

Solubility of Anthracene in Ternary Solvent Mixtures of 2,2,4-Trimethylpentane + 2-Propanone + Alcohols at 298.15 K

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Experimental solubilities are reported for anthracene dissolved in ternary solvent mixtures of 2,2,4-trimethylpentane + 2-propanone + methanol, 2,2,4-trimethylpentane + 2-propanone + ethanol, 2,2,4-trimethylpentane + 2-propanone + 1-propanol, and 2,2,4-trimethylpentane + 2-propanone + 2-propanol at 298.15 K. Nineteen compositions are studied for each of the four solvent systems. Results of these measurements were used to evaluate the prediction capability of a previously developed quantitative structure–property relationship employing the experimental solubility data in monosolvents, and the overall mean deviation (OMD) of the models varied between (13.5 and 15.5) %. Using fully predictive methods, the OMDs varied between (13.1 and 18.2) %.

Introduction

Solubility data are essential information for crystallization-based separations and chromatographic resolutions and also designing new drug formulations. Mixing solvents is a common method to alter the solubility. However, there is a significant lack of solubility data for many solutes; therefore, efforts have been devoted to obtain the required information with a minimum time and substance consumption. When the binary solvent mixtures are not able to dissolve a desired amount of a solute in a given volume, the third solvent could be added to the mixture. The possible number of compositions for the ternary solvents is quite high, and all of them could not be determined experimentally. The development of the ab initio solubility prediction methods with an acceptable error range would be an ideal solution to address the problem. A number of mathematical models have been presented for this purpose, and a summary of the models was given in a recent paper.¹

Experimental solubility data of anthracene in a number of ternary solvent mixtures have been reported by Acree and co-workers, and their references were listed in a previous work.² However, there were no published data on the solubility of anthracene in 2,2,4-trimethylpentane + 2-propanone + alcohol mixtures. 2,2,4-Trimethylpentane is a highly branched saturated hydrocarbon and has been used in several partitioning studies to model the oil phase^{3–5} and was also used as a reference solvent in solubility studies involving drug molecules.⁶

A numerical method was developed employing the Jouyban–Acree model, the Abraham solute parameters, and the Abraham solvent coefficients.⁷ The basic Jouyban–Acree model for calculating the solubility of solutes in ternary solvents is

$$\ln C_m^{\text{Sat}} = x_1 \ln C_1^{\text{Sat}} + x_2 \ln C_2^{\text{Sat}} + x_3 \ln C_3^{\text{Sat}} + x_1 x_2 \sum_{i=0}^2 J_i (x_1 - x_2)^i + x_1 x_3 \sum_{i=0}^2 J'_i (x_1 - x_3)^i + x_2 x_3 \sum_{i=0}^2 J''_i (x_2 - x_3)^i \quad (1)$$

where C_m^{Sat} is the solute mol·L⁻¹ solubility in the ternary solvent mixtures; x_1 , x_2 , and x_3 are the mole fractions of solvents 1, 2, and 3 in the absence of the solute; C_1^{Sat} , C_2^{Sat} , and C_3^{Sat} denote the mol·L⁻¹ solubility of the solute in the neat solvents 1, 2, and 3, respectively; and J_i (for binary mixtures of solvents 1 and 2), J'_i (for binary mixtures of solvents 1 and 3), and J''_i (for binary mixtures of solvents 2 and 3) are the curve-fit coefficients in the Jouyban–Acree model that are determined through regression analysis by fitting the measured anthracene solubilities in the respective binary solvents to eq 1. The solution model used in deriving eq 1 is based on two-body and three-body interactions, and the various curve-fit coefficients are functions of solvent–solvent and solute–solvent interaction terms. The coefficients are described in greater detail elsewhere.⁸ It should be noted that all C^{Sat} terms in this work are expressed as the number of moles of anthracene dissolved in a liter of the solution. In a previous work,⁷ quantitative structure–property relationships (QSPRs) were proposed to calculate the numerical values of the J_i , J'_i , and J''_i terms using Abraham solvent coefficients of 22 solvents and Abraham parameters of five solutes. The QSPRs enable us to predict the solubility of a solute in nonaqueous mixed solvent without employing any experimental data from mixed solvents.

The QSPR models proposed in an earlier work⁷ using water-to-solvent coefficients were

$$J_0 = 0.028 + 2.123(c_1 - c_2)^2 - 0.160E(e_1 - e_2)^2 + 0.282S(s_1 - s_2)^2 + 1.713B(b_1 - b_2)^2 + 2.006V(v_1 - v_2)^2 \quad (2)$$

$$J_1 = 0.033 + 0.670(c_1 - c_2)^2 - 0.477E(e_1 - e_2)^2 + 0.051S(s_1 - s_2)^2 + 0.476B(b_1 - b_2)^2 - 0.234V(v_1 - v_2)^2 \quad (3)$$

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$$J_2 = 0.022 + 2.024(c_1 - c_2)^2 - 0.204E(e_1 - e_2)^2 + 0.034S(s_1 - s_2)^2 + 0.243B(b_1 - b_2)^2 + 0.848V(v_1 - v_2)^2 \quad (4)$$

and the QSPR models using gas-to-solvent coefficients were

$$J_0 = 0.062 + 0.118(c_1 - c_2)^2 - 0.332E(e_1 - e_2)^2 + 0.410S(s_1 - s_2)^2 + 2.399B(b_1 - b_2)^2 + 15.715L(l_1 - l_2)^2 \quad (5)$$

$$J_1 = 0.103 - 1.864(c_1 - c_2)^2 - 1.590E(e_1 - e_2)^2 + 0.119S(s_1 - s_2)^2 + 1.010B(b_1 - b_2)^2 - 9.493L(l_1 - l_2)^2 \quad (6)$$

$$J_2 = -0.008 + 1.075(c_1 - c_2)^2 + 0.053E(e_1 - e_2)^2 + 0.084S(s_1 - s_2)^2 + 0.414B(b_1 - b_2)^2 + 7.727L(l_1 - l_2)^2 \quad (7)$$

where c , e , s , b , v , and l are the model constants (i.e., the Abraham solvent coefficients); subscripts 1 and 2 denote solvents 1 and 2; E is the excess molar refraction of solute; S is dipolarity/polarizability of solute; B stands for the solute's hydrogen-bond basicity; V is the McGowan volume of the solute; and L is the logarithm of the solute gas-hexadecane partition coefficient at 298.15 K. The numerical values of c , e , s , b , v , and l employed in this work were listed in Table 1. The numerical values of the j_i' and j_i'' terms were also computed using eqs 2 to 4 (water-to-solvent) and eqs 5 to 7 (gas-to-solvent) employing the corresponding Abraham solvent coefficients.

The aims of this work are to report the experimental solubility data of anthracene in ternary mixtures of 2,2,4-trimethylpentane, 2-propanone, and C_1 – C_3 alcohol at 298.15 K and also to check the prediction capability of previously reported QSPR models for predicting the solubility of solutes in ternary solvent mixtures.

Experimental Method

Materials. Anthracene (purity 96 %) was purchased from Fluka, and it was recrystallized several times from 2-propanone and ethyl acetate to yield a purified sample having a melting point of 488 K. The purity of recrystallized anthracene (~99 %) was checked by IR spectroscopy, and also the measured solubilities in a number of monosolvents were compared with the corresponding data from the literature. 2,2,4-Trimethylpentane (>99 %), 1-propanol (99.5 %), 2-propanol (99.5 %), absolute ethanol (99.9 %), and methanol (99.5 %) were purchased from Merck.

Apparatus and Procedure. The ternary solvent mixtures were prepared by mixing the appropriate volumes of the solvents, and then the mole fractions of the solvents were computed considering the densities of the neat solvents. The solvent composition could be calculated to 0.005 mol fractions. The solubility of anthracene was determined by equilibrating an excess amount of the solid with the ternary solvent mixtures at 298.15 K using a shaker (Behdad, Tehran, Iran) placed in an incubator equipped with a temperature controlling system with ± 0.2 K. Attainment of the equilibrium was verified by solubility measurements at different times and reached after 72 h. The solutions were filtered using hydrophobic Durapore filters (0.45 μm , Millipore, Ireland) and then diluted with methanol for spectrophotometric analysis at 356 nm quantified by a UV-vis spectrophotometer (Beckman DU-650, Fullerton, USA). The filter did not absorb the solute through a filtration process. Concentrations of the dilute solutions were determined from a UV absorbance calibration graph with the molar concentration of anthracene ranging from $\epsilon/(\text{L}\cdot\text{mol}^{-1}\cdot\text{cm}^{-1}) = 6947$ to $\epsilon/(\text{L}\cdot\text{mol}^{-1}\cdot\text{cm}^{-1}) = 6645$ for the anthracene compositions ranging from $(3.31\cdot 10^{-5}$ to $2.65\cdot 10^{-4}) \text{ mol}\cdot\text{L}^{-1}$. Each experi-

Table 1. Abraham Solvent Coefficients Employed in This Work Taken from Reference 10

water to solvent	c	e	s	a	b	v
1-propanol	0.148	0.436	-1.098	0.389	-3.893	4.036
2,2,4-trimethylpentane	0.288	0.382	-1.668	-3.639	-5.000	4.461
2-propanol	0.063	0.320	-1.024	0.445	-3.824	4.067
2-propanone	0.335	0.349	-0.231	-0.411	-4.796	3.963
ethanol	0.208	0.409	-0.959	0.186	-3.645	3.928
methanol	0.329	0.299	-0.671	0.080	-3.389	3.512
gas to solvent	c	e	s	a	b	l
1-propanol	-0.028	-0.185	0.648	4.022	1.043	0.869
2,2,4-trimethylpentane	0.275	-0.244	0.000	0.000	0.000	0.972
2-propanol	-0.060	-0.335	0.702	4.017	1.040	0.893
2-propanone	0.154	-0.277	1.522	3.258	0.078	0.863
ethanol	0.012	-0.206	0.789	3.635	1.311	0.853
methanol	-0.004	-0.215	1.173	3.701	1.432	0.769

mental data point is an average of at least three experiments with the measured $\text{mol}\cdot\text{L}^{-1}$ solubilities being reproducible to within ± 2.0 %. Calculated standard deviations ranged from $\sigma_n - 1 = 0.0002$ to $\sigma_n - 1 = 0.0018 \text{ mol}\cdot\text{L}^{-1}$.

Computational Methods. The J_i , j_i' , and j_i'' terms of the Jouyban-Acree model were computed using eqs 2 to 4 and then were used to predict anthracene solubility data in ternary solvent mixtures using eq 1 employing experimental values of C_1^{Sat} , C_2^{Sat} , and C_3^{Sat} . This numerical analysis was called method I. The same computations were carried out employing eqs 5 to 7, and it was called numerical method II. For solubility prediction methods I and II, the solubility data in monosolvent systems, i.e., three points for each ternary solvent system, are required. To further reduce the experimental data requirement in the prediction process, it is possible to use the Abraham solvation models to predict C_1^{Sat} , C_2^{Sat} , and C_3^{Sat} values and use the predicted solubilities in monosolvents in eq 1. The Abraham model for the water-to-solvent process is

$$\log\left(\frac{C_S}{C_W}\right) = c + e\cdot E + s\cdot S + a\cdot A + b\cdot B + v\cdot V \quad (8)$$

and for the gas-to-solvent process

$$\log\left(\frac{C_S}{C_G}\right) = c + e\cdot E + s\cdot S + a\cdot A + b\cdot B + l\cdot L \quad (9)$$

where C_S (the same term as C_1^{Sat} , C_2^{Sat} , and C_3^{Sat} from this work) and C_W are the solute solubility in the organic solvent and water (in $\text{mol}\cdot\text{L}^{-1}$), respectively; a is the Abraham solvent coefficient; A denotes the solute's hydrogen-bond acidity; and C_G is the gas phase concentration of the solute. Equation 8 requires the aqueous solubility of the solute (C_W), and eq 9 requires the C_G value. The numerical values of the solute's Abraham experimental parameters for anthracene are: $\log C_W = -6.430$, $E = 2.290$, $S = 1.340$, $A = 0.000$, $B = 0.280$, $V = 1.454$, $L = 7.568$, and $\log C_G = -9.460$.⁹ The predicted C_1^{Sat} , C_2^{Sat} , and C_3^{Sat} from eq 8 and J terms computed using eqs 2 to 4 were used to predict the C_m^{Sat} , and this numerical method was called method III. A similar numerical analysis employing eqs 9 and 5 to 7 was called method IV.

All predicted solubilities (C_m^{Sat}) were compared with the corresponding experimental values, and the mean deviation (MD) was calculated as a criterion by eq 10

$$\text{MD} = \frac{\sum \left\{ \frac{|(C_m^{\text{Sat}})_{\text{pred}} - (C_m^{\text{Sat}})|}{(C_m^{\text{Sat}})} \right\}}{N} \quad (10)$$

where N is the number of data points in each set.

methods and their overall MD were listed in Table 3. Of the numerical methods employing the experimental solubilities in solvents 1, 2, and 3, the method I was the best prediction method, whereas the numerical method IV was the best fully predictive method for anthracene solubilities in the investigated solvent systems. These findings are in agreement with the previous results obtained for the same analyses employing 194 data sets.⁷

Equations 2 to 7 were trained using the solubility data sets expressed in mole fraction units; however, in this work, we expressed the solubilities in mol·L⁻¹, and this difference in solubility expression could be compensated by adding a correction term to the Jouyban–Acree model as

$$\ln C_m^{\text{Sat}} = x_1 \ln C_1^{\text{Sat}} + x_2 \ln C_2^{\text{Sat}} + x_3 \ln C_3^{\text{Sat}} + x_1 x_2 \sum_{i=0}^2 J_i (x_1 - x_2)^i + x_1 x_3 \sum_{i=0}^2 J'_i (x_1 - x_3)^i + x_2 x_3 \sum_{i=0}^2 J''_i (x_2 - x_3)^i + [x_1 \ln MV_1 + x_2 \ln MV_2 + x_3 \ln MV_3 - \ln(x_1 MV_1 + x_2 MV_2 + x_3 MV_3)] \quad (11)$$

in which MV₁, MV₂, and MV₃ are the molar volumes of the solvents 1, 2, and 3, respectively. The numerical values of MV for the solvents used in this work are reported in Table 2. This correction improves the MD of the proposed method, as a detailed report could be found in Table 3.

Generally the overall MDs observed in these computations reveal that the developed QSPR models are robust and could be used for prediction purposes.

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Received for review January 15, 2008. Accepted February 1, 2008. The authors would like to thank the Drug Applied Research Center for the financial support under grant No. 85-83.

JE8000415