectively.

■ INTRODUCTION

New strategies are necessary for clean and efficient separation, purification, and enrichment processes in the biotechnology and (petro)chemical industries. For example, environmental restrictions regarding the quality of transportation fuels produced and the emissions from the refinery itself are currently foremost issues. Moreover, it has become clear that the burden imposed on present and future generations by fossil fuels is so heavy that the need to phase them out has become de facto. This imperative to reduce environmental pollution has ushered in a new generation of scientists focused on more eco-responsible methods. Among the new advances, ionic liquids (ILs) are being widely promoted as probable substitutes for traditional industrial solvents such as volatile organic compounds in a host of processes. Overall, as a class of solvent, ILs frequently combine the attractive features of excellent chemical stability, high thermal stability, and exceedingly low vapor pressure in a single solvent. ILs are commonly comprised of an asymmetric, bulky organic cation paired with a weakly coordinating anion that may be organic or inorganic in nature. The properties of the anion and functionality presented at the cationic or anionic site offer a means to alter the specific attributes of the solvent proper, giving rise to the notion of tuning, often in stepwise fashion, the key solvent features for the task at hand. Nowadays, it is widely accepted that ILs are among the most intriguing and diverse alternative media available not only for conventional solvent-driven chemical processes like synthesis and (bio)catalysis, but also next-generation electrolytes, lubricants, and modifiers of mobile and stationary phases within the separation sciences.^{1–3} Numerous works have shown that a large number of ILs exhibit selectivities and capacities better than the solvents typically employed to solve industrial separation problems.^{4–10} For instance, IL-assisted extractive distillation or liquid–liquid extraction forms a powerful approach in the separation of ethanol–water mixtures¹¹ and thiophene from aliphatic hydrocarbons.¹²

The thermodynamic properties of dialkylimidazolium-based ILs are relatively well-described in the literature.^{13–20} Nevertheless, there is a paucity of data concerning functional or task-specific ILs. Moreover, the sheer number of individual ILs (and classes thereof) that attract attention has grown considerably in the last couple of years.

Up to now, few experimental separation data exist for tris(pentafluoroethyl)trifluorophosphate ILs, despite the fact that ILs containing the tris(perfluoroalkyl)trifluorophosphate (FAP) anion show excellent hydrolytic, thermal, and electrochemical stability and provide numerous advantages in organic synthesis, electrosynthesis, gas sorption, and battery applications.^{21–26} One of the most peculiar properties exhibited by these ILs is their prominent hydrophobic nature.²⁷ Compared to other commonly used ILs for extractions, such as those containing the hexafluorophosphate ([PF₆][−]) or bis(trifluoromethylsulfonyle)imide ([Tf₂N][−]) anion, FAP-based ILs are substantially more hydrophobic and hydrolytically stable,²⁸ making them ideal candidates for the study of direct immersion extraction from aqueous matrixes.

This study is a continuation of our investigations into the thermodynamic properties of dialkylimidazolium and functionalized ILs.^{4–10,29} In previous work, we have shown that the introduction of polar chains into an IL strongly affects its behavior and interaction with organic compounds. For example, appending short polar chains to an imidazolium cation of an IL yields increased selectivity toward mixtures containing {alcohol + aliphatic} or {aromatic + aliphatic} solutes. This work is focused on the behavior of four new imidazolium-based ILs: 1-hexyl-3-methylimidazolium tris(pentafluoroethyl)trifluorophosphate, ([HmIm]⁺[FAP][−]), 1-butyl-3-methylimidazolium

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Figure 1. Chemical structures of the ILs investigated in this work.

bis(pentafluoroethylsulfonyl)imide, ([BMIm]⁺[BETI]⁻), 1,3-didecyl-2-methylimidazolium bis(trifluoromethylsulfonyl)imide, ([D₂MIm]⁺[Tf₂N]⁻), and 1-ethyl-3-methylimidazolium methanesulfonate ([EMIm]⁺[MeSO₃]⁻). The molecular structures of these ILs are given in Figure 1. In this work, gas–liquid chromatography was used to quantify intermolecular solute–IL interactions and to predict their potential in various extraction and extractive distillation processes.

Using linear solvation energy relationships (LSERs) and retention data, one can quantify various intermolecular solute–IL interactions. Along these lines, Acree and co-workers have reported mathematical correlations based on the general Abraham solvation parameter model for both the gas-to-solvent partition coefficient, K_L , and the water-to-solvent partition coefficient, P .^{30–32} Sprunger et al.^{33–35} later modified the Abraham solvation parameter model as

$$\log K_L = c_{\text{cation}} + c_{\text{anion}} + (e_{\text{cation}} + e_{\text{anion}}) \cdot E + (s_{\text{cation}} + s_{\text{anion}}) \cdot S + (a_{\text{cation}} + a_{\text{anion}}) \cdot A + (b_{\text{cation}} + b_{\text{anion}}) \cdot B + (l_{\text{cation}} + l_{\text{anion}}) \cdot L \quad (1)$$

$$\log P = c_{\text{cation}} + c_{\text{anion}} + (e_{\text{cation}} + e_{\text{anion}}) \cdot E + (s_{\text{cation}} + s_{\text{anion}}) \cdot S + (a_{\text{cation}} + a_{\text{anion}}) \cdot A + (b_{\text{cation}} + b_{\text{anion}}) \cdot B + (v_{\text{cation}} + v_{\text{anion}}) \cdot V \quad (2)$$

recasting each of the six solvent equation coefficients as a summation of their respective cation and anion contributions. It is important to note that, by splitting the system constants into ion-specific contributions, these authors make the assumption that each solute–ion interaction is unaffected by the chemical nature of the counterion present in the IL. We justify this choice in the following section.

The dependent variables in eqs 1 and 2 are solute descriptors as follows: E and S refer to the excess molar refraction in units of $(\text{cm}^3 \cdot \text{mol}^{-1})/10$ and a dipolarity/polarizability description of the solute, respectively, A and B are measures of the solute hydrogen-bond acidity and basicity, V is the McGowan volume in units of $(\text{cm}^3 \cdot \text{mol}^{-1})/100$, and L is the logarithm of the gas-to-hexadecane partition coefficient at 298 K. Sprunger et al. calculated equation coefficients for 8 cations and 4 anions using a database that contained 584 experimental $\log K_L$ and 571 experimental $\log P$ values. Importantly, no loss in predictive accuracy was observed by separating the equation coefficients into individual cation-specific and anion-specific values. Of course, the major advantage of splitting the equation coefficients into individual cation- and anion-specific contributions is that

one can begin to make predictions for far more ILs based on permutations comprising these specific ions.

EXPERIMENTAL PROCEDURES AND RESULTS

Materials and Reagents. 1-Ethyl-3-methylimidazolium methanesulfonate ([EMIm]⁺[MeSO₃]⁻, Alfa Aesar Chemicals, 0.99 mass fraction) was dried at 353 K for several days at reduced pressure to remove volatile impurities and trace water, yielding a water content below 0.02 mass fraction, as determined by Karl Fisher titration. High purity 1-hexyl-3-methylimidazolium tris(pentafluoroethyl)trifluorophosphate ([HMIm]⁺[FAP]⁻) from EMD was similarly dried before use. Ultrapure, spectroscopy-grade 1-butyl-3-methylimidazolium bis(pentafluoroethylsulfonyl)imide ([BMIm]⁺[BETI]⁻, >0.999 mass fraction) was synthesized and dried following established methods.^{36,37} 1,3-Didecyl-2-methylimidazolium bis(trifluoromethylsulfonyl)imide ([D₂MIm]⁺[Tf₂N]⁻) was prepared from 1,3-didecyl-2-methylimidazolium chloride ([D₂MIm]⁺Cl⁻, 0.96, Sigma) and lithium bis(trifluoromethylsulfonyl)imide (Li⁺[Tf₂N]⁻, 3M). In a typical preparation, [D₂MIm]⁺Cl⁻ was combined with 1.05 equivalents of Li⁺[Tf₂N]⁻ in a 1:1 (v/v) dichloromethane–water system to produce an initially milky-white upper phase and a hazy bottom layer. After vigorous shaking overnight, the biphasic system was allowed to reestablish. The now-clear aqueous phase was discarded, and the organic phase washed several additional times with doubly distilled deionized water, using a separatory funnel, until the washes tested negative for the presence of halide using concentrated silver nitrate reagent. After two additional washes with warm deionized water, the organic phase was dried using a rotary evaporator, followed by gentle further drying on a Schenk line overnight at 333 K to give [D₂MIm]⁺[Tf₂N]⁻ in ~95 % isolated yield.

In addition to the treatment mentioned above, each IL was further purified by subjecting the liquid to a very low pressure of about 5 Pa at 343 K for approximately 24 h. Next, packed columns were conditioned for a 12 h duration. Based upon our experience, we can safely assume that this procedure adequately removes any volatile chemicals and moisture from the IL and Chromosorb. Beyond this soft thermal treatment, no other attempts were made to analyze or specifically identify the impurities remaining within the ILs. Test solutes were purchased from Aldrich at a purity ≥ 99.5 % and were used without further purification because our gas–liquid chromatography technique efficiently separates any impurities on the column.

Apparatus and Experimental Procedure. Inverse chromatography experiments were carried out using a Varian CP-3800 gas chromatograph equipped with a heated on-column injector and a flame ionization detector. The injector and detector temperatures were kept at 523 K during all experiments. The helium flow rate was adjusted to obtain adequate retention times. Methane was used to determine the column hold-up time. Exit gas flow rates were measured with a soap bubble flow meter. The temperature of the oven was determined with a Pt100 probe and controlled to within ± 0.1 K. A personal computer directly recorded detector signals, and the corresponding chromatograms were generated using Galaxie software.

Using a rotary evaporation preparatory technique, 1.0 m length columns were packed with a stationary phase consisting of 0.20 to 0.35 mass fraction of IL on Chromosorb WHP (60–80 mesh). After the evaporation of chloroform in vacuo, the support was equilibrated at 333 K during 6 h. Before conducting

measurements, each packed column was conditioned for 12 h at 363 K with a flow rate of $20 \text{ cm}^3 \cdot \text{min}^{-1}$. The packing level was calculated from the masses of the packed and empty columns and was checked throughout experiments. The masses of the stationary phase were determined to a precision of $\pm 0.0003 \text{ g}$. A (1 to 5) μL volume of the headspace sample vapor was injected to satisfy infinite dilution conditions, and each experiment was repeated at least twice to confirm reproducibility. Retention times were generally rigorously reproducible to within (0.01 to 0.03) min. To verify stability under these experimental conditions, ruling out elution of the stationary phase by the helium stream, measurements of retention time were repeated systematically each day for three selected typical solutes. No changes in the retention times were observed during this study.

Theoretical Basis. The retention data garnered by inverse chromatography experiments were used to calculate partition coefficients of the numerous solutes in the different ILs. The net retention volume, V_N , was calculated via the typical relationship as follows:³⁸

$$V_N = \frac{3}{2} \cdot \frac{\left[\left(\frac{P_i}{P_o} \right)^2 - 1 \right]}{\left[\left(\frac{P_i}{P_o} \right)^3 - 1 \right]} \cdot U_0 \cdot t'_R \cdot \frac{T_{\text{col}}}{T_r} \cdot \left(1 - \frac{P_{\text{ow}}}{P_o} \right) \quad (3)$$

The adjusted retention time, t'_R , was taken as the difference between the retention time of a particular solute and that of methane, T_{col} is the column temperature, U_0 is the flow rate of the carrier gas measured at room temperature (T_r), P_{ow} is the vapor pressure of water at T_r , and P_i and P_o are the inlet and outlet pressures, respectively.

Activity coefficients at infinite dilution for solute 1 in IL 2, $\gamma_{1,2}^\infty$, were calculated with the following expression:³⁸

$$\ln \gamma_{1,2}^\infty = \ln \left(\frac{n_2 RT}{V_N \cdot P_1^0} \right) - P_1^0 \cdot \frac{B_{11} - V_1^0}{RT} + \frac{2B_{13} - V_1^\infty}{RT} \cdot J \cdot P_0 \quad (4)$$

where n_2 is the number of moles of stationary phase component within the column, R is the gas constant, T is the oven temperature, B_{11} is the second virial coefficient of the solute in the gaseous state at temperature T , B_{13} is the mutual virial coefficient between solute 1 and the carrier gas (helium, denoted by "3"), and P_1^0 is the probe vapor pressure at temperature T . All thermodynamic properties of the pure solutes needed for these calculations were given in previous work.⁴

Gas-to-IL partition coefficients, K_L , used in the LSER approach were calculated using the expression

$$K_L = \frac{RT}{\gamma_{1,2}^\infty P_1^0 V_{\text{solvent}}} \quad (5)$$

The corresponding water-to-IL partition coefficients, P , were calculated through eq 6

$$\log P = \log K_L - \log K_w \quad (6)$$

which requires knowledge of the solute's gas-phase partition coefficient into water, K_w , which is available for most of the solutes studied here. Water-to-IL partition coefficients calculated through eq 6 pertain to a hypothetical partitioning process involving solute transfer from water to the anhydrous IL. For

convenience, we have collected these partition coefficients in the last two columns of Tables 1 to 4.

RESULTS AND DISCUSSION

Activity Coefficients at Infinite Dilution of Organic Compounds in Ionic Liquids. The errors in the experimental determination of activity coefficient are evaluated to be about 3 %. For all ILs studied in this work, no interfacial adsorption was observed while the average relative standard deviation between data sets obtained from different packed columns was about (3 to 4) %. Experimental activity coefficients at infinite dilution calculated using eqs 3 to 5 are listed in Tables 1 to 4. The ILs studied show similar behaviors to typical dialkylimidazolium ILs. Activity coefficients at infinite dilution for most organic compounds decrease with an increase in temperature. Of the series of organic compounds studied, alkanes exhibit the lowest solubility in these four ILs. The solubility of apolar compounds increases with the increase of the alkyl chain length grafted onto the imidazolium cation. For compounds containing the same number of carbon atoms but originating from different solute families, it was observed that $\gamma_{\text{alcohol}} < \gamma_{\text{aromatic}} < \gamma_{\text{alkyne}} < \gamma_{\text{alkene}} < \gamma_{\text{alkane}}$. This overall trend is followed for all ILs, regardless of the cation or anion identity. It is noteworthy that the presence of multiple bonds within the solute increases solubility considerably.

In general, the infinite dilution activity coefficients of the alcohols are relatively small, with the solubility of alcohols and chloroalkanes being higher in $[\text{EMIm}]^+[\text{MeSO}_3]^-$ than in the other ILs studied. The hydroxyl group can potentially interact with either the anion and/or the cation of the IL. Interestingly, these classes of compound follow similar trends as the hydrocarbons. Branched-chain alcohols have a lower solubility compared to linear alcohols, and their activity coefficients increase with increasing chain length. Notably, ketones and aldehydes strongly interact with ILs and thus show even higher solubilities.

In Table 5, activity coefficients measured at infinite dilution for selected organic solutes in $[\text{EMIm}]^+[\text{MeSO}_3]^-$ from this work are compared with recent data published by Blahut et al.³⁹ Reasonably good agreement is observed with a standard deviation of about 6 % for polar compounds, although the deviation is closer to 30 % for *n*-alkanes.

Selectivities and capacities at infinite dilution calculated from activity coefficients respectively, S_{12}^∞ and k_1^∞ , are reported in Table 6 for illustrative separation problems at 323.15 K: hexane/benzene, hexane/methanol, hexane/thiophene, and cyclohexane/thiophene:

$$S_{12}^\infty = \frac{\gamma_{1/\text{RTIL}}^\infty}{\gamma_{2/\text{RTIL}}^\infty} \quad (7)$$

$$k_1^\infty = \frac{1}{\gamma_{1/\text{RTIL}}^\infty} \quad (8)$$

Concerning the separation of benzene from hexane, the selectivities obtained using $[\text{HmIm}]^+[\text{FAP}]^-$ and $[\text{EMIm}]^+[\text{MeSO}_3]^-$ are of the same order of magnitude as for classical solvents used in industry like sulfolane (30.5), dimethylsulfoxide (22.7), and *N*-methyl-2-pyrrolidinone (12.5). Nevertheless, the capacity of $[\text{EMIm}]^+[\text{MeSO}_3]^-$ is lower than those observed with other ILs. A better capacity may be obtained by a moderate lengthening in the alkyl chain grafted to the

Table 1. Infinite Dilution Activity Coefficients and Logarithm of Partition Coefficients, $\log K_L$ and $\log P$, of Organic Compounds in $[\text{HmIm}]^+[\text{FAP}]^-$

solute	γ^∞			$\log K_L$	$\log P$
	312.80 K	332.85 K	354.65 K		
hexane	6.393	5.693	4.409	1.601	3.421
3-methylpentane	5.629	5.055	4.430	1.591	3.431
heptane	8.844	7.733	6.624	2.000	3.960
2,2,4-trimethylpentane	7.982	7.130	6.180	2.019	4.139
octane	12.207	10.534	8.867	2.365	4.475
nonane	17.681	15.467	12.441	2.747	4.897
decane	22.707	19.044	15.263	3.090	5.410
undecane	30.977	25.474	19.895	3.455	5.835
dodecane	39.253	33.077	25.673	3.826	6.356
methylcyclopentane	4.580	4.086	3.522	1.816	2.986
cyclohexane	4.782	4.166	3.615	1.942	2.842
methylcyclohexane	5.886	5.231	4.494	2.176	3.386
cycloheptane	9.005	13.241	28.671	2.482	3.072
benzene	0.517	0.552	0.564	2.984	2.354
toluene	0.674	0.727	0.753	3.386	2.736
ethylbenzene	0.956	1.032	1.043	3.687	3.107
<i>m</i> -xylene	0.939	0.997	1.010	3.773	3.163
<i>p</i> -xylene	0.992	1.034	1.000	3.719	3.129
<i>o</i> -xylene	0.888	0.947	0.957	3.891	3.151
1-hexene	3.668	3.422	3.142	1.801	2.961
1-hexyne	1.938	1.886	1.755	2.254	2.464
1-heptyne	2.545	2.501	2.318	2.625	3.065
2-butanone	0.204	0.195	0.171	3.402	0.682
2-pentanone	0.271	0.298	0.311	3.713	1.133
3-pentanone	0.236	0.280	0.301	3.739	1.239
1,4-dioxane	0.273	0.327	0.339	3.708	−0.002
methanol	1.571	2.006	1.581	2.333	−1.407
ethanol	2.095	1.688	1.312	2.482	−1.188
1-propanol	2.467	1.958	1.466	2.842	−0.718
2-propanol	2.061	1.622	1.259	2.614	−0.866
2-methyl-1-propanol	2.772	2.134	1.621	3.050	−0.250
1-butanol	4.903	2.324	1.756	2.984	−0.476
trifluoroethanol	0.987	0.891	0.728	2.755	−0.405
diethyl ether	0.837	0.866	0.897	2.029	0.739
diisopropyl ether	1.591	1.696	1.719	2.298	1.248
chloroform	1.092	1.090	1.054	2.324	1.534
dichloromethane	0.660	0.699	0.707	2.068	1.108
tetrachloromethane	2.191	2.078	1.939	2.243	2.430
acetonitrile	0.295	0.295	0.292	3.246	0.396
nitromethane	0.452	0.438	0.410	3.433	0.483
1-nitropropane	0.452	0.451	0.436	3.992	1.542
triethylamine	2.093	1.955	1.758	2.490	0.130
pyridine	0.302	0.326	0.331	3.873	0.433
thiophene	0.577	0.602	0.604	3.005	1.965
formaldehyde	0.096	0.134	0.146		
propionaldehyde	0.274	0.283	0.285	2.749	0.229

imidazolium cation. Indeed, longer alkyl chains are observed to increase the capacity, but with detriment to selectivity, as seen with $[\text{D}_2\text{MIm}]^+[\text{Tf}_2\text{N}]^-$. $[\text{EMIm}]^+[\text{MeSO}_3]^-$ behaves

Table 2. Infinite Dilution Activity Coefficients and Logarithm of Partition Coefficients, $\log K_L$ and $\log P$, of Organic Compounds in $[\text{BMIm}]^+[\text{BETI}]^-$

solute	γ^∞			$\log K_L$	$\log P$
	322.55 K	342.75 K	362.65 K		
hexane	9.490	8.798	8.430	1.341	3.161
3-methylpentane	8.232	7.793	7.616	1.320	3.160
heptane	13.633	12.370	11.625	1.686	3.646
2,2,4-trimethylpentane	13.282	11.712	10.496	1.641	3.761
octane	20.374	17.316	15.542	1.984	4.094
nonane	31.509	25.997	21.805	2.317	4.467
decane	37.382	33.298	27.989	2.715	5.035
undecane	57.328	45.877	37.821	2.999	5.379
dodecane	77.801	62.004	50.931	3.338	5.868
tridecane	111.158	78.063	68.856	3.688	
tetradecane	153.275	112.679	91.528	4.011	
methylcyclopentane	6.847	6.055	5.792	1.513	2.683
cyclohexane	7.002	6.121	5.405	1.614	2.514
methylcyclohexane	9.090	7.960	7.065	1.827	3.077
cycloheptane	19.825	35.188	56.459	2.114	2.694
benzene	1.012	1.016	1.029	2.556	1.926
toluene	1.397	1.417	1.456	2.931	2.281
ethylbenzene	2.043	2.052	2.062	3.221	2.641
<i>m</i> -xylene	2.024	2.026	2.090	3.302	2.692
<i>p</i> -xylene	2.049	2.034	2.002	3.277	2.687
<i>o</i> -xylene	1.873	1.890	1.965	3.434	2.774
1-hexene	6.065	5.546	5.242	1.437	2.597
1-hexyne	2.859	2.729	2.639	1.958	2.168
1-heptyne	3.914	3.761	3.576	2.306	2.746
2-butanone	0.453	0.389	0.351	2.905	0.185
2-pentanone	0.666	0.686	0.701	3.193	0.613
3-pentanone	0.624	0.656	0.695	3.182	0.682
1,4-dioxane	0.429	0.607	0.576	3.427	−0.283
methanol	1.234	0.997	0.942	2.263	−1.477
ethanol	1.647	1.367	1.179	2.437	−1.233
1-propanol	1.991	1.622	1.349	2.786	−0.774
2-propanol	1.766	1.456	1.249	2.526	−0.954
2-methyl-1-propanol	2.264	1.838	1.574	2.978	−0.322
1-butanol	2.493	1.997	1.704	3.167	−0.293
trifluoroethanol	0.457	0.412	0.373	2.962	−0.198
diethyl ether	1.715	1.704	1.653	1.564	0.394
diisopropyl ether	3.462	3.458	3.427	1.817	1.817
chloroform	0.613	0.740	0.790	2.530	1.740
dichloromethane	0.356	0.436	0.539	2.308	1.348
tetrachloromethane	2.403	2.349	2.330	2.087	2.277
acetonitrile	0.528	0.514	0.504	2.855	0.005
nitromethane	0.625	0.682	0.699	3.216	0.266
1-nitropropane	0.769	0.821	0.756	3.620	1.170
triethylamine	2.735	3.614	3.268	2.322	−0.038
pyridine	0.386	0.429	0.450	3.668	0.228
thiophene	0.977	0.973	0.981	2.642	1.552
formaldehyde	0.134	0.155	0.164	1.893	−0.127
propionaldehyde	0.539	0.533	0.522	2.315	−0.205
butyraldehyde	0.681	0.726	0.611	2.629	0.299
ethene				0.002	0.942
propene				0.402	1.372
1-butene				0.673	1.683
1,3-butadiene				0.939	1.389
carbon dioxide				0.259	0.339

Table 3. Infinite Dilution Activity Coefficients and Logarithm of Partition Coefficients, $\log K_L$ and $\log P$, of Organic Compounds in $[\text{D}_2\text{MIm}]^+[\text{TF}_2\text{N}]^-$

solute	γ^∞			$\log K_L$	$\log P$
	323.10 K	333.15 K	343.15 K		
hexane	1.825	1.792	1.756	2.074	3.894
3-methylpentane	1.708	1.675	1.633	2.006	3.846
heptane	2.531	2.111	2.077	2.261	4.221
octane	2.538	2.484	2.448	2.947	5.057
nonane	3.306	3.172	3.448	3.357	5.507
decane	3.562	3.461	3.328	3.793	6.113
methylcyclopentane	1.354	1.326	1.301	2.243	3.413
cyclohexane	1.318	1.285	1.256	2.396	3.296
methylcyclohexane	1.517	1.484	1.454	2.660	3.870
cycloheptane	3.167	4.458	6.093	2.980	3.570
benzene	0.429	0.431	0.434	2.930	2.300
toluene	0.512	0.520	0.527	3.373	2.723
ethylbenzene	0.652	0.662	0.689	3.723	3.143
<i>m</i> -xylene	0.645	0.653	0.663	3.805	3.195
<i>p</i> -xylene	0.647	0.660	0.657	3.794	3.204
<i>o</i> -xylene	0.626	0.616	0.603	3.878	3.218
1-hexene	1.393	1.376	1.364	2.111	3.271
1-hexyne	0.925	0.917	0.899	2.456	2.666
1-heptyne	1.065	1.060	1.061	2.887	3.327
2-butanone	0.318	0.292	0.264	3.035	0.315
2-pentanone	0.397	0.404	0.407	3.409	0.829
3-pentanone	0.37	0.378	0.386	3.397	0.897
1,4-dioxane	0.463	0.460	0.453	3.309	−0.401
methanol	0.963	0.857	0.755	2.312	−1.428
ethanol	1.271	1.150	1.041	2.536	−1.134
1-propanol	1.307	1.160	1.061	2.94	−0.620
2-propanol	1.267	1.140	1.035	2.657	−0.823
2-methyl-1-propanol	1.300	1.171	1.062	3.215	−0.085
1-butanol	1.376	1.202	1.117	3.392	−0.068
trifluoroethanol	0.399	0.379	0.355	3.013	−0.147
diethyl ether	0.746	0.771	0.773	1.978	0.578
diisopropyl ether	1.122	1.232	1.233	2.416	1.386
chloroform	0.374	0.395	0.402	2.731	1.941
dichloromethane	0.330	0.341	0.351	2.275	1.315
tetrachloromethane	0.776	0.777	0.777	2.589	2.779
acetonitrile	0.470	0.453	0.440	2.875	0.025
nitromethane	0.596	0.559	0.536	3.125	0.175
1-nitropropane	0.504	0.487	0.479	3.777	1.327
triethylamine	3.672	3.174	2.863	2.013	−0.347
pyridine	0.328	0.331	0.334	3.699	0.259
thiophene	0.422	0.423	0.424	3.007	1.977
formaldehyde	0.074	0.080	0.085	2.180	0.160

similarly to 1-ethyl-3-methylimidazolium dicyanamide and appears to be a good choice for separating hexane/methanol, hexane/thiophene, and cyclohexane/thiophene mixtures. Results for the three other ILs studied suggest they will not attract particular interest for these specific separation problems.

Linear Solvation Energy Relationship (LSER) Characterization. In Table 1, there are 45 experimental $\log K_L$ and $\log P$ values

Table 4. Infinite Dilution Activity Coefficients and Logarithm of Partition Coefficients, $\log K_L$ and $\log P$, of Organic Compounds in $[\text{EMIm}]^+[\text{MeSO}_3]^-$

solute	γ^∞			$\log K_L$	$\log P$
	312.55 K	322.45 K	332.45 K		
hexane	206.773	189.568	152.483	0.304	2.124
3-methylpentane	156.837	135.415	115.201	0.333	2.173
heptane	432.487	2232.657	496.685	0.666	2.626
2,2,4-trimethylpentane	445.177	386.576	333.734	0.472	2.592
octane	588.387	556.416	184.450	0.963	3.073
nonane	1047.037	925.051	483.466	1.024	3.174
decane	1408.052	1303.804	1158.638	1.558	3.818
undecane	2011.800	1893.008	1717.795	1.926	4.306
dodecane	2552.251	2422.466	2292.163	2.315	4.845
tridecane	3376.144	3276.796	3068.670	2.712	
tetradecane	4065.351	4003.456	3828.889	3.128	
methylcyclopentane	102.064	95.800	79.455	0.673	1.843
cyclohexane	96.795	88.264	76.345	0.853	1.753
methylcyclohexane	169.213	131.109	130.385	0.946	2.196
cycloheptane	194.190	250.689	322.731	1.335	1.915
benzene	4.306	4.271	4.235	2.297	1.667
toluene	13.109	8.735	8.569	2.187	1.537
ethylbenzene	23.694	16.842	16.470	2.427	1.847
<i>m</i> -xylene	19.280	18.753	18.224	2.688	2.078
<i>p</i> -xylene	18.073	17.795	17.311	2.694	2.104
<i>o</i> -xylene	14.725	14.514	14.256	2.907	2.247
1-hexene	86.953	83.446	68.874	0.628	1.788
1-hexyne	10.621	10.699	10.664	1.785	1.995
1-heptyne	19.195	19.396	19.386	2.020	2.460
2-butanone	3.930	3.686	3.348	2.336	−0.384
2-pentanone	7.789	7.704	7.571	2.470	−0.110
3-pentanone	7.576	7.451	7.371	2.439	−0.061
1,4-dioxane	2.675	2.666	2.660	2.936	−0.774
methanol	0.249	0.254	0.264	3.439	−0.301
ethanol	0.438	0.418	0.405	3.476	−0.194
1-propanol	0.742	0.734	0.722	3.704	0.144
2-propanol	0.924	0.907	0.877	3.290	−0.190
diethyl ether	21.818	20.373	18.006	0.779	−0.391
diisopropyl ether	84.519	74.151	67.694	0.739	−0.291
chloroform	0.563	0.479	1.418	2.762	1.972
dichloromethane	0.471	0.531	1.299	2.530	1.570
tetrachloromethane	4.572	4.793	0.669	2.243	2.433
acetonitrile	1.263	0.818	0.836	2.709	−0.141
nitromethane	2.057	1.261	0.801	2.716	−0.234
1-nitropropane	4.190	2.702	1.726	2.978	0.528
triethylamine	8.322	14.329	18.845	2.441	0.081
thiophene	1.871	1.905	1.951	2.755	1.665
formaldehyde	0.615	0.656	0.691	-	-
propionaldehyde	2.756	2.714	2.652	1.974	−0.546
butyraldehyde	4.869	4.947	3.509	2.056	−0.274

for solutes dissolved in $[\text{HMIIm}]^+[\text{FAP}]^-$ at 298 K. Preliminary regression analyses on the entire data set indicated that dichloromethane was a statistical outlier. The compound was removed, and analysis of the remaining 44 tabulated experimental data

points gave:

$$\log K_L = -0.324(0.111) - 0.242(0.121)E + 2.312(0.111)S \\ + 1.162(0.167)A + 0.672(0.118)B + 0.729(0.030)L \\ (N = 44, SD = 0.124, R^2 = 0.969, F = 237.2) \quad (9)$$

$$\log P = -0.058(0.164) - 0.138(0.149)E + 0.616(0.150)S \\ - 2.420(0.208)A - 4.287(0.146)B + 3.554(0.130)V \\ (N = 44, SD = 0.156, R^2 = 0.994, F = 1174.5) \quad (10)$$

Table 5. Activity Coefficients at Infinite Dilution of Various Organic Compounds in [EMIm]⁺[MeSO₃][−] at 323.15 K

solute	Blahut et al. ³⁹	this work
	<i>T</i> = 323.15 K	<i>T</i> = 322.45 K
methylcyclohexane	198	131
<i>m</i> -xylene	20.5	18.75
benzene	4.5	4.271
methanol	0.239	0.254
chloroform	0.515	0.479
acetonitrile	0.873	0.818
thiophene	2.06	1.905

where *N* denotes the number of experimental values used in the regression analysis, SD refers to the standard deviation, *R*² is the squared correlation coefficient, and *F* is the Fisher *F*-statistic. All regression analyses were performed using SPSS statistical software. The standard errors in the calculated coefficients are given parenthetically immediately following the respective coefficient. Solute descriptors used in the analysis are tabulated in Table 7. Equations 9 and 10 prove to be a very accurate mathematical description of the log *K*_L and log *P* values for the studied solutes dissolved in [HMIIm]⁺[FAP][−] and can be used to estimate log *K*_L and log *P* values for additional solutes in this IL.

As noted above, each of the calculated equation coefficients corresponds to the sum of the respective cation- and anion-specific contributions. We have reported³⁵ log *K*_L equation coefficients of *c*_{cation} = −0.395, *e*_{cation} = −0.062, *s*_{cation} = 1.975, *a*_{cation} = 2.234, *b*_{cation} = 0.621, and *l*_{cation} = 0.768 for the [HMIIm]⁺ cation. Equation coefficients of *c*_{anion} = 0.071, *e*_{anion} = −0.180, *s*_{anion} = 0.337, *a*_{anion} = −1.072, *b*_{anion} = 0.051, and *l*_{anion} = −0.039 are calculated for the [FAP][−] anion by subtracting the [HMIIm]⁺ equation coefficients from those in eq 9. Anion-specific equation coefficients of *c*_{anion} = −0.005, *e*_{anion} = −0.249, *s*_{anion} = 0.383, *a*_{anion} = −1.062, *b*_{anion} = 0.084, and *v*_{anion} = −0.051 for [FAP][−] for the log *P* correlation were calculated in a similar fashion. The calculated anion-specific equation

Table 6. Selectivities *S*₁₂[∞] and Capacities *k*₁[∞] at Infinite Dilution for Different Separation Problems at 323.15 K

ILs		<i>S</i> ₁₂ [∞] / <i>k</i> ₁ [∞]			
anion	cation	hexane/ benzene	hexane/ methanol	hexane/ thiophene	cyclohexane/ thiophene
[Tf ₂ N]	1-hexyl-3-methylimidazolium	12.38/1.93	4.89/0.81	6.16/1.02	7.14/1.02
	tris(pentafluoroethyl)trifluorophosphate, [HMIIm] ⁺ [FAP] [−]				
	1-butyl-3-methylimidazolium	9.37/0.99	5.69/0.81	9.68/1.02	7.14/1.02
	bis(pentafluoroethylsulfonyl)imide, [BMIm] ⁺ [BETI] [−]				
	1,3-didecyl-2-methylimidazolium	4.23/2.32	1.89/4	4.33/2.38	3.14/2.38
	bis(trifluoromethylsulfonyl)imide, [D ₂ MIm] ⁺ [Tf ₂ N] [−]				
	1-ethyl-3-methylimidazolium	48.1/0.23	826/4	110/0.53	51.9/0.53
	methanesulfonate, [EMIm] ⁺ [MeSO ₃] [−]				
	1,3-dimethoxyimidazolium	21.3/0.47	42.05/0.94	24.8/0.94	12.6/0.94
	1-(methylethylether)-3-methylimidazolium	15.5/0.85	17.4/0.93	18.1/1.0	10.9
	1-ethanol-3-methylimidazolium	20.6/0.47	49.1/1.12	24.7/0.56	14.2/0.56
	1-ethyl-3-methylimidazolium	37.5/1.43	19.5/1.20	-	-
	1-(hexylmethylether)-3-methylimidazolium	9.1/1.23	6.8/0.91	10.0/1.35	6.4/1.35
	1,3-bis(hexylmethylether)imidazolium	4.9/1.67	3.2/1.06	5.3/1.75	3.7/1.75
	1-butyl-3-methylimidazolium	16.7/1.11	-	-	-
[DCA]	1-hexyl-3-methylimidazolium	9.5/1.29	6.1/0.82	-	-
	trimethylhexylammonium	9.9/1.01	8.5/0.86	10.7/1.09	7.2/1.09
	4-methyl- <i>N</i> -butyl-pyridinium	18.8/1.43	21.2/0.83	10.6/1.56	6.1/1.56
	triethylsulphonium	21.6/0.91	17.8/0.77	25.5/1.05	14.3/1.05
	triethyl(tetradecyl) phosphonium	2.7/2.56	1.1/1.02	2.6/2.5	1.95/2.5
[BF ₄]	1-cyanopropyl-3-methylimidazolium	56.0/0.22	432/1.69	105/0.41	41.3/0.41
	1-ethyl-3-methylimidazolium	43.4/0.39	255/2.27	69.6/0.63	28.8/0.63
[PF ₆]	1-ethanol-3-methylimidazolium	-/0.10	-/0.98	-/0.17	136.1/0.17
	1-ethanol-3-methylimidazolium	-/0.17	-/0.77	-/0.23	59.7/0.23

Table 7. Solute Descriptors of Compounds Used in the Study

solute	E	S	A	B	L	V
hexane	0.000	0.000	0.000	0.000	2.668	0.9540
3-methylpentane	0.000	0.000	0.000	0.000	2.581	0.9540
heptane	0.000	0.000	0.000	0.000	3.173	1.0949
2,2,4-trimethylpentane	0.000	0.000	0.000	0.000	3.106	1.2358
octane	0.000	0.000	0.000	0.000	3.677	1.2358
nonane	0.000	0.000	0.000	0.000	4.182	1.3767
decane	0.000	0.000	0.000	0.000	4.686	1.5176
undecane	0.000	0.000	0.000	0.000	5.191	1.6590
dodecane	0.000	0.000	0.000	0.000	5.696	1.7994
tridecane	0.000	0.000	0.000	0.000	6.200	1.9400
tetradecane	0.000	0.000	0.000	0.000	6.705	2.0810
methylcyclopentane	0.225	0.100	0.000	0.000	2.907	0.8454
cyclohexane	0.310	0.100	0.000	0.000	2.964	0.8454
methylcyclohexane	0.244	0.060	0.000	0.000	3.319	0.9863
cycloheptane	0.350	0.100	0.000	0.000	3.704	0.9863
benzene	0.610	0.520	0.000	0.140	2.786	0.7164
toluene	0.601	0.520	0.000	0.140	3.325	0.8573
ethylbenzene	0.613	0.510	0.000	0.150	3.778	0.9982
m-xylene	0.623	0.520	0.000	0.160	3.839	0.9982
p-xylene	0.613	0.520	0.000	0.160	3.839	0.9982
o-xylene	0.663	0.560	0.000	0.160	3.939	0.9982
1-hexene	0.080	0.080	0.000	0.070	2.572	0.9110
1-hexyne	0.166	0.220	0.100	0.120	2.510	0.8680
1-heptyne	0.160	0.230	0.090	0.100	3.000	1.0089
2-butanone	0.166	0.700	0.000	0.510	2.287	0.6879
2-pentanone	0.143	0.680	0.000	0.510	2.755	0.8288
3-pentanone	0.154	0.660	0.000	0.510	2.811	0.8288
1,4 dioxane	0.329	0.750	0.000	0.640	2.892	0.6810
methanol	0.278	0.440	0.430	0.470	0.970	0.3082
ethanol	0.246	0.420	0.370	0.480	1.485	0.4491
1-propanol	0.236	0.420	0.370	0.480	2.031	0.5900
2-propanol	0.212	0.360	0.330	0.560	1.764	0.5900
2-methyl-1-propanol	0.217	0.390	0.370	0.480	2.413	0.7309
1-butanol	0.224	0.420	0.370	0.480	2.601	0.7309
trifluoroethanol	0.015	0.600	0.570	0.250	1.224	0.5022
diethyl ether	0.041	0.250	0.000	0.450	2.015	0.7309
diisopropyl ether	-0.063	0.170	0.000	0.570	2.501	1.0127
chloroform	0.425	0.490	0.150	0.020	2.480	0.6167
dichloromethane	0.390	0.570	0.100	0.050	2.019	0.4943
tetrachloromethane	0.460	0.380	0.000	0.000	2.823	0.7391
acetonitrile	0.237	0.900	0.070	0.320	1.739	0.4042
nitromethane	0.313	0.950	0.060	0.310	1.892	0.4237
1-nitropropane	0.242	0.950	0.000	0.310	2.894	0.7055
triethylamine	0.101	0.150	0.000	0.790	3.040	1.0538
pyridine	0.631	0.840	0.000	0.520	3.022	0.6753
thiophene	0.687	0.570	0.000	0.150	2.819	0.6411
propionaldehyde	0.196	0.650	0.000	0.450	1.815	0.5470
butyraldehyde	0.187	0.650	0.000	0.450	2.270	0.6879
ethene	0.107	0.100	0.000	0.070	0.289	0.3470
propene	0.100	0.080	0.000	0.070	0.946	0.4880
1-butene	0.100	0.080	0.000	0.070	1.529	0.6290
1,3-butadiene	0.320	0.230	0.000	0.100	1.543	0.5862
carbon dioxide	0.000	0.280	0.050	0.100	0.058	0.2810

coefficients that have been calculated for the $[\text{FAP}]^-$ can be combined with our previously reported cation-specific equation coefficients³⁵ to enable $\log K_L$ and $\log P$ predictions for additional ILs containing the $[\text{FAP}]^-$ anion.

The experimental $\log K_L$ and $\log P$ data compiled in Table 2 for solutes dissolved in $[\text{BMIm}]^+[\text{BETI}]^-$ at 298 K can be used to calculate the anion-specific equation coefficients for the $[\text{BETI}]^-$ anion. Included as the last five entries in Table 2 are $\log K_L$ and $\log P$ values determined for gaseous solutes, including four alkenes (ethene, propene, 1-butene, 1,3-butadiene) and carbon dioxide, all of which were calculated from published Henry's law constants reported earlier by Kilaru and Scovazzo.⁴⁰ The analysis of the $\log K_L$ and $\log P$ data in Table 2 yields the following two Abraham model correlations:

$$\log K_L = -0.460(0.046) + 0.141(0.084)E + 2.206(0.076)S \\ + 1.980(0.108)A + 0.696(0.083)B + 0.613(0.012)L \\ (N = 53, \text{SD} = 0.093, R^2 = 0.989, F = 860.1) \quad (11)$$

$$\log P = 0.023(0.072) + 0.083(0.099)E + 0.334(0.095)S \\ - 1.701(0.130)A - 4.236(0.098)B + 3.041(0.062)V \\ (N = 51, \text{SD} = 0.110, R^2 = 0.996, F = 2094) \quad (12)$$

The derived correlation models describe the observed $\log K_L$ and $\log P$ results to within standard deviations of $\text{SD} = 0.093$ (eq 11) and $\text{SD} = 0.110$ (eq 12) log units, respectively. The calculated anion-specific equation coefficients for the $[\text{BETI}]^-$ anion for the $\log K_L$ correlation model are: $c_{\text{anion}} = -0.033$, $e_{\text{anion}} = 0.004$, $s_{\text{anion}} = 0.245$, $a_{\text{anion}} = 0.199$, $b_{\text{anion}} = 0.250$, and $l_{\text{anion}} = 0.081$. These values were computed by subtracting the published cation-specific equation coefficient values³⁵ of $c_{\text{cation}} = -0.427$, $e_{\text{cation}} = 0.137$, $s_{\text{cation}} = 1.961$, $a_{\text{cation}} = 2.179$, $b_{\text{cation}} = 0.946$, and $l_{\text{cation}} = 0.694$ for $[\text{BMIm}]^+$ from the coefficients in eq 11. The $\log P$ anion-specific equation coefficients for $[\text{BETI}]^-$ of $c_{\text{anion}} = 0.068$, $e_{\text{anion}} = -0.334$, $s_{\text{anion}} = 0.217$, $a_{\text{anion}} = -0.196$, $b_{\text{anion}} = -0.238$, and $v_{\text{anion}} = -0.279$ were computed in similar fashion.

Assembled in Table 3 are the partition coefficient data for solutes dissolved in $[\text{D}_2\text{MIm}]^+[\text{Tf}_2\text{N}]^-$ at 298 K. The analysis of the tabulated $\log K_L$ and $\log P$ values yields the following expressions:

$$\log K_L = -0.252(0.089) - 0.269(0.088)E + 1.603(0.082)S \\ + 1.946(0.125)A + 0.354(0.093)B + 0.856(0.027)L \\ (N = 40, \text{SD} = 0.082, R^2 = 0.979, F = 315.3) \quad (13)$$

$$\log P = -0.093(0.147) - 0.052(0.118)E + 0.040(0.128)S \\ - 1.620(0.176)A - 4.667(0.132)B + 4.034(0.132)V \\ (N = 40, \text{SD} = 0.118, R^2 = 0.996, F = 1816) \quad (14)$$

Triethylamine was removed from the final regression analysis as its calculated $\log K_L$ and $\log P$ values differ from the observed values by more than three standard deviations. Equations 13 and 14 describe the observed $\log K_L$ and $\log P$ data to within standard deviations of 0.082 and 0.118 log units for the remaining 40 solutes. The calculated coefficients in eqs 13 and 14 correspond to the cation-specific values for the $[\text{D}_2\text{MIm}]^+$ cation itself. This is true because in establishing our computation methodology, the equation coefficients for the $[\text{Tf}_2\text{N}]^-$ anion were set equal to

zero to provide a reference point from which all other equation coefficients would be calculated.

In Table 4, there are 44 experimental $\log K_L$ and 42 experimental $\log P$ values for solutes dissolved in $[\text{EMIm}]^+[\text{MeSO}_3]^-$. Preliminary regression analyses on the entire data set indicated that triethylamine and carbon tetrachloride were statistical outliers. These two solutes were eliminated from the data set, and the regression analysis performed to yield

$$\log K_L = -1.398(0.119) + 0.485(0.162)E + 2.562(0.160)S \\ + 6.616(0.275)A + 0.495(0.198)B + 0.642(0.028)L \\ (N = 42, SD = 0.153, R^2 = 0.976, F = 288.5) \quad (15)$$

$$\log P = -0.799(0.207) + 0.493(0.204)E + 0.644(0.217)S \\ + 2.842(0.363)A - 4.440(0.243)B + 3.007(0.164)V \\ (N = 40, SD = 0.189, R^2 = 0.981, F = 393.6) \quad (16)$$

Equations 15 and 16 describe experimental $\log K_L$ and $\log P$ data to within standard deviations of $SD = 0.153$ and $SD = 0.189$ log units, respectively. As was the case for all four ILs studied, a slightly larger deviation was noted for the $\log P$ correlation. The slightly larger standard deviation is to be expected as the $\log P$ values also contain the experimental uncertainty associated with $\log K_w$ data that were used to convert the measured $\log K_L$ data to $\log P$ via eq 6. The calculated anion-specific equation coefficients for $[\text{MeSO}_3]^-$ based on the $\log K_L$ correlation are: $c_{\text{anion}} = -0.872$, $e_{\text{anion}} = 0.234$, $s_{\text{anion}} = 0.276$, $a_{\text{anion}} = -1.703$, $b_{\text{anion}} = -0.552$, and $l_{\text{anion}} = 0.001$. These values were computed by subtracting the published cation-specific equation coefficient values³⁵ of $c_{\text{cation}} = -0.526$, $e_{\text{cation}} = 0.248$, $s_{\text{cation}} = 2.286$, $a_{\text{cation}} = 2.219$, $b_{\text{cation}} = 1.047$, and $l_{\text{cation}} = 0.641$ for $[\text{EMIm}]^+$ from the coefficients in eq 15. The $\log P$ anion-specific equation coefficients for $[\text{MeSO}_3]^-$ of $c_{\text{anion}} = 0.824$, $e_{\text{anion}} = 0.094$, $s_{\text{anion}} = 0.400$, $a_{\text{anion}} = 4.289$, $b_{\text{anion}} = -0.742$, and $v_{\text{anion}} = -0.098$ were computed likewise.

CONCLUDING REMARKS

Partition and infinite dilution activity coefficients of organic compounds in the four new ILs $[\text{HMIm}]^+[\text{FAP}]^-$, $[\text{BMIm}]^+[\text{BETI}]^-$, $[\text{D}_2\text{MIm}]^+[\text{Tf}_2\text{N}]^-$, and $[\text{EMIm}]^+[\text{MeSO}_3]^-$ were measured using inverse gas chromatography from (312 to 353) K. The partition coefficients were also converted into water-to-IL partition coefficients using the corresponding gas-to-water partition coefficients. Both sets of partition coefficients were analyzed using the Abraham solvation parameter model with cation-specific and anion-specific equation coefficients. The derived equations correlated the experimental gas-to-IL and water-to-IL partition coefficient data to within average standard deviations of 0.113 and 0.143 log units, respectively.

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REFERENCES

(1) Meindersma, G. W.; Galán Sánchez, L. M.; Hansmeier, A. R.; De Haan, A. B. Application of task-specific ionic liquids for intensified separations. *Monatsh. Chem.* **2007**, *138*, 1125–1136.

(2) Brennecke, J. F.; Maginn, E. J. Ionic liquids: Innovative fluids for chemical processing. *AIChE J.* **2001**, *47*, 2384–2389.

(3) Earle, M. J.; Seddon, K. R. Ionic liquids. Green solvents for the future. *Pure Appl. Chem.* **2000**, *72*, 1391–1398.

(4) Revelli, A. L.; Sprunger, L. M.; Gibbs, J.; Acree, W. E., Jr.; Baker, G. A.; Mutelet, F. Activity Coefficients at Infinite Dilution of Organic Compounds in Trihexyl(tetradecyl)phosphonium Bis(trifluoromethylsulfonyl)imide Using Inverse Gas Chromatography. *J. Chem. Eng. Data* **2009**, *54*, 977–985.

(5) Revelli, A. L.; Mutelet, F.; Turmine, M.; Solimando, R.; Jaubert, J. N. Activity Coefficients at Infinite Dilution of Organic Compounds in 1-Butyl-3-methylimidazolium Tetrafluoroborate Using Inverse Gas Chromatography. *J. Chem. Eng. Data* **2008**, *54*, 90–101.

(6) Mutelet, F.; Butet, V.; Jaubert, J. N. Application of Inverse Gas Chromatography and Regular Solution Theory for Characterization of Ionic Liquids. *Ind. Eng. Chem. Res.* **2005**, *44*, 4120–4127.

(7) Mutelet, F.; Jaubert, J. N. Accurate measurements of thermodynamic properties of solutes in ionic liquids using inverse gas chromatography. *J. Chromatogr., A* **2006**, *1102*, 256–267.

(8) Mutelet, F.; Jaubert, J. N.; Rogalski, M.; Boukherissa, M.; Dicko, A. Thermodynamic Properties of Mixtures Containing Ionic Liquids: Activity Coefficients at Infinite Dilution of Organic Compounds in 1-Propyl Boronic Acid-3-Alkylimidazolium Bromide and 1-Propenyl-3-alkylimidazolium Bromide Using Inverse Gas Chromatography. *J. Chem. Eng. Data* **2006**, *51*, 1274–1279.

(9) Mutelet, F.; Jaubert, J. N.; Rogalski, M.; Harmand, J.; Sindt, M.; Mieloszynski, J. L. Activity Coefficients at Infinite Dilution of Organic Compounds in 1-Methacryloyloxyalkyl-3-methylimidazolium Bromide Using Inverse Gas Chromatography. *J. Phys. Chem. B* **2008**, *112*, 3773–3785.

(10) Mutelet, F.; Revelli, A. L.; Jaubert, J. N.; Sprunger, L. M.; Acree, W. E., Jr.; Baker, G. A. Partition Coefficients of Organic Compounds in New Imidazolium and Tetralkylammonium Based Ionic Liquids Using Inverse Gas Chromatography. *J. Chem. Eng. Data* **2010**, *55*, 234–242.

(11) Arlt, M.; Seiler, M.; Jork, C.; Schneider, T. DE Patent No. 10114734, 2001.

(12) Alonso, L.; Arce, A.; Francisco, M.; Soto, A. Solvent extraction of thiophene from *n*-alkanes (C_7 , C_{12} , and C_{16}) using the ionic liquid $[\text{C}_8\text{mim}][\text{BF}_4]$. *J. Chem. Thermodyn.* **2008**, *40*, 966–972.

(13) Poole, C. F. Chromatographic and spectroscopic methods for the determination of solvent properties of room temperature ionic liquids. *J. Chromatogr., A* **2004**, *1037*, 49–82.

(14) Heintz, A. Recent developments in thermodynamics and thermophysics of non-aqueous mixtures containing ionic liquids. a review. *J. Chem. Thermodyn.* **2005**, *37*, 525–535.

(15) Deenadayalu, N.; Letcher, T. M.; Reddy, P. Determination of Activity Coefficients at Infinite Dilution of Polar and Nonpolar Solutes in the Ionic Liquid 1-Ethyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide Using Gas-Liquid Chromatography at the Temperature 303.15 or 318.15 K. *J. Chem. Eng. Data* **2005**, *50*, 105–108.

(16) Krummen, M.; Wasserscheid, P.; Gmehling, J. Measurement of Activity Coefficients at Infinite Dilution in Ionic Liquids Using the Dilutor Technique. *J. Chem. Eng. Data* **2002**, *7*, 1411–1417.

(17) Letcher, T. M.; Soko, B.; Ramjugernath, D.; Deenadayalu, N.; Nevines, A.; Naicker, P. K. Activity Coefficients at Infinite Dilution of Organic Solutes in 1-Hexyl-3-methylimidazolium Hexafluorophosphate from Gas-Liquid Chromatography. *J. Chem. Eng. Data* **2003**, *48*, 708–711.

(18) Domańska, U.; Marciniak, A. Physicochemical properties and activity coefficients at infinite dilution for organic solutes and water in the ionic liquid 1-decyl-3-methylimidazolium tetracyanoborate. *J. Phys. Chem. B* **2010**, *114*, 16542–16547.

(19) Domańska, U.; Marciniak, A.; Królikowska, M.; Arasimowicz, M. Activity coefficients at infinite dilution measurements for organic solutes and water in the ionic liquid 1-hexyl-3-methylimidazolium thiocyanate. *J. Chem. Eng. Data* **2010**, *55*, 2532–2536.

(20) Marciniak, A. Influence of cation and anion structure of the ionic liquid on extraction processes based on activity coefficients at infinite dilution. A review. *Fluid Phase Equilib.* **2010**, *294*, 213–233.

- (21) Freemantle, M. Ionic liquids in organic synthesis. *Chem. Eng. News* **2004**, 82, 44–49.
- (22) Zein El Abedin, S.; Borissenko, N.; Endres, F. Electropolymerization of benzene in a room temperature ionic liquid. *Electrochem. Commun.* **2004**, 6, 422–426.
- (23) Muldoon, M. J.; Aki, S. N. V. K.; Anderson, J. L.; Dixon, J. K.; Brennecke, J. F. Improving carbon dioxide solubility in ionic liquids. *J. Phys. Chem. B* **2007**, 111, 9001–9009.
- (24) Endres, F.; MacFarlane, D.; Abbott, A. Electropolymerization of benzene in a room temperature ionic liquid. *Electrodeposition from Ionic Liquids*; Wiley-VCH: New York, 2008.
- (25) Chrobok, A.; Swadzba, M.; Baj, S. Oxygen solubility in ionic liquids based on 1-alkyl-3-methylimidazolium cations. *Pol. J. Chem.* **2007**, 81, 337–344.
- (26) Dyson, P. J.; Laurenczy, G.; Ohlin, A.; Vallance, J.; Welton, T. Determination of hydrogen concentration in ionic liquids and the effect (or lack of) on rates of hydrogenation. *Chem. Commun.* **2003**, 2418–2419.
- (27) O'Mahony, A. M.; Silvester, D. S.; Aldous, L.; Hardacre, C.; Compton, R. G. Effect of water on the electrochemical window and potential limits of room-temperature ionic liquids. *J. Chem. Eng. Data* **2008**, 53, 2884–2891.
- (28) Baker, S. N.; Baker, G. A. A Simple Colorimetric Assay of Ionic Liquid Hydrolytic Stability. *Aust. J. Chem.* **2005**, 58, 174–177.
- (29) Revelli, A.-L.; Mutelet, F.; Jaubert, J.-N.; Garcia-Martinez, M.; Sprunger, L. M.; Acree, W. E., Jr.; Baker, G. A. Study of ether-, alcohol-, or cyano-functionalized ionic liquids using inverse gas chromatography. *J. Chem. Eng. Data* **2010**, 55, 2434–2443.
- (30) Acree, W. E., Jr.; Abraham, M. H. The analysis of solvation in ionic liquids and organic solvents using the Abraham model linear free energy relationship. *J. Chem. Technol. Biotechnol.* **2006**, 81, 1441–1446.
- (31) Abraham, M. H.; Acree, W. E., Jr. Comparative analysis of solvation and selectivity in room temperature ionic liquids using the Abraham linear free energy relationship. *Green Chem.* **2006**, 8, 906–915.
- (32) Abraham, M. H.; Zissimos, A. M.; Huddleston, J. G.; Willauer, H. D.; Rogers, R. D.; Acree, W. E., Jr. Some novel liquid partitioning systems: Water-ionic liquids and aqueous biphasic systems. *Ind. Eng. Chem. Res.* **2003**, 42, 413–418.
- (33) Sprunger, L.; Clark, M.; Acree, W. E., Jr.; Abraham, M. H. Characterization of room-temperature ionic liquids by the Abraham model with cation-specific and anion-specific equation coefficients. *J. Chem. Inf. Model.* **2007**, 47, 1123–1129.
- (34) Sprunger, L. M.; Proctor, A.; Acree, W. E., Jr.; Abraham, M. H. LFER correlations for room temperature ionic liquids: Separation of equation coefficients into individual cation-specific and anion-specific contributions. *Fluid Phase Equilib.* **2008**, 265, 104–111.
- (35) Sprunger, L. M.; Gibbs, J.; Proctor, A.; Acree, W. E., Jr.; Abraham, M. H.; Meng, Y.; Yao, C.; Anderson, J. L. Linear Free Energy Relationship Correlations for Room Temperature Ionic Liquids: Revised Cation-Specific and Anion-Specific Equation Coefficients for Predictive Applications Covering a Much Larger Area of Chemical Space. *Ind. Eng. Chem. Res.* **2009**, 48, 4145–4154.
- (36) Burrell, A. K.; Del Sesto, R. E.; Baker, S. N.; McCleskey, T. M.; Baker, G. A. The Large Scale Synthesis of Pure Imidazolium and Pyrrolidinium Ionic Liquids. *Green Chem.* **2007**, 9, 449–454.
- (37) Baker, S. N.; McCleskey, T. M.; Pandey, S.; Baker, G. A. Fluorescence studies of protein thermostability in ionic liquids. *Chem. Commun.* **2004**, 10, 940–941.
- (38) Cruikshank, A. J. B.; Windsor, M. L.; Young, C. L. The use of gas chromatography to determine activity coefficients and second virial coefficients of mixtures. *Proc. R. Soc. London* **1966**, A295, 259–270.
- (39) Blahut, A.; Sobota, M.; Dohnal, V.; Vrbka, P. Activity coefficients at infinite dilution of organic solutes in the ionic liquid 1-ethyl-3-methylimidazolium methanesulfonate. *Fluid Phase Equilib.* **2010**, 299, 198–206.
- (40) Kilaru, P. K.; Scovazzo, P. Correlations of low-pressure carbon dioxide and hydrocarbon solubilities in imidazolium-, phosphonium-, and ammonium-based room temperature ionic liquids. Part 2. Using activation energy of viscosity. *Ind. Eng. Chem. Res.* **2008**, 47, 910–919.