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#### STIRLING-ENGINE THERMODYNAMIC ANALYSIS: A USERS GUIDE TO SEAM!

by

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Components Technology Division

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NOMENCLATURE

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#### Nomenclature

Major Symbols	Definition	Greek Symbols	
AF	Free-flow area	α	Crank angle
AW	Wetted surface area	Y	Specific heat ratio
AX	Cross-sectional area	δ	Differentials of variables
С	Specific heat	μ	Viscosity
D	Diameter	π	P1 = 3.14159
d	Derivative of a viriable	ρ	Density
E	Energy	σ	Ratio of minimum free flow area to frontal area
e	Eccentricity	ω	Crank angular speed
f	Fanning friction factor	•	Phase angle
н	Enthalpy		
h	Heat-transfer coefficient		
j	Colburn factor	Subscripts	
k	Conductivity		
L	Length	AC	Half the maximum compression space
m	Mass	AE	Half the maximum expansion space
ů	Mass flow rate	С	Compression space
M	Dimensionless uss	D	Dead space
Р	Ргевзиге	DC <sub>x</sub>	Dead space on compression side of x
P	Dimensionless pressure	DEx	Dead space on expansion side of x
Q	Heat flow rate	E	Expansion space
R	Gas constant, effective thermal resistance	f	Friction
Re	Reynolds Number = puD <sub>b</sub> /µ	8	Gas
r	Radius	н	Heater
τvt	Dimensionless volume to temperature ratio	h	Hydraulic
s <sub>T</sub>	Stanton number = h/Cppu	i	Inner wall
Т	Gas temperature	ĸ	Cooler
T	Dimensionless temperature	o	Outer wall
T	Gas temperature of adjacent heat exchanger	P	Pressure
те	Outside environment température	R	Regenerator
TW	Inner wall temperature	Т	Total
t	Time	v	Volume
u	Gam velocity	w	Wall
v	Valume	x	Variable component or position notation
V	Dimensionless volume	a	Crank angle
w	Work		
ω	Dimensionless work		
x	Volume fraction		

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#### ABSTRACT

This report provides background and procedural information for the use of a general-purpose Stirling-engine analysis code developed at Argonne Mational Laboratory and available through the National Energy Software Center. Different engine configurations are easily specified, or the user may make use of provided data for existing engines, both kinematic and free-piston. The code models heat transfer and fluid mechanics throughout the engine and accounts for system energy flows and losses. Good agreement is shown between code predictions and experimental measurements. The present analysis method was chosen for fast execution and useful information on energy flows in the system. A description is provided of the code structure that is intended to accept different analysis modules that can provide improved system modeling or optimization capability.

#### 1. INTRODUCTION

In the last 15 years various techniques and codes for analyzing Stirling engines have emerged. See, for example, Rios [1], Urieli [2], Tew [3], Martini [4], Schock [5], Gedeon [6], Kirkley [7], Glassford [8], Rauch [9], Organ [10], and Beans [11]. These, as well as earlier techniques and codes, may be separated into the following categories for purposes of comparison.

#### Category 1: Engine Performance Predictions Made

These codes calculate overall performance parameters such as engine power and efficiency, but provide no information on component performance or transient conditions during the cycle. They use closed-form solutions to simplified dynamic equations. Typical assumptions are that piston motion is sinusoidal and that temperatures within the engine do not vary with time.

#### Category 2: Limited Transient Information Calculated

These codes account for actual piston movement, compute changing conditions within the engine during the cycle, and calculate engine performance. Typical assumptions are that the working fluid is an ideal gas, momentum effects are ignored, and pressure is uniform within the engine at any time.

#### Category 3: Detailed Transient Information Calculated

In these codes the entire set of field equations is solved in terms of position and time; i.e., conditions are determined in each engine cell at each time step. Typical assumptions are that one-dimensional analysis is sufficient and that steady flow correlations may be used to predict heattransfer and fluid-friction coefficients.

Examples of analysis models in the above three categories are Schmidt [12], Martini [4], and Urieli [2], respectively. The analysis codes outlined in the latter two categories attempt to realistically model heat transfer and fluid flows in the system. However, a comparative code study [13] found the available codes were too constrained to permit a comparison on the basis of the same set of experimental data. Existing codes:

- Were generally calibrated for a particular engine or type of engine,
- Had differing gas and metal properties,
- Had differing heat transfer and friction correlations,
- Were unable to achieve stable cyclic steady state, or
- Were classified as proprietary and accessible only under license.

Each category of codes was intended for a particular need; however, the relative merits of codes within each class or between classes could not be assessed. Nor was there the capability of analyzing different Stirling engines over a range of operating conditions with any of the existing codes, much less the capability of comparing such calculations between codes. The requirements considered in the development of the Argonne Stirling engine analysis code are listed in Table I. TABLE I. Requirements Considered in Development of Argonne Stirling Engine Analysis Code Available for wide distribution Well documented Validated against real engines User oriented Compatible with both mini and large computers Able to evaluate a wide range of volume-variation techniques Able to compute answers using different components, materials, and working fluids easily Able to achieve cyclic steady state Able to compute answers using a stable numerical-integration scheme Able to determine mass and energy flows Able to be used with different solution techniques for the governing equations describing Stirling engine fluid dynamics

The approach selected to meeting these requirements was to separate the analysis method from the more general requirements of providing standardized input and output capabilities and libraries of standard functions. The code is thus structured to have the generalized modules described in Chapter 2 and the replaceable analysis modules, in this case SEAM1 (Stirling Engine Analysis Module 1), which is described in Chapter 3. SEAMI is based upon the D.Sc. Thesis of Rios [1] and falls into the second category of code types described That is, performance and transient information are in the introduction. provided, but computation time is short. Thus, the needs of most Stirlingcycle researchers are accommodated. Future code releases will provide improved analysis capability. The details of how to use the code, including input, perturbation, and graphics are in Chapter 4. Finally, Chapter 5 compares code predictions with experimental data.

The code and sample input and output are available from the National Energy Software Center.

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#### 2.1 DESCRIPTION OF GENERAL MODULES

The Stirling engine analysis system consists of the four modules as shown in Fig. 1.



Fig. 1. Framework of Stirling Engine Analysis System

The analysis module provides a specific analysis capability and is discussed in detail in Chapter 3. The more general system modules are now discussed as well as the general function of the analysis module.

Briefly stated, the <u>Input</u> module reads the engine specifications and operating data, provides default values, estimates initial conditions, and edits the results to verify the starting point. The <u>Output</u> wodule writes out transient and summary results as specified by the Input data. The <u>Standard Functions</u> module contains standard calculation subroutines that any Stirlingengine code might need, such as gas and metal properties, heat-transfer and friction coefficients, variable volume calculations, and additional heat losses that are not integrated into the analysis module.

#### 2.2 INPUT MODULE

This section contains a general description of how the Input Module works and how the data are input. The meanings of the individual input variables are given in Appendix A.

2.2.1 <u>The Tasks of the Input Module</u>. The Input Module does the following tasks for the ANL Stirling Engine Analysis Model through the use of four subprograms:

Reads the optional perturbation data to control the number of cases, and calls the other subroutines (INPDRV).

Reads the data describing the engine type, dimensions, and operating conditions, as well as calculation parameters such as time step, number of cycles, etc. (INPUT).

Computes omitted input variables (if possible), default options, and other initializing values from the input data (INITAL).

Organizes and prints the input data in an easy-to-read format for editing by the user (EDTINP).

The design options available are shown in Table II.

2.2.2 <u>Driver Module</u>. The INPDRV Subroutine is called from the Main program for each case. As is shown in Fig. 2 this routine determines where the input is to be read from and whether the data needs to be reinitialized or editted.

2.2.3 <u>Input Data</u>. The INPUT Subroutine is called from INPDRV one time and reads three types of data:

- (1) The title, and general scalar values describing the engine and operating conditions as a whole.
- (2) An array of values for each of 30 or less contiguous engine cells through which the working gas flows.
- (3) An array of values for each of four or less other types of engine components such as a buffer space.

Each of the above types of input can be seen in the sample input deck, Table A-1 of Appendix 4.

All input is read from logical unit 5. The three input blocks are briefly described below.

- (1) The title is read as an 80-character alphanumeric array and occupies one card (or record). The title should be used as a general input deck identifier. The general scalar variables, such as gas type, frequency, engine design, etc. are listed in Namelist GINPT. This Namelist is read only once.
- (2) The basic cell information arrays, II (dimension 8) and AA (dimension 18), are in Namelist CELL, which is read once for each of the adjacent cells. Array II contains integer values,

#### TABLE II. Design Options Available

1. Mechanical Configurations

In line design or alpha engine; two pistons, two cylinders (Fig. A-2).

Double acting piston design (Fig. A-3).

Displacer design (Fig. A-4).

GPU-3: IDESGN = 3

2. Type Drive Mechanisms

Connecting rod mechanism.

Rhombic drive.

Dynamic analysis (not yet available) for free piston.

GPU-3: IDRIVE = 1 (Fig. A-5).

3. Working Fluids

	Hydrogen	Air
	Helium	Carbon dioxide
	Nitrogen	Methane
4.	Structural Materials	
	Aluminum T4-2024	Stainless steels 304, 310, 316
	Copper	Titanium nickel
	Inconel X-750	Nickel
	K Monel	

5



# Fig. 2. INPDRV Subprogram

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and AA contains floating-point values for the cell. After Namelist CELL is read, the temporary values in II and AA are assigned to the appropriate location in the permanent storage (see Appendix A).

(3) Namelist ADDED is read once for each "other" type of cell. The cell information arrays in Namelist ADDED are JJ (dimension 6) and BB (dimension 13). As above, these values are stored each time they are read. These array names are described in Appendix A.

2.2.4 <u>Input Initialization</u>. The Initial Subprogram is called from INPDRV as a function of the value in variable ICHNG. The program is broken into two segments, the first of which initializes variables for every case such as temperature convergence and time-step related variables. The second segment is called whenever a significant data change is input. This section:

- Initializes piston areas and cylinder bores.
- Determines which cells are associated with the various heat exchangers,
- Initializes the variable volume routine discussed in Sec.
   2.3.3 and determines the crank angle for minimum total compression volume.
- Initializes gas reference conditions.
- Sets up "Schmidt Analysis" constants.
- Resets gas mass and pressure to be consistent.

2.2.5 <u>Input Edit</u>. The EDTINP Subprogram is called from INPDRV as a function of the value in variable ICHNG. The program edits the input for the convenience of the user.

#### 2.3 STANDARD FUNCTIONS MODULE

This module consists of separate subroutines used to calculate values that are needed by most Stirling-engine codes. The calculation of gas and metal properties, heat-transfer and friction coefficients, volumes, and conduction losses are put in separate subroutines, which will be used by the various analysis modules. Hence, the analysis modules may be compared without being influenced by these standard calculations. The various subroutines in this module are described below.

2.3.1 <u>Gas and Metal Properties</u>. The following routines are used by the various modules to determine the thermophysical properties of gas and metal.

XGAS:	a function subprogram to return gas values
XMETAL:	a function subprogram to return metal values
VALUE:	a subroutine used to evaluate the polynominal approximation of the experimental data
BLOCK DA	TA: a tabulation of the coefficients needed by the polynominal fit

The gas and metal properties returned to the calling program are shown in Table III.

TABLE III. Fluid an	d Metal Properties Avai	lable
Fluid Properties	Gases Included	
Specific Heat, C <sub>p</sub>	H <sub>2</sub> , He, N <sub>2</sub> , Air, Co <sub>2</sub> ,	сн <sub>4</sub>
Thermal Conductivity, k		
Viscosity, µ		
Gas Constant, R		
Metal Properties	Metals Included	
Specific Heat, C <sub>D</sub>	Aluminum T4-2024	K Monel
Thermal Conductivity, k	Copper	Titanium
Density, p	Inconel X-750	Nickel
		<u></u>

Each of the above properties, except for the gas constant, is dependent upon the gas or metal temperature. Therefore, to obtain property values, the temperature and property identifying number must be supplied as arguments. A metal property also requires that the engine cell number be supplied as an argument, since different components of the engine may have different wall metals.

2.3.1.1 <u>Description of Property Subroutines</u>. Each gas and metal property is approximated at a function of temperature T by cubic splines using a library program contained in the International Mathematical and Statistical Library (IMSL) package.

The temperature range for each approximated set of property data is taken to be 300 K  $\leq$  T  $\leq$  T<sub>max</sub>, where T<sub>max</sub> is determined by the availability of reliable data for the given gas or metal. For consistency, this temperature range is transformed to the interval [0,1]. The interval is then divided into four subintervals with "nodes" at 0, 0.25, 0.5, 0.75, and 1. The data on the four subintervals are approximated with four cubic polynomials that meet smoothly at the interior nodes.

The Property Subroutine then evaluates a function f(T) of a gas or metal property for T between 300 K and  $T_{max}$ :

$$f(T) = \sum_{i=0}^{3} C_{i}(TR - n)^{i} = \text{ property value}, \qquad (1)$$

where,

$$TR = (T - 300)/(T_{max} - 300) = temperature ratio,$$

$$n = the "node" just to the left of TR. (n = 0, 0.25, 0.5)$$

$$0.75, or 1),$$

$$C_{0}, C_{1}, C_{2}, C_{3} = the appropriate set of cubic coefficients for the given property, material, and sub-interval.$$

,

If T < 300 K or T >  $T_{max}$ , the property value is calculated at T = 300 K or T =  $T_{max}$ , respectively. The user should, however, be aware that for metals,  $T_{max} \cong$  melting point.

2.3.1.2 <u>Implementation of the Property Subroutines</u>. To calculate one of the four gas properties and store its value in location X, the following Fortran statement is used in the Analysis Module:

X = XGAS(IPROP,T),

where

and

T = temperature (K)

and

IPROP = an integer variable, initialized in INITAL and stored in common, that identifies the gas property desired, as shown below:

IPROP	Gas Property Value Returned	Units
IRGAS	Gas constant, R	J/(kg-K)
IMUGAS	Viscosity, µ	N-S/m <sup>2</sup>
ICPGAS	Specific hear, C <sub>p</sub>	J/(kg-K)
IKGAS	Thermal conductivity, k	₩/(m-K)

Note that other gas properties, such as  $C_v$  and  $\gamma = C_p/C_v$ , can be obtained from the above properties. The type of gas is identified by the input variable IGAS, which is in common block IGEN and has a value from 1 to 6 as listed in Sec. 4.2.1.

To obtain one of the three metal properties and store the value in location X, the following Fortran statement is used:

X = XMETAL (IPROP, ICELL, T)

T = temperature (K)

ICELL = the engine cell number. The property value returned is for the wall metal, MTLWAL (ICELL) (see App. A.3.1),

and

where

IPROP = an integer variable, initialized in INITAL and stored in common, that identified the metal property, as shown below:

IPROP	Metal Property Value Returned	Units
IKM	Conductivity, k	₩/(m-K)
ICPM	Specific heat, C <sub>p</sub>	J/(kg-K)
IRHOM	Density, p	kg/m <sup>3</sup>

In two cases we use properties of metal from places other than an ordinary engine cell wall: (a) the filler metal in the regenerator, or (b) the wall metal in one of the four additional types of engine components: displacer dome, cold piston buffer space, hot piston buffer space, and crankcase.

To obtain a property of the filler metal in a regenerator cell with cell number ICELL, the following Fortran statement is used:

X = XMETAL(IPROP, ICELL + 1000, T),

where

IPROP, ICELL, and T are as above.

Finally, to obtain a property of the wall metal of one of the four additional components in case (b) above, we use the statement:

X = XMETAL(IPROP, ICELL + 2000, T),

where

IPROP and T are as above, and ICELL is the appropriate subscript for IAMTL.

In each of the above cases, the metal properties subroutine determines the metal type from the value of ICELL and from the values of the arrays MTLWAL, MTLWIR, and IAMTL (see the input description in Appendix A).

2.3.1.3 <u>Values in Property Subroutines. The</u> data values for the gas and metal properties were obtained from Refs. [15]-[17]. When computed and tabulated values were compared, the accuracy of the Properties Subroutine was found to be within 2% for gases and 8% for metals. The 816 cubic coefficients for the spline approximation (51 approximations x four intervals for each approximation x four coefficients for each interval = 816 coefficients) are stored in a BLOCK DATA subroutine.

2.3.2 <u>Heat-Transfer and Friction-Factor Subroutine</u>. When supplied with an engine cell number as well as the Reynolds and Prandtl numbers, Re and Pr, for the gas flowing through a passage, this subroutine, HTF, returns the Stanton number and "Fanning" friction factor, for a variety of flow passages. The convective heat-transfer coefficient, h, can easily be obtained from the Stanton number, St, since

$$St = h/C_pG, \qquad (2)$$

where

 $C_p$  = specific heat at constant pressure G = mass flux of the gas.

and

correlation formulas for friction The and heat-transfer coefficients were taken from a variety of standard sources and were derived from experimental steady flow data, even though they are being used for reversing flow. Some results are available for nonsteady and reversing flow. such as [18]-[24], and limited formulas are available. However, most of these studies have not settled the pertinent question of how reversing-flow correlations compare with steady-flow correlations. Kim [25], for example, reports that heat-transfer and friction factors in reversing-flow experiments with randomly packed sphere regenerators were about 20% higher than the steady-flow correlations. The "uncertainty" in these results was estimated to be within 20%. On the other hand, Murray and Martin [26] indicate that in wire-mesh-screen regenerators, sinusoidal flow conditions give heat-transfer factors that are lower than under steady flow. Finally, the more recent paper by Baibikov et al. [21], indicates that for accelerated flow in a rectangular tube, the instantaneous laminar friction factor is initially above and later below the steady-state correlation, but the instantaneous turbulent friction factor is always below the steady-flow value. Presently, steady-flow correlations are used.

The formulas giving friction factors and Stanton numbers have different forms, depending on whether the flow is laminar (Re < 2100), turbulent (Re > 4000), or in the transition region (2100 < Re < 4000). Authors seem to disagree as to the Reynolds number range constituting the transition region. The lower limit is well established around Re = 2000 or 2100, but the upper limit varies, depending on the author. Some authors, for example, Tew ([3], p. 42), use a Reynolds number as high as 10,000 for the beginning of the turbulent region. Others do not have a transition region and make an abrupt jump from laminar to turbulent flow, for example, Martini ([27], p. 120). However, many authors agree that friction factors and heat transfer coefficients are quite unpredictable in the transition region.

For the ANL code, the transition region, 2100 < Re < 4000, has been chosen because the upper limit 4000 is recommended by some of the more recent texts, such as Benedict ([28], pp. 231-133) and Ward-Smith ([29], p. 21). In this region a linear approximation is used resulting in curves of the form shown in Fig. 3, for both f and St.

Due to the small hydraulic diameter in the regenerator matrix of the Stirling engine, the average Reynolds number is always less than 2100 and is therefore in the "laminar" region. Thus, only the laminar portion of the formulas is needed. By comparing the empirical formulas with the experimental data published by various authors, the accuracy of the formulas is estimated to be within 20% for steady flow. However, because of the limited available data, it is difficult to estimate their accuracy for reversing flow. These empirical formulas are believed to provide the correct order of magnitude for friction factors and Stanton numbers.

The subroutine does not correct for the temperature gradient from the fluid to the wall, as discussed in Kays and London ([30], [31]). The Analysis Module makes these corrections as necessary.

2.3.2.1 Friction Factors. The friction factor, f, computed by the subroutine, HTF, is the "Fanning" friction factor defined by the equation



Fig. 3. The Three Flow Regions

$$\Delta P = 4f \frac{L}{D_{\rm H}} \frac{1}{2} \rho U^2, \qquad (3)$$

where

 $\Delta P$  = pressure drop due to friction in a flow passage of length L

and

U = velocity of flow.

The "Fanning" friction factor is a dimensionless quantity and generally is a function of the Reynolds number and  $L/D_{\rm H}$ . If the factor 4f in Eq. 3 is replaced by  $\lambda$ , then  $\lambda$  is called the "Darcy" friction factor. Since the ANL subroutine HTF computes the "Fanning" friction factor, any added correlation that calculates the larger "Darcy" factor must be divided by four.

Flow losses due to friction or area changes within the element are calculated for each type of flow passage shown in Table IV.

TABLE IV. Types of Flow Passages Modeled

Round tubes	Parallel plane + spheres, SLRE matrix
Rectangular tube	Orifice
Screen regenerator matrix	Area contraction coefficient
Packed sphere matrix	

The friction-factor formulas used and references for each of the cases are described below.

#### 2.3.2.1.1 Friction Factor for Round Tubes

Laminar (Re < 2100).

$$f = \begin{cases} 16/\text{Re} & \text{if } \text{Re} < 10\text{L/D}_{\text{H}} \\ 6.137 & \left(\frac{\text{D}_{\text{H}}}{\text{L}}\right)^{0.416} & \text{Re}^{-0.584} & \text{if } \text{Re} > 10\text{L/D}_{\text{H}} \end{cases}$$
(4)

Turbulent (Re > 4000).

$$f = \left[1 + \left(\frac{D_{H}}{L}\right)^{0.5}\right] (0.0014 + 0.025 Re^{-0.32})$$
(5)

Transition (2100 < Re < 4000)

$$f = f_1 + (f_2 - f_1)(Re - 2100)/(4000 - 2100),$$
 (6)

where  $f_1$  and  $f_2$  are the friction factors at Re = 2100 and Re = 4000, respectively, from Eqs. 4 and 5, giving a linear variation between the values of f with Re.

References. laminar: Benedict ([28], p. 256).

turbulent: Benedict ([28], p. 250-251), Kays and London ([30], p. 56), Kreith ([32], p. 433), and Ward-Smith ([29], p. 233).

<u>Remarks</u>. The laminar equation has two parts. The first part of the laminar solution is the classical Hagen-Poiseuille formula. The second part is an approximation to the Langhaar equation for Re >  $10L/D_{\rm H}$ . A third part would have been added, valid for Re >  $1000L/D_{\rm H}$ , except that Re is not expected to be in this region since the tubes where most of the frictional loss occurs generally satisfy  $L/D_{\rm H}$  > 2, which implies that  $1000L/D_{\rm H}$  > 2000 or a Reynolds number in the transition region. In this third part Benedict [28] recommends using the Kline-Shapiro equation:

$$f = 3.435 (Re L/D_H)^{-0.5}$$
.

The turbulent equation (Eq. 5) has two factors. The first factor of Eq. 5 accounts for entrance effects. It was obtained as an approximation of the entrance effects shown on the curves in Kays and London ([30], p. 56) and was found to be in good agreement with entrance-effect factors in the other references. The second factor is the Drew et al. formula, which, according to Benedict ([28], pp. 250-251), is in excellent agreement with Prandtl's equation for  $4000 < \text{Re} < 3 \times 10^{5}$  and is easier to use.

Finally, the transition equation (Eq. 6) is simply the equation of a straight line in the (f, Re) plane. It gives practically the same results as

a straight line in the  $(\log_{10} f, \log_{10} Re)$  plane and is more efficient to calculate. Since usually  $L/D_{\rm H} < 200$  in the Stirling engine tubes, the value Re = 2100 will occur in the Langhaar portion (i.e., the second part) of the laminar formula, Eq. 4, so only that part of the laminar equation is used to compute  $f_1$ .

Laminar (Re ≼ 2100).

$$f = [1.47 - 1.48(a/b) + 0.92(a/b)^2] f_{round},$$
(7)

(8)

where

a/b = ratio of small side to large side of the rectangular cross section of the tube or aspect ratio

and



Turbulent (Re > 4000).

f

$$f = \int f$$
round

<u>Transition</u> (2100 < Re < 4000).  $f = f_1 + (f_2 - f_1) + (Re - 2100)/(4000 - 2100),$ 

where  $f_1$  and  $f_2$  are calculated at Re = 2100 and Re = 4000.

<u>Remarks</u>: The first factor in the laminar formula (Eq. 7) is a quadratic least-squares fit of data in Table C3 of Ward-Smith ([29], p. 180), with an approximation error less than 3%. This multiplier is for fully developed flow, but it is also being used for short tubes due to a lack of data for short tubes.

The multiplier 1 in the turbulent formula (Eq. 8) is from Table C5 of Ward-Smith ([29], p. 184). The above remark about fully developed flow holds here also.

2.3.2.1.3 <u>Friction Factor for Screen Matrix</u>. For any Reynolds number in the regenerator,

$$= 10^{(A \cdot Re^{-0.33})} \cdot B, \qquad (9)$$

where

$$A = \frac{1.33}{p^2} \left( \frac{1-P}{\sigma} \right)^{-0.33},$$
  
B = 10<sup>-0.54/P</sup> · P<sup>3</sup>/[8(1 - P)\sigma<sup>2</sup>],

- P = porosity, void fraction, of the regenerator matrix.
- s = ratio of minimum free flow area over frontal area for the matrix.

References. Tong ([33], pp. 32, 64, 80)

<u>Remarks</u>. The ratio  $\sigma$  in Eq. 9 can be computed for a square weave mesh from the formula

$$\sigma = (1 - Md)^2$$

where

M = mesh number (number of wires per unit length)

and

d = wire diameter.

Finally, note that data from which Eq. 9 is derived were taken at Re < 1000 and the relation is not valid for Re > 1000. However, due to the small hydraulic diameter, Reynolds numbers in the regenerator are not likely to exceed this range.

2.3.2.1.4 Friction Factor for Packed Sphere Matrix

$$f = \begin{cases} 24.92 \text{Re}^{-0.698} & \text{if } \text{Re} < 100 \\ 5.12 \text{Re}^{-0.347} & \text{if } \text{Re} > 100. \end{cases}$$
(10)

References. Kays and London ([30], pp. 86,123).

<u>Remarks</u>. This formula was obtained by forming linear least-square fits to the data in the above reference.

#### 2.3.2.1.5 Friction Factor for Metnet Matrix

$$4f = A(y)[1 + 10.38/Re(d)](D_{H}/d)$$
(11)

where

and

$$D_{\mu}/d$$
 = ratio of  $D_{\mu}$  to d; Ref. Eq. 9

hydraulic diameter,

References. General Motors [34, Sec. 6.006]

<u>Remarks</u>. This correlation formula (Eq. 11) was obtained from GM for the low-cost nickel base regenerator material, Metnet. The GM formula used the "Darcy" friction factor, and so the formula was divided by 4 to obtain the "Fanning" factor. Also, the GM formula used a Reynolds number based on their unique fiber diameter, d. If a Metnet with a different fiber diameter is used, then the value of d (DIAM in the code) should be changed in subroutine HTF, provided one agrees that the GM correlation is still valid for a range of fiber sizes. The "filler factor," denoted by y in Eq. 11, is defined to be the fraction of the Metnet matrix volume that is filled with metal. The fibers are hollow, so that the porosity p, which is the fraction of the volume that the working gas can fill, is not quite equal to 1 - y, but instead P < 1 - y. However, the friction routine assumes that in the case of Metnet, the user has input 1 - y for the porosity.

#### 2.3.2.1.6 Friction Factor for SLRE Matrix

f = friction factor for rectangular tubes. (12)

References. Hoehn et al. [35]

<u>Remarks</u>. This type of regenerator matrix was used by Jet Propulsion Labs (JPL), for the tests described in the above reference. The matrix is a corrugated sheet rolled into a spiral in which the flow passages approximate parallel infinite planes. On both ends of the spiral device an array of small balls were placed. This entire matrix was then tested at JPL. The results correlated well with rectangular tube data with a constant multiplier. In this case the subroutine simply uses the rectangular tube formulas (Eqs. 7 and 8) with aspect ratio a/b = 0.

References. Ward-Smith ([29], pp. 306-434)

<u>Remarks</u>. In case the engine cell numbered ICELL has an orifice, it is assumed that the user has supplied the orifice coefficient with the input data, and that the coefficient is stored in the array ORIFCE.

The orifice coefficient, f, gives the pressure loss  $\Delta P$  through the orifice, by means of the equation

 $\Delta P = f \cdot \frac{1}{2} \rho U^2,$ 

where

 $\rho$  = gas density

and

U = velocity of the gas entering the orifice.

2.3.2.1.8 Loss Factor for Area Contraction and Expansion. The area contraction and expansion coefficients are for calculated nonrecoverable pressure loss due to the flow from a larger flow area into a smaller flow area or vice versa, as in Fig. 4.

Both the contraction and expansion formulas above were taken from the "NASA" code by Tew et al. [3]. These formulas, in turn, agree with intermediate curves shown in Kays and London ([30], Fig. 18, p. 45). Note that the cutoff Reynolds number 3000 in the above contraction and expansion correlations is roughly the midpoint of the transition range 2100 < Re < 4000.

The nonrecoverable pressure loss  $\Delta P$  due to flow-area contraction or expansion is obtained from



Fig. 4. Contraction and Expansion

where

 $\Delta P = f \cdot \frac{1}{2} \rho U^2,$ 

 $\rho$  = gas density

and

U = velocity of the gas in the <u>smaller</u> of the two flow areas.

Contraction

$$f = K_{C} = \begin{cases} 1 - 0.4A & \text{if } Re \leq 3000 \\ 0.5 - 0.4A & \text{if } Re > 3000. \end{cases}$$
(14)

Expansion

$$f = K_E = \begin{cases} 1 - 2.6A + 1.005A^2 & \text{if } \text{Re} \leq 3000 \\ 1 - 2.0928A + 0.996A^2 & \text{if } \text{Re} > 3000, \end{cases}$$
(15)

where

A = quotient of flow areas, smaller over larger.

References. Tew et al. [3]; Kays and London [30].

2.3.2.2 <u>Heat-transfer Coefficients</u>. The Stanton number, St, is calculated for each of the following types of flow passage:

- Round tubes
- Rectangular tubes
- Screen regenerator matrix
- Packed sphere matrix
- Metnet matrix
- Corrugated spiral, SLRE-type, matrix

In most cases, correlation formulas from the literature were used to obtain the "Colburn factor"  $j = St \cdot Pr^{2/3}$ , from which St is easily found. The subroutine includes an Input Option defining j = f/2, the Colburn Analogy, to provide correspondence with other analysis techniques (e.g., Urieli [2]).

2.3.2.2.1 Heat-transfer Coefficient for Round Tubes

Laminar (Re < 2100).

St = 
$$1.86 \text{Re}^{-2/3} (D_{\text{H}}/\text{L})^{1/3} \text{Pr}^{-2/3}$$
. (16)

Turbulent (Re > 4000).

St = 
$$0.036 \text{Re}^{-0.2} (D_{\text{H}}/\text{L})^{1/18} \text{Pr}^{-2/3}$$
. (17)

Transition (2100 < Re < 4000).

St is linearly interpolated between Re = 2100 and 4000.

References. Chapman ([36], p. 338); Jacob ([37], pp. 544-547).

<u>Remarks</u>. Among several correlations discussed by Chapman, these were recommended as being the best.

2.3.2.2.2 Heat-transfer Coefficient for Rectangular Tubes

<u>Laminar</u> (Re < 2100).

 $St = j \cdot Pr^{-2/3}$ ,

where

 $j = C \cdot f_{rect}$ 

f<sub>rect</sub> = the friction factor for rectangular tubes

$$C = 0.25 + 0.09 \left(1 - \frac{a}{b}\right)^2 + 3.2 \left(\frac{D_H/L}{1 + .3D_H/L}\right) \frac{3}{b}$$
(18)

a/b = "aspect" ratio.

Turbulent (Re  $\geq$  4000).

$$St = j \cdot Pr^{/2/3}$$
, (19)

where

 $j = 0.44f_{rect}$ 

and

 $f_{rect}$  = the fliction factor for rectangular tubes.

<u>Transition</u> (2100 < Re < 4000).

St is linearly interpolated between Re = 2100 and 4000.

References. Kays and London ([30], pp. 56-59).

<u>Remarks</u>. Both the laminar and turbulent correlations were obtained by trial and error from the curves in Figs. 30-32 of the above reference. In the laminar case, the multiplier C calculated in Eq. 18 agrees with the corresponding values taken from the Kays-London curves to within about 5%. In the turbulent case, the multiplier 0.44 in Eq. 19 compares with the values 0.41-0.47 taken from the Kays-London curves. The Kays-London curves have a wider transition region than is being used here, and so in the transition region, these correlations may not agree as well.

#### 2.3.2.2.3 Heat-transfer Coefficient for Screen Matrix. For all Re,

St = 
$$\phi(P) \cdot \operatorname{Re}^{-\mathbf{m}(P)} \cdot (Pr)^{-1}$$
, (20)

where

$$P = porosity,$$
  
m(P) = 0.43P + 0.15,

and

$$\phi(\mathbf{P}) = \begin{cases} \mathbf{P}/2 & \text{if } \mathbf{P} < 0.39 \\ 1.54 - 6.36\mathbf{P} + 7.56\mathbf{P}^2 & \text{if } 0.39 < \mathbf{P} < 1. \end{cases}$$

References. Coppage and London [38].

<u>Remarks</u>. The equations for m(P) and  $\phi(P)$  were obtained from curves given in the above reference.

2.3.2.2.4 Heat-transfer Coefficient for Packed Sphere Matrix. For all Re,  
St = 
$$0.21 \text{Re}^{-0.31} (\text{Pr})^{-1}$$
 (21)

References. Kays and London ([30], p. 123); Coppage and London [38].

<u>Remarks</u>. This correlation is for random packed spheres with a porosity of .39.

$$St = C_{\Lambda} \cdot D_{H}/(4d), \qquad (22)$$

where

$$C_{\Lambda} = \begin{cases} P_{0} - P_{1} \cdot \text{Re}(d) + [\text{Re}(d) + 15]^{-1.105} & \text{if Re}(d) < 30 \\ \\ C_{\Lambda}(30) \left(\frac{\text{Re}(d)}{30}\right)^{-0.279} & \text{if Re}(d) > 30, \end{cases}$$

$$Re(d) = Re \cdot d/D_{H},$$

$$P_{o} = -0.0153 + 1.5745y - 2.865y^{2},$$

$$P_{1} = 0.000292 + 0.003945y + 00835y^{2},$$

$$y = "filler factor,"$$

$$C_{\Lambda}(30) = P_{o} - 0.30 P_{1} + 0.011$$

#### References. General Motors [34].

<u>Remarks</u>. See also the remarks for the Metnet friction factor in Sec. 2.3.2.1.5. The GM correlation was based on wire diameter and has been converted here to hydraulic diameter. GM called the variable  $C_{\Lambda}$  the "heat-transfer factor," and according to [34], Sec. 6.006, pp. 9 and 44,

$$C_{\Lambda} = \frac{d}{L} \begin{bmatrix} h & A_{s} \\ \hline m & C_{p} \end{bmatrix},$$

where

h = average convective heat-transfer coefficient for surface of regenerator material

and

 $A_{s}$  = wetted surface area of regenerator material.

To convert  $C_A$  to Stanton number St, the definition of Stanton number is used:

$$St = h/(C_p \rho U) = h A_F/(C_p m),$$

where

 $A_{\rm F}$  = free-flow area.

After rearranging, one has

St = 
$$\frac{h}{C} \frac{A}{m} \frac{d}{L} \frac{A}{K} \frac{F}{d}$$
  
=  $C_{\Lambda} \frac{D}{4L} \frac{H}{d}$ , which is Eq. 22.

It should also be remarked that the formula for  $C_{\Lambda}$  in Eq. 22, as was given in the GM report, had only the first part, namely,  $C_{\Lambda} = P_0 - P_1 \cdot \text{Re}(d) + [\text{Re}(d) + 15]^{-1 \cdot 185}$ , which was used for all Reynolds numbers. However, this formula gives negative heat-transfer factors for some Reynolds numbers that might occur in the regenerator. For example, when the filler factor is y = 0.3, then  $C_{\Lambda}$  is negative when Re > 163 [or Re(d) > 92], using the original GM correlation. For this reason, in the range Re(d) > 30, the GM correlation was replaced by a straight line in the log-log plane.

#### 2.3.2.2.6 Heat-transfer Coefficient for SLRE Matrix

St = Stanton number for rectangular tubes with the (23) aspect ratio input by user

References. Hoehn et al. [35].

<u>Remarks</u>. See the remarks for the friction factor for this type of matrix in Sec. 2.3.2.1.6.

2.3.2.3 <u>Implementation of Subroutine HTF</u>. Many of the factors and terms in the preceding correlations are constant throughout the cycle of the engine for a given cell. For example,  $D_{\rm H}/L$ , A, and B in Eq. 9, the polynomials in y for the Metnet correlations, and several others need be computed only once for a given cell. Therefore, subroutine HTF has two entry points: an initialization entry and a main entry.

The first call to the subroutine is from subroutine RIOSIN and is of the form

CALL HTF(ICELL,DUMMY,DUMMY,DUMMY,DUMMY) where ICELL is any value less than 1 and DUMMY is a dummy variable.

At this time, the subroutine calculates constant information for each cell, such as the length L of the passage containing the cell,  $D_{\rm H}/L$  for the cell, and others. This information is initialized and stored in a container array.

Subsequently, when the Analysis Module needs the value of a heat-transfer coefficient or a friction factor other than a contraction or expansion coefficient, the following call is made:

CALL HTF(ICELL, RE, PR, F, ST),

where

ICELL = the cell number, from 1 to 30, for which the friction and heat-transfer coefficient are needed, RE = Reynolds number based on hydraulic diameter, and

PR = Prandtl number.

The subroutine then returns the friction factor (or orifice coefficient) F and Stanton number ST for cell number ICELL.

To obtain an area contraction coefficient, a statement of the form

CALL HTF(108, RE, AR, F, ST)

is used where,

AR = flow-area ratio, smallest over largest.

The subroutine then returns the contraction coefficient as F and also returns St = 0.

An area <u>expansion coefficient</u> is obtained in the same way except that 109 is the first argument:

```
CALL HTF(109, RE, AR, F, ST).
```

The subroutine then returns similar values.

When  $1 \leq \text{ICELL} \leq 30$ , the subroutine determines the type of flow passage from the common array value MTYPE(ICELL), which is an input value described in Appendix A. To introduce a new type of flow passage into this subroutine, the user must: (a) input a different value for MTYPE, (b) change the array IT in the DATA statement of subroutine HTF to transfer logical control, and (c) introduce coding for the additional correlation formulas in subroutine HTF.

2.3.3 <u>Volume Subroutine</u>. Subroutine VOLUME performs two major tasks for a variety of engine designs and drives:

- (1) It provides minimum and maximum piston positions, strokes, phase angle, and the crank angle at which the compression volume is minimum. It also calculates the compression displacement when the design is a displacer type.
- (2) It calculates the volumes in the expansion and compression spaces and their rates of change with respect to time for a given crank angle.

The subroutine performs these calculations for three different designs: <u>in-line</u>, <u>double-acting</u>, and <u>displacer</u>, which are shown in Appendix A, Figs. <u>A-2</u>, A-3, and A-4, respectively. Two drive types may be specified: <u>connecting-rod drive</u> and <u>rhombic drive</u>, which are illustrated schematically in Figs. 5 and 6.

In these figures, the following notation is used:

- r = crank radius,
- L = connecting-rod length,
- e = eccentricity,

and

α = variable crank angle, measured from a line parallel to the piston axis (radians) with piston at T.D.C.

A double-acting design is treated as a variation of an in-line design. It is assumed, in the double-acting case, that the user has input an appropriate value of the volume phase angle or an equivalent crank phase angle. The motion can then be considered equivalent to that of an in-line design with the compression space in back of the compression piston. In some double-acting cases this equivalence is not exact, but a reasonable approximation of the actual motion is obtained if the correct volume phase angle is input.

For a rhombic drive, the two connecting rods are of the same length as shown in Fig. 6. This is equivalent to the drive in Fig. 7 where the two crank angles in the latter figure are constrained to be the same. The desired volumes and derivatives can be calculated from these figures.

The piston position x is given by

 $g(\alpha) = (L^2 - (e - r \sin \alpha)^2)^{1/2}$ 

x

where

$$= \mathbf{r} \cos \alpha + \mathbf{g}(\alpha), \qquad (24)$$



Fig. 5. Drive Type O Connecting-Rod Drive



Fig. 6. Drive Type 1 Rhombic Drive



Fig. 7. Equivalent to Rhombic Drive

For the rhombic drive in Figs. 6 or 7, the position of the expansion piston is given by

$$\mathbf{x}_{E, \text{ rhombic}} = \mathbf{r} \cos \alpha - \mathbf{g}(\alpha). \tag{25}$$

The function g is evaluated by means of an arithmetic statement function in subroutine VOLUME.

In the nonrhombic drive cases, the Subroutine VOLUME does not require identical r, L, and e for the compression and expansion pistons. The expansion and compression crank angles,  $a_E$  and  $a_C$ , are constrained to differ by a constant,  $\phi_{crank}$ , so that

$$\alpha_{\rm E} = \alpha_{\rm C} + \phi_{\rm crank}, \tag{26}$$

where

The piston velocities (except for the expansion piston of the rhombic drive) can be obtained by differentiating Eq. 24 with respect to time t:

where

$$dx/dt = [-r \sin \alpha + g'(\alpha)](d\alpha/dt)$$
(27)  
$$g'(\alpha) = r(\cos \alpha)(e - r \sin \alpha)/g(\alpha).$$

.....

In Eq. 27 the sign in front of  $g'(\alpha)$  must be reversed for the expansion piston of the phombic drive.

Given the parameters r, L, and e for both the compression and expansion pistons, as well as  $\phi_{\rm crank}$ ,  $\alpha$ , and  $d\alpha/dt$ , the compression and expansion space volumes, and their derivatives are calculated using the preceding equations.

2.3.3.1 Initial Calculations. Since most Stirling engine codes begin the computation cycle at the point where the compression space volume is minimum, subroutine VOLUME calculates the compression crank angle at which this minimum occurs. If the engine design is "in-line," this minimum occurs when the compression piston position is maximum, i.e., at a compression crank angle  $\alpha_{\rm C} = \psi$  such that

$$\sin \psi = e_C / (r_C + L_C). \qquad (28)$$

However, when the engine design is a "displacer type," the compression space is between the two pistons. The change in compression-space displacement is then a function of the motion of both pistons, which are in turn separated by a phase angle. In this case, an iterative scheme is required to find the minimizing angle  $\alpha_{\rm C} = \psi$ . The expression to be minimized is the volume of the compression space.

For a "connecting-rod-type" drive, this volume is

$$S(\alpha) = AF_E \cdot x_E - AF_C \cdot x_C + \text{ constant}$$
(29)  
=  $AF_E[r_E\cos(\alpha + \phi_{crank}) + g_E(\alpha + \phi_{crank})]$   
-  $AF_C[r_C\cos\alpha + g_C(\alpha)] + \text{ constant},$ 

where A is the cross-sectional area of the cylinders, and the constant term accounts for unswept volume and where the subscripts E and C mean that expansion and compression values for e, r, L are to be used, respectively. The variable angle,  $\alpha$ , is found by solving S'( $\alpha$ ) = 0, numerically using a "bisection" method, i.e., the root  $\alpha = \psi$  is bracketed into successively smaller intervals.

From Eqs. 24 and 25, the distance between the piston positions for the rhombic drive case is

$$S_{\text{rhombic}}(\alpha) = \text{constant} - 2g(\alpha).$$
 (30)

In this case, the minimizing angle,  $\alpha = \psi$ , is easily found to be

$$\psi = \frac{\pi/2 \text{ if } e > r}{\operatorname{arcsin}(e/r) \text{ if } e < r.}$$

Note that Eq. 30 also implies that  $S_{rhombic}$  is maximum when  $g(\alpha)$  is minimum, i.e., when  $\alpha = 1.5\pi$ . The compression displacement volume, therefore, is given by

compression displacement = 
$$2[g(\psi) - g(1.5\pi)]$$
(piston area).

The input subroutine allows the user to specify either the crank phase angle,  $\phi_{crank}$ , or the volume phase angle,  $\phi_{vol}$ . The crank phase angle is the difference between the crank angles at which the expansion and compression pistons are at top dead center, as shown in Fig. 8:

$$\phi_{\text{crank}} = \alpha_{\text{E}} - \alpha_{\text{C}}$$

The volume phase angle,  $\phi_{vol}$ , is the angle at which the expansion volume minimum precedes the compression volume minimum at top dead center, as shown in Fig. 9. These phase angles are related by the equation

$$\phi_{\rm crank} = \phi_{\rm vol} - \psi + \alpha_{\rm E,min}, \tag{31}$$

where

and

$$\psi$$
 = the compression crank angle  $\alpha_{\rm C}$  at which V<sub>C</sub> is minimum  
 $\alpha_{\rm E,min}$  = the expansion crank angle  $\alpha_{\rm E}$  at which V<sub>E</sub> is minimum  
= arcsin ( $e_{\rm E}/(L_{\rm E} + r_{\rm E})$ ).

If the user specifies  $\phi_{vol}$  but not  $\phi_{crank}$ , then the volumes subroutine calculates  $\phi_{crank}$ . However, in an engine with a displacer design and a connecting-rod drive, inspection of Eqs. 29 and 31 reveals that  $\phi_{crank}$  and  $\psi$  are both unknowns. Thus, in this situation the subroutine numerically solves Eqs. 31 and S'( $\alpha$ ) = 0 simultaneously to find  $\phi_{crank}$  and  $\psi$ .

2.3.3.2 <u>Implementation of Subroutine VOLUME</u>. The first call to subroutine VOLUME is from subroutine INITAL and is of the form

The subroutine then calculates various values needed for later calls, such as maximum and minimum piston positions, strokes,  $\psi$ ,  $\phi_{crank}$ , or  $\phi_{vol}$ . See Appendix C for definitions of the corresponding Fortran variable names. These variables are in common block VARVOL.

If the engine design is a displacer-type, a second call to the volumes subroutine is made by EDINPT and by RIOSIN and is of the form

CALL VOLUME(3, DUMMY).

The subroutine then computes the compression volume displacement for the convenience of the user, i.e., the portion of the compression volume swept by the pistons. This calculation is used to provide a normalizing volume for the Analysis Module.

All subsequent calls are of the form

CALL VOLUME(1, DUMMY).

The subroutine then calculates the following values, which are variables in common block VARVOL:

VOLS(2) = the portion of the swept compression volume behind the expansion piston in the case of an engine with a displacer design, otherwise


Fig. 8. Crank Phase Angle,  $\phi_{crank}$ 



Fig. 9. Volume Phase Angle,  $\phi_{vol}$ 

DVOLDT(I), (I = 1,2,3,4,5) = the rate of change of each of the above five volumes with respect to time.

Thus, after the above CALL statement, the active expansion volume is VOLS(1) and the active compression volume is VOLS(2) + VOLS(3).

2.3.3.3 <u>Free-Piston Volume Variation</u>. In order that a thermodynamic analysis of free-piston Stirling engines be performed, the motion of the pistons must be specified. Harmonic motion of fixed frequency and phase can easily be specified by requiring the pistons to behave as though they are connected by any of the mechanical drive systems described in Sec. 2.3.3. An alternative is that the user provide his own volume-variation routine that either prescribes piston motion or calculates piston motion from the dynamics of the system.

2.3.4 <u>Additional Losses Subroutine</u>. This subroutine calculates several energy losses that need to be calculated at the end of a cycle. In the present version of the code, SEAMI, these extra losses are regarded as additional heat loads that must enter into the heater and, in some cases, must exit through the cooler.

The following loss calculations  $\ensuremath{\mathsf{pr}}\xspace$  shown in Table V.

TABLE V. Engine Loss Mechanisms Modeled

Dynamic Piston Motion Axial Conduction along: Piston walls Cylinder walls Regenerator walls Regenerator filler.

Each of the above losses is discussed below.

2.3.4.1 <u>Dynamic Piston Motion Losses - QDYNAMIC</u>. These losses are related to the dynamic motion of the displacer piston in the expansion zone. The loss is considered to flow from the expansion to the cylinder walls and then to the cooling water. In an in-line design this loss does not exist. The code breaks the loss into two components: shuttle and gap. 2.3.4.1.1 <u>Shuttle Conduction Loss</u>. Shuttle conduction takes place when the expansion piston absorbs heat at the hot end of a stroke and releases it at the cold end of the stroke. The present formula used by the Losses Subroutine for the shuttle loss assumes sinusoidal piston motion, a linear and constant longitudinal temperature distribution, and no axial piston conduction. It was derived by Rios ([1], pp. 129-135), and is

$$Q_{\text{shuttle}} = \frac{\pi}{8} \frac{D}{g} \frac{S}{L} \left[ \frac{2\lambda_1^2 - \lambda_1}{2\lambda_1^2 - 1} \right] (k_g \text{ S}\Delta T), \qquad (32)$$

where

 $\begin{array}{l} \lambda_1 = (k_p/k_g) \, \sqrt{\omega g^2/(2\alpha_p)}, \\ D = \text{piston diameter}, \\ S = \text{piston stroke}, \\ \Delta T = \text{temperature change from hot to cold end of piston,} \\ L = "shuttle length," usually the distance from piston face to seal or the displacer stroke; see Rios ({1}, p. 135); \\ g = width cf "gap" between piston and cylinder, \\ k_p,k_g = \text{piston and gas conductivities}, \\ \alpha_p = \text{diffusivity of piston wall metal}, \\ \omega = \text{frequency}, \end{array}$ 

and

Q<sub>shuttle</sub> has units of watts.

2.3.4.1.2 Gap Loss. This loss, also known as the "appendix" or "pumping" loss, occurs in displacer piston engines. The radial gap between the displacer piston and the cylinder is assumed to be sealed at the cold end. Pressurization and depressurization of the gas cause the gas to flow into and out of the gap. The gas loses heat while it is at the cold end of the gap and must be reheated once it leaves the gap at the warm end. To estimate this loss, the Losses Subroutine uses a formula originally developed by Rios ([1], pp. 136-138) for a refrigerator and later modified by Martini ([27], Appendix D) to apply to a heat engine. The modification was necessary because, in a refrigerator the maximum gap pressure and minimum gap temperature occur simultaneously, while in a heat engine both gap pressure and gap temperature reach a maximum simultaneously. With Martini's modification, the Rios formula for gap loss in watts is

$$Q_{gap} = \left| \frac{\gamma}{\gamma - 1} \frac{y}{2} V_{gap} \sin \phi \cdot \left[ P_{min} / (x - y) - P_{max} / (x + y) \right] \omega \right|$$
(33)

where

$$x = (T_E + T_K)/(T_E - T_K)$$

y = S/L,

and other notations are as defined in Eq.32 and in the nomenclature.

In developing this formula, sinusoidal voluma, pressure, temperature, and mass variations were assumed.

2.3.4.1.3 <u>Total Dynamic Piston Motion Losses</u>. The total dynamic piston motion loss is the sum of the shuttle and gap losses, or

$$Q_{\rm dynamic} = Q_{\rm shuttle} + Q_{\rm gap}$$
 (34)

2.3.4.2 <u>Axial Conduction Losses</u>. Each of these conduction losses is computed by means of the simple linear conduction formula,

$$Q = k \cdot AX(\Delta T/L), \tag{35}$$

where

k = thermal conductivity evaluated at T<sub>mean</sub>, AX = cross-sectional area, L = conduction length,

and

 $\Delta T$  = temperature difference.

In the case of conduction through the regenerator filler material, allowance is made for the nonsolid conduction path by multiplying the right side of Eq. 35 by a factor named FUDGE, which is defined as

> $1 - \sigma$ , for tube matrices FUDGE = 0.05(1 -  $\sigma$ ), for screens or spheres 0.5(1 -  $\sigma$ ), for Metnet.

The last two factors were approximated based on the contact between different layers of the matrix.

2.3.4.3 <u>Implementation of the Losses Subroutine</u>. The Losses Subroutine is called by the Analysis Module with the Fortran statement

CALL LOSSES.

All information needed by the subroutine is stored in common blocks. These losses are returned as the following Fortran variables:

QEXPSH = shuttle loss QEXPGP = gap loss QDYNAM = shuttle + gap losses QPISWL = conduction along expansion piston wall QCYLWL = conduction along expansion cylinder wall QREGWL = conduction along regenerator wall QREGFL = conduction along regenerator filler QSTATC = the sum of the above four conduction losses. When returned, each of these losses has already been multiplied by the total number of cylinders (NCYL) and has units of watts.

2.3.4.4 <u>Future Additions to the Losses Subroutine</u>. The following changes or additional losses are being considered for future inclusion in this routine:

- (1) Revised shuttle and pumping formulas will be added after investigating the recent literature on the subject.
- (2) Radiation losses through the displacer or hot cap will be added.
- (3) Power losses due to gas leakage will be added. This includes leakage between expansion and compression spaces as well as between these spaces and the appropriate buffer spaces.
- (4) Power losses due to ring friction will be added.
- (5) Hysteresis losses in the expansion, compression, and buffer spaces will be added. This loss, called the "cyclic heat transfer loss" by Toscano et al. ([39], p. 56), is the result of periodic heating and cooling of the gas near the gas-wall interface inside the cylinders and other spaces. The effect is a decrease in the maximum pressure and an increase in the minimum pressure of the working gas, resulting in a loss of power.

2.3.5 Engine Constraints and Optimization. The present code is capable of predicting engine performance over a wide range of temperatures, pressures, and frequencies. Not all of these results are meaningful because the code does not address:

> Mechanical friction Alternator inefficiencies Combustion inefficiencies Auxiliary power needs for cooling, etc.

These losses do not affect the thermodynamic engine performance, but are of major importance in determining the overall performance of the system. Indeed, high thermodynamic efficiency can be calculated for conditions in which the mechanical losses are so large that the engine cannot operate. The above effects must be included so that overall performance be calculated and should be included as engine constraints.

When engines are subjected to the pressures and temperatures predicted by a Stirling engine code, stresses occur that may be near or beyond the limits of the engine materials. Whether these material limits are approached or exceeded with the engine and conditions being modeled would establish additional constraints on the engine parameters. These additional constraints could be used along with an optimization routine to give optimal design values.

#### 2.4 ANALYSIS MODULE (GENERIC)

The general features of the Analysis Module for the ANL System are discussed in this section. The first such Analysis Module, SEAMI, prepared for the ANL System is described in Chapter 3.

2.4.1 <u>Tasks of the Analysis Module</u>. The following are the major tasks and characteristics of the Analysis Module:

- The Analysis Module solves the field equations describing the mass and energy flows in the engine. It predicts temperatures, pressures, and other parameters that determine the state of the engine during each cycle. These calcultions are continued for successive cycles until steady-state (periodic) conditions are reached (defined as conditions being repeated from one cycle to the next within a specified convergence criterion).
- The Analysis Module calls the Losses Subroutine for additional losses due to conduction, radiation, leakage, etc., and obtains net performance characteristics such as power and efficiency.
- The Analysis Module uses the three other modules of the ANL Stirling Engine Analysis System: Input, Special Functions, and Output. It must therefore be applicable to a large variety of engines and operating conditions.
- The Analysis Module must use a solution method that converges quickly and provides meaningful results.

# 2.5 OUTPUT MODULE

2.5.1 <u>Tasks of the Output Module</u>. The Output Module writes in an easyto-read format the answers to various questions that Stirling engine designers may have regarding a specific engine or type of engine. It also answers questions about the analysis code itself. Some specific answers are:

- The values of certain performance characteristics, such as power, efficiency, energy losses, energy flows, etc., for an engine under specified operating conditions.
- How these performance characteristics vary when the operating conditions are varied.
- How engine conditions, such as pressures, temperatures, and velocities, vary throughout a complete cycle (crankshaft revolution) of the engine.
- How the conditions vary from one end of the engine to the other end.
- The speed of the code's iterative technique used to find a cyclic steady-state solution.
- How accurate the code's solution is after it converges.

The Output Subroutine OUT1, has been designed to work with any analysis module and writes the results of the computation in several ways to answer the above questions. The arrangement of the output data is controlled by several input parameters which are outlined below.

2.5.2 <u>Controlling Output with Input</u>. The form of the output is controlled by the three input variables NPRT1, NPRT2, and IGRAPH, which control the writing of:

> Engine zone-by-zone information (NPRT1) Cycle-to-cycle or case-to-case comparison information (NPRT2) Graphics data (IGRAPH).

The uses of these three parameters are described as follows:

- (1) NPRT1 = the number of computational time steps between prints of engine zone-by-zone information. The current Analysis Module, SEAM1, requires NPRT1 to be a multiple of the number of steps in a cycle, NSTEP.
- (2) NPRT2 = 1 directs the Output Subroutine to write cycle-tocycle convergence information.

NPRT2 > 1 directs the Output Subroutine to write case-to-case comparison information for NPRT2 cases at a time. The term case refers to a running of the code for a specific engine and specific operating conditions. For example, if a perturbation study is run having two pressures each with five frequencies, the case results may be separated into two pressure groups by setting NPRT2 = 5.

(3) IGRAPH = 0 results in no graphics data being written.

IGRAPH = 1 is a directive to write curve data (such as P-V data) at  $5^{\circ}$  intervals. This data is saved for the last cycle of each case.

IGRAPH = 2 signals that graphics data are to be saved for case-to-case comparisons. This option is designed for perturbation runs in which the user wants curves that show the variations in performance parameters.

The Output Subroutine writes all output on unit 6, except for graphics output, which is written on unit 8.

2.5.3 <u>Filling the Output Arrays</u>. The information in this section is for use by those wishing to replace the current analysis module, SEAMI, with another analysis module.

The Output subroutine, OUT1, writes values from the three arrays given below. (Dimensions are included in parentheses.)

SCALR(50,10) VECTR(15,30) GRAFIC(10,75). These arrays are in a COMMON block and must be filled by the analysis module of the code before OUTl is called. The arrays have indices (I and K). The second index, K, indicates variation in time for GRAFIC, cycle number for SCALR when NPRT2 = 1, or case number when NPRT2 > 1, and engine zone for VECTR (see Appendix A). The first index, I, identifies the type of information that is being stored. For example,

SCALR(1,K) SCALR(2,K)	= average engine pressure (MPa) = engine speed (RPM)
etc.	:
VECTR(1,K)	= maximum gas temperature in zone K (K)
VECTR(2,K)	= average gas temperature in zone K (K)
etc.	:
GRAFIC(1,K	) = Kth compression crank angle (rad.) at 5° increments
GRAFIC(2,K	) = live expansion volume at Kth angle (cm <sup>3</sup> )
etc.	:
	:

For definitions of the other information identifiers for each array, see code variable definitions (Appendix C), the actual code listing comments, and the output edit (Appendix B).

The Analysis Module fills each of the above three arrays during or after the appropriate computational cycles, as directed by the input parameters, NPRT1, NPRT2, and IGRAPH.

For the array SCALR(I,K), if NPRT2 = 1, then K represents the cycle number. But if NPRT2 > 1, then K represents the case number. The Analysis Module distinguishes between these two situations as follows:

- If NPRT2 = 1, fill array SCALR(I,K) (for I = 1,...,50) at the end of each cycle, where K = the cycle number, NCYCLE; however, when NCYCLE passes 10, K will start over at 1 after editing the last 10 cycles. For example, if NCYCLE = 13 then K = 3, and if NCYCLE = 30 then K = 10. (A Fortran statement for this is K = MOD(NCYCLE - 1,10) + 1.)
- If NPRT2 > 1, do as above except let K = 10 each time. In this situation, the Output routine will properly rearrange the information in the array SCALR for successive cases.

The zone-by-zone array, VECTR(I,K), and the graphics array, GRAFIC(I,K), can be filled at the end of each Analysis Module cycle, and results editted as specified by the user.

The subroutine of SEAM1 that fills the arrays SCALR and VECTR is called RIOSPR. For SEAM1, the number of engine zones for which information is stored in array VECTR is set to 5 in RIOSPR.

2.5.4 <u>Calling the Output Subroutine</u>. Assuming that the three output arrays SCALR, VECTR, and GRAFIC have been filled, the computations have been completed, and the convergence criterion has been checked, the Output Subroutine is called after each cycle, as follows:

CALL OUT1(NCASE, IGONOW)

where

NCASE = the case number

and

IGONOW = 0 if convergence has occurred 1, if convergence has not occurred.

The subroutine OUT1 will then use NPRT2, IGRAPH, and the other variables stored in COMMON blocks to automatically:

- Write zone-by-zone information every NPRI cycles.
- Save cycle-to-cycle or case-to-case comparison information in array SCALR if IGONOW = 1.
- Write or save array SCALR in the appropriate way if IGONOW = 0.
- Write or save graphics data, if requested, and IGONOW = 0. The graphics data are written from the array GRAFIC if IGRAPH = 1, or from part of the array SCALR if IGRAPH = 2.

Basically, IGONOW = 1 directs OUT1 to write transient engine data, and IGONOW = 0 directs OUT1 to write summary information for the case or perturbation study.

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# 3. SEAM1 (STIRLING ENGINE ANALYSIS MODULE 1)

#### 3.1 BACKGROUND

3.1.1 <u>Rios Analysis</u>. The original code, which provides the basis for the Analysis Module, was developed in 1969 by Rios [1] as part of his D.Sc. thesis at Massachusetts Institute of Technology. His work was a continuation of previous work by Rea and Smith [40] and Qvale and Smith [41], [42], [43] on Stirling-cycle analysis. The original code was designed for a refrigerator of the two-piston, two-cylinder configuration, but has since been modified for a heat engine.

Rios' objective for his code was that it be more generally applicable than previously developed codes. Rios' model is one in which the power output and heat input of the basic cycle are calculated first without losses. These total cycle results are then modified with energy losses typical of a real engine. Numerous other codes have been written since his, some of which give more detailed evaluation of newer, more complex Stirling engine designs. Examples are Urieli [2], Tew et al. [3], and Schock [4]. Such codes divide the engine into many small control volumes, and the basic governing differential equations of fluid mechanics applied to each volume are solved. Although these methods provide detailed information on engine performance, interrelate the losses with each other, and also solve the basic power output, the resulting system of equations is large and requires extensive computer time to reach a stable solution. Therefore, a simpler model such as Rios', is better suited for a first analysis of Stirling engine designs.

#### 3.2 DESCRIPTION OF SEAM1 COMPUTATIONAL PROCEDURES

3.2.1 What the Code Calculates and Predicts. The code calculates the efficiency of the engine based on net power and net heat input. The net heat input is the work performed during a cycle in the expansion space plus heat-loss terms. The net power is defined as the P-V power (the difference between the expansion and compression work done during a cycle calculated by integrating  $\phi p dV$ ) minus the power loss terms. Section 3.2.3 gives the derivation of the analysis used for calculation of expansion and compression work.

Losses that reduce net power are due to two effects. The first is frictional losses of the working fluid as it passes through system components. The second is due to a lowering of the gas temperature in the expansion space and a raising of the temperature in the compression space due to the thermal resistances encountered in the heater and cooler. The analysis for calculating these two effects is derived in Sec. 3.2.4.

The heat-loss terms that must be added to expansion power in order to determine net heat input are described in Sec. 3.2.4.

3.2.2 <u>General Scheme for Solution of Governing Equations</u>. Section 2 described the general Stirling engine code system which is intended to provide a framework for a series of analysis modules which will meet the differing needs of Stirling engine designers. A flow chart of the entire code is shown in Fig. 10. The case to be run is defined by the input data as described in Sec. 2. Because the input routines are general a call is made to the ANALIS



Fig. 10. Main Program

subroutine to particularize the input for the assumptions to be used in the analysis. Then the outer-loop iteration on temperature and energy flows is started.

Successive calls to the ANALIS module will compute these temperatures and energy flows until the values at 0° crank angle match those after  $360^{\circ}$  of integration. In the case of the Rios' type analysis this usually takes about four cycles. The CONVRG subroutine determines the level of accuracy, currently at 0.1 percent change, and what the next estimate of the conditions at 0° will be, currently the last value is used. As additional analysis modules are written CONVRG will be modified to retain this low number of outer loop cycles per case.

As was mentioned, the first call to the ANALIS subroutine particularizes the input for the analysis to follow. In the case of the Rios' analysis a routine called RIOSIN, described in Sec. 3.3.1 was included to fulfill this need.

All subsequent calls to the ANALIS routine, described in Sec. 3.3.2, result in the calculation of power, efficiency, and the distribution of energy through the cycle. The description of the cycle integration of pressure and mass flow is given in Sec. 3.3.3. Once the mass flows and pressures through the cycle have been determined the energy flows through the heat exchangers as detailed in Sec. 3.3.4, are computed. The losses due to conduction are calculated, as shown in Sec. 2.3.4, and added to the energy flow terms resulting in a change in the temperatures in the engine. The calculations are displayed as determined by the various output options available and logic control is returned to the Main Program to determine convergence.

3.2.3 <u>Calculation of Expansion and Compression Work During Cycle.</u> The assumptions necessary for the following derivations are shown in Table VI. The equations for the conservation of energy, the conservation of mass, and the equation of state are used. The momentum equation does not apply due to the assumption of uniform pressure distribution at any instant.

The derivation of the differential equations for pressure and mass are included in Rios' thesis [1], but they will be repeated here in condensed form for completeness and continuity of this report. This is also the case with some of the loss calculations later in this section. Rios' analysis obtains expressions similar to earlier work by Kirkley [7] and Qvale and Smith [43].

The energy equation for a variable cylinder volume may be written

$$dE = dQ - P dV + H dm$$
(36)

The dQ term is zero for an adiabatic cylinder. The internal energy change and enthalpy flux are written as

$$dE = C_T dm + mC_V dT$$
 and  $H dm = C_T dm$ .

Equation 36 then reduces to

TABLE VI. Assumptions Used in Computing SEAMl Expansion and Compression Work Terms

1. Pressure throughout the engine is uniform at any instant.

- 2. Perfect heat transfer in the heater, regenerator, and cooler.
- 3. Temperature in the heat exchange components is constant with time at any point.
- 4. Uniform cross-sectional temperatures and velocities.
- 5. Hot and cold cylinders are adiabatic.
- 6. Perfectly mixed gases in the cylinders.
- 7. Ideal Gas Law applies.

$$C_{v}T dm + mC_{v} dT = -P dV + C_{p}T dm.$$
 (37)

When gas is moving into the cylinder (dm > 0), T is the adjacent heatexchanger gas temperature T\*. Thus, Eq. 37 may be written for both inflow and outflow:

$$C_v T dm + mC_v dT = -P dV + C_p T^* dm$$
 (inflow: dm > 0); (38)

$$C_v T dm + mC_v dT = -P dV + C_p T dm \quad (outflow: dm < 0). \quad (39)$$

The equation of state for the system

$$PV = mRT$$
(40)

yields the following formula when differentiated:

$$\mathbf{RT} \, \mathbf{dm} \, + \, \mathbf{mR} \, \mathbf{dT} \, = \, \mathbf{PdV} \, + \, \mathbf{VdP} \, . \tag{41}$$

Substituting Eq. 41 into Eq. 38, reducing, and rearranging yields

$$du = \frac{PdV}{RT^*} + \frac{VdP}{\gamma RT^*} \quad (inflow), \qquad (42)$$

where  $\gamma$  is the specific heat ratio.

Equation 39 can be manipulated to yield a similar equation,

$$dm = \frac{PdV}{RT} + \frac{VdP}{\gamma RT} \quad (outflow). \tag{43}$$

The cylinder gas temperature can be eliminated from Eq. 43 by substituting Eq. 46 to yield

$$d\mathbf{m} = \mathbf{m} \left[ \frac{d\mathbf{V}}{\mathbf{V}} + \frac{d\mathbf{P}}{\gamma \mathbf{P}} \right]. \tag{44}$$

Equations 42 and 44 are valid for both expansion and compression cylinders.

The conservation of mass, when written for the closed system of the expansion, compression, and dead volumes is

$$\mathbf{m}_{\mathrm{T}} = \mathbf{m}_{\mathrm{C}} + \mathbf{m}_{\mathrm{D}} + \mathbf{m}_{\mathrm{E}} = \mathrm{constant}.$$

Differentiating the above equation yields

$$\mathrm{dm}_{\mathrm{C}} + \mathrm{dm}_{\mathrm{D}} + \mathrm{dm}_{\mathrm{E}}^{\mathrm{m}} 0. \tag{45}$$

The constant reduced isothermal dead volume is defined as the ratio of mass in the dead space to mass in one-half the maximum expansion volume at  $T_E^*$  and the same pressure

$$V_{\rm D} = \left(\frac{\frac{{}^{\rm m}{\rm D}}{\frac{{}^{\rm m}{\rm AE}}{{}^{\rm m}{\rm E}}}\right), \tag{46}$$

where

$$V_{AE} \equiv (V_{E_{MAX}})/2.$$

Note that script is used for nondimensionlized quantities. Since mass in the dead space is proportional to pressure, rearranging and differentiating Eq. 46 gives

$$dm_{D} = V_{D} \frac{V_{AE} \frac{dP}{RT_{E}}}{RT_{E}}$$
 (47)

Four mass flows are possible between the variable cylinder volumes and the dead volume:

$$dm_{\rm C} < 0, \ dm_{\rm E} > 0, \tag{48}$$

$$dm_{\rm C} < 0, \ dm_{\rm E} < 0, \tag{49}$$

$$dm_{\rm C} > 0, \ dm_{\rm E} > 0, \tag{50}$$

$$dm_{C} > 0, \ dm_{E} < 0.$$
<sup>(51)</sup>

Substituting the mass derivatives of Eqs. 42 and 47 into Eq. 45, and using situation 50 yields

$$\frac{P \ dV_C}{RT_C^{\star}} + \frac{V_C \ dP}{\gamma RT_C^{\star}} + \frac{V_D \ dP}{RT_E^{\star}} + \frac{P \ dV_E}{RT_E^{\star}} + \frac{V_E \ dP}{\gamma RT_E^{\star}} = 0.$$
(52)

With the following variables to nondimensionalize Eq. 52

$$P \equiv \frac{P}{P_{MAX}}, V_{C} \equiv \frac{V_{C}}{V_{AC}}, V_{E} \equiv \frac{V_{E}}{V_{AE}}, \tau_{VT} \equiv \frac{V_{AC} T_{E}^{*}}{V_{AE} T_{C}^{*}}$$
(53)

т.

the result is

$$P(r_{VT} dV_{C} + dV_{E}) + (\frac{1}{\gamma}r_{VT}V_{C} + \frac{1}{\gamma}V_{E} + V_{D}) dP = 0.$$

The differential pressure may then be expressed as

$$dP = -\gamma P \frac{\pi V T \frac{dV_C + dV_E}{\pi V T V_C + V_E + \gamma V_D}}{V T V_C + V_E + \gamma V_D} \quad \text{for } dm_C > 0, \ dm_E > 0.$$
 (54)

As with Eq. 52, the mass derivatives of Eqs. 42 and 44 can be nondimensionalized to yield

$$dM = PdV + \frac{VdP}{\gamma} \quad (inflow) \quad (55)$$

and

$$dM = M \frac{dV}{V} + \frac{dP}{\gamma P} \qquad (outflow), \qquad (56)$$

where

$$M_{\rm X} = \frac{{\rm RT}_{\rm X}^{\star}}{{\rm V}_{\rm AX} {\rm P}_{\rm max}} {\rm m}_{\rm X}$$

and X refers to the volume used: E, C, or D.

In a manner similar to that used to find Eq. 54, the following differential pressures can be found:

$$dP = -\gamma \frac{r_{VT} M_C \frac{dV_C}{V_C} + M_E \frac{dV_E}{V_E}}{\frac{r_{VT} M_C}{P} \frac{M_E}{P} + \gamma V_D} \qquad (dm_C < 0)$$
(57)

$$dP = -\gamma \frac{PdV_{E} + r_{VT} M_{C} \frac{dV_{C}}{c}}{V_{E} + r_{VT} \frac{M_{C}}{p} + \gamma V_{D}} \qquad (dm_{C} < 0)$$
(58)

and

$$d\mathbf{P} = -\gamma \frac{r_{VT} \quad PdV_{C} + M_{E} \frac{dV_{E}}{V_{E}}}{r_{VT} \quad V_{C} + \frac{M_{E}}{H} + \gamma V_{D}} \qquad (dm_{C} > 0)$$
(59)

The dimensionless work for both expansion and compression cylinders is found using

....

$$\omega = \frac{\oint \mathbf{p} \, \mathrm{d}V}{\mathbf{P}_{\mathrm{MAX}} \, \mathbf{V}_{\mathrm{A}}} = \oint \mathcal{P} \, \mathrm{d}V. \tag{60}$$

The integration implied in Eq. 60 is performed numerically as described in Sec. 3.3.3.

3.2.4 <u>Analysis of Losses.</u> The losses found in a typical Stirling engine can be divided into two categories: those affecting basic power (the P-V diagram) and those that appear as a heat load on the heat exchangers. Five heat losses are evaluated: (1) regenerator ineffectiveness or reheat loss; (2) a correction to regenerator ineffectiveness due to the oscillating temperature of the regenerator matrix; (3) dynamic power loss, found in engines where a piston displacer separates the hot and cold spaces and "shuttles" heat between them; (4) a correction to the dynamic power loss due to the temperature change of the gas flowing in and out of the gap between the displacer piston and cylinder; and (5) static conduction losses. The first two are calculated in the Analysis Module; the last three are calculated in the Standard Functions Module.

3.2.4.1 Pressure Drop Losses Due to Fluid Frictional Effects. Equation 60 was derived assuming uniform pressure; however, friction pressure loss occurs in all the heat-exchanger components, with the primary loss incurred in the regenerator. To account for these losses, Rios ([1], p. 106) begins by defining the system reference pressure as the expansion cylinder pressure

$$P_E \equiv P_e$$

There is no reason given for choosing the expansion space as the reference. In some codes, for example Tew [2], the reference pressure is at the midpoint of the regenerator. We have retained the Rios assumption for consistency. He then states that the pressure difference between the expansion and compression spaces can be represented as

$$\delta P_{f} \equiv P_{C} - P_{E}$$
(61)

If the expansion work is represented as

$$W_E = \phi P_E dV_E$$

an approximation to the compression work is

 $W_{C} = \oint P_{c} dV_{C} = \oint (P_{E} + \delta P_{f}) dV_{C}$  $= \oint P_{E} V_{C} + \oint \delta P_{f} dV_{C}.$ 

The correction to the compression work due to pressure drop is then defined as

$$\delta W_{\rm C} = \oint \delta P_{\rm f} \, dV_{\rm C}. \tag{62}$$

Two problems arise with this method of maintaining the expansion space variables the same while varying the compression space variables due to The first problem relates to the net work done by the pressure drop. engine. The net work is the sum of the expansion and compression works. The work correction due to friction loss should be applied to either the changing compression volume,  $\delta V_{C}$ , as is done in Eq. 62, or to the changing expansion volume,  $\delta V_{\rm F}$ , if the system reference pressure is assumed in the compression zone. In the Tew code the pressure loss term would be split between  $\delta V_{C}$  and  $\delta V_{\rm F}$  as the reference pressure is in the regenerator. Therefore, the work correction due to friction is a function of the reference pressure assumption. We have run a few cases changing the reference pressure from the expansion zone to the compression zone and have noted that although the net power does change about 5% in some hydrogen cases, and even more in helium cases, the code consistently predicts a higher work correction term and a lower efficiency for the Rios assumption of expansion space reference As was indicated we have retained this assumption. The second pressure. problem with this simplified model is that conservation of mass is no longer satisfied in the compression zone. To examine this problem, Rios introduces an artificial compression zone volume variation

$$V_{C \text{ with}} \equiv V_{C \text{ w/o}} + \delta V_{C}.$$

The compression work then becomes

$$W_{C} = \phi \left( P_{E} + \delta P_{f} \right) d(V_{C} + \delta V_{C}).$$
(63)

A more accurate estimate of work lost due to pressure drop than Eq. 62 would be

$$\delta W_{C} \equiv W_{C} - W_{C} = \oint (P_{E} + \delta P_{f}) d(V_{C} + \delta V_{C}) - \oint P_{E} dV_{C}$$
with w/o  
 $\delta P = \delta P$ 

or

$$\Im W_{C} = \oint \delta P_{f} dV_{C} + \oint P_{E} d(\delta V_{C}) + \oint \delta P_{f} d(\delta V_{C}).$$
(64)

The last integral in Eq. 64 containing the two differential terms is negligible for the pressure and volume differences of a practical Stirling engine. The nondimensionalized pressure-drop work loss then becomes

$$SW_{\rm C} = \phi \, \delta P_{\rm f} \, dW_{\rm C} + \phi \, P_{\rm E} d(\delta V_{\rm C}) \tag{65}$$

Rios derives a discrete form of  $\oint P_{\rm E} d(\delta V_{\rm C})$  in Appendix B of his thesis, but does not include it in his code because it is negligible when  $\delta P_{\rm f}$  is small relative to  $P_{\rm MAX} - P_{\rm MIN}$ , as is typical of a real engine. He therefore uses the nondimensionless form of Eq. 62 in his model.

Rios begins his evaluation of  $\oint \delta P_f dV_C$  ([1], pp. 107-114) by stating that the total pressure drop is the sum of the pressure drops of each component

$$\delta P_{f} = \delta P_{K} + \delta P_{R} + \delta P_{H}.$$

Since the evaluation of all three pressure drops is essentially the same, only that of one component will be described here.

To facilitate the evaluation of the presure drop along the length of the component, a dimensionless length (x/L) is defined as the distance from the end of the component nearest the cold cylinder (x) divided by the component length (L). Appropriate subscripts for x and L are K (cooler), R (regenerator), and H (heater). The pressure drop at a point in the component may then be expressed as the product of a friction factor and a kinetic-energy term ([24], p. 21). For any of the three components

$$d(\delta P_f) = f_x \frac{L}{D_h} \rho_x \frac{u^2 x}{2} d(\frac{x}{L}).$$
(66)

The friction factor  $f_x$ , density  $\rho_x$ , and velocity  $u_x$  are functions of position x and time. It is assumed that the hydraulic diameter  $D_h$  does not vary with position. The velocity at x can be expressed as

$$u_{x} = \frac{1}{\rho_{x} AF} \frac{\partial m_{x}}{\partial t} = \frac{m_{x}}{\rho_{x} AF},$$
 (67)

where AF is the free-flow area within the component, and m is defined as the mass flow rate on the warm (expansion) side of position x at time t; the dimensionless equivalent of m is

$$\hat{M}_{x} = \frac{\dot{m}_{x} R T^{*} \chi}{P_{MAX} V_{AX}}.$$
(68)

In Eq. 61,  $\partial P_f$  was defined as positive when the pressure decreases toward the warm end. Thus,  $d(\delta P_f)$  is positive when  $\hat{m}_x$  is positive. Using this fact, along with Eq. 67 and the ideal gas expression

$$\rho_{\mathbf{x}} = \frac{P_{\mathbf{x}}}{RT_{\mathbf{x}}},$$

Eq. 67 can be rewritten and integrated over the length to yield the following equation for each component:

$$\delta P_{f} = \frac{1}{2} \frac{L}{D_{h}} \frac{R}{AF^{2}} \int_{\frac{X}{L}} \frac{1}{2} \left[ \frac{1}{P_{x}} f_{x} | \mathbf{m}_{x} | \mathbf{m}_{x} T_{x} \right] d(\frac{X}{L})$$
(69)

 $P_x$  can be taken out of the integral if it is replaced with the reference pressure  $P_E;$  this will cause negligible error for  $\delta P_f^{} << P_E^{}$ .

Using Eq. 69, the work-loss integral becomes

$$\oint \delta P_{\mathbf{f}} dV_{\mathbf{c}} = \frac{1}{2} \frac{L}{D_{\mathbf{h}}} - \frac{R}{AF^2} \oint \begin{bmatrix} \frac{\mathbf{x}}{\mathbf{L}} = 1 \\ \frac{1}{P_{\mathbf{x}}} & \int_{\mathbf{x}}^{\mathbf{L}} = 1 \\ \frac{\mathbf{x}}{\mathbf{L}} = 0 \end{bmatrix} \mathbf{f}_{\mathbf{x}} \left[ \mathbf{f}_{\mathbf{x}} \left| \mathbf{m}_{\mathbf{x}}^{*} \right| \mathbf{m}_{\mathbf{x}}^{*} \mathbf{T}_{\mathbf{x}} \right] d\left( \frac{\mathbf{x}}{\mathbf{L}} \right) \end{bmatrix} dV_{\mathbf{c}}.$$

Reversing the order of integration yields

$$\oint \delta P_{f} dV_{c} = \frac{1}{2} \frac{L}{D_{h}} \frac{R}{AF^{2}} \int_{\frac{x}{L}}^{\frac{x}{L}} = 0 \begin{bmatrix} T_{x} \oint \frac{f_{x} |\tilde{m}_{x}| \tilde{m}_{x} dV_{c}}{P_{x}} \\ \frac{x}{L} = 0 \end{bmatrix} d(\frac{x}{L}).$$
(70)

By defining the variable

$$\alpha \equiv \omega t$$
,

which leads to

$$\dot{m}_{x} = \omega \frac{dm}{d\alpha},$$

Eq. 70 may be nondimensionalized using Eqs. 53 and 68:

$$\oint \delta P_{f} dV_{c} = \frac{1}{2} \left(\frac{L}{D_{h}}\right) \frac{\omega^{2} V_{AC}^{2}}{AF^{2} RT_{c}^{*}} \int_{\frac{X}{L}}^{\frac{X}{2}} \frac{T_{x}}{T_{c}^{*}} \oint f_{x} \left[\frac{\left|\frac{\delta M_{x}}{\partial \alpha}\right| \frac{\delta M_{x}}{\partial \alpha} \frac{dV_{c}}{\partial \alpha}}{P_{x}} d\alpha\right] d\left(\frac{X}{L}\right).$$
(71)

Equation 71 is integrated for each component by determining the values for the constants, the positional gas temperature,  $T_x$ , the average friction factor,

 $f_x$ , and the integral of the bracketed angular dependent values. The positional gas temperature  $T_x$  can be approximated as  $T_c$  for the cooler,  $T_e$  for the heater, and the following linear relationship for the regenerator:

$$T_{R} = T_{c}^{\dagger} + \left(T_{e}^{\dagger} - T_{c}^{\dagger}\right) \left(\frac{x}{L}\right)_{R}.$$
 (72)

To determine the variation  $\partial M_{\chi}/\partial \alpha$  in Eq. 71, Rios approximates the pressure in the dead space as uniform. Therefore, with X as the fraction of reduced dead volume on the compression side of x

$$\mathbf{m}_{\mathrm{DC}_{\mathbf{X}}} = \mathbf{X} \mathbf{m}_{\mathrm{D}} \text{ and } \mathbf{m}_{\mathrm{DE}_{\mathbf{X}}} = (1 - \mathbf{X})\mathbf{m}_{\mathrm{D}}$$

Jsing the conservation of mass for the total system, the time derivative causes

$$dm_{C} + dm_{D} + dm_{E} = 0 = dm_{C} + \frac{x}{1 - x} + dm_{E}.$$
 (73)

With  $m_y$  as the mass of the system on the expansion side of x

$$dm_{x} = dm_{DE_{x}} + dm_{E}.$$
 (74)

Combining Eqs. 73 and 74 yields

$$dm_{C} + \frac{dm_{x} - dm_{E}}{1 - x} + dm_{E} = 0.$$

Nondemensionalizing as in Eq. 71 and solving for  $\partial M_{\nu}/\partial \alpha$ ,

$$\frac{\partial M_{\mathbf{x}}}{\partial \alpha} = \mathbf{x} \frac{\partial M_{\mathbf{C}}}{\partial \alpha} + \frac{1}{\pi_{\mathbf{vr}}} \frac{\partial M_{\mathbf{E}}}{\partial \alpha} - \frac{\partial M_{\mathbf{C}}}{\partial \alpha}.$$
 (75)

By determining the average value of  $\partial M_{\chi}/\partial \alpha$  for the various components, the Reynolds number and hence the average friction factor,  $f_{\chi}$  can be determined. The bracketed term in Eq. 71

$$\phi \begin{array}{c|c}
\frac{\partial M_{x}}{\partial \alpha} & \frac{\partial M_{x}}{\partial \alpha} & \frac{\partial V_{c}}{\partial \alpha} \\
\hline
P_{x} & \partial \alpha & \partial \alpha \\
\end{array}$$

can then be integrated separately for each component, thereby providing the  $\oint \partial P_f \partial V_r$  needed to determine the work loss in Eq. 65.

3.2.4.2 <u>Imperfect Heat-Exchanger Loss</u>. Imperfect heat-exchanger heat transfer is the second type of loss affecting the basic power. Since a

temperature gradient exists between the heat-exchanger walls and the gas due to thermal resistance of the fluid film, gas entering the cylinder and regenerator will not be at the heat-exchanger wall temperature. However, if the temperature difference between the gas and the heat-exchanger wall is small, the effect on the cycle will be negligible.

SEAMI's approach for evaluating this loss begins by first calculating actual heat flows into and out of the engine. Actual heat in per cycle is computed by adding the heat converted to useful work in the expansion cylinder and those heat flows that increase the load on the heater; these include dynamic shuttle and piston-gap losses, regenerator ineffectiveness and its correction, and conduction down the cylinder wall, piston wall, regenerator wall, and regenerator filler material. Subtracted from this total is the friction loss for the hot end of the engine that lessens the heat load. Mathematically this can be expressed as

$$Q_{H} = W_{E} + Q_{DYNAMIC} + Q_{REGEN} + Q_{CYLWL} + Q_{PISWL} + Q_{REGWL} + Q_{REGFIL} - Q_{HTRFRIC} - Z1 \cdot Q_{REGFRIC},$$
(76)

where Zl is the input fraction of regenerator frictional heat generation in the heater space.

Actual heat out of the engine per cycle is the sum of the cold cylinder work and those heat flows that increase the cooler load. (Since the cold work is a negative value, the heat flows are subtracted from it to increase the magnitude of actual heat out.) The heat flows that increase the cooler load are the regenerator ineffectiveness and its correction, and the friction loss on the cold end of the engine, plus some conduction losses that find their way into the cooler. Because not all engine designs are alike, some of the conduction losses can go directly to the cooling water. These options are explained in Appendix A. When all these losses went through the cooler, the heat flow out of the cooler would be

$$Q_{c} = W_{c} - Q_{REGEN} - Q_{COOLFRIC} - (1-21) \qquad Q_{REGFRIC}$$
$$- Q_{PISWL} - Q_{REGFIL} - Q_{DYNAMIC} - Q_{CYWLW}, \qquad (77)$$

where the second line represents the optional heat loads.

In both Eqs. 76 and 77

W <sub>x</sub>	is from the integration of Eq. 65,
QXXFRIC	is from the appropriate form of Eq. 71,
<b>Q</b> DYNAMIC	is from Eq. 34,
Q <sub>REGEN</sub>	is from the evaluation of Eq. 84

and the remaining Q's due to conduction are from Eq. 35.

With these actual heat flows in the heater and cooler, the effective inner-wall temperatures of these exchangers can be computed using the heattransfer formula,

$$Q_{\mathbf{x}} = \frac{TE_{\mathbf{x}} - TW_{\mathbf{x}}}{R_{\mathbf{x}}},$$
(78)

where  $Q_x$  = actual heat flow, TE<sub>x</sub> = the temperature of the medium outside the heater or cooler tubes (combustor or water temperature, respectively), TW<sub>x</sub> = inner-wall temperature, and R = the sum of the thermal resistances between TE and TW. These resistances include the convective resistance between the outer and inner walls, and assuming circular tubes in the heater and cooler have the form

$$R_{\mathbf{x}} = \left(\frac{1}{h_{o} A W_{o} N}\right)_{\mathbf{x}} + \left(\frac{\ln \left(\frac{D_{o}}{D_{i}}\right)}{2\pi k_{w} L N}\right)_{\mathbf{x}},$$
(79)

where  $h_0 = convective coefficient$  for the tube exterior,  $AW_0 = outside-tube$  surface area, N = number of tubes,  $k_w = wall$  thermal conductivity, and L = tube length.

The effective gas temperatures can be found from the inner-wall temperatures by using

$$T_{x} = TW_{x} - Q_{x} / (h AW)_{x}.$$
(80)

Of course, the user also has other options, such as specifying constant gas temperature in a heat exchanger. These options are explained in Appendix A.

3.2.4.3 Regenerator Ineffectiveness  $\left(Q_{\text{REGEN}}\right)$ . Regenerator ineffectiveness also known as reheat loss, represents the ratio of the net enthalpy flow per cycle through the regenerator to the heat transfer necessary to heat the gas from the cold-end temperature to the hot-end temperature. To examine regenerator ineffectiveness, Rios used the derivations of Qvale and Smith [42]. However, since their solution was derived for sinusoidal pressure and flow variations, Rios rederived their equations for general flow and pressure variations. The entire derivation is included in Rios' thesis ([1], pp. 121-127); for brevity, only the assumptions and the final result will be given here.

The assumptions are:

- (1) The regenerator gas state is unaffected by fluid friction.
- (2) The matrix temperature at any point in the regenerator is constant with time.
- (3) The regenerator is efficient; therefore, the gas to matrix temperature difference is small relative to the longitudinal temperature change.

(4) There is no axial conduction.

The reheat loss is given by the dimensionless formula

$$\lambda_{R} = \left[\frac{1}{\frac{1}{12CR} + \frac{1}{12ER} \frac{M_{ACR}}{M_{AER}}}\right] \left[1 + N_{PH} \frac{1}{12CR} + \frac{1}{12ER} \frac{M_{ACR}}{M_{AER}}\right]. \quad (81)$$

The notation is that of Rios [1].

The terms in the first pair of brackets of the above equation represent the regenerator's transfer qualities. The second pairs of brackets represent the effect of heat transfer due to compression and expansion of the gas in the regenerator dead space.

This yields the actual reheat loss as

$$Q_{\text{REHEAT}} = N \, \mathring{\mathbf{m}}_{R} \, C_{P} \, \pi \, \lambda_{R} (T_{H} - T_{K}). \qquad (82)$$

3.2.4.3.1 <u>Correction to Regenerator Ineffectiveness</u>. This correction results from an oscillation of the regenerator-matrix temperature during the cycle. In calculating the reheat loss, this oscillation was assumed negligible; however, this assumption is not always valid. The temperature swing loss is the additional heat load resulting from a finite regenerator heat capacity. Martini ([27], p. 139) gives the regenerator-matrix temperature change as

$$\Delta T_{MATRIX} = \frac{{}^{m}_{H}C_{v}(TW_{H} - TW_{C})}{3 FREQ(M C_{P})_{MATRIX}}$$

and gives the actual correction to the reheat loss as

$$Q_{\text{TSWING}} = \left[\frac{{}^{\text{m}}_{\text{R}}{}^{\text{C}}_{\text{v}}}{3}\right] \frac{\Delta^{\text{T}}_{\text{MATRIX}}}{2}$$
(83)

and the total regenerator ineffectiveness is the sum of Eqs. 82 and 83).

$$Q_{\text{REGEN}} = Q_{\text{REHEAT}} + Q_{\text{TSWING}}$$
(84)

#### 3.3 DESCRIPTION OF SUBPROGRAM ELEMENTS OF SEAMI

The analysis module consists of five major routines: RIOSIN, ANALIS CYCLER, HTFLOW, and RIOSPR.

3.3.1 <u>RIOSIN Subroutine</u>. As was indicated in Sec. 3.2.2 the general input is particularized for the analysis to be used. The RIOSIN routine collapses the cell input into the five volumes monitored by the analysis. It

computes and stores the volumes and their derivatives for every step to be calculated. Although this requires several large arrays, it was felt the calculational time saved was worthwhile. In addition, the routine initializes the masses, temperatures, and pressures to be used.

3.3.2 <u>ANALIS Subroutine</u>. The ANALIS subroutine (Fig. 11) provides the framework for execution of the Rios technique. Few calculations are performed by it, its primary purpose being to direct the execution by calling the appropriate routines. Note that ANALIS calls the LOSSES routine described in Chapter 2 to compute the standard loss mechanisms. ANALIS is called from the MAIN program at the start of each cycle.



Fig. 11. ANALIS Subprogram

3.3.3 <u>CYCLER Subroutine</u>. The main purpose of CYCLER is to compute the pressure variations during a cycle, and the net work per cycle by evaluating the pressure-volume integral. The routine follows these basic steps:

(1) <u>Initialization</u>. Initialize the cycle by calculating values for the hot and cold space masses based upon the current gas temperature and pressure. Initialize the dimensionless works, negative mass accumulators, and minimum/maximum gas temperatures.

(2) <u>Define Decision Matrix</u>. Determine which of the four options for work integration is appropriate by evaluating the direction of mass flows (Eqs. 48-51). For the first step, mass is assumed to be increasing in the cold space and decreasing in the hot space (Eq. 51).

(3) <u>Main Loop for Work Integration</u>. The pressure, mass, and work Eqs. 54-60 are written in discrete form and are represented by DP, DMW, DMC, WC, and WW. A numerical integration of the Runge-Kutta second-order type ([45] pp. 52-54) is then performed. The volume, mass, and pressure at the start of a step are used to calculate the same variable at the midpoint of the step. Both values are averaged to calculate the complete step. After each integration step, the signs of the mass derivative terms are checked to determine which of the four mass-flow possibilities is appropriate. The entire cycle is integrated in this way for NSTEP steps.

(4) <u>Record Results</u>. The pressure and the differentials of pressure, compression-zone mass, and expansion-zone mass are saved for each step. The variable volume gas temperature are calculated, and the maximum/minimum values are updated if necessary.

(5) <u>Buffer Zone Calculation</u>. The variation in volume of the buffer zone was saved previously so an isothermal relationship is assumed when a buffer (added volume) calculation is desired.

- (6) Graphics. If desired, the code will save
- 1. Crank angle 2. Expansion-zone volume
- 3. Pressure 4. Compression-zone volume
- 5. Compression-zone mass 6. Expansion-zone mass
- 7. Cold piston torque 8. Compression zone temperature
  - 9. Expansion zone temperature

These data are used for an additional print option as well as various crank angle curves.

(7) <u>Convergence</u>. The last part of the inner loop checks the agreement of the final cycle values of dimensionless pressure, P, and hot space mass, XMW, with the values from the beginning of the cycle. If  $\Delta P > 0.5\%$  or  $\Delta XMW > 0.1\%$ , the cycle is iterated with the final dimensionless pressure and hot space mass of the previous cycle as starting values. The NITE counter allows a maximum of 15 cycles before exiting the loop and printing.

3.3.4 <u>HTFLOW Subroutine</u>. This routine calculates the flow of energy from the heater to the cooler water. Because this calculation resides outside of the cycle loop it requires the inclusion of a calculation for: regenerator ineffectiveness; cooler, regenerator, and heater frictional losses; and average values of heat-transfer coefficients. The routine follows these basic steps:

(1) <u>Calculate Dimensionless Pressure</u>. The average cycle pressure PNAVG is found by summing the pressures of each increment and then dividing by NSTEP. The maximum pressure is found and the dimensionless quantities are adjusted to the new maximum pressure. The phase angle between the pressure and volume variations, FIPV, is calculated for use in the piston gap loss, Eq. 33.

(2) <u>Compute Values Used in Loss Calculations</u>. Subroutine PDINT integrates Eq. 75 to determine the mass-flow-rate terms needed to evaluate the loss  $\phi \partial P$   $\partial V_C$ , Eq. 71. It additionally evaluates the integrals used in the reheat loss, Eq. 81, such that XII = I<sub>1x</sub>, XI2 = I<sub>2x</sub>, XI3 = I<sub>1x</sub>/I<sub>2x</sub>. where x refers to either the compression or the expansion side of the regenerator.

The flow integrals UIN and UDM (equivalent to XINT and DMRE), are linearly interpolated in routine XNTERP for five volume locations in the heat exchangers to determine appropriate Reynolds numbers and kinetic energies.

(3) <u>Pressure-Drop Losses</u>. The pressure drop is expressed as the kinetic energy multiplied by a friction factor as shown in Eq. 66. It is represented in the code by GLS (cooler) and GLH (heater). The QP factor found in the code contains the engine parameters necessary to convert the pressure drops GLS and GLH to power losses QKOLFR and QHTRFR. The HTF routine in the Standard Functions module is called to compute contraction and expansion losses in the heater (ALOSSH) and cooler (ALOSSC); these are added to QHTRFR and QKOLFR, respectively, to obtain total friction losses.

The regenerator pressure-drop loss it similar to the heater and cooler losses in that it is expressed in the same form with the kinetic energy term multiplied by a friction factor. However, it differs by splitting the regenerator into three sections: cool, middle, and warm. The Reynolds number and friction factor are evaluated at each section. A weighted average of these individually calculated pressure drops is taken by using Simpson's Rule.

(4) <u>Calculate Wall and Gas Temperature for the Heater and</u> <u>Cooler</u>. Actual heat flows are computed for the heater (QACTH) and cooler (QACTC). Unless some other option has been chosen by the user, the inner-wall temperatures TWALLD(JHOT) and TWALLD(JCOOL) are then found using Eq. 78; effective gas temperatures TGASD (JHOT) and TCASD (JCOOL) are then found with a form of Eq. 80.

(5) <u>Regenerator Ineffectiveness Loss and its Correction</u>. The regenerator ineffectiveness loss QREGRH is found from Eq. 84 as was discussed earlier.

3.3.5 <u>RIOSPR</u> Subroutine. This routine provides a method of cataloguing the results of a cycle using the Rios technique so that they may be edited by the output processor. The routine saves about 50 variables on a cycle-by-cycle or case-by-case system as a function of the output-edit control variable NPRT2. In addition, the routine saves an array of variables for each zone used in the calculation, including heat flows, temperatures, mass flows and effective Nusselt numbers.

# 4. TEST RESULTS AND CONCLUSIONS

This chapter describes the results of using SEAM1 to analyze the GPU-3 engine. A comparison is made between SEAM1 calculations, calculations reported from the Tew/NASA code [47], and experimental measurements made at NASA/LeRC on the GPU-3 engine [46].

#### 4.1 GPU-3 PERFORMANCE PREDICTIONS USING SEAM1

GPU-3 engine and component measurements [46] were used to prepare data for the input processor. Power and efficiency were determined as follows from the measured alternator output and cold-side heat flows:

where

$$P = P_a + P_{I_a},$$

P = "indicated" engine power (gross output with no mechanical losses),

P<sub>a</sub> = measured alternator power/alternator efficiency,

P<sub>L</sub> = measured mechanical losses (sum of heat to engine oil plus buffer water);

where

 $Q_H = Q_C + P$ ,

Q<sub>H</sub> = heat into heater head

and

Q<sub>C</sub> = measured cooling-water reject heat (sum of heat from crankcase and cooler tubes)

Therefore the efficiency n is obtained from

$$\eta = P/Q_{u}$$
.

These definitions are the basis for the values of power and efficiency given in Table VII and used in Figs. 12-14.

A sample map run requires that pressure, gas type, frequency, and heater wall temperature be supplied in addition to other fixed engine specifications. In the experimental runs, the cooling-water flows and inlet temperatures were reasonably constant, which implied that the heat-transfer film coefficient between the water and tube wall was also constant. Data given for temperature probes on the outer heater wall were used to provide heater temperature.

Since the GPU-3 crankcase is water cooled, conduction and other heat losses between the hot and cold ends of the engine combine to raise the temperature of the cooling water. The remaining energy losses and compression work are associated with the working fluid and combine as the heat transferred from the working fluid to the cooler tubes. The gas temperature is then predicted according to the Rios assumption that "Work in the movable spaces is provided from energy transferred by the adjacent heat exchanger." This model is not exact, but produced calculated values of cooling-water heat flow close to that measured.

	Operating Conditions			Indicated Power (kW)			Indicated Efficiency (%)		
Gas	Temperature (K)	Mean Pressure (MPa)	Engine Speed	NA SA Code	SEAM1 Code	Ежрегішенtal Data	NASA Code	SEAM) Code	Experimental Data
н <sub>2</sub>	Heater Ref-	2.7	1500	1.94	1.91	1.95		36.8	35.5
	erence: 922		2500	2.93	2.91	2.93		37.1	35.0
	Water Inlet: 289		3500	3.35	3.34	3.37		32.9	31.4
He	Heater Ref-	2.7	3000	2.2	1.91	2.06	24.7	22.4	23.1
	erence: 922	4.1		3.64	3.41	3.43	27.6	27.3	26.4
	Water	5.5		5.12	4.48	4.64	30.4	27.6	27.1
	infet: 289	6.9		6.18	5.29	5.48	30.2	26.9	26.5

# TABLE VII.Comparison of SEAM1 Calculations with GPU-3 ExperimentalData and NASA Code Predictions [47]

Table VII compares performance predictions from SEAMI with experimental data and with a more sophisticated analysis code developed at NASA [3]. SEAMI is seen to provide good predictions for engine power, but somewhat overestimates efficiency. Optimistic predictions of efficiency from approximate models are common since all engine losses are not included in simplified analyses. Computations from SEAMI indicate that frictional losses and losses due to imperfect regeneration are the dominating influence on efficiency. Table VII shows that the agreement between measured and calculated values is maintained whether engine speed, system pressure, or working fluid is varied.

Figure 12 shows predictions of indicated power as a function of engine speed and mean cycle pressure. A good match is shown with experimental data. However, the engine was unable to overcome losses and develop power above 3 kW at engine speeds below 1500 rpm, so a comparison could not be made in this region.

Figure 13 shows the prediction of efficiency as a function of engine speed and mean cycle pressure. A large increase in efficiency is seen when the pressurization is increased from 2.76 to 4.1 MPa, but negligible improvement occurs for further increases in pressurization except at speeds below 1500 rpm. These effects can be explained in terms of the relative magnitudes of the conduction, friction losses, and regenerator losses. Conduction losses are determined almost entirely by the temperature difference between the hot and cold sides of the engine, thus only changing slightly with pressurization and speed. When pressurization is increased, gross power



# GPU-3 HELIUM 927K/339K

Fig. 12. Power Comparison



GPU-3 HELIUM 927K/339K

Fig. 13. Efficiency Comparison

increases faster than losses, and efficiency improves. At 4.1 MPa, flow losses dominate conduction losses, and further pressurization does not significantly improve efficiency since flow losses also increase with pressurization. At low speed, flow losses are reduced and efficiency improvements can be obtained by increased pressurization as is shown by Fig. 13. No measurements of efficiency above 33% were made, although the code predicts 40% should have been possible at the lower speeds.

Figure 14 presents the same data as an engine map of power versus efficiency at different pressurization levels. In this figure the combined deviations from measured values of power and efficiency are most noticeable. The significant result is that the trends are correct and only the magnitude needs more work.

Heat transfer between the gaseous working fluid and the heater and cooler walls was found to occur in the transition region between laminar and turbulent effects. A linear variation is assumed for the correlations in the transition region. We assumed a transition to turbulence at a Reynolds number of 4000, as was discussed in Chapter 2. These assumptions significantly affect the computed gas temperature and therefore the magnitude of power and efficiency.

#### 4.2 CONCLUSIONS

The GPU-3 example above shows that SEAM1 makes reasonably accurate predictions of Stirling-engine performance characteristics. This capability is a result of appropriately accounting for energy losses as well as heat flows into, out of, and through the engine. In addition to providing useful design information, SEAM1 required very little computer computation time since convergence to a solution usually occurred within three iterations. SEAM1 thus provides Stirling-engine analysis capability that should meet the needs of a wide spectrum of researchers in this field. GPU-3 HELIUM 927K/339K



Fig. 14. Engine Map

# APPENDIX A DIRECTIONS FOR USING THE CODE

This appendix contains directions for specifying input for the current version of the ANL Stirling Engine Analysis Code.

#### A.1 GENERAL INPUT DATA GROUPS

The input information is broken into three groups.

The first group provides general information to the code, such as title, frequency, gas type, and number of components in the other groups.

The second group provides information for the basic Stirling-cycle calculation. These data are put in by component, and an option is given to subdivide the component into cells for greater accuracy. For example, for the cooler (a relatively constant parameter component), data could be input once and then subdivided into constant volume cells to modify the cell-to-cell volume ratio and decrease numerical diffusion. It is important to remember that all codes treat a 200-tube heat exchanger as 200 identical tubes and therefore simulate only the average tube. The input emphasizes this by expecting the data on a per-tube basis. In those cases in which one expansion space feeds several heat exchangers, the number of tubes is the number per exchanger times the number of exchangers per expansion-compression unit.

The third group provides information for those volumes not directly connected to the working space. These added volumes include the various buffer spaces, crankcase, and hot piston dome. In Fig. A-1 they are the alphabetic labeled volumes. The information provided includes the data necessary to calculate the mass, pressure, and heat flow in these spaces.

Ail data are input according to Namelist conventions. The general data are entered by name into Namelist name GINPT. The second group is entered through the dummy variables II and AA using Namelist name CELL for each component. The third group of data is entered through the dummy variables JJ and BB using the Namelist name ADDED. These added volume values are only input if the option NADD has been previously input in the general data group.

See Table A-1 of Section A.6 for the actual input deck used for the GPU-3 example discussed below. It is suggested that before attempting to put together an input deck, the user should make up some input data worksheets as in Table A-2. On these worksheets the data are organized for easy reading when writing the Namelist statements that appear in the input deck, Table A-1.

All input variables are zeroed out initially, so if any input values are omitted from a Namelist, they will remain equal to zero. All data values are input using the International System of Units (SI).

The following description of the input variables used by the input processor module has two parts: the general description and the GPU-3 example (Fig. A-1). Each input variable is described and assigned values that model the GPU-3 (ground power unit) engine built by General Motors for the U.S. Army in 1965 and recently tested extensively at NASA/LeRC ([46],[47]).



Fig. A-1. GPU-3 SEAM1 Cell Location

# A.2 TITLE AND GENERAL INPUT

#### First Input. Title

The first card image is used to head each page of printout, up to 80 columns. In the graphics routine the first 24 columns are used as a general plot title.

General Input. Namelist Name GINPT

The GINPT namelist block can be divided into two categories:

- (1) Integer values saved by the input processor as common IGEN.
- (2) Floating-point values saved in common FLTGEN.

# A.2.1 COMMON IGEN

# ICHNG

Determines if changes will be made to the initial input

0 - No additional changes.

Non 0 - Used to signal perturbation option (see Sec. A.5).

GPU-3: ICHNG = 1 so that frequency could be varied.

#### IDESIGN

Type of engine design: three options

- 1 In-line design, also known as an alpha engine; two pistons, two cylinders (Fig. A-2).
- 2 Double-acting piston design; repetitive arrangement of two or more basic configurations (Fig. A-3)
- 3 Displacer design; one cylinder contains both a displacer and a piston (Fig. A-4).

**GPU-3: IDESGN = 3** 

#### IDRIVE

Drive mechanism used: three options

- 0 Connecting-rod mechanism
- 1 Rhombic drive
- 2 Dynamic analysis (not yet available)

GPU-3: IDRIVE = 1 (Fig. A-5).





- **1** EXPANSION SPACE
- 2 HOT CONNECTING DUCT
- **3 HEATER**
- 4 REGENERATOR
- 5 COOLER
- 6 COLD CONNECTING DUCT
- 7 COMPRESSION SPACE

- A DISPLACER
- B DISPLACER BUFFER
- C COLD PISTON BUFFER
- D CRANKCASE




Fig. A-3. Design Type 2 Double Acting Design





### IGAS

Working fluid: six options

- 1 hydrogen4 air2 helium5 carbon dioxide3 nitrogen6 methane
- GPU-3: IGAS = 1, hydrogen is used in this sample run; other gases have been used experimentally and by other codes for the GPU-3.

#### IMASS

This is used to select which of the following two parameters is to be held fixed while the other is to be allowed to vary as the program iterates to convergence on the effective gas temperatures: PMEAN (mean gas pressure for one cycle) or TMASS (total gas mass in the engine). With this option the code will model engines that can be characterized as either operating at a specified mean pressure, or sharing a fixed mass in the system, in which case then, mean pressure will be computed.

- 0 PMEAN fixed, TMASS calculated.
- 1 TMASS fixed, PMEAN calculated.
- GPU-3: IMASS = 0; not input, selected to match method used by NASA-Lewis code.

### IMOM

Consideration of working fluid momentum effects: two options

- 0 Momentum equation used in calculating friction only (no gas inertial effects are considered).
- 1 Momentum equation is used as an integral part of the basic analysis (e.g., Urieli-type code).
- GPU-3: IMOM = 0; not input, approach originally designed by RIOS and used by SEAM1.

### IPRTl

Debugging variable if > 0, more output will be printed to observe internal calculations: four options

- 1 Initialization output increased.
- 2 Energy-flow output increased.
- 3 Entire-convergence output increased.
- 4 Final cycle parameters output increased.

GPU-3: IPRT1 = 0.

### IGRAPH

Determines if regults are saved to be graphed by the computer: three options

- 0 No graph.
- 1 Save graphics info for each case.
- 2 Save graphics info for case to case comparison. Current version of SEAM1 uses a proprietary graphics package, TELLAGRAF by ISSCO to graph P-V diagrams and engine maps (see Sec. A.8).
- GPU-3: IGRAPH = 1.

### NADD

Number of alphabetic added volumes; integer value from 0 to 4, depends on engine design, analysis used, and user discretion (Figs. A-2, A-3, and A-4 for possible added volumes).

GPU-3: NADD = 2 (Fig. A-1). Displacer space (A) used for heattransfer calculations; conduction down its walls to cold space and internal radiation from the hot end to the cold end. Buffer space (C), for use in torque calculations.

### NCODE

Used to select analysis module:

0 - SEAM1 (Rios based) (Ref. [1])
1 - SEAM2 (Tew based) (Ref. [3])
2 - SEAM3 (Urieli based) (Ref. [2])
GPU-3: NCODE = 0; not input.

#### NCOMP

Number of components the engine is divided into by the user. The value chosen for NCOMP depends upon engine complexity and user discretion; it is suggested that the components be chosen to geometrically separate different gas-flow areas. These components can be partitioned into smaller, identically sized cells using input NCEL to give them cell-to-cell volumetric consistency. The minimum value of NCOMP for a typical Stirling engine would be 5: expansion space, heater, regenerator, cooler, and compression space. The maximum value is 30.

GPU-3: NCOMP = 11 (Fig. A-1). This value is greater than the minimum value because the heater was divided into two cells and the connecting ducts between the five components mentioned above were designated as individual cells.

### NCYL

Number of cylinders in the engine; one expansion compression unit per cylinder.

GPU-3: NCYL = 1.

# NOPT

Indicates additional losses to be included in heat flow from the gas through the cooler walls to the cooling fluid. Four options:

- 0 No additional losses (friction, reheat, and compression work only).
- 1 Conduction along piston walls + axially through the regenerator mesh added to NOPT = 0.
- 2 Dynamic losses (shuttle + gap) added to NOPT = 1.
- 3 Axial conduction along cylinder walls added to NOPT = 2.

GPU-3: NOPT = 1.

#### NPRT1

Number of time steps/printouts of general zone information. In the SEAMI analysis, general zone information is not available within the cycle, so this option is less relevant.

GPU-3: NPRT1 = 720; two full cycles/printout.

#### NPRT2

Number of cases/full printout of power and energy flows. If only one case is being run this value should be 1.

GPU-3: NPRT2 = 6; six cases compared together.

### NREVL

Maximum number of iterations the analysis portion of the program goes through to evaluate the effective gas temperatures; generally, gas temperatures converge sufficiently by the fourth iteration.

GPU-3: NREVL = 12; Convergence is satisfactory with SEAMI when hot and cold gas temperatures are within 2 K of previous values, and the energy flow has been resolved to less than 2%.

# NSTEP

Number of time steps in one revolution. Maximum present value is 720 (dimensioned array limitation).

GPU-3: NSTEP = 360, one time step per one degree of revolution.

### A.2.2 COMMON FLTGEN

### CMPCR

Compression piston crank radius; used by the volume subroutine.

- Note: The stroke can be calculated from the geometry, for example, Stroke =  $((CMPCRL + CMPCR)^2 CMPECC^2)^{1/2} (CMPCRL CMPCR)^2 CMPECC^2)^{1/2}$ .
  - GPU-3: CMPCR = 1.38E-2 m, Table 1, Ref. [46]; see Fig. A-5. Same as EXPCR for rhombic drive. If the eccentricity is zero, then CMPCR = STROKE/2.

### CMPCRL

Compression piston connecting rod length; used by the volume subroutine.

- <u>Note</u>: Sinusoidal motion will be approximated if CMPECC = 0 and CMPCR << CMPCRL. It is recommended that the user set CMPCRL = 100 \* CMPCR if sinusoidal motion is desired. Similar comments hold for the expansion piston parameters.
  - GPU-3: CMPCRL = 4.60E-2 m, Table 1, Ref. [46]; and Fig. A-5. Same as EXPCRL for rhombic drive.

### CMPDV

Compression zone dead volume; sum of all volumes in compression cylinder not swept by compression piston, such as the piston-cylinder clearance volumes. In a displacer design (Fig. A-4) this volume can be substantial, especially with variable stroke piston drives. There must always be at least a small amount of dead volume.

GPU-3: CMPDV =  $1.09E-5 \text{ m}^3$ ; Table 2 of Ref. [47]; sum of last 5 volumes in Section 5.

#### CMPECC

Compression piston crank radius eccentricity.

GPU-3: CMPECC = 2.08E-2 m; Table 1 of Ref. [46] and Fig. A-5. Same as EXPECC for rhombic drive. See note after CMPCRL.

#### CMPGAP

Compression piston-cylinder wall gap. Used for computing dead volume around compression piston; not presently used.

GPU-3: CMPGAP = 1.5E-4 m; Table 1 of Ref. [46] (cylinder bore at liner - piston diameter)/2).

#### CMPRD

Compression piston rod diameter; used in volume calculations to determine the area behind the compression piston.

GPU-3: CMPRD = 2.22E-2 m; Table 1 of Ref. [46].

### CRANKD

Crank angle between top dead center for expansion and compression pistons in degrees. If input as 0, will be calculated from PHASED.

GPU-3: CRANKD =  $0.0^{\circ}$ ; not input, for a rhombic drive, CRANKD is calculated by the code.

#### EXPCR

Expansion piston or displacer crank radius.

GPU-3: EXPCR = 1.38E-2 m; Table 1 of Ref. [46] and Fig. A-5, same as CMPCR for rhombic drive.

### EXPCRL

Expansion piston or displacer connecting rod length.

GPU-3: EXPCRL = 4.60E-2 m; Table 1 of Ret. [46]; see Fig. A-5, same as CMPCRL for rhombic drive.

### EXPDV

Expansion zone dead volume; sum of all volumes in expansion zone not swept by the expansion piston or displacer, such as the manifold and clearance gaps. There must always be at least a small amount of dead volume.

GPU-3: EXPDV =  $1.25E-5 \text{ m}^3$ ; Table 2 of Ref. [46], sum of all dead volumes in Section 1.

### EXPECC

Expansion piston or displacer crank radius eccentricity.

GPU-3: EXPECC = 2.08E-2 m; same as CMPECC for rhombic drive.

### EXPGAP

Gap between cylinder wall and expansion piston or displacer. Used to compute the dead volume around the displacer for the dynamic gap loss calculation in SEAM.

GPU-3: EXPGAP = 2.5E-4 m; Table 1 of Ref. [46] (cylinder bore above liner - displacer diameter)/2.

### EXPRD

Rod diameter for the expansion piston or displacer; used in volume calculations to determine the area behind the expansion piston.

GPU-3: EXPRD = 9.52E-3 m; Table 1 of Ref. [46].

# FREQ

Frequency of the system (Hz).

GPU-3: FREQ = 16.67, 25., 33.33, 41.67, 50., 58.33; varied to match cases run by experiment and NASA-Lewis code. Only the first of these frequencies is included in namelist GINPT. The others are input by means of Namelist PERTIN (see Sec. A.5).

#### HYSTF

Thermal hysteresis factor. Not used by SEAMI.

GPU-3: HYSTF = 0; not input.

### PHASED

Crank angle (degrees) between minimum volumes of the expansion and compression zones; if input as 0, computed from CRANKD.

GPU-3: PHASED =  $0.0^{\circ}$ ; not input, for a rhombic drive, PHASED is calculated by code.

### PMEAN

System gas pressure averaged over the cycle. Either PMEAN or TMASS is held fixed while the other is allowed to vary (see TMASS and IMASS). If 0, it will be either computed from ideal gas formula or averaged from the sum of the cell pressures.

GPU-3: PMEAN = 2.74E+6 Pa; Case H141B, Ref. [46].

### REGHT

Distance from the top of the regenerator to the bottom of the curved portion of the cylinder dome, measured parallel to the cylinder axis. Its primary use is in steady-state heat conduction; the sum of this length and XLNGTH for the regenerator is the conduction path distance from the expansion space to the cooler.

GPU-3: REGHT = 2.86E-2 m; approximation from available data (see Fig. A-1.).

### STARTD

Crank angle (degrees) at time = 0.0; compression volume will start at a minimum if STARTD = 0.0.

GPU-3. STARTD =  $0.0^{\circ}$ .

### TCMBST

Either combustor or external heater tube wall temperature. The code decides which of the two has been input by using the input value of HCEXT for the

heater cell. If HCEXT is greater than 0.0, TCMBST is assumed to be the combustor temperature. If HCEXT is equal to 0.0, TCMBST is assumed to be the external heater wall temperature. Note: When HCEXT is very large, combustor and external heater wall temperature become nearly equal.

GPU-3: TCMBST = 0.0 K; set equal to TWALL of the heater by the input processor. Heater TWALL was perturbated along with the frequency to better match the results of the NASA-Lewis experiments, Ref. [46]. See perturbation section on how TWALL of the heater was varied.

### TWA'TER

Similar to TCMBST but for cooler; either mean coolant temperature or external cooler tube wall temperature. As with TCMBST, the code decides which of the above temperatures has been input by using the input value of HCEXT for the cooler. If TWATER = 0.0, it will be set equal to the cooler wall temperature.

GPU-3: TWATER = 287.0 K; inlet cooler water temperature was used as an approximation for the mean coolant temperature; the outlet temperature varied from the inlet by only a few degrees K (Ref. [46]).

### TMASS

Total mass in the contiguous system. If not input, or input as 0.0, it will be computed provided that the other three parameters needed by the ideal gas equation have been input.

Pressure -- PMEAN for the system or PGAS for each cell.

Volume - VOL for each cell or inputs to compute VOL.

Temperature --- TGAS or TWALL for each cell. (If TGAS is not input, it is initially assigned the value of TWALL for that cell.)

Depending on the value of IMASS, TMASS will be either held fixed or allowed to vary as the program iterates to convergence on the effective gas temperatures.

GPU-3: TMASS = 0.0 kg; not input.

#### TWENVR

External temperature; either room temperature or engine surface temperature. If TWENVR = 0.0, then it will be assigned 300 K as a default.

GPU-3: TWENVR = 0.0 K; not input.

### ZOPT1

Code dependent option.

SEAMI: ZOPTI is the fraction of the regenerator friction energy that is added to the heater; the remainder is added to the cooler. GPU-3 ZOPTI = 0.5. Half the energy to both the heater and cooler.

# A.3 INPUT FOR THE WORKING FLUID VOLUMES

Data for each of the component cells are input using Namelist name CELL. As with the general input, the individual cell values can be split into two categories:

- (1) Integer values input in array II stored in COMMON INCELL.
- (2) Floating-point value input in array AA stored in COMMON FLCELL.

The input format for the GPU-3 sample run is shown in Table A-1. The input module reads the numerical data assigned to the elements of arrays II and AA for each component. It then assigns each element to a particular COMMON BLOCK array whose subscript represents the cell number. The first component is assumed to be the expansion cylinder and the last is the compression cylinder.

The analysis module only uses three of the dead volume cells when determining temperatures, heat flow options, etc. As other modules are developed, more dead volume cells will be used. Therefore, this option is included for all cells, even though not currently used.

The variables and their location in array II are described below.

A.3.1 COMMON INCELL

### $\mathbf{MHTRF} = \mathbf{II}(1)$

Heat-transfer correlation system; allows the user to specify the formula for computing gas-wall heat transfer. Three options:

- 0 Reference formula; the (St,Re) correlation currently available in the heat-transfer subprogram will be used.
- 1 Colburn analogy. Sets Colburn number, j = Fanning friction factor/2.
- 2 Constant value allows the user the option of entering his own value for heat transfer (not currently available).

GPU-3: MHTRF = 0 for all cells.

# MQFLOW = II(2)

Component gas-wall-external environment heat flow; four options

- 0 Wall temperature is constant over all cycles.
- Wall temperature changes with heat flow (typical heater or cooler options).
- 2 Constant gas temperature.
- 3 No net heat flow wall-gas (typically used for adiabatic components).

GPU-3: MQFLO'i = 3 for components 2, 5, 7, 9 and 10. These components are adiabatic (relative to the environment) connecting ducts. Their walls absorb and emit heat, but the sum of such energy transfers is zero for a cycle.

MQFLOW = 1 for components 1, 3, 4, 6, 8, and 11. The SEAMI sample run allowed the cooler wall temperature to vary from cycle to cycle. This in turn caused the regenerator wall temperature to vary, since SEAM1 computes it using the heater and cooler wall temperatures.

$$\mathbf{MTLWAL} = \mathbf{II}(3)$$

Metal type of wall materials; nine options:

7 <b>- Aluminum</b> 2024- <b>T</b> 4	12 - Stainless 310
8 - Copper	13 - Stainless 316
<b>9 - Inconel X-750</b>	14 - Titanium 120-VCA
10 - K MONEL	15 - Nickel

11 - Stainless 304

GPU-3: MTLWAL = 12 for all cells. The power piston was actually SAE 4340 steel, but this was not available as an option.

### MTLWIR = II(4)

Metal type for regenerator filler. Same options as MTLWAL.

GPU-3: MTLWIR = 11 for cell 6, MTLWIR = 0 for all others.

# MTYPE = II(5)

Component description; all cells fall into one of four categories:

Heat Exchanger

10 - Heater or cooler cylinder or tube

11 - Heater or cooler rectangular duct

Connecting Duct

- 15 Cylindrical
- 16 Rectangular
- 17 Orifice

Variable Volume (21 and 22 are typically used in gamma and free piston designs)

20 - Cold

21 - Displacer side cold

22 - Piston side cold

25 - Hot

Regenerator

- 30 Screen
- 31 Sphere
- 32 MET NET
- 33 Corrugated metal (rectangular tubes)
- 34 Round tube matrix

NIHX = II(6)

Number of units of this type per expansion-compression unit. Each tube or duct in a heater or cooler is considered 1 NIHX.

GPU-3: NIHX = 1 for cells 1 and 11; expansion and compression spaces will always have this value by definition. NIHX = 40 for cells 2, 3, 4, and 5 (heater tubes) NIHX = 8 for cells 6 and 10; regenerators and cooler-tocompression space ducts. NIHX = 312 for cells 7, 8, and 9 (cooler tubes).

$$NOPT1 = II(7)$$

Optional input variable; meaning depends on analysis module used. Not used by SEAMI.

GPU-3: NOPT1 = 0 for all cells; need not be input.

# NCEL = II(8)

Number of computational cells that this component is divided equally into; this value is not saved in common.

- GPU-3: NCEL(6) = 5 (regenerator); NCEL = 1 for all other cells. Currently the expansion and compression spaces can only be one cell in length.
- A.3.2 COMMON FLCELL

Common FLCELL contains the mnemonics for array AA. For brevity,

actual values from the GPU-3 sample for each variable and each cell have been left out of the descriptions below; they are included in the input-data printout (Table A-1) in SI units.

$$AFLOW = AA(1)$$

Gas flow area with its normal parallel to the axis of the component. In a regenerator, AFLOW = SIGMA \* Duct Frontal Area; this gives the minimum flow area that is used in the heat-transfer and friction correlations. If AFLOW is not input, it will be computed, provided either the hydraulic diameter (DH) or the combination of the volume (VOL) and length (XLNGTH) is input. In the variable volumes, the flow area must be input. The AFLOW value is per NIHX.

GPU-3 The area of the displacer rod was subtracted from the total cross-sectional area for the compression space AFLOW. All other AFLOW values were direct area calculations as described above and are explicitly input.

# ASPECT = AA(2)

Ratio of the short side to the long side of a rectangular duct; used in heat-transfer and friction calculations.

GPU-3: Not input; no rectangular ducts.

# AXWALL = AA(3)

Cross-sectional area of the wall, used for axial heat conduction calculations. Values are not needed from the cooler cell to the compression cell as these walls are approximately at the cooler temperature. In the regenerator, AXWALL corresponds to the casing, not the filler. All AXWALL values are per NIHX. The code assumes that the temperature varies linearly in space and that the conductivity varies linearly with temperature. An appropriate cross-sectional area for heat flow is needed for variable area walls.

GPU-3: Inner and outer wall diameters were available for all cells (Fig. A-6 and Ref. [47]).

### AWET = AA(4)

Wetted area used for wall to gas flow; if not input, computed from VOL and DH. For expansion and compression zones, AWET is determined at maximum volume, not including the wetted area within the piston-cylinder wall gap. AWET is per NIHX.

GPU-3: Expansion space: AWET(1) = stroke\*perimeter + displacer head area + cylinder dome area - heater tube inlet area. Compression space (at full stroke): AWET(11) = cylinder wall area + connecting rod area + piston head area + displacer bottom area -- cooler tube inlet area. <u>Regenerator</u>: AWET(6) = 0.0, left to be calculated. All other cells were tubes or ducts: AWET = perimeter\*length = 4 Vol/D<sub>h</sub>.



Fig. A-6. GPU-3 Dimensions for Heat Conduction

# DH = AA(5)

Mean hydraulic diameter. If not input, calculated from VOL and AWET. For screen regenerators, DH = (porosity\*wire diameter)/(1-porosity); (Ref. [33] pp. 8 and 25). (For METNET regenerators, Ref. [34], Section 6.004, p. 26).

GPU-3: A piston rod passed through the compression space, and a screened regenerator was used; DH for these two cells was computed as mentioned above. For all other cells, DH = actual diameter.

# FRICML = AA(6)

Friction multiplier, used to account for differences between the available friction correlations and actual conditions (i.e, reversing flow modeled as steady flow). If FRICML = 1.0, the correlations in the friction subprogram (HTS) are not altered. If FRICML = 0.0, there will be no flow friction in that component. The default value is 1.0.

GPU-3: In the regenerator, FRICML(6) = 2.0 to attempt to model the friction loss of the GPU-3 regenerator. FRICML = 1.0 for all other cells.

$$HCEXT = AA(7)$$

External film heat-transfer coefficient. Used with TCMBST, TWATER, TWENVR, and QFLOW (if MQFLOW < 2); for determining outer-wall temperature or environment-to-wall heat flux. If HCEXT = 0. for a cell, either TCMBST (if heater cell), TWATER (if cooler cell), or TWENVR (if any other cell) is assumed to be the cell's outer-wall temperature. The same result is obtained if HCEXT is very large.

GPU-3: HCEXT =  $3000.0 \text{ W/(m}^2 \cdot \text{K})$  for cooler cell 8; used with TWATER and the calculated heat flow to find TWALL(8). HCEXT = 0.0 for all other cells. TCMBST was the heater outer-wall temperature from test results (Ref. [46]). For all other cells, no heat flux to the environment is calculated by SEAM1.

# ORIFICE = AA(8)

Orifice coefficient (see MTYPE = 17); used to account for pressure-drop losses caused by orifices commonly found in test engines. It is not to be used for expansion and contraction losses between components; those are accounted for in the friction-factor portion of the heat-transfer subprogram.

GPU-3: ORIFCE = 0.0 for all cells; no orifices.

$$PGAS = AA(9)$$

Initial gas pressure. If not input, computed either from total mass and the sum of the volumes or from PMEAN; in such a situation, all cell pressure will be equal.

GPU-3: PGAS = 0.0 Pa, for all cells.

### POROS = AA(10)

Porosity = (void volume)/(total volume); for regenerator filler material or MTLWIR. If MET NET, use POROS = 1.0 - filler factor. Not the same as SIGMA, POROS gives average flow area and should be used with average flow velocity in friction and heat-transfer calculations.

GPU-3: POROS = 0.697

# QFLOW = AA(11)

External wall surface to environment heat flux; used with TCMBST, TWATER, and TWENVR when MQFLOW = 1. This allows a constant heat flux to be input. If 0.0, then heat flow will be computed.

GPU-3: 
$$QFLOW = 0.0 W$$
, for all cells.

# SIGMA = AA(12)

Minimum flow area/frontal area for regenerator. Less than or equal to porosity; used with maximum velocity in heat-transfer and friction correlations. For screen regenerators, SIGMA = (1-mesh\*wire dia.)\*\*2; (Ref. [33]).

GPU-3: SIGMA = 0.468 using the screen formula above.

# TGAS = AA(13)

Design-point initial gas temperature; if not input, TGAS = TWALL. Either TGAS or TWALL must be input.

CPU-3: TGAS = 0.0 K for all cells; set equal TWALL.

$$TWALL = AA(14)$$

Design-point inner-wall temperature; constant within any one cycle for SEAM1. TWALL = TGAS if set to 0 or not input. Only TWALL in the heater and cooler is used by the SEAM1 analysis module. However, approximate values for the other cells are needed because the input processor computes the initial system mass (TMASS) with them if it was not input. Regenerator filler is initialized to regenerator wall temperature.

GPU-3: Cells 1-5 were assigned the experimental heater temperature (TCMBST) and cells 7-11 were assigned the cooler temperature. Regenerator cell 6 was set at the average of the two. In the test engine, heater temperature changed as the frequency was varied (Ref. [46]). To match this situation in the sample run, TCMBST was varied with frequency (Table A-1).

$$VOL = AA(15)$$

Gas volume or total displacement. The expansion and compression volumes need not be input here; they are variable and either their time-dependent values are computed by the volume subprogram or the user can replace this subprogram with a different method. If other cells are not input, they will be calculated from AFLOW\*XLNGTH. If known, VOL values should be input since AFLOW\*XLNGTH may not include all the dead volume for that cell.

GPU-3: All values were taken from Table 2 of Ref. [46] and are listed below:

Component Cell	Volume (m <sup>3</sup> )
1	0
2	(9.68E-6)/40 = 2.42E-7
3	$\frac{(47.46 + 7.67)(E-6)}{2(40)} = 6.891E-7$
4	6.891E-7
5	$\frac{(13.29 + 2.74 + 7.36)(E-6)}{40} = 5.848E-7$
6	$\frac{5.3E-5}{8} = 6.68E-6$
7	$\frac{(2.59 + 2.18)(E-6) + (4.838E-9)}{312}$
8	$\frac{1.313E-5}{312} \frac{3.55}{4.61} = 3.241E-8$
9	$\frac{1.313E-5}{312} \frac{(4.61 - 3.55)}{2(4.61)} = 4.838E-9$
10	$\frac{(3.92 + 2.77 + 3.56)(E-6)}{8} = 1.281E-6$

0

### VOLWL = AA(16)

Volume of wall material used in wall-temperature calculations; if not input, computed from AXWALL\*XLNGTH. Not presently used.

GPU-3: Both XLNGTH and AXWALL were approximated to compute VOLWL (10) for the irregularly shaped connecting duct. Compression space VOLWL(11) was assumed to equal expansion space VOLWL(1). All other cells were computed from AXWALL\*XLNGTH. These values we ce input for future use; they are not presently used.

# WALLTH = AA(17)

Wall thickness; used primarily for calculating the heat flow through and temperature gradient across the heater and cooler tube walls. It will be used with the other cells in future applications for heat-flow calculations with the environment. If not input, it is calculated from AXWALL and the wall diameter.

GPU-3: Taken from Table 1 of Ref. [46] for the cooler tubes; not input for the others.

### XLNGTH = AA(18)

Component length; used for heat-conduction calculations and computing VOL, VOLWL, and AFLOW if they are not input. If XLNGTH is 0.0 or not input, it is computed from VOL/AFLOW.

- GPU-3: For expansion and compression spaces, XLNGTH = stroke + clearance. XLNGTH for all other cells came from Table 1 of Ref. [46].
- A.4 INPUT FOR THE ADDED VOLUMES

Information for the added alphabetic cells is input in a manner similar to that for the cells described above. A separate Namelist entry, ADDED, is used for the added cells. Numerical data are entered in arrays JJ (integer) and BB (floating point). The input processor assigns variables to the elements of both arrays and places the JJ values in common IADD, while BB values are put in common FADD.

In engines similar to the GPU-3, which is a displacer design, three added cells are common: A, C, and D (Fig. A-4). However, for this sample run, only cells A and C were input; cell D, the crankcase space, was unspecified in the available data and is not used in the present code. For this run cell l is type A and cell 2 is type C.

A.4.1 COMMON IADD

# IACOND = JJ(1)

Heat-transfer mechanism(s) present between the added cell and the adjacent variable volume. Three options:

- 0 no heat transfer
- 1 only conduction
- 2 conduction and radiation (e.g., hollow displacer)

Only options 0 and 1 are presently used. No radiation transfer is calculated.

GPU-3: IACOND(1) = 2; heat transfer in the hollow displacer is both by conduction down the wall and radiation to the compression space. The conduction only is presently calculated.

IACOND(2) = 1; conduction paths exist from the compression zone to the buffer space via the compression piston and cylinder walls. Heat flow along these paths is generally negligible due to the small temperature gradient and hence is not included.

IALEAK = JJ(2)

Leak condition between added and variable volumes; four options:

- 0 no leaks
- 1 gas leakage in both directions
- 2 gas leakage into the added volume only (unidirectional)
- 3 gas leakage out of the added volume only

Gas leakage is not presently computed. This option is intended for later code versions.

GPU-3: IALEAK = 1 for both added cells; input for future use. Gas leakage between the expansion space and the displacer is the result of a small pressure release hole in the displacer side; this hole allows the pressure inside the displacer to be near equilibrium with the expansion space pressure, thus relieving stress on the displacer wall. Flow through the hole during a cycle is assumed to be insignificant due to its small (unspecified) size. Leakage between the compression space and buffer space C occurs past the piston rings.

$$IAMTL = JJ(3)$$

Wall material; same nine options as MTLWAL. Used prsently for determining conduction properties.

- GPU-3: IAMTL(1) = IAMTL(2) = 12; stainless 310.
  - Note: IAMTL(2) refers to the wall material surrounding buffer space C, not to the material the power piston is made of.

$$IATYPE = JJ(4)$$

Component description; four options:

10 - piston dome or displacer (volume A)

20 - cold piston buffer space (volume C)

- 25 hot piston buffer space (volume B)
- 40 crankcase (volume D)

Not all added volumes are common to each design (Figs. A-2, A-3, and A-4).

GPU-3: Of the three IATYPES that are common to design 3, 10, 20, and 40, IATYPE = 10 for cell 1 and 20 for cell 2 were used. IATYPE 25 is not used in design 3 engines because the displacer is bounded by the expansion and compression zones.

NRINGS = 
$$JJ(5)$$

Number of rings in leakage calculations; not used by SEAMI.

GPU-3: NRINGS(1) = 0; leakage from the expansion space to the compression space past the displacer rings is not evaluated.

For displacer leakage see IALEAK.

NRINGS(2) = 2 for the power piston.

$$NSHELD = JJ(6)$$

Number of radiation shields in displacer A (IATYPE = 10); primarily for IDESGN = 3. Not presently used.

- GPU-3: NSHELD(1) = 2.
- A.4.2 COMMON FADD

### ADPGAS = BB(1)

Gas pressure in added cell; buffer space pressure will be used for torque calculations in future versions. ADPGAS for all cells will be used in future leakage calculations. If not input, it is set equal to PMEAN.

GPU-3: ADPGAS(1) = 0.0 Pa. If needed, it would be approximately the same as the expansion space pressure.

ADPGAS(2) = 3.23E6 Pa; Ref. [46].

$$ADRADA = BB(2)$$

Radiation surface area term for inside the displacer (engines with IDESGN = 3); ADRADA = shape factor\*surface area. Intended use:

q = 
$$\sigma A_1 F_{12} \left( T_1^4 - T_2^4 \right) = \sigma (ADRADA) \left( T_1^4 - T_2^4 \right).$$

Not presently used.

GPU-3: ADRADA(1) =  $0.0 \text{ W/K}^4$ .

# ADTGAS = BB(3)

Gas temperature inside added volume at the start of the cycle.

GPU-3: ADTGAS for A and C was set equal to the expansion and compression space temperatures, respectively; for use in later versions.

# ADVOL = BB(4)

Gas volume; if variable, maximum used. <u>Note</u>: The displacer volume is not considered part of the dead volume.

GPU-3: ADVOL(1) calculated from dimensions (Fig. A-6) (assuming displacer dome was flat).

ADVOL(2) from Table 1 of Ref. [47].

# ADWALX = BB(5)

Effective length for axial conduction along displacer (.ATYPE = 10); generally assumed to be the displacer length. In an in-line design, ADWALX is the length used for axial wall conduction from the expansion zone to the hot buffer space.

GPU-3: Displacer length (Fig. A-6).

ADWLDI = BB(6)

Wall inner diameter; for use with ADWLTH in heat-conduction calculations.

GPU-3: Inner displacer diameter and piston cylinder bore (Table 1 of Ref. [41]).

ADWLTH = BB(7)

Wall thickness; for heat-conduction calculations.

GPU-3: ADWLTH(1) from Table 1 of Ref. [46].
ADWLTH(2) approximated as minimum expansion cylinder wall
thickness (Fig. A-6).

$$EMIS = BB(8)$$

Emissivity of radiation shields in displacer; not currently used by SEAMI.

GPU-3: 0.3.

# RINGCL = BB(9)

Clearance between ring and wall; no leakage is possible unless RINGLK > 0.0. Not presently used.

GPU-3: Not input.

# RINGFR = BB(10)

Ring friction coefficient. Typical values: 0.15 = plastics, 0.8 = metals.Not presently used.

GPU-3: RINGFR(2) = 0.15.

### RINGHT = BB(11)

Ring height; not presently used.

GPU-3: 0.002 m.

### RINGLK = BB(12)

Ring-leak coefficient; not presently used. If input as 0.0 in later versions, then it will be calculated from RINGCL, RINGHT, NRING, gas properties, and laminar flow through an annulus.

GPU-3: Not used.

# SLNGTH = BB(13)

Effective length for shuttle heat-transfer calculation in IDESGN = 3 engines, usually displacer stroke (Ref. [27], p. 129).

GPU-3: Displacer stroke (Table 1 of Ref. [46].

A.5 PERTURBATION INPUT

All of the previous input information can be thought of as a description of the design point conditions. To allow the user an easy method of seeing the effect of changes, two perturbation options are included: a batch and an interactive technique. The batch technique can be used to generate engine maps where many cases are generated, and the interactive technique to modify geometry. With both systems the user may change any of the previous inputs and execute the new case (see Table A-1).

Two previously described integer variables control the input and output: ICHNG and NPRT2.

# ICHNG; Five Options

0 - The current case will be the last case to be executed.

- 1 An additional case will be run, the data changes will follow the base input deck.
- 2 The added case requires reinitialization of the input, used for changes to variable volume input (see subroutine INITAL).
- 3 An additional case will be run, the data changes will come from logical unit 10. This allows for interactive input (see Section A.5.2).
- 4 Interactive added case requires reinitialization.

- -N N is 1-4 as above; the negative indicates a full input edit is desired for the added case.
- GPU-3: In the base data input, ICHNG is set to 1. It remains 1 until the last case, where it is then set to 0.

# NPRT2

The number of cases to be compared on the output and graphically displayed as group.

GPU-3: NPRT2 = 6, because six frequencies were run.

### A.5.1 Additional Input Options

All data modifications are input through the namelist block PERTIN. All cell variables are input by their used name and actual cell location, as displayed by the input editor. For example, AWET(15) is the wetted area in the compression zone in the sample problem. In addition to all the previously mentioned input names related to common blocks IGEN, FLTGEN, INCELL, FLCELL, FADD, and IADD, six additional variables have been added:

#### NMODS

The number of cases in this perturbation group. This allows the variation of frequency, combustion temperature, and stroke ratio to be input easily. It allows the user to run a 24-case engine map as four pressure runs with six frequency changes instead of 24 pressure-frequency combinations.

GPU-3: In the first group it is set to 6 for the six speed settings. In the next three groups, it is set to 1 because neither frequency nor stroke ratio is to be varied.

# ITWLCH; Two Options:

- 0 no modification of combustion temperature
- 1 modification of combustion temperature with case
- GPU-3: In the first group it is set to 1 and values for TWLHI are input.

### DFREQ

The incremental change in frequency in a perturbation run (cycles/sec).

GPU-3: It is set to 8.33; therefore the frequency varies from the initial 16.67 to 58.32 Hz in six intervals. In the second perturbation group, it is set to 0.0 as NMODS was set to 1. Note that the base frequency was also input in the second group, the default value is the initial value of 16.67 Hz.

### DSTRK

The incremental change in stroke ratio in a perturbation run. In many free piston designs, the frequency is fixed and the displacer to power-piston stroke ratio is varied to change the power. This is not a percentage change, but rather an absolute change in the ratio.

GPU-3 not used

# TWLHI

The combustion temperature for each case. Only input if ITWLCH is greater than 0.

GPU-3 Set to outer-wall temperatures given in test results (see Ref. [46]).

# A.5.2 Interactive Perturbations

To help the designer perfect his device, the code allows an interactive session. The cases run in this manner will still edit the results as discussed in Sec. 4.6 for the system printer, logical unit 6. In addition, selected variables will be displayed on logical unit 11. We normally assign units 10 (interactive input) and 11 to the terminal. The output is determined in subroutine OUT1 and currently displays:

- Engine Speed
- Total Heat In
- Total Heat Out
- Total Heat Recovered
- Engine Efficiency
- Cooler Gas Temperature
- Heater Gas Temperature

A typical session is shown in Table A-3; this session followed the first seven cases shown in Table A-1 by changing the value of ICHNG to 3 in case 7.

# A.6 SAMPLE INPUT DECK

A copy of the sample problem input is shown in Table A-1. The input was prepared from worksheets similar to those shown in Table A-2.

The input is for the GPU-3 engine and corresponds to the hydrogen cases in Table VII. In the sample problem the code predicts power, efficiency, etc. for six speed settings at 2.74 MPa. Case 7 is a duplicate of the 3500 rpm speed setting with some internal prints turned on. Case 8 is a duplicate of Case 7 with the total gas mass fixed instead of the more common mean pressure being held constant. The values for wall and gas temperatures are input to reduce the number of iterations. The final case is a duplicate of Case 8 with added final prints turned on.

GPU-3 HYDROGEN 9271	K <b>/339K ST</b> I	IRLING E	GINE	DATA:	1 (UPDATED	JAN 83)
7GINPT	ICHNG=1		IDESG	N=3,		IDRIVE=1,
ICAS=1,	IPRT1=0,		IGRAP	H=1,		NADD=2,
NCOMP=11	NPRT2=6,		NCYL=	1,		NOPT=1,
NPRT1=720,	NREVL=12,		NSTEP	=360,		
CMPCR=.0138,	CMPCRL=.0460	),	CMPDV	<b>-1.093</b>	E−5,	CMPECC=.0208,
CMPGAS=.00015,	CMPRD=.0222	•	EXPCR	<b></b> 0138	,	EXPCRL=.0460,
EXPDV=1.25E-5,	EXPECC=.0208	3,	EXPGA	s=.000	25,	EXPRD=.00952,
FREQ=16.67,	PMEAN=2.74E	5,	START	D=0.,		REGHT=0.0286,
TCMBST=890.0,	TWATER=287.	•	ZOPTI	=0.5,		
& END						
* EXPANSION SPACE						
& CELL	II <b>-</b> 0,	1,		12,		0
	25,	1,		0,		1,
AA=3.86E-3	0.0,	1.07E-3	,	1.43E	-2,	.0701,
1.0,	7*0.,	927.,		0.,	-	3.54E-5,
0.,	3.312E-2,	<b>&amp;END</b>				
*						
EXPANSION SPACE TO	HEATER					
&CELL	II=0,	3,		12,		0,
	15,	40,	_	0,		1,
AA=7.16E-6,	0.0,	1.116E-	5,	3.67E	-4,	3.02E-3,
1.0,	7*0.,	927.,		2.42E	-7,	4.32E-7,
0.,	.0397,	<b>&amp;</b> END				
HEATER (TURES IN +	1/2 HEADER)					
LCRIT.	TTen	1		12		0
	10	40		0		· ,
AA=7.16E-6.	0.0.		5.	7.37E	-4	1, 3,02F-3
1.0.	7*0.	927.	.,	6.891	E-7.	8.67E-7.
0.0.	0777.	<b>&amp;END</b>			_ ,	
*	· · · · · <b>,</b>					
HEATER (1/2 HEADER	+ TUBES DOWN	N)				
& CELL	II=0,	1,		12,		0,
	10,	40,		0,		1,
AA=7.16E-6,	0.0,	1.116E-	5,	7.37E	-4,	3.02E-3,
1.0,	7*0	927.,		6.891	E-7,	8.67E-7,
0.0,	.0777,	<b>GEND</b>				
HEATER TO REGENERA	TOR	•		••		•
ACELL	11=0,	3,		12,		0,
AA-7 168-6	12,	40,	E	U,		1,
AA-/.10E-0,	740	1.1106-	,	4.80E	-4,	3.U2E-3,
1.0,	0512	72/•) ERND		2.848	2-/,	J•/18−/,
*	.0312,	g LND				
RECENTRATOR						
&CELL	II=0.	1.		12.		11.
	30,	8,		0.		5.
	•	-				•

TABLE A-1. Sample Problem Input for GPU-3 Example

AA=1.88E-4,	0.0,	1.322E-4,	0.,	9.35E-5
Z•,	3ru,	.697,	U., 2.00F (	.468,
0.226	034., (FND)	0.08L-0,	2.996-0,	V.,
•0220,	GEND			
DECENEDATOD TO COO				
LOFIT	TT=A	3	12	0
accel	11-0,	J, 312	1 <b>2</b> ,	0, 1
AA=9 16F-7	1,	1 070F-6	∨, 1.80F-5	1, 3 ()8F-3
1.0	7 <b>*</b> 0	339	2.013F-8	5.678-9
2 55F-4	0053	Δ59., &FND	2.0155 0,	5.072 9,
*	.0055,	<b>ULIND</b>		
COOLER				
&CELL	II=0.	1.	12.	0.
	10.	312.	0.	1.
AA=9.16E-7.	0	1.070E-6.	1.20E-4.	1.08E-3.
1.0.	3000 .	6*0.	339.	3.241E-8.
3.80E-8.	2.55E-4.	.0355.	& END	,
*	•			
COOLER TO CONNECTI	NG DUCT TUBE	S		
&CELL	II=0,	3,	12,	0,
	15,	312,	0,	1,
AA=9.16E-7,	0.0,	1.07E-6,	1.80E-5,	1.08E-3,
1.0,	7*0.,	339.,	4.838E-9,	5.67E-9,
2.55E-4,	.0053,	&END		
*				
CONNECTING DUCTS				
& CELL	II=0,	3,	12,	0,
	15,	8,	0,	1,
AA=2.80E-5,	0.0,	3.8E-5,	0.0,	5.97E-3,
1.0	7*0.,	339.,	1.281E-6,	1.20E-6,
0.,	3.18E-2,	&END		
*				
COMPRESSION SPACE				
&CELL	II <b>-</b> 0,	1,	12,	0,
	20,	1,	0,	1,
AA=3.77E-3,	0.0,	3.8E-5,	1.52E-2,	6.04E-2,
1.0,	7*0.,	339.,	0.0,	3.54E-5,
0.,	3.18E-2,	<b>&amp;END</b>		
*				
DISPLACER DOME				
& ADDED	JJ=2,	1,	12,	10,
	0,	2,		
BB=2*0.,	890.,	1.66E-4,	.04359,	.06642,
.00159,	0.3,	4 <b>*</b> 0,	.04359,	& END
*				
POWER PISTON BUFFE	R SPACE			_
& ADDED	JJ=2*1,	12,	20,	2,
	σ,	<b></b>		
BB=3.23E+6,	С.,	315.,	<b>5.21E-4</b> ,	U.,
.0701,	.00381,	2*0.,	·15,	.002,

TABLE A-1. Sample Problem Input for GPU-3 Example (Contd.)

TABLE A-1. Sample Problem Input for GPU-3 Example (Contd.) **&END** \* SINGLE PRESSURE MAP RUN CHANGING TCMBST....CASES 1-6 &PERTIN DFRE0=8.33. NMODS=6. ITWLCH=1, TWLHI=890., 899.0, 909.0, 918.0, 927.0, 937.0, 4\*0.0, & END \* LAST RPM WITH ADDED CYCLE PRINTS....CASE 7 **&PERTIN** DFREQ=0.0, NMODS=1. ITWLCH=0, TCMBST=937.0, FREQ=58.3, IPRT1=2, ICHNG=2, &END × NOTE THAT ICHNG IS A 2 TO REINITIALIZE CASES 8 AND 9 \* SAME CASE WITH THE MASS FIXED AND PMEAN VARIABLE....CASE 8 MASS AND TEMPERATURE VALUES ARE FROM CASE 7 FOR THIS EXAMPLE &PERTIN IPRT1=2, IMASS=1, TMASS=3.263E-4, PGAS(1)=15\*0.0, TGAS(1)=5\*887.77,5\*578.45,5\*351.28, TWALL(1)=887.77,4\*932.61 5\*627.96,4\*323.30,351.28, **&END** SAME CASE WITH ADDED FINAL PRINTS....CASE 9 &PERTIN IPRT1=4. ICHNG=0, & END × NOTE THAT ICHNG IS 0, FINAL CASE IS CASE 9

# TABLE A-2. Worksheet for Namelist CELL

	1	2	3	4	5	6	7	8
INCELL (II)	EXP. SPACE	CONNECT. DUCT	HEATER	REGEN	ERATOR	COOLER	CONNECT. DUCT	COMP. SPACE
MHTRF 1								
MQ <b>FLOW</b> 2								
MTLWAL 3			Ţ		·			
MTLWIR 4								
MTYPE 5								
NIHX 6								
NOPTI 7								
NCELLS 8								

# COMMON INCELL

# COMMON FLCELL

	1	2	3	4	5	6	7	8
FLCELL (AA)	EXP. SPACE	CONNECT. DUCT	HEATER	REGEN	IERATOR	COOLER	CONNECT. DUCT	COMP . SPACE
AFLOW 1								
ASPECT 2								
AXWALL 3								
AWET 4								
DH 5								
FRICML 6								

TABLE A-	2. Worksh	eet for	Namelist	CELL	(Contd.)	
----------	-----------	---------	----------	------	----------	--

	1	2	3	4	5	6	7	8
FLCELL (AA)	EXP. SPACE	CONNECT. DUCT	HEATER	REGEN	IERATOR	COOLER	CONNECT. DUCT	COMP. SPACE
HCEXT 7								
ORIFCE 8								
PGAS 9								
POROS 10								
QFLOW 11								
SIGMA 12								
TGAS 13								
TWALL 14								
WALLTH 15								
VOL 16			·					
VOLWL 17								
XLNGTH 18								

# TABLE A-3. Sample Interactive Session

RUN TERMINAL FI 6 DISK OUTPUT DATA FI 5 DISK TERMINAL DATA FI 8 DISK PLOT DATA FI 9 DISK DUMMY DATA FI 10 TERMINAL FI 11 TERMINAL LOAD SEAM RIOS START EXECUTION BEGINS... CASE NUMBER 1 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 1000.2 6745.8 2760.2 -3985.1 0.409 327.297 843.071 CASE NUMBER 2 QIN POWER QOUT EFFIC TGAS KOL TGAS HOT RPM 9404.8 3863.4 -5541.1 0.411 340.073 848.927 1500.0 CASE NUMBER 3 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 11955.5 4769.0 -7186.5 0.399 353.219 856.177 1999.8 CASE NUMBER 4 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 2499.6 14371.5 5445.9 -8925.6 0.379 366.870 862.895 CASE NUMBER 5 QIN POWER QOUT EFFIC TGAS KOL TGAS HOT RPM 15643.7 5889.8 -10753.9 0.354 381.061 870.017 2999.4 CASE NUMBER 6 POWER QOUT EFFIC TGAS KOL TGAS HOT RPM QIN 18774.5 6100.9 -12673.7 0.325 395.840 878.457 3499.2 NEXT DATA CHANGE FOR INTERACTIVE RUNNING? AWET (12)=2.4E-4MORE INPUT? Y=YES N=NO Ν CASE NUMBER 7 POWER QOUT EFFIC TGAS KOL TGAS HOT RPM QIN 1000.2 6855.6 2877.4 -3978.2 0.420 316.189 842.589 CASE NUMBER 8 QIN POWER QOUT EFFIC TGAS KOL TGAS HOT RPM 1500.0 9584.7 4055.2 -5529.2 0.423 327.486 848.312 TABLE A-3. Sample Interactive Session (Contd.)

CASE NUMBER 9 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 1999.8 12210.2 5040.0 -7169.9 0.413 339.265 855.444 CASE NUMBER 10 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 2499.6 14698.1 5801.8 -8896.1 0.395 351.583 862.082 CASE NUMBER 11 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 2999.4 17049.3 6331.2 -10718.2 0.371 364.467 869.105 CASE NUMBER 12 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 3499.2 19263.4 6627.2 -12636.2 0.344 377.948 877.440 NEXT DATA CHANGE FOR INTERACTIVE RUNNING? ICHNG=0 MORE INPUT? Y=YES N=NO Y NEXT DATA CHANGE FOR INTERACTIVE RUNNING? NMODS=0 MORE INPUT? Y=YES N=NO N CASE NUMBER 13 RPM QIN POWER QOUT EFFIC TGAS KOL TGAS HOT 1000.2 6855.6 2877.4 -3978.2 0.420 316.189 842.589 PRINT OUTPUT DATA (CC PRINT TERMINAL DATA R: T=21.81/23.08 16:38:21

# A.7 SAMPLE OUTPUT

Appendix B shows the output printout that was generated on unit 6 by running the code with the GPU-3 input deck of Sec. A-6. To avoid further reductions in size we have truncated the output beyond column 90. This should only effect the pages with added prints and little information should be lost. The total execution time for the nine cases was less than 20 sec on an IBM 3033. Less than 200K bytes (50K words) of core storage were required for the object code and common blocks.

# A.8 GRAPHICS CAPABILITY

As mentioned in Sec. 2.5, the Output routine OUT1 writes certain graphics information on output device 8. The nature of the information written depends on the value of IGRAPH. Since graphics systems are installation-dependent, the data are written in "raw" form, and are therefore up to the user to read the data and use them in a way compatible with their own graphics system. Currently, at ANL, a Fortran program GRAF (Appendix D) is being used for the case-to-case results. The program was used to generate the three map displays discussed in Sec. 4. In addition to these displays the code generates two power-versus-RPM curves (Figs. A-7 and A-8). The first graph displays separation of cooler heat flow, power out and losses versus RPM. The second graph displays the major loss mechanisms in a Stirling engine versus RPM. The code uses the SEAMI graphics output, read in through logical unit 10, and generates a file on logical unit 11 that the proprietary package "TELLAGRAF" uses to generate displays. A listing of the logical unit 11 file is included as Appendix E.

This section describes the graphics information that is written on the output file by OUT1. The appropriate Format statements can be found in the code listing for OUT1. Also, definitions of the variables used below appear in Appendix C.

A.8.1 IGRAPH = 1

If IGRAPH = 1, the following information is written on unit 8 after the final cycle.

- NTITLE
- NCASE, engine speed, mean pressure (PMEAN), combustion temperature (TCMBST), gas mass (TMASS), Schmidt Analysis ratio (SCHDEL) and phase angle (THETA), and compression zone minimum crank angle (PSIMIN)
- (GRAFIC(L, I), I = 1, 75), L = 1, 9 for I = 1, 2, ..., 73

GRAFIC(1,I) = the Ith angle 5°, 10°, ..., 360°
GRAFIC(2,I) = expansion live volume at angle I
GRAFIC(3,I) = pressure at angle I
GRAFIC(4,I) = compression live volume at angle I
GRAFIC(5,I) = compression live mass at angle I



Fig. A-7. GPU-3 Power Flow Comparisons



Fig. A-8. GPU-3 Power Loss Comparison

GRAFIC(6,I) = expansion live mass at angle I
GRAFIC(7,I) = crankshaft torque at angle I
GRAFIC(8,I) = cooler gas temperature at angle I
GRAFIC(9,I) = heater gas temperature at angle I

```
and for I = 74,75
```

GRAFIC(L,I) is undefined.

A.8.2 IGRAPH = 2

If IGRAPH = 2, the following information is written on unit 8. The purpose is to provide graphs that show the case-to-case variation of the SEAML code predictions.

Written once for each NPRT2 case:

- NTITLE
- IMASS, engine speed (rpm), PMEAN, TCMBST, TWATER, gas mass (kg) written for each case
- NCASE
- Average pressure (MPa)
- Engine speed (rpm)
- Gas mass (kg)
- Energy flow into heater (kW)
- Net power (kW)
- Efficiency
- Heater gas temp. (K)
- Cooler gas temp. (K)
- Cooler wall to gas heat flow (negative) (kW)
- Conduction losses to cooling water (kW)
- Static conduction losses (kW)
- Dynamic conduction losses (shuttle + gap) (kW)
- Fluid friction losses (kW)
- Regenerator reheat loss (kW)
- Gas leakage loss (= zero for SEAM1) (kW)
- Total heat flow out (kW)

### A.9 OBTAINING THE CODE FROM NESC

A copy of the ANL Stirling Engine Analysis System Fortran code can be obtained on tape from the National Energy Software Center (NESC) located at
ANL. A nominal service fee may be charged by NESC. This report is part of the user documentation sent by NESC with the code. The address and phone number of NESC are:

National Energy Software Center, Bldg. 221 Argonne National Laboratory 9700 South Cass Avenue Argonne, Illinois 60439

Telephone: (312) 972-7250

## APPENDIX B GPU-3 SAMPLE PROBLEM OUTPUT

### GPU-3 HYDROGEN 927K/339K STIRLING ENGINE DATA: 1 (UPDATED JAN 83)

### THIS RUN STARTED AT TIME 11.33.22

#### EDIT COMMON IGEN FOR RUN NUMBER 1

0-NO CHANGES TO CELL INFORMATION 1-CHANGES TO BE MADE	1
1-IN-LINE 2-DOUBLE ACTING 3-DISPLACER	3
0-CONNECTING ROD 1-RHOMBIC DRIVE 2-DYNA. ANALYSIS(NA)	1
HORKING FLUID TO BE USED	1
1-H2 2-HE 3-N2 4-AIR 5-CO2 6-CH4	
0=PHEAN IS CONSTANT, 1=TMASS IS CONSTANT	0
0-FRICTION ONLY MOMENTUUM EQUATION	0
1-FULL NOHENTUUM EQUATION	
0-STANDARD PRINT >0-CODE DEPENDENT ADDITIONAL PRINTS	0
O NO GRAFHICS, 1=SAVE CYCLE FILE, 2=SAVE CASE FILE	1
NUMBER OF ADDED COMPONENTS (LETTERED VOLUMES IN DESIGN)	2
O-RIOS 1-UREILI 2-TEW	0
NUMBER OF COMFONENTS (NUMBERED VOLUMES IN DESIGN)	11
NUMBER OF CYLINDERS IN ENGINE	1
COOLER GAS HEAT FLOW OPTION	1
NURBER OF STEPS/PRINT OF ZONE INFORMATION	720
NUMBER OF CASES/FRINT OF ENERGY FLOW INFORMATION	6
NUMBER OF FULL REVOLUTIONS TO BE CALCULATED(CYCLES)	12
NUMBER OF TIME STEPS IN 1-REVOLUTION	360

#### EDIT COMMON FLTGEN

COMPRESSION PISTON CRANK RADIUS (H)	0.01320
COMPRESSION PISTON CONNECTING ROD LENGTH (N)	0.04500
COMPRESSION ZONE DEAD VOLUME (CU M)	1.093E-05
COMPRESSION PISTON CRANK RADIUS ECCENTRICITY (M)	0.02800
COMPRESSION PISTON-CYLINDER WALL GAP (M)	0.00015
COMPRESSION PISTON ROD DIAMETER (M)	0.02220
EXPANSION PISTON CRANK RADIUS(M)	0.01330
EXPANSION PISTON CONNECTING ROD LENGTH (M)	0.04600
EXPANSION ZONE DEAD VOLUME (CU M)	1.2502-05
EXPANSION PISTON CRANK RADIUS ECCENTRICITY (M)	0.02020
EXPANSION PISTON-CYLINDER HALL GAP (M)	0.00025
EXPANSION PISTON ROD DIAMETER (M)	0.00952
FREQUENCY OF SYSTEM (CYCLES/SEC)	16.67
THERMAL HYSTERISIS FACTOR	0.0
VOLUME PHASE ANGLE (DEGREES)	110.35
PISTON PHASE ANGLE (DEGREES)	0.0
AVERAGE PRESSURE OF SYSTEM IN CYCLE (PA)	2.740E+06
CRANK ANGLE AT TIME = 0.0 (DEGREES)	0.0
DISTANCE BETHEEN TOP OF REG. AND BOTTOM OF CYL. DOME	0.02860
EXTERNAL HEATER TEMPERATURE	890.00
EXTERNAL COOLER TEMPERATURE	287.00
TOTAL MASS IN CONTIGUOUS SYSTEM (KG)	3.886E-04
EXTERNAL ENVIRONMENT TEMPERATURE	300.00
CODE DEPENDENT OPTION ZOPT1	0.50
TIME STEP (SEC)	1.666E-04

GPU-3 HYDROGEN	927K/339K	STIRLING	ENGINE	DATA:	1	UPDATED	JAN 831

#### EDIT MOST OF COMMON JMISC

FIRST FIXED VOLUME CELL	2
FIRST CELL IN HEATER	3
TYPICAL HEATER VALUES COME FROM CELL	3
LAST CELL IN HEATER	4
FIRST CELL IN REGENERATOR	6
TYPICAL REGENERATOR VALUES COME FROM CELL	8
LAST CELL IN REGENERATOR	10
FIRST CELL IN COOLER	12
TYPICAL COOLER VALUES COME FROM CELL	12
LAST CELL IN COOLER	12
LAST FIXED VOLUME CELL	14
CELL NUMBER OF COMFRESSION ZONE	15
LAST CONTIGUOUS CELL IN SYSTEM	15

#### EDIT CONSION VARVOL

CURRENT CRAME ANGLE (RAD)	0.0
CUMPRESSION PISTUN AREA (SU M)	3.//01-03
CUMPRESSION CYLINDER BORE (M)	0.05973
COMPRESSION ZONE PISTON OVERLAP (M)	0.02120
COMPRESSION PISTCH MAXIMUM STROKE POSITION (M)	0.05607
COMPRESSION PISTON MINIMUM STROKE POSITION (M)	0.02458
COMPRESSION PISTON CURRENT STROKE POSITION (M)	0.04546
COMPRESSION PISTON TOTAL STROKE (CNPHAX-CMPHIN) (H)	0.03149
CONPRESSION ZONE MAXIMUM DISPLACEMENT (CU M)	1.142E-04
CRANK ANGLE BETHEEN TOC OF EXP. & COM. PISTONS(RAD)	0.0
VOLUME PHASE ANGLE (RADIANS)	1.92605
ABSOLUTE ANGLE AT MININUM VOLUME (RAD)	1.57080
ABSOLUTE EXPANSION CRANK ANGLE AT STARTD=0. (RAD)	1.57030
SCHMIDT ANALYSIS PRESSURE RATIO	3.08777
SCHMIDT ANALYSIS PRESSURE PHASE ANGLE (RAD)	0.96302
INCREMENTAL CRANK ANGLE (RAD/SEC)	0.01745
EXPANSION PISTON AREA (SQ M)	3.860E-03
EXPANSION CYLINDER BORE (M)	0.07010
EXPANSION MAXIMUM STROKE FOSITION (M)	0.05607
EXPANSION MINIMUM STROKE POSITIC'L (M)	0.02458
EXPANSION PISTON CUPRENT POSITION (M)	0.04546
EXPANSION PISTON TOTAL STROKE (M)	0 03149
EXPANSION ZONE MAXIMUM DISPLACEMENT (CU M)	1.2158-04
ACTIVE VOLUMES: (CU M) 1	9.311E-05
2	0.0
3	1.093E-05
4	1.487E-06
5	7.065E-05
EDIT COMMON GASPRP	
GAS SPECIFIC HEAT AT CONSTANT PRESURE (1//KG-K)	1.456F+D4
GAS SPECIFIC HEAT AT CONSTANT VOLUME (J/KG-K)	1.043E+04
GAS SPECIFIC HEAT PATTO	1 39529
CAR CONSTANT ( 1/KG-K)	4124 K
UND GUIDINII (J/NU"N)	7167.0

EDIT HEAT EXCHANGER VALUES PER NIHX         - COMMONS INCELL AND FLCELL           CELL         * 1         * 2         * 3         * 4         * 5         * *           MTRF         0         0         0         0         0         0           MTQLOH         =         1         3         1         1         3           MTHAL         12         12         12         12         12           MTHA         1         40         40         40         40         40           NDPT         0         0         0         0         0         0         0           NPT         0         0         0         0         0         0         0         0           AFLOH         3.850E-03         7.160E-06         7.160E-06         7.160E-06         7.160E-06         0	GPU	-3	HYDROGEN 927K	/339K STI	RLING ENGINE	DATA: 1 (	UPDATED JAN 83)
CELL         *         1         *         2         *         3         *         4         *         5         *         7         8         7         *         5         *         7         8         7         *         5         7         8         7 <th7< th="">         7         7         7</th7<>		Ε	DIT HEAT EXCH	ANGER VALUES	PER NIHX	- COMMONS I	NCELL AND FLOEL
MHTRF       =       0       0       0       0       0       0       0       0         MATLAL       =       1       3       1       1       3         MILHAR       =       12       12       12       12       12       12         MITYPE       =       25       15       10       10       15         NIMX       =       1       40       40       40       40       40         NOPT1       =       0       0       0       0       0       0         AFLOH       =       3.860E-03       7.160E-06       7.160E-06       7.160E-06       7.160E-06       7.160E-06         ASPECT       =       0.070.0       0.0       0.0       0.0       0.0       0.0         AKEXT       =       1.070E-02       3.020E-03       <	CELL		* 1 *	* 2 *	* 3 *	* 4 *	* 7 * *
MCRIDN       I <thi< th=""> <thi< th=""></thi<></thi<>	MHTRF	4	U	ų	U	U	U
HTLHAL       =       12       12       12       12       12       12         HTLHAR       =       0       0       0       0       0       0         NIHX       =       1       40       40       40       40       40         NIHX       =       1       40       40       40       40       40         NIHX       =       1       400       40       40       40       40         AFLET       =       3.850E-03       7.160E-06       7.160E-06       7.160E-06       7.160E-06       7.160E-06         AKET       =       1.070E-02       3.020E-03       3.020E-03       3.020E-03       3.020E-03       3.020E-03         FRICHL       =       1.00       1.00       1.00       1.00       1.00       1.00       1.00         FRICHL       =       0.0       0.0       0.0       0.0       0.0       0.0       0.0         GRIA       =       0.0       0.0       0.0       0.0       0.0       0.0       0.0         GRIA       0.0       0.0       0.0       0.0       0.0       0.0       0.0       0.0       0.0 <t< td=""><td>MGFLOH</td><td>=</td><td>1</td><td>5</td><td>1</td><td>1</td><td>5</td></t<>	MGFLOH	=	1	5	1	1	5
MTLHIR       =       0       0       0       0       0       0         MTYPE       25       15       10       10       15         NIHX       =       1       40       40       40       40       40         NOPT1       =       0       0       0       0       0       0         AFLOH       =       3.850E-03       7.160E-06       7.160E-06       7.160E-06       7.160E-06       7.160E-05       1.116E-05       1.116E-05       1.116E-05       1.116E-05       1.116E-05       1.116E-05       1.116E-05       1.116E-05       1.10E-05       3.020E-03	MTLHAL	Ξ	12	12	12	12	12
HTYPE       =       25       15       10       10       15         NIHX       =       1       40       40       40       40         NOPT1       =       0       0       0       0       0         AFLOH       =       3.850E-03       7.160E-06       7.160E-06       7.160E-06       7.160E-06       7.160E-06         AKHLI       =       1.070E-03       1.116E-05       1.116E-05       1.116E-05       1.116E-05       1.116E-05         AKET       =       1.430E-02       3.020E-03       3.020E-03       3.020E-03       3.020E-03       3.020E-03         FRICHL       =       1.00       1.00       1.03       1.00       1.00       1.00         FRICHL       =       1.00       0.0       0.0       0.0       0.0       0.0         GRAS       =       4.056E+06       4.056E+06 <t< td=""><td>MTLHIR</td><td>=</td><td>0</td><td>0</td><td>Q</td><td>0</td><td>0</td></t<>	MTLHIR	=	0	0	Q	0	0
NIRX         =         1         40         40         40         40           NOPT1         =         0         0         0         0         0         0           AFL0H         =         3.850E-03         7.160E-06         7.160E-06         7.160E-06         7.160E-06         7.160E-06         7.160E-06         7.160E-06         7.160E-06         7.160E-05         1.116E-05         1.00         0.0	MTYPE	=	25	15	10	10	15
NOPT1         =         0         0         0         0         0         0           AFLOH         3.850E-03         7.160E-06         7.160E-06         7.160E-06         7.160E-06         7.160E-06           ASPECT         0.0         0.0         0.0         0.0         0.0         0.0           AXHALL         =         1.070E-03         1.116E-05         1.116E-05         1.116E-05         1.116E-05           AH:ET         =         1.430E-02         3.670E-04         7.370E-04         4.800E-04           DH         =         7.010E-02         3.020E-03         3.020E-03         3.020E-03         3.020E-03           FRICHL         =         0.0         0.0         0.0         0.0         0.0         0.0           GRAS         =         4.056E+06         4.056E+06         4.056E+06         4.056E+06         4.056E+06           FORMS         =         0.0         0.0         0.0         0.0         0.0         0.0           STGMA         =         0.0         0.0         0.0         0.0         0.0         0.0           VDL         =         9.311E-05         2.420E-07         8.670E-07         8.670E-07         5.848E-07 </td <td>NIHX</td> <td>=</td> <td>1</td> <td>40</td> <td>40</td> <td>40</td> <td>40</td>	NIHX	=	1	40	40	40	40
AFLOH       =       3.850E-03       7.160E-06       7.160E-06       7.160E-06       7.160E-06         ASPECT       =       0.0       0.0       0.0       0.0       0.0         AXHALL       =       1.070E-03       1.116E-05       1.116E-05       1.116E-05       1.116E-05         AKHT       =       1.430E-02       3.670E-04       7.370E-04       7.370E-03       3.020E-03         FRICHL       =       1.00       1.00       1.00       1.00       1.00       1.00         MCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0         POROS       =       0.0       0.0       0.0       0.0       0.0       0.0         GFLCH       =       0.0       0.0       0.0       0.0       0.0       0.0         GFLCH       =       0.0       0.0       0.0       0.0       0.0       0.0         GFLCH       =       927.00       927.00       927.00       927.00       927.00       927.00         VDL       =       9.311E-05       2.420E-07       8.670E-07       5.710E-07       NALLTH       =       0.03313       0.03970       0.07770       0.07770 <t< td=""><td>NOPT1</td><td>Ξ</td><td>0</td><td>0</td><td>0</td><td>0</td><td>0</td></t<>	NOPT1	Ξ	0	0	0	0	0
ASPECT       =       0.0       0.0       0.0       0.0       0.0         AXHALL       =       1.070E-03       1.116E-05       1.116E-05       1.116E-05       1.116E-05         AH:ET       =       1.430E-02       3.670E-04       7.370E-04       7.370E-04       4.860E-04         DH       =       7.010E-02       3.020E-03       3.020E-03       3.020E-03       3.020E-03         FRICHL       =       1.00       1.00       1.00       1.00       0.0       0.0         MCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0         ORIFCE       =       0.0       0.0       0.0       0.0       0.0       0.0         ORGS       =       0.0       0.0       0.0       0.0       0.0       0.0         SIGMA       =       0.0       0.0       0.0       0.0       0.0       0.0         VOL       =       9.311E-05       2.420E-07       6.891E-07       8.670E-07       5.710E-07         NALLT       =       9.27.00       927.00       927.00       927.00       927.00       927.00         VOLK       =       3.546E-05       4.320E-07       8	AFLOH	=	3.850E-03	7.160E-06	7.160E-06	7.160E-06	7.160E-06
AXHALL       =       1.070E-03       1.116E-05       1.116E-05       1.116E-05       1.116E-05         AVET       =       1.430E-02       3.670E-04       7.370E-04       7.370E-03       3.020E-03       3.020E-03         FRICHL       =       1.00       1.00       1.00       1.00       1.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0         PGAS       =       0.0       0.0       0.0       0.0       0.0         PGROS       =       0.0       0.0       0.0       0.0       0.0         PGROS       =       0.0       0.0       0.0       0.0       0.0         TGAS       =       9.7       0.0       0.0       0.0       0.0       0.0         TGAS       =       9.7       0.0       927.00       927.00       927.00       927.00         VOL       =       9.31E-05       2.420E-07       6.891E-07       6.870E-07       5.870E-07         NALLTH       =       0.03313       0.03970       0.07770       0.05120       10       *         WHTRF       =       0       0       0       0       0       0       0 <td>ASPECT</td> <td>Ξ</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td>	ASPECT	Ξ	0.0	0.0	0.0	0.0	0.0
AVET       =       1.430E-02       3.670E-04       7.370E-04       7.370E-04       4.860E-04         DH       =       7.010E-02       3.020E-03       3.020E-03       3.020E-03       3.020E-03         FRICHL       =       1.00       1.00       1.00       1.00       1.00       1.00         MCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.0556E+06       4.0556E+06       4.0556E+06       4.0556E+06       4.0556E+06         POROS       =       0.0       0.0       0.0       0.0       0.0       0.0         SIGMA       =       0.0       0.0       0.0       0.0       0.0       0.0         VOL       =       9.311E-05       2.420E-07       6.891E-07       8.670E-07       5.648E-07         VOLKL       =       3.540E-05       4.320E-07       8.670E-07       8.670E-07       5.648E-07         VALLTH       =       0.03313       0.30970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       -       COMMONS INCEL AND FLCELL         CELL       *       6       *       7       *       8<	AXHALL	=	1.070E-03	1.116E-05	1.116E-05	1.116E-05	5 1.116E-05
DH       -       7.010E-02       3.020E-03       3.020E-03       3.020E-03       3.020E-03         FRICHL       =       1.00       1.00       1.00       1.00       1.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0         ORIFCE       =       0.0       0.0       0.0       0.0       0.0         PGAS       =       0.0       0.0       0.0       0.0       0.0       0.0         QFLOM       =       0.0       0.0       0.0       0.0       0.0       0.0         TGAS       =       927.00       927.00       927.00       927.00       927.00         VOL       =       9.311E-05       2.420E-07       6.891E-07       6.891E-07       5.740E-07         NALLTH       =       0.00456       0.00091       0.00091       0.00091       0.00091         VOL       =       9.311E-05       2.420E-07       8.670E-07       8.670E-07       5.770E-07         NALLTH       =       0.00456       0.00091       0.00091       0.00091       0.00091         XLIGTH       =       0.3313       0.03970       0.07770       0.07770       0.05120 <tr< td=""><td>ALET</td><td>=</td><td>1.430E-02</td><td>3.6702-04</td><td>7.370E-04</td><td>7.370E-04</td><td>4.860E-04</td></tr<>	ALET	=	1.430E-02	3.6702-04	7.370E-04	7.370E-04	4.860E-04
FRICHL       1.00       1.00       1.00       1.00       1.00       1.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0         ORIFCE       =       0.0       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.0       0.0       0.0       0.0       0.0       0.0         GFLOM       =       0.0       0.0       0.0       0.0       0.0       0.0         THALL       =       927.00       927.00       927.00       927.00       927.00       927.00         VOL       =       9.311E-05       2.420E-07       8.670E-07       8.670E-07       5.848E-07         VOLKL       =       3.54CE-05       4.320E-07       8.670E-07       8.670E-07       5.710E-07         MALLTH       =       0.03313       0.03970       0.07770       0.05120       0.05120         EDIT REGENERATOR VALUES PER NIHX       - COMHONS INCEL AND FLCELL         CELL       *       6       *       7       *       8       #       9 <td>пн</td> <td>-</td> <td>7.010E-02</td> <td>3.0205-03</td> <td>3.020E-03</td> <td>3.020E-03</td> <td>3.020E-03</td>	пн	-	7.010E-02	3.0205-03	3.020E-03	3.020E-03	3.020E-03
HCEXT       =       1.00       1.00       1.00       1.00       1.00       1.00         MCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       9.0       0.0	FRICH	=	1 00	1 00	1 00	1 00	
MCLTAT       0.0       0.0       0.0       0.0       0.0         PGAS       =       0.056+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         PDROS       =       0.0       0.0       0.0       0.0       0.0       0.0         PGROS       =       0.0       0.0       0.0       0.0       0.0       0.0         GFLOM       =       0.0       0.0       0.0       0.0       0.0       0.0         TMALL       927.00       927.00       927.00       927.00       927.00       927.00         VOL       =       9.311E-05       2.420E-07       6.891E-07       6.891E-07       5.848E-07         VOLHL       =       3.54CE-05       4.320E-07       8.670E-07       8.670E-07       5.710E-07         XALLTH       =       0.03313       0.03970       0.07770       0.05120       0.05120         EDIT REGENERATOR VALUES PER NIHX       - COMHONS INCEL AND FLCELL         CELL       *       *       7       *       8       #       9       *       10       *         MHTFF       0       0       0       0       0       0       0       0	PUSAL	-	n n	0.0	0 0	0 0	0.0
DRAFCE       -       0.0       0.0       0.0       0.0       0.0       0.0         PGAS       =       0.0       0.0       0.0       0.0       0.0       0.0         QFLQM       =       0.0       0.0       0.0       0.0       0.0       0.0         SIGMA       =       0.0       0.0       0.0       0.0       0.0       0.0         THALL       927.00       927.00       927.00       927.00       927.00       927.00         THALL       927.00       927.00       927.00       927.00       927.00       927.00         VOL =       9.311E-05       2.420E-07       8.670E-07       8.670E-07       5.710E-07         WALLTH       =       0.03313       0.03970       0.07770       0.00091       0.00091         VOLKI       =       3.540E-05       4.320E-07       8.670E-07       8.670E-07       5.710E-07         WALLTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       -       COMMONS INCEL AND FLCELL         CELL       *       6       *       7       *       8       *       9       *<	OBIECE	-	n n	0.0	0.0	0.0	n n
PDROS       =       4.0502405       4.0502404       4.	DCAC	-	0.0 6 0545+04	6 0565-06	4 054F-04	0.0 6 0565.06	0.0 6 05(c.0/
PHORS       =       0.0       0.0       0.0       0.0       0.0         GFLOM       =       0.0       0.0       0.0       0.0       0.0         SIGMA       =       0.0       0.0       0.0       0.0       0.0         TGAS       =       927.00       927.00       927.00       927.00       927.00         THALL       =       927.00       927.00       927.00       927.00       927.00         VUL =       9.311E-05       2.420E-07       6.691E-07       8.670E-07       5.710E-07         WALLTH       =       0.00456       0.00091       0.00091       0.00091         VULKL       =       3.540E-05       4.320E-07       8.670E-07       8.670E-07       5.710E-07         WALTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       -       COMMONS INCEL AND FLCELL         K       #	PUAS	-	4.0502700	4.0002400	4.0002700	4.0302400	0 0 0
Gridding       0.0       0.0       0.0       0.0       0.0         TGAS       =       927.00       927.00       927.00       927.00       927.00         THALL       =       927.00       927.00       927.00       927.00       927.00       927.00         VOL       =       9.311E-05       2.420E-07       6.891E-07       6.670E-07       5.848E-07         VOLKI       =       3.540E-05       4.320E-07       8.670E-07       6.670E-07       5.710E-07         NALLTH       =       0.00456       0.00091       0.00091       0.00091       0.00091         XLIGTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       - COMMONS INCEL AND FLCELL         CELL       *       *       *       *       *         MHTRF       0       0       0       0       0       0         MHTRF       1       1       1       1       1       1       1         MTRF       0       0       0       0       0       0       0         MHTRF       10       1       1       1       1       1 </td <td>PUKUS</td> <td>=</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td>	PUKUS	=	0.0	0.0	0.0	0.0	0.0
SLEMA       =       0.0       0.0       0.0       0.0       0.0         TGAS       =       927.00       927.00       927.00       927.00       927.00       927.00         THALL       =       927.00       927.00       927.00       927.00       927.00       927.00         VOL       =       9.31E-05       2.420E-07       6.891E-07       6.891E-07       5.710E-07         VOLKI       =       3.54CE-05       4.320E-07       8.670E-07       8.670E-07       5.710E-07         NALLTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       - COMMONS INCEL AND FLCELL         CELL       *       6       *       7       *       8       *       9       *       10       *         MHTRF       0       0       0       0       0       0       0       0         MTLHA       12       12       12       12       12       12       12         MTLHR       11       11       11       11       11       11       11       11       11       11         MTLWIR       8       8 </td <td>QFLOW</td> <td>=</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td>	QFLOW	=	0.0	0.0	0.0	0.0	0.0
16AS       =       927.00       927.00       927.00       927.00       927.00         THALL       =       927.00       927.00       927.00       927.00       927.00         VUL =       9.311E-05       2.420E-07       6.891E-07       6.891E-07       5.848E-07         VOLKL       =       3.540E-05       4.320E-07       8.670E-07       8.670E-07       5.710E-07         WALLTH       =       0.00456       0.00091       0.00091       0.00091       0.00091         XLIGTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       - COMMONS INCEL AND FLCELL         CELL       *       6       *       7       *       8       *       9       *       10       *         MHTRF       0       0       0       0       0       0       0       0       0         M4LLTH       11       1       1       1       1       1       1       1       1       1         M4FLOH       1       1       1       1       1       1       1       1       1       1       1       1       1	SIGNA	2	0.0	U.U	0.0	0.0	U.U
THALL       =       927.00       <	TGAS	=	927.00	927.00	927.00	927.00	927.00
VOL = 9.311E-05 2.420E-07 6.891E-07 6.891E-07 5.848E-07 VOLKL = 3.54CE-05 4.320E-07 8.670E-07 8.670E-07 5.710E-07 WALLTH = 0.00456 0.00091 0.00091 0.00091 XLNGTH = 0.03313 0.03970 0.07770 0.07770 0.05120 EDIT REGENERATOR VALUES PER NIHX - COMMONS INCEL AND FLCELL (ELL * 6 * 7 * 8 8 * 9 * * 10 * * MHTRF = 0 0 0 0 0 0 0 MQFLOH = 1 1 1 1 1 1 1 MTLHAL = 12 12 12 12 12 MTLWAR = 11 1 1 1 1 MTLWAR = 1 0 0 0 0 AFLOH = 1.880E-04 1.880E-04 1.880E-04 1.820E-04 ASPECT = 0.0 0.0 0.0 0.0 AFLOH = 1.322E-04 1.322E-04 1.322E-04 1.322E-04 AKET = 3.635E-02 3.635E-02 3.635E-02 3.635E-02 DH = 9.350E-05 9.350E-05 9.350E-05 9.350E-05 FRICHL = 2.00 2.00 2.00 2.00 2.00 2.00 HCEXT = 0.0 0.0 0.0 0.0 0.0 ORIFCE = 0.0 0.0 0.0 0.0 0.0 ORIFCE = 0.0 0.0 0.0 0.0 PGAS = 4.056E+06 4.056E+06 4.056E+06 4.056E+06 PDROS = 0.6970 0.6970 0.6970 0.6970 0.6970 QFLOH = 0.3640 0.3400 634.00 634.00 634.00 SIGMA = 0.4680 0.4680 0.4680 0.4680 0.4680 VOLKL = 5.980E-07 5.980E-07 5.980E-07 5.980E-07 THALL = 634.00 634.00 634.00 634.00 634.00 VOL = 1.336E-06 1.336E-06 1.336E-06 1.336E-06 1.336E-06 VOLKL = 5.980E-07 5.980E-07 5.980E-07 5.980E-07 VOLKL = 5.980E-07 5.980E-07 5.980E-07 5.980E-07 VOLKL = 5.980E-07 5.980E-07 5.980E-07 5.980E-07 MALLTH = 0.00173 0.00173 0.00173 0.00173 VOLVES 0.00452 0.00452 0.00452 0.00452 0.00452	THALL	=	927.00	927.00	927.00	927.00	927.00
VOLKL       =       3.540E-05       4.320E-07       8.670E-07       8.670E-07       5.710E-07         WALLTH       =       0.00456       0.00091       0.00091       0.00091       0.00091         XLNGTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       -       COMMONS INCEL AND FLCELL         CELL       *       6       *       7       *       8       *       9       *       10       *         MHTRF       =       0       0       0       0       0       0       0         MUTLWL       *       1       1       1       1       1       1       1         MTLWR       =       12       12       12       12       12       12         MTLWR       =       11       11       11       11       11       11       11         MTLWR       =       30       30       30       30       30       30         NIHX       =       8       8       8       8       8       8         NOPT1       =       0       0       0       0	VOL	=	9.311E-05	2.420E-07	6.8912-07	6.891E-07	<b>5.8</b> 48E-07
NALLTH       =       0.00456       0.00091       0.00091       0.00091       0.00091       0.00091         XLNGTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       -       COMMONS INCEL AND FLCELL         CELL       *       6       *       7       *       8       *       9       *       10       *         MHTRF       =       0       0       0       0       0       0       0         MGFLOW       =       1       1       1       1       1       1       1         MTLWAL       =       12       12       12       12       12       12         MTLWIR       =       11       11       11       11       11       11       11         MTYPE       =       30       30       30       30       30       30       30         AFLON       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.822E-04       1.322E-04         AFLON       1.322E-04       1.322E-04       1.322E-04       1.322E-04       3.635E-02       3.635E-02       3.635E-02       3.635E-02 </td <td>VOLKL</td> <td>Ξ</td> <td>3.54CE-05</td> <td>4.320E-07</td> <td>8.670E-07</td> <td>8.670E-07</td> <td>5.7105-07</td>	VOLKL	Ξ	3.54CE-05	4.320E-07	8.670E-07	8.670E-07	5.7105-07
XLIGTH       =       0.03313       0.03970       0.07770       0.07770       0.05120         EDIT REGENERATOR VALUES PER NIHX       -       COMMONS INCEL AND FLCELL         CELL       *       6       *       7       *       8       *       9       *       10       *       *         MHTRF       =       0       0       0       0       0       0       0         MGFLOW       =       1       1       1       1       1       1       1         MTLWIR       =       12       12       12       12       12       12         MTLWIR       =       11       11       11       11       11       11         MTLWIR       =       1       0       0       0       0       0       0         MTLWIR       =       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.822E-04       1.322E-04       1.322E-04 </td <td>HALLTH</td> <td>=</td> <td>0.00456</td> <td>0.00091</td> <td>0.00091</td> <td>0.00091</td> <td>0.00091</td>	HALLTH	=	0.00456	0.00091	0.00091	0.00091	0.00091
EDIT REGENERATOR VALUES PER NIHX         - COMMONS INCEL AND FLCELL           CELL         * 6 * * 7 * * 8 * * 9 * * 10 * *           MHTRF         =         0         0         0           MGFLOW         =         1         1         1         1           MTLWAL         =         12         12         12         12           MTLWAL         =         11         1         1         1         1           MTLWAL         =         12         12         12         12         12           MTLWAR         =         11         11         11         11         11         11           MTYPE         =         30         30         30         30         30         30           NIHX         =         8         8         8         8         8         8           NOPT1         =         0         0         0         0         0           AKALL         =         1.322E-04         1.322E-04         1.322E-04         1.322E-04         3.22E-04           AKBECT         =         0.0         0.0         2.00         2.00         2.00         2.00           DH         <	XLNGTH	=	0.03313	0.03970	0.07770	0.07770	0.05120
CELL       *       6       *       7       *       8       *       9       *       *       10       *       *         MHTRF       =       0       0       0       0       0       0       0         MQFLOW       =       1       1       1       1       1       1       1         MTLWAL       =       12       12       12       12       12       12         MTLWIR       =       11       11       11       11       11       11         MTYPE       =       30       30       30       30       30       30         NIHX       =       8       8       8       8       8       8         NOPT1       =       0       0       0       0       0       0       0         AKHALL       =       1.322E-04       1.32EE		F	DTT REGENERAT	OR VALUES PE	R NIHX - C	OMMONS THE	L AND FLOFLI
HHTRF       =       0       0       0       0       0         MQFLOH       =       1       1       1       1       1         MTLMAL       =       12       12       12       12       12         MTLWIR       =       11       11       11       11       11       11         MTYPE       =       30       30       30       30       30       30         NIHX       =       8       8       8       8       8       8         NOPT 1       =       0       0       0       0       0       0         AFLOH       =       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.822E-04         ASPECT       =       0.0       0.0       0.0       0.0       0.0         AWET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         DH       =       9.30       0.0       0.0       0.0       0.0       0.0         DH       =       0.0	CELL		* 6 *	* 7 *	* 8 *	* 9 *	* 10 * *
MIRL       -       0       0       0       0       0         MTLHAL       =       12       12       12       12       12         MTLWIR       =       11       11       11       11       11       11         MTYPE       =       30       30       30       30       30       30         NIHX       =       8       8       8       8       8         NOPT1       =       0       0       0       0       0         AFLOH       =       1.880E-04       1.880E-04       1.880E-04       1.850E-04       1.850E-04         ASPECT       =       0.0       0.0       0.0       0.0       0.0         AKHALL       =       1.322E-04       1.322E-04       1.322E-04       1.322E-04       1.322E-04         AWET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICML       =       2.00       2.00       2.00       2.00       2.00         CMEXT       0.0       0.0	MUTRE	=	<b>N</b>		 	n n	
MTLHAL       =       12       12       12       12       12         MTLHAL       =       11       11       11       11       11       11         MTLWR       =       11       11       11       11       11       11         MTYPE       =       30       30       30       30       30       30         NIHX       =       8       8       8       8       8       8         NOPT1       =       0       0       0       0       0       0         ASPECT       =       0.0       0.0       0.0       0.0       0.0       0.0         AWALL       =       1.322E-04       1.322E-04       1.322E-04       1.322E-04       1.322E-04         AWET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICML       =       2.00       2.00       2.00       2.00       2.00       2.00         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06	MOELOW	=	ĭ	ĭ	1	1	1 1
HTLWLR       -       12       11	MTILIAI	-	12	12	12	12	12
MTYPE       =       30       30       30       30       30       30         NIHX       =       8       8       8       8       8       8         NOPT1       =       0       0       0       0       0       0         AFLOH       =       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.880E-04         ASPECT       =       0.0       0.0       0.0       0.0       0.0         AXHALL       =       1.322E-04       1.322E-04       1.322E-04       1.322E-04         AHET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICHL       =       2.00       2.00       2.00       2.00       2.00       1.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0         PGROS       =       0.6970       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOH       =       0.0       0.0       0.0       0.0       0.0       0.0	MTLUTD	-	11	11	11	11	11
NIHZ       =       30       30       30       30       30         NIHX       =       8       8       8       8       8         NOPT1       =       0       0       0       0       0         AFLOH       =       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.880E-04         ASPECT       =       0.0       0.0       0.0       0.0       0.0         AXHALL       =       1.322E-04       1.322E-04       1.322E-04       1.322E-04         AWET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICHL       =       2.00       2.00       2.00       2.00       2.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOH       =       0.0       0.0 <td< td=""><td>MTYDE</td><td>2</td><td>30</td><td>30</td><td>30</td><td>30</td><td>30</td></td<>	MTYDE	2	30	30	30	30	30
NOPT 1       =       0       0       0       0       0       0       0         AFLOH       =       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.880E-04       1.850E-04         ASPECT       =       0.0       0.0       0.0       0.0       0.0         AXHALL       =       1.322E-04       1.322E-04       1.322E-04       1.322E-04         AKHT       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICHL       =       2.00       2.00       2.00       2.00       2.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOH       =       0.0       0.0       0.0       0.0       0.0       0.0         GAS =       634.00       634.00       634.00       634.00       634.00	NTIN	2	50	30	50	20	30
$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	NULTY	-	0	0	0	0	0
AFEON=1.880E-041.880E-041.880E-041.880E-041.880E-04ASPECT=0.00.00.00.00.0AXHALL=1.322E-041.322E-041.322E-041.322E-04AHET=3.635E-023.635E-023.635E-023.635E-02CH=9.350E-059.350E-059.350E-059.350E-05FRICML=2.002.002.002.00HCEXT=0.00.00.00.0PGAS=4.056E+064.056E+064.056E+06POROS=0.69700.69700.69700.6970QFLOM=0.00.00.00.0TGAS=634.00634.00634.00634.00TGAS=634.00634.00634.00634.00VOL=1.336E-061.336E-061.336E-061.336E-06VOLH=5.980E-075.980E-075.980E-075.980E-07VOLH=0.001730.001730.001730.00173XLNGTH=0.004520.004520.004520.00452	AFLON	-	1 9907 06	1 9000 06	1 9905 04	1 9905 0/	4 9000 04
ASPELT       =       0.0       0.0       0.0       0.0       0.0         AXHALL       =       1.322E-04       1.322E-04       1.322E-04       1.322E-04       1.322E-04         AWET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICHL       =       2.00       2.00       2.00       2.00       2.00       2.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOH       =       0.0       0.0       0.0       0.0       0.0         GAS       =       634.00       634.00       634.00       634.00       634.00         SIGMA       =       0.4680       0.4680       0.4680       0.4680       0.4680         TGAS       =       634.00       634.00       634.00       634.00       634.00	AFLUN	-	1.0000-04	1.00UE-U4	1.0000-04	1.0000-0-	1 1.0000-04
AXHALL       =       1.322E-04       1.322E-04       1.322E-04       1.322E-04       1.322E-04         AWET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICHL       =       2.00       2.00       2.00       2.00       2.00         DHEEXT       =       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOH       =       0.0       0.0       0.0       0.0       0.0         TGAS       =       634.00       634.00       634.00       634.00       634.00         SIGMA       =       0.4680       0.4680       0.4680       0.4680       0.4680         TGAS       =       634.00       634.00       634.00       634.00       634.00       634.00         VOL       =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.33	ASPELI	=	U.U 1 7005 0/	U.U	0.0		
AWET       =       3.635E-02       3.635E-02       3.635E-02       3.635E-02       3.635E-02         DH       =       9.350E-05       9.350E-05       9.350E-05       9.350E-05       9.350E-05         FRICHL       =       2.00       2.00       2.00       2.00       2.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOH       =       0.0       0.0       0.0       0.0       0.0         TGAS       =       634.00       634.00       634.00       634.00       634.00         THALL       =       634.00       634.00       634.00       634.00       634.00         VOL       =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.336E-06         VOLHL       =       5.980E-07       5.980E-07       5.980E-07       5.980E-07       5.980E-07         HALLTH       =       0.00173       0.00173       0.00173       0.00173       0.00173 </td <td>AXHALL</td> <td>=</td> <td>1.322E-04</td> <td>1.322E-04</td> <td>1.322E-04</td> <td>1.322E-04</td> <td>4 1.322E-04</td>	AXHALL	=	1.322E-04	1.322E-04	1.322E-04	1.322E-04	4 1.322E-04
$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	AWET	=	3.635E-02	3.635E-U2	3.635E-02	3.635E-02	2 3.635E-02
FRICML       =       2.00       2.00       2.00       2.00       2.00         HCEXT       =       0.0       0.0       0.0       0.0       0.0       0.0         ORIFCE       =       0.0       0.0       0.0       0.0       0.0       0.0         PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOH       =       0.0       0.0       0.0       0.0       0.0       0.0         SIGMA       =       0.4680       0.4680       0.4680       0.4680       0.4680       0.4680         TGAS       =       634.00       634.00       634.00       634.00       634.00         THALL       =       634.00       634.00       634.00       634.00       634.00         VOL =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.336E-06         VOLHL       =       5.980E-07       5.980E-07       5.980E-07       5.980E-07         HALLTH       =       0.00173       0.00173       0.00173       0.00173       0.00173 <td>DH</td> <td>=</td> <td>9.350E-05</td> <td>9.350E-05</td> <td>9.350E-05</td> <td>9.350E-0</td> <td>5 9.350E-05</td>	DH	=	9.350E-05	9.350E-05	9.350E-05	9.350E-0	5 9.350E-05
HCEXT=0.00.00.00.00.0ORIFCE=0.00.00.00.00.0PGAS=4.056E+064.056E+064.056E+064.056E+064.056E+06POROS=0.69700.69700.69700.69700.6970QFLOH=0.00.00.00.00.0SIGMA=0.46800.46800.46800.46800.4680TGAS=634.00634.00634.00634.00634.00THALL=634.00634.00634.00634.00634.00VOL =1.336E-061.336E-061.336E-061.336E-061.336E-06VOLHL=5.980E-075.980E-075.980E-075.980E-07HALLTH=0.001730.001730.001730.001730.00173XLNGTH=0.004520.004520.004520.004520.00452	FRICHL	=	2.00	2.00	2.00	2.00	2.00
ORIFCE         =         0.0         0.0         0.0         0.0         0.0         0.0           PGAS         =         4.056E+06         4.056E+06 <td>HCEXT</td> <td>Ŧ</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td> <td>0.0</td>	HCEXT	Ŧ	0.0	0.0	0.0	0.0	0.0
PGAS       =       4.056E+06       4.056E+06       4.056E+06       4.056E+06       4.056E+06         POROS       =       0.6970       0.6970       0.6970       0.6970       0.6970         QFLOW       =       0.0       0.0       0.0       0.0       0.0       0.0         SIGMA       =       0.4680       0.4680       0.4680       0.4680       0.4680         TGAS       =       634.00       634.00       634.00       634.00       634.00         THALL       =       634.00       634.00       634.00       634.00       634.00         VOL       =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.336E-06         VOLH       =       5.980E-07       5.980E-07       5.980E-07       5.980E-07       5.980E-07         HALLTH       =       0.00173       0.00173       0.00173       0.00173       0.00173         XLNGTH       =       0.00452       0.00452       0.00452       0.00452       0.00452	ORIFCE	=	0.0	0.0	0.0	0.0	0.0
$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	PGAS	=	4.056E+06	4.056E+06	4.056E+06	4.056E+0(	6 4.056E+06
QFLOW =       0.0       0.0       0.0       0.0       0.0         SIGMA =       0.4680       0.4680       0.4680       0.4680       0.4680         TGAS =       634.00       634.00       634.00       634.00       634.00         THALL =       634.00       634.00       634.00       634.00       634.00         VOL =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.336E-06         VOLWL =       5.980E-07       5.980E-07       5.980E-07       5.980E-07         HALLTH =       0.00173       0.00173       0.00173       0.00173         XLNGTH =       0.00452       0.00452       0.00452       0.00452	POROS	=	0.6970	0.6970	0.6970	0.6970	0.6970
SIGMA =       0.4680       0.4680       0.4680       0.4680       0.4680         TGAS =       634.00       634.00       634.00       634.00       634.00         THALL =       634.00       634.00       634.00       634.00       634.00         VOL =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.336E-06         VOLWL =       5.980E-07       5.980E-07       5.980E-07       5.980E-07         HALLTH =       0.00173       0.00173       0.00173       0.00173         XLNGTH =       0.00452       0.00452       0.00452       0.00452	QFLOH	=	0.0	0.0	0.0	0.0	0.0
TGAS       =       634.00       634.00       634.00       634.00       634.00         THALL       =       634.00       634.00       634.00       634.00       634.00         VOL       =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.336E-06         VOLHL       =       5.980E-07       5.980E-07       5.980E-07       5.980E-07         HALLTH       =       0.00173       0.00173       0.00173       0.00173         XLNGTH       =       0.00452       0.00452       0.00452       0.00452	SIGMA	=	0.4680	0.4680	0.4680	0.4680	0.4680
THALL =       634.00       634.00       634.00       634.00       634.00         VOL =       1.336E-06       1.336E-06       1.336E-06       1.336E-06       1.336E-06         VOLHL =       5.980E-07       5.980E-07       5.980E-07       5.980E-07       5.980E-07         HALLTH =       0.00173       0.00173       0.00173       0.00173       0.00173         XLNGTH =       0.00452       0.00452       0.00452       0.00452	TGAS	Ξ	634.00	634.00	634.00	634.00	634.00
VOL         =         1.336E-06         1.336E-07         1.336E-07 <td>THALL</td> <td>=</td> <td>634.00</td> <td>634.00</td> <td>634.00</td> <td>634.00</td> <td>634.00</td>	THALL	=	634.00	634.00	634.00	634.00	634.00
VOLWL         =         5.980E-07         5.980E-07<	VOL	=	1.336E-06	1.336E-06	1.336E-06	1.336E-D	6 1.336E-06
HALLTH = 0.00173 0.00173 0.00173 0.00173 0.00173 XLNGTH = 0.00452 0.00452 0.00452 0.00452 0.00452	VOLHL	=	5.980E-07	5.980E-07	5.980E-07	5.980E-0	7 5.980E-07
XLNGTH = 0.00452 0.00452 0.00452 0.00452 0.00452	HALLTH	Ŧ	0.00173	0.00173	0.00173	0.00173	0.00173
	XLNGTH	Ŧ	0.00452	0.00452	0.00452	0.00452	0.00452

	GPU	-3	HYDI	ROGEI	927	(/339к	STI	RLING	ENGIN	E DAT	'A: 1	(U	PDATE	0 J/	AN 8	3)
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AFL	0:1	=		9.16	0E-07	9.160	-07	9.16	DE-07	2.	800E	-05	3.7	770E-	-03	
ASPE	CT	=		0.0		0.0		0.0	)	0	1.0		0.	.0		
AXHA	LL	=		1.07	0E-06	1.070	E-06	1.07	0E-06	3.	800E	-05	3.8	30DE-	-05	
AH	ET	=		1.80	0E-05	1.200	E-04	1.80	0E-05	5.	966E	-04	1.5	520E-	-02	
	DH	=		1.08	0E-03	1.080	E-03	1.08	30E-03	5.	970E	-03	6.0	)40E-	-02	
FRIC	HL	Ξ		1.	00	1.0	)	1.	.00		1.00			1.00		
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ORIF	CE	Ξ		0.0		0.0		0.0	)	C	).0		D.	. O		
FG	AS	2		4.05	SE+06	4.056	E+06	4.05	66E+06	4.	056E	+06	4.(	D56E-	+06	
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QFL	<b>F:O</b>	=		0.1	Û	0.0		0.	.0		0.0			0.0		
SIG	Al S	Ŧ	1	0.0		0.0		0.0		0.	0		0.0	)		
TG	AS	=		339.	00	339.0	ו	339.	.00	- 33	59.0 <b>0</b>		339	9.00		
TRA	LL.	=		339.	00	339.0	0	339.	.00	- 33	59.00		339	9.00		
V	OL .	=		2.01	3E-08	3.241	E-08	4.8.	S8E-09	) <b>1</b> .	281E	-06	1.0	093E-	-05	
VOL	HL.	=		5.67	0E-09	3.800	E-08	5.67	70E-09	· 1.	20 <b>0</b> E	-06	3.!	540E	-05	
HALL	TH	=	0	.000	26	0.0002	5	0.000	)26	0.0	0160		0.01	0020		
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IALE	AK	=		1		1										
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NSHE	LD	=		2												
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## RIOS/SEAM1 ANALYSIS CONSOLIDATED INPUT INFORMATION

ZONE	EXPANSION 1	HEATER 2	REGENERATOR 3	COOLER 4	COMPRESSION 5
VOLUHE (CU M)	1.21536-04	8.8200E-05	5.3440E-05	2.81508-05	1.1425E-04
FLOH AREA (SQ M)	3.8600E-03	2.8640E-04	1.5040E-03	2.8579E-04	3.7700E-03
WETTED AREA (SQ M)		5.8960E-02	1.4541E+00	3.7440E-02	
HYD DIA (M)	0.070100	0.003020	0.000093	0.001080	0.060400
TOT LNGTH (M)		0.246300	0.022600	0.046100	
HT EXCH LIGTH (M)		0.155400		0.035500	
TEMPERATURE (K)	927.00	927.00	584.52	339.00	339.00
REGENERATOR H	ALL DIAMETER (M)	0.02262	AVG HT TRANS	F REYN EXPONENT	0.5503
NINIMUM TOT	AL VOLUME (CU M)	2.3248E-04	NAXIHUM TOTA	L VOLUME (CU H)	3.52612-04
ANGLE AT HIN TO	TAL VOLUME (DEG)	290.4998	ANGLE AT MAX TOT	AL VOLUME (DEG)	128.5000
AVERAG	E PRESSURE (MPA)	2.7400	TOTAL	GAS MASS (KES)	3.9565E-04
NORMALIZED V	ALUES FOR XMASE,	TEMP RATIO,	RVT = 0.00002	478 2.7345	2.5705

GPU-3 HY	DROGEN 927K/33	9K STIRL	ING ENGINE DA	TA: 1 (UF	DATED JAN 83)
ZONI	E OUTPUT FOR C	ASE 1	CYCLE NUMBER	1 FLUX	ERROR= -534.07
ZONE MUMBER TEMP GAS MAX TEMP GAS AVG HALL-GAS DEL T AVG HALL-GAS DEL T MAX HALL-GAS CHNG Q AVG HASS FLOH KG NAX MASS FLOH KG REYHOLDS NUMBER DEL-P FRICTION M NUSSELT NUMDER	1 K 950.30 K 819.91 K 0.0 K -130.38 H -664.01 /S 0.003343 /S 0.003343 /S 0.003343 PA 0.0 0.0	2 819.91 819.91 68.89 68.89 2591.75 0.003343 0.003343 1796.17 0.000842 4.78	3 584.52 584.52 0.0 -176.27 0.004020 0.004020 17.56 0.072585 3.77	4 323.17 323.17 -28.76 -1154.22 0.004333 0.004833 1878.62 0.000616 5.84	5 390.29 323.17 0.0 -67.11 69.94 0.094833 0.004833 0.004833 25.53 0.0 0.0
ZON	E OUTPUT FOR C	ASE 1	CYCLE NUMBER	3 FLUX	ERROR= -6.02
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG WALL-GAS DEL T AVG HALL-GAS DEL T MAX WALL-GAS CHIIG Q AVG MASS FLOW KG. MAX MASS FLOW KG. REYNOLDS NUMBER DEL-P FRICTION M NUSSELT NUMBER	1 K 815.26 K 803.33 K 0.0 K -11.93 W -570.03 /S 0.003744 /S 0.003744 96.30 PA 0.0 0.0	2 803.33 803.33 85.15 3134.77 0.003744 0.003744 2236.63 0.000842 5.34	3 531.47 531.47 0.0 -189.07 0.004384 0.004384 20.47 0.020842 4.11	4 332.73 332.73 -36.26 -36.26 -1472.61 0.005133 0.005133 2020.59 0.000665 5.98	5 382.02 332.73 0.0 -49.29 66.01 0.005133 0.005133 27.46 0.0 0.0
ZON	E OUTPUT FOR C	ASE 1	CYCLE NUMBER	5 FLUX	ERROR= -0.58
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG HALL-GAS DEL T AVG HALL-GAS DEL T MAX HALL-GAS CHNG Q AVG MASS FLOH KG MAX MASS FLOH KG REYNOLDS NUMBER DEL-P FRICTION M NUSSELT NUMBER	1 K 820.16 K 802.04 K 0.0 K -18.12 H -568.21 /S 0.003729 /S 0.003729 95.50 PA 0.0 0.0	2 802.04 862.04 86.44 3199.26 0.003729 0.003729 2218.11 0.000841 5.26	3 533.26 533.26 0.0 -187.92 0.004371 0.004371 20.37 0.020903 4.10	4 332.78 332.78 -36.31 -1473.64 0.005125 0.005125 2017.58 0.000663 5.98	5 382.00 332.78 0.0 -49.22 65.77 0.005125 0.005125 27.42 0.0 0.0
ZON	E OUTPUT FOR C	ASE 1	CYCLE NUMBER	6 FLUX	ERROR= 0.15
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG HALL-GAS DEL T AVG HALL-GAS DEL T MAX WALL-GAS CHNG Q AVG MASS FLOH KG MAX MASS FLOH KG REYNOLDS NUMBER DEL-P FRICTION M NUSSELT NUMBER	1 K 820.62 K 801.92 K 0.0 K -18.70 H -568.04 S 0.003727 S 0.003727 95.42 PA 0.0 0.0	2 801.92 801.92 86.55 3200.09 0.003727 0.003727 2216.23 0.000840 5.25	3 533.44 533.44 0.0 -187.82 0.004370 20.36 0.020909 4.09	4 332.77 332.77 -36.30 -36.30 -1473.45 0.005125 0.005125 2017.27 0.001663 <u>5</u> .98	5 382.01 332.77 0.0 -49.24 65.75 0.005125 0.005125 27.41 0.0 0.0

GPU-3 HYDRO	DGEN 927K/339k	STIRL	ING ENGINE DA	TA: 1 (UP	DATED JAN 83)
ZONE	OUTPUT FOR CAS	SE 2	CYCLE NUMBER	1 FLUX	ERROR= -41.69
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K HALL-GAS DEL T AVG K HALL-GAS DEL T MAX K HALL-GAS CHMG Q H AVG MASS FLOH KG/S MAX MASS FLOH KG/S REYNOLDS NUMBER DEL-P FRICTION MPA NUSSELT NUMBER	1 950.21 828.47 0.0 -121.74 -614.89 0.005014 0.005014 115.99 0.0 0.0	2 828.47 828.47 68.42 68.42 4600.64 0.005014 0.005014 2693.97 0.001773 8.54	3 584.52 584.52 0.0 -270.09 0.006029 0.006029 26.34 0.035279 4.72	4 328.55 328.55 -28.54 -2024.86 0.007248 0.007248 2817.30 0.001261 10.32	5 390.36 328.55 0.0 -61.81 70.92 0.007248 0.007248 38.28 0.0 0.0
ZONE	DUTPUT FOR CAS	SE 2	CYCLE NUMBER	3 FLUX	ERROR= 1.59
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K HALL-GAS DEL T AVG K HALL-GAS DEL T MAX K HALL-GAS CHNG Q H AVG MASS FLOH KG/S NAX MASS FLOH KG/S REYHOLDS NUMBER DEL-P FRICTION MPA HUSSELT NUMBER	1 861.25 839.24 0.0 -22.02 -632.93 0.005421 0.005421 134.27 0.0 0.0	2 839.24 57.56 57.56 4657.40 0.005421 0.005421 3118.40 0.001694 11.08	3 545.50 545.50 0.0 -296.99 0.006435 0.006435 29.51 0.033930 5.02	4 328.64 328.64 -27.55 -27.55 -2191.08 0.007638 0.007638 3030.73 0.001162 11.80	5 378.02 328.64 0.0 -49.39 72.87 0.007638 0.007638 41.18 0.0 0.0
ZONE	OUTPUT FOR CAS	SE 2	CYCLE NUMBER	5 FLUX	ERROR= 0.02
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K HALL-GAS DEL T AVG K HALL-GAS DEL T MAX K HALL-GAS CHNG Q H AVG MASS FLOH KG/S MAX MASS FLOH KG/S REYNOLDS NUMBER DEL-P FRICTION HPA NUSSELT NUMBER	1 859.68 839.47 0.0 -20.21 -633.19 0.005430 0.005430 134.68 0.0 0.0	2 839.47 839.47 57.33 57.33 4657.77 0.005430 0.005430 3128.00 0.001697 11.15	3 544.71 544.71 0.0 -297.49 .006442 0.006442 29.57 0.033903 5.03	4 328.62 -27.53 -27.53 -2192.01 0.007641 0.007641 3033.66 0.001161 11.82	5 377.79 323.62 0.0 -49.17 72.91 0.007641 0.007641 41.22 0.0 0.0
ZONE	OUTPUT FOR CA	SE 3	CYCLE NUMBER	1 FLUX	ERROR= -26.22
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K NALL-GAS DEL T AVG K HALL-GAS DEL T MAX K HALL-GAS CHNG Q H AVG MASS FLOW KG/S MAX MASS FLOW KG/S REYNOLDS NUMBER DEL-P FRICTION MPA NUSSELT NUMBER	1 950.23 857.38 0.0 -92.85 -662.77 0.006684 0.006684 154.64 0.0 0.0	2 857.38 857.38 48.86 5992.73 0.006684 0.006684 3591.47 0.002854 15.57	3 584.52 534. 0.0 0 ~391 0.008037 0.008037 35.11 0.049807 5.53	4 328.01 328.01 -23.06 -23.06 -2791.14 0.009663 0.009663 3755.97 0.001794 17.60	5 390.36 328.01 0.0 -62.36 76.27 0.009663 0.009663 51.04 0.0 0.0

GPU-3 HYDRO	GEN 927K/339K	STIRL	ING ENGINE DA	TA: 1 (UP	DATED JAN 83)
ZONE O	JTPUT FOR CAS	E 3	CYCLE NUMBER	3 FLUX	ERROR= -1.46
ZCHE NUMBER TEMP GAS MAX K TEMP GAS AVG K WALL-GAS DEL T AVG K WALL-GAS DEL T MAX K WALL-GAS CHING Q H AVG MASS FLOH KG/S MAX MASS FLOH KG/S REYNOLDS NUMBER DEL-P FRICTION MPA NUSSELT NUMBER	1 884.01 852.98 0.0 -21.04 -674.97 0.007100 0.007100 172.74 0.0 0.0	2 862.98 862.98 43.18 6063.20 0.007100 0.007100 4012.02 0.002989 18.86	3 553.19 553.19 0.0 -421.82 0.008473 0.008473 38.47 0.048740 5.81	4 328.14 323.14 -22.13 -2957.86 0.010110 0.010110 4016.54 0.001859 19.86	5 377.61 328.14 0.0 -49.47 77.30 0.010110 0.010110 54.58 0.0 0.0
ZONE O	JTPUT FOR CAS	E 3	CYCLE NUMBER	4 FLUX	ERROR= 0.24
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K WALL-GAS DEL T AVG K WALL-GAS DEL T MAX K WALL-GAS CHING Q W AVG MASS FLOW KG/S MAX MASS FLOW KG/S REYNOLDS NUMBER DEL-P FRICTION MPA NUSSELT NUMBER	1 884.10 862.94 0.0 -21.16 -674.72 0.007101 0.007101 172.76 0.0 0.0	2 862.94 862.94 43.21 6068.71 0.007101 4012.53 0.002991 18.86	3 553.12 553.12 0.0 -421.72 0.003474 0.008474 33.48 0.048740 5.81	4 328.15 328.5 -22.13 -22.13 -2958.10 0.010109 0.010109 4017.24 0.001857 19.86	5 377.50 328.15 0.0 -49.35 77.29 0.010109 0.010109 54.59 0.0 0.0
ZONE O	UTFUT FOR CAS	E 4	CYCLE NUMBER	1 FLUX	ERROR= -5.08
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K HALL-GAS DEL T AVG K HALL-GAS DEL T MAX K HALL-GAS CHNG Q W AVG MASS FLOW KG/S MAX MASS FLOW KG/S REYNOLOS NUMBER DEL-P FRICTION MPA NUSSELT NUMBER	1 950.24 870.89 0.0 -79.35 -680.73 0.008354 0.008354 193.28 0.0 0.0	2 870.89 870.89 43.74 43.74 7331.89 0.003354 0.008354 4428.99 0.004348 21.29	3 584.52 584.52 0.0 -517.65 0.010046 0.010046 43.28 0.066046 6.25	4 333.53 333.53 -23.32 -23.32 -3610.33 0.012079 0.012079 4694.65 0.002657 22.51	5 390.36 333.53 0.0 -56.83 78.23 0.012079 0.012079 63.79 0.0 0.0
ZONE O	UTPUT FOR CAS	E 4	CYCLE NUMBER	3 FLUX	ERROR= -2.10
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K WALL-GAS DEL T AVG K WALL-GAS CEL T MAX K WALL-GAS CHNG Q W AVG MASS FLOW KG/S HAX MASS FLOW KG/S REYNOLDS NUMBER DEL-P FRICTION MPA NUSSELT NUMSER	1 891.62 870.73 0.0 -20.89 -681.71 0.008766 0.008766 211.97 0.0 0.0	2 870.73 870.73 43.87 7303.18 0.008766 0.008766 4923.20 0.004390 22.20	3 561.04 561.04 0.0 -543.17 0.010434 0.010434 46.91 0.064999 6.48	4 335.42 335.42 -24.02 -3796.10 0.012416 0.012416 4861.40 0.002763 23.14	5 385.69 335.42 0.0 -50.26 78.00 0.012416 0.012416 66.06 0 0.0

GPU-	3 HYDROGE	N 927K/339k	STIRL	ING ENGINE DA	TA: 1 (UF	DATED JAN	83)
	ZONE OUT	PUT FOR CAS	SE 4	CYCLE NUMBER	4 FLUX	ERROR=	0.23
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG HALL-GAS DEL T WALL-GAS DEL T HALL-GAS CHNG AVG MASS FLOH MAX MASS FLOH REYNOLDS NUMBE DEL-P FRICTION HUSSELT NUMBER	K AVG K MAX K Q H KG/S KG/S R I MPA	1 891.87 870.70 -21.17 -681.45 0.008764 0.008764 211.90 0.0 0.0	2 870.70 870.70 43.90 7309.28 0.008764 0.008764 4921.43 0.004390 22.20	3 561.16 561.16 0.0 -542.91 0.010431 0.010431 46.89 0.065001 6.48	4 335.46 335.46 -24.04 -3798.31 0.012412 0.012412 4859.47 0.002761 23.14	5 385.75 335.46 0.0 -50.29 77.99 0.012412 0.012412 66.03 0.0 0.0	
	ZONE OUT	PUT FOR CAS	SE 5	CYCLE NUMBER	1 FLUX	ERROR= -	3.24
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG WALL-GAS DEL T WALL-GAS DEL T WALL-GAS CHNG AVG MASS FLOW MAX MASS FLOW REYNOLDS NUMBE DEL-P FRICTION NUSSELT NUMBER	K AVG K Max K Q H Kg/S Kg/S R MPA	1 950.24 878.58 0.0 -71.66 -685.65 0.010025 0.010025 231.93 0.0 0.0	2 878.58 878.58 44.47 44.47 8585.25 0.010025 5386.60 0.006015 24.52	3 584.52 584.52 0.0 0.0 -642.12 0.012055 0.012055 52.66 0.083911 6.91	4 340.67 340.67 -24.95 -4468.59 0.014494 0.014494 5633.35 0.003698 26.05	5 390.37 340.67 0.0 -49.69 78.94 0.014494 0.014494 76.55 0.0 0.0	
	ZONE OUT	PUT FOR CAS	SE 5	CYCLE NUMER	3 FLUX	ERROR= -	1.70
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG HALL-GAS DEL T HALL-GAS DEL T HALL-GAS CHNG AVG MASS FLOH MAX MASS FLOH REYNOLDS NUMBER DEL-P FRICTION NUSSELT NUMBER	K AVG K MAX K Q W KG/S KG/S ER M MPA	1 899.65 878.68 0.0 -20.97 -687.89 0.010383 0.010383 249.49 0.0 0.0	2 878.68 878.68 44.41 44.41 8482.44 0.010383 0.010383 5794.50 0.005995 25.30	3 569.36 569.36 0.0 -667.68 0.012327 0.012327 54.85 0.082802 7.06	4 343.12 -25.96 -25.96 -4691.96 0.014632 0.014632 5642.10 0.003817 26.09	5 394.26 343.12 0.0 -51.14 78.70 0.014632 0.014632 76.67 0.0 0.0	
	ZONE OUT	PUT FOR CAS	SE 5	CYCLE NUMBER	4 FLUX	ERROR=	0.23
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG HALL-GAS DEL HALL-GAS DEL HALL-GAS CHNG AVG MASS FLOH MAX MASS FLOH REYNOLDS NUMBI DEL-P FRICTION NUSSELT NUMBI	K K T AVG K T MAX K Q H KG/S KG/S ER N MPA R	1 899.82 878.65 0.0 -21.18 -687.65 0.010381 0.010381 249.40 0.0 0.0	2 878.65 878.65 44.44 44.44 8487.48 0.010381 0.010381 5792.51 0.005995 25.29	3 569.54 0.0 -667.37 0.012322 0.012322 54.82 0.082799 7.06	4 343.17 -25.99 -25.99 -4694.95 0.014623 0.014623 5636.94 0.003815 26.07	5 394.47 343.17 0.0 -51.30 78.69 0.014623 0.014623 76.60 0.0 0.0	

GPU-3	HYDROG	EN 927K/339K	STIR	ING ENGINE DA	TA: 1 (UI	PDATED JAN	83)
	ZONE OU	TPUT FOR CAS	E 6	CYCLE NUMBER	1 FLUX	ERROR= -	5.71
ZONE NUMBER		1	2	3	4	5	
TEMP GAS MAX	к	950.23	887.46	584.52	348.15	390.36	
TEMP GAS AVG	К	887.46	887.46	584.52	348.15	348.15	
HALL-GAS DEL T	AVG K	0.0	45.05	0.0	-26.56	0.0	
HALL-GAS DEL T	MAX K	-62.78	45.05	0.0	-26.56	-42.22	
HALL-GAS CHHG Q	H	-694.52	9787.29	-771.85	-5380.79	79.85	
AVG MASS FLOH	KG/S	0.011695	0.011695	0.014064	0.016909	0.016909	
MAX MASS FLOW	KG/S	0.011695	0.011695	0.014064	0.016909	0.016909	
REYNOLDS NUMBER		270.58	6284.25	61.43	6572.08	89.30	
DEL-P FRICTION	MPA	0.0	0.007920	0.103334	0.004894	0.0	
NUSSELT NUMBER		0.0	27.59	7.52	29.47	0.0	
	ZONE OU	TPUT FOR CAS	E 6	CYCLE NUMBER	3 FLUX	ERROR=	-1.12
ZONE NUMBER		1	2	3	4	5	
TEMP GAS MAX	К	908.87	887.79	578.38	351.24	403.29	
TEMP GAS AVG	ĸ	887.79	887.79	578.38	351.24	351.24	
WALL-GAS DEL T	AVG K	0.0	44.82	0.0	-27.95	0.0	
HALL-GAS DEL T	MAX K	-21.08	44.82	0.0	-27.95	-52.05	
HALL-GAS CHIG Q	i H	-695.23	9599.50	-794,10	-5645.60	79.59	
AVG MASS FLOW	KG/S	0.011945	0.011945	0.014146	0.016750	0.016750	
MAX HASS FLOW	KG/S	0.011945	0.011945	0.014146	0.016750	0.016750	
REYNOLDS NULIBER	1	284.93	6617.71	62.25	6357.77	86.39	
DEL-P FRICTION	MPA	0.0	0.007786	0.102045	0.005009	0.0	
NUSSELT NUMBER		0.0	28.13	7.57	28.72	0.0	
	ZONE OU	TPUT FOR CAS	SE 6	CYCLE NUMBER	4 FLUX	ERROR=	0.21
ZONE NUMBER		1	2	3	4	5	
TEMP GAS MAX	К	908.98	887.77	578.64	351.30	403.67	
TEMP GAS AVG	K	887.77	887.77	578.64	351.30	351.30	
HALL-GAS DEL T	AVG K	0.0	44.84	0.0	-27.98	0.0	
WALL-GAS DEL T	MAX K	-21.21	44.84	0.0	-27.98	-52.37	
WALE-GAS CHNG Q	1 H	-695.01	9602.59	-793.73	-5649.36	79.58	
AVG MASS FLOW	KG/S	0.011942	0.011942	0.014138	0.016735	0.016735	
MAX MASS FLOW	KG/S	0.011942	0.011942	0.014138	0.016735	0.016735	
REYNOLDS NUMBER	2	284.83	6615.35	62.20	6348.23	86.26	
DEL-P FRICTICN	MPA	0.0	0.007785	0.102032	0.005006	0.0	
NUSSELT NUMBER		0.0	28.13	7.57	28.68	0.0	

#### CASE TO CASE COMPARISON INFORMATION

CASE NUMBER	1	2	3	4	5	6
AVERAGE PRESSURE MPA	2.7400	2.7400	2.7400	2.7400	2.7409	2.7400
SPEED RPM	1000.20	1500.00	1999.80	2499.60	2999.40	3499.20
GAS MASS KG	0.0003526	0.0003470	0.0003426	0.0003373	0.0003319	0.0003263
INDIC HEAT IN W	3712.12	5176.64	6595.50	7842.74	9027.50	10150.25
INDIC POWER OUT W	1224.20	1905.45	2512.94	2907.27	3183.35	3337.53
EFFICIENCY	0.3298	0.3681	0.3810	0.3707	0.3526	0.3228
EXPANSION HALL T K	801.92	839.47	862.94	870.70	878.65	887.77
EXPANSION GAS T K	801.92	839.47	862.94	870.70	878.65	887.77
WALL TO GAS NET Q H	-568.04	-633.19	-674.72	-681.45	-687.65	-695.01
P-V WORK W	2487.09	3833.79	5120.82	6436.45	7674.64	8393.79
HYSTERESIS W	0.0	0.0	0.0	0.0	0.0	0.0
COMBUSTOR TEMP K	890.00	899.00	909.00	918.00	927.00	937.00
HEATER HALL T K	858.47	895.80	906.16	914.60	923.09	932.61
HEATER GAS T K	301.92	839.47	862.94	870.70	878.65	837.77
MALL TO GAS NET Q W	3200.09	4657.77	6053.71	7309.28	8487.48	9502.59
WALL CONDUCTION W	512.03	518.87	526.80	533.46	540.02	547.66
FRICTION P-DROP MPA	0.0002402	0.0016974	0.0029907	0.0043902	0.0059948	0.0077845
REGENERATOR WALL T K	592.47	598.94	606.09	613.01	620.13	627.95
REGENERATOR GAS T K	533.44	544.71	553.12	561.16	559.54	578.64
WALL TO GAS NET Q W	-187.82	-297.49	-421.72	-542.91	-667.37	-793.73
WALL CONDUCTION M	512.03	518.87	526.80	533.46	540.02	547.66
FRICTION D-DROP MPA	0.0209092	0.0339028	0.0487396	0.0650011	0.0327990	0.1020325
WATER TEMPERATURE K	287.00	287.00	287.00	287.00	207.00	287.00
COOLER HALL T K	296.47	301.09	305.02	311.42	317.13	323.32
COOLER GAS T K	332.77	328.62	328.15	335.46	343.17	351.30
FALL TO GAS NET Q W	-1473.45	-2192.01	-2958.10	-3798.31	-4694.95	-5649.36
HALL CONDUCTION W	-1014.31	-1079.15	-1124.22	-1136.93	-1148.98	-1163.10
FRICTION P-DROP MPA	0.0006634	0.0011613	0.0018572	0.0027613	0.0038149	0.0050055
COMPRESSION HALL T K	332.77	328.62	328.15	335.46	343.17	351.30
COMPRESSION GAS T K	332.77	328.62	328.15	335.46	343.17	351.30
HALL TO GAS NET Q H	65.75	72.91	77.29	77.99	73.69	79.58
P-V HORK H	-1177.30	-1717.81	-2258.75	-2840.63	-3439.81	-4027.26
HYSTERESIS H	0.0	0.0	0.0	0.0	0.0	0.0
MAX PRESSUREMPAMIN PRESSURENPAINITIAL PRESSUREMPAP-VE PHASE ANGLE DEGSTATIC PUR LOSSMDYNAMIC PUR LOSSMFRICTION PUR LOSSMREGENATE PUR LOSSMLEAKAGE FUR LOSSMNET Q TO COLO H20M	3.6098	3.6248	3.6326	3.6291	3.6254	3.6220
	1.9415	1.9170	1.9047	1.9102	1.9160	1.9215
	3.2392	3.3199	3.3354	3.3284	3.3212	3.3143
	-249.5309	-250.1750	-250.4647	-250.3349	-250.1998	-250.0641
	-798.19	-831.86	-856.46	-866.13	-875.70	-887.10
	-325.96	-364.76	-390.17	-394.34	-397.95	-402.05
	-85.58	-210.52	-409.13	-688.55	-1060.47	-1533.94
	-143.73	-252.92	-376.60	-497.36	-621.39	-747.25
	0.0	0.0	0.0	0.0	0.0	0.0
	-2487.76	-3271.16	-4082.32	-4935.23	-5843.92	-6812.45
UNACCT PUR LOSS W	0.15	0.02	0.24	0.23	0.23	0.21
REGENATE EFFECTIVES	0.8725	0.8643	0.8574	0.8571	0.8579	0.8595

# RIOS/SEAM1 ANALYSIS CONSOLIDATED INPUT INFORMATION

ZONE	EXPANSION 1	HEATER 2	REGENERATOR 3	COOLER 4	COMPRESSION 5
VOLUME (CU M)	1.2153E-04	8.8200E-05	5.3440E-05	2.8150E-05	1.1425E-04
FLOW AREA (SQ M)	3.8600E-03	2.86408-04	1.5040E-03	2.8579E-04	3.7700E-03
WETTED AREA (SQ M)		5.8960E-02	1.4541E+00	3.7440E-02	
HYD DIA (M)	0.070100	0.003020	0.000093	0.001080	0.060400
TOT LNGTH (M)		0.246300	0.022600	0.046100	
HT EXCH LNGTH (M)		0.155400		0.035500	
TEMPERATURE (K)	927.00	927.00	584.52	339.00	339.00
REGENERATOR WALL	DIAMETER (M)	0.02262	AVG HT TRANS	F REYN EXPONENT	0.5503
MINIMUM TOTAL	VOLUME (CU M)	2.3248E-04	MAXIMUM TOTA	L VOLUME (CU M)	3.5261E-04
ANGLE AT MIN TOTAL	. VOLUME (DEG)	290.4998	ANGLE AT MAX TOT.	AL VOLUME (DEG)	128.5000
AVERAGE P	RESSURE (MPA)	2.7400	TOTAL	GAS HASS (KGS)	3.9565E-04
NORMALIZED VALU	JES FOR XMASE,	TEMP RATIO,	RVT = 0.00002	478 2.7345	2.5705

	GPU-3	HYDROGEN	927K/339K	STIRLING	ENGINE DA	TA: 1 (UP	DATED JAN 831	ļ	
1	NITE.1 1.00375	EST, TEST	1,DUMC,DUME, 59 1.55161	COEFM= 2 2 1	1.75476E- .00446 0	04 1.43051 .16819 1	E-05 0.0 .54934 2	0.0 1.00444 0	).
(VC/V) PRES P-V AN	E)*(TW) COLD F SURE RA GLE IN PE	(TC) = CRK = XTIO = XHE = RAD = BUFN =	2.5705 -0.3196 1.9296 1.5491 1.2361 0.8852	I MAXIMUM TOTAL	VDEAD JARM HORK PRESSURE XMC GAS MASS PMAX	= 4.112 = 0.714 = 1.087 = 0.165 = 0.000325 = 3643316.	9 7 4 2 5 Mean 0	PRESSURE = 27 PMIN = 18	141 XEE
			PRESSURE D	ROP INTEGR	AL				
X/L = 0.  X/L = 1.  X/L = 0.  X/L = 0.	0 10 20 30 40 50 60 70 80 90 00	INTEGRAL INTEGRAL INTEGRAL INTEGRAL INTEGRAL INTEGRAL INTEGRAL INTEGRAL INTEGRAL	= 1.2913 = 1.1441 = 1.0080 = 0.8828 = 0.7686 = 0.6652 = 0.5725 = 0.4902 = 0.4131 = 0.3555 = 0.3015	DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE =	0.3381 0.3195 0.3019 0.2852 0.2694 0.2545 0.2407 0.2280 0.2167 0.2071 0.2071 0.1997	XI1 = -0 XI1 = -0	.6967 XI .6712 XI .6428 XI .6428 XI .5739 XI .5326 XI .4352 XI .4302 XI .3653 XI .2372 XI .1918 XI	2 = 3.6494 $2 = 3.6397$ $2 = 3.6263$ $2 = 3.5921$ $2 = 3.5743$ $2 = 3.5590$ $2 = 3.5460$ $2 = 3.5517$ $2 = 3.5533$	
FLOW PR COOLER HEATER REGENATOR	INTS F = ( = 1 = 1	COM CYCLE 0.003598 0.006876 0.016730	R 21.672623 22.282150 1339.4702	65.322 105.710 1379.3	189 0. 526 0. 625 0.	006361 006080 168992	0.310025 0.214432 0.257860		
HEAT FLOW	IS = IS =	-0.4538 0.001590 0.7684 0.004830	-0.3196 3000.0 0.7147 100000000.	747.25 202.54 402.05 217.22	17 79 98 -27 22 213 13 45	.5762 -550 .1842 34 .3857 4 .6611 88	6.1641 9.5789 6.4770 6.7815		
REGENERAT	OR LOS	SES =	7 <b>19.9810</b> 0.010139	<b>125.5</b> 727 0.342775	594.4084	6.18	.76 2.73	45	
PR DYNAMIC P	INTS FI	ROM ROUTI	NE LOSSES 400.12939 94.79234	2.35135 0.99478	3 -9214 397.778	1 2 4.0 0.2 308	2769 152.5	8554	
CONDUCTIO	IN LOSS	ES	887.4648 0.026600	79.5683 0.003214	213.30 0.000	544 548. 540	0149 45.	5175	
		ZONE OUTP	UT FOR CASE	7 CYC	LE NUMBER	1 FLUX	ERROR= 1.	94	
ZONE NUMB TEMP GAS TEMP GAS WALL-GAS WALL-GAS AVG MASS AVG MASS MAX MASS REYNOLDS DEL-P FRI NUSSELT N	SER MAX AVG DEL T DEL T CHNG Q FLOH FLOH FLOH NUHBER CCTION WMBER	K K May K Max K N Kg/s 0 Mpa 0	1 950.23 886.78 0.0 -63.45 -693.06 9.011691 0.011691 270.49 6.0 0.0	2 886.78 886.78 45.66 918.57 011691 0 011691 0 282.15 007916 0 27.59	3 584.52 584.52 0.0 -766.50 .014059 .014059 61.41 .103287 7.52	4 349.58 349.58 -27.18 -5506.17 0.016903 0.016903 6569.87 0.004891 29.46	5 390.36 349.58 0.0 -40.78 79.57 0.016903 0.016903 89.27 0.0 0.0		

		GPL	1-3	HYD	ROGEN	1 9	27K/	'339K		STIRL	ING	E١	IGINE	DAT	<b>\:</b> 1	t	UFD/	TED	JAN	83)			
	4	NI	TE,	TEST	, TES1	1,		,DUM	E,CI	OEFM=	2	3.	81470	)E-05	51.	220 4	705-	114 D	.0	2	•	0.0	<b>a</b> 1
	,	1.00	144	<b>T</b>	U. 160	512		1.047	00	2	•		1305	υ.	1004	0	1.2	100		۲	1.	00332	0.1
ſ	VCZV	'E ) <del>#</del> (	( <b>T</b> M	/TC)	=	2	. 384	6					VDF4	ND =		3.9	607						
•		col	LD	HORK	=	-0	. 333	ž			i	CAR	N HOR	к =		Ū.6	955						
	PRES	SURI	ER	ATIC	) =	1	.890	1		MAXI	HUH	PR	ESSUR	RE =		1.0	937						
				XMS	=	1	.551	1					XH	1C =		0.1	685						
P-V	AN	IGLE	IN	RAD	) =	1	.223	3		TC	ITAL	G٨	S HAS	SS =	0.0	003	265		ME	AN P	RES	SURE =	2740
			P	BUEN	=	0	.889	3					PM/	τX =	362	553	57.0					PMIN =	1918
							<b>00</b> 00	CUDE	<b>D</b> ro														
vzi -	n	0		TNT	ECDAI	-	1 1	30RE	UR	00 TUL	EGR	AL n	3652		VT 1	_	-0.4	6.18		vr2	-	3 4518	
X/L =	Ň.	10		TNT	FGRAL		1	10.78			-	0. 0	3270		YT1	-	-0.0	347		XIZ	-	3 6413	
X/L =	Ŏ.	20		INT	EGRAL	: =	1.	0566		DHRE	=	Ŏ.	3099		<b>X</b> 1	Ξ	-0.6	5041		XI2	=	3.6271	
X/L =	Ō.	30		INT	EGRAL	_ =	Ó.	9304		DMRE	=	Ō.	2937		XI1	=	-0.!	5701		XI2	=	3.6979	
X/L =	0.	40		INT	EGRAL	. =	0.	8152		DHRE	Ξ	0.	2785		XI1	=	-0.!	5324		XI2	=	3.5913	
X/L =	0.	50		INT	EGRAL	. =	0.	7103		DMRE	=	0.	2644		XII	=	-0.4	4901		XI2	=	3.5733	
X/L =	0.	60		INT	EGRAL	- =	0.	6171		DMRE	=	0.	2513		XI1	4	-0.4	4419		XI2	=	3.5584	
X/L =	0.	70		INT	EGRAL	- =	0.	5338		DMRE	=	0.	2394		XI1	Ξ	-0.	5867		XI2	Ξ.	3.5435	
X/L =	υ.	80			EGRAL	- =	Ū.	4606		DNRE	=	υ.	2289		XII	Ξ	-8.	5225		X12	=	3.5%60	
X/L =	U. 1	90		- TU11	EGRAL		U. 0	3/0/			=	0.	2137			=	-0.1	2404 1566		X12 VT2	-	3.2213	
X/L -		00		101	EGRAI		υ.	.5411		District	-	υ.	.2137		XI I	-	-0.	CCCI		×12	-	3.3010	
FLO	W P8	INT	SF	ROP	CYCLE	R																	
C00	LER	=		0.00	3703		22.	0249	J2	66.	731	796	5	0.0	0638	8	1	0.313	746				
EA	TER	=		0.00	6797		22.	2435	00	104.	310	18 '	1	0.0	06 <b>01</b>	6		0.227	440				
REGEN	ATOR	!=		0.01	16224		132	29.51	68	136	52.1	587	7	0.1	6775	4	I	0.269	295				
												• •											
HEAT	FLC	IS =		-(	1.465	5	•	0.33	38	719	.98	10	2	79.5	68.	-5	623	.9570					
115 4 7		·~ -		0.0	101590			3000		204	2. JU 1 1 2	13		27.0. 17 3	614 67.1		300	5/92					
HEAT	FLUP	15 -		0 0	1.7939	, 1	0000	0.09 1000	00	21/	). 12 5 71	74	2	13.0	044 920		997	.91/9 1970	• 				
				0.0	101000		0000	,0000	•	<u>с</u> (-	1.31	эт	-	11.0	207		007						
REGEN	ERAT	OR I	109	SES	=	74	8.20	)26	1	31.360	59	6	516.8	359		6.	. 325	4	2.	5367	1		
						Ö.	0102	253	Ó	.37338	31					-							
	PF	SINT:	SF	ROM	ROUT:	INĒ	LOS	SES					3	1		2							
DYNAM	IC F	'IST	ON	LOSS	SES	- 4	01.6	57383		3.6	+476		13	397.	D	(	J.24	274	15	3.237	/06		
COND			<b>.</b>	re			94.0	1391		0.99	/4/8		378.	0295	U 4	E4		677		2 10	~		
LUNDU		ni L	055	53			00/.	.33/4	ł	79.0	2014		C 12	.40 I 0034	0	2,	1/./	5/3		10.42	000		
							V. V4	20000	,	0.00.	JC 14	r	0.0	0024	v								

GPU-3	HYDROGE	N 927K/339K	STIRLI	IG ENGINE DA	TA: 1 (UP	DATED JAN 8	3)
NITE, 1 1.0035	TEST, TES 2 0.16	T1,DUHC,DUM 847 1.551	E,COEFH= 14 2	2 7.53403E- 1.00341 0	05 7.34329 1.16852 1	E-05 0.0 .55104	0.0 2 1.00334 0.1
(VC/VE)*(TH COLD PRESSURE R P-V ANGLE IN F	KATE) = HORK = KATIO = XME = NRAD = PBUFN =	2.3777 -0.3335 1.8849 1.5509 1.2230 0.8899	MAXIM Tot	VDEAD WARM HORK M PRESSURE XMC AL GAS MASS PMAX	= 3.976 = 0.693 = 1.093 = 0.168 = 0.000326 = 3621775.	0 3 5 6 MEA 0	N PRESSURE = 2740 PMIN = 1921
		PRESSUR	DROP INTE	SRAL			
$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	INTEGRA INTEGRA INTEGRA INTEGRA INTEGRA INTEGRA INTEGRA INTEGRA INTEGRA	$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	DMRE           DMRE	= 0.3461 = 0.3279 = 0.3107 = 0.2945 = 0.2793 = 0.2651 = 0.2520 = 0.2209 = 0.2209 = 0.2144	XI1 = -0 XI1 = -0	.6594 X .6322 X .6017 X .5680 X .5300 X .4878 X .4395 X .3345 X .3203 X .2444 X .1536 X	12 = 3.6520 $12 = 3.6415$ $12 = 3.6273$ $12 = 3.6100$ $12 = 3.5913$ $12 = 3.5733$ $12 = 3.5583$ $12 = 3.5424$ $12 = 3.5460$ $12 = 3.5512$ $12 = 3.5617$
ELON DETNICE		CD					
COOLER =	0.003714	22.0406	66.8	34412 0.	006393	0.319780	
HEATER = REGENATOR=	0.006780	22.1465 1330.14	515 103.92 197 1362	21707 0. . 1294 0.	006020	0.223081 0.270037	
HEAT FLOWS =	-0.468	30 -0.33	335 748.3	2026 79.	.6120 -564	5.0273	
HEAT FLOWS =	0.00159 0.748 0.00483	00 3000 32 0.69 30 10000000	0.0         201.9           033         401.0           0.         214.0	9176 -27. 6738 213. 1055 44	.9571 35 .4816 4 .8374 88	1.2444 6.4855 57.7749	
REGENERATOR LOS	SSE <b>S =</b>	747.1277 0.010229	130.7624 0.373719	616.365	5 6.31	01 2.5	294
PRINTS I Dynamic Piston	FROM ROUT	INE LOSSES 402.14990	0 4.260	3 43 1610 78 397 881	1 2 5.0 0.2	3603 153.	22943
CONDUCTION LOS	SES	887.147 0.02660	2 79.58 0 0.0032	33 213.40 14 0.000	046 547. 340	6807 46	.4788
	ZONE OUT	FOR CAS	SE 7 C	YCLE NUMBER	3 FLUX	ERROR= -0	1.40
ZONE NUMBER TEMP GAS MAX TEMP GAS AVG HALL-GAS DEL T HALL-GAS DEL T HALL-GAS CHNG ( AVG MACS FLOH MAX MASS FLOH REYNOLDS NUMBE(	K AVG K Max K Q H Kg/S Kg/S R MPA	1 908.97 887.77 0.0 -21.20 -695.14 0.011940 0.011940 284.79 0.0	2 887.77 887.77 44.84 44.84 9599.94 0.011940 0.011940 6614.33 0.007782	3 578.45 578.45 0.0 -793.61 0.014139 0.014139 62.22 0.101996	4 351.24 351.24 -27.96 -5645.03 0.016740 0.016740 6353.54 0.005005	5 403.36 351.24 0.0 -52.11 79.58 0.016740 0.016740 86.33	
NUSSELT NUMBER		0.0	28.12	7.57	28.70	0.0	

G	PU-3 HYDRO	GEN 927K/339K	STIRLING	ENGINE DA	TA: 1 (UPDATED	JAN 83)
1 1 1.	ITE,TEST,T 00334 0.	EST1,DUMC,DUHE 16852 1.55093	,COEFM≈ 2 3 2 1	6.77109E-0 .00326 0	05 6.96182E-05 0 .16850 1.55086	.0 0.0 2 1.00319 0.1
(VC/VE) C PRESSU P-V AHGL	*(TW/TC) = OLD WORK = RE RATIO = XME = E IN RAD = PBUFN =	2.3759 -0.3338 1.8850 1.5508 1.2228 0.8896	MAXIMUM Total	VDEAD HARM HORK PRESSURE XMC GAS MASS PMAX	= 3.9720 = 0.6933 = 1.0933 = 0.1685 = 0.0003263 = 3622020.0	MEAN PRESSURE = 2740 Phin = 1921
		PRESSURE I	DROP INTEGR	AL		
X/L = 0.0 X/L = 0.10 X/L = 0.20 X/L = 0.30 X/L = 0.40 X/L = 0.60 X/L = 0.60 X/L = 0.70 X/L = 0.80 X/L = 0.90 X/L = 1.00	INTEG INTEG INTEG INTEG INTEG INTEG INTEG INTEG INTEG	IRESOURCE         IRAL         IRAL	DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE = DMRE =	0.3461 0.3279 0.3107 0.2945 0.2793 0.2652 0.2521 0.2521 0.2402 0.2297 0.2210 0.2146	$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	XI2 = 3.6520 XI2 = 3.6415 XI2 = 3.6273 XI2 = 3.6100 XI2 = 3.5913 XI2 = 3.5733 XI2 = 3.5533 XI2 = 3.5485 XI2 = 3.5460 XI2 = 3.5512 XI2 = 3.5617
FLOW PRIN COOLER = HEATER = BEGENATOR-	ITS FROM CY 0.0037 0.0067 0.0161	CLER 12 22.02677 78 22.14076 67 1329 983	9 66.806 2 103.898 4 1361 9	839 0. 178 0. 719 0	006394 0.319 006020 0.228 168078 0.270	<b>784</b> 201
RECENTION-	0.0101	1327.703	1 1301.7		100070 0.270	101
HEAT FLOWS	≠ -0.4 0.001 = 0.7 0.004	682 -0.333 590 3000. 481 0.693 830 100000000.	8 747.12 0 201.82 3 402.14 214.07	77 79. 83 -27. 99 213. 71 44.	5833 -5647.0820 9796 351.2200 4046 46.4788 8424 887.7698	
REGENERATOR	LOSSES =	746.9780 0.010228	130.7183 0.374166	616.2598	6.3090	2.5275
PRIN DYNAMIC PIS	ITS FROM RO TON LOSSES	OUTINE LOSSES 6 402.07202 94.77168	4.20555 0.99478	3 1 15967 397,866	2 .0 0.23501 70	152.58096
CONDUCTION	LOSSES	887.1206 0.026600	79.5786 0.003214	213.39 0.0003	20 547.6724 40	46.4780
	ZONE C	OUTPUT FOR CASE	7 CYC	LE NUMBER	4 FLUX ERROR:	. 0.10
ZONE NUMBER	2	1	2	3	4	5
TEMP GAS MA	х к	908.96	887.77	578.63	351.28 403	5.68
TEMP GAS AV	G K	887.77	887.77	578.63	351.28 35	1.28
HALL-GAS DE		U.U -21 10	44.84 66 84	U.U 0 0	-27.90	J.U 5 4h
WALL-GAS DE		-695 04	9599 73	-793 46	-5647 08 70	) 58
AVG MASS FL	OH KG/S	0.011938 0	011938 0	.014133	0.016729 0.01	729
HAX MASS FL	OH KG/S	0.011938 0	011938 0	.014133	0.016729 0.01	5729
REYNOLDS HU	#1BER	284.74	6613.28	62.18	6345.94 80	5.23
DEL-P FRICT NUSSELT NUP	ION MPA	0.0 0 0.0	.007780 0 28.12	101985 . 7.57	0.005003 0.0 28.68	).0

# RIOS/SEAM1 ANALYSIS CONSOLIDATED INPUT INFORMATION

ZONE	EXPANSION 1	HEATER 2	REGENERATOR 3	COOLER 4	COMPRESSION 5
VOLUME (CU M)	1.2153E-04	8.8200E-05	5.3440E-05	2.8150E-05	1.1425E-04
FLOW AREA (SQ M)	3.8600E-03	2.8640E-04	1.5040E-03	2.8579E-04	3.7700E-03
HETTED AREA (SQ M)		5.8960E-02	1.4541E+00	3.7440E-02	
HYD DIA (M)	0.070100	0.003020	0.000093	0.001030	0.060400
TOT LNGTH (M)		0.246300	0.022600	0.046100	
HT EXCH LNGTH (M)		0.155400		0.035500	
TEMPERATURE (K)	887.77	887.77	578.66	351.28	351.28
REGENERATOR HA	LL DIAMETER (H)	0.02262	AVG HT TRANS	SF REYN EXPONENT	0.5503
NINIMUN TOTA	L VOLUME (CU M)	2.3208E-04	MAXIMUM TOTA	AL VOLUME (CU M)	3.5261E-04
ANGLE AT MIN TOT	AL VOLUME (DEG)	290.4998	ANGLE AT MAX TOT	TAL VOLUME (DEG)	128.5000
AVERAGE	PRESSURE (MPA)	2.7402	TOTAL	. GAS MASS (KGS)	3.2630E-04
NORMALIZED VA	LUES FOR XMASE,	TEMP RATIO,	RVT = 0.00002	2645 <b>2</b> .5272	2.3757

NITE, TEST, TES 1 1.00319 0.16	T1,DUMC,DUME,CO 849 1.55075	EFM= 26.96 2 1.0031	182E-05 7 <b>.343</b> 2 3 0.16847	9E-05 0.0 1.55067 2	0.0 1.00306 0.1
(VC/VE)*(TH/TC) = COLD WORK = PRESSURE RATIO = XME = P-V ANGLE IN RAD = PBUFN =	2.3757 -0.3339 1.8850 1.5506 1.2228 0.8915	V WARM MAXIMUM PRES TOTAL GAS	DEAD = 3.97 WORK = 0.69 SURE = 1.09 XMC = 0.16 MASS = 0.00032 PHIX = 3622038	14 33 32 85 63 MEAN 1 3.0	PRESSURE = 2740 PMIN = 1921
X/L =       0.0       INTEGRA         X/L =       0.10       INTEGRA         X/L =       0.20       INTEGRA         X/L =       0.30       INTEGRA         X/L =       0.40       INTEGRA         X/L =       0.50       INTEGRA         X/L =       0.60       INTEGRA         X/L =       0.60       INTEGRA         X/L =       0.70       INTEGRA         X/L =       0.80       INTEGRA         X/L =       0.90       INTEGRA         X/L =       1.00       INTEGRA	PRESSURE DRO L = 1.3484 L = 1.1994 L = 1.0616 L = 0.9349 L = 0.8191 L = 0.6202 L = 0.6202 L = 0.5366 L = 0.4631 L = 0.3990 L = 0.3432	INTEGRAL         DHRE =       0.34         DHRE =       0.32         DMRE =       0.31         DMRE =       0.29         DMRE =       0.27         DMRE =       0.26         DIRE =       0.25         DMRE =       0.22         DMRE =       0.22         DMRE =       0.22         DIRE =       0.22         DIRE =       0.22	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	0.6592       XI2         0.6320       XI2         0.6014       XI2         0.5676       XI2         0.5297       XI2         0.4874       XI2         0.3840       XI2         0.3199       XI2         0.2439       XI2	= 3.6521 = 3.6415 = 3.6272 = 3.6100 = 3.5913 = 3.5732 = 3.5583 = 3.5484 = 3.5460 = 3.5512 = 3.5617
FLOW PRINTS FROM CYCL COOLER = 0.003712 HEATER = 0.0036778 REGENATOR = 0.016145 HEAT FLOWS = -0.468 0.00155 HEAT FLOWS = 0.748 0.00483	ER 22.025635 322.140823 51329.9927 32 -0.3339 30 3000.0 31 0.6933 30 10000000	66.805237 103.898529 1361.9824 746.9780 201.8173 402.0720 216.0753	0.006394 0.006020 0.168083 79.5786 -56 -27.9851 213.3920 64.8638	0.319783 0.228219 0.270172 347.8750 351.3379 46.4780 857.7883	
REGENERATOR LOSSES =	746.8032 13 0.010228 0.	214.0753 30.7051 616 .374231	.0981 6.3	3083 2.527	2
PRINTS FROM ROU DYNAMIC PISTON LOSSES CONDUCTION LOSSES	VINE LOSSES 401.99219 94.77132 887.0625 0.026600	3 4.15722 0.99478 39 79.5722 2 0.003214 0	1 2 15791.0 0 17.83521 13.3749 54 000340	.23500 152.58 7.6409 46.4	5781 5748
ZONE OU	FPUT FOR CASE	B CYCLE HU	IMBER 1 FLUX	K ERROR= 0.1	10
ZONE NUMBER TEMP GAS MAX K TEMP GAS AVG K WALL-GAS DEL T AVG K WALL-GAS DEL T MAX K HALL-GAS CHNG Q H AVG MASS FLOW KG/S MAX MASS FLOW KG/S REYNOLDS NUMBER DEL-P FRICTION MPA NUSSELT NUMBER	1 908.97 887.77 8 0.0 -21.20 -694.94 95 <sup>6</sup> 0.011938 0.0 0.011938 0.0 284.74 66 0.0 0.0 0.0 0.0 0.0 0.0 0.0	2 3 37.77 578. 37.77 578. 44.84 0. 44.84 0. 99.96 -793. 11938 0.014 11938 0.014 11938 0.014 13.27 62. 07780 0.1019 28.12 7.	4 66 351.34 66 351.34 0 -27.98 0 -27.98 28 -5647.87 13 0.016728 13 0.016728 17 6344.96 986 0.005002 57 28.67	5 403.75 351.34 0.0 -52.41 79.57 0.016728 0.016728 86.22 0.0 0.0	

#### \*\*\*\* SCHMIDT ANALYSIS VALUES ARE \*\*\*\*

PSININ	TC/TH	RESTR	SCHAA	SCHBB	SCHDEL	THETA
1.57080	0.39569	0.00203		0.00057	-0.49451	0.96302
PSTR/PM 1.2043E+00	PST 3.2997E+0	VARV0	DT 2E-08 3.	11HVOT	SUMV	SHPVOT 1.0462E+00

#### RIOS/SEAM1 ANALYSIS CONSOLIDATED INPUT INFORMATION

ZONE		EXPANSION 1	HEATER 2	REGENERATOR 3	CODLER 4	COMPRESSION 5
VOLUME (CU	(M)	1.2153E-04	8.8200E-05	5.3440E-05	2.8150E-05	1.1425E-04
FLOW AREA (SQ	(M) 3	5.8600E-03	2.8540E-04	1.5040E-03	2.8579E-04	3.7700E-03
HETTED AREA (SQ	( M )		5.8960E-02	1.4541E+00	3.7440E-02	
HYD DIA	(M)	0.070100	0.003020	0.000093	0.001080	0.060400
TOT LNGTH	(M)		0.246300	0.022600	0.045100	
HT EXCH LIIGTH	(M)		0.155400		0.035500	
TEMPERATURE	(K)	887.77	£87.77	578.66	351.28	351.28
REGEHER	ATOR HALL	DIAMETER (M)	0.02262	AVG HT TRANS	F REYN EXFONENT	0.5503
NINIM	UH TOTAL \	/OLUME (CU M)	2.3248E-04	MAXIMUH TOTA	L VOLUME (CU N)	3.5261E-04
ANGLE AT	MIN TOTAL	VOLUME (DEG)	290.4998	ANGLE AT MAX TOT.	AL VOLUME (DEG)	128.5000
	AVERAGE PF	RESSURE (MPA)	2.7402	TOTAL	GAS HASS (KGS)	3.2630E-04
NORMAL	IZED VALUE	ES FOR XMASE,	TEMP RATIO,	RVT = 0.00002	645         2.5272	2.3757

GPU-3	HYDROG	EN 927K/339	K STIRL	ING ENGINE D	ATA: 1 (UI	PDATED JAN	83)
	ZONE OU	TPUT FOR C	SE 9	CYCLE NUMBER	1 FLUX	ERROR=	0.00
ZOHE NUMBER		1	2	3	4	5	
TEMP GAS MAX	K	908.97	837.77	578.66	351.34	403.74	
TEMP GAS AVG	K	887.77	887.77	578.66	351.34	351.34	
HALL-GAS DEL T	AVG K	0.0	44.84	0.0	-27.98	0.0	
HALL-GAS DEL T	MAX K	-21.20	44.84	0.0	-27.98	-52.41	
MALL-GAS CHIIG O	а н	-694.95	9599.70	-793.29	-5647.66	79.57	
AVG MASS FLOW	KG/S	0.011938	0.011938	0.014132	0.016728	0.016728	
MAX MASS FLOW	KG/S	0.011938	0.011938	0.014132	0.016728	0.016728	
REYNOLDS NUMBER	2	284.74	6613.27	62.17	6344.94	86.22	
DEL-P FRICTION	MPA	0.0	0.007780	0.101986	0.005002	0.0	
NUSSELT NULBER		9.0	28.12	7.57	28.67	0.0	

1	1	0
т	т	7

INNER CYCLE DATA FOR CASE 9 SPEED= 3498. NET MASS= 0.000326

ANGLE	нот	COLD	PRESSURE	SCHMIDT	HORK	COLD	нот
	VOLUME	VOLUME		PRESSURE		MASS	MASS
	CU.CM	CU.CH	MPA	MB7	HATIS	GMS	CIIS
0.0	93.576	10.931	3.3143	4.0090	0.0	0.010560	0.041327
10.00	102.679	11.203	3.2185	3.6681	1785.34	0.010537	0.044335
20.00	111.214	12.010	3.1204	3.3303	3511.41	0.011151	0.046881
30.00	118.852	13.458	3.0209	3.0160	5138.30	0.012323	0.048360
40.00	125.260	15.708	2.9202	2.7357	6637.62	0.014202	0.050173
50.00	130.111	18.945	2.8178	2.4928	7990.44	0.016837	0.050735
60.00	133.112	23.355	2.7134	2.2865	9185.43	0.020449	0.050481
70.00	134.026	29.092	2.6080	2.1141	10217.06	0.024907	0.049354
80.00	132.685	36.251	2.5024	1.9721	11083.83	0.030215	0.047403
90.00	129.020	44.835	2.3982	1.8571	11786.46	0.035252	0.044668
100.00	123.059	54.741	2.2976	1.7659	12326.41	0.042837	0.041273
110.00	114.952	65.730	2.2029	1.6960	12704.50	0.049740	0.037369
120.00	104.971	77.419	2.1172	1.6452	12919.50	0.055698	0.033128
130.00	93.511	89.271	2.0433	1.6121	12967.11	0.063438	0.028732
140.00	81.085	100 <b>.607</b>	1.9842	1.5957	12839.14	0.069681	0.024361
150.00	63.298	110.638	1.9430	1.5954	12523.57	0.075163	0.020183
160.00	55.805	118.537	1.9230	1.6113	12005.88	0.079633	0.016344
170.00	44.245	123.556	1.9270	1.6438	11271.96	0.082894	0.012959
180.00	34.163	125.171	1.9579	1.6939	10312.92	0.084764	0.010109
190.00	25.928	123.201	2.0178	1.7631	9130.43	0.035139	0.007837
200.00	19.712	117.865	2.1082	1.8535	7741.05	0.033955	0.006153
210.00	15.503	109.717	2.228	1.9676	6178.73	0.081235	0.005050
220.00	13.165	99.518	2.3771	2.1085	4495.51	0.077074	0.004513
230.00	12.504	88.097	2.5483	2.2798	2760.77	0.071632	0.004527
240.00	13.318	76.233	2.7359	2.4848	1053.75	0.065148	0.005063
250.00	15.427	64.593	2.9303	2.7264	-515.62	0.057916	0.006136
260.00	13.680	53.697	3.1196	3.0055	-1863.39	0.050293	0.007757
270.00	22.959	43.915	3.2912	3.3187	-2891.73	0.042693	0.009920
280.00	28.172	35.470	3.4337	3.6559	-3525.27	0.035505	0.012559
290.00	34.245	28.456	3.5385	3.9972	-3716.72	0.023073	0.015700
300.00	41.108	22.857	3.6012	4.3107	-3453.51	0.023624	0.019161
310.00	48.694	18.572	3.6221	4.5559	-2758.54	0.019257	0.022866
320.00	56.919	15.442	3.6056	4.6926	-1685.07	0.015944	0.026702
330.00	65.678	13.280	3.5587	4.6951	-307.33	0.013569	0.030562
340.00	74.832	11.902	3.4896	4.5628	1290.40	0.011975	0.034347
350.00	84.205	11.153	3.4059	4.3208	3023.77	0.011005	0.037964
359.00	92.646	10.931	3.3235	4.0421	4635.91	0.010583	0.041002

COLL_7	UVDBOCTH	0274 /7704	OTTOL THE	THETHE			1464		
0-0-3	NIUKUBEN	72/11/ 3371	SITKLING	EUGTUE	UAIA:	LUPDATED	JAN	ວວງ	

CASE TO CASE COMPARISON INFORMATION

CASE NUMBER	7	8	9
AVERAGE PRESSURE MPA	2.7400	2.7400	2.7400
SFEED RFM	3498.00	3498.00	3498.00
GAS MASS KG	0.0003263	0.0003263	0.0003263
INDIC HEAT IN W	10147.40	10147.60	10147.34
INDIC POWER CUT W	3337.09	3336.62	3336.67
EFFICIENCY	0.3289	0.3288	0.3288
EXPANSION WALL T K	887.77	887.77	887.77
EXPANSION GAS T K	887.77	887.77	887.77
WALL TO GAS NET Q H	-695.04	-694.94	-694.95
P-V MORK H	8895.87	8896.36	8896.37
HYSTERESIS H	0.0	0.0	0.0
COLEUSTOR TEMP K	937.00	937.00	937.00
REATER WALL T K	932.61	932.61	932.61
HEATER GAS T K	837.77	887.77	887.77
WALL TO GAS NET Q W	9599.73	9599.96	9599.70
WALL CONDUCTION W	547.67	547.64	547.64
FRICTION P-DROP MPA	0.0077799	0.0077799	0.0077799
REGENERATOR HALL T K	627.96	627. <b>98</b>	627.98
REGENERATOR GAS T K	578.63	578.66	578.66
HALL TO GAS NET Q H	-793.46	-793.28	-793.29
HALL CONDUCTION H	547.67	547.64	547.64
FRICTION P-DROP MPA	0.1019847	0.1019855	0.1019857
WATER TEMPERATURE K	287.00	287.00	287.00
COOLER HALL T K	323.30	323.35	323.35
COOLER GAS T K	351.28	351.34	351.34
HALL TO GAS NET Q W	-5647.08	-5647.87	-5647.66
HALL CONDUCTION W	-1163.14	-1163.01	-1163.01
FRICTION P-DROP MPA	0.0050025	0.0050024	0.0050024
COMPRESSION HALL T K	351.28	351.34	351.34
COMPRESSION GAS T K	351.28	351.34	351.34
WALL TO GAS NET Q H	79.58	79.57	79.57
P-V HORK H	-4026.10	-4027.05	-4027.01
HYSTERESIS H	0.0	0.0	0.0
MAX PRESSURE MPA MIN PRESSURE MPA INITIAL PRESSURE MPA P-VE PHASE ANGLE DEG STATIC PHR LOSS H FRICTION PHR LOSS H REGENATR PHR LOSS H LEAKAGE PHR LOSS H	3.6220 1.9215 3.3143 -250.0633 -887.12 -402.07 -1532.68 -746.98 0.0	3.6221 1.9215 3.3143 -250.0625 -887.06 -401.99 -1532.69 -746.80 0.0	3.6221 1.9215 3.3143 -250.0627 -887.07 -402.00 -1532.69 -746.81 0.0
UNACCT PHR LOSS H REGENATR EFFECTVNS	0.10	0.10	0.00

GPU-3 HYDROGEN 927K/339K STIRLING ENGINE DATA: 1 (UPDATED JAN 83) THIS RUN ENDED AT TIME 11.33.38 THE ELAPSED TIME FOR THIS RUN IS 15.86

## APPENDIX C DEFINITIONS

VARIABLE COMBO BLOC	N CALC. IN K ROUTINE	DEFINITION/UNITS
	а) тырыт	-GAS PRESSURE TH ADDED VOLUME (MPA)
ΔΠΡΔΠΔ ( ΕΔΠ	DI TNPHT	-RADIATION SURFACE AREA TERM (SQ M)
	D) INFILT	-GAS TENDEDATIDE IN ADDED VOLUME (K)
ADVOL ( EAD		-GAS TENECRATORE IN ADDED VOLUNE (R)
		- SEEECTIVE LENGTH FOR AVIAL WEAT CONDUCTION
ADRAEK ( FAD		ALONG DISPLACER SHELL (M)
ADRLDI ( FAD	DJ INPUT	-WALL INNER DIAMETER OF ADDED VOLUME (M)
ADHLTH ( FAD	D) INPUT	-WALL THICKNESS OF ADDED VOLUME (M)
AFC (RICS	F) RIOSIN	-COOLER TOTAL FLOW AREA (SQ M)
AFH (RIOS	F) RIOSIH	-HEATER TOTAL FLOW AREA (SQ M)
AFLOH (FLCEL	L) INPUT	-GAS FLOW AREA PER TUBE FOR A CELL (SQ M)
AFR (RIOS	F) RIOSIN	-REGENERATOR TOTAL GAS FLOW AREA (SQ M)
ALOS <b>SC</b> (	) HTFLOW	-CCOLER EXPANSION/CONTRACTION FRICTION POMER LOSS (H)
ALOSSE (	) HTFLON	-HEATER EXFANSION/CONTRACTION FRICTION POMER LOSS (H)
AMETAL (	) LOSSES	-REGENERATOR METAL DIFFUSIVITY (SQ.M/SEC)
ANGLE (VARVO	L) INITAL	-CRAHK ANGLE (RADIANS)
	RIDSIN	
ARG ( PTOS		-PRESSURE TO VOLUME PHASE ANGLE (RADIANS)
ADODE (	) THTTAI	-CONSCIENTIONAL ABEA OF EVENNETON DIGTON
ANODE (	VOLUME	DOD (CO N)
ACDECT (FLORE)		ROU ( 34 11) RATTO OF CHORT (LONG CTREC FOR
ASPECT (PECEL		RECTANGULAR DUCT
AWC (RIOS	FJ RIOSIN	-COOLER TOTAL WETTED AREA (SQ M)
ANET (FLCEL	L) INPUT	-WETTED AREA PER TUBE OF A CELL (SQ M) Hyd dia = volume / Awet
AWH (RIOS	F) RIOSIN	-HEATER TOTAL HETTED AREA (SQ M)
AHR (RIOS	F) RICSIN	-REGENERATOR TOTAL HETTED AREA (SO M)
AXHALL (FLCEL	L) INPUT	-CROSS-SECTIONAL AREA OF WALL FOR HEAT CONDUCTION (SQ M) FOR ONE TUBE
C (RIOS	D) RIOSIN	-COMPRESSION ZONE TOTAL DIMENSIONLESS VOLUME
CBUF ( RIOS	D) RIOSIN	-COMPRESSION BUFFER ZONE TOTAL DIMENSIONLESS
		-COMERESSION ZONE TOTAL DIMENSIONLESS VOLUME
		AT THE REGINNIC OF THE STRENDICESS TOUCHE
		-COMPRESSION DISTON AREA (CO M)
CHEAF CVARVO	NET INITAL	-CONDECCION CYLINDED DODE (N)
CHIPBUK LVARVU	NU INLIAL	CONFRESSION CILINDER BURE (N)
LIPCK IFLIGE	INPUT	-LOMPRESSION PISION LRANK RAUIUS (M)
CMPCRL (FLIGE	NI INPUT	LENGTH (M) SHOULD BE LESS THAN 1000*CMPCR
CMPDEL (VARVO	)L) VOLUME	-OVERLAP IN COMPRESSION ZONE PISTON MOTION TYPICAL OF DISPLACER MACHINES (M)
CMPDV (FLTGE	EN) INPUT	-COMPRESSION ZONE DEAD VOLUME (CU M)
	INITAL	WILL BE TREATED THE SAME AS ACTIVE VOLUME
		IF WILL RE ANTARATIC IN SEAM 1
CHPECC (FLTG	EN) INPUT	-COMPRESSION PISTON CRANK RADIUS
		-COMPRESSION RIGION CVIINNER HALL CAR (M)
CHPMAX (VARVO	DL) VOLUME	-COMPRESSION PISTON MAXIMUM STROKE POSITION

VARIADLE	COMMON BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
CMFMIN	(VARVOL)	VOLUHE	-COMPRESSION PISTON MINIMUM STROKE POSITION
CHPPOS	(VARVOL)	VOLUHE	-CONPRESSION PISTON CURRENT STROKE POSITION (M)
CMFRD	(FLTGEN)	INPUT	-COMPRESSION PISTON ROD DIAMETER (M)
CMPSRK	(VARVOL)	VOLUME	-CONFRESSION PISTON NET STROKE (M)
CONVER	()	HTFLOH	-CONVERSION FACTOR TO CHANGE WORK TERMS TO FOWER TERMS FOR A DESIGN
CPGAS	(GASFRP)	INITAL	-REFERENCE VALUE OF GAS SPECIFIC HEAT
		HTFLOW	AT CONSTANT PRESSURE (J/KG-K)
CRANK	(VARVUL)	TNTTAL	-CRARK ARGLE BETHEEN THE OF EXPANSION AND
CRANKD	(FLTGEN)		-SAME AS CRANK (DEGREES)
CTU		DIGEN	-COOLED TOTAL LENGTH (M) -
CTIE	( 21055)	PTOSTN	-COOLER TOTAL LENGTH (H)
CVGAR	(GASEPP)	TNTTAL	-REFERENCE VALUE OF GAS SPECTETC HEAT
CIONS	CORDINE	HTFLOH	AT CONSTANT VOLUME (J/KG-K)
DARFRC	( PDEOP)	HTFLOH	-DARCY FRICTION FACTOR IN THE COOLER
DARFRH	( POROP)	HTFLCH	-DARCY FRICTION FACTOR IN THE HEATER
DARFRR	( PDCOP)	HTFLOH	-DARCY FRICTION FACTOR IN THE REGENERATOR
DC	( RIOSD)	RIOSIN	-COMPRESSION ZONE VOLUMETRIC TIME DERIV AT MID STEP (DIMENSIONLESS/RAD)
DCI	( RIOSD)	RIOSIN	-COMPRESSION ZONE VOLUMETRIC TIME DERIV AT BEGINING OF STEP (DIMENSIONLESS/RAD)
DE	( RIOSD)	RIOSIN	-EXPANSION ZONE VOLUMETRIC TIME DERIV AT MID STEP (DIMENSIONLESS/RAD)
DEI	( RIOSD)	RIDSIN	-EXPANSION ZONE VOLUMETRIC TIME DERIV AT BEGINNING OF STEP (DIMENSIONLESS/RAD)
DELANG	(VARVOL)	INITAL	-CRANK RADIANS PER TIHE STEP (RAD)
DFREQ	()	INPDRV	-CHAMGE IN FREQUENCY IN EACH Perturbation (HZ)
DH	(FLCELL)	INFUT	-HYDRAULIC DIAMETER OF A CELL (M)
DPR	( RIOSD)	HTFLOW	-ARRAY CONTAINING THE DIMENSIONLESS PRESSURE
		CYCLER	CHANGE OVER A STEP
DSTRK		INPORV	-CHARGE IN STROKE RATIO IN EACH PERTURBATION
DTIME	( ANISC)	INITAL	-TIME STEP (SEC)
570181	(VARVUL)	VULUNE	SAME NUMBERING SCHEME AS VOL
E	( R1050)	RIUSIN	AT THE MID TIME STEP
EBUF	( RICSD)	RIOSIN	-EXPANSION BUFFER ZONE TOTAL DIMENSIONLESS Volume at the mid time step
EI	( RIOSD)	RIOSIN	-EXPANSION ZONE TOTAL DIMENSIONLESS VOLUME AT THE BEGINING OF THE STEP
EMIS	( FADD)	INPUT	-EMISSIVITY OF THE DISPLACER RADIATION Shields
ERR	()	CONVRG	-MAXIMUM FRACTIONAL CHANGE IN COOLER HEAT FLOW TERMS
EXPAP	(VARVOL)	INITAL	-EXPANSION PISTON AREA (SQ M)
EXPBOR	(VARVOL)	INITAL	-EXPANSION CYLINDER BORE (M)

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VARIABLE	CONTION BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
EXPCR	(FLTGEN)	INPUT	-EXPANSION PISTON CRANK RADIUS (M)
EXPCRL	(FLTGEN)	INPUT	-EXPANSION PISTON CONNECTING ROD
EXPDV	(FLTGEN)	INPUT INPURV	-EXPANSION ZONE DEAD VOLUNE (CU M) WILL BE TREATED THE SAME AS ACTIVE VOLUME TE WILL BE ADIABATIC IN SEAM 1
EXPECC	(FLTGEN)	INPUT	-EXPANSION PISTON CRANK RADIUS ECCENTRICITY (M)
EXEGAP	(FUTGEN)	TNPUT	-EXPANSION PISTON CYLINDER UALL GAP (M)
EXPLIAX	(VARVOL)	VOLUME	-EXPANSION PISTON NAVIMUH STOCKE POSITION
CALIBA	( Patrol /	TOLONE	(M)
EXPHIN	(VARVOL)	VOLUME	-EXPANSION PISTON MINIMUM STRCKE POSITION
EXPPOS	(VARVOL)	VOLUHE	-EXPANSION PISTON CURRENT STROKE POSITION (M)
EXPRO	(FLTGEN)	INPUT	-EXPANSION PISTON ROD DIAMETER (M)
EXPSRK	(VARVOL)	VOLUME	-EXPANSION PISTON NET STROKE (M)
FREQ	(FLTGEN)	INPUT	-FREQUENCY (HZ)
		INFORV	
FRICML	(FLCELL)	INPUT	-FRICTION MULTIPLIER FOR A CELL
FUNCC		VOLUME	-STATEMENT FUNCTION USED TO COMPUTE THE ABSOLUTE AXIAL POSITION OF THE COMPRESSION PISTON (M)
GAMMA	(GASPRP)	INITAL	-REFERENCE SPECIFIC HEAT RATIO
GRAFIC	( OUTPT)	CYCLER	-ARRAY CONTAINING CYCLIC DATA AT 5 DEGREE INTERVALS CURRENTLY CONTAINS: 1-ANGLE, 2-EXP VOL, 3-PRESS, 4-CMP VOL, 5-CMP MASS, 6-EXP MASS, 7-CMP PIS TORQ, 8-CMP TEMP, 9-EXP TEMP, 10-EMPTY
HAF	( AMISC)	INPUT	-0.5
HASC	( )	HTFLOW	-HEAT TRANSFER CONDUCTANCE FROM THE GAS TO THE COOLER WALL (W/K)
HASH	( )	HTFLOH	-HEAT TRANSFER CONDUCTANCE FROM THE GAS TO THE HEATER HALL (W/K)
HCEXT	(FLCELL)	INPUT	-HALL TO ENVIRONS HEAT TRANSFER COEFFICIENT (W/SQ.M-K)
HCMBST	()	HTFLOW	-HEAT TRANSFER COEFFICIENT BETHEEN THE HEATER WALL AND THE COMBUSTION GAS (W/SQ.M-K)
HCV	( RIOSF)	CYCLER RIOSIN	-DIMENSIONLESS COOLER DEAD VOLUME
KHV	( RIOSF)	RIOSIN	-DIMENSIONLESS HEATER DEAD VOLUME
HRV	( RIOSF)	CYCLER	-DIMENSIONLESS REGENERATOR DEAD VOLUME
		RIOSIN	
HTLL	( RIOSF)	RIOSIN	-HEATER TOTAL LENGTH (M)
HTLS	( RIOSF)	RIOSIN	-HEATER TOTAL HEATED LENGTH (M)
HYSTE	(FLTGEN)	INPUT	-THERMAL HYSTERSIS FACTOR
TACOND	( [000]	INPLIT	-KEY FOR CONDUCTION BETWEEN VARIABLE AND
TALEAV	( TADD)	TNPLIT	ADDED VOLUMES
THEEKU	. 1400)	- 11 VI	ADDED VOLUMES
IAHTL	( IADD)	INPUT	-KEY FOR HALL MATERIAL IN ADDED VOLUMES

VARIABLE	11 14	ionanian Block	CALC. IN ROUTINE	DEFINITION/UNITS
IATYPE	(	IADD)	INFUT	-KEY FOR ADDED VOLUME DESCRIPTION CURRENTLY USES: 10-PSITON DOME OR DISPLACER (VOL A) 20-COLD PISTON BUFFER SPACE (VOL C) 25-HOT PISTON BUFFER SPACE (VOL B)
				40-CRANKCASE (VOL D)
ICHNG	ç	IGEN)	INPUT	-KEY TO USE PERTURBATION SYSTEM
ICPGAS	i.	JUILECI	THTIAL	-CAS HEAT CAPACITY IDENTIFIER
ICPM	t	JHISC)	INITAL	-METAL HEAT CAPACITY IDENTIFIER SET TO 27, COEFFICIENTS IN NEXT BLOCK DATA
IDESGN	ſ	IGEN)	INPUT	-KEY TO DETERNINE ENGINE TYPE 1-IN LINE, 2-DBLE ACTING, 3-DISPLACER
IDRIVÉ	(	IGEN)	INPUT	-KEY TO DETERMINE DRIVE MECHANISH D-CONNECTING ROD, 1-RHOMBIC DRIVE
IERROR	(	JHISC)	MAIN CCHVRG INPDRV INPUT INITAL VOLUME ANALIS	-GENERAL ERROR KEY IF <b>0</b> , NO ERROR
IGAS	(	IGEN)	INPUT	-WORKING FLUID BEING USED 1-Hydrogen 2-Helium 3-Nitrogen 4-Air 5-CO2 6-Methanf
IGRAPH	l	IGEN)	INPUT	-KEY FOR GRAPHICAL OUTPUT
IKGAS	(	JMISC)	INITAL	-GAS THERMAL CONDUCTIVITY IDENTIFIER SET TO 18, COEFFICIENTS IN NEXT BLOCK DATA
IKM	t	JMISC)	INITAL	-METAL THERMAL CONDUCTIVITY IDENTIFIER SET TO 18, COEFFICIENTS IN NEXT ELOCK DATA
IMASS	(	IGEN)	INPUT	-KEY TO DETERMINE CONSTANT MASS OR MEAN PRESSURE 0-P FIXED, 1-M FIXED
IMOD	(	JMISC)	INPORV	-CURRENT STEP IN PERTURBATION (0-NMODS) IF LT 0, THEN ON LAST CASE.
INCH	(	IGEN)	INPUT	-KEY FOR INERTIAL EFFECTS CALC
IMUGAS	(	JHISC)	INITAL	-GAS DYNAMIC VISCOSITY IDENTIFIER
IND	(	)	CYCLER	SET TO 6, COEFFICIENTS IN NEXT BLOCK DATA -KEY FOR INTEGRATION BOUNDARY CONDITIONS
IPRT1	(	IGEN )	INPUT	1-MASS INCREASE BOTH VOLUMES 2-MASS INCREASE HOT VOLUME 3-MASS INCREASE COLD VOLUME 4-MASS DECREASE BOTH VOLUMES -KEY TO PRODUCE ADDED PRINTS 0-NO ADDITIONAL PRINTS 1-ADDED INITIALIZATION PRINTS 2-CYCLE BY CYCLE PRINTS 3-DETAILED WITHIN CYCLE PRINTS 4-CYCLE WRAPUP PRINTS
IRGAS	ť	JMISC)	INITAL	-GAS CONSTANT IDENTIFIER SET TO 0, COEFFICIENTS IN NEXT BLOCK DATA

١	ARIABLE	(	DOMUCN BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
	IRHCH	(	JMISC)	INITAL	-METAL DENSITY IDENTIFIER SET TO 36, CREEFICIENTS IN NEXT BLOCK DATA
	IRUN	(	)	NAIN	-CURRENT CASE NUMBER
	ITHLCH	(	j	INPORV	-KEY FOR COMBUSTION TEMPERATURE CHANGE
			-		WITH PERTURBATION STEP, INCD
	JCELL	(	JMISC)	INFUT	-CELL NUMBER BEING INPUT, AFTER INPUT
				0011	COMPLETED JCELL=TOTAL NUMBER OF CELLS
					IN THE ENGINE. ON LAST STEP JCELL IS SET
					TO 0 TO KEY TIMERS.
	JCOLN	(	JMISC)	INITAL	-LAST COOLER CELL
	JCOL1	ł	JHISC)	INITAL	-FIRST COOLER CELL
	JCOOL	l	JHISC)	INITAL	-HIDDLE COOLER CELL
	JFIXN	(	JHISC)	INITAL	-LAST CONSTANT VOLUME CELL
	JFIX1	(	JMISC)	INITAL	-FIRST CONSTANT VOLUME CELL
	JHOT	(	JMIEC)	THITAL	-NIODLE HEATER CELL
	JHTEN	(	JHISC)	INITAL	-LAST HEATER CELL
	JHTR 1	(	J:119C)	INITAL	-FIRST HEATER CELL
	JREG	C	JHISC)	IHITAL	-MIDDLE REGENERATOR CELL
	JREGN	(	JHISC)	INITAL	-LAST REGENERATOR CELL
	JREG1	(	JHISCI	INITAL	-FIRST REGENERATOR CELL
	EHTRF	C	INCELL)	INFUT	-FRICTION TO NUSSELT NUMBER CORRELATION
	MQFLOH	ť	INCELL)	INPUT	-CELL GAS TO WALL TO EXTERNAL ENVIRONS
	-				HEAT FLOW CALCULATION,
					O-CONSTANT T HALL, 1-CONSTANT Q HALL
					2-CONSTANT T GAS , 3-NO HET Q HALL
	MTLHAL	(	INCELL)	INPUT	-NETAL USED IN WALL
					7-AL 2024 T4 8-COPPER
					9-INCONEL X750 10-K MONEL
					11-304 SS 12-310 SS
					13-316 SS 14-TI 120VCA
					15-NI
	MTLHIR	ſ	INCELL)	INFUT	-HETAL USED IN FILLER MATERIAL
				<b>B</b> 11-1-1-	USED IN REGENERATORS, NUMBER AS MILWAL
	MTYPE	l	INCELLJ	INFUT	-COMPONENT DESCRIPTION OF CELL:
					10-TUBE OR CYCLINDER TT-RECT DUCT
					17 ODJETOR CONVECTOR
					22 VARIADLE COLD VOL 21 DICRACER CIDE 20
					20-VARIABLE LULU VUL 21-UISPLAUER SIDE 20
					CAPTISTUM STUE ZU ZO-VARTABLE DUT VUL
					32_MET HET BEGEN 37_GIDE GUEET BEGEN
					34-THDE DECEMEDATOD
	NADD	(	TGEN )	тырит	-NUMBER OF ADDED COMPONENTS
	NCASE	ì	105117	MATN	-CURRENT OUTPUT CASE MUNRER, SEE TRUM
	NCHPRC	ì	JHTSC	TNPLIT	-FIRST, KEY, CELL TN COMPRESSION ZONE
	NCODE	ì	IGEN)	INPUT	-KEY FOR ANALYSTS MODULE
		•			D-RIOS, 1-URIELI, 2-TEN
					IF GT 9, OPTIMIZATION ALSO IN EFFECT.
	NCOMP	ſ	IGEN)	INPUT	-NUMBER OF COMPONENTS INPUT, <= JCELL
	NCYCLE	ĺ	JMISC)	ANALIS	-CURRENT CYCLE NUMBER, <=NREVL

VARIABLE	C	COMMON BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
NCYL	(	IGEN)	INPUT	-NUMBER OF CYLINDERS IN ENGINE
NDIV	(	)	CYCLER	-NULBER-EXPANSION SET TO NEED 22
NDS	ſ	)	HTFLOW	-NUMBER OF AXIAL DIVISIONS USED BY PDINT TO SUBDIVIDE INTEGRAL FOR MASS FLUX TERMS SET TO 10
NIHX	С	INCELL)	INPUT	-NUIBER OF HEAT EXCHANGERS REPRESENTED
NMODS	ť	)	INPDRV	-NUMBER OF PERTURBATIONS TO BE RUN, USED TO
NOPT	ſ	IGEN)	INPUT	-HEAT FLOW OPTION USED IN COOLING WATER O-QDYNAM+QSTATC DIRECT TO WATER 1-QDYNAM+QREGHL+QCYLML TO WATER 2-QREGHL+QCYLML DIRECT TO WATER 3-ONLY QREGWL DIRECT TO WATER (ALL OTHER HEAT FLOWS TO THE GAS THRU THE CCOLER INTO THE WATER)
NOPT1 NPRT1	()	INCELL) IGEN)	input Infut	-NOT USED, CELL DEPENDENT INTEGER -PRINT FREQUENCY WITHIN THE CYCLE I SET THIS TO 2*NSTEP TO EDIT EVERY OTHER CASE, CONTROLS OUTPUT OF VECTR IT HILL BE MORE RELEVANT IN SEAM 2 OR SEAM 3
NPRT2 NREVL	( (	IGEN) IGEN)	INPUT INPUT	-NUNBER OF CASES TO BE EDITTED TOGETHER -MAXIMUM NUMBER OF CYCLES TO BE COMPUTED
NOTHER	٢	TADBL	TNRUT	-NUMBER OF RINGS FOR LEAKAGE CALC
NCULID	ì		TNPUT	-NUMBER OF SHIELDS IN RISPLACER
NSTEP	ì	TGENI	TNEUT	-NUMBER OF STEPS IN & REVOLUTION
NSTRK	ì	INTSCI	TNEDRY	-KEY FOR STROKE (1) OR EREQUENCY (0)
NTITLE	(	JMISC)	INPUT	VARIATION WITH CASE -CARD IMAGE OF FIRST INPUT CARD THIS AFPEARS ON TOP OF EACH PAGE AND IS OUTPUT WITH GRAPHICS, I USE THE FIRST
NVOLA	(	JHISC)	INPUT	-ADDED VOLUME COMPONENT REPRESENTING
NVOLB	ť	JHISC)	INPUT	-ADDED VOLUME COMPOHENT REPRESENTING
NVOLC	ł	JMISC)	INPUT	-ADDED VOLUME COMPONENT REPRESENTING
NVOLD	(	JMISC)	INPUT	-ADDED VOLUME COMPONENT REPRESENTING
NZONES	ſ	JHISC)	RIOSPR	-NUMBER OF COMPUTATIONAL ZONES TO BE USED IN CALCULATION, SEAM 1 USES 5
OHEGA	(	AMISC)	INITAL	-FREQUENCY (RAD)
ONE	Ċ	AMISC)	INPUT	-1.000
ORIFCE	(	FLCELL	INPUT	-CELL ORIFICE PRESSURE DROP COEFFICIENT Equ'Ivalent to constant famming friction
PDROPC	(	PDROP)	HTFLOW	-FRICTION PRESSURE DROP IN COOLER (PA)
PDROPH	(	PDROP )	HTFLOW	-FRICTION PRESSURE DROP IN HEATER (PA)
PDROPR	(	PDROP )	HTFLOW	-FRICTION PRESSURE DROP IN REGENERATOR (PA)

VARIABLE	BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
PGAS	(FLCELL)	INPUT	-GAS PRESSURE IN CELL (PA)
PGASAD	(DYNPRP)	INITAL CYCLER	-CURRENT VALUE OF GAS PRESSURE IN ADDED Volumes (PA)
PGASD	(DYNPRP)	INITAL	-CURRENT VALUE OF GAS PRESSURE IN CELLS (PA)
FHASED	(FLTGEN)	INPUT INITAL INPDRV	-CRANK ANGLE BETHEEN EXPANSION VOLUME MINIMUM AND COMPRESSION VOLUME MINIMUM (DEG)
PHASER	(VARVOL)	VOLUME INITAL	-SAME AS PHASED (RAD)
PI	( AMISC)	INPUT	-3.14159
PIOV4	( AMISC)	INPUT	-PI / 4
PITER	( )	CYCLER	-INHER ITERATION INITIAL DIMENSIONLESS PRESSURE VALUES
PMAX	(ENFLOW)	HTFLCH RIOSIN	-CURRENT MAXIMUM PRESSURE IN CYCLE (PA)
PMEAN	(FLTGEN)	INPUT INITAL	-MEAN PRESSURE IN CYCLE (PA)
PMEAND	(DYNPRP)	INITAL RIOSIN HTFLON	-CURRENT MEAN PRESSURE IN CYCLE (PA)
PMIN PHXANG	(ENFLOW) (ENFLOW)	HTFLOW HTFLOH	-CURRENT MINIHUM PRESSURE IN CYCLE (PA) -CRANK ANGLE AT WHICH PRESSURE REACHES A Maximum (DEG)
PNAVG	()	HTFLOH	-DIMENSIONLESS AVERAGE PRESSURE IN CYCLE
PNHAX POROS	( RIOSF) (FLCELL)	HTFLOW INPUT	-DINENSIONLESS MAXIMUM PRESSURE IN CYCLE -POROSITY, VOID FRACTION, OF FILLER
		AMALTO	NET DOUED IN ENGINE (LATTE)
PR	( RIOSD)	CYCLER	-DIMENSIONLESS PRESSURE AT EACH STEP IN CYCLE
PSIMIN	(VARVOL)	VOLUME	-ABSOLUTE ANGLE AT NHICH THE COMPRESSION ZONE VOLUME IS A MINIMUM (RAD)
PSISTR	(VARVOL)	VOLUME	-ABSOLUTE ANGLE AT WHICH THE EXPANSION Zone volume is a minihum (rad)
PST	()	INITAL	-SCHMIDT ANALYSIS DETERMINED INITIAL Pressure (PA)
PSTOPM	( )	INITAL RIOSIN	-RATIO OF STARTING PRESSURE TO AVERAGE FRESSURE, BASED ON SCHMIDT ANALYSIS
QACTC	(ENFLOW)	HTFLOH	-GAS TO COOLER WALL HEAT FLOW (W)
QACTH	(ENFLOW)	HTFLON	-GAS TO HEATER HALL HEAT FLOH (H)
OCYLHL	(ENFLOW)	LOSSES	-HEAT FLOH ALONG CYLINDER HALL (W)
QDYHAM	(ENFLCH)	LOSSES	-SUM OF HEAT FLOW DUE TO QEXPGP+QEXPSH (W)
QEXPGP	()	LOSSES	-HEAT FLOW DUE TO PISTON GAP PRESSURIZATION (H)
QEXPSH	()	LOSSES	-HEAT FLOW BETWEEN PISTON AND CYLINDER HALL Due to the relative motion (#)
QFLON	(FLCELL)	INPUT	-HEAT FLOW FROM CELL WALL TO EXTERNAL Environment (W)
QFRIC	(ENFLOW)	KTFLOW	-TOTAL FRICTIONAL HEAT FLOW (W)

.

VARIABLE	COMITION BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
QHTRFR QHYSTC	(    ) (ENFLOH)	HTFLOW	-HEAT FLOW DUE TO HEATER FRICTION (H) -HYSTERESIS HEAT FLOW IN COMPRESSION ZONE
QHYSTE	(ENFLOW)		(H) -HYSTERESIS HEAT FLOW IN EXPANSION ZONE
OKOLFR	()	HTFLOH	-HEAT FLOH DUE TO COOLER FRICTION (N)
QLEAK	(ENFLOW)	LOSSES	-HEAT FLOW DUE TO GAS LEAKAGE (H)
OPISHL	(ENFLCH)	LOSSES	-HEAT FLOH ALONG PISTON HALL (H)
GREGER	(ENFLOW)	HTFLCH	-TOTAL REGENERATOR REHEAT LOSS (W)
QREGFL	(ENFLOH)	LOSSES	-CONDUCTION HEAT FLOW THRU FILLER MATERIAL (H)
QREGFR	()	HTFLOW	-HEAT FLOW DUE TO REGENERATOR FRICTION (W)
QREGHL	(ENFLOW)	LOSSES	-CONDUCTION HEAT FLOH ALONG THE REGENERATOR HALL (H)
QSTATC	(ENFLOH)	LOSSES	-SUM OF ALL CONDUCTION HEAT FLOHS (H) QPISHL+QCYLHL+QREGHL+QREGFL
RUIA	( RIUSF)	RIUSIN	-REGENERATOR INNER HALL DIAMETER [M]
REGHT	(FLIGEN)	INPUT	-CONDUCTION HEIGHT FROM THE TOP OF THE REGENERATOR TO THE TOP OF THE EXPANSION CYLINDER (M)
REYC	( PDROP)	HTFLOW	-REYNOLDS NUMBER BASED ON DH AND XMDOT- FOR THE COOLER
REYH	( PDROP)	HTFLOW	-REYNOLDS NUMBER BASED ON DH AND XMDOT- FOR THE HEATER
REYR	( PDROP)	HTFLON	-REYNOLDS NUMBER BASED ON DH AND XMDOT- FCR THE REGENERATOR
RGAS	(GASPRP)	INITAL RIOSIN	-REFERENCE GAS CONSTANT (J/KG-K)
RGL	( RIOSF)	RIUSIN Losses	-TOTAL LENGTH OF REGENERATOR (M)
RINGCI.	( FADD)	INPUT	-GAP BETHEEN RING AND WALL (M)
RINGFR	( FADD)	INPUT	-RING FRICTION COEFFICIENT
RINGHT	( FADD)	INPUT	-RING HEIGHT (M)
RINGLK	( FADD)	INPUT	-RING LEAK COEFFICIENT (KG/PA-SEC)
RP	()	HTFLOW	-PRESSURE RATIO PMAX/PMIN
RVT	( RIOSF)	CYCLER	-DISPLACED MASS RATIO COLD (VOL/TEMP) * HOT (TEMP/VOL)
SCALR	( OUTPT)	RIOSPR	-ARRAY CONTAINING 50 VARIABLES FOR OUTPUT A FULL LIST OF THIS CONTAINER ARRAY IS GIVEN IN ROUTINES OUT1 AND RIOSPR
SCHDEL	(VARVOL)	INITAL	-SCHMIDT ANALYSIS CONSTANT, RELATES PRESSURE RATIO, SCHDEL = SCHAA/SCHBB
SIGHA	(FLCELL)	INPUT	-RATIO OF MINIMUM FLOW AREA TO FRONTAL AREA IN A CELL. SIGMA<=POROS
SLNGTH	( FADD)	INPUT INITAL	-LENGTH USED FOR SHUTTLE HEAT FLOW (M)
STARTD	(FLTGEN)	INPUT	-CRANK ANGLE AT TIME=0.0 (DEGREE)
STAFTR	(VARVOL)	INITAL	-SAME AS STARTD (RAD)
STC	()	HTFLOW	-COOLER TUBE AVERAGE STANTON NUMBER
SUHOC	( RIOSF)	RIOSIN	-SUM OF THE ABS(DC). (CU M/SEC)

•

VARIABLE	COMMON BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
TCMBST	(FLTGEN)	INPUT INPORV	-EXTERNAL HEATER TEMPERATURE (K)
TEST	()	CYCLER	-NET CHANGE IN EXPANSION SPACE DIMENSIONLESS MASS OVER THE CYCLE
TEST1	()	CYCLER	-NET CHANGE IN DIMENSIONLESS ENGINE PRESSURE OVER THE CYCLE
TGAS	(FLCELL)	INPUT	-GAS TEMPERATURE IN A CELL (K)
TGASAD	(DYHPRP)	INITAL	-CURRECHT GAS TEMPERATURE IN A ADDED VOLUME (K)
TGASD	(DYNPRP)	INITAL HTFLOW	-CURRENT GAS TEMPERATURE IN A CELL (K)
TGASO	(DYNPRP)	INITAL CONVRG	-LAST VALUE OF TGASD (K) USED FOR CONVERGENCE
THETA	(VARVOL)	INITAL	-SCHMIDT ANALYSIS PRESSURE VOLUME PHASE ANGLE (RAD)
TIME	( AMISC)	INITAL	-CURRENT TIME (SEC)
THASS	(FLTGEN)	INPUT INITAL	-INITIAL TOTAL MASS OF GAS IN ENGINE (KG)
THASSD	(DYNPRP)	RIOSIN HTFLOW	-CURRENT MASS OF GAS IN ENGINE (KG)
THAXC	( PDROP)	CYCLER	-MAXIMUM GAS TEMPERATURE DURING CYCLE IN COMPRESSION ZONE (K)
THAXE	( PDROP)	CYCLER	-MAXIMUM GAS TEMPERATURE DURING CYCLE IN EXPANSION ZONE (K)
THINC	( PDROP)	CYCLER	-MINIMUM GAS TEMPERATURE DURING CYCLE IN COMPRESSION ZONE (K)
THINE	( PDROP)	CYCLER	-HININUM GAS TEMPERATURE DURING CYCLE IN Expansion Zone (K)
TORQC	(ENFLOW)	RIOSIN Analis	-TORQUE IN COMPRESSION ZONE
TORQE	(ENFLOW)	RIOSIN Analis	-TORQUE IN EXPANSION ZONE
TREGND	(DYNPRP)	INITAL	-CURRENT REGENERATOR HALL TEMPERATURE (K)
TREGWO	(DYNPRP)	CONVRG INITAL	-LAST REGENERATOR WALL TEMPERATURE (K) USED IN CONVERGENCE SCHEME
TRSHLD	(DYNPRP)		-CURRENT VALUE OF RADIATION SHIELD TEMPERATURE (K)
TRTO	( RIOSF)	HTFLOH RIOSIN CYCLER	-CURRENT GAS TEMPERATURE RATIO THOT/TCOOL
THALL	(FLCELL)	INPUT	-HALL TEMPERATURE OF CELL (K)
THALLO	(DYNPRP)	INITAL HTFLOH	-CURRENT WALL TEMPERATURE OF CELL (K)
THATER	(FLTGEN)	INPUT INITAL	-COOLING WATER AVERAGE TEMPERATURE (K)
THENVR	(FLTGEN)	INPUT INITAL	-AVERAGE ENVIRONMENT TEMPERATURE (K) Initalized to 300. K
THLHI	()	INPORV	-PERTURBATION DEPENDENT TOMBST (K)/
THO	( AMISC)	INPUT	-2.00
VAC	( RIOSF)	RIOSIN	-HALF THE MAXIMUM COMPRESSION DISPLACEMENT (CU M)

VARIABLE	CONTINN BLOCK	CALC. IN ROUTINE	DEFINITION/UNITS
VAE	( RIOSF)	RIOSIN	-HALF THE MAXIMUM EXPANSION DISPLACEMENT (CU M)
VCD VD	( RIOSF) ( RIOSF)	RIOSIN RIOSIN	-TOTAL COOLER RELATED DEAD VOLUME (CU M) -TOTAL ENGINE RELATED DIMENSIONLESS DEAD
VECTR	( OUTPT)	RIOSPR	-ARRAY CONTAINING 15 VARIABLES BY ZONE FOR OUTPUT
			1 TG MAX(K) 2 TG AVG(K) 3 TH-TG AVG(K) 4 TH-TG MAX(K) 5 Q NET (H) 6 M FLUX(KG/S) 7 M FLUX MAX 8 REY NUMBR 9 D-P FRIC(MPA) 10 NUSSELT NUMBR 11-15 NOT USED
VOL VOLAD	(FLCELL) (DYNFRP)	INITAL	-CELL VOLUHE (CU M) -ADDED VOLUME CELL CURRENT TOTAL VOLUME {CU.M}
VOLS	(VARVOL)	VOLUME	-VARIABLE VOLUME ARRAY (CU M) 1-EXPANSION 2-HOT SIDE COMPRESSION 3-COLD SIDE COMPRESSION 4-HOT SIDE BUFFER 5-COLD SIDE BUFFER
VOLHL	(FLCELL)	INPUT	-WALL VOLUME BY CELL (CU M)
VRO	( RIOSF)	RIOSIN	-TOTAL REGENERATOR RELATED DEAD VOLUME (CU M)
WALLTH	(FLCELL)	INPUT	-HALL THICKNESS OF A CELL (H)
HC	( RIOSF)	CYCLER HTFLOW	-DIHENSIONLESS COMPRESSION SPACE WORK
WE	( RIOSF)	CYCLER HTFLOW	-DIMENSIONLESS EXPANSION SPACE WORK
HORKC	(ENFLOW)	ANALIS	-COMPRESSION SPACE HORK (J)
HORKE	(ENFLOW)	ANALIS	-EXPANSION SPACE WORK (J)
XLNGTH	(FLCELL)	INPUT	-CELL LENGTH (M)
XOMC	( RIOSD)	CYCLER HTFLOH	-ARRAY OF CHANGES IN DIMENSIONLESS MASS IN THE COMPRESSION SPACE
XDHE	( RIOSD)	CYCLER HTFLOH	-ARRAY OF CHANGES IN DIMENSIONLESS MASS IN THE EXPANSION SPACE
XMC	( RIOSF)	CYCLER RIOSIN HTFLON	-CURRENT DIMENSIONLESS MASS IN COMPRESSION ZONE
XHDOTC	( PDROP)	HTFLOH	-AVERAGE CYCLE MASS FLUX IN COOLER (KG/SEC)
XHDOTH	( PDROP)	HTFLOH	-AVERAGE CYCLE MASS FLUX IN HEATER (KG/SEC)
XMDOTR	( PDROP)	HTFLOW	-AVERAGE CYCLE MASS FLUX IN REGENERATOR (KG/SEC)
XME	( RIOSF)	CYCLER RIOSIN HTFLOW	-DIHENSIONLESS MASS IN EXPANSION ZONE
XNHT	( RIOSF)	RIOSIN	-AVERAGE EXPONENT IN NUSSELT CORRELATION
XNUSC	( PDROP)	HTFLOH	-NUSSELT NUMBER IN COOLER
XNUSH	( PDROP)	HTFLOH	-NUSSELT NUMBER IN HEATER
XNUSR	( PDROP)	HTFLOH	-NUSSELT NUMBER IN REGENERATOR
XPSTRT ZERO	( RIOSF) ( AMISC)	RIOSIN INPUT	-INITIAL DIMENSIONLESS PRESSURE ESTIMATE -0.0

APPENDIX D GRAF LISTING

#### SUBPROGRAM GRAF

C-GRA00010 C-SETS UP TELLAGRAF FILE FOR POHER AND POHER LOSS PLOTS GRA00020 C-VS RPM IE THESE ARE THE CASE BY CASE PLOT GRA00030 C~ GRA00040 
 IMENSION
 PMEAN(50), SPEED(50), XMASS(50), QIN(50),

 FORER(50), EFFIC(50), TROTG(50), TROLG(50),QRGKOL(50),

 QUMXKOL(50), QSTDY(50),QDYNAM(50), QFRIC(50),QREGEF(50),
 DIMENSION GRA00050 GPA00060 X X GRA00070 QLEAK(50), QOUT(50), DUM(8,50) GRA00080 DIMENSION IA(20), PROUT(5),NC10(5),NC20(5) GRA00090 C-GRA00100 C-NEED TO KNOW THAT 4 PRESSURE CASES ARE COMING IN GRA00110 C-AND THAT NRPM = NPRT2 IN SEAM IS 6 GRA00120 C-GRA00130 NPRES=4 GRA00140 NRPM=6 GRA00150 IOUT=3 GRA00160 IOUT=0 GRA00170 C-GRA00180 DO 600 NPR=1,NPRES GRA00190 C-ONE OF EACH PLOT IOUT = 0GRA00200 Ç-IOUT = 1 POWER LOSSES VS RPH IOUT = 2 HEAT LOSSES VS RPH GRA00210 C-ICUT = 3 BOTH 1 AND 2 CRA00220 IOUT = 4 POWER VS RPH AND EFFIC VS RPM C-GRA00230 C-IOUT = 5 POMER VS EFFICIENCY GRA00240 C-IOUT = 6 BOTH 4 AND 5 GRA00250 C-GRA00260 **100 CONTINUE** GRA00270 C-ERA00280 READ UNIT 5, IE TERMINAL FOR WHATEVER C-ERA00290 READ (10,2000) IA GRA00300 2000 FORMAT(2044) GRA00310 READ (10,2005) IMASS, RPM, P, TCMB, TWATER, TMASS GRAC0320 2005 FORMAT(13, F9.2, F9.4, 2F9.2, F9.6) GRA00330 C-GRA00340 GRA00350 **18 CONTINUE** C-GRA00360 DO 200 L=1,NRPH GRA00370 READ(10, 1000) NCASE, PMEAN(NCASE), SPEED(NCASE), XMASS(NCASE), GRA00380 X QIN(NCASE), POWER(NCASE), EFFIC(NCASE), THOTG(NCASE), GRA00390 X TKOLG(NCASE) GRA00400 READ(10,1001) QHGKOL(NCASE),QHMKOL(NCASE), QSTDY(NCASE), GRA00410 QDYNAM(NCASE), QFRIC(NCASE), QREGEF(NCASE), QLEAK(NCASE), X GRA00420 X QOUT(NCASE) GRA00430 GRA00440 C-1000 FORMAT(14,2F9.2,F10.6,2F10.2,F8.4,2F9.2) GRA00450 1001 FORMAT(1X,8F9.2) GRA00460 C-GRA00470 1005 FORMAT( 1H ,14,2F9.2,F10.6,2F10.2,F8.4,2F9.2) GRA00480 HRITE(6, 1005) NCASE, PHEAN(NCASE), SPEED(NCASE), XHASS(NCASE), GRA00490 QIN(NCASE), POWER(NCASE), EFFIC(NCASE), THOTG(NCASE), GRA00500 X X TKOLG(NCASE) GRA00510 C-GRA00520 DUM( 1, L)=POHER(NCASE)-QDYNAM(NCASE) GRA00530 DUM(2,L)=QIN(NCASE)+QHGKOL(NCASE) GRA00540 DUM(3,L)=-QSTDY(NCASE) GRA00550

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DUH(5,L)=DUH(4,L)-QREGEF(NCASE)
                                                                                                           GRA00570
                                                                                                           GRA00580
         DUM(6,L)=DUH(5,L)-QFRIC(NCASE)
         DUH(7,L)=THOTG(NCASE)-TKOLG(NCASE)
                                                                                                           GRA00590
         IF(L.EQ.1) NC10(NPR)=NCASE
                                                                                                           GRA00600
         IF(L.EQ.NRPM) NC20(NPR)=NCASE
                                                                                                           GRA00610
         IF(L.EQ.1) PROUT(NPR)=P
                                                                                                           GRA00620
                                                                                                           GRA00630
C-
   200 CONTINUE
                                                                                                           GRA00540
C-
                                                                                                            GRA00650
         BASIC DATA READ IN AND STORED
C--
                                                                                                           GRA00660
C-
                                                                                                           GRA00670
   300 FORMAT(' GENERATE A SIMPLE PLOT .',/' NO BORDER. ',
                                                                                                           GRA00680
   1 'HINDOH 1.0 8.0 1.0 10.0 . WINDOH FILL. ')
309 FORMAT(' TITLE HEIGHT=0.5,0.4,0.3, ''',6A4,' ''')
310 FORMAT(' ''POMER LOSSES VS SPEED''')
                                                                                                           GRA00690
                                                                                                           GRA00700
                                                                                                           GRA00710
   311 FORMATC'
                       "POHER FLOWS VS SPEED" ")
                                                                                                           GRA00720
                       TITLE HEIGHT=1.0,''',6A4,' '' .')
   312 FORMAT('
                                                                                                           GRA00730
   313 FORMAT(' ''PRESSURE=', F5.2, ' MPA'' .')
                                                                                                           GRA00740
   314 FORMAT( ' 'GAS MASS=', F6.5, ' KG''.')
                                                                                                           GRA00750
C-
                                                                                                           GRA00760
   320 FORMAT(' X AXIS LABEL '' SPEED ((RPM))'' .')
321 FORMAT(' X AXIS LABEL '' INDICATED EFFICIENCY ((%))''.')
                                                                                                           GRA00770
                                                                                                           GRA00780
   330 FORMAT(' Y AXIS LABEL ''PONER ((KH)) '', MIN=0.0 .')
                                                                                                          GRA00790
   331 FOPMAT(' Y AXIS LABEL ''PCHER LOSS ((KH)) '', MIN=0.0 .')GRAG0800332 FORMAT(' Y AXIS LABEL '' INDICATED EFFICIENCY ((%))''.')GRAG0810333 FORMAT(' Y AXIS LABEL '' INDICATED POWER ((KH))'', MIN=0.0 .')GRA00820
C-
                                                                                                           GRA00230
   340 FORMAT(' CURVE 1 SHADE BELOW . ')
341 FORMAT(' Y AXIS TRANSFORM 0. 1000000. 0. 1000. ')
342 FORMAT(' Y AXIS TRANSFORM 0. 1. 0. 100. ')
343 FORMAT(' X AXIS TRANSFORM 0. 1. 0. 100. ')
                                                                                                            GRA00540
                                                                                                            GRA00350
                                                                                                            GRA00860
                                                                                                            GRA00870
   350 FORMAT(' EVERY MESSAGE SIMPLEX, COORDINATE UNITS,X=',F8.2,'.')
                                                                                                            GRA00880
C-
                                                                                                            GRA00390
   360 FORMAT(' MESSAGE 1 ''POHER OUT'', Y=',F8.2,'.')
361 FORMAT(' MESSAGE 2 ''DYNAMIC LOSSES'', Y=',F8.2,'.')
362 FORMAT(' MESSAGE 3 ''OTHER LOSSES '', Y=',F8.2,'.')
363 FORMAT(' MESSAGE 4 ''COOLER HEAT OUT '', Y=',F8.2,'.')
364 FORMAT(' MESSAGE 5 ''TOTAL HEAT IN '', Y=',F8.2,'.')
365 FORMAT(' MESSAGE 1 ''CONDUCTION LOSS '',Y=',F8.2,'.')
366 FORMAT(' MESSAGE=1 ''CONDUCTION LOSS '',Y=',F8.2,'.')
                                                                                                            GRA00900
                                                                                                            GRA00910
                                                                                                            GRA00920
                                                                                                            GRA00930
                                                                                                           GRA00940
                                                                                                           GRA00950
   366 FORHAT(' MESSAGE=3 ''REGENERATOR LOSS '',Y=',F8.2,'.')
367 FORHAT(' MESSAGE=4 ''FRICTION LOSS '' ,Y=',F8.2,'.')
                                                                                                           GRA00950
                                                                                                            GRA00970
   370 FORMAT(' EVERY CURVE SYMBOL COUNT 0, SPLINE . ')
371 FORMAT(' EVERY CURVE SYMBOL COUNT 0, PARA3 .')
                                                                                                            GRA00980
                                                                                                            GRA00990
   372 FORHAT( ' CURVE 5 SCATTERED, SYMBOL TYPE RING .')
                                                                                                            GRA01000
C-
                                                                                                            GRA01010
   380 FORMAT( ' NO LEGEND . ')
                                                                                                            GRA01020
   381 FORMAT( ' LEGEND STYLE SIMPLEX, ', 1X,
                                                                                                            GRA01030
       A ' TEXT ''CALCULATED:''.')
                                                                                                            GRA01040
   394 FORMAT( ' PAGE LAYOUT IS LRV. ')
                                                                                                            GRA01050
   400 FORHAT( ' INPUT DATA. ')
                                                                                                            GRA01060
   410 FORHAT(' ''CURVE',12,'''.',6(/1X,3(F10.4,F9.1,3X)) )
420 FORHAT(' END OF DATA. ')
                                                                                                            GRA01070
                                                                                                            GRA01080
   422 FORMAT( ' SUBPLOT ', 12, '. ')
                                                                                                            GRA01090
   423 FORMAT( ' SEND ', 12, '.')
                                                                                                            GRA01100
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SUBPROGRAM GRAF
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DUM(4,L)=DUM(3,L)-QDYNAM(NCASE)

GRA00560
SUBPROGRAM GRAF

424	FORMAT(' ROTATION=MOVIE. ')	GRA01110
C~		GRA01120
	MLST=NRPM	GRA01130
	NST=NC10(NPR)	GRA01140
	IF(QIN(NCASE).LT.QIN(NST)) NCASE=NST	GRAU1150
~	IFUNCASE.EQ.NSTJ NLST=1	62AU 1160 CDA01170
L-	TC//TD-0	CRAUTIZU CRA01100
	LUKIE-U Tekodynam(noace) IT û ûîrotn(noace)) tekte-1	CRA01100
	TE(CONVAMINICAGE) IT & REVENUE NEASED) TORIF-1 TE(CONVAMINICAGE) IT & REVENUE NEASED) TORIF-1	GRADITES GRADITED
r-	In the manifulation of the measure in the second state of the second sec	GRA01200
U I	TELTOUT GT 33 50 TO 600	GRA01220
	IF(IDUT.EQ.0 .400. NER.LT.0) GO TO 600	GRA01230
C-		GRA01240
	ERITE(11,394)	ERA01250
	NC9=NC10(NFR)+1	GRA01260
	IF(ICUT.EQ.2) GO TO 500	ERA0 1270
C-		GRA01280
C-	IOUT = 0, 1, 3	GRA0 1290
C-	GRAPHICS FOR POWER LOSSES VS RPM FOR A MEAN PRESSURE	GRA01300
C-		GRA01310
	WRITE(11,300)	ERA01320
	ERITE(11,309) (IA(I),I=1,6)	ERAU1330
	KRLIE(11,311) XE(XMOD 50 0) UDITE(11 747) D	UXAU1340
	IF(IMASS.EQ.U) RKITE(II,SIS) P IE(IMACC ED 1) UDITE(11 316) THACD	CRAU 1330
	IF(16A55.EQ.1) KALIE(11,514) (MA55 Upits(11 320)	GRAU 1330 GDA0 1370
	UDTTE(11.330)	07401370
	LOTTE(11,348)	60401300
	DUU1=SPEED(NEST)	CRA01600
	WRITE(11.350) DUN1	GRAC 14 10
	DUN1=0.001*POHER(NCASE)*0.5	6PA01420
	WRITE(11,360) DUM1	GRA01430
	DUM1=0.001*0.5*(POWER(NCASE)+DUM(1,NLST))	GRA01440
	IF(ISKIP.EQ.0) KRITE(11,361) DUM1	GRA01450
	DUM1=0.001*(DUM(2,NLST)*0.8+0.2*DUH(1,NLST))	GRA01460
	WRITE(11,362) DUH1	GRA01470
	DUM1=0.001*0.5*(DUM(2,NLST)+QIN(NCASE))	GRA01480
	WRITE(11,363) DUM1	GRA0 1490
CC	DUI11=SPEED(NCASE)=0.5	GRAU1500
LC	HRITELTIJOHJ VININGAGEJ	GRAU 12 10
	UDTTE (11 TEG) DINI	GRAU 1020
	MALIELII,3047 DUNI Lotte(11 341)	GRAU 1530
	URTTE(11,37)	GRA01550
	WRITE(11,380)	GRA01560
	KRITE(11,400)	GRA01570
	II=1	GRA01580
	HRITE(11,410) II,(SPEED(L+NC9),POWER(L+NC9),L=1,NLST)	GRA01590
	IF(ISKIP.GT.0) 60 TO 480	GRA01600
	II=II+1	GRA01610
	<pre>kRITE(11,410) II,(SPEED(L+NC9),DUH(1,L),L=1,NLST)</pre>	GRA01620
480	II=II+1	GRA01630
	HRITE(11,410) II,(SPEED(L+NC9),DUM(2,L),L=1,NLST)	GRAD164D
	II=II+1	GRA01650

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SUBPROGRAM GRAF
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	UDTTE(11, 610) TT (CREED(LANCO) OTN(LANCO) Lat NUCT)	CDA01660
		ORAU 1000
	WRITE(11,420)	GRAU 1570
	II=2*NPR-1	GRA01600
	WRITE(11,422) II	GRA01690
	TE(TOUT, EQ. 1) GO TO 600	GRA01700
<b>C</b> -		GPA01710
500		CDA01770
200		6RAU1720
C-	1001=0, 2, 3	GRAU 1730
C-	GRAPHICS FOR HEAT LOSSES VS RPM FOR A MEAN PRESSURE	GRA01740
C-		GRA01750
	HRITE(11,300)	GRA01760
	$h_{RTTE(11, 309)}$ (TA(T), T=1.6)	68A01770
		69401720
	$\mathbf{x}_{(1)} = \mathbf{x}_{(1)} = x$	CR401700
	1F(17,ASS,EQ,U) ERTTE(11,S1S) P	GRAU1790
	IF(IMASS.EQ.1) WRITE(11,314) TMASS	GRA018CO
	KRITE(11,320)	GRA01310
	KRITE(11,331)	GRA01820
	WRITE(11.340)	69401830
		69101340
		CRA01070
		GRAU 1850
	DUN1=0.001+BUM(3,NLSTJ#0.5	GRA01380
	KRITE(11,365) DUM1	GRA01870
	DUH1=0.001×0.5×(DUH(3,NLST)+DUH(4,NLST))	GRA01830
	TE(TSKIP, LE. 1) NUTTE(11.361) DUM1	68401890
	01141=0 001+0 5+(0114(5.NIST)+0144(6.NIST))	69401900
		CDA01010
		CRAU 1910
	DUN1=0,001+0,0×(DUN10,NES1)+DUN10,NES1))	GRAU 1920
	HRITE(11,367) DUA1	ERA01930
	KRITE(11,341)	CRA01940
	NRITE(11,370)	GRA01950
	HRITE(11,330)	67401960
		67/01070
	FINELEL	CDA01090
	$11 \circ 1$	08201920
	RRITE(: 1,440) II,(SPEED(L+AC9),DUA(3,2),L=1,ACS1)	GRAU 1990
	IF(ISKIP.GT.1) GO TO 485	GRA02000
	II=II+1	GRA02010
	WRITE(11,410) II,(SPEED(L+NC9),DUM(4,L),L=1,NLST)	GRA02020
485	TT=TT+1	GRA02030
100	$D_{1}$	CRA02060
	MATLE (1) (0) 11, (3) EED(E*MC/))DO((3)E))E=()ME3()	CRACEOTO
		GRAUZUOU
	RRI[E(1],410) II,(SPEED(L+NC9),DUM(6,L),L=1,NLST)	GRA02060
	WRITE(11,420)	GRA02070
	II=2*NPR	GRA02080
	WRITE(11.422) II	GRA02090
C-		60402100
- 600	CONTINUE	CDA02110
- 000	CONTINUE	CR402110
<u> </u>		GRAUZ IZU
C-	ALL DATA NOW IN POWER, PMEAN, SPEED, AND EFFIC TO DO OTHER PLOTS	GRA02130
C-		GRA02140
	IF(IOUT.GT.0.AND. IOUT.LT.4) GO TO 750	GRA02150
C-		GRA02160
-	WRTTE(11,394)	60102170
	TELTONT ED EL CO TO 700	CD 102190
~	1007-0 4 4	UKAU2 160
C-	1001=0, 4, 6	GRAUZ 190
C-	GRAPHICS FOR POHER VS RPM FOR ALL MEAN PRESSURES	GRA02200

SUBPROGRAM GRAF

C-	AND EFFICIENCY VS RPM FOR ALL MEAN PRESSURES	GRA02210
C-		GRA02220
	HRITE(11,300)	GRA02230
	<pre>kRITE(11,312) (IA(I),I=1,6)</pre>	GRA02240
	WRITE(11,333)	GRA02250
	WRITE(11.341)	GRA02260
	WRITE(11.329)	GRA02270
	WPTTE(11,371)	67402280
	ROTTE(11, 381)	62402290
	UDITE(11.400)	69402300
	DO 450 NED-1 NEDEC	60402300
	NC1-NC10(NDD)	60402370
		60X02320
		CRAU2330
	F-FR/JUILINFR/	00402340
	HRAIE(11)16(3) T	GRAU2330
150	KALLELIN, IZITI (SPEEDILI) POWER(LI) L=NUT, NUZ)	GKAUZ3OU
650	CONTINUE	ERAUZ5/U
	KRITE(11, 1214)	GRA02380
	KRITE(11,420)	GRA02390
	WRITE(11,372)	GRA02400
	11=25	GRA02410
	KRITE(11,422) II	GRA02420
C-		GRA02430
	HRITE(11,394)	GRA02440
	WRITE(11,300)	CRA02450
	HRITE(11,312) (IA(1),I=1,6)	GRA02460
	WRITE(11,332)	GRA02470
	HRITE(11,342)	GRA02480
	KRITE(11,320)	GRA02490
	KRITE(11,371)	GRA02500
	WRITE(11.381)	GRA02510
	W9TTF(11.400)	GRA00520
	NO 675 NPR=1.NPRES	67462530
	N° 1=N° 10( NPR )	GPA02540
	NC2=NC20(N92)	GRA02550
	P-PDOIT(NEP)	60402560
	LIDITE(11 1918) D	GDA02570
	NGLIC(1) (C)U) F UDTTE(11 1919) (CDEED(L) EKETC(L) L+NP1 NP2)	60402589
475		GDA02500
615	LIDTTE(11 1216)	CDA02570
	NKIE(1)(217)	CDA02600
	MK11C(11)420J	CDA02670
	WATIELIIJJ/2J	CD402670
	11-20	CRAUZOJU CRAUZOJU
~	WRITE(11)422) 11	000402040
L-		6RAU263U
-	15(1001.54.4) 60 10 /20	GRAUZOOU
<u>u</u> -		GRAU26/U
U-	1001 = 0, 0, 0,	GRAUZ680
c-	GRAPHICS FOR POHER VS EFFICIENCY FOR ALL MEAN PRESSURES	GRAU2690
C~		6RA02700
700	CONTINUE	GRA02710
	HRITE(11,394)	GRA02720
	HRITE(11,300)	GRA02730
	HRITE(11,312) (IA(I),I=1,6)	GRA02740
	WRITE(11,333)	GRA02750

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HRITE(11,321)
      WRITE(11,371)
      WRITE(11,341)
      KRITE(11,343)
KRITE(11,381)
      HRITE(11,400)
      DO 725 NPR=1,NPRES
      NC1=NC10(NPR)
      NC2=hc20(NPR)
      P=PRCUT(NPR)
      I'RITE(11,1210) P
      WRITE(11,1213) (EFFIC(L), POWER(L), L=NC1, NC2)
  725 CONTINUE
      KRITE(11,1214)
      KRITE(11,420)
      KRITE(11,372)
      II=27
      WRITE(11,422) II
C-
 1210 FORMAT(' '' P =',F5.2,' (MPA)'' ')
 1211 FORHAT(1H ,3(3X,F10.4,F10.0) )
 1212 FORMAT( 1H ,3(3X,F10.4,F10.5) )
 1213 FORMAT(1H ,3(3X,F8.5,F10.0) )
1214 FORMAT(' '' EXPR. DATA ''.')
C-
  750 CONTINUE
C-
      HRITE(11,424)
      IF(IOUT.GT.3) GO TO 820
      DO 800 NPR=1,NPRES
      IF(IOUT.EQ.0.AND.NPR.LT.0) GO TO 800
      IF(IOUT.EQ.2) GO TO 790
      II=NFR+2-1
      KRITE(11,423) II
      IF(IOUT.EQ.1) GO TO 800
  790 II=NPR*2
      KRITE(11,423) II
  800 CONTINUE
C-
  820 IF(IOUT.LT.4.AND.IOUT.GT.0) GO TO 850
      IF(IOUT.EQ.5) GO TO 840
      II=25
      WRITE(11,423) II
      II=26
      WRITE(11,423) II
       IF(10UT.EQ.4) 60 TO 850
  840 II=27
      HRITE(11,423) II
  850 CONTINUE
C-
      RETURN
       EHD
```

GRA02760 GRA02770 GRA02780 GRA02790 GRA02800 GRA02810 GRA02820 GRA02830 GRA02840 GRA02850 GRA02860 GRA02870 GRA02880 GRA02890 GRA02900 GRA02910 ERA02920 GRA02930 GRA02940 GRA02950 GRA02960 GRA02970 GRA02930 GRA02390 GRA03000 GRA03010 GRA03020 GRA03030 GRA03040 GRA03050 GRA03060 GRA03070 GRA03080 GRA03090 GRA03100 GRA03110 GRA03120 GRA03130 GRA03140 GRA03150 GRA03160 GRA03170 GRA03180 GRA03190 GRA03200 GRA03210 GRA03220 GRA03230 GRA03240 GRA03250 GRA03260 6RA03270

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SUBPROGRAM GRAF
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# APPENDIX E GRAF OUTPUT/TELLAGRAF INPUT

GRAF OUTPUT / TELLAGRAF INPUT

PAGE LAYOUT IS LRV. GENERATE A SIMPLE PLOT . NO BORDER. WINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' PL!!ER FLOWS VS SPEED! 'FRESSURE= 2.74 MPA' X AXIS LABEL ' SPEED ((RPH))' . Y AXIS LABEL 'PCHER ((KW)) ', MIN=0.0 . CURVE 1 SHADE BELOH EVERY MESSAGE SIMPLEX, COCRDINATE UNITS, X= 3499.20. MESSAGE 1 'PO'IER OUT', Y= 0.73. MESSAGE 3 'OTHER LOSSES ', Y= 2.53. MESSAGE 4 'COOLER HEAT OUT ', Y= 6.04. MESSAGE 5 'TOTAL HEAT IN ', Y= 9.37. Y AXIS TRANSFORM 0. 1000000. 0. 1000. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INPUT DATA. 'CURVE 1'. 1000.2000 1095.1 1500.0000 1494.1 1999.8000 1929.3 2499.6001 2105.2 2999.3999 1907.8 3499.2000 1453.6 'CURVE 2'. 1000.2000 2627.8 1999.8000 3119.2 2182.6 1500.0000 2499.6001 3331.1 2999.3999 3149.6 3499.2000 2708.0 'CURVE 3'. 1000.2000 3781.6 1500.0000 5065.8 1999.8000 6431.2 2999.3999 8573.6 3499.2000 2499.6001 7629.1 9370.0 END OF DATA. SUBPLOT 1. GENERATE A SIMPLE PLOT . NO BORDER. WINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' 'POHER LOSSES VS SPEED' 'PRESSURE= 2.74 MPA' X AXIS LABEL ' SPEED ((RPM))' . Y AXIS LABEL 'POWER LOSS ((KW)) ', MIN=0.0 . CURVE 1 SHADE BELOH . EVERY NESSAGE SIMPLEX, COORDINATE UNITS,X= 3499.20. MESSAGE=1 'CONDUCTION LUSS ',Y= 0.51. MESSAGE=3 'REGENERATOR LOSS ',Y= MESSAGE=4 'FRICTION LOSS ',Y= 1.60. 3.48. Y AXIS TRANSFORM 0. 1000000. 0. 1000. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INFUT DATA. CURVE 1'. 1000.2000 908.0 1500.0000 935.0 1999.8000 970.0 1003.0 992.0 1012.0 2499.6001 2999.3999 3499.2000 'CURVE 2'. 1999.8000 1000.2000 1287.0 1394.0 1532.0 1500.0000 2499.6001 1648.0 2999.3999 1731.0 3499.2000 1812.0 'CURVE 3'. 1000.2000 1483.0 1500.0000 1869.0 1999.8000 2439.0 3169.0 2999.3999 4054.0 3499.2000 5146.0 2499.6001 END OF DATA.

SUBPLOT 2. PAGE LAYOUT IS LRV. GENERATE A SIMPLE PLOT . NO BORDER. WINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' 'POHER FLOWS VS SPEED' 'PRESSURE= 4.10 MPA'. X AXIS LABEL ' SPEED ((RPM))'. Y AXIS LABEL 'POWER ((KH)) ', MIN=0.0 . CURVE 1 SHADE BELOW . EVERY MESSAGE SIMPLEX, COORDINATE UNITS, X= 3499.20. NESSAGE 1 'POWER OUT', Y= 1.47. MESSAGE 3 'OTHER LOSSES ', Y= 4.05. MESSAGE 4 'COOLER HEAT OUT', Y= 9.0 9.01. MESSAGE 5 'TOTAL HEAT IN ', Y= 13.79. Y AXIS TRANSFORM 0. 1000000. 0. 1000. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INPUT DATA. 'CURVE 1'. 1000.2000 1828.0 1500.0000 2815.4 1999.8000 3359.6 2499.6001 3544.2 2999.3999 3613.9 3499.2000 2930.1 'CURVE 2'. 3007.6 1000.2000 4629.5 1500.0000 4064.6 1999.8000 2499.6001 4822.2 2999.3999 4704.1 3499.2000 4230.8 TERVE 31. 5308.6 1000.2000 1500.0000 7521.6 1999.8000 9401.5 2499.6001 11050.2 2999.3999 12524.1 3499.2000 13789.8 END OF DATA. SUBPLOT 3. GENERATE A SIMPLE PLOT . NO EORDER. WINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' 'POHER LOSSES VS SPEED' 'FRESSURE= 4.10 MPA' X AXIS LABEL ' SPEED ((RPM))' . Y AXIS LABEL 'PCHER LOSS ((KH)) ', MIN=0.0 . CURVE 1 SHADE BELOW . EVERY MESSAGE SIMPLEX, COORDINATE UNITS,X= 3499.20. MESSAGE=1 'CONDUCTION LOSS ',Y=
MESSAGE=3 'REGENERATOR LOSS ',Y= 0.52. 1.80. MESSAGE=4 'FRICTION LOSS ',Y= 4.12. Y AXIS TRANSFORM 0. 1000000. 0. 1000. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INPUT DATA. 'CURVE 1'. 1000.2000 974.0 1500.0000 1014.0 1999.8000 1028.0 2499.6001 1034.0 2999.3999 1042.0 3499.2000 1047.0 'CURVE 2'. 1000.2000 1459.0 1500.0000 1657.0 1999.8000 1799.0 1921.0 2999.3999 2499.6001 2045.0 3499.2000 2160.0 'CURVE 3'. 1000.2000 1671.0 1500.0000 2189.0 1999.8000 2836.0 2499.6001 3674.0 2999.3999 4750.0 3499.2000 6072.0

END OF DATA. SUBPLOT 4. PAGE LAYOUT IS LRV. GENERATE A SIMPLE PLOT . NO BORDER. HINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' 'POWER FLOWS VS SPEED' 'PRESSURE= 5.55 MPA' X AXIS LABEL ' SPEED ((RPM))' . Y AXIS LABEL 'PONER ((KH)) ', MIN=0.0 CURVE 1 SHADE BELOH . EVERY MESSAGE SIMPLEX, CCORDINATE UNITS, X= 3499.20. MESSAGE 1 'POWER OUT', Y= 1.93. MESSAGE 3 'OTHER LOSSES ' , Y= 4.93. MESSAGE 4 'CODLER HEAT OUT ', Y= 11.51. MESSAGE 5 'TOTAL HEAT IN ', Y= 17.92. Y AXIS TRANSFORM 0. 1000000. 0. 1000. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INFUT DATA. 'CURVE 1'. 2724.2 1000.2000 1500.0000 3803.5 1999.8000 4429.1 2499.6001 4662.8 2999.3999 4479.6 3499.2000 3854.2 'CURVE 2'. 1000.2000 3921.3 1500.0000 5025.2 1999.8000 5657.9 2999.3999 3499.2000 5104.4 5897.7 5723.6 2499.6001 'CURVE 3'. 1000.2000 6951.3 1500.0000 9680.2 1999.8000 12105.9 2499.6001 14296.7 2999.3999 16244.6 3499.2000 17921.4 END OF DATA. SUBPLOT 5. GENERATE A SIMPLE PLOT . NO BORDER. WINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' POHER LOSSES VS SPEED 'PRESSURE= 5.55 MPA' X AXIS LABEL ' SPEED ((RPM))' . Y AXIS LABEL 'POHER LOSS ((KH)) ', MIN=0.0 CURVE 1 SHADE BELOW . EVERY MESSAGE SIMPLEX, COORDINATE UNITS, X= 3499.20. MESSAGE=1 'CONDUCTION LOSS ',Y= MESSAGE=3 'REGENERATOR LOSS ',Y= 0.50. 1.90. MESSAGE=4 'FRICTION LOSS ' ,Y= 4.63. Y AXIS TRANSFORM 0. 1000000. 0. 1000. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INPUT DATA. CURVE 1' 1000.2000 977.0 1500.0000 991.0 1999.8000 995.0 2499.6001 996.0 2999.3999 999.0 3499.2000 999.0 'CURVE 2'. 1000.2000 1582.0 1500.0000 1775.0 1999.8000 1946.0 2999.3999 2499.6001 2110.0 2267.0 3499.2000 2407.0 'CURVE 3'. 1810.0 1500.0000 2359.0 1999.8000 3101.0 1000.2000

2999.3999 5329.0 3499.2000 6855.0 2499.6001 4082.0 END OF DATA. SUBPLOT 6. PAGE LAYOUT IS LRV. GENERATE A SIMPLE PLOT . NO BORDER. WINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' POHER FLOWS VS SPEED 'FRESSURE= 6.92 MPA' X AXIS LABEL ' SPEED ((RPM))' . Y AXIS LABEL 'POHER ((KH)) ', MIN=0.0 CURVE 1 SHADE BELOW . EVERY MESSAGE SIMPLEX, COORDINATE UNITS, X= 3499.20. HESSAGE 1 'POHER OUT', Y= 2.31. HESSAGE 3 'OTHER LOSSES ', Y= 5.70. HESSAGE 4 'COOLER HEAT OUT', Y= 13.8 MESSAGE 5 'TOTAL HEAT IN', Y= 21.80. Y AXIS TRANSFORM 0. 1000000. 0. 1000. 13.84. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INPUT DATA. CURVE 1'. 1000.2000 3516.6 1500.0000 4686.2 1999.8000 5424.9 5290.7 5664.3 2999.3999 2499.6001 3499.2000 4627.6 'CURVE 2'. 4744.9 5913.6 1999.8000 1000.2000 6656.9 1500.0000 2499.6001 6899.7 2999.3999 6509.2 3499.2000 5872.2 'CURVE 3'. 1000.2000 8490.9 1500.0000 11731.6 1999.8000 14713.9 2499.6001 17387.7 2999.3999 19642.2 3499.2000 21799.2 END OF DATA. SUBPLOT 7. GENERATE A SIMPLE PLOT . NO BORDER. HINDOW 1.0 8.0 1.0 10.0 . HINDOW FILL. TITLE HEIGHT=0.5,0.4,0.3, ' GPU-3 HELIUM 927K/339K ' "POHER LOSSES VS SPEED" 'PRESSURE= 6.92 MPA' X AXIS LABEL ' SPEED ((RPM))' . Y AXIS LABEL 'POHER LOSS ((KN)) ', MIN=0.0 . CURVE 1 SHADE BELOW . EVERY MESSAGE SIMPLEX, COORDINATE UNITS, X= 3499.20. MESSAGE=1 'CONDUCTION LOSS ',Y= 0.49. HESSAGE=3 'REGENERATOR LOSS ',Y= 2.04. MESSAGE=4 'FRICTION LOSS ',Y= 5.15. Y AXIS TRANSFORM 0. 1000000. 0. 1000. EVERY CURVE SYMBOL COUNT 0, SPLINE . NO LEGEND . INPUT DATA. CURVE 1'. 1000.2000 997.0 1500.0000 995.0 1999.8000 996.0 2499.6001 993.0 2999.3999 973.0 3499.2000 987.0 'CURVE 2'. 1722.0 1000.2000 1500.0000 1932.0 1999.8000 2149.0 2499.6001 2348.0 2999.3999 2501.0 3499.2000 2692.0 'CURVE 3'.

1000.2000 1967.0 2566.0 1999.8000 3412.0 1500.0000 2499.6001 4516.0 2999.3999 5876.0 3499.2000 7607.0 END OF DATA. SUBPLOT 8. PAGE LAYOUT IS LRV. GENERATE A SIMPLE PLOT . NO EORDER. HINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=1.0, ' GPU-3 HELIUM 927K/339K ' Y AXIS LABEL ' INDICATED POWER ((KW))', MIN=0.0 . Y AXIS TRANSFORM 0. 1000000. 0. 1000. X AXIS LABEL ' SPEED ((RPM))' EVERY CURVE SYMBOL COUNT 0, PARA3 TEXT 'CALCULATED:' . LEGEND STYLE SIMPLEX, INPUT DATA. P = 2.74 (MPA)' 1000.2000 1095. 1500.0000 1494. 1999.8000 1929. 2105. 2499.6001 2999.3999 1908. 3499.2000 1454. ' P = 4.10 (MPA)' 1000.2000 1828. 1500.0000 2815. 1999.8000 3360. 2499.6001 2999.3999 3414. 3499.2000 2930. 3544. ' P = 5.55 (MPA)' 1000.2000 2724. 1500.0000 3804. 1999.8000 4429. 2499.6001 3854. 4663. 2999.3999 4480. 3499.2000 ' P = 6.92 (MPA)' 1000.2000 3517. 1999.8000 5425. 1500.0000 4686. 2499.6001 5664. 2999.3999 5291. 3499.2000 4628. ' EXPR. DATA ' 'EXPR DATA' 1500. 1670. 2500. 2080. 3000. 2060. 3500. 1680. 1000. 1160. 1500. 2410. 2500. 3300. 3000. 3430. 3500. 2980. 3000. 4640. 3500. 4380. 2500. 4490. 3000. 5480. 3500. 5190. END OF DATA. CURVE 5 SCATTERED, SYMBOL TYPE RING . SUBPLOT 25. PAGE LAYOUT IS LRV. GENERATE A SIMPLE PLOT . NO BORDER. HINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=1.0, ' GPU-3 HELIUM 927K/339K ' . Y AXIS LABEL ' INDICATED EFFICIENCY ((%))'. Y AXIS TRANSFORM 0. 1. 0, 100. X AXIS LABEL ' SPEED ((RPM))' EVERY CURVE SYMBOL COUNT 0, PARA3 LEGEND SIYLE SIMPLEX, TEXT 'CALCULATED: ' . INPUT DATA. P = 2.74 (MPA) 1000.2000 0.28960 1500.0000 0.29490 1999.8000 0.30000 2499.6001 0.27590 0.22250 0.15510 2999.3999 3499.2000 ' P = 4.10 (MPA)' 1000.2000 0.34430 1500.0000 0.37430 1999.8000 0.35730 0.32070 2999.3999 0.27260 3499.2000 2499.6001 0.21250 ' P = 5.55 (MPA)' 1000.2000 0.39190 1500.0000 0.39290 1999.8000 0.36590 2499.6001 0.32610 3499.2000 2999.3999 0.27580 0.21510 ' P = 6.92 (MPA)'

1000.2000 0.41420 1500.0000 0.39950 1999.8000 0.36870 0.32580 0.26940 2499.6001 2999.3999 0.21230 3499.2000 ' EXPR. DATA ' 1000. 0.32 1500. 0.31 2500. 0.267 3000. 0.231 3500. 0.169 1500. 0.333 2500. 0.293 3500. 0.207 3000. 0.264 2500. 0.305 3500. 0.220 3000. 0.271 3000. 0.265 3500. 0.22 END OF DATA. CURVE 5 SCATTERED, SYMBOL TYPE RING . SUBPLOT 26. PAGE LAYOUT IS LRV. GENERATE A SIMPLE PLOT . NO BORDER. HINDOW 1.0 8.0 1.0 10.0 . WINDOW FILL. TITLE HEIGHT=1.0, ' GPU-3 HELIUM 927K/339K ' Y AXIS LABEL ' INDICATED POHER ((KW))', MIN=0.0 . X AXIS LABEL ' INDICATED EFFICIENCY ((%))'. EVERY CURVE SYMBOL COUNT 0, PARA3 . Y AXIS TRANSFORM 0. 1000000. 0. 1000. X AXIS TRANSFORM 0. 1. 0. 100. LEGEND STYLE SIMPLEX, TEXT 'CALCULATED:' . INPUT DATA. ' P = 2.74 (MPA)' 1095. 0.29490 1494. 0.28960 0.30000 1929. 2105. 0.27590 0.22250 1908. 0.15510 1454. ' P = 4.10 (MPA)' 0.34430 1828, 0.37430 2815. 0.35730 3360. 3544. 3414. 2930. 0.32070 0.27260 0.21250 ' P = 5.55 (MPA)' 0.39190 2724. 0.39290 3804. 0.36590 4429. 0.32610 4663. 0.27580 4480. 0.21510 3854. ' P = 6.92 (MPA)' 3517. 0.41420 0.39950 4686. 0.36870 5425. 0.32580 5664. 0.26940 5291. 0.21230 4628. ' EXPR. DATA ' 0.320 1160. 0.310 1670. 0.267 2080. 0.231 2060. 0.169 1680. 0.333 2410. 0.293 3300. 0.264 3430. 0.207 2980. 0.305 4490. 0.271 4640. 0.207 4380. 0.265 5480. 0.220 5190. END OF DATA. CURVE 5 SCATTERED, SYMBOL TYPE RING . SUBPLOT 27. ROTATION=MOVIE. \*\* SEND 1. \*\* SEND 2. \*\* SEND 3. 4. \*\* SEND **\*\*** SEND 5. ## SEND 6. SEND 7. SEND 8. SEND 25. SEND 26. SEND 27.

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