**A User's Manual
for the BNW-I Optimization
Code for Dry-Cooled
Power Plants**

Volume III

January 1977

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Battelle

Pacific Northwest Laboratories

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A USER'S MANUAL FOR THE BNW-I OPTIMIZATION
CODE FOR DRY-COOLED POWER PLANTS

VOLUME III

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January 1977

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PREFACE

This document has been issued in four volumes to facilitate handling. Volume I is a narrative description of the code algorithms, as well as logic, input and output information. Volumes II through IV are appendices of Volume I, providing listings of the BNW-I optimization code for each of three dry-cooled heat rejection systems. These are:

Volume II - Metal Finned Tube Versions of the BNW-I Computer Code

Volume III - Plastic System Versions of the BNW-I Computer Code

Volume IV - Ammonia System Versions of the BNW-I Computer Code

Complete distribution has been given only to Volume I. Copies of one or more of the other three volumes may be obtained by writing the National Technical Information Service, U.S. Department of Commerce, 5281 Port Royal Road, Springfield, VA, 22151.

APPENDIX F

PLASTIC VERSION OF THE BNW-I COMPUTER CODE

Figure F-1 is a subroutine linkage chart indicating which subroutines may call or may be called by others. This chart should be of assistance in using the listing making up the remainder of this appendix.

- INDICATES CALLING PROGRAM
- INDICATES CALLED PROGRAM

FIGURE F-1. Plastic Circular Model Subroutine Linkages


```
PROGRAM PLCIR1(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT)
```

```
PROGRAM PLCIR1 IS A VERSION OF THE BNWI COMPUTER  
OPTIMIZATION CODE DEVELOPED BY PNL FOR EPDA UNDER THE  
DRY COOLING TOWER PROGRAM. IT DETERMINES THE OPTIMUM  
DRY COOLING TOWER DESIGN FOR A PARTICULAR SIZE POWER  
PLANT WITH A PLASTIC TUBE COOLING SURFACE AND CIRCULAR  
TOWER ARRANGEMENT OF THE TUBE BUNDLES.
```

```
DIMENSION PCST(8)
```

```
LOGICAL FIRST, FXTMP
```

```
COMMON
```

```
  $ AFTR, ALPHA
```

```
  $ ,CAPF, C5SPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAPF
```

```
  $ ,CRJ, CSEALP, CELAST, CFS, COANG, CLUVR, CTAILS, CVM
```

```
  $ ,DEEPL, DESVEL, DANGLE
```

```
  $ ,EFPF
```

```
  $ ,FCR, FIRST, FIXL, FCOS, FXTMP
```

```
  $ ,GREFE
```

```
  $ ,HXNP, HPCST
```

```
  $ ,THEAT
```

```
  $ ,ITMAX, ITMIN
```

```
  $ ,JCONC
```

```
  $ ,KCONV, KALEXT
```

```
  $ ,MXEXT
```

```
  $ ,NTUCAL(2), NTA
```

```
COMMON
```

```
  $ ODR
```

```
  $ ,PSIZE, PER, PWCOS, PLAVC, PFACT
```

```
  $ ,POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCU
```

```
  $ ,PREU, PREDUCE
```

```
  $ ,RBP, REDUCE, ROESEL, ROEELA, ROOFL, RFX
```

```
  $ ,SAAF, SIGMA, SPAMAT(2)
```

```
  $ ,TD, TPO(4), TEFF, TLIM, TLRA, TSEALP, TELAST, THFIN, TFX
```

```
  $ ,TJRA, G, TW
```

```
  $ ,UCS, UWS
```

```
  $ ,VAS(3)
```

```
  $ ,WEV
```

```
  $ ,XDEP1, XW, XD
```

```
COMMON /SINK/ VAR(5), CPIP1, CCOS1, W3, COSM1, EFF1
```

```
  $ , CLAM1, REA11, Z1, HRFAC2, W41, U1, PPOW1,
```

```
  $ , FPO1, DEFC1, WIDT1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,
```

```
  $ , REW1, NW1, ZPLNC2, ZSI712, ZSPBP, SW41, SW31,
```

```
  $ , SP1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
```

```
  $ , R2MIN, V2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONBA1, XNTS1, VELD1
```

```
  $ , TL11, UCON1, FMCS1, FRAC1, EFFC1, CH1, CA1, CS1
```

```
  $ , CLTC1, CFC1, CPCC1, FITC1, CSCL, CEPRE1, DEPI1, AST1
```

```
  $ , CAPCS1, XVEAN1, BLDAN1, CPLEN1, DPFE1, WH1, NTTU1, AD11, ABL1
```

```
  $ , VTHD1, WTER1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
```

```
  $ , AIRFE1, WATFE1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACTTP1, ADJTP1
```

```
  $ , ACTH1, ADJBP1, ACTVH1, ADJVH1, ADJPP1, THPA11, TCTF1, AFCST1
```

```
  $ , CS1, WATER1, WSTRC1, CFJUV1, HUBO11, TOWLE1, CSE1, CHF1
```

```
  $ , CBAL, NUTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
```

```
COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1
```

```
  $ GAIR, FAIR, HPAIR, HPWAT, PLANCT1
```

```
COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
```

```
  $ , CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,
```

```

      $ FPOW, DELFC, WIDTH, ELENG, VAIR, VWAT, HI, MO, T4,
      $ REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3,
60  $ SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
      $ BP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELDX
      $ TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
      $ CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPIP, AST
      $ CAPCST, XNFAN, BLDANG, CPLEN, DPFL, WHX, ATUB, ADIA, ABLN
65  $ WTHDR, WTRM, STRUCC, CPERF, HPPERF, TOTCF, EFFIN, ANTU
      $ AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTP, ADJTP
      $ ACTBD, ADJBD, ACTVH, ADJVH, ADJPPF, THAIR, TCTF, AFCST
      $ CSPD, WATERW, WSTRCT, CFOUND, HUBDIA, TOWLEN, CSE, CHF
      $ CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
70  COMMON /VARVAR/ TPER(16), TA(15)
      COMMON /INDIS/ DIST
      COMMON /TINE/ XNS, TTD, TLA, XNTS, ARPS
81  FORMAT("1TD USED IN THE FOLLOWING CALCULATIONS IS ="F8.3)
930  FORMAT(T02, "AMBIENT TURBINE", T28, "HEAT", T83, "COST TO",
75  $ T93, "POWER COST", T105, "PCT TIME", T115, "PORTION OF")
931  FORMAT(T04, "TEMP", T10, "OUTLET", T20, "BACK", T28, "RATE", T50, "HX"
      $, T57, "HX", T64, "POWER", T72, "CHANGE IN", T83, "REPLACE",
      $, T93, "AT AMBIENT", T104, "AT AMBIENT", T115, "INCREMENTAL")
932  FORMAT(T11, "TEMP", T18, "PRESSURE", T27, "FACTOR", T35, "RANGE"
80  $, T42, "TTOP", T49, "LMTD", T57, "ITD", T62, "GENERATED"
      $, T72, "FUEL COST", T83, "LOST CAP", T95, "TEMP", T106, "TEMP"
      $, T115, "POWER COST")
933  FORMAT( T02, T31(" " ), T9, " ", T17, " ", T26, " ", T32, " ", T40, " "
85  $, T47, " ", T54, " ", T61, " ", T71, " ", T81, " ", T92, " ", T103, " "
      $, T114, " ")
934  FORMAT( T03, "DEG F", T11, "DEG F", T19, "IN. Hg", T35, "DEG F"
      $, T41, "DEG F", T49, "DEG F", T56, "DEG F", T62, "MEGAWATTS"
      $, T72, "MILLS/KWH", T82, "MILLS/KWH", T93, "MILLS/KWH"
      $, T106, "PERCENT", T115, "MILLS/KWH")
90  944  FORMAT(140, T91, "FINAL INCREMENTAL COST", G11.5)
945  FORMAT(140, T96, "CAPACITY CHARGE $", G15.8)
      FIRST=.TRUE.
15  NUCASE = 0

C
C      READ IN THE EXTERNALLY FIXED PARAMETERS OF THE DRY COOLING
C      TOWER SYSTEM AND THE INITIAL STARTING POINT OF THE
C      OPTIMIZATION ROUTINE. A DESCRIPTION OF THE INPUT CARDS
C      IS GIVEN IN SUBROUTINE SETUP
95
C
C      CALLI SETUP(TSTAR, TEND, NUCASE)
100  20  CONTINUE
C
C      INPUT PRINTOUT SUMMARY
C
C      CALLI IMPSUM
105
C
C      THE FOLLOWING IS A ROUTINE WHICH USES PATTERNED AND
C      GRADIENT SEARCH ROUTINES TO DETERMINE THE OPTIMUM DRY
C      COOLING TOWER DESIGN
110
C
      DO 7 IS=1,5
      7  VAR(IS)=0.0
      TD=YSTAR
      1  WRITE(4,81)TD

```

```

115      K=4
      C
      C      SCALING THE STEAM SUPPLY AND TURBINE TO ACCOUNT FOR CHANGE
      C      IN HEAT RATE OF TURBINE
      C
120      CALL SSCALE
      C
      C      COURSE PATTERN SEARCH FOR OPTIMUM POINT
      C
      4 CALL SHOT(1)
      IF (ICOR1.GT.0.0) GO TO 5
125      VAS(4)=VAS(4)/4.
      GO TO 4
      5 L=0
      C
      C      EXTENDING THE SEARCH BEYOND THE LIMITS OF THE PATTERN
130      C      SEARCH
      CALL XTEND(L)
      IF (L.EQ.1) GO TO 4
      C
      C      FINE PATTERN SEARCH FOR THE OPTIMUM POINT
135      CALL SHOT(2)
      2 JCONV=0
      C
      C      GRADIENT SEARCH FOR THE OPTIMUM POINT
      CALL SERCH
140      IF (JCONV.EQ.0) GO TO 10
      K=K+1
      IF (K.GT.0) GO TO 2
10      CONTINUE
145      C
      C      PRINTOUT OF DRY COOLING TOWER DESIGN
      C
      CALL OUT2(RBP,HRFAC1,SSCD,CASSS1,PLANCT1,PLANC1)
      CALL OUT4(1)
      CALL OUT4(2)
150      CALL ROTHXD
      CALL ROTHXC(AFRO1)
      CALL RORT1(DESVEL,POHCIR)
      CALL RORT2(EFFC1,CONMAT,CONMA2)
      CALL OPTFAN
155      WRITE(4,100)
      100 FORMAT(1-1)
      WRITE(4,930)
      WRITE(4,931)
      WRITE(4,932)
160      WRITE(4,933)
      WRITE(4,934)
      WRITE(4,933)
      CLSUM=0.0
      FCSJM=0.0
165      C
      C      CALCULATION AND PRINTOUT OF THE PERFORMANCE PARAMETERS OF
      C      THE DRY COOLING TOWER AND POWER PLANT FOR A YEARLY
      C      TEMPERATURE PROFILE
      C
170      DO 3 I=1,NTA
      3 CALL VARIT(TA(I),TPER(I),PCST(I),I,CLSUM,FCSJM)

```

```
      ACOS=0.0
      DO 9 I=1,NTA
      ACOS=ACOS+PCST(I)
175      8 CONTINUE
      WRITE(6,944) ACOS
      WRITE(6,945) CAPCS1
      C
      C      CAPITAL AND OPERATION COST SUMMARY PRINTOUT
180      C
      CALL SUMCOS(FCR, PSIZE, CAPF, CCOS1, CPIP1, CONBA1, ATUBC1, CPLEN1
      S ,FBAC1, FMCS1, STRUC1, CFOUN1, CAPCS1, SPCD1, SSCD, HRFAC1
      S ,HREFAS, YFPMIN, PLAN1, CLAN1, CLSUM, FCSUM, COSM1, CSTLV1
      S ,CSTHS1, CFANE1*XNFAN1, CYLRN1*XNFAN1)
185      TD=TD + 5.
      FIRST = .TRUE.
      KALEXT = 0
      WRITE(6,100)
      IF (TD.LE.TEND) GOTO 1
190      6 CONTINUE
      NUCASE=1
      CALL SETUP(TSTAR,TEND,NUCASE)
      IF (NUCASE.EQ.0) GOTO 15
      GO TO 20
195      END
```

SUBROUTINE CALC(T1,RANGE,CWARA,AFRON,WLRAT,M)

SUBROUTINE CALC OF THE PLASTIC TUBE DRY COOLING TOWER SYSTEM CODE DETERMINES THE DIMENSIONS AND DESIGN PARAMETERS OF THE HEAT EXCHANGER. THE COST OF THE HEAT EXCHANGER SURFACE IS FOUND BY A SEPARATE ROUTINE INITIATED FROM THIS SUBROUTINE. THE DESIGN AND COSTING OF THE FAN AND PIPING SYSTEMS ARE DONE BY SEPARATE ROUTINES ALSO INITIATED FROM THE CALC SUBROUTINE.

THE INPUT PARAMETERS ARE SUPPLIED TO THE CALC SUBROUTINE BY THE OPTIMIZATION ROUTINE DEVELOPED BY M.I.T. IT IS A COMBINATION OF A PATTERN AND GRADIENT SEARCH ROUTINE. THE PURPOSE OF THE OPTIMIZATION PART OF THE CODE IS TO MINIMIZE THE INCREMENTAL COST OF DRY COOLING BY VARYING THE DESIGN OF THE DRY COOLING TOWER. IT THEREFORE SUPPLIES FIVE DESIGN VARIABLES TO SUBROUTINE CALC AND IN RETURN AN INCREMENTAL COST IS FOUND.

THE FOLLOWING ARE THE INPUT PARAMETERS TO SUBROUTINE CALC

- T1 - STEAM TURBINE EXHAUST TEMPERATURE (DEGREES F)
- RANGE - TEMPERATURE DIFFERENCE OF THE WATER ENTERING AND LEAVING THE HEAT EXCHANGER (DEGREES F)
- CWARA - RATIO OF THE HEAT CAPACITY OF THE WATER TO THE AIR (DIMENSIONLESS)
- AFRON - FRONTAL AREA OF THE HEAT EXCHANGER IN THE DIRECTION OF AIR FLOW (SQ FT)
- WLRAT - RATIO OF THE WIDTH TO THE LENGTH OF THE HEAT EXCHANGER (DIMENSIONLESS)
- M - PARAMETER WHICH SPECIFIES WHICH OF THE ABOVE HAS BEEN VARIED BY THE OPTIMIZATION ROUTINE SINCE THE LAST TIME THROUGH CALC

DEFINITIONS OF VARIABLES

- AAIR - AIR SIDE HEAT TRANSFER AREA (SQ FT)
- AFC - CAPITAL COST OF FAN SYSTEM (\$)
- ANTU - HEAT EXCHANGER NUMBER OF TRANSFER UNITS (DIMENSIONLESS)
- BAR - ATMOSPHERIC PRESSURE FOR A PARTICULAR ELEVATION (IN HGA)
- CMIN - THE SMALLEST HEAT TRANSFER CAPACITY BETWEEN THE AIR AND THE WATER (BTU/HR DEG F)
- CONL - THERMAL CONDUCTIVITY OF THE TUBE WALL (BTU/HR FT DEG F)
- DEEPL - UPPER OR LOWER LIMIT ON THE NUMBER OF TUBES IN DEPTH (DIMENSIONLESS)
- DELPA - AIR SIDE PRESSURE DROP ACROSS THE HEAT EXCHANGER BUNDLE (LBF/SQ FT)
- DELPPI - PRESSURE DROP THROUGH THE SUPPLY AND RETURN PIPING SYSTEM (LBF/SQ FT)
- DELPWC - PRESSURE DROP THROUGH THE CONDENSER (LBF/SQ FT)
- DELPWT - PRESSURE DROP THROUGH THE HEAT EXCHANGER BUNDLE (LBF/SQ FT)

60	C	DEPTH	- DEPTH OF THE HEAT EXCHANGER PARALLEL TO THE AIR FLOW (FT)
	C	DI	- INSIDE DIAMETER OF THE HEAT EXCHANGER TUBE (IN)
	C	EFF	- HEAT EXCHANGER EFFECTIVENESS (DIMENSIONLESS)
	C	EFFP	- PUMP EFFICIENCY (PERCENT)
	C	ELFNG	- LENGTH OF HEAT EXCHANGER TUBES (FT)
	C	ELEV	- SITE ELEVATION (FT)
65	C	FAIR	- AIR SIDE FRICTION FACTOR (DIMENSIONLESS)
	C	FIXL	- THE FIXED LENGTH OF HEAT EXCHANGER TUBES SPECIFIED BY INPUT TO THE CODE (FT)
	C	GAIR	- MASS FLUX OF AIR THROUGH THE TRANSVERSE AREA BETWEEN TUBES OF THE HEAT EXCHANGER (LBM/SQ FT HR)
70	C	GAIRD	- MASS FLUX OF AIR THROUGH THE DIAGONAL AREA BETWEEN TUBE ROWS OF THE HEAT EXCHANGER (LBM/SQ FT HR)
	C	GWAT	- MASS FLUX OF WATER THROUGH THE EXCHANGER TUBES (LBM/SQ FT HR)
	C	HI	- WATER SIDE HEAT TRANSFER COEFFICIENT THROUGH THE HEAT EXCHANGER TUBES (BTU/HR SQ FT DEG F)
75	C	HO	- AIR SIDE HEAT TRANSFER COEFFICIENT THROUGH THE HEAT EXCHANGER BUNDLE (BTU/HR SQ FT DEG F)
	C	HPWAT	- HORSEPOWER REQUIREMENTS OF WATER PUMPING SYSTEM FOR THE CONDENSER, PIPING SYSTEM, AND COOLING TOWER (HP)
80	C	HFAC1	- HEAT RATE FACTOR OF STEAM TURBINE AT THE RATED BACK PRESSURE (DIMENSIONLESS)
	C	HFAC2	- HEAT RATE FACTOR OF STEAM TURBINE AT THE DESIGN TEMPERATURE (DIMENSIONLESS)
85	C	HNYP	- NUMBER OF PASSES OF WATER THROUGH THE HEAT EXCHANGER (DIMENSIONLESS)
	C	IHEAT	- INTERNAL VARIABLE FOR SELECTING THE FRICTION FACTOR AND HEAT TRANSFER COEFFICIENT FOR THE INLINE OR STAGGERED TUBE SPACING (DIMENSIONLESS)
90	C	KCONV	- INTERNAL VARIABLE FOR SPECIFYING THAT THE SET OF INPUT VARIABLES LEAD TO UNREASONABLE ANSWERS (DIMENSIONLESS)
	C	NTUCAL	- SPECIFIES THE TYPE OF NTU-EFFECTIVENESS CALCULATION TO BE USED BY THE CODE (DIMENSIONLESS)
95	C	NJMTOW	- NUMBER OF CIRCULAR TOWERS (DIMENSIONLESS)
	C	NW	- NUMBER OF HEAT EXCHANGER TUBES IN WIDTH (DIMENSIONLESS)
	C	ODL	- OUTSIDE DIAMETER OF HEAT EXCHANGER TUBES (IN)
100	C	P	- STEAM TURBINE BACK PRESSURE (IN HGA)
	C	PDOW	- POWER REQUIREMENTS OF WATER PUMPING SYSTEM FOR THE CONDENSER PIPING SYSTEM AND COOLING TOWER (KW)
	C	PSIZE	- POWER OUTPUT OF PLANT (KW)
	C	QIN	- HEAT SUPPLIED BY THE STEAM SUPPLY SYSTEM (BTU/HR)
	C	QREU	- HEAT REJECTED BY THE DRY COOLING TOWER (BTU/HR)
105	C	REAIR	- REYNOLDS NUMBER OF THE AIR FLOWING THROUGH THE MINIMUM CROSS-SECTIONAL AREA OF THE HEAT EXCHANGER (DIMENSIONLESS)
	C	REFF	- EFFECTIVE HEAT EXCHANGER TUBE WALL THICKNESS BASED ON AIR SIDE TUBE AREA (FT)
110	C	REWAT	- REYNOLDS NUMBER OF THE WATER FLOWING THROUGH THE HEAT EXCHANGER TUBES (DIMENSIONLESS)
	C	TCOS	- INCREMENTAL COST FOR THE USE OF DRY COOLING TOWERS (MILLS/KWH)
	C	TOWFCS	- TOTAL COST OF THE PIPING SYSTEM (K\$)

```

115      C      TEFF - RATED BACK PRESSURE EFFICIENCY OF THE STEAM
      C      TURBINE (PERCENT)
      C      TEFFM - EFFICIENCY OF THE STEAM TURBINE AT THE DESIGN
      C      TEMPERATURE (PERCENT)
      C      TEO - COEFFICIENTS OF THIRD ORDER CURVE FIT OF HEAT
120      C      RATE FACTOR VERSUS TURBINE BACK PRESSURE
      C      (DIMENSIONLESS)
      C      TTD - TERMINAL TEMPERATURE DIFFERENCE BETWEEN THE STEAM
      C      AND WATER TEMPERATURES OF THE CONDENSER (DEG F)
      C      TA - EXIT TEMPERATURE OF THE AIR FROM THE HEAT EXCHANGER
125      C      BUNDLE (DEG F)
      C      U - OVERALL HEAT TRANSFER COEFFICIENT OF THE HEAT
      C      EXCHANGER (BTU/HR SQ FT DEG F)
      C      VAAV - AVERAGE SPECIFIC VOLUME OF THE AIR IN THE HEAT
      C      EXCHANGER BUNDLE (CU FT/LBM)
130      C      VAIN - SPECIFIC VOLUME OF THE AIR ENTERING THE HEAT
      C      EXCHANGER BUNDLE (CU FT/LBM)
      C      VAIR - VELOCITY OF THE AIR IN THE MINIMUM CROSS-SECTIONAL
      C      AREA OF THE HEAT EXCHANGER (FT/SEC)
      C      VAO - SPECIFIC VOLUME OF THE AIR LEAVING THE HEAT EX-
135      C      CHANGER BUNDLE (CU FT/LBM)
      C      VOL - TOTAL VOLUME OF THE HEAT EXCHANGER (CU FT)
      C      VWAT - WATER VELOCITY THROUGH THE HEAT EXCHANGER TUBES
      C      (FT/SEC)
      C      WIDTH - TOTAL HEAT EXCHANGER WIDTH (FT)
140      C      WR - MASS FLOW RATE OF WATER THROUGH THE COOLING TOWER
      C      (LBM/HR)
      C      WA - MASS FLOW RATE OF AIR THROUGH THE COOLING TOWER
      C      (LBM/HR)
      C      XD - LONGITUDINAL PITCH BETWEEN ADJACENT TUBE ROWS
145      C      OF THE HEAT EXCHANGER FROM CENTERLINE TO
      C      CENTERLINE (IN)
      C      XDG - LONGITUDINAL DIAGONAL PITCH BETWEEN TUBES IN
      C      ADJACENT ROWS OF THE HEAT EXCHANGER CENTERLINE TO
      C      CENTERLINE MEASUREMENT (IN)
150      C      XW - TRANSVERSE PITCH BETWEEN ADJACENT TUBES IN THE SAME
      C      TUBE ROW OF THE HEAT EXCHANGER FROM CENTERLINE
      C      TO CENTERLINE (IN)
      C      ZD - NUMBER OF HEAT EXCHANGER TUBES IN DEPTH
155      C      HEAT EXCHANGER DIMENSIONAL RELATIONSHIP
      C      AT - INSIDE TUBE AREA (SQ FT/FT)
      C      OSA - OUTER TUBE SURFACE AREA (SQ FT/FT)
      C      ATOT - TOTAL OUTER SURFACE AREA (SQ FT/FT)
160      C      VOLP - HEAT EXCHANGER VOLUME (CU FT/FT)
      C      ART - CROSS SECTIONAL ROOT TUBE AREA (SQ FT/FT)
      C      ACS - UNIT CROSS-SECTIONAL AREA (SQ FT/FT)
      C      ALPHA - TUBE SURFACE AREA PER UNIT HEAT EXCHANGER VOLUME
      C      (SQ FT/FT)
165      C      SIGMA - RATIO OF FREE FLOW AREA TO TOTAL FRONTAL
      C      AREA (DIMENSIONLESS)

```

```

      LOGICAL FXTLNG
      LOGICAL FIRST, FXTMP
      COMMON
      $ AFTR, ALPHA

```

170

```

175 $ ,CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONW2, CAP1
    $ ,CBU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILS, CVM
    $ ,DEEPL, DESVEL, DANGLE
    $ ,EFFP
    $ ,FCR, FIRST, FIXL, FCOS, EXTEMD
    $ ,G3EFF
    $ ,HXNP, HPCST
180 $ ,IHEAT
    $ ,ITMAX, ITMIN
    $ ,JCONC
    $ ,KCONV, KALEXT
    $ ,MXEXT
    $ ,NTUCAL(2), NTA
185 COMMON
    $ ,CDR
    $ ,PSIZE, PER, PWCOS, PLANC, PFACT
    $ ,POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCU
    $ ,QREU, QREDUCE
190 $ ,RBP, REDUCE, ROESL, ROELA, ROOFL, RFX
    $ ,SAAF, SIGMA, SPAMAT(2)
    $ ,TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
    $ ,TUBARG, TW
    $ ,UCS, UWS
195 $ ,VAS(5)
    $ ,WTV
    $ ,XDEPA, XW, XD
COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFFI
200 $ , CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,
    $ , FPOW, DEFC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4,
    $ , REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3,
    $ , SOC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
    $ , BP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELDX
205 $ , TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
    $ , CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPIP, AST
    $ , CAPCST, XNFAN, BLDANG, CPLEN, DPFL, WHX, ATTUB, ADIA, ABLN
    $ , WTHOR, WTRFM, STRUCC, CPERF, HPPERF, TOTCF, EFFIN, ANTU
    $ , AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCITP, ADJTP
210 $ , ACTBPD, ADJBPD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
    $ , CSPD, WATERW, WSTRCT, CFOUND, HUBDIA, TOWLEN, CSE, CHF
    $ , CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
215 $ , CLAN1, REA11, Z1, HRFAC2S, W41, U1, PPOW1,
    $ , FPOW1, DEFC1, WIDTH1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,
    $ , REW1, NW1, ZPLNC2, ZSIZ12, ZSPBP, SW41, SW31,
    $ , SPC1, PTOT1, PLNC31, AFK01, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
    $ , BP2MIN, NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONBA1, XNTS1, VELD1
    $ , TL1, UCON1, FMC1, FBAC1, EFFC1, CH1, CA1, CS1
220 $ , CLTC1, CFC1, CPCC1, FITC01, CSC1, CEPRE1, DEPIP1, AST1
    $ , CAPCST1, XNFAN1, BLDAN1, CPLEN1, DPFL1, WH1, ATTU1, ADI1, ABL1
    $ , WTHO1, WTRF1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
    $ , AIRF1, WATF1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACTTP1, ADJTP1
    $ , ACTB1, ADJB1, ACTVH1, ADJVH1, ADJPP1, THPA1, TCTF1, AFCST1
225 $ , CSP1, WATER1, WSTRC1, CFOUND1, HUBD1, TOWLE1, CSE1, CHF1
    $ , CBA1, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,
    $ , GAIR, FAIR, HPAIR, HPWAT, PLANC1
COMMON /DJB/DI/XDG/SF

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230      COMMON /FLSW/ FXTLNG
      COMMON /INDIS/ DIST
      COMMON /HEADEX/ DUM12(16), WB
      COMMON /HXD/ AI, ATOT
      COMMON /LACALL/ SRN
235      COMMON /TIVE/ XNS,TTD,TLA,XNTS,ARPS
      COMMON /SURFEX/ DOL, DUM1ST(15)
      COMMON /TUBE/ KGA,FGA(7),LD,ESA(6),TID(7,6),FTF(7,6)
      COMMON /FAN/ FANDAP(153,10),FANDAH(153,10),FMCPF, FBCPF,
      $VELREC,AFR,EL-EV,EHR
240      300 FORMAT(" CALC M=",I1,3X,"T1=",IPE11.4,3X,"RANGE=",E11.4,3X,
      $ "CWAPA=",E11.4,3X,"AFRON=",E11.4,3X,"WLRAT=",E11.4)
245      301 FORMAT(" CALC M=",I1,3X,"T1=",IPE11.4,3X,"RANGE=",E11.4,3X,
      $ "CWARA=",E11.4,3X,"AFRON=",E11.4,3X,"WLRAT=",E11.4,T110,"TCOS=",
      $ E11.4)
      8 FORMAT("NO ZERO DIVISOR IN SUBROUTINE CALC. AFRON=",IPE13.4,6X,
      $ "SIGMA=",E13.4)
250      305 FORMAT(" /CALC/ ",T1=","E9.3," HRFAC2=","E9.3," TEFFM=","E9.3,
      $ " QIN=","E9.3,"QREJ="," N3=","E9.3," N4=","E9.3)
      316 FORMAT(" IN SUBROUTINE CALC A VALUE OF",G13.5," FOR AFRON WAS IGNO-
      $ RED BECAUSE IT PRODUCES ZERO VALUE FOR NW")
255      903 FORMAT("ERROR IN DEPTH CALCULATION LOOP IN SUBROUTINE CALC."
      $ /1X,"W,W3,DI,ZD,AAIR,VOL,AFRON",I3,6G13.5)
      303 FORMAT(1X,I3," ITERATIONS IN CALC WITHOUT CONVERGING ON DEPTH, PZD
      $ ="G13.5," ZD="G13.5," AFRON="G13.5)
      DATA M*7K /0/
260      C
      C      THE FOLLOWING ARE BRANCH POINTS OF THE SUBROUTINE
      C      DEPENDING ON THE PARAMETER WHICH HAS BEEN VARIED SINCE THE
      C      LAST TIME THROUGH CALC, THE PROGRAM BY PASSES THOSE
      C      CALCULATIONS THAT DO NOT HAVE TO BE RECALCULATED
265      C
      C      IF (FXTLNG3.AND.LVC.EQ.M.AND.M.EQ.5) RETURN
      C      KCONV=0
      C      IF (M.EQ.5) GO TO 23
      C      IF (M.EQ.4) GO TO 22
      C      IF (M.EQ.3) GO TO 21
      C      IF (M.EQ.2) GO TO 20
270      C
      C      THE BACK PRESSURE OF THE TURBINE IS GIVEN HERE AS A
      C      FUNCTION OF THE STEAM TURBINE EXHAUST TEMPERATURE (IN HGA)
      C
      C      P=EXP((7.169-9240./(T1+460.))
      C      BP2=P
275      C
      C      THE HEAT RATE FACTOR OF THE TURBINE IS CALCULATED HERE
      C      AS A FUNCTION OF THE TURBINE BACK PRESSURE (DIMENSIONLESS)
      C
      C      HEAT RATE FACTOR CURVE FIT
      C
      C      HRFAC2=TP0(1) +TP0(2)*P +TP0(3)*P**2 + TP0(4)*P**3
280      C
      C      THE OFF DESIGN TURBINE EFFICIENCY IS GIVEN BY THE
      C      FOLLOWING (PERCENT)
      C
      C      TEFFM=TEFF/HRFAC2
285      C

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C      THE TOTAL HEAT CONSUMPTION OF (BTU/HR) THE PLANT IS
C      GIVEN AS A FUNCTION OF POWER OUTPUT OF THE PLANT
C      (MW) AND THE TURBINE EFFICIENCY
C
290      QIN=3413.*PSIZE*1000./TEFFM
C
C      THE HEAT REJECTED BY THE DRY COOLING TOWER (BTU/HR)
C      IS THE FOLLOWING
C
295      QREJ=QIN*(1.-TEFFM)
C
C      KNOWING THE AMOUNT HEAT REJECTED BY THE DRY COOLING
C      TOWER AND THE RANGE OF THE WATER, THE MASS FLOW RATE OF THE
C      WATER FLOWING THROUGH THE TOWER CAN BE CALCULATED (LBM/HR)
300
C      20 W3=QREJ/RANGE
C
C      GIVEN THE CAPACITY RATIO OF THE AIR TO THE WATER, THE
C      MASS AIR FLOW RATE CAN BE CALCULATED (LBM/HR)
305
C      21 W4=W3/(CWARA*.24)
C
C      THE DESIGN OF THE HEAT EXCHANGER IS HANDLED BY THE
C      FAMILIAR NTU- EFFECTIVENESS RELATIONSHIP, DEPENDING
310      UPON THE VALUE OF THE CAPACITY RATIO THE EFFECTIVENESS
C      (DIMENSIONLESS) IS DEFINED BY EITHER OF THE FOLLOWING TWO
C      RELATIONSHIPS
C
C      IF (CWARA.GE.1.) GO TO 30
315
C      CAPACITY RATIO LESS THAN ONE:
C
C      EFF = RANGE/(T1 - TTD - TD)
C      CMIN=W3
C      G=1.
320      GO TO 31
C
C      CAPACITY RATIO GREATER THAN ONE:
C
325      30 EFF = CWARA*RANGE/(T1 - TTD - TD)
C      CMIN=W4*.24
C      G=CWARA
330      31 H = CWARA*RANGE/(T1-TTD - TD)
C      IDB=0
C
C      THE HEAT TRANSFER CAPACITY OF A HEAT EXCHANGER IS REP-
C      RESENTED BY THE NONDIMENSIONED NUMBER OF HEAT TRANSFER UNITS:
C      NTU. THIS PARAMETER IS DEPENDENT UPON THE FLOW ARRANGEMENTS
C      OF THE COLD AND HOT FLUIDS
335
C      COUNTER FLOW HEAT EXCHANGER ARRANGEMENT
C
340      33 IF (NTUCAL(1).EQ."COUNTER FL") CALL NUNO2P(T1,TD,TTD,CWARA,RANGE,W3
C      S ,W4,ANTU)
C
C      CROSS FLOW HEAT EXCHANGER ARRANGEMENT

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      IF(NTUCAL(1).EQ."CROSS FLOW") ANTU=-3*ALOG(1.+ALOG(1.-1/CWARA))
345      C
      C      SINGLE PASS HEAT EXCHANGER
      C
      IF (HXNP .EQ. 1. .AND. NTUCAL(1) .EQ. "TABLE") 1) CALL
      $ NTJIP (CWARA,EFF,ANTU)
350      C
      C      TWO PASS HEAT EXCHANGER
      C
      IF (HXNP .EQ. 2. .AND. NTUCAL(1) .EQ. "TABLE") 1) CALL
      $ NTJIP (CWARA,EFF,ANTU)
      22 CONTINUE
355      C
      C      HEAT EXCHANGER DIMENSIONS
      C
      C      INSIDE TUBE AREA
      AI=3.14159*DI*12./144.
360      C
      C      OUTER TUBE SURFACE AREA
      OSA=3.14159*ODL*12./144.
365      C
      C      TOTAL OUTER SURFACE AREA
      ATOT=OSA
      C
      C      HEAT EXCHANGER UNIT VOLUME
      VOLP=AI*AD*1./144.
370      C
      C      RATIO OF HEAT EXCHANGER SURFACE AREA TO VOLUME OF HEAT
      C      EXCHANGER
      ALPHA=ATOT/VOLP
      C
      C      UNIT CROSS-SECTIONAL AREA
375      C
      ACS = YW/12.0
      ACSO = 2.0*XDG/12.0
      C
      C      CROSS-SECTIONAL TUBE AREA
      ART = ODL/12.0
380      C
      ARTD = 2.0*ART
      C
      C      RATIO OF FREE AIR FLOW AREA TO TOTAL FLOW AREA
      SIGMA = (ACS - ART)/ACS
      SIGMAD = (ACSD - ARTD)/ACS
385      C
      C      THE AIR FLOW AREA (SQ FT) NORMAL TO THE DIRECTION OF AIR
      C      FLOW IS CHECKED TO DETERMINE IF IT IS A REASONABLE VALUE
      C
      IF (AFRON*SIGMA.EQ.0.0) WRITE(6,300) M,T1,RANGE,CWARA,AFRON,WLRAT
390      IF (AFRON*SIGMA.EQ.0.0) WRITE(6,301) TCOS
      IF (AFRON*SIGMA.EQ.0.0) WRITE(6,8) AFRON,SIGMA
      C
      C      THE AIR MASS FLUX IS DETERMINED FOR THE MINIMUM CROSS-
      C      SECTIONAL FLOW AREA
395      C
      GAIR= W4/(AFRON*SIGMA)
      GAIRD = W4/(AFRON*SIGMAD)
      GAIR1 = GAIR
      IF(GAIRD .GT. GAIR) GAIR1 = GAIRD

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400      IF (IHEAT .EQ. 3) GAIR1 = GAIR
      C
      C      THE AIR SIDE REYNOLDS NUMBER FOR THE MINIMUM CROSS-
      C      SECTIONAL FLOW AREA IS FOUND BASED ON THE OUTSIDE TUBE
      C      DIAMETER
405      REAIR=ODL*GAIR1/(.046*12.0)
      C
      C      THE AIR SIDE HEAT TRANSFER (BTU/HR SQ FT DEG F) COEFFICIENT
      C      AND FRICTION FACTOR IS DETERMINED
410      CALL FRICHO (FAIR,HO,ODL,XW,XD,XDG,GAIR1,IHEAT)
      C
      C      THE WIDTH (FT) OF THE HEAT EXCHANGER IS CALCULATED
      C      DEPENDING ON IF THE LENGTH OF THE HEAT EXCHANGER TUBES IS
415      FIXED OR ALLOWED TO FLOAT
      C
23      IF (FXTLNG) WIDTH=AFRONT/FIXL
      IF (.NOT.FXTLNG) WIDTH=SQRT(WLRAT*AFRONT)
      C
420      THE NUMBER OF TUBES IN WIDTH
      C
      NW=WIDTH/XW*12
      C
      C      A CHECK ON THE NUMBER OF TUBES IN WIDTH
425      IF (NW.LT.1) WRITE (6,316) AFRONT
      IF (NW.LT.1) MKTR = MKTR + 1
      IF (MKTR.GT.200) STOP "AFRONT IS BEING DRIVEN TO ZERO"
      IF (NW.LT.1) GOTO 10
      WT2=WIDTH
      NW2=NW
      C
      C      THIS IS THE START OF THE ITERATION LOOP FOR DETERMINING
      C      THE NUMBER OF TUBES IN DEPTH OF THE HEAT EXCHANGER
435      KN=0
      ZD=2.
      C
      C      WATER SIDE REYNOLDS NUMBER
440      S REWAT=.48*.W3/(3.14*1.65*DI*(ZD/HXNP)*NW)
      C
      C      WATER SIDE HEAT TRANSFER COEFFICIENT (BTU/HR SQ FT DEG F)
      C
445      DITTUS BOELTER RELATIONSHIP
      HI=.1836*(REWAT**.8)/DI
      C
      C      NUSSELT LAMINAR FLOW RELATIONSHIP
      IF (REWAT .LT. 2400.) HI = 3.66+.354/(DI/12.)
450      C
      C      CHECK ON WATER SIDE HEAT TRANSFER COEFFICIENT TO
      C      DETERMINE IF IT IS A REASONABLE VALUE
      C
455      IF (LEGVAR (HI).EQ.0) GOTO 6
      WRITE (4,903) NW,W3,DI,ZD,AAIR,VOL,AFRONT
      STOP

```

6 CONTINUE

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C
C      OVERALL HEAT TRANSFER CALCULATION BASED ON THE OUTSIDE
460 C      SURFACE AREA (BTU/HR SQ FT DEG F)
C
      REFFI = ATOT / (2.*3.14159)
      U = 1.0 / (1.0/HO +
465 S      REFF = ALOG(ODL/DI) / CONLI +
S      ATOT / (AI*HI) )
C
      AIR SIDE HEAT TRANSFER SURFACE AREA (SQ FT)
C
      AAIR=AMTU*CMIN/U
470 C
      VOLUME OF THE HEAT EXCHANGER (CU FT)
C
      VOL=AAIR/ALPHA
C
475 C      DEPTH OF THE HEAT EXCHANGER (FT)
C
      DEPTH=VOL/AFRON
C
480 C      THE NUMBER OF TUBES IN DEPTH
C
      PZD=70
      ZD=12.*DEPTH/XD
C
      CONVERGENCE CRITERION OF ITERATION LOOP
485 C
      IF (ABS(ZD-PZD)/PZD*.LT.*001) GOTO 11
C
      CHECK ON THE NUMBER OF TIMES THROUGH ITERATIVE LOOP
C
490 C
      KN=KN+1
      IF(KN.GT.70) WRITE(6,303) KN,PZD,ZD,AFRON
      IF(KN.GT.40) GOTO 10
      Z=ZD
      GOTO 5
495 C      10 KCONV=1
      LVC=M
      RETURN
C
      RESTRICTING THE NUMBER OF TUBES IN DEPTH BY EXTERNAL
500 C      VARIABLE DEEPL
C
      11 TEST = " "
      IF (DEEPL .LT. 0.0) TEST = ".GT."
      IF (DEEPL .GT. 0.0) TEST = ".LT."
505 C      IF (TEST .EQ. ".GT." .AND. ZD .GT. ABS(DEEPL)) GOTO 10
      IF (TEST .EQ. ".LT." .AND. ZD .LT. DEEPL) GOTO 10
C
      WATER SIDE FRICTION FACTOR AND PRESSURE DROP CALCULATION
      OF THE HEAT EXCHANGER
510 C
      GWAT = HXNP * 576. * W3 / (3.14159*DI*DI*ZD*VW)
C
      VELOCITY OF WATER THROUGH THE TUBES

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515      C      VWAT=GWAT/(62.*3600.)
      C
      C      HEAT EXCHANGER TUBE LENGTH
      C
      C      IF(FXTLNG) ELENG=FIXL
520      C      IF(.NOT.FXTLNG) ELENG=WIDTH/WLRAT
      C
      C      WATER SIDE FRICTION FACTOR
      C
      C      IF(REWAT.GT.2000.) GO TO 12
525      C      FWAT=16./REWAT
      C      GO TO 14
      C      12 IF(REWAT.GT.1.E5) GO TO 13
      C      FWAT=.0791/(REWAT**.25)
      C      GO TO 14
530      C      13 FWAT=.046/(REWAT**.2)
      C
      C      WATER SIDE PRESSURE DROP THROUGH THE HEAT EXCHANGER
      C
535      C      14 DELPWT = HXNP * 48. * FWAT * ELENG * (GWAT/3500.)**.2 /
      C      3 (DI * 62. * 64.4)
      C      AIRFF = FAIR
      C      WATFF = FWAT
      C
      C      CONDENSER DESIGN
540      C
      C      CALLI SPDES(TD,T1,RANGE,TTD,XNS,PREJ,VELD,RHO,ARPS,TLA,XNTS,HDLQS)
      C      DELPWC=HDLQS*62.
      C
      C      COSTING OF THE HEAT EXCHANGER SURFACE AND HEADERS
545      C
      C      CALLI COSTEX(ATOT)
      C
      C      FAN SYSTEM DESIGN
550      C
      C      T4=CWAPA*RANGE+TD
      C      BARLN=3.39953-3.81835E-5*ELEV
      C      BAR=EXP(BARLN)
      C
      C      SPECIFIC VOLUME OF AIR FOR THE INLET TO THE HEAT EX-
555      C      CHANGER BUNDLE AND THE EXIT OF THE FAN (CU FT/LBM)
      C
      C      SPVOL=(T4+459.67)/1.325/BAR
      C      VAIN= (TD+459.67)/(1.325*BAR)
      C      VAOUT= (T4+459.67)/(1.325*BAR)
      C      VAAV=(VAIN+VAOUT)/2.
560      C      VAIR=GAIR1*VAAV/3600.
      C
      C      AIR SIDE PRESSURE DROP THROUGH THE HEAT EXCHANGER
      C
      C      DELPA = (GAIR1/3600.)**.2 * Z * (4.*FAIR) * VAAV/64.4
      C      DPTPSF=DELPW
565      C      OPTINW = DPTPSF/ 5.2022
      C      IF((OPTINW*.07495*SPVOL).GT.1.35) RETURN
      C
      C      DESIGN AND COST OF THE FAN SYSTEM
570      C
      C      CALLI FAN (OPTINW)

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C      AFC GREATER THAN .49E+9 MEANS NO SUITABLE FAN WAS FOUND BY
C      SUBROUTINE FAN. SET TCOS TO HIGH VALUE TO THROW OUT THIS
C      POINT IN THE SEARCH FOR A MINIMUM
575      IF( AFC .GT. .49E+9) TCOS = 1.E+38
C      IF( AFC .GT. .49E+9) RETURN
C
C      DESIGN AND COST OF THE WATER PIPING SYSTEM
580      CALL PIPORT(T1, W3, TTD, RANGE, CTOWD, DELPWT, DELPWC, DIST
S          .DESVEL, REDUCE, QREDUCE, WB, ZD, XW, TCWFCS, NUMTOW
S          .DELPWP, EPDP, HPWAT, RHO, CDANG, POHCIR, POHLEC, EFPF)
C      DELPW = DELPWT + DELPWC + DELPIP
C      IF(TCWFCS .GT. 1.E+39) TCOS = 1.E+38
585      IF(TCWFCS .GT. 1.E+39) RETURN
C      PPON=HPWAT/(1.341*EFPF)
C
C      SCALING UP THE POWER PLANT AND THE DRY COOLING TOWER TO
C      MEET THE POWER REQUIREMENTS OF THE FAN AND PIPING SYSTEMS
590      CALL SCALP(RANGE, CWARA, AFRON, WLRAT, TCWFCS, NUMTOW)
C
C      DETERMINE THE INCREASED COST OF PRODUCING ELECTRICAL
C      POWER FROM POWER PLANT USING A DRY COOLING TOWER AS THE HEAT
C      REJECTION SYSTEM
595      CALL NOVART(CWARA,TCOS)
C      LVC=M
C      RETURN
600      END

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SUBROUTINE CHNGE(M)

THIS ROUTINE IS CALLED BY SUBROUTINE SERCH WHEN PRESSURE DROP RESTRICTION IS ENCOUNTERED. IT SEARCHES BY CHANGING A VARIABLE OTHER THAN THAT SELECTED BY SUBROUTINE SERCH.

LOGICAL FXTLNG

DIMENSION DP(5), DV(5), VAJ(5)

COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,

\$ GAIR, FAIR, HPAIR, HPWAT, PLANC1

LOGICAL FIRST, FXTMP

COMMON

\$ AFTR, ALPHA

\$ CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAFI

\$ CRU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILS, CVM

\$ DEEPI, DESVEL, DANGLE

\$ EFFF

\$ FCP, FIRST, FIXL, FCOS, FXTMP

\$ GBEFF

\$ HXNP, HPCST

\$ IHEAT

\$ ITMAX, ITMIN

\$ JCONS

\$ KCONV, KALEXT

\$ MXEXT

\$ NTUCAL(2), NTA

COMMON

\$ ODR

\$ PSIZE, PER, PWCOS, PLANC, PFACT

\$ POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCU

\$ QREJ, QREDUCE

\$ RBP, REDUCE, ROESEL, ROEELA, ROOFL, RFX

\$ SAAF, SIGMA, SPAMAT(2)

\$ TD, TPO(4), TEFF, TLJM, TLPRA, TSEALP, TELAST, THFIN, TFIX

\$ TUBAGG, TW

\$ UCS, UWS

\$ VAS(5)

\$ WFFV

\$ XDEPA, XW, XD

COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF

\$ CLAND, REAIR, Z, HRFAC2, W4, U, PPOW

\$ FPOW, DELFC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4

\$ REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3

\$ SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPC5, PSIZ13, WT2

\$ CP2, NWE, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELDX

\$ TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS

\$ CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPIP, AST

\$ CAPCST, XNFAN, BLDANG, CPLEN, DPFL, WHX, WTTUB, ADIA, ABLN

\$ WTHDR, WTFRM, STRUCC, CPERF, HPPERF, TOTCF, EFFIN, ANTU

\$ AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTTR, ADJTR

\$ ACTBDD, ADJBDP, ACTVH, ADJVVH, ADJPPF, HPAIR, TCTF, AFCST

\$ CSPD, WATERW, WSTRCT, CFOUNO, HUBDIA, TOWLEN, CSE, CHF

\$ CRA, NUMTOW, CTOWD, ATUBC, CSTLYR, CSTHS, CYLRNG, CFANEL

COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1

\$ CLAN1, REAI1, Z1, HRFAC2S, W41, U1, PPOW1

\$ FPOW1, DELFC1, WIDTH1, ELENG1, VAIR1, VWAT1, HI1, HO1, T41

\$ REW41, NW1, ZPLNC2, ZSIZ12, ZSPBP, SW41, SW31

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      SPC1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
      S, R22MIN, NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONBA1, XNTS1, VELD1
60    S, TLA1, UCON1, FMCS1, FBAC1, EFFC1, CH1, CA1, CSI
      S, CLTC1, CFC1, CPCC1, FITC1, CSC1, CEPRE1, DEPI1, AST1
      S, CAPCS1, XNFAN1, BLDAN1, CPLEN1, DPFE1, WH1, WTTU1, ADI1, ABL1
      S, WTH1, WTRF1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
65    S, AIRFF1, WATFF1, XNOD1, TCTP1, FDCPF1, FMTRC1, ACTTP1, ADJTP1
      S, ACTB1, ADJRP1, ACTVH1, ADJVH1, ADJPP1, THPA1, TCTF1, AFCST1
      S, CS1, WATER1, WSTRC1, CFOUN1, HUBD1, TOWLE1, CSE1, CHF1
      S, CBAL, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFAVE1
      COMMON /FLSW/ FXTLNG
      COMMON /LACALL/ SRN
70    COMMON /TINE/ XNS, TTD, TLA, XNTS, ARPS
      L=0
      KI=0
      DO 1 I=1,3
1    DV(I)=.05
75    DO 2 I=1,2
      2 DV(I+3)=.2
      DO 3 I=1,5
      VAJ(I)=VAR(I)
80    3 VAL(I)=VAR(I)
      4 VAL(M)=(1.+DV(M))*VAR(M)
      IF(FXTMP) VAL(1) = TFIX
      IF(FXTMP) VAL(2) = RFIX
      IF(VAL(1).LE.0.0) GO TO 36
      IF(M.GT.3) GO TO 10
85    IF(VAL(1).LE.0.0) GOTO 36
      H = VAL(3)*VAJ(2)/(VAJ(1)-TTD-TD)
41    IF(M.GT.1) GO TO 36
      IF(ALOG(1.-H)/VAL(3).LE.-1.) GO TO 36
10    SRN="/CHNGE-1/"
90    CALL CALC(VAL(1),VAL(2),VAL(3),VAL(4),VAL(5),1)
      IF(KO.V.EQ.1) GO TO 36
      PA=DELP
      PA1=DEPA1
      DP(M)=DELP-DEPA1
95    IIB=1
      IF(FXTLNG) IIB=2
      DO 35 II=IIB*5
      I=6-II
      IF(I.EQ.5.AND.DV(1).GT..005) GO TO 35
100    IF(I.EQ.M) GO TO 35
      11 VAL(I)=(1.-DV(I))*VAR(I)
      IF(VAL(I).LE.0.0) GO TO 34
      VAJ(I)=VAL(I)
105    IF(FXTMP) VAJ(1) = TFIX
      IF(FXTMP) VAJ(2) = RFIX
      IF(I.GT.3) GO TO 17
      IF(VAJ(1).LE.0.0) GOTO 12
      H = VAL(3)*VAJ(2)/(VAJ(1)-TTD-TD)
110    43 IF(M.GT.1) GO TO 12
      IF(ALOG(1.-H)/VAJ(3).LE.-1.) GO TO 12
      GO TO 17
      12 VAJ(I)=VAR(I)
      GO TO 34
      17 J=I

```

```

115 IF (M.LT.1) J=M
    SRN="/CHNGE-2/"
    CALL CALC(VAJ(1),VAJ(2),VAJ(3),VAJ(4),VAJ(5),J)
    VAJ(I)=VAR(I)
    IF (KCONV.EQ.1) GO TO 34
120 PA=DELP
    PA1=DEPA1
    DP(I)=DELP-DEPA1
    E=0.
    C=1.
    D=1.
125 18 VAL(I)=(1.+DV(I))*(E-DP(M))/DP(I)*VAR(I)
    IF (EXT=MP) VAL(1) = TFIX
    IF (EXT=MP) VAL(2) = RFIX
    IF (VAL(I).LE.0.0) GO TO 34
    IF (I.GT.3) GO TO 24
    IF (VAL(1).LE.0.0) GOTO 34
    H = VAL(3)*VAL(2)/(VAL(1)-TTD-TD)
45 IF (H.GE.1.) GO TO 34
    IF (ALOG(1.-H)/VAL(3).LE.-1.) GO TO 34.
135 24 SRN="/CHNGE-3/"
    CALL CALC(VAL(1),VAL(2),VAL(3),VAL(4),VAL(5),J)
    IF (KCONV.EQ.1) GO TO 34
    IF (DELP.GE.XDEPA.AND.DELP.LE.1.01*XDEPA) GO TO 26
    IF (DELP.GE.1.01*XDEPA) GO TO 25:
140 C=D/10
    IF (C.LT..001) GO TO 34
    E=E+C
    GO TO 18
145 25 D=C/10.
    IF (D.LT..001) GO TO 34
    E=E-D
    GO TO 18
26 IF (TCOS.GE.TCOS1) GO TO 34
    CALL STORE
150 L=1
    DO 27 IJ=1,5
27 VAJ(IJ)=VAR(IJ)
    VAL(M)=(1.+DV(M))*VAR(M)
    IF (EXT=MP) VAL(1) = TFIX
155 IF (EXT=MP) VAL(2) = RFIX
    IF (VAL(M).LE.0.0) GO TO 36
    IF (M.GT.3) GO TO 33
    IF (VAL(1).GE.170..OR.VAL(1).LT.110.) GO TO 36
    H = VAL(3)*VAL(2)/(VAL(1)-TTD-TD)
160 47 IF (H.GE.1.) GO TO 36
    IF (ALOG(1.-H)/VAL(3).LE.-1.) GO TO 36
33 SRN="/CHNGE-4/"
    CALL CALC(VAL(1),VAL(2),VAL(3),VAL(4),VAL(5),M)
    IF (KCONV.EQ.1) GO TO 36
165 PA1=DEPA1
    PA=DELP
    DP(M)=DELP-DEPA1
    GO TO 11
170 34 VAL(I)=VAR(I)
35 CONTINUE
36 DO 37 I=1,5

```

SUBROUTINE CHNGE

74/74 OPT=1

FTN 4.2+74351

12/20/66

175 37 DV(I)=DV(I)
K1=K1+1
IF(K1=Q.1) GO TO 4
K1=0
IF(DV(I).LE.,005) GO TO 39
DO 38 I=1,5
38 DV(I)=DV(I)/5.
GO TO 4
180 39 RETURN
END

SUBROUTINE COSTEX(ATOT)

```

C
C
C      SUBROUTINE COSTEX DETERMINES THE COST OF THE HEAT EXCHANGER
5  C      BUNDLES OF THE DRY COOLING TOWERS. THE COST OF THE HEAT
C      EXCHANGER BUNDLE IS BROKEN DOWN INTO SEVERAL SUBCOMPONENTS
C      1. HEADER
C      2. TUBING
C      3. TUBING SEALANT
C      4. SPACERS
10 C      5. BUNDLE FRAME
C      6. BUNDLE ASSEMBLY
C      THE WEIGHT OF THE HEAT EXCHANGER BUNDLE AND THE WATER ARE
C      ALSO CALCULATED.
C
15 C      DEFINITION OF VARIABLES
C      ABC      - HOLE FACTOR FOR THE HEADER COSTS (DIMENSIONLESS)
C      AT       - CROSS-SECTIONAL AREA OF THE TUBE (SQ IN)
C      BSECF    - BUNDLE SHIPPING AND ERECTION FACTOR OF THE HEAT
C                EXCHANGER (DECIMAL)
20 C      CA      - BUNDLE ASSEMBLY AND FRAME COSTS ($)
C      CRA      - BUNDLE ASSEMBLY COST ($)
C      CBJ      - COST OF BOLTED HEADER JOINT ($/FT)
C      CELAST   - COST OF THE ELASTOMER ($/LBF)
C      CEPREP   - COST OF END PREPARATION FOR EACH TUBE ($/TUBE)
25 C      CFS     - UNIT FRAME COSTS ($/LBF)
C      CH       - COST OF THE HEADER FOR EACH BUNDLE
C      CHC      - STEEL HEADER COSTS ($/LBF)
C      CHF      - BUNDLE FRAME COST ($)
C      CHX      - COST OF THE HEAT EXCHANGER ($)
30 C      CP      - UNIT PLASTIC COSTS ($/LBF)
C      CS       - COOLING SURFACE COST ($)
C      CSC     - TUBE SPACER COSTS ($/TUBE-SPACER)
C      CSE      - COST OF SEALING PLATE AND SEALANT ($)
C      CSEALP   - COST OF SEAL PLATE ($/LBF)
35 C      DI      - INSIDE DIAMETER OF TUBE (IN)
C      ELENGL   - LENGTH OF THE HEAT EXCHANGER TUBES (FT)
C      FA       - TOTAL TUBE FLOW AREA PER PASS SQ (IN)
C      FACT     - HEADER FACTOR WHICH DEPENDS ON THE TYPE OF HEADER
C                (DIMENSIONLESS)
40 C      FITCO   - TUBING COST ($/FT)
C      FP       - PRESSURE FACTOR (DIMENSIONLESS)
C      FI       - HEADER DEPTH MATERIAL FACTOR (IN)
C      F2       - HEADER WIDTH MATERIAL FACTOR (IN)
C      Hd       - HEADER DEPTH PER PASS (IN)
45 C      HEDMAT  - TYPE OF HEADER MATERIAL (DIMENSIONLESS)
C      HEDTUB   - NUMBER OF TUBES PER HEADER
C      HEDTYP   - TYPE OF HEADER
C      HEDVOL   - HEADER VOLUME (CU FT)
C      HW       - HEADER WIDTH (IN)
50 C      HXNP    - NUMBER OF PASSES THROUGH THE HEAT EXCHANGER
C                (DIMENSIONLESS)
C      NW       - NUMBER OF HEAT EXCHANGER TUBES IN WIDTH
C                (DIMENSIONLESS)
C      ODL      - OUTSIDE DIAMETER OF TUBE (IN)
55 C      PCF     - PROCUREMENT COST FACTOR (DECIMAL)
C      POHBARI  - INDIRECT CONSTRUCTION COST FOR HEAT EXCHANGER
C                BUNDLE (DECIMAL)

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60	ROEEL	- DENSITY OF THE SEALING ELASTOMER (LBM/CU IN)
	ROEL	- TUBING MATERIAL DENSITY (LBM/CU IN)
	ROESEL	- DENSITY OF STEEL SEALER PLATE (LBM/CU IN)
	SPAMA	- SPACER MATERIAL (DIMENSIONLESS)
	SS	- SPACING BETWEEN SPACERS (FT)
	TELAST	- THICKNESS OF ELASTOMER LAYER (IN)
	TS	- THICKNESS OF SPACER MATERIAL (IN)
65	TUBVOL	- VOLUME OF WATER INSIDE THE TUBES (CU FT)
	TH	- THICKNESS OF THE HEADER WALLS (IN)
	WATERW	- TOTAL WEIGHT OF THE WATER IN THE HEAT EXCHANGER BUNDLE (LBF)
	Wb	- WIDTH OF THE HEAT EXCHANGER BUNDLE (F)
70	WHX	- WEIGHT OF MATERIAL MAKING UP THE EXCHANGER (LBF)
	WI	- WEIGHT OF MATERIAL IN THE HEAT EXCHANGER (LBF)
	WTFRM	- WEIGHT OF THE HEAT EXCHANGER FRAME (LBF)
	WTHDR	- WEIGHT OF THE HEAT EXCHANGER HEADER (LBF)
	WTUB	- WEIGHT OF THE TUBES IN THE HEAT EXCHANGER (LBF)
75	XD	- LONGITUDINAL TUBE SPACING BETWEEN TUBE ROWS (IN)
	XBUN	- NUMBER OF HEAT EXCHANGER BUNDLES (DIMENSIONLESS)
	XW	- TRANSVERSE TUBE PITCH NORMAL TO AIR FLOW (IN)
	Z	- NUMBER OF HEAT EXCHANGER TUBES IN DEPTH (DIMENSIONLESS)
80	ARRAYS	
	TUBMA	- LINER MATERIAL
	CL	- LINER FIXED COSTS (\$)
85	CLM	- LINER MATERIAL COSTS (\$/LB)
	ROEL	- DENSITY OF LINER MATERIALS (LB/CU IN)
	GIGLI	- LINER GAGE
	THKLIN	- THICKNESS OF LINER (IN)
	FINTY	- TYPE OF FIN
	CFM	- FIN MATERIAL COSTS (\$/LB)
90	CF	- FINNING FIXED COSTS (\$/FT)
	ONLINE	- COMMON DIAMETERS OF LINER (IN)
	MAXFH	- MAXIMUM FIN HEIGHT (IN)
	STANFT	- STANDARD FIN THICKNESS (IN)
	FPL	- LOWEST FIN PITCH (FPI)
95	FPH	- HIGHEST FIN PITCH (FPI)
	HEDTY	- TYPE OF HEADER
	HEDMA	- HEADER MATERIAL
	ROEHM	- HEADER MATERIAL DENSITY (LB/CU IN)
	CHM	- COST OF HEADER MATERIAL (\$/LB)
100	CHW	- COST OF HEADER MACHINING AND WELDING (\$/FT)
	CH	- NOZZEL AND ATTACHING COST (\$/HOLE)
	CHH	- TUBE AND PLUGHOLE PREPARATION (\$/HOLE)
	FE	- COST LENGTH FACTOR FOR TUBES (DIMENSIONLESS)
	FINMA	- TYPE OF FIN MATERIAL
105	FPL	- LOWER LIMIT ON STANDARD FIN PITCHES THAT ARE COMMERCIALY AVAILABLE (FINS/IN)
	FPH	- UPPER LIMIT ON STANDARD FIN PITCHES THAT ARE COMMERCIALY AVAILABLE (FINS/IN)
	MAXFH	- MAXIMUM FIN HEIGHT FOUND COMMERCIALY (IN)
110	ROEF	- DENSITY OF FIN MATERIAL (LBM/CU IN)
	STANFT	- FIN THICKNESS LIMITS FOUND COMMERCIALY (IN)
	REALINTUB	

```

115 LOGICAL FIRST, FXTMP
COMMON
$ AFTR, ALPHA
$ ,CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAP1
120 $ ,CRJ, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILE, CVM
$ ,DEEPL, DESVEL, DANCE
$ ,EFFP
$ ,FCR, FIRST, FIXL, FCOS, FXTMP1
$ ,GBEFF
125 $ ,HXVP, HPCST
$ ,IHEAT
$ ,ITHAY, ITMIN
$ ,JCONC
$ ,KCONV, KALEXT
$ ,MXEXT
130 $ ,NTUCAL(2), NTA
COMMON
$ ODR
$ ,PSIZE, PER, PWCOS, PLANC, PFACT
$ ,POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSLI
135 $ ,QREJ, QREDUCE
$ ,R3D, REDUCE, ROESEL, ROELA, ROOFL, RFIX
$ ,SAAF, SIGMA, SPAMAT(2)
$ ,TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
140 $ ,TUBANG, TW
$ ,UCS, UWS
$ ,VAS(4)
$ ,W=V
$ ,XDEPA, XW, XD
COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF1
145 $ , CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,
$ , FPOW, DELFC, WIDTH, ELENG, VAIR, VWHAT, HI, HO, T4,
$ , REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3,
$ , SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
$ , BP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELDX
150 $ , TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
$ , CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPIP, AST
$ ,CAPCST, XNFAN, BLDANG, CPLEN, DPTEL, WHX, WTTUB, ADIA, ABLN1
$ , WTHR, WTERM, STRJCC, CPERF, HPPERF, TOTCF, EFFIN, ANTU
155 $ , AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCITP, ADJTP
$ , ACTBD, ADJBPD, ACTVH, ADUVH, ADJPPF, THPAIR, TCTF, AFCST
$ , CSRD, WATERW, WSTRCT, CFQUND, HUBDIA, TOWLEN, CSE, CHF
$ ,CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
COMMON /DJB/ DI, XDG, SF
COMMON /PLCOST/ WPL
160 COMMON /ESCAL/ BSECF
COMMON /SEALER/ HRFAC1, SSCD, PLANC1, CASSS1,
$ GAIR, FAIR, HPAIR, HPMAT, PLANCT1
COMMON /HEADX/ CHH, CN, CHM, CMW, CRJ, CWJ, CST, CMO, CSR, CSM, PITCHF, CPM,
165 IPRESS, HEDMAT, HEDTYP, NPASS, WB
COMMON /SURFEX/ ODL, GAGLIN, NTUB, TUBMAT, FINTP, FINMAT, CFB, APLATE,
$ COATC, ZINCC, CASTC, SS, EPREPC, XTUBMA, XHEDTY, XPINTY
COMMON /RORT3/ TUBCST, SHLCST, FETCST, CHX
C
170 DIMENSION TUBMA(2), CL(2), CLM(2), ROEL(2)
DIMENSION HEDTY(4), HEDMA(3), ROEHM(3), CHC(4), CHMAT(3)
DIMENSION ROES(2), SPAMA(2), CP(2)

```

```

C
C
C
C      TABLE I
175 C      LINER TUBING COSTS AND DENSITY
C
C      DATA CL /0.0, 0.002/
C      DATA CLM /0.72, 0.775/
C      DATA ROEL /0.035, 0.033/
180 C      DATA CD /1.10, 2.20/
C      DATA ROES /0.044, 0.0314/
C      DATA TUBMA/ "POLYETHYLEN", "POLYPROPYLEN"/
C      DATA SPAMA /"POLYVINYLEN", "POLYCARBON"/

C
C      TABLE II
185 C      HEADER FABRICATION COSTS
C
C      DATA HEDTY / "WELD REMOV", "WELD PLUG ", "FORM REMOV",
C      "FORM PLUG " /
190 C      DATA (MEDMA(I), I=1, 3)/ "STEEL", "ALUMINUM", "GALVANIZED"/
C      DATA ROEHM / .284, .09751, .284/
C      DATA CONAT / .53, 1.3, .57/
C      DATA CHC / 1.05, 1.00, 0.95, 0.90 /

C
C      DEFINING THE CASE UNDER CONSIDERATION
195 C
C      IF (.NOT. FIRST) GOTO 55
C      LFLAG=0
C      DO 10 I=1, 4
200 C      ITUBMA = I
C      IF (ITUBMAT .EQ. TUBMA(I)) GO TO 25
10 CONTINUE
C      PRINT 11
C      LFLAG=1
205 C      11 FORMAT(5X, "NO MATCH FOR LINER MATERIAL")
25 DO 30 I=1, 2
C      ISPAMA = I
C      IF (SPAMAT(I) .EQ. SPAMA(I)) GOTO 45
30 CONTINUE
210 C      PRINT 31
C      LFLAG = 1
31 FORMAT(5X, "NO MATCH FOR SPACER MATERIAL")
45 CONTINUE
C      IF (LFLAG.NE.0) STOP
215 C      55 CONTINUE
C      IF (FIRST) GOTO 125

C
C      LINER TUBING COSTS
220 C
C      WL = 37.69911*ROEL(ITUBMA)*(ODL**2.0 - DI**2.0)/4.0
C      CLTC = (CLM(ITUBMA) * WL + CL(ITUBMA))
C      PCF = 1.10
C      CLTC = CLTC*PCF
C      FITCO = CLTC

225 C
C      TUBE SPACER COSTS
C
C      TS = .364

```

```

230      HD = XN * (Z/HXNP) + 1.0
      AT = 3.14159 * ODL * ODL / 4.
      CSC = CP(ISPAMA) * (XW * HXNP * HD/Z - AT) * TS * ROES(ISPAMA)
      C
      C      END PREPARATION COST
      C
235      CEPREP = EPREPC
      C
      C      COOLING SURFACE COST
      C
      CS = Z * NW * (FITCO * ELENG + CSC * ((ELENG * 5 * SS) / SS) + CEPREP)
240      CS = CS * POHBAF
      C
      C
      C      DEFINING THE CASE FOR THE HEADER
245      IF (.NOT. FIRST) GOTO 145
      DO 130 I=1,4
      IHEDTY = I
      IF (HEDTYP.EQ. HEDTY(I)) GO TO 135
      130 CONTINUE
      PRINT 131
      STOP
      131 FORMAT(5X,"NO MATCH FOR HEADER TYPE")
      135 DO 140 I=1,3
      IHEDMA=I
      IF (HEDMAT.EQ. HEDMA(I)) GOTO 142
      140 CONTINUE
      PRINT 141
      STOP
      141 FORMAT(5X,"NO MATCH FOR HEADER MATERIAL")
250      142 FIRST=.FALSE.
      RETURN
      C
      C      HEADER AND NOZZEL COSTS
      C
265      145 CONTINUE
      C
      C      NUMBER OF BUNDLES IN COOLING TOWERS
      XNRJN = NW * XW / (12.0 * WB)
      XNMDO = XNRJN / 8.0
270      C
      C      NUMBER OF TUBES PER BUNDLE
      HEDTUB = 12. * Z * WB / XW
      ABC=1.0
      IF (IHEDTY.EQ.2.OR.IHEDTY.EQ.4) ABC=2.0
275      FP=1.00
      FA = .785398 * DI * DI * HEDTUB / HXNP
      C
      C      HEADER DEPTH AND WIDTH
      HD = XN * (Z/HXNP) + 1.0
      HW = FA / (2.0 * HD) + 2.0
      F1 = 2.0 * HXNP * HXNP * HD / 10.0
      F2 = 2.0 * HXNP * FA / (20.0 * HD)
      IF (IHEDTY.EQ.1.OR.IHEDTY.EQ.2) FACT=2.*F1+.4.
      IF (IHEDTY.EQ.3.OR.IHEDTY.EQ.4) FACT=2.*F1
285      C

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C      HEADER COSTS
      CHM= CHMAT(IHEDMA)
      CH=(CHM*ROEHM(IHEDMA))*(12.*WB*TW*(2.*F1*HD+(F2+2.)*HW)+F1*FA*
290 $ TW)+CMW*(FACT*WB+(4.0*F1*HD+2.0*(F2+2.0)*HW)/12.0)+
      $ 4.0*CBJ*(HXNP*HD/12.+WB)+
      1CHH*(24.0*480*Z*WB/XW)+4.0*CN*SQR(FA/3.14159))*XNBUN*FP
      CH=CH*POHBAF
      IF(WB.GT.14.0) PRINT 150
295 150 FORMAT(5X,"THE SPECIFIED HEADER LENGTH IS BEYOND THE PRACTICAL LIM
      +IT")

C      COST OF HEADER SEALANT
      CSE = 2. * (CSEALP * ROESEL * TSEALP * 12. * WB * HXNP * HD
300 $ + CELAST * ROEELA * TELAST * (12. * WB * HXNP * HD + HEDTUB
      $ * AT)) * XNBUN
      CSE = CSE * POHBAF

C      BUNDLE ASSEMBLY AND FRAME COSTS

C      BUNDLE FRAME COST
      CVF = CFS*ELENG*(86.0 + 2.0*WB)*XNBUN
      CVF = CVF * POHBAF
      CHF = CVF

C      BUNDLE ASSEMBLY COST
      CBA = (1150. * SQR(Z*ELENG)/42. + 650. * SQR(ELENG)/9.5
310 $ + 400. * SQR(WB) / 3.5 + 500.) * XNBUN
      CBA = CBA * POHBAF
      CA = CVF + CBA

C      WEIGHT OF HEAT EXCHANGER

C      TUBE MATERIAL WEIGHT OF COOLING TOWERS
      WTTUB = Z * NW * ELENG * WL

320 C      HEADER MATERIAL WEIGHT OF COOLING TOWERS
      WTHDR = ROEHM(IHEDMA) * (12.*WB*TW * (2.*F1*HD+(F2+2.)*HW)+
      $ F1*FA*TW) * XNBUN

C      TOTAL FRAME WEIGHT
      WTFRM = 20.0 * ELENG * (2.*WB/(2.*SS)) * SQR(Z/6.)*XNBUN

325 C      TOTAL WEIGHT OF WATER IN HEAT EXCHANGER
      TURVOL = Z*NW*ELENG*3.14159*DI*DI/(144.0*4.0)
      HEDVOL = 2.0 * HXNP * HD * HW * WB / 144. * XNBUN
      WATERW = (TURVOL + HEDVOL)*62.4

C      TOTAL MATERIAL WEIGHT OF HEAT EXCHANGER
      WHX = WTTUB + WTHDR + WTFRM

335 C      TOTAL HEAT EXCHANGER COSTS
      BSECF = 1.12
      CHX = BSECF * (CS + CH + CA + CSE)
      RETURN
      END
340

```

SUBROUTINE FAN (OPTINW)

```

C
C
C      SUBROUTINE FAN SELECTS THE OPTIMUM FAN SYSTEM FOR THE PARTIC-
5      C      ULAR HEAT EXCHANGER GEOMETRY SELECTED. FOR THE PARTICULAR
C      FAN SYSTEM THE FOLLOWING PARAMETER ARE SPECIFIED-
C          1. BLADE DIAMETER
C          2. HUB DIAMETER
C          3. NUMBER OF BLADES PER FAN
C          4. BLADE ANGLE
10     C      KNOWING THE NUMBER OF FANS AND THE PACKING FACTOR OF THE
C      FANS, THE CIRCULAR TOWER DIAMETER CAN EASILY BE
C      DETERMINED. THE COST OF THE FAN SYSTEM IS THEN FOUND. THE
C      FAN SYSTEM RESULTING IN THE MINIMUM COST IS SPECIFIED AS THE
C      OPTIMUM.
15     C      IN THIS SUBROUTINE THERE ARE TWO ARRAYS WHICH CONTAIN DATA
C      FOR THE FOLLOWING FAN DIAMETERS (24,26,28,30,40,60). FOR
C      EACH FAN DIAMETER THERE IS PERFORMANCE DATA FOR FANS WITH
C      DIFFERENT NUMBER OF BLADES AND BLADE ANGLES. THE DATA
C      ARRAYS FANDAP CONTAINS THE FOLLOWING INFORMATION-
20     C      FANDAP(I,J)
C      J=1,5 - COEFFICIENTS FOR THIRD ORDER CURVE FIT OF VOLUM-
C              METRIC FLOW RATE VERSUS TOTAL PRESSURE DROP ACROSS
C              THE FAN
C      J=6 - LOWER PRESSURE DROP LIMIT (IN WATER)
25     C      J=7 - UPPER PRESSURE DROP LIMIT (IN WATER)
C      J=8 - DIAMETER OF FAN (FT)
C      J=9 - NUMBER OF BLADES PER FAN
C      J=10 - BLADE ANGLE (DEGREES)
C      I=1,153 - DIFFERENT SETS OF DATA FOR EACH FAN AND
30     C      PERFORMANCE POINT
C      THE DATA ARRAY FANDAH CONTAINS THE FOLLOWING INFORMATION-
C      FANDAH (I,J)
C      J=1,5 - COEFFICIENTS FOR FOURTH ORDER CURVE FIT OF
C              HORSEPOWER VERSUS VOLUMETRIC FLOW RATE
35     C      J=6 - LOWER LIMIT ON VOLUMETRIC FLOW RATE OF AIR THROUGH
C              THE FAN FOR WHICH DATA IS AVAILABLE
C      J=7 - UPPER LIMIT ON VOLUMETRIC FLOW RATE OF AIR THROUGH
C              THE FAN FOR WHICH DATA IS AVAILABLE
C      J=8 - DIAMETER OF FAN (FT)
40     C      J=9 - NUMBER OF BLADES PER FAN
C      J=10 - BLADE ANGLE (DEGREES)
C
C      DEFINITION OF VARIABLES
C      A - AIR FLOW AREA OF THE FAN (SQ FT)
45     C      APLN - NUMBER OF FAN BLADES (DIMENSIONLESS)
C      ADIA - FAN DIAMETER (FT)
C      ANFCOS - ANNUAL FAN COSTS ($)
C      ANSFPC - ANNUAL CAPITAL COST OF PLENUM, FOUNDATION, AND
50     C      STRUCTURES ($)
C      ANSEPF - TOTAL ANNUAL COST OF THE FAN SYSTEM AND STRUCTURE
C      BAR - BAROMETRIC PRESSURE (IN HGA)
C      BLDANG - FAN BLADE ANGLE (DEGREES)
C      CAPF - PERCENTAGE OF TIME THE PLANT IS PRODUCING POWER
55     C      (PERCENT)
C      CDANG - COSINE OF THE ANGLE FOR THE DELTA HEAT EXCHANGER
C              ARRANGEMENT (DIMENSIONLESS)
C      CFM - ESTIMATE OF THE VOLUMETRIC FLOW RATE OF AIR THROUGH

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C      EACH FAN (CU FT/MIN)
60  C      CFROS - FAN STACK COSTS WITH AND WITHOUT VELOCITY RECOVERY
C          ($)
C      CT - CONVERGENCE PARAMETER FOR THE VOLUMETRIC FLOW RATE
C          THROUGH EACH FAN (DIMENSIONLESS)
C      CINC - INCREMENTAL VOLUMETRIC FLOW RATE OF AIR USED IN
C          DETERMINING THE FAN PERFORMANCE POINT (CU FT/MIN)
65  C      CMOT - COST OF FAN MOTORS PER FAN ($)
C      CPL - COST OF PLENUM FOR THE ENTIRE TOWER SYSTEM ($)
C      CPM - COST OF PLENUM MATERIAL ($/LBM)
C      CSR - COST OF THE SPEED REDUCER ($)
C      CVM - FAN RING MATERIAL UNIT COST ($/LBF)
70  C      DIST - DISTANCE FROM THE CONDENSER ROOM TO THE FIRST
C          CIRCULAR TOWER (FT)
C      DPTINW - PRESSURE DROP ACROSS THE HEAT EXCHANGER (IN H2O)
C      DSSTM - DISTANCE FROM THE SWITCH GEAR TO THE MOTOR (FT)
C      DTOW - DIAMETER OF THE CIRCULAR TOWERS (FT)
75  C      DITSG - DISTANCE FROM THE TOWER TO THE SWITCH GEAR (FT)
C      EFCSF - ESCALATION FACTOR FOR FAN COST (DIMENSIONLESS)
C      EHR - HEAT RATE OF PLANT (BTU/KW-HR)
C      ELENG - LENGTH OF HEAT EXCHANGER TUBES (FT)
C      ELEV - PLANT ELEVATION FROM SEA LEVEL (FT)
80  C      FMAD - FAN DIAMETER (FT)
C      FANLEC - ELECTRICAL WIRING COSTS FOR THE FAN SYSTEM ($)
C      FCS - PLANT FUEL COST (CENTS/MMBTU)
C      FCR - FIXED CHARGE RATE ON CAPITAL FOR ONE
C          YEAR (FRACTIONAL)
85  C      FOST - CAPITAL COST OF THE FAN ($)
C      FMC - FAN MOTOR COST PER HORSEPOWER FOR MOTORS OF SMALL
C          HORSEPOWER ($/HP)
C      FNDCT - FOUNDATION COSTS FOR THE CIRCULAR TOWERS ($)
C      FROW - POWER REQUIREMENTS OF THE FAN SYSTEM (KW)
90  C      GREFF - GEAR BOX EFFICIENCY OF THE FAN SYSTEM (PERCENT)
C      H2 -
C      HFR - HEIGHT OF THE FAN RING (FT)
C      HPAIR - HORSEPOWER REQUIREMENTS OF THE FAN SYSTEM (HP)
C      HOPF - HORSEPOWER REQUIREMENTS OF EACH FAN (HP)
95  C      HUBDIA - DIAMETER OF THE FAN HUB (FT)
C      I - PERFORMANCE POINT OF A FAN (DIMENSIONLESS)
C      ITMAX - MAXIMUM NUMBER OF TOWERS ALLOWED BY INPUT VARIABLE
C          (DIMENSIONLESS)
C      ITMIN - N
100  C      ITMIN - MINIMUM NUMBER OF TOWERS ALLOWED BY INPUT VARIABLE
C          (DIMENSIONLESS)
C      ITOWN - NUMBER OF CIRCULAR TOWERS (DIMENSIONLESS)
C      LAF,LFE - VARIABLES USED IN SPECIFYING WHICH FANS ARE TO BE
C          CONSIDERED FOR USE IN THE FAN SYSTEM
105  C          (DIMENSIONLESS)
C      NOF - NUMBER OF FANS MAKING UP THE FAN SYSTEM
C          (DIMENSIONLESS)
C      PFACT - PACKING FACTOR, RATIO OF CIRCULAR TOWER ROOF AREA
C          TO FAN SWEEP AREA (DIMENSIONLESS)
110  C      PLANC - BASE PLANT COSTS ($/KW)
C      POHFAN - INDIRECT COST FACTOR FOR FANS (DECIMAL)
C      POHSTC - INDIRECT COST FACTOR FOR CIRCULAR TOWER STRUCTURES
C          (DECIMAL)
C      ROOFL - CIRCULAR TOWER ROOF LOAD (LBF/SQ FT)

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115      C      SAAF - SHIPPING AND ASSEMBLY FACTOR (DECIMAL)
          C      SPVOL - SPECIFIC VOLUME OF THE AIR EXITING THE HEAT
          C           EXCHANGER (LBM/CU FT)
          C      STRUCC - CIRCULAR TOWER STRUCTURE COST ($)
          C      TAN19 - TANGENT OF 19 DEGREES TO BE USED IN COSTING OF
120      C      ENTRY BELL TO THE FAN (DECIMAL)
          C      TAN 8 - TANGENT OF 8 DEGREES TO BE USED IN COSTING OF EXIT
          C           STACK FROM THE FAN (DECIMAL)
          C      TCSTF - TOTAL COST OF THE FAN SYSTEM ($)
          C      TCSTPF - TOTAL COST OF A FAN ($)
125      C      TOTCFM - TOTAL VOLUMETRIC FLOW RATE FOR THE AIR THROUGH
          C           THE FAN SYSTEM (CU FT/MIN)
          C      TOTHP - TOTAL HORSEPOWER REQUIREMENT OF THE FAN SYSTEM (HP)
          C      TP - TOTAL PRESSURE DIFFERENTIAL ACROSS THE FAN (IN H2O)
          C      TA - AIR EXIT TEMPERATURE FROM THE HEAT EXCHANGER
130      C           (DEG F)
          C      UCS - UNIT COST OF THE STACK ($/LBF)
          C      UWS - UNIT WEIGHT OF THE STACK (LBF/CU FT)
          C      VEL - AVERAGE VELOCITY OF THE AIR LEAVING THE FAN
          C           (FT/SEC)
135      C      VELREC - SPECIFIES WHETHER VELOCITY RECOVERY STACKS ARE
          C           GOING TO BE USED OR NOT (DIMENSIONLESS)
          C      V0 - NON RECOVERABLE AIR VELOCITY HEAT EXITING THE FAN
          C           (IN H2O)
          C      WATERW - WEIGHT OF WATER IN THE HEAT EXCHANGER TUBES AND
140      C           BUNDLES (LBF)
          C      WEV - UNIT WEIGHT OF THE ENTRY BELL (LBF/SQ FT)
          C      WHX - WIEGHT OF THE HEAT EXCHANGER (LBF)
          C      WIDTH - WIDTH OF THE HEAT EXCHANGER (F)
          C      WPL - WIEGHT OF THE PLENUM MATERIAL (LBF/ SQ FT)
145      C      W4 - MASS FLOW RATE OF AIR THROUGH THE HEAT EXCHANGER
          C           (LBM/HR)
          C      XNFAN - NUMBER OF FANS (DIMENSIONLESS)
          C
          C      REAL NOF
150      COMMON /FAN/ FANJAP(153,10),FANJAH(153,10),FMCPFL, FBCPFL,
          $VELREC,AFC,ELEV,EHR
          LOGICAL FIRST, FXTMP
          COMMON
          $ AFTP, ALPHA
155      $ ,CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2,CAP
          $ ,CBU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILS, CVM
          $ ,DEEPL, DESVEL, DANGLE
          $ ,EFPF
          $ ,FCR, FIRST, FIXL, FCOS, FXTMP
160      $ ,GBEFF
          $ ,HXVP, HPCST
          $ ,IHEAT
          $ ,ITMAX, ITMIN
          $ ,JCONS
165      $ ,KCONV, KALEXT
          $ ,MXEXT
          $ ,NTUCAL(2), NTA
          COMMON
          $ OOR
170      $ ,PSIZE, PER, PWCOS, PLANC, PFACT
          $ ,POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCU

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S ,QREJ, QREDUCE
S ,R3P, REDUCE, ROESEL, ROEELA, ROOFL, RFIX
S ,SAAF, SIGMA, SPAMAT(2)
175 S ,TD, TPO(4), TEFF, TLIM, TLRA, TSEALP, TELAST, THFIN, TFIX
S ,TURANG, TW
S ,UCS, UWS
S ,VAS(5)
S ,WAV
180 S ,XJEP, XW, XD
COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
S ,CLAND, REAIR, Z,HRFAC2, W4, U, PPOW,
S ,FRON, DELEC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4,
185 S ,REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3,
S ,SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
S ,B02, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELOX
S ,TLX, UCON, FMOST, FBACC, EFFC, CH, CA, CS
S ,CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPID, AST
190 S ,CAPCST, XNFAN, BLDANG, CPLEN, DPPEL, WHX, WTTUB, ADIA, ABLN
S ,WTHAR, WTFRM, STRJCC, CPERF, HPERF, TOTCF, EFFIN, ANTU
S ,AIRFF, WATFF, XNMOD, TOTPF, FDCPF, FMTRC, ACCTTP, ADJTP
S ,ACTROD, ADJBP0, ACTVH, ADJVV, ADJPPF, THPAIR, TCTF, AFCST
S ,CSD, WATERV, WSTRCT, CFOUNO, HUBDIA, TOWLEN, CSE, CHF
195 S ,CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRN, CFANEL
COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,
S ,GAIR, FAIR, HPAIR, HPWAT, PLANC1
COMMON /HEADAX/ CHH, CN, CHM, CMW, CRU, CWU, CST, CMO, CSR, CSM, PITCHF, CPM
SPRESS, HEDMAT, HEOTYP, NPASS, WB
COMMON /ENLOOP/ LFB, LFE
200 COMMON /PLCOST/ WPL
COMMON /INDIS/ DIST
COMMON /PME/ PMELEC
DATA (FANDAP( 1,J),J=1,10) /
S .7951 .6520 .-6.315 .11.944 .-8.252 ,
205 S .19 .625 .24. .5. .6. /
DATA (FANDAP( 2,J),J=1,10) /
S 1.059 .-8.172 .-1.262 .2533 .-2.331 ,
S .25 .765 .24. .5. .8. /
DATA (FANDAP( 3,J),J=1,10) /
210 S 1.346 .-1.635 .1.685 .-1.666 .5886 ,
S .31 .91 .24. .5. .10. /
DATA (FANDAP( 4,J),J=1,10) /
S .5643 .4.692 .-14.335 .15.950 .-6.562 ,
S .365 .94 .24. .6. .12. /
215 DATA (FANDAP( 5,J),J=1,10) /
S .4015 .5.087 .-16.529 .17.327 .-6.713 ,
S .42 .98 .24. .6. .14. /
DATA (FANDAP( 6,J),J=1,10) /
220 S 1.337 .9315 .-4.655 .5.368 .-2.424 ,
S .477 .95 .24. .6. .15. /
DATA (FANDAP( 7,J),J=1,10) /
S -3.074 .25.489 .-57.905 .54.456 .-19.277 ,
S .532 .1.01 .24. .5. .18. /
DATA (FANDAP( 8,J),J=1,10) /
225 S 1.226 .3.829 .-11.905 .12.904 .-5.363 ,
S .605 .98 .24. .6. .20. /
DATA (FANDAP( 9,J),J=1,10) /
S -17.109 .96.0 .-182.414 .152.343 .-47.879 ,

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230      $ .68      ,1.015      , 24. , 6. , 22. /
        DATA (FANDAP( 10,J),J=1,10) /
        $ .9109      ,-.6216      ,-.0576      ,.09596      ,-.0758      ,
        $ .205      ,.795      , 24. , 8. , 6. /
        DATA (FANDAP( 11,J),J=1,10) /
        $ 1.059      ,-.7222      ,.0581      ,.0384      ,-.0676      ,
235      $ .264      ,.969      , 24. , 8. , 8. /
        DATA (FANDAP( 12,J),J=1,10) /
        $ 1.194      ,-.6306      ,-.0933      ,.01957      ,-.00947      ,
        $ .327      ,1.138      , 24. , 8. , 10. /
        DATA (FANDAP( 13,J),J=1,10) /
240      $ 1.442      ,-.1399      ,1.550      ,-.1.418      ,.4356      ,
        $ .343      ,1.12      , 24. , 8. , 12. /
        DATA (FANDAP( 14,J),J=1,10) /
        $ .4597      ,.4.638      ,-.10.373      ,.8.729      ,-.2.719      ,
        $ .445      ,1.21      , 24. , 8. , 14. /
245      DATA (FANDAP( 15,J),J=1,10) /
        $ 1.533      ,-.5932      ,-.5343      ,.6805      ,-.3261      ,
        $ .529      ,1.14      , 24. , 8. , 16. /
        DATA (FANDAP( 16,J),J=1,10) /
        $ .244      ,.7.202      ,-.14.395      ,.12.133      ,-.3.683      ,
250      $ .612      ,1.25      , 24. , 8. , 18. /
        DATA (FANDAP( 17,J),J=1,10) /
        $ 2.321      ,-.2.232      ,1.862      ,-.7.451      ,-.0714      ,
        $ .684      ,1.15      , 24. , 8. , 20. /
        DATA (FANDAP( 18,J),J=1,10) /
255      $ -12.148      ,.55.65      ,-.83.947      ,.55.657      ,-.13.939      ,
        $ .756      ,1.24      , 24. , 8. , 22. /
        DATA (FANDAP( 19,J),J=1,10) /
        $ .8525      ,-.2121      ,.6814      ,.5934      ,-.1894      ,
        $ .214      ,.95      , 24. , 10. , 6. /
260      DATA (FANDAP( 20,J),J=1,10) /
        $ 1.307      ,-.2.057      ,3.129      ,.2.760      ,.8712      ,
        $ .276      ,1.15      , 24. , 10. , 8. /
        DATA (FANDAP( 21,J),J=1,10) /
        $ 1.140      ,-.3050      ,-.4077      ,.2543      ,-.0612      ,
265      $ .34      ,1.365      , 24. , 10. , 10. /
        DATA (FANDAP( 22,J),J=1,10) /
        $ 1.211      ,-.1516      ,-.5856      ,.3418      ,-.07576      ,
        $ .327      ,1.34      , 24. , 10. , 12. /
        DATA (FANDAP( 23,J),J=1,10) /
270      $ 1.247      ,.0813      ,-.6502      ,.1965      ,-.01166      ,
        $ .455      ,1.4      , 24. , 10. , 14. /
        DATA (FANDAP( 24,J),J=1,10) /
        $ 1.314      ,.5641      ,-.1.534      ,.8592      ,-.1989      ,
        $ .55      ,1.37      , 24. , 10. , 16. /
275      DATA (FANDAP( 25,J),J=1,10) /
        $ .5757      ,.4.363      ,-.7.5248      ,.4.961      ,-.1.231      ,
        $ .652      ,1.55      , 24. , 10. , 18. /
        DATA (FANDAP( 26,J),J=1,10) /
        $ -.076      ,.6.982      ,-.10.793      ,.6.833      ,-.1.667      ,
280      $ .745      ,1.44      , 24. , 10. , 20. /
        DATA (FANDAP( 27,J),J=1,10) /
        $ -158.996      ,.548.34      ,-.659.02      ,.350.82      ,-.69.909      ,
        $ 1.02      ,1.48      , 24. , 10. , 22. /
        DATA (FANDAP( 28,J),J=1,10) /
285      $ 1.090      ,-.1.005      ,.2432      ,.1717      ,-.1.515      ,

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      $ .205      ,.55      , 26. , 6. , 6. /
      DATA (FANDAP( 29,J),J=1,10) /
      $ 1.144      ,-.0621      , -3.590      , 6.245      , -4.382      ,
      $ .248      ,.66      , 26. , 6. , 8. /
290  DATA (FANDAP( 30,J),J=1,10) /
      $ 1.196      ,.1327      , -2.291      , 1.492      , -1.2727      ,
      $ .295      ,.779      , 26. , 6. , 10. /
      DATA (FANDAP( 31,J),J=1,10) /
      $ 1.576      , -1.413      , 1.077      , -.8904      , -.2331      ,
395  $ .35      ,.84      , 26. , 6. , 12. /
      DATA (FANDAP( 32,J),J=1,10) /
      $ -.3976      ,13.678      , -38.403      , 44.263      , -19.254      ,
      $ .41      ,.87      , 26. , 6. , 14. /
      DATA (FANDAP( 33,J),J=1,10) /
400  $ 2.497      , -4.479      , 5.789      , -2.571      , -1.061      ,
      $ .456      ,.85      , 26. , 6. , 16. /
      DATA (FANDAP( 34,J),J=1,10) /
      $ -31.553      ,200.29      , -450.42      , 445.5      , -164.67      ,
      $ .525      ,.89      , 26. , 6. , 18. /
405  DATA (FANDAP( 35,J),J=1,10) /
      $ -37.926      ,229.06      , -493.03      , 468.48      , -156.93      ,
      $ .595      ,.88      , 26. , 6. , 20. /
      DATA (FANDAP( 36,J),J=1,10) /
      $ 199.82      , -940.76      , 1663.3      , -1295.9      , 373.75      ,
310  $ .65      ,.90      , 26. , 6. , 22. /
      DATA (FANDAP( 37,J),J=1,10) /
      $ 1.166      , -1.456      , 2.750      , -4.222      , 1.818      ,
      $ .22      ,.605      , 26. , 8. , 6. /
      DATA (FANDAP( 38,J),J=1,10) /
315  $ 1.178      , -.1032      , -2.070      , 3.033      , -1.935      ,
      $ .275      ,.755      , 26. , 8. , 8. /
      DATA (FANDAP( 39,J),J=1,10) /
      $ 1.431      , -.9074      , .04604      , .5361      , -.6993      ,
      $ .333      ,.885      , 26. , 8. , 10. /
320  DATA (FANDAP( 40,J),J=1,10) /
      $ 1.330      ,.5223      , -3.196      , 3.499      , -1.643      ,
      $ .37      ,.985      , 26. , 6. , 12. /
      DATA (FANDAP( 41,J),J=1,10) /
      $ .8602      ,3.760      , -8.974      , 7.814      , -2.788      ,
325  $ .45      ,1.083      , 26. , 8. , 14. /
      DATA (FANDAP( 42,J),J=1,10) /
      $ 1.929      , -.6431      , -.5586      , .9619      , -.6993      ,
      $ .513      ,1.03      , 26. , 8. , 16. /
      DATA (FANDAP( 43,J),J=1,10) /
330  $ -.6.205      ,44.085      , -97.033      , 72.068      , -22.635      ,
      $ .536      ,1.14      , 26. , 8. , 18. /
      DATA (FANDAP( 44,J),J=1,10) /
      $ -13.827      ,76.312      , -138.97      , 111.051      , -33.333      ,
      $ .65      ,1.06      , 26. , 8. , 20. /
335  DATA (FANDAP( 45,J),J=1,10) /
      $ -14.527      ,69.914      , -108.62      , 75.63      , -20.0      ,
      $ .74      ,1.125      , 26. , 8. , 22. /
      DATA (FANDAP( 46,J),J=1,10) /
      $ 1.084      , -.5941      , .3743      , -.6713      , .2083      ,
340  $ .23      ,.78      , 26. , 11. , 6. /
      DATA (FANDAP( 47,J),J=1,10) /
      $ 1.284      , -.9263      , .9886      , -1.0606      , .303      ,

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$ .29      .98      , 26. , 11. , 8. /
DATA (FANDAP( 48,J),J=1,10) /
345 $ 1.320      ,-.09006 , -1.233      , 1.396      , -.6345
$ .355      , 1.15      , 26. , 11. , 10. /
DATA (FANDAP( 49,J),J=1,10) /
$ 1.385      ,.3155      , -1.959      , 1.880      , -.7164
$ .415      , 1.28      , 26. , 11. , 12. /
350 DATA (FANDAP( 50,J),J=1,10) /
$ 1.376      ,.7735      , -2.250      , 1.701      , -.5449
$ .49      , 1.415      , 26. , 11. , 14. /
DATA (FANDAP( 51,J),J=1,10) /
$ .4584      ,.5911      , -11.257      , 8.504      , -.2414
355 $ .57      , 1.444      , 26. , 11. , 16. /
DATA (FANDAP( 52,J),J=1,10) /
$ -6.278      ,34.035      , -53.2555      , 35.675      , -.88359
$ .65      , 1.525      , 26. , 11. , 18. /
DATA (FANDAP( 53,J),J=1,10) /
360 $ -25.743      ,103.427      , -144.837      , 89.298      , -.20622
$ .75      , 1.38      , 26. , 11. , 20. /
DATA (FANDAP( 54,J),J=1,10) /
$ -67.904      ,225.828      , -273.144      , 146.373      , -.29455
365 $ 1.11      , 1.46      , 26. , 11. , 22. /
DATA (FANDAP( 55,J),J=1,10) /
$ 1.141      ,-.331      , -1.453      , -1.591      , 2.453
$ .19      ,.54      , 28. , 6. , 6. /
DATA (FANDAP( 56,J),J=1,10) /
370 $ 1.045      ,2.745      , -16.574      , 30.038      , -.20517
$ .23      ,.63      , 28. , 6. , 8. /
DATA (FANDAP( 57,J),J=1,10) /
$ .9281      ,5.303      , -23.573      , 36.246      , -.20781
$ .28      ,.71      , 28. , 6. , 10. /
DATA (FANDAP( 58,J),J=1,10) /
375 $ 1.058      ,5.352      , -22.775      , 33.866      , -.18871
$ .33      ,.71      , 28. , 6. , 12. /
DATA (FANDAP( 59,J),J=1,10) /
$ -3.092      ,37.887      , -111.734      , 139.178      , -.64532
380 $ .39      ,.78      , 28. , 6. , 14. /
DATA (FANDAP( 60,J),J=1,10) /
$ -1.430      ,26.222      , -79.847      , 102.926      , -.5000
$ .435      ,.72      , 28. , 6. , 16. /
DATA (FANDAP( 61,J),J=1,10) /
385 $ -22.914      ,167.722      , -422.785      , 467.638      , -.193335
$ .49      ,.785      , 28. , 6. , 18. /
DATA (FANDAP( 62,J),J=1,10) /
$ -4.125      ,46.711      , -131.308      , 150.511      , -.714578
$ .53      ,.76      , 28. , 6. , 20. /
DATA (FANDAP( 63,J),J=1,10) /
390 $ -99.262      ,607.748      , -1365.5      , 1350.4      , -.508349
$ .58      ,.79      , 28. , 6. , 22. /
DATA (FANDAP( 64,J),J=1,10) /
$ 1.149      ,-.0283      , -3.051      , 3.750      , -.1911
395 $ .20      ,.67      , 28. , 8. , 6. /
DATA (FANDAP( 65,J),J=1,10) /
$ 1.386      ,-.4003      , -2.450      , 3.275      , -.1655
$ .255      ,.79      , 28. , 8. , 8. /
DATA (FANDAP( 66,J),J=1,10) /
$ 1.479      ,-.4131      , -.8639      , -.0806      , .3017

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400      S .3      ,.9      , 28. , 8. , 10. /
        DATA (FANDAP( 67,J),J=1,10) /
        S 1.542    ,1.115    , -6.969    ,9.507    , -4.848    ,
        S .35     ,.9      , 28. , 8. , 12. /
        DATA (FANDAP( 68,J),J=1,10) /
405      S .4343    ,9.668    , -26.867    ,28.991    , -11.655    ,
        S .44     ,.98     , 28. , 8. , 14. /
        DATA (FANDAP( 69,J),J=1,10) /
        S -.1495    ,13.991    , -36.402    ,38.619    , -15.385    ,
        S .43     ,.94     , 28. , 8. , 16. /
410      DATA (FANDAP( 70,J),J=1,10) /
        S -1.626    ,22.206    , -51.296    ,49.975    , -18.322    ,
        S .557     ,.98     , 28. , 8. , 18. /
        DATA (FANDAP( 71,J),J=1,10) /
        S -15.419    ,94.430    , -191.291    ,170.303    , -56.97    ,
415      S .6      ,.96     , 28. , 8. , 20. /
        DATA (FANDAP( 72,J),J=1,10) /
        S -182.795    ,850.555    , -1466.4    ,1121.9    , -321.938    ,
        S .8      ,1.01    , 28. , 9. , 22. /
        DATA (FANDAP( 73,J),J=1,10) /
420      S 1.907     , -8.155    ,26.542    , -39.870    ,20.833    ,
        S .203     ,.72     , 28. , 9. , 6. /
        DATA (FANDAP( 74,J),J=1,10) /
        S 1.707     , -2.471    ,5.482     , -7.257    ,3.078     ,
        S .3      ,1.025    , 28. , 9. , 10. /
425      DATA (FANDAP( 75,J),J=1,10) /
        S -5.491     ,43.171    , -95.551    ,90.264    , -31.495    ,
        S .443     ,1.045    , 28. , 9. , 14. /
        DATA (FANDAP( 76,J),J=1,10) /
        S -11.476    ,71.058    , -139.528    ,119.048    , -37.792    ,
430      S .555     ,1.08     , 28. , 9. , 18. /
        DATA (FANDAP( 77,J),J=1,10) /
        S -111.138    ,485.02    , -778.16    ,553.442    , -147.595    ,
        S .57     ,1.11    , 28. , 9. , 22. /
        DATA (FANDAP( 78,J),J=1,10) /
435      S .9182     , -6.397    ,12.63     , -1.283    ,1.08     ,
        S .118     ,.54     , 28. , 10. , 2. /
        DATA (FANDAP( 79,J),J=1,10) /
        S 1.191     , -5.515    , -7.045    , -7.974    , -6.976    ,
        S .2      ,.8      , 28. , 10. , 6. /
440      DATA (FANDAP( 80,J),J=1,10) /
        S 1.478     , -2.616    , -2.549    ,3.408     , -1.70     ,
        S .31     ,1.03     , 28. , 10. , 10. /
        DATA (FANDAP( 81,J),J=1,10) /
        S 0.4844     ,8.207     , -20.171    ,19.338    , -6.894    ,
445      S .45     ,1.15     , 28. , 10. , 14. /
        DATA (FANDAP( 82,J),J=1,10) /
        S -12.956    ,75.341    , -141.915    ,115.921    , -35.119    ,
        S .53     ,1.17     , 28. , 10. , 18. /
        DATA (FANDAP( 83,J),J=1,10) /
450      S -131.140    ,528.522    , -784.764    ,516.323    , -127.273    ,
        S .71     ,1.21     , 28. , 10. , 22. /
        DATA (FANDAP( 84,J),J=1,10) /
        S .9394     , -6.355    ,34.96     , -1.169    ,.7752     ,
        S .122     ,.64     , 28. , 12. , 2. /
455      DATA (FANDAP( 85,J),J=1,10) /
        S 1.205     , -5.51     ,18.97     , -1.018    ,.6163     ,

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$ .216      .94      , 28. , 12. , 6. /
  DATA (FANDAP( 86,J),J=1,10) /
460 $ 1.504      ,-.1562      ,=1.505      ,1.699      ,-.7334      ,
$ .33      ,1.2      , 28. , 12. , 10. /
  DATA (FANDAP( 87,J),J=1,10) /
$ .6086      ,6.967      ,=-15.551      ,13.341      ,-.4.215      ,
$ .43      ,1.32      , 28. , 12. , 14. /
  DATA (FANDAP( 88,J),J=1,10) /
465 $ 1.227      ,4.415      ,=-9.275      ,7.309      ,-.2.178      ,
$ .52      ,1.44      , 28. , 12. , 18. /
  DATA (FANDAP( 89,J),J=1,10) /
$ 1.036      ,-.4415      ,=-6.142      ,15.125      ,-.14.698      ,
$ .12      ,.38      , 30. , 8. , 2. /
470  DATA (FANDAP( 90,J),J=1,10) /
$ 2.034      ,=-5.822      ,13.159      ,=-16.404      ,6.562      ,
$ .22      ,.64      , 30. , 8. , 6. /
  DATA (FANDAP( 91,J),J=1,10) /
475 $ 1.109      ,6.519      ,=-26.233      ,35.842      ,=-18.121      ,
$ .32      ,.79      , 30. , 8. , 10. /
  DATA (FANDAP( 92,J),J=1,10) /
$ -9.489      ,76.086      ,=-183.815      ,190.216      ,=-73.502      ,
$ .48      ,.85      , 30. , 8. , 14. /
  DATA (FANDAP( 93,J),J=1,10) /
480 $ -1009.5      ,5246.17      ,=-10188.02      ,8781.48      ,=-2836.03      ,
$ .7      ,.88      , 30. , 8. , 18. /
  DATA (FANDAP( 94,J),J=1,10) /
$ 5.2445      ,=-4.875      ,0.      ,0.      ,0.      ,
$ .83      ,.91      , 30. , 8. , 22. /
485  DATA (FANDAP( 95,J),J=1,10) /
$ 1.055      ,-.7416      ,=-2.354      ,6.096      ,=-6.699      ,
$ .12      ,.4      , 30. , 10. , 2. /
  DATA (FANDAP( 96,J),J=1,10) /
490 $ 1.611      ,=-1.705      ,1.163      ,=-1.643      ,.7516      ,
$ .23      ,.7      , 30. , 10. , 6. /
  DATA (FANDAP( 97,J),J=1,10) /
$ .5192      ,9.050      ,=-26.525      ,29.287      ,=-12.083      ,
$ .34      ,.9      , 30. , 10. , 10. /
  DATA (FANDAP( 98,J),J=1,10) /
495 $ -9.716      ,71.057      ,=-157.956      ,150.679      ,=-53.458      ,
$ .46      ,1.0      , 30. , 10. , 14. /
  DATA (FANDAP( 99,J),J=1,10) /
$ -504.715      ,2209.6      ,=-3604.35      ,2607.84      ,=-706.956      ,
$ .82      ,1.045      , 30. , 10. , 18. /
500  DATA (FANDAP(100,J),J=1,10) /
$ -3515.3      ,13939.07      ,=-20703.7      ,15672.5      ,=-3385.42      ,
$ .97      ,1.08      , 30. , 10. , 22. /
  DATA (FANDAP(101,J),J=1,10) /
505 $ 1.076      ,-.9295      ,=-.3826      ,.4669      ,=-.8643      ,
$ .12      ,.44      , 30. , 11. , 2. /
  DATA (FANDAP(102,J),J=1,10) /
$ 1.555      ,=-1.08      ,=-.4653      ,.5259      ,=-.2670      ,
$ .24      ,.765      , 30. , 11. , 6. /
  DATA (FANDAP(103,J),J=1,10) /
510 $ .9216      ,6.142      ,=-18.702      ,18.968      ,=-7.415      ,
$ .35      ,.98      , 30. , 11. , 10. /
  DATA (FANDAP(104,J),J=1,10) /
$ -13.274      ,109.841      ,=-218.930      ,188.787      ,=-60.351      ,

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515      $ .576      ,1.07      , 30. , 11. , 14. /
        DATA (FANDAP(105,J),J=1,10) /
        $ -3000.2    ,12053.9    ,18124.3 ,12096.4 , -3024.19 ,
        $ .917      ,1.11      , 30. , 11. , 18. /
        DATA (FANDAP(106,J),J=1,10) /
520      $ -39.918    ,78.558     , -36.939 ,0.0      ,0.0      ,
        $ 1.07      ,1.16      , 30. , 11. , 22. /
        DATA (FANDAP(107,J),J=1,10) /
        $ 1.032      ,-.2723     , -3.275  ,5.874    , -5.731   ,
        $ .125      ,.485       , 30. , 12. , 2. /
        DATA (FANDAP(108,J),J=1,10) /
525      $ 1.523      ,-.8049     , -.869   ,.9265    , -.397    ,
        $ .245      ,.83        , 30. , 12. , 6. /
        DATA (FANDAP(109,J),J=1,10) /
        $ 1.151      ,4.199      , -12.180 ,11.996   , -4.465   ,
        $ .35       ,1.05       , 30. , 12. , 10. /
530      DATA (FANDAP(110,J),J=1,10) /
        $ -14.035    ,83.829     , -160.549 ,132.788  , -40.673  ,
        $ .51       ,1.14       , 30. , 12. , 14. /
        DATA (FANDAP(111,J),J=1,10) /
535      $ -4739.04   ,17939.56   , -25154.2 ,15654.5  , -3649.91 ,
        $ .978      ,1.19      , 30. , 12. , 18. /
        DATA (FANDAP(112,J),J=1,10) /
        $ 1.376      ,-.1865     , -15.858 ,53.187   , -69.015  ,
        $ .13       ,.385       , 40. , 8. , 2. /
        DATA (FANDAP(113,J),J=1,10) /
540      $ 2.508      ,-.2.762    , 6.513   , -15.566  , 9.394    ,
        $ .225      ,.64        , 40. , 8. , 6. /
        DATA (FANDAP(114,J),J=1,10) /
        $ 1.969      ,6.765      , -22.032 ,24.257   , -11.119  ,
        $ .32       ,.83        , 40. , 8. , 10. /
545      DATA (FANDAP(115,J),J=1,10) /
        $ -6.169     ,63.615     , -156.602 ,163.373  , -63.846  ,
        $ .447      ,.91       , 40. , 8. , 14. /
        DATA (FANDAP(116,J),J=1,10) /
550      $ -5.464     ,55.577     , -127.737 ,123.57   , -49.557  ,
        $ .54       ,.96       , 40. , 8. , 18. /
        DATA (FANDAP(117,J),J=1,10) /
        $ -191.805   ,955.903    , -1748.194 ,1419.63  , -433.33  ,
        $ .675      ,1.0       , 40. , 8. , 22. /
        DATA (FANDAP(118,J),J=1,10) /
555      $ 1.802      ,.454       , -11.977 ,27.924   , -27.683  ,
        $ .14       ,.38       , 40. , 10. , 2. /
        DATA (FANDAP(119,J),J=1,10) /
        $ 2.222      ,2.029      , -2.762  ,10.241   , -3.528   ,
        $ .253      ,.72       , 40. , 10. , 6. /
560      DATA (FANDAP(120,J),J=1,10) /
        $ 1.717      ,10.358     , -31.846 ,36.638   , -16.245  ,
        $ .367      ,.92       , 40. , 10. , 10. /
        DATA (FANDAP(121,J),J=1,10) /
        $ -10.728    ,85.651     , -189.652 ,179.696  , -63.371  ,
565      $ .495      ,1.02      , 40. , 10. , 14. /
        DATA (FANDAP(122,J),J=1,10) /
        $ -90.812    ,472.054    , -875.215 ,713.056  , -216.564 ,
        $ .53       ,1.073     , 40. , 10. , 18. /
        DATA (FANDAP(123,J),J=1,10) /
570      $ -251.346  ,1060.7     , -1650.93 ,1141.51  , -296.667 ,

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$ .80      .1.127      , 40. , 10. , 22. /
DATA (FANDAP(124,J),J=1,10) /
$ 1.920    , -1.696    , 3.019    , 48.274    , 3.907    ,
$ .14      , .44      , 40. , 12. , 2. /
575 DATA (FANDAP(125,J),J=1,10) /
$ 2.561    , -1.195    , .1299    , -1.262    , .399    ,
$ .255     , .84      , 40. , 12. , 6. /
DATA (FANDAP(126,J),J=1,10) /
$ .4204    , 17.453    , -43.194    , 42.370    , -15.566    ,
580 $ .39      , 1.06     , 40. , 12. , 10. /
DATA (FANDAP(127,J),J=1,10) /
$ -11.44    , 75.814    , -145.248    , 117.676    , -35.539    ,
$ .52      , 1.17     , 40. , 12. , 14. /
DATA (FANDAP(128,J),J=1,10) /
585 $ -7.134    , 51.677    , -90.389    , 58.768    , -19.929    ,
$ .635     , 1.24     , 40. , 12. , 18. /
DATA (FANDAP(129,J),J=1,10) /
$ -448.799    , 1598.46    , -2115.93    , 1245.43    , -275.191    ,
590 $ .99      , 1.3      , 40. , 12. , 22. /
DATA (FANDAP(130,J),J=1,10) /
$ 1.843     , -.07846    , -6.985    , 17.722    , -17.908    ,
$ .145     , .48      , 40. , 14. , 2. /
DATA (FANDAP(131,J),J=1,10) /
595 $ 2.525     , -1.142    , .7597    , -2.214    , 1.017    ,
$ .27      , .93      , 40. , 14. , 6. /
DATA (FANDAP(132,J),J=1,10) /
$ .8452     , 13.03     , -29.085    , 25.619    , -8.539    ,
$ .40      , 1.19     , 40. , 14. , 10. /
DATA (FANDAP(133,J),J=1,10) /
600 $ -3.555     , 39.492    , -78.853    , 64.69     , -19.54     ,
$ .573     , 1.28     , 40. , 14. , 14. /
DATA (FANDAP(134,J),J=1,10) /
$ -39.186    , 178.576    , -272.965    , 181.609    , -44.911    ,
605 $ .63      , 1.35     , 40. , 14. , 18. /
DATA (FANDAP(135,J),J=1,10) /
$ -118.82    , 406.731    , -504.395    , 279.236    , -57.944    ,
$ .85      , 1.435    , 40. , 14. , 22. /
DATA (FANDAP(136,J),J=1,10) /
610 $ 4.988     , -2.081    , -24.207    , 55.248    , -45.947    ,
$ .135     , .492     , 60. , 12. , 4. /
DATA (FANDAP(137,J),J=1,10) /
$ 5.529     , -.2277    , -27.832    , 50.082    , -33.077    ,
$ .195     , .59      , 60. , 12. , 6. /
DATA (FANDAP(138,J),J=1,10) /
615 $ 2.068     , 38.609    , -157.75    , 240.715    , -137.116    ,
$ .235     , .56      , 60. , 12. , 8. /
DATA (FANDAP(139,J),J=1,10) /
$ 2.644     , 37.353    , -146.207    , 215.777    , -119.45    ,
620 $ .23      , .73      , 60. , 12. , 10. /
DATA (FANDAP(140,J),J=1,10) /
$ -41.688    , 396.76     , -1195.8     , 1548.1     , -740.92     ,
$ .333     , .744     , 60. , 12. , 12. /
DATA (FANDAP(141,J),J=1,10) /
625 $ -7.944     , 124.78     , -369.35     , 456.25     , -210.91     ,
$ .397     , .76      , 60. , 12. , 14. /
DATA (FANDAP(142,J),J=1,10) /
$ -40.774    , 349.5      , -929.9      , 1076.8     , -468.43     ,

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$ .451      ,.76      , 60. , 12. , 16. /
DATA (FANDAP(143,J),J=1,10) /
630 $ -1619.9 ,9561.7 , -21439.7 ,21080.3 , -7759.4 ,
$ .51      ,.786      , 60. , 12. , 18. /
DATA (FANDAP(144,J),J=1,10) /
$ 4.129     , -3.795     ,.7758     , -8.697     ,8.977     ,
635 $ .12      ,.48      , 60. , 16. , 2. /
DATA (FANDAP(145,J),J=1,10) /
$ 4.804     , -3.225     , -1.142     , -3.317     ,2.953     ,
$ .134      ,.62      , 60. , 16. , 4. /
DATA (FANDAP(146,J),J=1,10) /
640 $ 5.296     , -1.8909    , -9.21      ,8.711      , -3.365     ,
$ .202      ,.76      , 60. , 16. , 6. /
DATA (FANDAP(147,J),J=1,10) /
$ 6.217     , -3.071     , -1.696     , -2.459     ,2.489     ,
$ .231      ,.76      , 60. , 16. , 8. /
DATA (FANDAP(148,J),J=1,10) /
645 $ 5.008     ,14.159     , -55.056    ,58.651     , -31.803     ,
$ .31      ,.93      , 60. , 15. , 10. /
DATA (FANDAP(149,J),J=1,10) /
$ 5.504     ,13.941     , -45.551    ,47.755     , -19.574     ,
650 $ .356      ,.90      , 60. , 16. , 12. /
DATA (FANDAP(150,J),J=1,10) /
$ -34.30     ,265.14     , -612.11    ,604.01     , -220.51     ,
$ .435      ,.98      , 60. , 15. , 14. /
DATA (FANDAP(151,J),J=1,10) /
$ 25.353     , -96.07     ,197.51     , -185.15    ,62.299     ,
655 $ .49      ,.91      , 60. , 16. , 16. /
DATA (FANDAP(152,J),J=1,10) /
$ -220.05     ,1153.5     , -2169.     ,1802.6     , -562.09     ,
$ .55      ,.98      , 60. , 16. , 18. /
DATA (FANDAP(153,J),J=1,10) /
660 $ -390.036    ,841.7     , -445.22     ,0.0        ,0.0        ,
$ .95      ,1.0      , 60. , 16. , 22. /
DATA (FANDAH( 1,J),J=1,10) /
$ -93.846     ,983.578     , -2376.14    ,2520.20     , -1060.61     ,
665 $ 400000.     ,760000.     , 24. , 6. , 6. /
DATA (FANDAH( 2,J),J=1,10) /
$ 7.793      ,288.39     , -481.24     ,349.65     , -139.86     ,
$ 400000.     ,860000.     , 24. , 5. , 8. /
DATA (FANDAH( 3,J),J=1,10) /
670 $ -115.79     ,1005.09     , -1846.07    ,1498.74     , -486.6     ,
$ 400000.     ,950000.     , 24. , 5. , 10. /
DATA (FANDAH( 4,J),J=1,10) /
$ 80.751     , -103.62     ,720.59     , -340.42     ,261.73     ,
$ 400000.     ,1025000.     , 24. , 6. , 12. /
DATA (FANDAH( 5,J),J=1,10) /
675 $ 155.98     , -527.75     ,1464.53     , -1447.9     ,460.03     ,
$ 400000.     ,1100000.     , 24. , 6. , 14. /
DATA (FANDAH( 6,J),J=1,10) /
$ -196.02     ,1138.28     , -1400.76    ,749.81     , -163.17     ,
$ 650000.     ,1180000.     , 24. , 6. , 15. /
680 DATA (FANDAH( 7,J),J=1,10) /
$ 205.61     , -579.29     ,1312.33     , -1087.12    ,296.36     ,
$ 500000.     ,1250000.     , 24. , 6. , 18. /
DATA (FANDAH( 8,J),J=1,10) /
$ 705.77     , -2402.05    ,3785.21     , -2521.68    ,601.4     ,

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685      $ 800000. ,1330000. , 24. , 6. , 20. /
        DATA (FANDAH( 9,J),J=1,10) /
        $ 721.32 , -2194.49 ,3143.5 , -1889.81 ,405.8 ,
        $ 750000. ,1400000. , 24. , 6. , 22. /
        DATA (FANDAH( 10,J),J=1,10) /
690      $ 177.57 , -697.3 ,1776.99 , -2003.05 ,757.58 ,
        $ 400000. ,780000. , 24. , 8. , 6. /
        DATA (FANDAH( 11,J),J=1,10) /
        $ 185.52 , -582.33 ,1372.23 , -1437.06 ,501.17 ,
        $ 400000. ,880000. , 24. , 8. , 8. /
695      DATA (FANDAH( 12,J),J=1,10) /
        $ 143.97 , -192.78 ,439.12 , -444.8 ,119.46 ,
        $ 400000. ,970000. , 24. , 8. , 10. /
        DATA (FANDAH( 13,J),J=1,10) /
        $ 169.15 , -256.19 ,512.11 , -361.99 ,36.131 ,
700      $ 500000. ,1050000. , 24. , 8. , 12. /
        DATA (FANDAH( 14,J),J=1,10) /
        $ -77.675 ,1050.7 , -1876.53 ,1567.15 , -530.3 ,
        $ 500000. ,1140000. , 24. , 8. , 14. /
        DATA (FANDAH( 15,J),J=1,10) /
705      $ 148.08 , -168.6 ,627.63 , -604.74 ,160.84 ,
        $ 700000. ,1240000. , 24. , 8. , 16. /
        DATA (FANDAH( 16,J),J=1,10) /
        $ 142.97 , -189.66 ,786.1 , -749.69 ,204.99 ,
        $ 650000. ,1330000. , 24. , 8. , 18. /
        DATA (FANDAH( 17,J),J=1,10) /
710      $ -235.94 ,1539.71 , -2094.92 ,1360.06 , -354.31 ,
        $ 900000. ,1400000. , 24. , 8. , 20. /
        DATA (FANDAH( 18,J),J=1,10) /
        $ -112.66 ,849.55 , -906.93 ,564.88 , -163.17 ,
715      $ 900000. ,1400000. , 24. , 8. , 22. /
        DATA (FANDAH( 19,J),J=1,10) /
        $ 22.074 ,483.11 , -1316.1 ,1603.54 , -833.33 ,
        $ 400000. ,780000. , 24. , 10. , 6. /
        DATA (FANDAH( 20,J),J=1,10) /
720      $ 58.107 ,431.89 , -1131.38 ,1196.97 , -524.48 ,
        $ 400000. ,880000. , 24. , 10. , 8. /
        DATA (FANDAH( 21,J),J=1,10) /
        $ 112.44 ,139.49 , -323.24 ,300.12 , -145.69 ,
        $ 400000. ,970000. , 24. , 10. , 10. /
725      DATA (FANDAH( 22,J),J=1,10) /
        $ -100.95 ,1345.91 , -2651.05 ,2365.19 , -839.16 ,
        $ 550000. ,1060000. , 24. , 10. , 12. /
        DATA (FANDAH( 23,J),J=1,10) /
        $ -196.47 ,1864.5 , -3537.84 ,3061.97 , -1031.47 ,
730      $ 580000. ,1140000. , 24. , 10. , 14. /
        DATA (FANDAH( 24,J),J=1,10) /
        $ -436.64 ,2301.51 , -4681.25 ,3571.12 , -1051.86 ,
        $ 720000. ,1250000. , 24. , 10. , 16. /
        DATA (FANDAH( 25,J),J=1,10) /
735      $ -27.599 ,620.01 , -768.57 ,558.36 , -191.62 ,
        $ 650000. ,1330000. , 24. , 10. , 18. /
        DATA (FANDAH( 26,J),J=1,10) /
        $ -762.28 ,3309.25 , -4177.96 ,2502.21 , -599.65 ,
        $ 850000. ,1400000. , 24. , 10. , 20. /
740      DATA (FANDAH( 27,J),J=1,10) /
        $ -279.88 ,1653.67 , -2140.73 ,1475.52 , -414.92 ,

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$ 900000. ,1400000. , 24. , 10. , 22. /
DATA (FANDAH( 28,J),J=1,10) /
745 $ -59.966 ,641.02 , -1263.85 ,1123.39 , -414.92 ,
$ 500000. ,900000. , 26. , 6. , 6. /
DATA (FANDAH( 29,J),J=1,10) /
$ 147.44 , -436.19 , 915.07 , -784.62 , 209.79 ,
$ 500000. ,990000. , 26. , 6. , 8. /
DATA (FANDAH( 30,J),J=1,10) /
750 $ 46.138 ,166.73 , -282.52 ,272.1 , -126.46 ,
$ 500000. ,1080000. , 26. , 6. , 10. /
DATA (FANDAH( 31,J),J=1,10) /
$ 133.94 , -252.12 , 498.13 , -354.08 , 67.873 ,
755 $ 500000. ,1180000. , 26. , 6. , 12. /
DATA (FANDAH( 32,J),J=1,10) /
$ 172.97 , -372.85 , 722.82 , -517.47 , 114.80 ,
$ 500000. ,1270000. , 26. , 6. , 14. /
DATA (FANDAH( 33,J),J=1,10) /
760 $ -.3204 ,452.26 , -648.81 , 493.49 , -156.59 ,
$ 750000. ,1350000. , 26. , 6. , 16. /
DATA (FANDAH( 34,J),J=1,10) /
$ 130.3 , -92.296 , 235.95 , -117.56 , 2.759 ,
$ 700000. ,1430000. , 26. , 6. , 18. /
DATA (FANDAH( 35,J),J=1,10) /
765 $ 162.16 , -194.34 , 432.03 , -278.64 , 53.34 ,
$ 900000. ,1500000. , 26. , 6. , 20. /
DATA (FANDAH( 36,J),J=1,10) /
$ 322.67 , -447.74 , 423.14 , -95.091 , -15.494 ,
770 $ 940000. ,1500000. , 26. , 6. , 22. /
DATA (FANDAH( 37,J),J=1,10) /
$ -350.23 , 2212.31 , -4250. , 3636.36 , -1212.12 ,
$ 600000. ,940000. , 26. , 8. , 5. /
DATA (FANDAH( 38,J),J=1,10) /
775 $ 83.708 , 7433 , 115.75 , -152.03 , 23.31 ,
$ 600000. ,1040000. , 26. , 8. , 8. /
DATA (FANDAH( 39,J),J=1,10) /
$ 160.08 , -245.62 , 483.82 , -364.34 , 67.599 ,
$ 600000. ,1150000. , 26. , 8. , 10. /
DATA (FANDAH( 40,J),J=1,10) /
780 $ 77.044 , 115.59 , -11.038 , -49.109 , -3.771 ,
$ 600000. ,1250000. , 26. , 8. , 12. /
DATA (FANDAH( 41,J),J=1,10) /
$ 175.39 , -257.33 , 533.44 , -449.33 , 100.19 ,
785 $ 600000. ,1340000. , 26. , 8. , 14. /
DATA (FANDAH( 42,J),J=1,10) /
$ -474.23 , 2189.22 , -2769.15 , 1597.82 , -363.64 ,
$ 840000. ,1440000. , 26. , 8. , 16. /
DATA (FANDAH( 43,J),J=1,10) /
790 $ 193.55 , -238.44 , 578.44 , -479.25 , 100.02 ,
$ 600000. ,1520000. , 26. , 8. , 18. /
DATA (FANDAH( 44,J),J=1,10) /
$ -559.84 , 2354.58 , -2794.35 , 1546.54 , -335.66 ,
$ 1050000. ,1570000. , 26. , 8. , 20. /
DATA (FANDAH( 45,J),J=1,10) /
795 $ -4347.74 , 13226.42 , -14504.08 , 7162.39 , -1342.66 ,
$ 1150000. ,1600000. , 26. , 8. , 22. /
DATA (FANDAH( 46,J),J=1,10) /
$ -324.08 , 2261.12 , -4454.17 , 3924.24 , -1363.64 ,

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      $ 600000. , 970000. , 26. , 11. , 5. /
      DATA (FANDAH( 47,J),J=1,10) /
      $ 297.49 , -674.34 , 923.09 , -453.77 , 0.0 ,
      $ 600000. , 1080000. , 26. , 11. , 8. /
      DATA (FANDAH( 48,J),J=1,10) /
      $ 165.74 , -105.07 , 169.48 , -24.391 , -71.678 ,
      $ 600000. , 1190000. , 26. , 11. , 10. /
      DATA (FANDAH( 49,J),J=1,10) /
      $ -121.21 , 1158.54 , -1704.59 , 1170.09 , -335.11 ,
      $ 600000. , 1300000. , 26. , 11. , 12. /
      DATA (FANDAH( 50,J),J=1,10) /
      $ -34.067 , 818.08 , -1116.29 , 766.02 , -230.43 ,
      $ 600000. , 1390000. , 26. , 11. , 14. /
      DATA (FANDAH( 51,J),J=1,10) /
      $ 12.917 , 602.92 , -670.08 , 415.16 , -126.02 ,
      $ 600000. , 1500000. , 26. , 11. , 16. /
      DATA (FANDAH( 52,J),J=1,10) /
      $ 223.46 , -1.088 , 80.012 , 1.166 , -34.965 ,
      $ 600000. , 1600000. , 26. , 11. , 18. /
      DATA (FANDAH( 53,J),J=1,10) /
      $ -3.922 , 1038.49 , -1360.42 , 847.22 , -208.33 ,
      $ 1000000. , 1600000. , 26. , 11. , 20. /
      DATA (FANDAH( 54,J),J=1,10) /
      $ -3555.68 , 11081.15 , -11777.09 , 5652.78 , -1041.67 ,
      $ 1170000. , 1600000. , 26. , 11. , 22. /
      DATA (FANDAH( 55,J),J=1,10) /
      $ 32.974 , 97.99 , -185.86 , 213.99 , -116.55 ,
      $ 500000. , 1020000. , 28. , 5. , 6. /
      DATA (FANDAH( 56,J),J=1,10) /
      $ 80.295 , -71.86 , 154.45 , -110.7 , 11.083 ,
      $ 500000. , 1110000. , 28. , 6. , 8. /
      DATA (FANDAH( 57,J),J=1,10) /
      $ 85.09 , -39.55 , 76.619 , -26.452 , -17.992 ,
      $ 500000. , 1220000. , 28. , 6. , 10. /
      DATA (FANDAH( 58,J),J=1,10) /
      $ 163.72 , -352.71 , 588.45 , -352.27 , 56.818 ,
      $ 730000. , 1330000. , 28. , 5. , 12. /
      DATA (FANDAH( 59,J),J=1,10) /
      $ -30.521 , 391.0 , -386.5 , 205.0 , -55.628 ,
      $ 500000. , 1450000. , 28. , 6. , 14. /
      DATA (FANDAH( 60,J),J=1,10) /
      $ 522.91 , -1352.27 , 1663.48 , -841.6 , 145.26 ,
      $ 1030000. , 1560000. , 28. , 6. , 16. /
      DATA (FANDAH( 61,J),J=1,10) /
      $ 744.22 , -1005.75 , 2170. , -1022.22 , 166.67 ,
      $ 1000000. , 1630000. , 28. , 5. , 18. /
      DATA (FANDAH( 62,J),J=1,10) /
      $ 550.31 , -1015.79 , 914.44 , -298.92 , 21.461 ,
      $ 1250000. , 1700000. , 28. , 6. , 20. /
      DATA (FANDAH( 63,J),J=1,10) /
      $ -190.67 , 1135.05 , -1362.37 , 760.4 , -159.66 ,
      $ 1290000. , 1760000. , 28. , 6. , 22. /
      DATA (FANDAH( 64,J),J=1,10) /
      $ -51.432 , 688.46 , -1396.44 , 1273.01 , -461.14 ,
      $ 500000. , 1050000. , 28. , 8. , 6. /
      DATA (FANDAH( 65,J),J=1,10) /
      $ 27.126 , 271.5 , -455.18 , 381.06 , -143.86 ,

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      $ 530000. ,1180000. , 28. , 8. , 8. /
      DATA (FANDAH( 66,J),J=1,10) /
      $ 157.22 , -318.65 , 623.34 , -446.78 , 91.05 ,
860  $ 550000. ,1280000. , 28. , 8. , 10. /
      DATA (FANDAH( 67,J),J=1,10) /
      $ 297.63 , -873.87 , 1501.18 , -1021.21 , 231.07 ,
      $ 650000. ,1400000. , 28. , 8. , 12. /
      DATA (FANDAH( 68,J),J=1,10) /
      $ 177.36 , -395.03 , 889.58 , -672.74 , 160.98 ,
865  $ 600000. ,1540000. , 28. , 9. , 14. /
      DATA (FANDAH( 69,J),J=1,10) /
      $ 79.60 , -25.75 , 395.79 , -348.17 , 80.49 ,
      $ 900000. ,1600000. , 28. , 9. , 16. /
      DATA (FANDAH( 70,J),J=1,10) /
870  $ 250.75 , -520.49 , 949.34 , -600.17 , 122.38 ,
      $ 930000. ,1700000. , 28. , 9. , 18. /
      DATA (FANDAH( 71,J),J=1,10) /
      $ 311.62 , -376.48 , 398.49 , -114.14 , -4.08 ,
      $ 1200000. ,1750000. , 28. , 8. , 20. /
875  DATA (FANDAH( 72,J),J=1,10) /
      $ -257.36 , 1167.2 , -1145.64 , 581.78 , -120.54 ,
      $ 1250000. ,1770000. , 28. , 8. , 22. /
      DATA (FANDAH( 73,J),J=1,10) /
      $ -13.15 , 483.04 , -828.15 , 703.03 , -274.70 ,
880  $ 500000. ,1050000. , 28. , 9. , 6. /
      DATA (FANDAH( 74,J),J=1,10) /
      $ 102.65 , 7.17 , 38.10 , 39.95 , -66.37 ,
      $ 500000. ,1290000. , 28. , 9. , 10. /
      DATA (FANDAH( 75,J),J=1,10) /
885  $ 125.12 , -50.93 , 318.54 , -250.86 , 51.63 ,
      $ 600000. ,1570000. , 28. , 9. , 14. /
      DATA (FANDAH( 76,J),J=1,10) /
      $ 183.11 , -95.27 , 404.55 , -307.01 , 61.86 ,
      $ 950000. ,1770000. , 28. , 9. , 18. /
890  DATA (FANDAH( 77,J),J=1,10) /
      $ -7314.5 , 19307.41 , -18251.29 , 7656.64 , -1207.28 ,
      $ 1250000. ,1770000. , 28. , 9. , 22. /
      DATA (FANDAH( 78,J),J=1,10) /
895  $ 1415.04 , -8770.24 , 21006.05 , -22060.6 , 8484.84 ,
      $ 500000. ,830000. , 28. , 10. , 2. /
      DATA (FANDAH( 79,J),J=1,10) /
      $ -38.9 , 910.41 , -1370.82 , 1144.03 , -422. ,
      $ 550000. ,1070000. , 28. , 10. , 6. /
900  DATA (FANDAH( 80,J),J=1,10) /
      $ 131.94 , -73.08 , 191.65 , -68.24 , -48.20 ,
      $ 570000. ,1320000. , 28. , 10. , 10. /
      DATA (FANDAH( 81,J),J=1,10) /
      $ 224.07 , -284.12 , 540.09 , -336.88 , 55.13 ,
905  $ 500000. ,1580000. , 28. , 10. , 14. /
      DATA (FANDAH( 82,J),J=1,10) /
      $ 713.7 , -1798.52 , 2459.25 , -1335.48 , 259.29 ,
      $ 850000. ,1770000. , 28. , 10. , 18. /
      DATA (FANDAH( 83,J),J=1,10) /
910  $ -1153.75 , 4181.1 , -4529.62 , 2243.76 , -426.4 ,
      $ 1200000. ,1770000. , 28. , 10. , 22. /
      DATA (FANDAH( 84,J),J=1,10) /
      $ 1151.37 , -5675.67 , 14912.2 , -14463.5 , 5109.47 ,

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$ 500000. ,860000. , 28. , 12. , 2. /
DATA (FANDAH( 85,J),J=1,10) /
915 $ -257.67 ,1727.79 ,2934.3 ,2274.14 ,724.96
$ 550000. ,1180000. , 28. , 12. , 6. /
DATA (FANDAH( 86,J),J=1,10) /
$ 90.637 ,287.08 ,415.77 ,341.86 ,146.78
$ 570000. ,1340000. , 28. , 12. , 10. /
920 DATA (FANDAH( 87,J),J=1,10) /
$ 454.87 ,1066. ,1726.52 ,1108.2 ,233.1
$ 500000. ,1630000. , 28. , 12. , 14. /
DATA (FANDAH( 88,J),J=1,10) /
$ 553.85 ,920.47 ,1271.64 ,674.16 ,108.39
925 $ 650000. ,1770000. , 28. , 12. , 18. /
DATA (FANDAH( 89,J),J=1,10) /
$ 71.003 ,131.14 ,292.2 ,268.88 ,66.078
$ 500000. ,920000. , 30. , 9. , 2. /
DATA (FANDAH( 90,J),J=1,10) /
930 $ .6823 ,399.64 ,784.08 ,706.5 ,243.37
$ 500000. ,1220000. , 30. , 8. , 6. /
DATA (FANDAH( 91,J),J=1,10) /
$ 140.32 ,267.88 ,605.71 ,460.68 ,109.65
$ 500000. ,1490000. , 30. , 8. , 10. /
935 DATA (FANDAH( 92,J),J=1,10) /
$ 223.24 ,353.83 ,529.46 ,270.74 ,40.306
$ 500000. ,1770000. , 30. , 8. , 14. /
DATA (FANDAH( 93,J),J=1,10) /
$ -469.74 ,1952.01 ,2176.9 ,1114.75 ,216.07
940 $ 1000000. ,1770000. , 30. , 8. , 18. /
DATA (FANDAH( 94,J),J=1,10) /
$ -2790.78 ,7918.48 ,7719.83 ,3355.91 ,546.08
$ 1400000. ,1770000. , 30. , 8. , 22. /
DATA (FANDAH( 95,J),J=1,10) /
945 $ -2116.64 ,11988.3 ,24400. ,21818.2 ,7272.73
$ 600000. ,940000. , 30. , 10. , 2. /
DATA (FANDAH( 96,J),J=1,10) /
$ -155.27 ,1062. ,1749.99 ,1364.18 ,420.48
$ 600000. ,1260000. , 30. , 10. , 6. /
950 DATA (FANDAH( 97,J),J=1,10) /
$ 70.014 ,279.3 ,479.95 ,404.31 ,128.79
$ 600000. ,1530000. , 30. , 10. , 10. /
DATA (FANDAH( 98,J),J=1,10) /
$ 48.586 ,424.68 ,556.3 ,369.77 ,94.019
955 $ 600000. ,1870000. , 30. , 10. , 14. /
DATA (FANDAH( 99,J),J=1,10) /
$ 1838.82 ,4736.59 ,5146.6 ,2386.56 ,400.67
$ 1110000. ,1870000. , 30. , 10. , 18. /
DATA (FANDAH(100,J),J=1,10) /
960 $ 3840.5 ,8553.07 ,7718.76 ,3055.38 ,449.55
$ 1440000. ,1870000. , 30. , 10. , 22. /
DATA (FANDAH(101,J),J=1,10) /
$ 573.86 ,2682.76 ,5269.32 ,4489.9 ,1363.64
$ 600000. ,950000. , 30. , 11. , 2. /
965 DATA (FANDAH(102,J),J=1,10) /
$ 104.31 ,77.393 ,160.7 ,29.672 ,47.348
$ 600000. ,1280000. , 30. , 11. , 6. /
DATA (FANDAH(103,J),J=1,10) /
$ -156.28 ,1106.85 ,1431.07 ,844.31 ,197.5

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970      $ 600000. ,1560000. , 30. , 11. , 10. /
        DATA (FANDAH(104,J),J=1,10) /
        $ 109.35 ,142.38 , -19.254 , -15.095 , -2.55 ,
        $ 700000. ,1870000. , 30. , 11. , 14. /
        DATA (FANDAH(105,J),J=1,10) /
975      $ 1252.38 , -3070.33 , 3409.94 , -1571.34 , -255.69 ,
        $ 1040000. ,1870000. , 30. , 11. , 18. /
        DATA (FANDAH(106,J),J=1,10) /
        $ 6428.22 , -14958.5 , 13695. , -5504.54 , 821.78 ,
        $ 1450000. ,1870000. , 30. , 11. , 22. /
980      DATA (FANDAH(107,J),J=1,10) /
        $ -58.06 , 308.5 , 102.27 , -616.16 , 303.03 ,
        $ 600000. ,950000. , 30. , 12. , 2. /
        DATA (FANDAH(108,J),J=1,10) /
985      $ -272.45 , 1420.3 , -1840.91 , 1030.3 , -227.27 ,
        $ 600000. ,1290000. , 30. , 12. , 6. /
        DATA (FANDAH(109,J),J=1,10) /
        $ -107.44 , 844.15 , -980.16 , 527. , -119.46 ,
        $ 600000. ,1580000. , 30. , 12. , 10. /
        DATA (FANDAH(110,J),J=1,10) /
990      $ 172.04 , -75.343 , 334.05 , -244.14 , 48.077 ,
        $ 700000. ,1870000. , 30. , 12. , 14. /
        DATA (FANDAH(111,J),J=1,10) /
        $ 867.44 , -1854.72 , 2097.31 , -952.54 , 148.6 ,
        $ 1050000. ,1870000. , 30. , 12. , 18. /
995      DATA (FANDAH(112,J),J=1,10) /
        $ 642.55 , -1667.56 , 1862.69 , -928.03 , 170.45 ,
        $ 1000000. ,1620000. , 40. , 8. , 2. /
        DATA (FANDAH(113,J),J=1,10) /
1000     $ -234. , 926.78 , -837.06 , 339.56 , -55.0 ,
        $ 1000000. ,2160000. , 40. , 8. , 6. /
        DATA (FANDAH(114,J),J=1,10) /
        $ 59.02 , 212.2 , -81.972 , 14.603 , -2.878 ,
        $ 1000000. ,2570000. , 40. , 8. , 10. /
        DATA (FANDAH(115,J),J=1,10) /
1005     $ 420.1 , -453.47 , 450.55 , -159.26 , 18.324 ,
        $ 1200000. ,3040000. , 40. , 8. , 14. /
        DATA (FANDAH(116,J),J=1,10) /
        $ 502.08 , -434.25 , 352.16 , -95.755 , 7.843 ,
        $ 1700000. ,3320000. , 40. , 8. , 18. /
1010     DATA (FANDAH(117,J),J=1,10) /
        $ -256.24 , 1014.48 , -557.16 , 149.48 , -15.597 ,
        $ 2200000. ,3550000. , 40. , 8. , 22. /
        DATA (FANDAH(118,J),J=1,10) /
        $ 2370.11 , -7565.44 , 3025.59 , -3659.81 , 625.0 ,
1015     $ 1200000. ,1700000. , 40. , 10. , 2. /
        DATA (FANDAH(119,J),J=1,10) /
        $ -904.63 , 2572.63 , -2225.35 , 966.9 , -130.21 ,
        $ 1200000. ,2260000. , 40. , 10. , 6. /
        DATA (FANDAH(120,J),J=1,10) /
1020     $ 29.548 , 465.32 , -341.49 , 132.62 , -22.035 ,
        $ 1200000. ,2740000. , 40. , 10. , 10. /
        DATA (FANDAH(121,J),J=1,10) /
        $ -556.3 , 1461.13 , -834.02 , 221.53 , -23.765 ,
        $ 1270000. ,3180000. , 40. , 10. , 14. /
1025     DATA (FANDAH(122,J),J=1,10) /
        $ 621.15 , -428.07 , 299.22 , -60.185 , 1.457

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$ 1800000. ,3460000. , 40. , 10. , 18. /
  DATA (FANDAH(123,J),J=1,10) /
1030 $ 9055.63 , -11236.6 , 5513.37 , -1173.03 , 91.146 ,
$ 2500000. , 3740000. , 40. , 10. , 22. /
  DATA (FANDAH(124,J),J=1,10) /
$ -230.79 , 658.96 , -336.11 , 37.037 , 0.0 ,
$ 1200000. , 1720000. , 40. , 12. , 2. /
  DATA (FANDAH(125,J),J=1,10) /
1035 $ -254.45 , 908.1 , -574.62 , 157.2 , -18.939 ,
$ 1200000. , 2330000. , 40. , 12. , 6. /
  DATA (FANDAH(126,J),J=1,10) /
$ -151.19 , 779.21 , -444.03 , 119.08 , -14.569 ,
$ 1200000. , 2830000. , 40. , 12. , 10. /
1040 $ 543.7 , -459.81 , 452.62 , -152.95 , 16.208 ,
$ 1300000. , 3270000. , 40. , 12. , 14. /
  DATA (FANDAH(128,J),J=1,10) /
$ 1111.47 , -1181.9 , 794.01 , -202.17 , 16.754 ,
1045 $ 1850000. , 3610000. , 40. , 12. , 18. /
  DATA (FANDAH(129,J),J=1,10) /
$ -13201.1 , 17641.5 , -8397.4 , 1786.5 , -143.23 ,
$ 2540000. , 3750000. , 40. , 12. , 22. /
1050 $ -6179.5 , 17637.9 , -18314.6 , 8430.56 , -1458.33 ,
$ 1200000. , 1730000. , 40. , 14. , 2. /
  DATA (FANDAH(131,J),J=1,10) /
$ 227.15 , 112.24 , -105.4 , 60.29 , -16.572 ,
$ 1200000. , 2330000. , 40. , 14. , 6. /
1055 $ 181.38 , 234.11 , -57.838 , 7284 , -1.093 ,
$ 1200000. , 2370000. , 40. , 14. , 10. /
  DATA (FANDAH(133,J),J=1,10) /
$ -103.26 , 846.19 , -428.34 , 105.65 , -11.837 ,
1060 $ 1270000. , 3360000. , 40. , 14. , 14. /
  DATA (FANDAH(134,J),J=1,10) /
$ 754.94 , -702.92 , 618.55 , -182.21 , 16.936 ,
$ 1920000. , 3720000. , 40. , 14. , 18. /
1065 $ 1717.77 , -1161.5 , 466.83 , -55.358 , -8156 ,
$ 2540000. , 3750000. , 40. , 14. , 22. /
  DATA (FANDAH(136,J),J=1,10) /
$ -27.579 , 253.49 , -106.3 , 21.961 , -2.126 ,
$ 2000000. , 4250000. , 60. , 12. , 4. /
1070 $ -15.899 , 293.54 , -122.47 , 25.347 , -2.262 ,
$ 2000000. , 4750000. , 60. , 12. , 6. /
  DATA (FANDAH(138,J),J=1,10) /
$ 253.5 , -26.009 , 41.5 , -9.273 , 4242 ,
1075 $ 2000000. , 5220000. , 60. , 12. , 8. /
  DATA (FANDAH(139,J),J=1,10) /
$ 213.04 , 37.044 , 28.83 , -8.833 , 5606 ,
$ 2000000. , 3650000. , 60. , 12. , 10. /
1080 $ 417. , -96.1665 , 67.171 , -11.709 , 5361 ,
$ 2250000. , 5170000. , 60. , 12. , 12. /
  DATA (FANDAH(141,J),J=1,10) /
$ -750.05 , 915.56 , -243.21 , 30.626 , -1.576 ,

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1685      $ 3250000. ,6700000. , 60. , 12. , 14. /
        DATA (FANDAH(142,J),J=1,10) /
        $ -1403.86 ,1518.16 , -419.53 ,53.4 , -2.615 ,
        $ 4100000. ,7000000. , 60. , 12. , 16. /
        DATA (FANDAH(143,J),J=1,10) /
        $ 2257.4 , -1224.36 ,330.67 , -35. , 1.33 ,
1690      $ 4500000. ,7000000. , 60. , 12. , 18. /
        DATA (FANDAH(144,J),J=1,10) /
        $ -135.88 ,544.46 , -304.19 ,79.677 , -8.757 ,
        $ 2000000. ,3700000. , 60. , 16. , 2. /
        DATA (FANDAH(145,J),J=1,10) /
1695      $ -75.05 ,442.32 , -203.89 ,41.82 , -3.658 ,
        $ 2000000. ,4250000. , 60. , 16. , 4. /
        DATA (FANDAH(146,J),J=1,10) /
        $ 70.414 ,251.15 , -86.013 ,14.616 , -1.285 ,
        $ 2000000. ,4650000. , 60. , 16. , 6. /
1700      DATA (FANDAH(147,J),J=1,10) /
        $ -94.021 ,440.34 , -147.35 ,24.961 , -1.963 ,
        $ 2700000. ,5250000. , 60. , 16. , 8. /
        DATA (FANDAH(148,J),J=1,10) /
        $ -20.122 ,394.28 , -107.34 ,14.133 , -1.9016 ,
1705      $ 2000000. ,5930000. , 60. , 16. , 10. /
        DATA (FANDAH(149,J),J=1,10) /
        $ 502.56 , -132.39 ,102.93 , -19.495 , 1.03 ,
        $ 3170000. ,6370000. , 60. , 16. , 12. /
        DATA (FANDAH(150,J),J=1,10) /
1710      $ 390.34 ,84.842 ,12.235 , -3.344 , .0746 ,
        $ 2500000. ,7000000. , 60. , 16. , 14. /
        DATA (FANDAH(151,J),J=1,10) /
        $ -1499.49 ,1558.69 , -401.72 ,49.621 , -2.345 ,
        $ 4700000. ,7000000. , 60. , 16. , 16. /
1715      DATA (FANDAH(152,J),J=1,10) /
        $ 5656.16 , -3754.3 ,1080.28 , -133.41 , .6 ,
        $ 4200000. ,7000000. , 60. , 16. , 18. /
        DATA (FANDAH(153,J),J=1,10) /
        $ 1251.23 , -90.429 ,13.143 , 0.0 , 0.0 ,
1720      $ 5250000. ,7000000. , 60. , 16. , 22. /
        DATA P1 /3.14159265/
        DATA TAN8 /1.1465/, TAN19/.344/, HB/5./

C
C      SPECIFIC VOLUME OF AIR LEAVING THE HEAT EXCHANGER AT THE
1725      C      ELEVATION SPECIFIED FOR THE PLANT
C
        BARLN=1.39853-3.81835E-5*ELEV
        BAR=EXP(BARLN)
        SPVOL=(T4+459.67)/1.325/BAR

C
C      TOTAL VOLUMETRIC FLOW RATE OF THE FAN SYSTEM
C
        TOTCFM=W4*SPVOL/60.
        AFC=5.F08
1735      AC=0.
        AHP=0.
        ADIA=0.
        ABLN=0.
        AVEL=0.
1740      IF(LFE.LT.1) LFE = 153

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```

      IF(LFB.LT.1) LFB = 1
      C
      C
      C      START OF ITERATIVE LOOP FOR DETERMINING THE OPTIMUM FAN
      C      SYSTEM
      C
      C      DO 400 I=LFB,LFE
      C
      C      C      INITIALIZATION OF FAN OPTIMIZATION PARAMETERS
      C
      C      TP=0.
      C      RCFMPF=0.
      C      CFMPF=0.
      C      NOP=0
      C      HPPF=0.
      C      TOTHP=0.
      C      FCST=0.
      C      CMOT=0.
      C      CSR=0.
      C      CPL=0.
      C      TCSTPF=0.
      C      TCSTF=0.
      C      VEL=0.
      C      CINC=80000.
      C      CFM=400000.
      C      FLOVP=n.
      C      TP=0.
      C      DF=0.
      C      CI=0.
      C
      C      CROSS-SECTIONAL FLOW AREA FOR THE FAN DEPENDING ON THE FAN
      C      DIAMETER
      C
      C      IF(I.LE.27) A=429.08
      C      IF(I.GT.27.AND.I.LE.54) A=495.96
      C      IF(I.GT.54.AND.I.LE.88) A=584.51
      C      IF(I.GT.88.AND.I.LE.111) A=658.37
      C      IF(I.GT.111.AND.I.LE.135) A=1123.91
      C      IF(I.GT.135) A=2680.4
      C
      C      DETERMINE THE NUMBER FANS, THE VOLUMETRIC FLOW RATE THROUGH
      C      EACH FAN, AND THE TOTAL PRESSURE DROP ACROSS EACH FAN
      C
      C      K=0
      C      50 CONTINUE
      C      K=K+1
      C      IF(K.GT.100) GO TO 59
      C
      C      THE PRESSURE DIFFERENTIAL ACROSS EACH FAN IS DEPENDENT UPON
      C      THE METHOD OF AIR DISCHARGE FROM THE FAN, WITH OR WITHOUT
      C      VELOCITY RECOVERY STACKS
      C      VELREC=0      NO VELOCITY RECOVERY
      C      VELREC=1      VELOCITY RECOVERY
      C
      C      THE VELOCITY RECOVERY IS BASED ON 13 FT HIGH STACKS WITH
      C      8 DEGREE SIDES AND FOR A 28 FT DIAMETER FAN THE EFFECTIVE-
      C      NESS OF THE STACK HAS BEEN TAKEN TO BE 80 PERCENT

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      C      AIR VELOCITY EXCITING THE FAN OR STACK
1200      IF(VELREC.EQ. 0.) VEL=CFM/60./A
      FAND= FANDAP(I,8)
      IF(VELREC.EQ.1.) VEL=CFM/60./((FAND+2.*13./28.*FAND*.14054)**2.*4./
      *3.1416
      FLOVP=CFM/1000000.
1205      IF(VELREC.EQ. 0.) VP=VEL**2/4452.852
      IF(VELREC.EQ. 1.) VP=0.2*((CFM/60./A)**2/4452.852+4.*VEL**2/4452.
      *852)

      C      TOTAL PRESSURE DIFFERENTIAL ACROSS THE FAN
      C      TP=OPTINW*.07495*SPVOL*VP
1210      C      CHECK IF PRESSURE DIFFERENTIAL AND VOLUMETRIC FLOW RATE ARE
      C      WITHIN SPECIFIED LIMITS
      C      IF(TP.GT.FANDAP(I,7)) GO TO 52
      IF(CFM.GT.FANDAH(I,7)) GO TO 54
1215      IF(CFM.LT.FANDAH(I,5)) GO TO 55
      IF(TP.LT.FANDAP(I,6)) GO TO 55
      IF(VP.GT.FANDAP(I,6)) GO TO 54

      C      CALCULATION OF VOLUMETRIC FLOW RATE THROUGH THE FAN FOR THE
      C      SPECIFIED PRESSURE DIFFERENTIAL ACROSS THE FAN
1220      RCFMPF=FANDAP(I,1)+FANDAP(I,2)*TP+FANDAP(I,3)*TP**2+FANDAP(I,4)*
      *TP**3+FANDAP(I,5)*TP**4

      C      SELECTION OF A VOLUMETRIC FLOW RATE TO CLOSER MATCH THE
      C      REQUIRED PRESSURE DIFFERENTIAL ACROSS THE FAN
1225      DF=RCFMPF-FLOVP
      IF(ABS(DF).LE.0.01) GO TO 57
      CI=1.+DF/RCFMPF
      IF(CI.GT.1..AND.CI*CFM.GT.(CFM+CINC)) GO TO 55
1230      IF(CI.LT.1..AND.CI*CFM.LT.(CFM-CINC)) GO TO 54
      CFM=CFM*CI
      GO TO 50
      55 CFM=CFM+CINC
      GO TO 50
1235      54 CFM=CFM-CINC
      GO TO 50
      59 CONTINUE
      GO TO 400
      62 CONTINUE
      GO TO 400
1240      57 CFMPF=RCFMPF*1000000.

      C      CALCULATION OF THE NUMBER OF FANS IN THE FAN SYSTEM
      C      NOF=TOTCFM/CFMPF
1245      IF(CFMPF.LT.FANDAH(I,6).OR.CFMPF.GT.FANDAH(I,7)) GO TO 400
      HPPF=FANDAH(I,1)+FANDAH(I,2)*RCFMPF+FANDAH(I,3)*RCFMPF**2+FANDAH(I
      *.4)*RCFMPF**3+FANDAH(I,5)*RCFMPF**4
      HPPF=HPPF/.07495/SPVOL

1250      C      CALCULATION OF HORSEPOWER REQUIREMENTS OF EACH FAN
      C      HPPF = HPPF/GBEFF
      C

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1255      C      CALCULATION OF THE NUMBER OF CIRCULAR TOWERS BASED ON AN
      C      ALLOWABLE FAN PACKING FACTOR
      C
      TOWN = (WIDTH * CDANG / (PI * FANDAP(I,8))) **2 / (NOF * PFACT)
1260      ITOWN = TOWN
      IF (ITOWN .LT. ITMIN) GOTO 400
      IF (ITOWN .GT. ITMAX) GOTO 400

      C      CALCULATION OF THE DIAMETER OF THE TOWERS
      DTOW = WIDTH * CDANG / (PI * ITOWN)

1265      C      FAN ELECTRICAL WIRING COSTS
      C
      VM=2300.
      IF (HPPF .LT. 250.) VM = 480.
      IF (HPPF .GT. 2000.) VM = 6900.
      DPTWR = DIST
      DTTSG = DTOW / 4. * (ITOWN*(3./2.) + 1.)
      DSGTM = DTOW / 2. + DTTSG / 2.
1270      IF (HPPF .LT. 251.) TRMA = 225000./NOF + 7.88*HPPF + (116. - .159
      S      * HPPF) * HPPF
      IF (HPPF .GE. 251.) TRMA = 225000./NOF + 7.88*HPPF +
      S      870./SQRT(HPPF) * HPPF
      VS = 7200.
      IF (HPPF .LT. 2000.) VS = 13900.
1280      TRMB = (DPTWR+DTTSG-1000.) * (37. + .47*HPPF*NOF / SQRT(VS)
      S      + .5 * NOF) / NOF
      TRMC = (100. + 1.1*HPPF) * (DSGTM-250.) / SQRT(VM)
      CSR = HPPF * 55. + HPPF** 1.5 + 1000.
      FANLEC = TRMA + TRMB + TRMC

1285      C      FAN MOTOR COSTS
      C
      FMC = 26.62
      IF (HPPF .GT. 300.) FMC = 24.33.
1290      BIGMC = 0.0
      IF (HPPF .GT. 300.) BIGMC = 9000.
      CMOT = HPPF * FMC + BIGMC

      C      TOTAL HORSEPOWER REQUIREMENT OF THE FAN SYSTEM
1295      70 TOTHP=HPPF*NOF

      C      CAPITAL COSTS OF THE FAN
      C
1300      IF (I.LT.88) FCST=FANDAP(I,9)*(22.4+FANDAP(I,8)*60.)+19.2*FANDAP(I,8
      S      *)
      IF (I.GE.88) FCST=FANDAP(I,9)*(51.2*FANDAP(I,8)*950.)+135.6*FANDAP(I
      S      *,8)*2700.
      EFCSF = 1.05
1305      FCST = FCST * EFCSF
      SAAFI = 1.15
      HFR = 13. / 28. * FAND

      C      STACK COSTS WITH VELOCITY RECOVERY
1310      IF (VELREC.EQ.1.) CFROS= UCS * U S * PI * (FAND*HFR*TAN8 + HFR
      S      * SQRT(1. + TAN8**2)

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S      + UCS * UWS * PI * (FAND*HB*TAN19) * HB
S      * SQRT(1. + TAN19**2)
1315  C      STACK COSTS WITH OUT VELOCITY RECOVERY
C      IF(VELDEC.EQ.0.) CFROS = CVM * WFM * PI * FAND**2 / 6.
S      + UCS * UWS * PI * (FAND * HB * TAN19) * HB
S      * SQRT(1. + TAN19**2)
1320  C      INCREASING THE FAN COSTS TO TAKE INTO ACCOUNT FOR SHIPPING
C      AND ASSEMBLY OF FAN SYSTEM COMPONENTS
C      CFROS = CFROS * SAAF * POHFAN
C      FCST = POHFAN * SAAF * FCST
1325  C      CSR = POHFAN * SAAF * CSR
C      CMOT = CMOT * POHFAN * SAAF
C      FANLEC = FANLEC * POHLEC
C      TOTAL CAPITAL COST OF THE FAN SYSTEM
C      TCSTF = FCST + CMOT + CSR + FANLEC + CFROS
1330  C      TCSTF = TCSTF * NOF
C      ANNUAL COST OF THE FAN SYSTEM
C      ANFCOS=(TCSTF*TOTHF**7457*PLANC)*FCR+EHR*FCOS/10**8*TOTHF*
1335  C      $.7457*CAPE*8760.
C      COST OF PLENUM
C      CPL = CPM * WPL * (ITOWN * PI/4. * DTOW**2 - NOF * PI/4. * (FAND*3.5)
1340  C      **2)
C      CPL=CPL * POHSTC
C      STRUCTURAL AND FOUNDATION COSTS OF THE CIRCULAR TOWER
C      STRUCC = .2458 * (PI*DTOW**2/4.) * ELENG * ITOWN
C      * (.00635 * ROOFL + .725)
1345  C      STRUCC = STRUCC * POHSTC
C      FNDC = .019 * (WHX+WATERW) * .92*(PI/4.)*DTOW**2*ITOWN
C      FNDC = FNDC * POHSTC
1350  C      ANNUAL FAN, STRUCTURAL AND FOUNDATION COSTS
C      ANSFPC = (CPL + STRUCC + FNDC) * FCR
C      ANSEPF = ANSFPC + ANFCOS
1355  C      STORAGE OF DESIGN PARAMETERS FOR THE LEAST COST FAN SYSTEM TO
C      TO BE PRINTED OUT BY THE SUBROUTINE RPTFAN
C
1360  150 IF (ANSEPF .GT. AFC) GOTO 400
C      AFC = ANSEPF
C      AFCH = ANFCOS
C      AC=TCSTF
C      AHP=TOTHF
C      ADIA=FANDAP(I,8)
1365  C      ARLN=FANDAP(I,9)
C      RLDANG=FANDAP(I,10)
C      XNFAN=NOF
C      NUMTOW = ITOWN

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1370      CTOWD = DTOW
         AVEL=VEL
         CFPERF=CFMPF
         HPPERF=HPPF
         TOTCF=TOTCFM
         FRCPF = FCST
1375      FMCPF = CMOT + CSR
         CPLEN=CPL
         CYLRNG = CPROS
         HPAIR=TOTHP
         FPOW=TOTHP/1.341
1380      DPFEL=(VP/(.07495*SPVOL))*5.2022
         DPHX = DPTINW * 5.20218 / 144.
         HUNDIA = SQRT (ADIA**2 + 4.*A/3.14159)
         TCTPF = TCSTPF
         FDCPF = FCST
1385      FMTRC = CMOT
         ACCTTP= (DPTINW + VP/(.07495*SPVOL)) * 5.2018/144.
         CFANEL = FANLEC
         ADJTP = TP * 5.20218/144.
         ACT3PD = DPHX
1390      ADJ3PO = DPHX * .07495*SPVOL
         ACTVH = DPFEL/144.
         ADJVH = VP * 5.20218 / 144.
         ADJPPF = HPPF * SPVOL * .07495
         THPAIR = HPAIR
1395      TCTFI = AC
         AFCST = AFCH
         CSRD = CSR
         400 CONTINUE
         RETURN
1400      END

```

SUBROUTINE FRICHO(FAIR,H0,ODL,XW,XD,XDG,GAIR,I)

THIS VARIATION TO SUBROUTINE FRICHO CALCULATES THE
FRICTION FACTOR AND HEAT TRANSFER COEFFICIENT FOR AIR FLOW
THROUGH A BANK OF PLASTIC HEAT EXCHANGER TUBES.

DEFINITION OF I

1 - MCADAMS RELATIONSHIPS FOR THE HEAT TRANSFER
COEFFICIENT AND FRICTION FACTOR THROUGH A BANK OF
STAGGERED BARE TUBES

2 - ZUKAUSKAS RELATIONSHIP FOR HEAT TRANSFER
COEFFICIENTS AND MCADAMS FRICTION FACTOR
RELATIONSHIP FOR A BANK OF STAGGERED TUBES

3 - ZUKAUSKAS HEAT TRANSFER COEFFICIENT AND MCADAMS
FRICTION FACTOR RELATIONSHIPS FOR IN LINE BARE
TUBES

DEFINITION OF VARIABLES

AMU - VISCOSITY OF AIR (LBM/FT-HR)
CP - SPECIFIC HEAT OF AIR (BTU/LBM DEG F)
FAIR - AIR SIDE FRICTION FACTOR FOR BARE TUBES (DIMENSION-
LESS)
GAIR - MASS FLUX OF AIR THROUGH MINIMUM CROSS-SECTIONAL
FLOW AREA (LBM/SQ FT-HR)
H0 - AIR SIDE HEAT TRANSFER COEFFICIENT (BTU/HR SQ FT
DEG F)
ODL - OUTSIDE DIAMETER OF THE PLASTIC TUBES (IN)
PRANTL - AIR SIDE PRANDTL NUMBER (DIMENSIONLESS)
RATIO - RATIO OF TRANSVERSE TO LONGITUDINAL PITCH OF THE
TUBES
REAIR - AIR SIDE REYNOLDS NUMBER BASED ON THE MINIMUM
CROSS-SECTIONAL FLOW AREA AND OUTSIDE DIAMETER
OF THE TUBES
THCONA - THERMAL CONDUCTIVITY OF AIR (BTU/HR-FT-DEG F)
XD - LONGITUDINAL PITCH OF TUBES PARALLEL TO AIR FLOW
XL - RATIO OF LONGITUDINAL PITCH TO THE OUTSIDE
DIAMETER OF THE TUBES
XT - RATIO OF TRANSVERSE PITCH TO THE OUTSIDE DIAMETER
OF THE TUBES
XW - TRANSVERSE PITCH OF TUBES NORMAL TO AIR FLOW

PROPERTIES OF AIR AT 100 DEGREES F

AMU = 0.04594
CP = 0.2406
THCONA = 0.01566

FLOW CONDITIONS

ODLF = ODL/12.0
PRANTL = AMU*CP/THCONA
REAIR = ODLF*GAIR/AMU

TRANSVERSE AND LONGITUDINAL PITCHES

```

C
C      XT = XW/ODL
60      XLI = XL/ODL
      RATIO = XT/XL
C
C****    AIR SIDE FRICTION FACTOR - EQUATIONS 6-13A AND B MCADAMS
C          "HEAT TRANSMISSION" THIRD EDITION
65      C
C          BRANCH POINT FOR STAGGERED AND INLINE TUBE ARRANGEMENTS
      GO TO (5,5,7)I
C
C          STAGGERED TUBE FRICTION FACTOR
70      5 CONTINUE
      FAIR = (0.250 + 0.1175/(XT - 1.0)**1.08)/(REAIR**0.16)
      GO TO 11
C
C          INLINE TUBE FRICTION FACTOR
75      7 VALUE = 0.430 + (1.13/XL)
      FAIR = (0.044 + 0.080*XL/(XT - 1.0)**VALUE)/(REAIR**0.15)
C
C****    AIR SIDE HEAT TRANSFER COEFFICIENT MCADAMS AND ZUKAUSKAS
C          CORRELATIONS
80      C
C          BRANCH POINT FOR STAGGERED AND INLINE TUBE ARRANGEMENT
      8 GO TO (10,20,60)I
C
C          STAGGERED TUBE ARRANGEMENT, EQUATION 10-11A MCADAMS "HEAT
85      TRANSMISSION" THIRD EDITION
      10 HO = 0.33*(REAIR**0.60)*(PRANTL**0.3333)*THCONA/ODLF
      RETURN
C
C          STAGGERED TUBE ARRANGEMENT, EQUATIONS 39, 40, AND 41 A.
90      ZUKAUSKAS "HEAT TRANSFER FROM TUBES IN CROSSFLOW"
C
      20 IF (REAIR .LT. 10.0) RETURN
      IF (REAIR .GT. 100.0) GO TO 30
C
      REYNOLDS NUMBER GREATER THAN 10 BUT LESS THAN 100
95      HO = 0.90*(REAIR**0.40)*(PRANTL**0.36)*THCONA/ODLF
      RETURN
C
C          REYNOLDS NUMBER GREATER THAN 100 AND LESS THAN 1000
100      30 IF (REAIR .GT. 1000) GO TO 40
      IF (RATIO .GT. 2.) GOTO 35
      XC = .3755 + 100.*(-.2*ALOG10(RATIO))
      XM = .5898 + .2*ALOG10(RATIO)
C
C          RATIO OF TRANSVERSE TO LONGITUDINAL PITCH LESS THAN 2
105      HO = XC * REAIR**XM * PRANTL**.35 * THCONA / ODLF
      RETURN
C
C          RATIO OF TRANSVERSE TO LONGITUDINAL PITCH GREATER THAN 2
110      35 HO = .5875 * REAIR**.6479 * PRANTL**.36 * THCONA / ODLF
      RETURN
C
C          REYNOLDS NUMBER GREATER THAN 1000 AND LESS THAN 2*00E05
      40 CONTINUE

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```

115      IF(RATIO .GT. 2.00) GO TO 50
      C
      C      RATIO OF TRANSVERSE TO LONGITUDINAL PITCH LESS THAN 2
      HO = 0.35*(RATIO**0.20)*(REAIR**0.60)*(PRANTL**0.36)*THCONA/ODLF
      RETURN
120      C
      C      RATIO OF TRANSVERSE TO LONGITUDINAL PITCH GREATER THAN 2
      50 HO = 0.40*(REAIR**0.50)*(PRANTL**0.36)*THCONA/ODLF
      RETURN
125      C
      C      INLINE TUBE ARRANGEMENT, EQUATIONS 38, 38, AND 42. A
      C      ZUKAUSKAS "HEAT TRANSFER FROM TUBES IN CROSSFLOW"
      C
      60 IF(REAIR .LT. 10) RETURN
      IF(REAIR .GT. 100) GO TO 70
130      C
      C      REYNOLDS NUMBER GREATER THAN 10 AND LESS THAN 100
      HO = 0.90*(REAIR**0.40)*(PRANTL**0.350)*THCONA/ODLF
      RETURN
135      C
      C      REYNOLDS NUMBER GREATER THAN 100 AND LESS THAN 1000
      70 IF(REAIR .GT. 1000.0) GO TO 80
      HO = 0.293*(REAIR**0.618)*(PRANTL**0.360)*THCONA/ODLF
      RETURN
140      C
      C      REYNOLDS NUMBER GREATER THAN 1000 AND LESS THAN 2.00E05
      80 IF(REAIR .GT. 2.00E05) GO TO 90
      HO = 0.270*(REAIR**0.630)*(PRANTL**0.360)*THCONA/ODLF
      RETURN
145      C
      C      REYNOLDS NUMBER GREATER THAN 2.00E05
      90 HO = 0.021*(REAIR**0.84)*(PRANTL**0.36)*THCONA/ODLF
      RETURN
      END

```

SUBROUTINE HEADER(GPMHDR,NBRANCH,BRCHGPM,RED,NN,J,DIA,REDCOST,
TEECOST,ELCOST,UPIPCST,VELO,EUCOST,FLGCST,DESVEL)

5

THIS SUBROUTINE DETERMINES DESIGN AND COST INFORMATION FOR
THE MAIN CIRCULATION PIPING AND THE QUADRANT PIPING.

DEFINITION OF VARIABLES

10

APIPCST - ABOVE GROUND PIPE COST (\$1000/FT)

BRCHCST - PORTION OF THE COST OF A TEE ATTRIBUTED TO THE
BRANCH (\$1000)

BRCHDIA - DIAMETER OF DISTRIBUTION PIPING. DIAMETER OF
BUNDLE FITTINGS (INCHES)

15

BRCHGPM - FLOW RATE TO CIRCULAR TOWER OR TUBE BUNDLE (GPM)

DESVEL - PIPING SYSTEM WATER DESIGN VELOCITY (FT/SEC)

DIA - PIPE COMPONENT DIAMETER (INCHES)

EJCOST - EXPANSION JOINT COST (\$1000)

ELCOST - 90 DEGREE ELBOW COST (\$1000)

20

FLGCST - FLANGE COST (\$1000)

GPMHDR - INITIAL FLOW INTO HEADER (GPM)

GPMREM - FLOW IN A HEADER SECTION (GPM)

IPRESS - PIPE COMPONENT DESIGN PRESSURE (PSI)

NFL - UPPER LIMIT FOR NUMBER OF TOWERS OR TUBE BUNDLES
PER QUADRANT

25

NFS - NUMBER OF POSITIONS IN UNIT COST ARRAYS. MUST
MATCH NUMBER OF POSITIONS IN DIAM ARRAY

NN - IF=0 THEN MAIN CIRCULATION HEADER IS DESIGNED
IF=1 THEN QUADRANT HEADER IS DESIGNED

30

PIPCST - BELOW GROUND PIPE COST (\$1000/FT)

RED - ALLOWABLE REDUCTION IN DIAMETER BETWEEN ADJACENT
HEADER SECTIONS (INCHES). IF RED=0 THE PROGRAM
CALCULATES THE REDUCTION

REDCOST - REDUCER COST (\$1000)

35

REDUCT - REDUCTION IN DIAMETER BETWEEN ADJACENT HEADER
SECTIONS (INCHES). ONLY USED WHEN RED=0

TEECOST - TEE COST (\$1000)

UPIPCST - UNIT PIPE COST (\$1000/FT)

VACST - VALVE COST (\$1000), VALVES ARE MOTOR OPERATED
BUTTERFLY VALVES

40

VELO - TRUE VELOCITY IN PIPE, ALWAYS LESS THAN
DESVEL (FT/SEC)

COMMON /CPIPE / APIPCST(23), DIAM(23), EJCST(23), ELCST(23)
\$, FLGCST(23)

45

\$, EL45(23), PIPICST(23), REDCST(23), TEECST(23), VACST(23)

COMMON /PRESS/ IPRESS

DIMENSION VELO(200)

DIMENSION DIA(200), REDCOST(200), TEECOST(200), UPIPCST(200)

50

LOGICAL CALL 1

DATA DIAM/12.,18.,24.,30.,35.,42.,48.,54.,60.,66.,72.,78.,84.,
90.,96.,102.,108.,114.,120.,126.,132.,138.,144.,

DATA FLGCST/.342,.618,.893,1.145,1.398,1.934,2.471,3.219,3.966,
\$5.53,7.134,9.815,12.496,14.725,16.954,20.455,23.956,25.61,27.264,
\$28.918,30.572,32.226,33.98/

55

DATA EJCST/.56,1.11,1.66,2.172,2.685,4.242,5.8,7.242,8.685,
\$10.072,11.46,13.955,16.45,19.845,23.24,26.93,30.62,34.14,37.66,
\$41.19,44.7,48.22,51.74/

```

60      DATA REDCST/.7,.8,.9,1.3,1.55,2.0,4.65,5.45,6.3,7.1,9.5,11.5,
      $13.5,15.5,17.5,19.3,45.5,60.7,73.0,87.0,101.1,114.1,127.7/
      DATA TEECST/.882,2.048,3.215,3.843,4.472,5.1,9.9,16.156,22.41,
      $28.561,37.261,42.1,46.944,51.785,65.968,71.104,2.117,5.131,25.
      $144.1,159.1,170.1,185.7/
      DATA PIPCST/.115,.15,.185,.225,.26,.295,.42,.465,.51,.555,.665,
      $5.71,.75,.795,.94,.99,1.28,1.335,1.39,1.445,1.505,1.555,1.61/
65      DATA AIPCST/.072,.100,.122,.148,.172,.198,.299,.328,.360,.390,
      $1.495,.525,.555,.585,.714,.745,1.023,1.070,1.11,1.15,1.19,1.23,
      $21.27/
      DATA ELCST/.638,1.34,2.04,2.50,3.15,3.71,8.03,14.2,20.4,26.5,
70      $134.1,39.4,44.6,49.8,64.9,70.2,102.1,116.1,129.1,143.1,157.1,171.1,185.7/
      DATA CALL 1 /.TRUE./
      C
      DATA NFS/23/, NFLV200/
      C
      C
75      C      CALL THE APPROPRIATE SUBROUTINE TO ESTABLISH UNIT COST DATA
      C      FOR THE PIPING SYSTEM COMPONENTS.
      C
      IF (CALL 1 .AND. IPRESS .EQ. 50) CALL P50
      IF (CALL 1 .AND. IPRESS .EQ. 75) CALL P75
80      IF (CALL 1 .AND. IPRESS .EQ. 125) CALL P125
      CALL I = .FALSE.
      DO 24 I=1,NFL
      REDCST(I)=0.
      TEECST(I)=0.
85      24 CONTINUE
      ELCST=0.
      FLGCST=0.
      C
      C      THE INITIAL CONDITION IS TO HAVE THE FLOW REMAINING IN THE
90      C      HEADER (GPMREM) EQUAL TO THE FLOW THAT ENTERS THE HEADER
      C      (GPMHDR).
      C
      GPMREM=GPMHDR
      ELCST=0.
95      CONST1=(3.1416/4.)*7.481*60.*DESVEL
      CONST2=(4./3.1413)*144.7/(60.*7.481)
      C
      C      IF NN=1 THE QUADRANT HEADERS ARE BEING SPECIFIED. THE CALC-
      C      ULATION OF BRANCH DIAMETER IS BY-PASSED BECAUSE THE BRANCH,
100      C      IN THIS CASE THE PIPE CONNECTING THE QUADRANT HEADER TO THE
      C      BRINLE HEADER, IS FIXED AT 8 INCHES DIAMETER. OTHERWISE, THE
      C      BRANCH DIAMETER IS THE DIAMETER OF THE DISTRIBUTION PIPING.
      C      THIS CALCULATION IS USED TO GET THE INDEX II TO DETERMINE THE
      C      BRANCH TEE COST (BRCHCST) BELOW.
105      C
      IF (NN.EQ.1) GO TO 23
      BRCHDIA=SQRT(BRCHGPM/CONST1)*12.
      IF (BRCHDIA.LT.DIAM(1)) BRCHDIA=DIAM(1)
      DO 10 I=1,NFS
110      II = I
      IF (BRCHDIA-DIAM(II)) 11,11,10
      10 CONTINUE
      11 BRCHDIA=DIAM(II)
      23 J=1

```

```

115      C      THE LOOP INCLUDING STATEMENTS 22 TO 21 DESIGNS AND COSTS THE
      C      COMPONENTS OF EACH HEADER SECTION.
      C
      C      COMPUTE THE REQUIRED PIPE DIAMETER FOR HEADER SECTION J BASED
120      C      ON THE FLOW REMAINING (GPMREM) AND THE DESIGN VELOCITY
      C      (DESVEL). THE DIAMETER ASSIGNED TO HEADER SECTION J IS THE
      C      NEXT LARGEST DIAMETER, IN 6 INCH INCREMENTS, FROM THE DIA-
      C      METER ARRAY, DIAM, IN SUBROUTINES P50, P75, OR P125.
      C
125      22 DIA(J)=SQRT(GPMREM/CONST1)*12.
      DO 12 I= 1,NFS
      I = I1
      IF(DIA(J)-DIAM(I))13,13,12
130      12 CONTINUE
      13 DIA(J)=DIAM(I)
      C
      C      THE MAIN CIRCULATION HEADER HAS AN EXPANSION JOINT AND
      C      APPROPRIATE FLANGES AT THE CONDENSER INLET AND OUTLET.
      C
135      IF(J.EQ.1 .AND. NN.NE.1) EJCOST=EUCST(I)
      IF(J.EQ.1 .AND. NN.NE.1) FLGCOST=3.*FLGCST(I)
      C
      C      IN THE STATEMENTS THROUGH STATEMENT 17 THE REDUCTION IN
      C      HEADER PIPE SIZE IS SPECIFIED. THE REDUCER COST IS DETER-
140      C      MINED. THE INDEXES USED TO DEFINE THE ARRAY POSITIONS FOR
      C      OTHER COMPONENT COSTS ARE DETERMINED.
      C
      C      IF A REDUCER IS COSTED FOR HEADER SECTION J IT IS INCLUDED IN
      C      THE COSTS FOR HEADER SECTION J-1. ITS LARGER DIAMETER WILL
145      C      BE THAT OF HEADER SECTION J-1. THE COST OF A REDUCER IS
      C      BASED ON ITS LARGER DIAMETER.
      C
      C      FOR J=1 THIS ROUTINE IS BY-PASSED BECAUSE THE FIRST HEADER
      C      WILL NOT HAVE A REDUCER PRECEDING IT.
150      C
      IF(J.EQ.1) GO TO 15
      C
      C      THE PROGRAM MAY HAVE A SPECIFIED VALUE OF RED WHICH FIXES THE
      C      REDUCTION IN PIPE DIAMETERS BETWEEN HEADER SECTIONS. RED
155      C      MUST BE A MULTIPLE OF 6. IF RED=0 THE ROUTINE CALCULATES A
      C      REDUCTION. FOR EXAMPLE, HEADER SECTION J-1 HAS BEEN ASSIGNED
      C      A DIAMETER OF 96 INCHES. IT IS DETERMINED THAT HEADER SECTION
      C      J SHOULD BE 84 INCHES. THE REQUIRED REDUCTION IS 12 INCHES.
160      C      IF RED=0 THEN A 96 INCH REDUCER IS COSTED AND HEADER SECTION
      C      J WILL BE ASSIGNED A DIAMETER OF 84 INCHES. IF RED=6 INCHES
      C      A 96 INCH REDUCER IS COSTED BUT DIAMETER J WOULD BE ASSIGNED
      C      A VALUE OF 90 INCHES. IF RED=12 INCHES THEN A 96 INCH RE-
      C      DUCER IS COSTED AND DIAMETER J IS ASSIGNED A VALUE OF 84
165      C      INCHES. IF RED=18 INCHES OR MORE THEN NO REDUCER IS SPECI-
      C      FIED AND DIAMETER J IS ASSIGNED A VALUE OF 96 INCHES. LARGER
      C      VALUES OF RED RESULT IN PIPE SIZES LARGER THAN REQUIRED BUT
      C      FEWER REDUCERS ARE REQUIRED.
      C
      IF(RED.NE.0.) GO TO 14
170      IF (ABS(DIA(J)-DIA(J-1)).LT.0.1) GO TO 15
      C

```

```

C      CALCULATION OF REDUCTION, RED NOT SPECIFIED.
C
175      REDUCT=DIA(J-1)-DIA(J)
          M = REDUCT/6. + .01
          IU = I
          GO TO 14
C
180      RED SPECIFIED, POSSIBLE REASSIGNMENT OF DIAMETER J.
C
          14 IF (DIA(J)-0.1*GT-DIA(J-1)-RED) GO TO 17
              DIA(J)=DIA(J-1)-RED
              M = RED / 6. + .01
              IU = I + (DIA(J) - DIAM(I)) / 6. + .01
185
C      DETERMINE REDUCER COST. IT HAS BEEN ASSUMED FROM THE RE-
C      DUCER COST DATA THAT, FOR EXAMPLE, A 96 INCH REDUCER WILL
C      COST THE SAME WHETHER THE REDUCTION IS TO 90, 84, OR 78
C      INCHES. IF THE TOTAL REDUCTION BETWEEN ADJACENT HEADER
190      SECTIONS EXCEEDS 18 INCHES THEN AN ADDITIONAL REDUCER MUST BE
C      COSTED. IN THE EXAMPLE, THIS WOULD BE A 78 INCH REDUCER. IF
C      THE TOTAL REDUCTION EXCEEDS 36 INCHES, SAY 96 TO 54, THEN A
C      96, 78, AND 60 INCH REDUCER WOULD BE COSTED, AND SO ON.
C
195      16 K=0
          JJ=M
          IF (JJ + IU .GT. NFL) J=2*NFL
          IF (J.GT.NFL) RETURN
200      18 REDCOST(J-1) = REDCOST(J-1) + REDCOST(IJ+JJ)
          K=K+1
          JJ=M-3*K
          IF (JJ.LE.0) GO TO 15
          GO TO 18
205      17 DIA(J)=DIA(J-1)
          15 M = (DIA(J) - DIAM(I))/6. + .01
C
C      DETERMINE TEE COSTS. IF THE LAST HEADER SECTION IS BEING
C      DESIGNED THEN USE AN ELBOW RATHER THAN A TEE. THE TEE COST
C      IS ASSUMED TO BE .67* THE COST OF A TEE OF THE "RUN" DIAMETER
210      PLUS .33* THE COST OF A TEE OF THE "BRANCH" DIAMETER. THE 9
C      INCH BRANCH DIAMETER CONNECTING THE QUADRANT HEADER TO THE
C      BUNDLE HEADER IS NOT AN ARRAY VALUE. BRCHCST IS ASSIGNED A
C      VALUE OF $200.
C
215      IF (M + I .GT. NFL) J=2*NFL
          IF (J .GT. NFL) RETURN
          IF (ABS(GPMPEM-BRCHGPM).LT.0.01) GO TO 19
          IF (VN .NE. 1) BRCHCST = TEECST(II) * .33
          IF (VN.EQ.1) BRCHCST=.2
220      TEECOST(J)=TEECOST (I+M)*0.67+BRCHCST
C
C      MAIN CIRCULATION PIPING IS UNDERGROUND. QUADRANT PIPING IS
C      ABOVE GROUND. FITTINGS COSTS WERE NOT DEPENDENT ON ABOVE OR
C      BELOW GROUND SPECIFICATION.
225
          GO TO 20
          19 ELCOST=ELCOST(I+M)
          20 IF (VN .NE. 1) UPIPCST(J) = PIPICST(I+M)

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```
230      C      SUBTRACT OUT THE FLOW TO ONE BRANCH FROM THE FLOW IN THE
      C      HEADER. IF NO FLOW REMAINS THEN THE LAST HEADER SECTION HAS
      C      BEEN DESIGNED. THERE ARE FINALLY J SECTIONS IN THE HEADER.
      C
      IF(NN.EQ.1) UPIPCST(J)=APIPCST(I+M)
535      VELO(J)=(GPMREM/DIA(J)**2)*CONST2
      GPMREM=GPMREM-BRCHGPM
      IF (GPMREM.LE.1.0) GO TO 21
      J=J+1
      IF (J.GT.NFL) RETURN
240      GO TO 22
21 CONTINUE
      RETURN
      END
```

SUBROUTINE INPSUM

C
C
C

THIS ROUTINE REPORTS INPUT SUMMARY AND CASE DESCRIPTION

5

LOGICAL FIRST, FXTMP
COMMON

\$ AFTR, ALPHA

\$ CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAP

\$ CRJ, CSEALP, CELAST, CFS, COANG, CLUVR, CHAILS, CVM

10

\$ DEEP1, DESVEL, DANGLE

\$ EEPF

\$ FOR, FIRST, FIXL, FCOS, FXTMP

\$ GREFF

\$ HXVP, HPCST

15

\$ IHEAT

\$ ITAX, ITVIN

\$ JCONS

\$ KCONV, KALEXT

\$ MXEXT

20

\$ NTUCAL(2), NTA

COMMON

\$ ODR

\$ PSIZE, PER, PWCOS, PLANC, PFACT

\$ POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSLC

25

\$ QREJ, QREDUCF

\$ R3P, REDUCE, ROESEL, ROEELA, ROOFL, RFIX

\$ SAAF, SIGMA, SPANAT(2)

\$ TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX

\$ TJRABG, TW

30

\$ UCS, UWS

\$ VAS(4)

\$ W=V

\$ XDEP1, XW, XD

COMMON /FAN/ FANDAP(153,10), FANAH(153,10), FMCPP, FBCPP,

35

SVELPEC, AFC, ELEV, EHR

COMMON /TINC2/ COM

126 FORMAT(//79X,"COEFFICIENTS FOR POLYNOMIAL CURVE FIT")

127 FORMAT(70X,"A0",11X,"A1",11X,"A2",11X,"A3",11X,"A4")

128 FORMAT(" HEAT RATE FACTOR AS FUNCTION OF BACKPRESSURE (INCHES OF M"

40

+ERCURY) ",1PSE13.5//)

129 FORMAT(T4,"TURBINE RATING BACKPRESSURE",F6.2," INCHES OF MERCURY")

130 FORMAT(T4,"SITE ELEVATION",F7.0," FEET ABOVE SEA LEVEL")

202 FORMAT(141,T30,"I N P U T S U M M A R Y A N D C A S E

D E S C R I P T I O N")

45

204 FORMAT(T2,3("-----"),190,2("-----"),"-")

206 FORMAT(T2,"OPTIONS SELECTED FOR THIS RUN",T90,"STARTING CONDITIONS

S")

200 FORMAT(140)

50

210 FORMAT(T4,"EXCHANGER DEPTH UNCONSTRAINED")

208 FORMAT(T5,"UPPER LIMIT ON TURBINE TEMP",F6.1," F")

215 FORMAT(T4,"EXCHANGER DEPTH CONSTRAINED TO ",A4,1X,F5.1," TUBES")

220 FORMAT(14,T30,"TURBINE OUTLET TEMPERATURE, T1",F10.3," F")

225 FORMAT(T4,"EXCHANGER LENGTH UNCONSTRAINED")

230 FORMAT(T4,"EXCHANGER LENGTH FIXED AT ",F5.0," FEET")

55

235 FORMAT(14,T30,"CAPACITY RATIO, CHARA",F10.3)

240 FORMAT(T4,"RUN WITH VELOCITY RECOVERY")

245 FORMAT(T4,"RUN WITHOUT VELOCITY RECOVERY")

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250 FORMAT(1H+,T91,"FRONTAL AREA, AFRO",F11.0)
255 FORMAT(T4,"NTU CALCULATION IS BY ",2A10)
60 260 FORMAT(1H+,T82,"WIDTH TO LENGTH RATIO, WLRAT",F10.3)
265 FORMAT(T8,"TUBE ARRANGEMENT ",A10)
300 FORMAT(//T51,"UNIT COSTS AND COSTING FACTORS"/T51,30(" ")/)
305 FORMAT(T2,"FUEL ",F7.3," CENTS/MMBTU"
      $,T30,"POWER PLANT CONSTRUCTION",F11.3," $/KW"
      $,T104,"FIXED CHARGE RATE",F9.3)
65 310 FORMAT(T2,"LAND ",F7.3," $/SQ FT"
      $,T30,"REPLACEMENT POWER",7X,F11.3," MILLS/KW-H"
      $,T105,"CAPACITY FACTOR",F9.3)
70 315 FORMAT(T2,"MOTORS",F7.3," $ / HP"
      $,T30,"STEAM SUPPLY",T54,F11.3," $/KW TURBINE OUTPUT"
      $,T93,"BASE THERMAL EFFICIENCY",F9.3)
320 FORMAT(T30,"CAPACITY CHARGE",T54,F11.3," $/KW-H"
      $,T93,"CONSTRUCTION COST MULTIPLIER",F9.3)
75 325 FORMAT(T95,"MAINT COSTS /CAPITAL COSTS",F9.3)
      WRITE(A,202)
      WRITE(A,204)
      WRITE(A,205)
      WRITE(A,204)
      WRITE(A,200)
      WRITE(A,203) TLIM
80
C
LOGSYM = ".LE."
IF(DEEPL.GT.0.0) LOGSYM = ".GE."
IF(DEEPL.EQ.0.0) WRITE(6,210)
IF(DEEPL.NE.0.0) WRITE(6,215) LOGSYM, ABS(DEEPL)
85
C
WRITE(6,220) VAS(1)
C
IF(FIXL.EQ.0.0) WRITE(6,225)
IF(FIXL.NE.0.0) WRITE(6,230) FIXL
90
C
WRITE(A,235) VAS(3)
C
IF(VELDEC.EQ.0.0) WRITE(6,245)
IF(VELDEC.NE.0.0) WRITE(6,240)
95
C
WRITE(6,250) VAS(4)
C
WRITE(6,255) NTUCAL
WRITE(6,250) VAS(5)
100
C
C
WRITE(6,255) TUBARG
C
WRITE(6,126)
WRITE(6,127)
WRITE(6,128) (TPO(I),I=1,4)
WRITE(6,129) RBP
WRITE(6,130) ELEV
105
C
WRITE(6,300)
WRITE(6,305) FCOS,PLANC,FCR
WRITE(6,310) COSTL,PWCOS,CAPFI
WRITE(6,315) HPCST,CSSPKW,TEFFI
110

```


SUBROUTINE INPSUM

74/74 OPT=1

FTN 4.2.74351

12/20/66

115

WRITE(6,320) CAPCHG,CCM

WRITE(6,325) PER

RETURN

END

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      SUBROUTINE HYDLOS(DIA,VEL,VIS,RHO,ID,HOLS)
C
C      SUBROUTINE HYDLOS FOR GIVEN VALUES OF INSIDE DIAMETER,
C      VELOCITY, VISCOSITY, AND DENSITY, DETERMINES THE FRICTION
5      HEAD LOSS PER FEET OF DRAWN TUBING (ID=1), STEEL PIPE (ID=2),
C      OR CAST IRON PIPE (ID=3) USING MOODY FRICTION FACTOR CHART
C      EQUATIONS
C      REFERENCE, KNUDSEN, J.G. AND KATZ, D.L. "FLUID DYNAMICS AND
10     HEAT TRANSFER", MCGRAW-HILL, NEW YORK, 1958, P.175
C
C      DIMENSION EP(3)
C
C      INSIDE SURFACE PROTUBERANCES FOR COMMERCIAL TUBING AND PIPE
C
15     DATA EP/0.00006,0.0018,0.0102,
C
C      CALCULATE REYNOLDS NUMBER AND DETERMINE IF IN LAMINAR OR
C      TURBULENT REGION
C
20     RE=300.*RHO*VEL*DIA/VIS
C      IF(RE-2000.)100,101,101
C
C      CALCULATE LAMINAR FLOW FRICTION FACTOR
C
25     100 F=16./RE
C      GO TO 102
C
C      CALCULATE RECIPROCAL OF RELATIVE ROUGHNESS AND RECIPROCAL OF
C      SQUARE ROOT OF FRICTION FACTOR FOR FULLY TURBULENT FLOW
C
30     101 RF=DIA/EP(ID)
C      FF=4.*ALOG10(RF)+2.28
C
C      CHECK TO DETERMINE IF TURBULENT FLOW IS FULLY DEVELOPED
C
35     CF=RF*FF/RE
C      IF(CF-0.01)104,103,103
C
C      DETERMINE RECIPROCAL OF SQUARE ROOT OF FRICTION FACTOR
C      FOR TRANSITION FLOW INITIALLY ASSUMING IT TO BE THE SAME AS
C      FOR FULLY TURBULENT FLOW
C
40     103 TRF=FF
C      107 TRFC=FF-4.*ALOG10(1.+4.67*RF*TRF/RE)
C
45     IF CALCULATED AND ASSUMED VALUES OF RECIPROCAL OF SQUARE ROOT
C      OF TRANSITION FLOW FRICTION FACTOR DO NOT AGREE WITHIN
C      SPECIFIED LIMITS, ASSUME NEW VALUE EQUAL TO CALCULATED VALUE
C      AND REPEAT CALCULATION
C
50     CALCULATION
C
C      IF ((ABS(TRFC-TRF)/TRF)-0.001)105,105,106
C      106 TRF=TRFC
C      GO TO 107
C
55     CALCULATE FULLY DEVELOPED TURBULENT FLOW OR TRANSITION FLOW
C      FRICTION FACTOR

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SUBROUTINE HYDLOS 74/74 OPT=1

FTN 4.2+74351

12/20/66

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C
60 105 FF=TRF
    104 F=1./FF**2
C
C      DETERMINE FRICTION HEAD LOSS
C
65 102 HDLS=74.594*F*VEL**2/DIA
C
    RETURN
    END
```

SUBROUTINE NOVART(TVAL3,VCST)

5	C	SUBROUTINE NOVART CALCULATES THE PERFORMANCE OF THE POWER PLANT AND DRY COOLING TOWER UNDER THE ASSUMPTION THAT THE AIR SIDE HEAT TRANSFER COEFFICIENTS AND AIR VELOCITY THROUGH THE HEAT EXCHANGER TUBES ARE UNCHANGED
	C	
	C	DEFINITION OF VARIABLES
10	C	CAPCHG - GAS TURBINE CAPITAL COST (\$/MW)
	C	CAPCST - COST OF GAS TURBINE (\$)
	C	CAPF - PERCENTAGE OF TIME THE PLANT IS PRODUCING POWER (PERCENT)
	C	CCOS - COST OF THE DRY COOLING TOWERS (\$)
15	C	CLAND - COST OF LAND TAKEN UP BY THE DRY COOLING TOWERS (\$)
	C	CONBAS - COST OF SURFACE CONDENSER (\$)
	C	COSM - COST OF MAINTAINING THE DRY COOLING TOWERS (\$)
	C	CRIP - COST OF PIPING AND PUMPING SYSTEMS (\$)
20	C	CSTCH - COST OF MAKE-UP POWER BY GAS TURBINES AT EACH AMBIENT AIR TEMPERATURE (MILLS/KW-HR)
	C	DELFC - INCREMENTAL FUEL COST FOR STEAM SUPPLY SYSTEM (MILLS/KW HR)
	C	EFF - HEAT EXCHANGER EFFECTIVENESS OF DRY COOLING TOWERS (DIMENSIONLESS)
25	C	EFFC - CONDENSER EFFECTIVENESS
	C	FCOS - FUEL COST FOR THE STEAM SUPPLY SYSTEM (MILLS/BTU)
	C	FCR - FIXED CHARGE RATE ON CAPITAL PER YEAR (PERCENT)
	C	FPOW - POWER REQUIREMENTS OF FAN SYSTEM (KW)
30	C	HRFAC1 - HEAT RATE FACTOR OF STEAM TURBINE AT RATED BACK PRESSURE (DIMENSIONLESS)
	C	HRFAC2 - HEAT RATE FACTOR OF STEAM TURBINE AT DESIGN CONDITIONS OF POWER PLANT (DIMENSIONLESS)
	C	HRFAC4 - HEAT RATE FACTOR OF STEAM TURBINE AT A PARTICULAR AMBIENT AIR TEMPERATURE (DIMENSIONLESS)
35	C	P - BACK PRESSURE OF STEAM TURBINE (IN. HG.)
	C	PARCOS - INCREMENTAL POWER PRODUCTION COST OF THE DRY COOLED POWER PLANT FOR A PARTICULAR AMBIENT AIR TEMPERATURE (MILLS/KW-HR)
40	C	PGEN - POWER OUTPUT OF PLANT AT A PARTICULAR AMBIENT AIR TEMPERATURE (MW)
	C	PPOW - POWER REQUIREMENTS OF THE PIPING SYSTEM (KW)
	C	PISZ13 - POWER OUTPUT OF STEAM TURBINE AT RATED BACK PRESSURE TO PRODUCE REQUIRED OUTPUT OF PLANT AT DESIGN CONDITIONS (MW)
45	C	PIOT - POWER OUTPUT OF PLANT AT SPECIFIED AMBIENT AIR TEMPERATURE (MW)
	C	PXCOS - COST OF FUEL FOR GAS TURBINE (MILLS/KW-HR)
	C	QTN1 - THERMAL ENERGY OUTPUT OF STEAM SUPPLY SYSTEM AT RATED BACK PRESSURE OF TURBINE (BTU/HR)
50	C	QREJCT - HEAT REJECTED AT A SPECIFIED AMBIENT AIR TEMPERATURE (BTU/HR)
	C	RANGE - TEMPERATURE RANGE OF WATER PASSING THROUGH THE HEAT EXCHANGER (DEG F)
55	C	SPCD - INCREMENTAL COST OF PLANT DUE TO SCALE UP OF STEAM SUPPLY SYSTEM AND THE SCALE UP OF THE PLANT TO TAKE INTO ACCOUNT FOR FAN AND PUMP POWER REQUIREMENTS (\$)

```

C      TA      - AMBIENT AIR TEMPERATURE (DEG F)
C      TEFF     - THERMAL EFFICIENCY OF CONVENTIONAL STEAM TURBINE
60      C      TEFF1  - THERMAL EFFICIENCY OF STEAM TURBINE AT RATED
C      C      TEFF3  - THERMAL EFFICIENCY OF STEAM TURBINE AT POWER
C      C      TEFF4  - THERMAL EFFICIENCY OF STEAM TURBINE ASSOCIATED
65      C      WITH A PARTICULAR AMBIENT AIR TEMPERATURE
C      C      (DIMENSIONLESS)
C      TLIM     - LIMIT ON THE TEMPERATURE EXITING THE STEAM
C      C      TURBINE (DEG F)
70      C      TPER     - PERCENT OF TIME AN AMBIENT TEMPERATURE OCCURS
C      C      DURING THE YEAR (PERCENT)
C      TPO      - COEFFICIENTS FOR THIRD ORDER CURVE FIT OF STEAM
C      C      TURBINE HEAT RATE FACTOR (DIMENSIONLESS)
C      TTOP     - TERMINAL TEMPERATURE DIFFERENCE OF SURFACE
75      C      CONDENSER FOR A PARTICULAR AMBIENT AIR TEMPERATURE
C      TVAL3    - THERMAL CAPACITY RATIO OF THE WATER TO THE AIR
C      C      PASSING THROUGH THE HEAT EXCHANGER (DIMENSIONLESS)
C      TI       - EXIT TEMPERATURE OF STEAM TURBINE (DEG F)
C      VCOST    - TOTAL INCREMENTAL COST OF DRY COOLING (MILLS/KW-HR)
80      C      W3      - MASS FLOW RATE OF WATER THROUGH THE HEAT EXCHANGER
C      C      (LBM/HR)
C      XCOST    - INCREMENTAL COST OF DRY COOLING FOR EACH AMBIENT
C      C      AIR TEMPERATURE (MILLS/KW-HR)
85      C      YFP     - PLANT SCALING FACTOR TO TAKE INTO ACCOUNT FOR
C      C      FAN AND PUMP POWER (DIMENSIONLESS)

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```

C      REAL XCOST(8)
C      COMMON /VARVAR/ VTPER(16), VTA(16)
C      LOGICAL FIRST, FXTMP
90      COMMON
C      $ AFTR, ALPHA
C      $ ,CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAPI
C      $ ,CBU, CSEALP, CELAST, CFS, COANG, CLUVR, CHALS, CVM
C      $ ,DEEPL, DESVEL, DANGLE
95      $ ,EFPF
C      $ ,FOR, FIRST, FIXL, FCOS, FXTMP
C      $ ,GREFF
C      $ ,HXNP, HPCST
C      $ ,IHEAT
100      $ ,ITMAX, ITMIN
C      $ ,JCONC
C      $ ,KCONV, KALEXT
C      $ ,MXEXT
C      $ ,NTJCAL(2), NTA
105      COMMON
C      $ ,DRR
C      $ ,PSIZE, PER, PWCOS, PLANC, PFACT
C      $ ,POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCU
C      $ ,OREU, QREDUCE
110      $ ,REP, REDUCE, ROESL, ROELA, ROOFL, RFIX
C      $ ,SAAF, SIGMA, SPAMAT(2)
C      $ ,TD, TPO(4), TEFF, TLIM, TLPA, TSEALP, TELAST, THFIN, TFIX
C      $ ,TJBAD3, TW
C      $ ,UCS, UWS

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115      $ ,VAS(5)
      $ ,WFW
      $ ,XDEPA, XW, XD
      COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
120      $ ,CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,
      $ ,FPOW, DELFC, WIDTH, ELENG, VAIR, VWAT, HY, HO, T4,
      $ ,REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3,
      $ ,SPCPTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
      $ ,BP2, VW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELDX
125      $ ,TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
      $ ,CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPIP, AST
      $ ,CAPCST, XNFAN, BLDANG, CPLEN, DPFEI, WHX, ATTUB, ADIA, ABLN
      $ ,WTHOR, WTERM, STRUCC, CPERF, HPPERF, TOTCF, EFFIN, ANTU
      $ ,AIREF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTP, ADJTP
130      $ ,ACTBD, ADJBD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
      $ ,CSO, WATERW, WSTRUCT, CFOWN, HUBDIA, TOWLEN, CSE, CHF
      $ ,CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
      COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1
      $ ,GAIR, FAIR, HPAIR, HPWAT, PLANCT1
      DIMENSION VLIST(9)
135      DATA NTRIP/0/
      DATA VLIST /"CCOS","SPCD","CLAND","CPIP","CONBAS","COSM"
      $ , "TPER","PARCOS","VCST"/

      C
      C      THERMAL EFFICIENCY OF TURBINE AT THE DESIGN POINT OF THE
140      C      PLANT.
      C
      C      TEFFB=TEFF/HRFAC2
      C
      C      THERMAL EFFICIENCY OF TURBINE AT THE RATED BACK PRESSURE
145      C
      C      TEFF1=TEFF/HRFAC1
      C      QIN1=3413.E+3 * PSIZ13/TEFF1
      C      VCST=0.0

150      C
      C      START OF LOOP FOR CALCULATING THE INCREMENTAL COST OF DRY
      C      COOLING FOR EACH TEMPERATURE RANGE
      C
      C      DO 300 I=1,NTA

155      C
      C      AMBIENT AIR TEMPERATURE AND PERCENTAGE OF YEAR OVER WHICH
      C      TEMPERATURE OCCURS.
      C
      C      TA=VTA(I)
      C      TPER=VTPER(I)

160      C
      C      ITERATIVE LOOP FOR CALCULATING THE EXIT TEMPERATURE OF THE
      C      STEAM TURBINE AS A FUNCTION OF THE AMBIENT AIR TEMPERATURE.
      C
      C      CALCULATION OF THE THERMAL EFFICIENCY OF STEAM TURBINE FOR
165      C      THE SPECIFIED EXIT TEMPERATURE OF THE TURBINE
      C
      C      T1=140.
      C      P=EXP(17.168-9240./(T1+460.))
      C      HRFAC4=TPO(1) * TPO(2)*P + TPO(3)*P**2 + TPO(4)*P**3
      C      TEFF4=TEFF/HRFAC4

170      C
      C      TEMPERATURE RANGE OF WATER FLOWING THROUGH THE HEAT EXCHANGER

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      QREJCT=QIN1*(1.-TEFF4)
      RANGE=QREJCT/(W3*(1.+YFP))

175      C      TERMINAL TEMPERATURE DIFFERENCE BETWEEN THE WATER AND THE
      C      STEAM OF THE SURFACE CONDENSER
      TTDP=RANGE/EFFC-RANGE

180      C      EXIT TEMPERATURE OF THE STEAM TURBINE ON PREVIOUS ESTIMATE
      IF (TVAL3.GT.1.) GOTO 2
      T11=RANGE/EFF + TA + TTDP
      GOTO 3
2    T11=RANGE-TVAL3/EFF + TA + TTDP

185      C      CONVERGENCE CRITERION FOR EXIT TEMPERATURE OF TURBINE
3    IF (.NOT. FXTMP .AND. (T11-T1)**2 .LT. .001) GOTO 4
      CVT = ABS( (T11-T1) / T11 )
      IF (FXTMP .AND. CVT .LT. 0.0001) GOTO 4
      T1=T11
190      GOTO 1

      C      TOTAL POWER OUTPUT OF TURBINE AT THE PARTICULAR AMBIENT
      C      AIR TEMPERATURE

195      C      4 PTOT = QIN1 * TEFF4 / 3413.E+3

      C      POWER OUTPUT FROM PLANT AT THE PARTICULAR AMBIENT AIR
      C      TEMPERATURE

200      PGEN=PTOT-PPOW/1000.-FPOW/1000.
      TEFFD=TEFF4
      IF (PGEN.GE.PSIZE) GOTO 5

      C      COST OF FUEL FOR GAS TURBINE MAKE UP POWER

205      C      CSTCL=(PSIZE-PGEN)/PSIZE*PWGOS
      TEFFD=TEFF3
      GOTO 6
5    CSTCL=0.0

210      C      INCREMENTAL COST OF FUEL FOR STEAM SUPPLY SYSTEM DUE TO STEAM
      C      TURBINE OPERATING AT OFF-DESIGN CONDITIONS (RATED BACK
      C      PRESSURE)

215      C      6 DELFC=FCOS*3413.E-5 * ((1.+YFP)/TEFFD-1./TEFFD)
      IF (T1.NE.1) GO TO 10

      C      TEMPERATURE LIMITATION ON MAXIMUM YEARLY EXIT, TEMPERATURE OF
      C      THE STEAM TURBINE

220      C      IF (T11 .GT. TLIM) VCST = 10. * T11
      C      IF (T11 .GT. TLIM) RETURN

      C      CAPITAL COST OF GAS TURBINE USED FOR MAKE-UP POWER OF STEAM
      C      PLANT

225      C      IF (PSIZE*LE*PGEN) GO TO 10
      CAPCST=CAPCHG*(PSIZE-PGEN)

```

```

230      10 CONTINUE
      C
      C      COST OF PRODUCING POWER WITH DRY COOLED PLANT AT SPECIFIED
      C      AMBIENT AIR TEMPERATURE
      C
      PARCOS = (CCOS + SPCD + CLAND + CPIP + CONBAS + CAPCST) * FCR /
235      $ (PSIZE * CAPF * 9760.) + COSM * DELFC + CSTCL
      XCOST(I) = TPER * PARCOS
      800 CONTINUE
      C
      C      SUMMATION OF INCREMENTAL POWER PRODUCTION COSTS
      C
240      DO 820 I=1,NTA
      VCST = VCST + XCOST(I)
      320 CONTINUE
      C
      C      DEBUG PRINT OUT STATEMENTS
      C
      NDBG=0
      IF (NDBG.EQ.0) RETURN
      NTRIP = NTRIP + 1
250      WRITE(4,902) NTRIP
      WRITE(4,900) CCOS,SPCD,CLAND,CPIP,CONBAS,COSM,TPER,PARCOS,VCST
      WRITE(4,901) VLIST
      900 FORMAT(1H,9G14.5)
      901 FORMAT(1H,9(4X,A6,4X))
255      902 FORMAT("0 NOVART CALL NO.",I10)
      RETURN
      END

```


SUBROUTINE NUN02P(T1, TD, TTD, CWARA, RANGE, W3, W4, ANTU)

C THIS ROUTINE DETERMINES THE NUMBER OF TRANSFER UNITS
C FOR A TRUE COUNTER-FLOW HEAT EXCHANGER.
C THE NTU-EFFECTIVENESS CORRELATION FOR TRUE COUNTER FLOW IS
C USED. THERE ARE THREE POSSIBLE CONDITIONS- CAPACITY RATIO
C GREATER THAN UNITY, EQUAL TO UNITY, AND LESS THAN UNITY.

C DEFINITION OF VARIABLES

C CMIN - MINIMUM CAPACITY (BTU/HR DEG F)
C CWARA - CAPACITY RATIO OF WATER TO AIR (DIMENSIONLESS)
C EFF - HEAT EXCHANGER EFFECTIVENESS (DIMENSIONLESS)
C ITD - INITIAL TEMPERATURE DIFFERENCE OF HEAT
C EXCHANGER (DEG F)
C RANGE - TEMPERATURE RANGE OF WATER (DEG F)
C T1 - STEAM SATURATION TEMPERATURE (DEG F)
C TD - AMBIENT DESIGN TEMPERATURE (DEG F)
C TTD - CONDENSER TERMINAL TEMPERATURE DIFFERENCE (DEG F)

REAL ITD
1 FORMAT('0IN S.R. NUN02P EFF IS GREATER THAN OR EQUAL TO 1.'/
\$ T2, 'EFF=', 1P12.6, T20, 'T1, TD, TTD, CWARA, RANGE=',
\$ 1P3E15.6)

ITD = T1 - TTD = TD
IF (CWARA.GE. 1.0) GOTO 200
EFF = RANGE / ITD
IF (EFF.GE. 1.0) GOTO 700
CMIN = W3
ZCAP = CWARA
GOTO 300

200 EFF = CWARA * RANGE / ITD
IF (EFF.GE. 1.0) GOTO 700
CMIN = W4 * 0.24
ZCAP = 1.0 / CWARA

IF (CWARA.EQ. 1.0) ANTU = EFF / (1.-EFF)
IF (CWARA.NE. 1.0) ANTU = (-ALOG((1.-EFF) / (1.-EFF*ZCAP))) / (1.-
\$ ZCAP)

RETURN
300 ANTU = (-ALOG((1.-EFF) / (1.-EFF*ZCAP))) / (1.-ZCAP)
RETURN

700 WRITE(4,1) EFF, T1, TD, TTD, CWARA, RANGE
STOP
END

```

1      SUBROUTINE NTU1P (CP, E, Y)
      C
      C      THIS ROUTINE DETERMINES THE NUMBER OF TRANSFER UNITS FOR A
      C      ONE-PASS CROSS-FLOW HEAT EXCHANGER.
      C      THE TABULATED DATA OF NTU VERSUS EFFECTIVENESS AND CAPACITY
      C      RATIO WAS TAKEN FROM "MEAN TEMPERATURE DIFFERENCE IN COUNTER-
      C      CROSS-FLOW HEAT EXCHANGERS". RA STEVENS, MS THESIS,
      C      SOUTHERN METHODIST UNIVERSITY, 1956. THE DATA WERE
      C      DETERMINED ANALYTICALLY.
10     C
      C      DIMENSION VE(16,11), VC(11), VY(16), PCOL(16)
      C
      C      DATA VC / 0.0, .1, .2, .3, .4, .5, .6, .7, .8, .9, 1. /
      C
15     C      DATA VY / 0.0, .25, .5, .85, 1.00, 1.25, 1.5, 1.75, 2.0, 2.5, 3.0,
      C      * 3.5, 4., 5., 6., 7. /
      C
      C      DATA (VE( 1,I),I=1,11) /
      C      $ 11 * 0.0 /
20     C      DATA (VE( 2,I),I=1,11) /
      C      $ .2212, .2148, .2164, .2141, .2117, .2095, .2072, .2050, .2028,
      C      $ .2007, .1945/
      C      DATA (VE( 3,I),I=1,11) /
      C      $ .3935, .3860, .3787, .3716, .3646, .3578, .3512, .3448, .3385,
25     C      $ .3323, .3263/
      C
      C      DATA (VE( 4,I),I=1,11) /
      C      $ .5728, .5574, .5427, .5285, .5147, .5014, .4885, .4760, .4640,
      C      $ .4523, .4410/
30     C      DATA (VE( 5,I),I=1,11) /
      C      $ .6321, .6141, .5966, .5797, .5633, .5475, .5323, .5175, .5033,
      C      $ .4896, .4763/
      C      DATA (VE( 6,I),I=1,11) /
      C      $ .7134, .6916, .6702, .6496, .6296, .6103, .5917, .5737, .5563,
35     C      $ .5396, .5243/
      C
      C      DATA (VE( 7,I),I=1,11) /
      C      $ .7769, .7522, .7281, .7046, .6819, .6598, .6385, .6179, .5980,
      C      $ .5788, .5603/
40     C      DATA (VE( 8,I),I=1,11) /
      C      $ .8259, .8000, .7741, .7487, .7239, .6998, .6763, .6536, .6316,
      C      $ .6104, .5899/
      C      DATA (VE( 9,I),I=1,11) /
      C      $ .8647, .8378, .8109, .7843, .7582, .7325, .7075, .6831, .6594,
45     C      $ .6365, .6143/
      C
      C      DATA (VE(10,I),I=1,11) /
      C      $ .9179, .8920, .8652, .8379, .8104, .7830, .7559, .7291, .7030,
      C      $ .6774, .6526/
50     C      DATA (VE(11,I),I=1,11) /
      C      $ .9502, .9270, .9018, .8753, .8479, .8199, .7917, .7635, .7357,
      C      $ .7082, .6814/
      C      DATA (VE(12,I),I=1,11) /
      C      $ .9698, .9501, .9273, .9024, .8758, .8480, .8194, .7904, .7613,
55     C      $ .7325, .7041/
      C
      C      DATA (VE(13,I),I=1,11) /

```

```

      * .9817, .9654, .9454, .9225, .8971, .8699, .8414, .8120, .7821,
      * .7522, .7226/
60      DATA (VE(14,I),I=1,11) /
      * .9433, .9830, .9683, .9495, .9273, .9019, .8742, .8447, .8140,
      * .7826, .7511/
      DATA (VE(15,I),I=1,11) /
65      * .9475, .9914, .9804, .9661, .9470, .9239, .8975, .9685, .8375,
      * .8052, .7723/
      C
      DATA (VE(16,I),I=1,11) /
      * .9991, .9955, .9883, .9767, .9605, .9397, .9149, .8866, .8557,
70      * .8229, .7889/
      C
      C
      C = CR
      IF( CR .GT. 1.) C = 1./C
75      C
      C
      C FIND COLUMNS WHICH BOUND C.
      C
      KL = 0
      DO 400 K=1,11
80      IF(C.LT.VC(K)) GOTO 410
      KL = K
400 CONTINUE
      C
      C
85      C GENERATE ARRAY PCOL BY INTERPOLATING BETWEEN VE VALUES IN
      C COLUMNS KL AND KL+1
      C
410 IF(KL.GT.0.0 .AND. KL.LT.11) FACTOR=(C-VC(KL+1))/(VC(KL)-VC(KL+1))
      DO 500 I=1,16
90      IF(KL.EQ.0) PCOL(I) = VE(I,1)
      IF(KL.EQ. 11) PCOL(I) = VE(I,KL)
      IF(KL.GT.0 .AND. KL .LT. 11)
      * PCOL(I) = (VE(I,KL) - VE(I,KL+1) ) * FACTOR +VE(I,KL+1)
500 CONTINUE
95      C
      C
      C FIND THE POSITION OF PCOL VALUES BOUNDING E
      C
      IA = 1
100      DO 600 I=1,16
      IF(E .LT. PCOL(I) ) GOTO 610
      IA = I
600 CONTINUE
105      C
      C
      C THE VY VALUES BOUNDING Y ARE VY(IA) AND VY(IA+1)
      C
      C INTERPOLATE BETWEEN VY VALUES TO GET Y
      C
110      *10 FACTOR = (E-PCOL(IA))/(PCOL(IA+1)-PCOL(IA) )
      Y = VY(IA) + (VY(IA+1)-VY(IA) ) * FACTOR
      RETURN
      END

```

```

1      SUBROUTINE NTU2P (CR, E, Y)
      C
      C      THIS ROUTINE DETERMINES THE NUMBER OF TRANSFER UNITS FOR A
      C      TWO-PASS COUNTER-CROSS-FLOW HEAT EXCHANGER WITH THE WATER
5      C      SIDE MIXED BETWEEN PASSES.
      C      THE TABULATED DATA OF NTU VERSUS EFFECTIVENESS AND CAPACITY
      C      RATIO WAS TAKEN FROM "MEAN TEMPERATURE DIFFERENCE IN COUNTER-
      C      CROSS-FLOW HEAT EXCHANGERS". RA STEVENS, MS THESIS,
      C      SOUTHERN METHODIST UNIVERSITY, 1956. THE DATA WERE
10     C      DETERMINED ANALYTICALLY.
      C
      DIMENSION VE(15,11), VC(11), YY(15), PCOL(15)
      DATA (VE( 1,I), I=1,11) /
15     $ 11 * 0.0 /
      DATA (VE( 2,I), I=1,11) /
      $ .2212, .2199, .2167, .2145, .2122, .2100, .2079, .2058, .2038,
      $ .2017, .1996/
      DATA (VE( 3,I), I=1,11) /
20     $ .3935, .3869, .3801, .3736, .3673, .3610, .3549, .3487, .3428,
      $ .3369, .3312/
      C
      DATA (VE( 4,I), I=1,11) /
      $ .5034, .4930, .4828, .4728, .4629, .4532, .4437, .4343, .4252,
      $ .4162, .4074/
25     DATA (VE( 5,I), I=1,11) /
      $ .6321, .6172, .6024, .5877, .5732, .5590, .5449, .5311, .5176,
      $ .5043, .4914/
      DATA (VE( 6,I), I=1,11) /
30     $ .7275, .7095, .6914, .6734, .6554, .6375, .6198, .6023, .5852,
      $ .5683, .5518/
      C
      DATA (VE( 7,I), I=1,11) /
      $ .8173, .7975, .7772, .7564, .7353, .7141, .6929, .6717, .6507,
      $ .6302, .6097/
35     DATA (VE( 8,I), I=1,11) /
      $ .8647, .8448, .8239, .8022, .7800, .7571, .7340, .7108, .6877,
      $ .6648, .6421/
      DATA (VE( 9,I), I=1,11) /
40     $ .9179, .8996, .8794, .8576, .8346, .8104, .7855, .7600, .7343,
      $ .7085, .6828/
      C
      DATA (VE(10,I), I=1,11) /
      $ .9502, .9344, .9160, .8954, .8728, .8485, .8227, .7959, .7684,
      $ .7406, .7127/
45     DATA (VE(11,I), I=1,11) /
      $ .9698, .9567, .9407, .9225, .9015, .8780, .8523, .8251, .7965,
      $ .7671, .7374/
      DATA (VE(12,I), I=1,11) /
50     $ .9817, .9712, .9575, .9406, .9206, .8977, .8721, .8445, .8152,
      $ .7848, .7538/
      C
      DATA (VE(13,I), I=1,11) /
      $ .9933, .9870, .9775, .9645, .9477, .9271, .9030, .8758, .8460,
      $ .8142, .7813/
55     DATA (VE(14,I), I=1,11) /
      $ .9975, .9939, .9876, .9779, .9642, .9462, .9234, .8976, .8679,
      $ .8355, .8013/

```

F-75

SUBROUTINE OUT2(RBP,HRFAC1,SSCD,CASSS1,PLANCT1,PLANC1)

C
C
C
C

THIS ROUTINE REPORTS STEAM SUPPLY COSTS DUE TO INCREASED HEAT RATE
AT RATING BACKPRESSURE.

5

1 FORMAT(1H0,T3,"STEAM SUPPLY SCALING TO COMPENSATE FOR INCREASED ",
\$ "HEAT RATE AT RATING BACKPRESS RE. RBP=",F5.2,T97,"IN. HG",
\$ T11³,"HRFAC1=",F11.6)

10

2 FORMAT(1H0,T5,"STEAM SUPPLY COST DIFFERENTIAL \$",T38,F12.0,
\$ T69,"STEAM SUPPLY UNIT COST",F12.0," \$/KW")

3 FORMAT(1X,T3,"PLANT COST INCLUDING STEAM SUPPLY \$",T38,F12.0,
\$ T53,"PLANT UNIT COST INCLUDING STEAM SUPPLY ",T91,F12.3,"\$/KW")

15

WRITE(4,1) RBP,HRFAC1
WRITE(4,2) SSCD,CASSS1
WRITE(4,3) PLANCT1,PLANC1
RETURN
END

SUBROUTINE OUT4(KWHICH)

C
C
C
C
C
C

WHEN CALLED WITH KWHICH = 1 THIS ROUTINE REPORTS CONDITIONS AFTER
SCALING PLANT AND STEAM SUPPLY BUT BEFORE
SCALING FOR FANS AND PUMPS

WHEN CALLED WITH KWHICH NOT 1 THE ROUTINE REPORTS CONDITIONS AFTER
SCALING FOR FANS AND PUMPS

LOGICAL FXTLNG

LOGICAL FIRST, FXTMP

COMMON

\$ AFTR, ALPHA

\$ CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAP

\$ CBU, CSEAL, CELAST, CFS, CDANG, CLUVR, CHAILS, CVM

\$ DEEPL, DESVEL, DANGLE

\$ EEPF

\$ FOR, FIRST, FIXL, FCOS, FXTMP

\$ GSEFF

\$ HXNP, HPCST

\$ IHEAT

\$ ITMAX, ITMIN

\$ JCONC

\$ KOONV, KALEXT

\$ MXEXT

\$ NTUCAL(2), NTA

COMMON

\$ ODR

\$ PSIZE, PER, PWCOS, PLANC, PFACT

\$ POH3IF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCD

\$ QRED, QREDUCE

\$ R3P, REDUCE, ROESEL, ROELA, ROEL, RFIX

\$ SAAF, SIGMA, SPAMAT(2)

\$ TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX

\$ TUBARG, TW

\$ UCS, UWS

\$ VAS(5)

\$ WFM

\$ XJEP1, XW, XD

COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF

\$ CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,

\$ FPOW, DELFC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4,

\$ REWAT, NW, PLANC2, PSIZ12, SP3P, SW4, SW3,

\$ SPC, PTOT, PLANC3, SAFR0V, AAIR, YFP, SPCD, PSIZ13, WT2,

\$ B02, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELOX

\$ TLAX, UCON, FMCST, FBACC, EFFC, C4, CA, CS

\$ CLTC, CFC, CPOC, FITC, CSC, CEPREP, DELPID, AST

\$ CAPOST, XNFAN, BLDANG, CPLEN, DPFEI, WHX, WTTUB, ADIA, ABLN

\$ WTHR, WTERM, STRUCC, CPERF, HOPERF, TOTCF, EFFIN, ANTU

\$ AIRFF, WATFF, XNMOD, TCTPF, FOCPE, FMTRC, ACCTTP, ADJTP

\$ ACTBPD, ADJBPD, ACTVH, ADJVH, ADJPPF, THAIR, TCTF, AFCST

\$ CSND, WATERW, WSTRICT, CFOUND, HUBDIA, TOWEN, CSE, CHF

\$ CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL

COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1

\$ CLAN1, REAI1, Z1, HRFAC2S, W41, U1, PPOW1,

\$ FPOW1, DELFC1, WIDT1, ELENG1, VAIR1, VWAT1, HI1, HO1, T41,

\$ REWAT1, NW1, ZPLNC2, ZSIZ12, ZSP3P, SW41, SW31,

\$ SPC1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,

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      S BP2MIN,NW2MIN,TCOS1,DEPA1,DPWT1,DPWC1,CONBA1,XNTS1,VELD1
      S, TL1, UCON1, FMCS1, FBAC1, EFFC1, CHI, CA1, CS1
60    S, CLTC1, CFC1, CPCC1, FITC1, CSC1, CEPRE1, DEPI1, AST1
      S, CAPCS1, XNFAN1, BLOAN1, CPLEN1, DPFE1, WH1, WTTU1, ADI1, ABL1
      S, WTHD1, WTRF1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFINT, ANTU1
      S, AIRFF1, WATFF1, XVMOD1, TCTPF1, FDCFF1, FMTRC1, ACTTP1, ADJTP1
      S, ACTBP1, ADJBP1, ACTVH1, ADJVM1, ADJPP1, HPA1, TCTF1, AFCST1
55    S, CS1, WATER1, WSTRC1, CFOUN1, HUBDI1, TOWLE1, CSE1, CHF1
      S, CBA1, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
      COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,
      S GAIR, FAIR, HPAIR, HPWAT, PLANCT1
      COMMON /DJB/ DI,XDG,SF
70    COMMON /FLSH/ FXTLNG
901  FORMAT(" CONDITIONS AFTER SCALING PLANT AND STEAM SUPPLY (BEFORE)
      *SCALING FOR FANS AND PUMPS)",T33,"HRFAC2=",G15.7)
906  FORMAT(1X,T88,"PSIZ12=",G15.7," M")
911  FORMAT(1X,T88,"PLANC2=",G15.7," S/KW")
75    916  FORMAT(1X,T88,"SPBP=",G15.9," S")
917  FORMAT(1X,T81,"BACK PRESSURE=",G15.7," IN. HG")
918  FORMAT(1X,T79,"SAT TEMPERATURE=",G15.9," DEG F")
921  FORMAT(1X,T14,"WATER FLOW RATE ",G15.9," LB MASS / HR")
926  FORMAT(1X,T14,"AIR FLOW RATE ",G15.9," LB MASS / HR")
80    931  FORMAT(1X,T14,"PUMP POWER ",G15.9," KILOWATTS")
936  FORMAT(1X,T14,"FAN POWER ",G15.9," KILOWATTS")
941  FORMAT(1X,T14,"HX SURFACE AREA ",G15.9," SQ FT")
946  FORMAT(1X,T14,"FRONTAL AREA ",G15.9," SQ FT")
951  FORMAT(1X,T11,"WIDTH/LENGTH RATIO ",G15.9)
85    956  FORMAT(1X,T15,"WIDTH ",I11,T45," TUBES")
961  FORMAT(1X,T15,"WIDTH ",G15.9," FEET")
962  FORMAT(1X,T9,"NO. CONDENSER TUBES ",G15.9)
963  FORMAT(1X,T8,"CONDENSER TUBE LENGTH ",G15.9," FT.")
964  FORMAT(1X,T15,"WATER VELOCITY ",G15.9," FT/SEC")
90    965  FORMAT(1X,T7,"CONDENSER HT TRFR AREA ",G15.9," SQ FT TOTAL")
1001 FORMAT(1X,"SCALING FOR FAN AND PUMP POWER REQUIREMENTS",
      + T80,"SCALING FACTOR ",G15.9)
1005 FORMAT(1X,T88,"PSIZE ",G15.9," M")
1006 FORMAT(1X,T88,"PSIZ13 ",G15.9," M")
95    1011 FORMAT(1X,T88,"PTOTAL ",G15.9," M")
1016 FORMAT(1X,T88,"PLANC3 ",G15.9," S/KW")
1021 FORMAT(1X,T88,"SPC ",G15.9," S")
1026 FORMAT(1X,T88,"SPCD ",G15.9," S")
8888 FORMAT(1H0,12(" ** ** ** ")//)
100  WRITE(4,8888)
      WLRTP = WIDT1/ELEN1
      IF (WLRTP-NE.1) GOTO 2000
      WRITE(4,901) HRFAC2
      WRITE(4,906) ZSIZ12
105  WRITE(4,911) ZPLNC2
      WRITE(4,916) ZSPBP
      WRITE(4,917) BP2MIN
      WRITE(4,918) VAR(1)
      WRITE(4,921) W31
110  WRITE(4,926) W41
      WRITE(4,931) (PPOW1/(1.+YFPMIN))
      WRITE(4,936) (FPOW1/(1.+YFPMIN))
      WRITE(4,941) (AAIR1/(1.+YFPMIN))
      WRITE(4,946) (AFRO1/(1.+YFPMIN))

```


SUBROUTINE OUT4

74/74 OPT=1

FTN 4.2.74351

12/20/76

```

115      WRITE(4,951) WL RTP/(1.+YFPMIN)
      WRITE(4,956) NW2MIN
      WRITE(4,961) WT2MIN
      WRITE(4,965) AST1
      WRITE(4,962) XNTS1
120      WRITE(4,963) TLA1
      WRITE(4,964) VELD1
      RETURN
2000 CONTINUE
125      WRITE(4,1001) (1.+YFPMIN)
      WRITE(4,1005) PSIZE
      WRITE(4,1006) SPS13
      WRITE(4,1011) PT0T1
      WRITE(4,1016) PLVC31
      WRITE(4,1021) SPC1
130      WRITE(4,1026) SPCD1
      WRITE(4,921) SW31
      WRITE(4,926) SW41
      WRITE(4,931) PPOW1
      WRITE(4,936) FPOW1
135      WRITE(4,941) AAIR1
      WRITE(4,946) AFRO1
      WRITE(4,951) WL RTP
      WRITE(4,956) NW1
      WRITE(4,961) WINT1
140      WRITE(4,965) AST1 * (1. + YFPMIN)
      WRITE(4,962) XNTS1 * (1. + YFPMIN)
      WRITE(4,963) TLA1
      WRITE(4,964) VELD1
      RETURN
145      END

```

```

SUBROUTINE P50
COMMON /PIP50 / APIPCST(23), DIAM(23), EJCST(23), ELCST(23)
$, FLGCST(23)
$, EL45(23), PIPCST(23), REDCST(23), TEECST(23), VACST(23)
COMMON /CPIPE/ X(230)

```

```

THIS SUBROUTINE SUPPLIES UNIT COST DATA TO SUBROUTINE
PIPCRT FOR PIPING SYSTEM COMPONENTS DESIGNED FOR
125 PSI. THIS DATA IS CALLED BY USING A VALUE OF
DPRESS=125 (DPRESS=PIPING DESIGN PRESSURE) ON CARD G1
OF THE INPUT. THUS, ANY COST DATA CAN BE SUBSTITUTED HERE
FOR STUDY PURPOSES.

```

DEFINITION OF VARIABLES

```

APIPCST - ABOVE GROUND PIPE COST ($1000/FT)
DIAM     - COMPONENT DIAMETER (INCHES)
EJCST    - EXPANSION JOINT COST ($1000)
ELCST    - 90 DEGREE ELBOW COST ($1000)
EL45     - 45 DEGREE ELBOW COST ($1000)
FLGCST   - FLANGE COST ($1000)
PIPCST   - BELOW GROUND PIPE COST ($1000/FT)
REDCST   - REDUCER COST ($1000)
TEECST   - TEE COST ($1000)
VACST    - VALVE COST ($1000). VALVES ARE MOTOR OPERATED
          BUTTERFLY VALVES

```

50 PSI

DATA APIPCST /

\$		.056,	.074,	.092,	.112,	.132,
\$	.152,	.240,	.265,	.290,	.322,	.353,
\$	.375,	.396,	.423,	.449,	.470,	.490,
\$	.511,	.691,	.727,	.772,	.812,	.852

DATA DIAM/

\$		12.	18.	24.	30.	36.
\$	42.	48.	54.	60.	66.	72.
\$	78.	84.	90.	96.	102.	108.
\$	114.	120.	126.	132.	138.	144.

DATA EJCST/

\$		.560,	1.11,	1.66,	2.17,	2.69,
\$	4.24,	5.80,	7.24,	8.69,	10.1,	11.5,
\$	14.0,	16.5,	19.8,	23.2,	25.9,	30.6,
\$	34.1,	37.7,	41.2,	44.7,	48.2,	51.7

DATA ELCST/

\$		.437,	.999,	1.55,	2.12,	2.68,
\$	3.24,	7.05,	12.0,	16.9,	20.3,	23.6,
\$	27.4,	31.1,	34.9,	38.7,	43.1,	47.4,
\$	51.7,	74.8,	77.9,	90.9,	88.0,	95.1

DATA EL45/

\$		.300,	.670,	1.03,	1.37,	1.71,
\$	2.05,	4.77,	8.94,	13.1,	15.4,	17.6,
\$	20.0,	22.4,	25.0,	27.6,	30.6,	33.6,

```

      $ 35.6 , 51.9 , 56.4 , 50.9 , 65.0 , 69.0 /
C
60 DATA FLGCST/
   $      .342,      .618,      .893,      1.15 ,      1.40 ,
   $ 1.93 , 2.47 , 3.22 , 3.97 , 5.55 , 7.13 ,
   $ 9.82 , 12.5 , 14.7 , 17.0 , 20.5 , 24.9 ,
65 $ 25.6 , 27.3 , 28.9 , 30.6 , 32.2 , 33.9 /
C
   DATA PIIPCST/
   $      .096,      .127,      .157,      .189,      .221,
   $      .253,      .353,      .402,      .441,      .472,      .503,
   $      .548,      .593,      .634,      .675,      .697,      .719,
70 $      .741,      .963,      1.03 ,      1.09 ,      1.17 ,      1.24 /
C
   DATA REFCST/
   $      .365,      .455,      .545,      .798,      1.05 ,
   $ 1.38 , 1.55 , 2.91 , 4.26 , 4.99 , 5.71 ,
75 $ 5.95 , 8.19 , 8.37 , 8.55 , 12.7 , 16.8 ,
   $ 20.9 , 35.9 , 42.9 , 49.9 , 56.9 , 63.8 /
   DATA TEECST/
   $      .494,      1.29 ,      2.09 ,      2.59 ,      3.08 ,
   $ 3.57 , 7.37 , 12.1 , 16.8 , 20.1 , 23.3 ,
80 $ 23.1 , 26.8 , 31.0 , 35.2 , 39.1 , 43.0 ,
   $ 46.9 , 68.6 , 74.9 , 81.2 , 87.8 , 94.4 /
C
   DATA VACST/
   $      3.64 ,      6.16 ,      8.67 ,      11.2 ,      13.8 ,
85 $ 17.4 , 21.0 , 27.7 , 34.3 , 37.4 , 40.4 ,
   $ 45.0 , 51.7 , 58.6 , 65.6 , 70.5 , 75.5 ,
   $ 80.5 , 85.5 , 90.6 , 95.6 , 101. , 106. /
C
90 DO 40 I=1,230
   X(I) = APIPCST(I)
40 CONTINUE
   RETURN
   END

```

```

SUBROUTINE P75
COMMON /PIP75 / APIPCST(23), DIAM(23), EJCST(23), ELCST(23)
$, FLGCST(23)
$, EL45(23), PIPCST(23), REDCST(23), TEECST(23), VACST(23)
COMMON /CPIPE/ X(230)

```

```

THIS SUBROUTINE SUPPLIES UNIT COST DATA TO SUBROUTINE
PIPCRT FOR PIPING SYSTEM COMPONENTS DESIGNED FOR
75 PSI. THIS DATA IS CALLED BY USING A VALUE OF
DPRESS= 75 (DPRESS=PIPING DESIGN PRESSURE) ON CARD 61
OF THE INPUT. THUS, ANY COST DATA CAN BE SUBSTITUTED HERE
FOR STUDY PURPOSES.

```

DEFINITION OF VARIABLES

```

APIPCST - ABOVE GROUND PIPE COST ($1000/FT)
DIAM     - COMPONENT DIAMETER (INCHES)
EJCST    - EXPANSION JOINT COST ($1000)
ELCST    - 90 DEGREE ELBOW COST ($1000)
EL45     - 45 DEGREE ELBOW COST ($1000)
FLGCST   - FLANGE COST ($1000)
PIPCST   - BELOW GROUND PIPE COST ($1000/FT)
REDCST   - REDUCER COST ($1000)
TEECST   - TEE COST ($1000)
VACST    - VALVE COST ($1000), VALVES ARE MOTOR OPERATED
          BUTTERFLY VALVES

```

75 PSI

DATA APIPCST/

\$		.056,	.074,	.092,	.112,	.132,
\$	.152,	.240,	.265,	.290,	.322,	.353,
\$	.385,	.471,	.501,	.530,	.576,	.622,
\$	.652,	.681,	.711,	.879,	.922,	.965,

DATA DIAM/

\$		12.	18.	24.	30.	36.
\$	42.	48.	54.	60.	66.	72.
\$	78.	84.	90.	96.	102.	108.
\$	114.	120.	126.	132.	138.	144.

DATA EJCST/

\$		.560,	1.11,	1.66,	2.17,	2.69,
\$	4.24,	5.80,	7.24,	8.59,	10.1,	11.5,
\$	14.0,	16.5,	19.8,	23.2,	26.9,	30.6,
\$	34.1,	37.7,	41.2,	44.7,	48.2,	51.7,

DATA ELCST/

\$		.437,	1.00,	1.56,	2.12,	2.68,
\$	3.24,	7.05,	12.0,	16.9,	20.3,	23.6,
\$	27.0,	39.2,	43.9,	48.6,	53.7,	58.7,
\$	66.8,	74.8,	82.9,	97.0,	106.	114.

DATA EL45/

\$		.300,	.665,	1.03,	1.37,	1.71,
\$	2.05,	4.77,	8.94,	13.1,	15.4,	17.6,
\$	19.9,	28.8,	32.1,	35.3,	38.9,	42.5,

```

C      $ 47.2 , 51.9 , 56.6 , 74.3 , 79.3 , 84.3 /
60      C      DATA FLGCST/
          $      .342, .618, .893, 1.15 , 1.40 ,
          $ 1.93 , 2.47 , 3.22 , 3.97 , 5.55 , 7.13 ,
          $ 9.82 , 12.5 , 14.7 , 17.0 , 20.5 , 24.0 ,
          $ 25.6 , 27.3 , 28.9 , 30.6 , 32.2 , 33.9 /
65      C      DATA PIPCST/
          $      .096, .127, .157, .189, .221,
          $ .253, .363, .402, .441, .472, .503,
          $ .534, .669, .713, .757, .815, .874,
          $ .919, .963, 1.08 , 1.19 , 1.28 , 1.36 /
70      C      DATA REDCST/
          $      .365, .455, .545, .798, 1.05 ,
          $ 1.36 , 1.55 , 2.91 , 4.26 , 4.99 , 5.71 ,
          $ 5.95 , 10.9 , 11.1 , 11.3 , 15.3 , 21.2 ,
          $ 28.6 , 35.9 , 43.3 , 62.5 , 71.2 , 79.9 /
          C      DATA TRECST/
          $      .494, 1.29 , 2.09 , 2.59 , 3.08 ,
          $ 3.57 , 7.37 , 12.1 , 16.8 , 20.1 , 23.3 ,
          $ 25.1 , 38.0 , 41.5 , 45.0 , 49.7 , 54.3 ,
          $ 61.5 , 68.6 , 75.8 , 99.1 , 107. , 115. /
          C      DATA VACST/
          $      3.64 , 6.16 , 8.67 , 11.2 , 13.8 ,
          $ 17.4 , 21.0 , 27.7 , 34.3 , 37.4 , 40.4 ,
          $ 45.0 , 51.7 , 58.6 , 65.6 , 70.5 , 75.5 ,
          $ 80.5 , 85.5 , 90.6 , 95.6 , 101. , 106. /
90      C      DO 40 I=1,230
          X(I) = APIPCST(I)
          40 CONTINUE
          RETURN
          END

```

```

SUBROUTINE P125
COMMON /PIP125/ APIPCST(23), DIAM(23), EJCST(23), ELCST(23)
$, FLGCST(23)
$, EL45(23), PIPCST(23), REDCST(23), TEECST(23), VACST(23)
COMMON /CPIPE/ X(230)

```

```

C      THIS SUBROUTINE SUPPLIES UNIT COST DATA TO SUBROUTINE
C      PIPCRT FOR PIPING SYSTEM COMPONENTS DESIGNED FOR
C      50 PSI. THIS DATA IS CALLED BY USING A VALUE OF
10    OPRESS= 50. (OPRESS=PIPING DESIGN PRESSURE) ON CARD G1
C      OF THE INPUT. THUS, ANY COST DATA CAN BE SUBSTITUTED HERE
C      FOR STUDY PURPOSES.

```

DEFINITION OF VARIABLES

```

15    C      APIPCST - ABOVE GROUND PIPE COST ($1000/FT)
C      DIAM      - COMPONENT DIAMETER (INCHES)
C      EJCST     - EXPANSION JOINT COST ($1000)
C      ELCST     - 90 DEGREE ELBOW COST ($1000)
20    C      EL45  - 45 DEGREE ELBOW COST ($1000)
C      FLGCST    - FLANGE COST ($1000)
C      PIPCST    - BELOW GROUND PIPE COST ($1000/FT)
C      REDCST    - REDUCER COST ($1000)
C      TEECST    - TEE COST ($1000)
25    C      VACST  - VALVE COST ($1000); VALVES ARE MOTOR OPERATED
C      BUTTERFLY VALVES

```

125 PSI

DATA APIPCST/

```

30    $      .056, .074, .092, .110, .158,
$      .204, .240, .276, .350, .386, .421,
35    $      .457, .555, .653, .718, .787, .822,
$      .858, .893, .928, 1.11, 1.16, 1.21

```

DATA DIAM/

```

40    $      12. , 18. , 24. , 30. , 36. ,
$      42. , 48. , 54. , 60. , 66. , 72. ,
$      78. , 84. , 90. , 96. , 102. , 108. ,
$      114. , 120. , 126. , 132. , 138. , 144.

```

DATA EJCST/

```

45    $      .560, 1.11, 1.66, 2.17, 2.69,
$      4.24, 5.80, 7.24, 8.69, 10.1, 11.5,
$      14.0, 15.5, 19.8, 23.2, 26.9, 30.6,
$      34.1, 37.7, 41.2, 44.7, 48.2, 51.7

```

DATA ELCST/

```

50    $      .437, .999, 1.55, 2.12, 3.47,
$      5.26, 7.05, 8.84, 21.5, 25.7, 29.9,
$      34.1, 47.6, 62.8, 59.4, 76.1, 82.7,
$      93.9, 105. , 116. , 130. , 141. , 152.

```

DATA EL45/

```

55    $      .300, .665, 1.03, 1.40, 2.33,
$      3.55, 4.77, 5.99, 15.0, 18.9, 22.7,
$      26.6, 35.5, 45.7, 51.7, 56.7, 61.7

```

```

60      C      $ 65.0 , 68.3 , 71.6 , 102. , 109. , 116. /
          DATA FLGCST/
          $      .342, .618, .893, 1.15 , 1.40 ,
          $ 1.93 , 2.47 , 3.22 , 3.97 , 5.55 , 7.13 ,
          $ 9.82 , 12.5 , 14.7 , 17.0 , 20.5 , 24.0 ,
          $ 25.6 , 27.3 , 28.9 , 30.6 , 32.2 , 33.9 /
65      C      DATA PIPCST/
          $      .096, .127, .157, .188, .257,
          $ .310, .363, .416, .501, .537, .572,
          $ .617, .753, .884, .946, 1.01 , 1.07 ,
          $ 1.13 , 1.18 , 1.23 , 1.43 , 1.52 , 1.60 /
70      C      DATA REDCST/
          $      .355, .455, .545, .635, 1.55 ,
          $ 2.44 , 3.33 , 4.22 , 5.63 , 6.61 , 7.58 ,
          $ 8.54 , 13.9 , 15.9 , 17.8 , 24.3 , 30.8 ,
          $ 45.5 , 62.1 , 77.7 , 88.5 , 101. , 113. /
80      C      DATA TEECST/
          $      .494, 1.29 , 2.09 , 2.89 , 4.22 ,
          $ 5.85 , 7.37 , 5.95 , 21.9 , 26.0 , 30.1 ,
          $ 34.2 , 47.0 , 59.8 , 66.2 , 72.7 , 79.1 ,
          $ 89.4 , 99.7 , 110. , 136. , 147. , 157. /
85      C      DATA VACST/
          $      3.64 , 6.16 , 8.67 , 11.2 , 13.8 ,
          $ 17.4 , 21.0 , 27.7 , 34.3 , 37.4 , 40.4 ,
          $ 45.0 , 51.7 , 58.6 , 55.6 , 70.5 , 75.5 ,
          $ 80.5 , 85.5 , 90.6 , 95.6 , 101. , 106. /
90      C      DO 40 I=1,230
          X(I) = APIPCST(I)
40      CONTINUE
          RETURN
          END

```

SUBROUTINE PIPCRT (TS, W3, ITD, TR, TOWERD, DELHX, DELCON, DIST,
 DESVEL, REDUCE, DREDUCE, BUNWIDT, TUBOEP,
 TRANPIT, COST, NCTOW, POP, EPDP, HPWAY,
 RHO, CDANG, POHCIR, POHLEC, EFFP)

THIS SUBROUTINE DESIGNS AND COSTS THE PIPING SYSTEM. THE PIP-
 ING SYSTEM INCLUDES ALL THE PIPE, VALVES, PUMPS AND FITTINGS
 BETWEEN THE CONDENSER AND THE HEAT EXCHANGER. PIPE DIAMETER
 IS DETERMINED FROM THE WATER FLOW RATE AND THE DESIGN
 VELOCITY. VALVE AND FITTING SIZES CORRESPOND TO THE PIPE
 SIZES WITH THE SAME FLOW RATE. THE PUMPS ARE SIZED
 ACCORDING TO TOTAL FLOW RATE AND TOTAL DYNAMIC HEAD.

THE SUPPLY AND RETURN PIPING DESIGNS ARE IDENTICAL ALTHOUGH
 DIFFERENCES IN WATER PROPERTIES ARE ACCOUNTED FOR IN THE HEAD
 LOSS AND PRESSURE DROP. COSTS FOR SUBSYSTEMS OF THE PIPING
 ARE MULTIPLIED BY A FACTOR OF TWO TO ACCOUNT FOR BOTH THE
 SUPPLY AND RETURN PIPING. THE PUMP STATION IS PROVIDED IN
 THE RETURN PIPING ONLY. THE COST AND PRESSURE DROP OF THE
 RETURN PIPING ACCOUNTS FOR THE LENGTH OF THE PUMP STATION
 WHICH IS ASSUMED TO BE 50 FEET.

DEFINITION OF VARIABLES

BUNGPM - WATER FLOW RATE TO EACH TUBE BUNDLE (GPM)
 BUNWIDT - TUBE BUNDLE WIDTH (FT)
 COST - TOTAL COST OF WATER CIRCULATION PIPING SYSTEM
 (\$1000)
 CBGP - PIPING COST PER TOWER GROUP (\$1000)
 CPTOW - PIPING COST PER TOWER (\$1000)
 CTOW - NUMBER OF CIRCULAR TOWERS
 DELCON - PRESSURE DROP IN CONDENSER (PSF)
 DELFIT - PRESSURE DROP IN BUNDLE FITTINGS (PSF)
 DELHX - PRESSURE DROP IN HEAT EXCHANGER (PSF)
 DELPUMP - PRESSURE DROP IN PUMP STATION PIPING (PSF)
 DELRET - PRESSURE DROP IN WATER CIRCULATION PIPING, RETURN
 SYSTEM (PSF)
 DELSUP - PRESSURE DROP IN WATER CIRCULATION PIPING,
 SUPPLY SYSTEM (PSF)
 DELSURE - TOTAL PRESSURE DROP IN WATER CIRCULATION PIPING
 (PSF)
 DELTD - PRESSURE DROP IN TOWER PIPING (PSF)
 DESVEL - PIPING SYSTEM WATER DESIGN VELOCITY (FT/SEC)
 DIAO - DIAMETER OF DISTRIBUTION PIPING (INCHES)
 DIAH - DIAMETER OF PIPE COMPONENTS FOR MAIN CIRCULATION
 HEADER (INCHES)
 DIAQ - DIAMETER OF PIPE COMPONENTS OF QUADRANT
 HEADER (INCHES)
 DIAT - DIAMETER OF TOWER PIPING (INCHES)
 DIST - DISTANCE FROM CONDENSER OUTLET TO BOUNDARY OF
 TOWER GROUP (FT)
 DSGTM - DISTANCE FROM ELECTRIC SWITCH GEAR TO PUMP MOTOR
 (FT)
 DYNHEAD - DYNAMIC HEAD SEEN BY PUMPS (FT OF WATER)
 EFFP - PUMP EFFICIENCY (DECIMAL FRACTION)
 EJOCST - EXPANSION JOINT COST (\$1000)

	C	ELCST	- 90 DEGREE ELBOW COST (\$1000)
	C	EL45	- 45 DEGREE ELBOW COST (\$1000)
60	C	EQLEN	- EQUIVALENT LENGTH (FT)
	C	EQLEND	- EQUIVALENT LENGTH OF DISTRIBUTION PIPING (FT)
	C	EQLENT	- EQUIVALENT LENGTH OF TOWER PIPING (FT)
	C	EQLFIT	- EQUIVALENT LENGTH OF BUNDLE FITTINGS (FT)
	C	EQLPUMP	- EQUIVALENT LENGTH OF PIPE IN PUMP STATION (FT)
65	C	FLGCST	- FLANGE COST (\$1000)
	C	FRG	- FLOW TO COMPLETE TOWER GROUPS (LBM/HR)
	C	GPCST	- COST OF PIPING FOR MAIN CIRCULATION HEADERS (\$1000)
	C	GGGPM	- FLOW RATE TO COMPLETE TOWER GROUPS (GPM)
70	C	GMCIRC	- FLOW RATE TO EACH CIRCULAR TOWER (GPM)
	C	GPMMAX	- MAXIMUM FLOW RATE THAT CAN BE TRANSPORTED THROUGH LARGEST DIAMETER PIPE AVAILABLE AT THE GIVEN DESIGN VELOCITY (GPM)
	C	GPMTOT	- TOTAL WATER FLOW RATE (GPM)
	C	HFD	- HEAD LOSS (FT OF WATER/100 FT OF EQUIVALENT LENGTH)
75	C	HEAD1,2	- HEAD LOSS FOR EQLEND, SUPPLY (1) AND RETURN (2), (FT/100 FT)
	C	HEAT1,2	- HEAD LOSS FOR EQLENT, SUPPLY (1) AND RETURN (2), (FT/100 FT)
	C	HEDR	- LENGTH OF MAIN CIRCULATION HEADER SECTIONS (FT)
80	C	HPPMP	- HORSE POWER PER PUMP (HP)
	C	HPWAT	- REQUIRED PUMP HORSE POWER (HP)
	C	IPRESS	- PIPING COMPONENT DESIGN PRESSURE (PSI)
	C	NTUNPQD	- TUBE BUNDLES PER QUADRANT
	C	NTOW	- CTOW
85	C	NFL	- UPPER LIMIT FOR NUMBER OF TOWERS OR TUBE BUNDLES PER QUADRANT
	C	NPS	- NUMBER OF POSITIONS IN UNIT COST ARRAYS
	C	NPMP	- TOTAL NUMBER OF PUMPS
	C	NPX	- NUMBER OF PUMPS SERVING EXTRA TOWER GROUP
90	C	NTOWGSP	- NUMBER OF COMPLETE TOWER GROUPS
	C	NTOWGSP	- NUMBER OF TOWERS PER GROUP
	C	NTUBPBU	- NUMBER OF TUBES PER BUNDLE
	C	PDIA	- DIAMETER OF PUMP STATION PIPING COMPONENTS (INCHES)
	C	PP	- PRESSURE DROP IN PIPING SYSTEM (PSF)
95	C	PIPCOST	- COST OF STRAIGHT PIPE FOR ONE HEADER SECTION OF MAIN CIRCULATION PIPING (\$1000)
	C	PTSCOS	- TOTAL PIPING SYSTEM COST (\$1000)
	C	PNELEC	- PUMP MOTOR ELECTRIC COST (\$)
	C	POHCIR	- INDIRECT COST FACTOR FOR CIRCULATION PIPING
100	C	POHLEC	- INDIRECT COST FACTOR FOR ELECTRICAL REQUIREMENTS
	C	PROP	- WATER PROPERTIES ARRAY
	C	PSTACST	- COST OF PUMP STATION FOR COMPLETE TOWER GROUP- PIPING AND PUMPS (\$1000)
	C	PUPITS	- COST OF PIPING COMPONENTS IN PUMP STATION OF COMPLETE TOWER GROUP (\$1000)
105	C	PUMPCST	- PUMP COSTS FOR COMPLETE TOWER GROUP (\$1000)
	C	QDELRSR	- PRESSURE DROP IN QUADRANT HEADER RETURN (R), SUPPLY (S), SUPPLY AND RETURN (SR) (PSF)
	C	QELCST	- COST OF ELBOW ON LAST QUADRANT HEADER SECTION (\$1000)
110	C	QHDCST	- TOTAL COST OF QUADRANT HEADER PIPING COMPONENTS (\$1000)
	C	QHEDR	- LENGTH OF SECTION OF QUADRANT HEADER (FT)
	C	QPIPCST	- COST OF STRAIGHT PIPE FOR ONE QUADRANT HEADER

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115      C      SECTION ($1000)
      C      QPDCST - QUADRANT REDUCER COST ($1000)
      C      QREDUCE - VALUE OF ALLOWABLE REDUCTION IN PIPE DIAMETER
      C      BETWEEN ADJACENT QUADRANT HEADER SECTIONS. CAN BE
      C      ZERO OR MULTIPLE OF SIX (INCHES)
120      C      QTECST - QUADRANT TEE COST ($1000)
      C      GTPCST - PIPE COMPONENTS COST FOR ONE QUADRANT
      C      HEADER ($1000)
      C      QUADGPM - FLOW RATE TO ONE QUADRANT (GPM)
      C      REDCOST - REDUCER COST ($1000)
125      C      REDUCE - VALUE OF ALLOWABLE REDUCTION IN PIPE DIAMETER
      C      BETWEEN ADJACENT HEADER SECTIONS OF MAIN CIRCULA-
      C      TION PIPING. CAN BE ZERO OR MULTIPLE OF SIX
      C      (INCHES)
      C      RHO,1,2 - DENSITY OF WATER AVERAGE, SUPPLY (1), RETURN (2)
130      C      (LBM/CU FT)
      C      TDCST - DISTRIBUTION AND TOWER PIPING COSTS ($1000)
      C      TF - WATER TEMPERATURE LEAVING CONDENSER (DEG F)
      C      TEECOST - TEE COST ($1000)
      C      TAPCST - TOTAL COST OF MAIN CIRCULATION HEADERS ($1000)
135      C      TH20 - WATER TEMPERATURE (DEG F)
      C      TI - WATER TEMPERATURE ENTERING CONDENSER (DEG F)
      C      TOWDIA - TOWER DIAMETER (FT)
      C      TPCST - TOTAL COST OF PUMP STATIONS ($1000)
      C      TQDCST - TOTAL COST OF QUADRANT HEADERS ($1000)
140      C      TR - TEMPERATURE RANGE OF WATER (DEG F)
      C      TRANPIT - TRANSVERSE TUBE PITCH (INCHES)
      C      TTRMA - TERMS IN PUMP ELECTRIC CHARGES DETERMINED BY
      C      TOMB, EMPIRICAL COST CORRELATIONS
      C      TQMC
145      C      TS - STEAM SATURATION TEMPERATURE (DEG F)
      C      TTD - CONDENSER TERMINAL TEMPERATURE DIFFERENCE (DEG F)
      C      TTDOST - TOTAL COST OF TOWER DISTRIBUTION PIPING ($1000)
      C      THBDEP - HEAT EXCHANGER TUBE ROWS IN DIRECTION OF AIR FLOW
      C      UBIPCST - UNIT COST OF STRAIGHT PIPE ($/FT)
150      C      VACST - VALVE COST ($1000)
      C      VFO - ACTUAL WATER VELOCITY (FT/SEC)
      C      VELOCIT - ACTUAL VELOCITY IN BUNDLE FITTINGS OR PUMP STATION
      C      PIPING (FT/SEC)
      C      VELOD - ACTUAL VELOCITY IN DISTRIBUTION PIPING (FT/SEC)
155      C      VFLOT - ACTUAL VELOCITY IN TOWER PIPING (FT/SEC)
      C      VIS,1,2 - WATER VISCOSITY AVERAGE, SUPPLY(1), RETURN(2),
      C      (LBM/FT HR)
      C      VV - PUMP MOTOR VOLTAGE (VOLTS)
      C      VC - PUMP SYSTEM VOLTAGE (VOLTS)
160      C      W3 - CIRCULATION WATER FLOW RATE (LBM/HR)
      C      XTOW - CTOW
      C
      C      VARIABLES APPLYING TO EXTRA TOWER GROUP WITH COUNTERPARTS
      C      FOR COMPLETE TOWER GROUPS
165      C
      C      ERELPM - DELPUMP
      C      ERELSR - DELSURE
      C      EDYNHD - DYNHEAD
      C      EFJCST - EJCST
170      C      EFLGCST - FLGCST
      C      EGPCST - GPCST

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C      EDDIA - PDIA
C      EDDP - PDP
C      EDMPCST - PUMPCST
775 C      EPCST - PSTACST
C      EPUFITS - PUFITS
C      EVCST - GPGP
C      EYFLO - FPG
C      EXGPM - GPGPM
780 C      NEXTOW - NTOWPGP
C
      DIMENSION VELO(200), UIPICST(200)
      COMMON /CPIPE / APIPCST(23), DIAM(23), EJCST(23), ELCST(23)
      $, FLGCST(23)
785 $, ELAQ(23), PIPICST(23), REDCST(23), TEECST(23), VACST(23)
      COMMON /PRESS/ IPRESS
      COMMON /PH20/ TH20(16), PROP(16,2)
      LOGICAL CALL 1
      COMMON /RPRT1/
790 $, RJNGPM
      $, DYNHFD, DIAD, DIAT, DIAH(200), DIAQ(200)
      $, EPCST, EGPCST, EPMPCST, EPUFITS, EDYNHD, EXGPM, EJCST, ELCST
      $, FLGCST
      $, GPMCTRC, GPGPM, GPCST
795 $, HEDR(200)
      $, JSAVE
      $, LSAVE
      $, NTURBRU, NRUNPD, NTOWGPS, NTOWPGP, NEXTOW
      $, PSTACST, PUFITS, PUMPCST, PIPICST(200), PISCOS
800 $, QHDCST, QUADGPM, QIPICST(200), QHEDR(200), QTECST(200)
      $, QRDCST(200), QELCST
      $, REDCST(200), RPTPL
      $, TEECST(200), TPCST, TDCST, TTDCST, TGPCST, TOWDIA, TRDCST
      $, XTOW
805 COMMON /PME/ PMELEC
      DATA CALL 1 /.TRUE./
      DATA DEGTM /100./
      DATA NFS /23/, NFL /200/
810
C
C      CALL THE APPROPRIATE SUBROUTINE TO ESTABLISH UNIT COST DATA
C      FOR THE PIPING SYSTEM COMPONENTS.
C
815 IF (CALL 1 .AND. IPRESS .EQ. 50) CALL P50
      IF (CALL 1 .AND. IPRESS .EQ. 75) CALL P75
      IF (CALL 1 .AND. IPRESS .EQ. 125) CALL P125
      CALL 1 = .FALSE.
      XTOW = NCTOW
      CTOW = NCTOW
820 TOWDIA = TOWERD
      DO 1 I=1,NFL
1 REDCST(I)=0.
      TE=TS-TTD
825
C
C      USE WATER TEMPERATURE TO SET WATER PROPERTIES.
C
      TI=TE-TR
      VISI=TLU(TE,TH20,PROP(1,2),15)

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230      RH01=TLU(TE,TH20,PROP,16)
      VIS2=TLU(TI,TH20,PROP(1,2),16)
      RH02=TLU(TI,TH20,PROP,16)
      RHO=(RH01+RH02)/2.
      VIS=(VIS1+VIS2)/2.
235      GPMTOT = W3/(60.*RHO/7.481)
      NTUBPGH=12.*BUNWIDT*TUBOEP/TRANPT
      CONST1=(3.1416/4.)*7.481*60.*DESVEL
      CONST2=(4./3.1416)*144./(60.*7.481)
      GPMCIRC=GPMTOT/CTOW
240      GPM4AX = (DIAM(NFS)**2/144.) * CONST1
      NTOWPGH=GPM4AX/GPMCIRC

      C
      C      IF THE FLOW TO ONE TOWER EXCEEDS THE FLOW THAT CAN BE
      C      TRANSPORTED THROUGH THE LARGEST DIAMETER PIPE THEN REJECT
      C      THIS DESIGN CONDITION.
245      C
      C      A TOWER GROUP CONSISTS OF ALL THE TOWERS SUPPLIED BY A SINGLE
      C      MAIN CIRCULATION PIPING HEADER. THE NUMBER OF TOWERS PER
      C      GROUP (NTOWPGH) CANNOT EXCEED THE MAXIMUM FLOW AVAILABLE IN
      C      THE LARGEST PIPE DIAMETER DIVIDED BY THE FLOW PER TOWER
250      C      (GPMCIRC).
      C

      IF(NTOWPGH.LT.1) COST = 1.E+40
      IF(NTOWPGH.LT.1) WRITE(6,6767)
6767  FORMAT('01N PIPING ROUTINE NUMBER OF TOWERS PER GROUP =0 WAS
255      $ REJECTED')
      IF(NTOWPGH.LT.1) RETURN
      IF(NTOWPGH.GT.CTOW) NTOWPGH=CTOW +1.E-40
      NTOWGPS=CTOW/NTOWPGH

      C
260      C      IF THE NUMBER OF CIRCULAR TOWERS EXCEEDS THE NUMBER OF TOWERS
      C      PER GROUP AND IS NOT AN EVEN MULTIPLE OF THE NUMBER OF TOWERS
      C      PER GROUP (E.G.-NCTOW=12, NTOWPGH=5) THEN A SEPARATE MAIN
      C      CIRCULATION HEADER AND PUMP STATION IS DESIGNED FOR THE
      C      NUMBER OF EXTRA TOWERS (NEXTOW, IN THIS CASE NEXTOW=2) AND
265      C      THE TOTAL FLOW TO THOSE EXTRA TOWERS (EXGPM). THIS SO
      C      CALLED "EXTRA TOWER GROUP" WILL BE DIFFERENT FROM THE MAIN
      C      TOWER GROUPS ONLY WITH RESPECT TO THE NUMBER OF TOWERS IN
      C      THE GROUP AND THE SIZE OF MAIN CIRCULATION PIPING. ALL THE
      C      PIPING ASSOCIATED WITH THE TOWER PIPING AND QUADRANT PIPING
270      C      IS UNAFFECTED BY THE EXTRA TOWER PROBLEM. THE LENGTH OF
      C      THE MAIN CIRCULATION HEADER SECTIONS IS ALSO UNAFFECTED.
      C      SINCE THERE IS LESS TOTAL FLOW TO THE EXTRA GROUP THE PIPE
      C      DIAMETER OF THE EXTRA GROUP MAIN CIRCULATION HEADER IS
275      C      SMALLER AND THE PUMP STATION REQUIREMENTS ARE REDUCED.
      C

      NEXTOW=CTOW-NTOWPGH*NTOWGPS
      EXGPM=NEXTOW*GPMCIRC
      GPXGPM=NTOWPGH*GPMCIRC
      QUADGPM=GPMCIRC/4.
280      NBUNPGH = (TOWDIA*3.14159)/(4.*BUNWIDT*COANG) +1.
      BUNSPM=QUADGPM/NBUNPGH

      C
      C      SIZE THE DISTRIBUTION PIPING.
285      C
      DIAO=SQRT(GPMCIRC/CONST1)*12.

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      DO 10 NT = 1,NFS
      ID = NT
      IF (DIAD-DIAM(ID))11,11,10
290 10 CONTINUE
      C
      C      SIZE THE TOWER PIPING.
      C
      11 DIAD=DIAM(ID)
      DIAT=SQRT(QUADGPM/CONST1)*12.
      DO 12 NT = 1,NFS
      IT = NT
      IF (DIAT-DIAM(IT))13,13,12
295 12 CONTINUE
      13 DIAT=DIAM(IT)
      C
      C      DETERMINE THE HEAD LOSS AND PRESSURE DROP IN THE DISTRIBUTION
      C      AND TOWER PIPING. THIS INCLUDES THE PIPING FROM THE MAIN
      C      CIRCULATION HEADER TO THE QUADRANT HEADER.
      C
      300 EQLEND=.2*TOWDIA+200.*DIAD/12.
      VELOD=(GPM/CIRC/DIAD**2)*CONST2
      EQLENT=TOWDIA+60.*DIAT/12.
      VELOT=(QUADGPM/DIAT**2)*CONST2
      305 CALL HYDLOS(DIAD,VELOD,VIS1,RHO1,2,HEAD1)
      CALL HYDLOS(DIAD,VELOD,VIS2,RHO2,2,HEAD2)
      310 CALL HYDLOS(DIAT,VELOT,VIS1,RHO1,2,HEAT1)
      CALL HYDLOS(DIAT,VELOT,VIS2,RHO2,2,HEAT2)
      DELTD=(EQLEND*(HEAD1*RHO1+HEAD2*RHO2)+EQLENT*(HEAT1*RHO1+HEAT2*
      SRHO2))/100.
      315
      C
      C      DETERMINE THE COST OF THE DISTRIBUTION AND TOWER PIPING.
      C
      C      THE DISTRIBUTION AND TOWER PIPING COST (TDCST) INCLUDES THE
      C      LENGTH OF PIPE (.2*TOWDIA) CONNECTING THE MAIN CIRCULATION
      320 HEADER TO THE TOWER DISTRIBUTION HEADER AND THE PIPE
      C      CONNECTING THE TOWER DISTRIBUTION HEADER TO THE QUADRANT
      C      HEADERS (ASSUMED TO TOTAL 3.25*TOWDIA). THE TOWER DISTRIBUTION
      C      HEADER IS COSTED AS FOUR PIPE TEES. THE TEE IS COSTED
      C      AS .67 TIMES THE COST OF A TEE OF THE "RUN" DIAMETER PLUS
      325 .33 TIMES THE COST OF A TEE OF THE "BRANCH" DIAMETER.
      C
      TDCST=.2*TOWDIA*PIPCST(ID)+4.*(0.67*TEECST(ID)+.33*TEECST(IT))
      +3.25*TOWDIA*PIPCST(IT)+10.*ELCST(IT)+2.*EL45(IT)+4.*VACST(IT)
      +8.*FLGCST(IT)
      330 TDCST=P.*TDCST
      C
      C      DESIGN AND COST THE QUADRANT PIPING.
      C
      335 CALL HEADER(QUADGPM,NBUNPOD,BUNGPM,QREDUCE,1,L,DIAD,QRDCST,QTECST,
      SQELCST,UPIPCST,VELO,QEJCST,QFLGCST,QSVEL)
      LSAVE = L
      QDEL5=.
      QDELP=.
      QTRCST=.
      340 IF (L.GT.NFL) COST = 1.E+40
      IF (L.GT.NFL) RETURN
      DO 20 KK=1,L

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345 I = KK
    IF(I.GT.1) GO TO 21
    QHEADR(I)=0.

    THE LENGTH OF STRAIGHT PIPE FOR QUADRANT HEADER SECTION I
    ACCOUNTS FOR THE LENGTH OF THE TEE AS BEING 1.75 TIMES THE
    DIAMETER OF THE TEE. NO ALLOWANCE IS MADE FOR REDUCER
    LENGTH.

350 GO TO 22

    DETERMINE THE HEAD LOSS AND PRESSURE DROP IN THE QUADRANT
    PIPING.

355 21 QHEADR(I) = BUNWIDT * CDANG * DIAQ(I) * 1.75 / 12.
    22 EQLEN=QHEADR(I)+20.*DIAQ(I)/12.
    CALL HYDLOS(DIAQ(I),VELO(I),VIS1,RH01,2,HEAD1)
    CALL HYDLOS(DIAQ(I),VELO(I),VIS2,RH02,2,HEAD2)
    QDELS=QDELS+HEAD1*RH01*EQLEN/100.
    QDELR=QDELR+HEAD2*RH02*EQLEN/100.
    QPIPCST(I)=QHEADR(I)*UPIPCST(I)
    IF(I.LT.L) QTPCST=QTPCST+QPIPCST(I)+QRDCST(I)+QTECST(I)
    IF(I.EQ.L) QTPCST=QTPCST+QPIPCST(I)+QRDCST(I)+QELCST
360 20 CONTINUE

    THE FITTINGS AND PIPE CONNECTING THE QUADRANT HEADER TO
    THE BUNDLE HEADER ARE GIVEN A DIAMETER OF 8 INCHES AND
    ESTIMATED TO COST $1.75 X 10**3 TOTAL FOR EACH TUBE BUNDLE.

370 QDELSR=(QDELS+QDELR)/2.
    QHDCST=QTPCST*2.+1.75*NBUNPQDI

    DESIGN AND COST THE MAIN CIRCULATION PIPING FOR THE
    EXTRA TOWER GROUP.

    VARIABLES DEFINING CONDITIONS IN THE EXTRA TOWER GROUP ARE
    GENERALLY RESET TO A ZERO VALUE EACH TIME PIPCRT IS CALLED SO
    THAT STORED VALUES FROM A PREVIOUS CALCULATION WILL NOT BE
    INCORRECTLY INCLUDED. IF THERE ARE NO EXTRA TOWERS
    SPECIFIED THEN BY-PASS THIS SET OF CALCULATIONS.

385 EDELSR=0.
    EPDIA=0.
    EGPCST=0.
    EEJCST=0.
    EFLGCST=0.
    IF(NEXTOW.EQ.0) GO TO 35
    CALL HEADER(EXGPM,NEXTOW,GPMYCIRC,REDUCE,0,JEX,DIAH,REDCOST,TEECOST
    ,ELCOST,UPIPCST,VELO,EEJCST,EFLGCST,DESVEL)
    DELSUP=0.
    DELRET=0.
    EGPCST=0.
    IF(JEX.GT.NFL) COST = 1.E+40
    IF(JEX.GT.NFL) RETURN

    THE HEADER SECTION FROM THE CONDENSER TO THE FIRST TOWER

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400      C      IS HEADER SECTION 1. THEN, ALL EVEN NUMBER HEADER SECTIONS
      C      ARE GIVEN ZERO LENGTH BECAUSE TOWERS ARE MATCHED ON OPPOSITE
      C      SIDES OF THE MAIN CIRCULATION HEADER.
      C
      DO 30 I2=1,JEX
405      I = I2
      IF(I.EQ.1) GO TO 31
      IF(MOD(I,2).EQ.0) HEDR(I)=0.
      IF(MOD(I,2).NE.0) HEDR(I)=1.5*TOWDIA

410      C      DETERMINE THE HEAD LOSS AND PRESSURE DROP IN THE MAIN CIRC-
      C      ULATION PIPING TO THE EXTRA TOWER GROUP.
      C
      GO TO 32
31 HEDR(I)=DIST+.5*TOWDIA
415 32 EQLEN=HEDR(I)+20.*DIAH(I)/12.
      CALL HYDLOS(DIAH(I),VELO(I),VIS1,RHO1,2,HEAD1)
      CALL HYDLOS(DIAH(I),VELO(I),VIS2,RHO2,2,HEAD2)
      DELSUP=DELSUP+HEAD1*RHO1-EQLEN/100.
      IF(I.GT.1) GO TO 33
420 DELRET=DELRET+HEAD2*RHO2*(EQLEN-50.)/100.
      GO TO 34
33 DELRET=DELRET+HEAD2*RHO2*EQLEN/100.
425 34 PIPCOST(I)=UPIPCST(I)*HEDR(I)
      IF(I.LT.JEX) EGPCST=EGPCST+PIPCOST(I)+REDCOST(I)+TEECOST(I)
      IF(I.EQ.JEX) EGPCST=EGPCST+PIPCOST(I)+REDCOST(I)+ELCOST
430 35 CONTINUE
      EDLSR=DELSUP+DELRET
      EPDIA=.7*DIAH(I)
      EGPCST=EGPCST+2.-50.*UPIPCST(I)+(EEJCST+EFLGCST)*2
      C
      C      DESIGN AND COST THE MAIN CIRCULATION PIPING FOR THE COMPLETE
      C      TOWER GROUPS. COMMENTS IN THE ABOVE SECTION ON EXTRA GROUP
      C      PIPING DESIGN APPLY HERE IDENTICALLY.
435      CALL HEADER(GPGPM,NTOWGPG,GPMCIRC,REDUCE,0,J,DIAH,REDCOST,TEECOST,
      SELCOST,UPIPCST,VELO,EJCOST,FLGCOST,DESVEL)
      JSAVE = J
      DELSUP=0.
440 DELRET=0.
      GPCST=0.
      IF(J.GT.NFL) COST = 1.E+40
      IF(J.GT.NFL) RETURN
      DO 40 I2=1,J
445 I = I3
      IF(I.EQ.1) GO TO 41
      IF(MOD(I,2).EQ.0) HEDR(I)=0.
      IF(MOD(I,2).NE.0) HEDR(I)=1.5*TOWDIA
      GO TO 42
450 41 HEDR(I)=DIST+.5*TOWDIA
42 EQLEN=HEDR(I)+20.*DIAH(I)/12.
      CALL HYDLOS(DIAH(I),VELO(I),VIS1,RHO1,2,HEAD1)
      CALL HYDLOS(DIAH(I),VELO(I),VIS2,RHO2,2,HEAD2)
      DELSUP=DELSUP+HEAD1*RHO1-EQLEN/100.
455 IF(I.GT.1) GO TO 43
      DELRET=DELRET+HEAD2*RHO2*(EQLEN-50.)/100.

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GO TO 44

43 DELRET=DELRET+HEAD2*RHO2*EQLN/100.

44 PIP COST(I)=UPIPCST(I)*HEAD(I)

IF(I.LT.J)GPCST=GPCST+PIPCOST(I)+REDCOST(I)+TEECOST(I)

IF(I.EQ.J)GPCST=GPCST+PIPCOST(I)+REDCOST(I)+ELCOST

DETERMINE THE HEAD LOSS AND PRESSURE DROP IN THE BUNDLE
 FITTINGS CONNECTING THE QUADRANT HEADER TO THE TUBE BUNDLE
 HEADER.

40 CONTINUE

DELSURF=DELSUP+DELRET

GPCST=GPCST+2.-50.*UPIPCST(1)+(EJCOST+FLGCOST)*2

EQLFIT=350.

DETERMINE THE HEAD LOSS AND PRESSURE DROP IN THE PIPING FOR
 THE PUMP STATION SERVING THE COMPLETE TOWER GROUP.

VELOCIT=(BUNGPM/8.**2)*CONST2

CALL HYDLOS(R.,VELOCIT,VIS,RHO,2,HEAD)

DELFIT=HEAD*RHO*EQLFIT/100.

EQLPUMP=200.

PDIA=.7*DIAH(1)

SUM THE PRESSURE DROPS AND DYNAMIC HEAD TO GET THE PUMP STA-
 TION COSTS. THE EQUATIONS FOR PUMP COSTS AND PUMP FITTINGS
 COSTS WERE EXTRAPOLATIONS OF AVAILABLE COST DATA.
 TWO PUMPS SERVE EACH TOWER GROUP. NO AUXILIARY PUMP
 CAPACITY IS PROVIDED.

VELOCIT=(GGGPM/PDIA**2)*CONST2

CALL HYDLOS(PDIA,VELOCIT,VIS2,RHO2,2,HEAD)

DELPUMP=HEAD*RHO2*EQLPUMP/100.

PDP=DELSURE+2*DELSR+DELFIT+DELPUMP+DELTD

DYNHEAD=(PDP+DELHX+DELCON)/RHO

PUMPCST=(.0129*DYNHEAD+1.065)*GGGPM/1000.

TOTAL COST OF PIPE, FITTINGS, AND PUMPS PER COMPLETE TOWER
 GROUP.

PUFITS=(2.5*GGGPM/1000.)*7./DESVEL

DESIGN AND COST THE PUMP STATION SERVING THE EXTRA TOWER
 GROUP. THE METHOD IS IDENTICAL TO THAT FOR THE COMPLETE
 TOWER GROUP.

PSTACST=PUMPCST+PUFITS

CPTOW=QHDCST+4.*TDCST

CPGP=CPTOW*NTOWPGP+GPCST+PSTACST

EDELPM=0.

EPDP=0.

EDYNHD=0.

EPMPCST=0.

EPUFITS=0.


```

515      EPSGST=0.
      EXGST=0.
      IF (NEXTOW.EQ.0) GO TO 50
      VELOCIT=(EXGPM/EPDIA**2)*CONST2
      CALL HYDLOS(EPDIA,VELOCIT,VIS2,RHO2,2,HEAD)
      EDELPM=HEAD*RHO2*EQLPUMP/100.
520      EPDP=EDELSP+QDELSP+DELFIT+EDELPM+DELTD
      EDYNHD=(EPDP+DELHX+DELCON)/RHO
      EPMPCST=(0.0129*EDYNHD+1.065)*EXGPM/1000.
      EPUFITS=(2.5*EXGPM/1000.)*7./DESVEL

C
525      C      DETERMINE TOTAL COSTS.
C
      EPSGST=EPMPCST+EPUFITS
      EXGST=CTOW*NEXTOW+EPSGST+EPSGST
50      CONTINUE
      COST=CGGP*NTOWGPS      +EXGST
      COST = COST * POHCIR
      TTDCST=TDGST*CTOW
      TGPCST=GPCST*NTOWGPS+EGPCST
      TPCST=PTACST*NTOWGPS+EPSGST
535      FPG = GPGPM * (60.0*RHO/7.481) * NTOWGPS
      EXFLO =EXGPM * (60.*RHO/7.481)
      HPWAT = (FPG*(PDP + DELHX + DELCON) +
$           EXFLO*(EPDP+ DELHX + DELCON)) / (62.*3600.*550.)

C
540      C      COMPUTE PUMP MOTOR ELECTRIC COSTS.
C
      NPX = 1
      IF (NEXTOW.GT. 0) NPX = 2
      NPMP = 2 * NTOWGPS + NPX
545      HPPMP = HPWAT/(NPMP*EFFP)
      IF (HPPMP.LT. 251.) TRMA = 112500./NPMP + 7.88 * HPPMP
$           + (116.-.159*HPPMP)*HPPMP
      IF (HPPMP.GE. 251. .AND. HPPMP.LE. 4000.) TRMA = 112500./NPMP
$           + 7.88*HPPMP + 870./SQRT(HPPMP)*HPPMP
550      IF (HPPMP.GT. 2000.) TRMA = 112500./NPMP + 7.88 * HPPMP
      VS = 7200.
      IF (HPPMP.LT. 2000.) VS = 13300.
      VM = 6000.
      IF (HPPMP.LT. 2000.) VM = 2300.
555      IF (HPPMP.LT. 251) VM = 480.
      TRMB = (DIST/2. - 1000.)*(37. + .47*HPPMP*NPMP/SQRT(VS)
$           + .5*(NPMP) / NPMP
      TRMC = (100. + 1.1 * HPPMP) + (DGSTM-250.) / SQRT(VM)
      PMELEC = (TRMA + TRMB + TRMC) * POHLEC
560      COST = COST + PMELEC/1000. * NPMP
      PISCOS = COST
      RPTPL = PMELEC/1000. * NPMP
      RETURN
      END

```

SUBROUTINE ROOT(TFIX,RFIX,TTD,TD,CWARL)

GIVEN THE EFFECTIVENESS THIS ROUTINE CALCULATES THE
CAPACITY RATIO LIMIT FOR THE HEAT EXCHANGER USING A
SINGLE PASS CROSSFLOW CORRELATION

DEFINITION OF VARIABLES

CWARA - THERMAL CAPACITY RATIO OF WATER TO AIR FLOWING
THROUGH THE HEAT EXCHANGER (DIMENSIONLESS)
EFF - EFFECTIVENESS OF HEAT EXCHANGER (DIMENSIONLESS)
RFIX - TEMPERATURE RANGE OF WATER FLOWING THROUGH THE
HEAT EXCHANGER (DEG F)
TD - HEAT EXCHANGER AMBIENT AIR DESIGN TEMPERATURE
(DEG F)
TFIX - EXIT TEMPERATURE OF THE TURBINE AT WHICH THE
SYSTEM IS TO BE DESIGNED FOR (DEG F)
TTD - TERMINAL TEMPERATURE DIFFERENCE OF THE SURFACE
CONDENSER (DEG F)

$EFF = RFIX / (TFIX - TTD - TD)$
 $CWARA = (1.00 - EFF) / EFF$

NEWTON-RAPHSON ROOT FINDING ROUTINE

10 $FUNC = CWARA * EFF - (1.0 - EXP(-CWARA))$
 $DFDC = EFF - EXP(-CWARA)$
 $CWARA = CWARA - FUNC / DFDC$
IF (ABS(FUNC) .GT. 0.01) GO TO 10
CWARL = CWARA
RETURN
END

SUBROUTINE RPRT1(DESVEL, PF)

THIS ROUTINE PRINTS PIPING COST REPORT

C
C
C

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5      COMMON /KPRT1/
      $ ,DYNH01 ,DIAD1 ,DIAT1 ,DIAM1(200) ,DIAQ1(200)
      $ ,EPC01 ,EGPCS1 ,EPGPC1 ,EPUF11 ,EDYNH1 ,EXGPM1 ,EUCOS1 ,ELCOS1
10     $ ,F_LGC01
      $ ,GPMC01 ,GPGPM1 ,GPCST1
      $ ,HEDR1(200)
      $ ,LSAV1
      $ ,LXAV1
15     $ ,NTUR01 ,NBUNP1 ,NTOWG1 ,NTOWP1 ,NEXT01
      $ ,PSTAC1 ,PUFIT1 ,PUMPC1 ,PIPCOS1(200) ,PISCO1
      $ ,QHDCS1 ,QUADG1 ,QIPIC1(200) ,QHEDR1(200) ,QTECS1(200)
      $ ,QPDOS1(200) ,QELCS1
      $ ,REDC01(200) ,RPTPL1
20     $ ,TEEC01(200) ,TPCS1 ,TDCS1 ,TTDCS1 ,TGPCS1 ,TOWD01 ,TQDCS1
      $ ,XTOW1
      COMMON /PRESS/ IPRESS
180    FORMAT(T31,16(" ")//T36,"PIPING",T55,I3," PSI DESIGN PRESSURE"
      $ //T31,16(" "))
200    FORMAT(/25X,"CIRCULATION PIPING TO EACH TOWER GROUP"/52X,"COST I
25     $N 10**3 DOLLARS FOR"/40X,50(" ")//12X,"HEADER DIAMETER" LENGTH
      $ PIPE TEES REDUCERS EXPANSION FLANGES"/12X,"SECTION (I
      $NCHES) (FEET)",33X,"JOINT(1) (3)"/)
203    FORMAT(1H,14X,I2,1X,F10.0)
204    FORMAT(/10X,"CIRCULAR TOWERS",I6,14X,"TOWER GROUPS",I4X,I6,/10X,
30     $ "TOWERS PER GROUP",I5,14X,"TOWERS IN INCOMPLETE GROUP",I6)
1204   FORMAT(/10X,
      $ "COST OF CIRCULATION PIPING FOR EACH TOWER GROUP $",F5.0," *10**
      $3"/10X,"COST OF CIRCULATION PIPING FOR INCOMPLETE GROUP" $",F5.0,
      $ " *10**3"/47X,"TOTAL COST OF CIRCULATION PIPING $",F5.0," *10**
35     $3"/)
205    FORMAT(/25X,"QUADRANT PIPING"/42X,"COST IN 10**3 DOLLARS FOR"/40X
      $ ,"/12X,"HEADER DIAMETER LENGTH"
      $ PIPE TEES REDUCERS"/12X,"SECTION (INCHES) (FEET)"/)
40     208    FORMAT(/10X,"TUBES PER BUNDLE",I10,/10X,"BUNDLES PER QUADRANT",I6
      $ ,/10X,"COST OF HEADERS PER QUADRANT $",F5.0," *10**3"/49X,"TOTA
      $ L COST OF QUADRANT HEADERS $",F5.0," *10**3"/)
209    FORMAT(/25X,"TOWER PIPING"/10X,"TOWER DIAMETER",23X,F5.0," FEET"/
45     $ 10X,
      $ "DIAMETER OF PIPE FROM CIRCULATION
      $ "/10X,"HEADER TO TOWER DISTRIBUTION HEADER",F7.0," INCHES"/10X,"DI
      $ AMETER OF TOWER DISTRIBUTION PIPE",F7.0," INCHES"/10X,"COST OF DI
      $ STRICTION PIPING PER TOWER $",F5.0," *10**3"/40X,"TOTAL COST O
      $ F TOWER DISTRIBUTION PIPING $",F5.0," *10**3"/)
50     211    FORMAT(/25X,"PUMP STATION"/10X,"DESIGN VELOCITY",15X,F3.0," FPS"/
      $ 10X,"FLOW PER QUADRANT",9X,F5.0," GPM"/10X,"FLOW PER BUNDLE",10X,F5.0," GPM"/
      $ F5.0," GPM"/10X,"FLOW PER TOWER GROUP "F5.0," GPM"/10X,
      $ "FLOW TO INCOMPLETE GROUP ",F5.0," GPM"/)
55     212    FORMAT(10X,"FOR EACH TOWER GROUP",20X,"FOR INCOMPLETE TOWER GROUP"
      $ /12X,"DYNAMIC HEAD",9X,F5.0," FEET",9X,"DYNAMIC HEAD",9X,F5.0,
      $ " FEET"/12X,"PUMP COST",11X,$",F5.0," *10**3",7X,"PUMP COST",11X,
      $ "$",F5.0," *10**3"/12X,"PUMP FITTINGS COST $",F5.0," *10**3",7X,
      $ "PUMP FITTINGS COST $",F5.0," *10**3"/12X,"PUMP STATION COST $"

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      S,F5.0," *10**3",7X,"PUMP STATION COST" S",F5.0," *10**3")
2120 FORMAT(//T58,"PUMP ELECTRICAL COSTS S",F6.0," *10**3"//)
60 2125 FORMAT(T58,"COST OF PUMP STATIONS S",F5.0," *10**3"////),
      S
      S,T54,"TOTAL PIPING SYSTEM COSTS S",F6.0," *10**3"//)
213 FORMAT(1H1)
214 FORMAT(1H .13X,I2.1X,7F10.1)
      WRITE(6,213)
65      WRITE(6,180) IPRESS
      WRITE(4,204) IFIX(XTOW1+1.E-30),NTOWG1,NTOWP1,NEXT01
      WRITE(4,200)
      DO 201 I = 1, JSAV1
      IF (I.GT.1) GO TO 202
70      WRITE(6,203) I,DIAH1(I), HEDR1(I), PIPCOS1(I)*PF, TEEC01(I)*PF,
      S REDC01(I)*PF, EJCOS1*PF, FLGC01*PF
      GO TO 201
202 IF (I.EQ. JSAV1) GOTO 210
      WRITE(6,203) I, DIAH1(I), HEDR1(I), PIPCOS1(I)*PF, TEEC01(I)*PF,
75      S REDC01(I)*PF
      GO TO 201
210 WRITE(6,203) I, DIAH1(I), HEDR1(I), PIPCOS1(I)*PF, ELCOS1*PF,
      S REDC01(I)*PF
201 CONTINUE
80      WRITE(4,1204) GPCST1*PF, EGPCST1*PF, TGPCST1*PF
      WRITE(6,209) TOWD11, DIAQ1, DIAT1, TDCS1*PF, TTDCS1*PF
      WRITE(4,205)
      DO 206 I = 1, LSAV1
      IF (I.EQ. LSAV1) GOTO 207
85      WRITE(6,214) I, DIAQ1(I), QHEDR1(I), QPIPC1(I)*PF, QTECS1(I)*PF,
      S QROCS1(I)*PF
      GO TO 206
207 WRITE(6,214) I, DIAQ1(I), QHEDR1(I), QPIPC1(I)*PF, QELCS1*PF,
      S QROCS1(I)*PF
90 206 CONTINUE
      WRITE(4,211) DESVEL, BUNGP1, QUADG1, GPMCI1, GPGPM1, EXGPM1
      WRITE(4,212) DYNH01, EDYNH1, PUMPC1*PF, EPMP1*PF, PUFIT1*PF,
      S EPJFI1*PF, PSTAC1*PF, EPSCS1*PF
      WRITE(4,2120) RPTPL1
95      WRITE(4,2125) TPCS1*PF, PISC01
      RETURN
      END

```

```

      SUBROUTINE RPRT2 (EFFC, TUBEM, TUBEM2)
C
C      THIS ROUTINE REPORTS CONDENSER DESIGN AND COSTS
C
5      COMMON /KPRT2/ UCON, TI, TEI, TOLM, XNP
      S, VELD, DELPWC, ARPS, TLA, XNTS, XNS, TS
      COMMON /KPRT3/ TUBCST, SHLCST, FETCST, CHX
6100  FORMAT(
10      C T40,20 ("=")/T41,"C O N D E N S E R"/T40,20 ("="))
6105  FORMAT(
      L T03,"--- DESIGN CONDITIONS ---"
      R T72,"--- DESIGN OPERATING CONDITIONS ---"/)
6110  FORMAT(
15      L T15,"STEAM TEMPERATURE",F6.1," F"
      R T60,"OVERALL HEAT TRANSFER COEFFICIENT ",F9.2," BTU/HR SQ FT DEG
      RE")
6115  FORMAT(
      L T10,"INLET WATER TEMPERATURE",F6.1," F"
      R T60,"AVERAGE WATER VELOCITY THRU COND ",F8.1," FT/SEC")
20      6120  FORMAT(
      L T11,"EXIT WATER TEMPERATURE",F6.1," F"
      R T65,"PRESSURE DROP THRU CONDENSER ",F8.1," LB/SQ FT")
6125  FORMAT(
25      L T02,"LOG MEAN TEMPERATURE DIFFERENCE",F6.1," F"
      R T70,"CONDENSER EFFECTIVENESS ",F9.3)
6130  FORMAT(
      L T05,"--- CONDENSER DESCRIPTION ---"
      R T79,"--- CONDENSER COSTS ---"/)
30      6135  FORMAT(
      L T17,"NUMBER OF SHELLS",I6,
      R T75,"TUBING MATERIAL S",F14.2*2X("2A10")")
6140  FORMAT(
      L T05,"HEAT TRANSFER AREA PER SHELL",G11.5," SQ FT"
      R T80,"SHELLS S",F14.2)
35      6145  FORMAT(
      L T07,"NUMBER OF PASSES PER SHELL",I6,
      R T77,"FIELD ERECTION S",F14.2)
6150  FORMAT(
40      L T22,"TUBE LENGTH",I6,T45,"FEET")
6155  FORMAT(
      L T08,"NUMBER OF TUBES PER SHELL",I6
      R T68,"TOTAL COST OF CONDENSER S",F14.0)
C
45      WRITE(6,6100)
      WRITE(6,6105)
      WRITE(6,6110) TS,UCON
      WRITE(6,6115) TI,VELD
      WRITE(6,6120) TE,DELPWC
      WRITE(6,6125) TOLM,EFFC
50      WRITE(6,6130)
      WRITE(6,6135) (IFIX(XNS)),TUBCST,TUBEM,TUBEM2
      WRITE(6,6140) ARPS,SHLCST
      WRITE(6,6145) (IFIX(XNP)),FETCST
      WRITE(6,6150) (IFIX(TLA))
55      WRITE(6,6155) (IFIX(XNTS)),(TUBCST+SHLCST+FETCST)
      RETURN
      END

```

SUBROUTINE RPTFAN

THIS ROUTINE REPORTS FAN DESCRIPTION AND COSTS

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COMMON /FAN/ FANDAP(153,10), FANDAH(153,10), FMCPEL, FBCPEL,
$VELREC, AFC, ELEV, EHR
LOGICAL FIRST, FXTMP
COMMON
$ AFTR, ALPHA
$ CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAFI
$ CBU, CSEALP, CELAST, CFS, COANG, CLUVR, CHAILE, CVM
$ DEEP, DESVEL, DANGLE
$ EFFO
$ FCR, FIRST, FIXL, FCOS, FXTMP
$ GBEFF
$ HXNP, HPCST
$ IHEAT
$ ITMAX, ITMIN
$ J-ONS
$ KCONV, KALEXT
$ MXEXT
$ NTUCAL(2), NTA
COMMON
$ ODR
$ PSIZE, PER, PWCOS, PLANC, PFACT
$ POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCU
$ QREJ, QREDUCE
$ RSP, REDUCE, ROESL, ROELA, ROOFL, RFIX
$ SAAF, SIGMA, SPAMAT(2)
$ TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
$ TJBANG, TW
$ UCS, UWS
$ VAS(5)
$ WFW
$ XDEPA, XW, XD

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COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
$ CLAN1, REAIL, Z1, HRFA2S, W41, U1, PPOW1,
$ FPOW1, DEFC1, WIDT1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,
$ REW1, W1, ZPLNC2, ZSIZ12, ZSPBP, SW41, SW31,
$ SPC1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
$ BP2MIN, NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONBA1, XNTS1, VELD1
$ TL1, UCON1, FMC1, FRAC1, EFFC1, CH1, CA1, CS1
$ CLT1, CFC1, CPCC1, FITC1, CSC1, CEPRE1, DEPI1, AST1
$ CAPCS1, XNFAN1, SLDAN1, CPLEN1, OPFEL1, WH1, WITUL, AD11, ABL1
$ WTH1, WTR1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
$ AIDF1, WATFF1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACTTP1, ADJTP1
$ ACTBP1, ADJBP1, ACTVH1, ADJVH1, ADJPP1, THPA11, TCTF1, AFCST1
$ CS1, WATER1, WSTRC1, CFOUN1, HUBO1, TOWLE1, CSE1, CHF1
$ CBA1, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
REAL MOTOR(4,3), DRIVE(3,2), PITCH(3,2), RECOVY(5,2)

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DATA ((MOTOR(I,K), I=1,4), K=1,3)/
* "TOTALLY FN", "CLOSED SQU", "IRREL CAGE", "MOTOR", "",
* "EXPLOSION", "PROOF SQUI", "IRREL CAGE", "MOTOR", "",
* "TWO SPEED", "SQUIRREL C", "AGE", "",
DATA ((DRIVE(I,K), I=1,3), K=1,2)/

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      * "SPIRAL BEV", "HEL GEAR DR", "IVE      ",
      * "V-RELT DRI", "VE      ", "      "/
60      DATA ((PITCH(I,K), I=1,3), K=1,2) /
      * "MANUAL PIT", "CH BLADES ", "      ",
      * "AUTO-VARIA", "BLE PITCH ", "BLADES  "/
      DATA ((RECOVY(I,K), I=1,5), K=1,2) /
85      * "FANS NOT E", "QUIPPED WI", "TH VELOCIT", "Y RECOVERY",
      * "DIFFUSERS",
      * "FANS EQUIP", "PED WITH V", "ELOCIITY RE", "COVERY OIF",
      * "FUSERS      "/

C
1000 FORMAT(1H )
1005 FORMAT(14I)
1010 FORMAT(T52, "F A N S")
1020 FORMAT(T51, "-----")
1030 FORMAT(T16, "---- DRIVE SYSTEM ----", T92, "---- FAN GEOMETRY ----")
1040 FORMAT(T84, "BLADE DIAMETER ", F6.2, " FEET")
1050 FORMAT(T87, "BLADE ANGLE ", F6.2, " DEGREES")
1060 FORMAT(T73, "NUMBER OF BLADES/FAN ", F6.2)
1070 FORMAT(T84, "NUMBER OF FANS ", F6.0)
1080 FORMAT(T17, "---- FAN COSTS ----", T78, "---- DESIGN CONDITIONS ----")

C
80 1085 FORMAT (T100, "(ACTUAL)", T122, "(ADJUSTED)")
1090 FORMAT(T73, "VOLUMETRIC FLOW RATE/FAN ", F12.0, " CU FT/MIN")
1100 FORMAT(T16, "BLADE AND HUB COST/FAN $", F10.0, T71,
      * "TOTAL VOLUMETRIC FLOW RATE", F12.0, " CU FT/MIN")
1120 FORMAT(T24, "MOTOR COST/FAN $", F10.0, T70,
      * "TOTAL AIR PRESSURE DROP OF H.X. ", F8.5, " PSI", T120, F8.5)
1130 FORMAT(T10, "SPEED REDUCER DRIVE COST/FAN $", F10.0, T69,
      * "PRESSURE DROP ACROSS H.X. BUNDLE ", F8.5, " PSI", T120, F8.5)
1140 FORMAT(T24, "STACK COST/FAN $", F10.0, T72,
      * "NON-RECOVERABLE VELOCITY HEAD ", F8.5, " PSI", T120, F8.5)
90 1145 FORMAT(T19, "ELECTRICAL COST/FAN $", F10.0
      * "S T83, "HORSEPOWER/FAN", F13.0, " HP", T116, F12.0)
1150 FORMAT(T79,
      * "FAN POWER REQUIREMENTS ", F8.0, " HP")
1190 FORMAT(T2, "*** ANNUAL OPERATIONAL COSTS $", F10.0)
95 1200 FORMAT(T37, 5A10)
1210 FORMAT(
      * "HUB DIAMETER ", F6.2, " FEET")
      WRITE(6,1005)
      WRITE(6,1000)
100  WRITE(6,1000)
      WRITE(6,1020)
      WRITE(6,1010)
      WRITE(6,1020)
      WRITE(6,1000)
105  IF (VELDEC.EQ.0) WRITE(6,1200) (RECOVY(I,1), I=1,5)
      IF (VELDEC.EQ.1) WRITE(6,1200) (RECOVY(I,2), I=1,5)
      WRITE(6,1000)
      WRITE(6,1030)
      WRITE(6,1000)
110  WRITE(6,1210) HUBDI1
      WRITE(6,1040) ADI1
      WRITE(6,1050) BLDANI
      WRITE(6,1060) ABL1
      WRITE(6,1070) XNFAN1

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```
115      WRITE(6,1000)
        WRITE(6,1000)
        WRITE(6,1000)
        WRITE(6,1000)
        WRITE(6,1000)
        WRITE(6,1000)
120      WRITE(6,1090) CFMPF1
        WRITE(6,1100) FDCPF1, TOTCF1
        WRITE(6,1120) FMTRC1, ACTTP1, ADUTP1
        WRITE(6,1130) CSRI,ACTBP1, ADJBP1
        WRITE(6,1140) CYLRN1, ACTVH1, ADUVH1
125      WRITE(6,1145) CFANE1, HPPF1, ADUPP1
        WRITE(6,1150) THPA11
        WRITE(6,1190) AFCST1
        RETURN
      END
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      SUBROUTINE RPTHXC(AFON)
      C
      C THIS ROUTINE REPORTS HEAT EXCHANGER DESIGN, OPERATING CONDITIONS
      C AND COST
      C
      LOGICAL FIRST, FXTMP
      COMMON
      $ AFON, ALPHA
      $ ,CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAP
      $ ,CRU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILE, CVM
      $ ,DEEP, DESVEL, DANGLE
      $ ,EFFP
      $ ,FCH, FIRST, FIXL, FCOS, FXTMP
      $ ,GREFF
      $ ,HXNP, HPCST
      $ ,IHEAT
      $ ,ITMAX, ITMIN
      $ ,JCONC
      $ ,KCONV, KALEXT
      $ ,MXEXT
      $ ,NTUCAL(2), NTA
      COMMON
      $ ODR
      $ ,PSIZE, PER, PWCOS, PLANC, PFACT
      $ ,POHRAF, POHFAN, POHLEC, POHCIR, POHCND, POMSTC, POHSLC
      $ ,QREJ, QREDUCE
      $ ,RAP, REDUCE, ROESEL, ROEELA, ROOFL, RFIX
      $ ,SAAF, SIGMA, SPAMAT(2)
      $ ,TD, TPO(4), TEFF, TLIM, TLPA, TSEALP, TELAST, THFIN, TFIX
      $ ,TUBANG, TW
      $ ,UCS, UWS
      $ ,VAS(5)
      $ ,WTV
      $ ,XDEPA, XW, XD
      COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
      $ ,CLAN1, REA11, Z1, HRFA25, W41, U1, PPOW1,
      $ ,FPOW1, DEFC1, WIDT1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,
      $ ,REWA1, NW1, ZPLNC2, ZSIZ12, ZSPBP, SW41, SW31,
      $ ,SPC1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCO1, SPS13, WT2MIN,
      $ ,B2MIN, NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONBA1, XNTS1, VELO1
      $ ,TLA1, UCON1, FMCS1, FBAC1, EFFC1, CH1, CA1, CSI
      $ ,CLTCL, CFCL, CPCC1, FITCL, CSC1, CEPRE1, DEPIP1, AST1
      $ ,CAPCS1, XNEAN1, RLDAN1, CPLEN1, DPFE1, WH1, WTTU1, ADI1, ABL1
      $ ,ATHCL, WTRF1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, AVTU1
      $ ,AIRFE1, WATFE1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACITP1, ADJTP1
      $ ,ACTBP1, ADJBP1, ACTVH1, ADJVH1, ADJPP1, THPA11, TCTF1, AFCST1
      $ ,CS1, WATER1, WSTRC1, CFOUN1, HUAD11, TOWLE1, CSE1, CHF1
      $ ,CBAL, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTH51, CYLRN1, CFANE1
      C
      COMMON /TINE/ XNS, TTD, TLA, XNTS, ARPS
      COMMON /HXD/ AI, ATOT
      COMMON /ESCAL/ BSEC
      6390 FORMAT(
      R T71, "T OF WATER ", F14.0, " LB")
      6400 FORMAT(
      R T71, "T OF TUBES", F14.0, " LB")
      6410 FORMAT(

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      L T8,"ALPHA", G14.8
      R,T71,"WT OF FRAME ",F14.0," LB")
60      6420 FORMAT(
      L T8,"SIGMA", G14.8
      R,T71,"WT OF HEADER",F14.0," LB")
      6422 FORMAT(
      R T71,"WT OF STRUCT",F14.0," LB")
65      6424 FORMAT(
      L T71," ROOF LOAD",F14.0," LB"
      R,T106,"(",F8.2," LB/SQ FT)")
      6430 FORMAT(
      L T3,"FITCO/ATOT", G14.8
70      5)
      6440 FORMAT (1H0,2A10,T15,"NTU EFFECTIVENESS CORRELATION USED")
      6500 FORMAT(1H0)
      6505 FORMAT(T35*30("-"))
      6510 FORMAT(T36,"H E A T   E X C H A N G E R")
75      6512 FORMAT(1H+,T90,F5.1," FANS",T110,F4.1," PASS")
      6515 FORMAT(
      L T2," WATER FLOW RATE",I11," LBM/HR"
      R,T71," COOLING SURFACE $",F10.0)
      6520 FORMAT(
      L T2," AIR FLOW RATE",I11," LBM/HR"
80      R,T71," HEADER AND NOZZEL $",F10.0)
      6525 FORMAT(
      L T2," TUBES IN DEPTH",F11.2," TUBES  (",F7.1," FT DEEP)"
      R,T70," BUNDLE ASSEMBLY $",F10.0)
85      6526 FORMAT(
      R T70," BUNDLE FRAME $",F10.0)
      6527 FORMAT(
      R T70," SEALING ELASTOMER $",F10.0)
      6530 FORMAT(
90      L T2,"TUBES ACROSS FRONT",I11," TUBES  (",F7.1," FT WIDE)"
      R,T71," PLENUM $",F10.0)
      6532 FORMAT(1X
      R, T71," LOUVERS $",F10.0)
      6533 FORMAT(1X
95      R, T71," HAIL SCREENS $",F10.0)
      6535 FORMAT(
      L T2," LENGTH",F11.0," FEET"
      R,T71," STRUCTURE $",F10.0)
      6537 FORMAT(
      R T71," FOUNDATION $",F10.0)
100      6540 FORMAT(
      L T2," FRONTAL AREA",I11," SQ FEET"
      R ,T71," HEAT XCHR SHIP AND ERECT $",F10.0)
      6541 FORMAT(T8,"SURFACE AREA",I11," SQ FT")
105      6555 FORMAT(T70,11(" "),2X,11(" "))
      6560 FORMAT(T73,"AIR",T87,"WATER")
      6565 FORMAT(T70,25(" "))
      6570 FORMAT(T50,"REYNOLDS NUMBER"
      $ ,2(1PE13.5,E14.5,3X))
110      6575 FORMAT(T48,"VELOCITY (FT/SEC)"
      $ ,2(1PE13.5,E14.5,3X))
      6580 FORMAT(T34,"PRESSURE DROP (LBS FORCE/SQ IN)"
      $ ,2(1PE13.5,E14.5,3X))
      6581 FORMAT(T44,"INLET TEMPERATUREI (F)",1PE13.5,E14.5)

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115      6582 FORMAT(T45,"EXIT TEMPERATURE (F)",1PE13.5,E14.5)
      6583 FORMAT(T56,"RANGE (F)",1PE13.5,E14.5)
      6584 FORMAT(T60,"CWARA",7X,1PE13.5)
      6585 FORMAT(T29,"HEAT TRFR COEFF (BTU/HR SQ FT DEG F)"
      5 ,2(1PE13.5,E14.5,3X))
120      6586 FORMAT(T62,"NTU",7X,1PE13.5)
      6587 FORMAT(T50,"FRICTION FACTOR"
      5 ,2(1PE13.5,E14.5,3X))
      6595 FORMAT(T35,"OVERALL U (BTU/HR SQ FT DEG F)"
      5 ,7X,1PE13.5,E14.5)
125      6600 FORMAT(T52,"EFFECTIVENESS"
      5 ,T76,F7.4)
      6610 FORMAT(T51,"FIN EFFICIENCY"
      5 ,T76,F7.4)

130      C
      WRITE(6,6500)
      WRITE(6,6505)
      WRITE(6,6510)
      WRITE(6,6512) XNFAN1, HXNP
      WRITE(6,6505)
135      WRITE(6,6500)
      WRITE(6,6565)
      WRITE(6,6560)
      WRITE(6,6555)
      WRITE(6,6570) REA11, REMA1
140      WRITE(6,6575) VAIR1, VWAT1
      WRITE(6,6580) DEPA1/144., DPWT1/144.
      WRITE(6,6585) H01, H11
      WRITE(6,6587) AIRFF1, WATFF1
      WRITE(6,6581) TD, VAR(1)-TTD
145      WRITE(6,6582) T41, VAR(1)-VAR(2)-TTD
      WRITE(6,6583) T41-TD, VAR(2)
      WRITE(6,6584) VAR(3)
      WRITE(6,6586) ANTU1
      WRITE(6,6585) U1
150      WRITE(6,6600) EFF1
      WRITE(6,6610) EFFIN1
      WRITE(6,6500)
      WRITE(6,6390) WATER1
      WRITE(6,6400) WTTU1
155      WRITE(6,6410) ALPHA, WTRF1
      WRITE(6,6420) SIGMA, WTHD1
      WRITE(6,6422) WSTRC1
      WRITE(6,6424) AFRON=ROOFL, ROOFL1
      WRITE(6,6430) FITCOL/ATOT
160      WRITE(6,6440) NTUCAL
      WRITE(6,6500)

      C
      WRITE(6,6515) IFIX(SW31), CS1
165      WRITE(6,6520) IFIX(SW41), CH1
      WRITE(6,6525) Z1, Z1=XD/12., CS41
      WRITE(6,6526) CHF1
      WRITE(6,6527) CSE1
      WRITE(6,6530) HW1, WIDT1, CPLEN1
      WRITE(6,6532) CSTLV1
170      WRITE(6,6533) CSTHS1
      WRITE(6,6535) ELENI, STRUC1

```

SUBROUTINE RPTHXC

74/74 OPT=1

FTN 4.2+74351

12/20/76

175

```
WRITE(6,6537) CFOUND1
WRITE(6,6540) IFIX(AFRON), (BSECF-1.)*(CA1 + CH1 + CSI)
WRITE(6,6541) IFIX(AAIR1)
RETURN
END
```

SUBROUTINE RPTHXD

C
C
C

THIS ROUTINE REPORTS HEAT EXCHANGER DESCRIPTION AND UNIT COST DATA

```

5 LOGICAL FIRST, FXTMP
COMMON
$ ,AFTR, ALPHA
$ ,CAFF, CSSPKW, CONF, CONL, COSIL, CAPCHG, CONMAT, CONMA2, CAPI
10 $ ,CRU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILE, CVM
$ ,DEEPL, DESVEL, DANGLE
$ ,EFFP
$ ,FCR, FIRST, FIXL, FCOS, FXTMP
$ ,GBEFF
15 $ ,HXNP, HPCST
$ ,IHEAT
$ ,ITMAX, ITMIN
$ ,JCONC
$ ,KCONV, KALEXT
$ ,MXEXT
20 $ ,NTUCAL(2), NTA
COMMON
$ ,ODR
$ ,PSIZE, PER, PWCOS, PLANC, PFACT
25 $ ,POHRAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSLC
$ ,QREJ, QREDUCE
$ ,RBS, REDUCE, ROESEL, ROELA, ROOFL, RFIX
$ ,SAAF, SIGMA, SPAMAT(2)
$ ,TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
30 $ ,TJBRAG, TW
$ ,UCS, UWS
$ ,VAR(5)
$ ,W=V
$ ,XDEPA, XW, XD
35 COMMON /HEADEX/ CHH, CN, CHM, CMW, CRJ, CWJ, CST
$ , CMO, CSR, CSM, PITCHF, CPM, PRESS, HEDMAT, HEDTYP, NPASS
$ , WB
COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
$ , CLAM1, REA11, Z1, HRFAC2, W41, U1, PPOW1,
40 $ , FPOW1, DEFC1, WIDTH1, ELENG1, VAIR1, VWAT1, HI1, HO1, T41
$ , REW1, NW1, ZPLNC2, ZSIZ12, ZSPBP, SW41, SW31,
$ , SP1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
$ , B2MIN, V2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONSA1, XNTS1, VELD1
$ , TL11, HCON1, FMCS1, FBAC1, EFFC1, CH1, CA1, CS1
45 $ , CLTC1, CFC1, CPCC1, FITC1, CSC1, CEPRE1, DEPIP1, AST1
$ , CAPCS1, XNFAN1, BLDAN1, CPLEN1, DFE11, WH1, ATTU1, AD11, AB11
$ , WTH1, WTR1, STRUC1, CFMPF1, HSPF1, TOTCF1, EFFIN1, ANTU1
$ , AIRF1, WATF1, XNM01, TCTF1, FOCF1, FMTFC1, ACTT1, ADJTP1
$ , ACTB1, ADJBP1, ACTVH1, ADJVH1, ADJPP1, THPA1, TCTF1, AFCST1
50 $ , CS1, WATER1, WSTR1, CFJUN1, HUBD1, TOWLE1, CSE1, CHF1
$ , CB1, NMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
COMMON /TINE/ XNS, TTD, TLA, XNTS, ARPS
COMMON /SURFEX/ ODL, GAGLIN, VTUB, TURMAT, FINTYP, FINMAT, CFB
$ , APLATE, COATC, ZINCC, CASTC, SS, EPREPC, XTUBMA, XHEDTY, XFINTY
COMMON /DUB/ DI, XDG, SF
55 COMMON /SUPPLY/ VAL(5), CPI2, CCOS, W3, COSM, EFF
$ , CLAM, REAIR, Z, HRFAC2, W4, U, PPOW,
$ , FPOW, DEFC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4,

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```

S REWAT, NW, PLANC2, PSIZ12, SP9P, SW4, SW3,
S SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
60 S BP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNYSX, VELDX
S TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
S CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPIP, AST
S, CAPCST, XNFAN, BLDANG, CPLEN, DPFLN, WHX, WTTUB, ADIA, ABLN
65 S, WTHAR, WTRM, STRUC, CPERF, HPERF, TOTCF, EFFIN, ANTU
S, AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTP, ADJTP
S, ACTRPD, ADJRPD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
S, CSND, WATERW, WSTRCT, CFOUNJ, HUGDIA, TOWLEN, CSE, CHF
S, CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
6600 FORMAT(1H1)
70 6601 FORMAT(1H )
6602 FORMAT(1H+, T10, " N O W - D E L I T A   H E A T   E X C H A N G E I
S R   D E S C R I P T I O N", T5, F5.1, " DEGREEI ")
6603 FORMAT(
L T22, "SUPPORT SPACING ", F7.3, T47, "FEET"
75 R, T57, "SEAL PLATE THKNS", F11.3, " INCH")
6605 FORMAT(
L T8, "TUBE PITCH NORMAL TO AIR FLOW ", F7.3, T47, "INCH"
R, T55, "SEAL PLATE DENSITY", F11.3, " LB/CU IN.")
6610 FORMAT(
80 L T2, "TUBE PITCH IN DIRECTION OF AIR FLOW ", F7.3, T47, "INCH"
R, T58, "ELASTOMER THKNS", F11.3, " INCH")
6615 FORMAT(
L T18, "TUBE DIAGONAL PITCH ", F7.3, T47, "INCH"
R, T56, "ELASTOMER DENSITY", F11.3, " LB/CU IN.")
85 6620 FORMAT(
L T23, "LINER MATERIAL ", 2A10
R )
6625 FORMAT(
L T11, "LINER THERMAL CONDUCTIVITY", F7.3
90 R )
6630 FORMAT(
L T8, "LINER TUBING OUTSIDE DIAMETER ", F7.4, T47, "INCH"
R, T62, "HEADER TYPE ", 2A10)
6635 FORMAT(1H+
95 L T38, "--- U N I T   C O S T S ---")
6640 FORMAT(
R T58, "HEADER MATERIAL (", 1A10, ") $", F8.3, "/LB")
6645 FORMAT(
R T59, "ROLLED JOINT, TUBE TO HEADER $", F9.3, "/TUBE")
100 6650 FORMAT(
R T59, "WELDED JOINT, TUBE TO HEADER $", F8.3, "/TUBE")
6655 FORMAT(
L T10, "SPACER CASTING $", G10.4, "/EA"
R, T55, "TUBE AND PLUG HOLE PREPARATION $", F8.3, "/HOLE")
105 6660 FORMAT(
L T9, "END PREPARATION $", G10.4, "/TUBE"
R, T65, "NOZZEL AND ATTACHING $", F8.3, "/HOLE")
6662 FORMAT(
L T14, "SEAL PLATE $", G10.4, "/LB"
110 R, T67, "BOLTED HEADER JOINT $", F8.3, "/FT")
6665 FORMAT(
L T14, "FRAME COST $", G10.4, "/LB"
R, T58, "HEADER MACHINING AND WELDING $", F8.3, "/FT")
6670 FORMAT(

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115      LT09,"LINER TUBING      S",G11.5,"/FT",  
        RT70,"STRUCTURAL STEEL S",F8.3,"/LB",  
        6695 FORMAT(  
        LT28,"TUBE SPACERS  S",G11.5,"/FT"  
        R)  
120      C  
        6617 FORMAT(  
        L T27,"LINER GAGE ",F5.1  
        R)  
        6710 FORMAT(  
125      LT9,"LINER TUBING INSIDE DIAMETER",F7.4,T47,"INCH"  
        R,T60,"HEADER LENGTH",F11.3," FEET")  
        WRITE(6,6600)  
        DO 20 I=1,3  
130      20 IF (DANGLE .LT. 1.E-30) WRITE(6,6602)  
        IF (DANGLE.GT.0.0) WRITE(6,6602) DANGLE  
        WRITE(6,6601)  
        WRITE(6,6603) SS, TSEALP  
        WRITE(6,6605) XW, ROESEL  
        WRITE(6,6610) XD, TELAST  
135      WRITE(6,6615) XDG, ROEELA  
        WRITE(6,6617) GAGLIN  
        WRITE(6,6620) TUBMAT,XTUBMA  
        WRITE(6,6625) CONL  
140      WRITE(6,6630) OOL,HEDTYP,XHEDTY  
        WRITE(6,6710) DI, WB  
        WRITE(6,6601)  
        WRITE(6,6601)  
      C  
        DO 30 I=1,3  
145      30 WRITE(6,6635)  
        WRITE(6,6601)  
        WRITE(6,6640) HEDMAT,CHM  
        WRITE(6,6645) CRJ  
        WRITE(6,6650) CWJ  
150      WRITE(6,6655) CASTC,CHH  
        WRITE(6,6660) EPREPC,CN  
        WRITE(6,6662) CSEALP,CBJ  
        WRITE(6,6665) CFS,CMW  
        WRITE(6,6670) CLTCL,CST  
155      WRITE(6,6695) CSC1  
      C  
        RETURN  
        END
```

SUBROUTINE SCALP (RANGE, CWARA, AFRON, WLRAT, TCWFCS, ITOWN)

SUBROUTINE SCALP SCALES THE PLANT AND DRY COOLING TOWER
DESIGNS AND COSTS LINEARLY UPWARD OR DOWNWARD TO ACCOUNT
FOR THE FOLLOWING FACTORS-

1. THE DESIGN TEMPERATURE OF THE POWER PLANT DOES
NOT CORRESPOND TO THE RATED BACK PRESSURE OF THE
STEAM TURBINE.
2. PART OF THE TOTAL POWER OUTPUT OF THE PLANT IS
USED IN SUPPLYING POWER TO THE FAN AND PUMPING
SYSTEMS.

THE FOLLOWING ARE POINTS ON THE HEAT RATE FACTOR CURVE WHICH
ARE USED IN DESCRIBING THE SCALING OF THE PLANT AND DRY COOL-
ING TOWERS. AT EACH OF THESE POINTS THE HEAT RATE FACTOR,
PLANT SIZE AND PLANT COSTS ARE DETERMINED.

POINT 0 - CONVENTIONAL TURBINE OPERATING AT RATED BACK
PRESSURE

POINT 1 - STEAM TURBINE OPERATING AT RATED BACK PRESSURE

POINT 2 - STEAM TURBINE OPERATING AT SYSTEM DESIGN EXIT
TEMPERATURE WITH OUTPUT OF TURBINE GENERATOR EQUAL
TO THE DESIGN POWER OUTPUT

POINT 3 - STEAM TURBINE OPERATING AT SYSTEM DESIGN EXIT
TEMPERATURE WITH THE POWER OUTPUT OF PLANT EQUAL
TO THE DESIGN POWER OUTPUT

THE DIFFERENCE BETWEEN POINT TWO AND THREE IS THE PLANT HAS
BEEN SCALED UP TO ACCOUNT FOR THE POWER CONSUMPTION OF THE
FANS AND PUMPS. BETWEEN POINT ONE AND TWO THE POWER PLANT
HAS BEEN SCALED UP OR DOWN TO ACCOUNT FOR AN INCREASE OR
DECREASE IN THE HEAT RATE FACTOR.

DEFINITION OF VARIABLES

AAIR - AIR SIDE HEAT TRANSFER AREA OF HEAT EXCHANGER
(SQ FT)

ADIA - FAN BLADE DIAMETER (FT)

AFRON - FRONTAL AREA OF THE HEAT EXCHANGER NORMAL TO AIR
FLOW (SQ FT)

ATUBC - HEAT EXCHANGER TUBE COST (\$)

BSECF - BUNDLE SHIPPING AND ERECTION COST FACTOR (DIMEN-
SIONLESS)

CA - BUNDLE ASSEMBLY COST (\$)

CAFF - PERCENT OF TIME PLANT IS GENERATING POWER DURING
THE YEAR (PERCENT)

CCOS - TOTAL COST OF THE DRY COOLING TOWER (\$)

CFANEL - COST OF THE ELECTRICAL WIRING FOR THE FAN SYSTEM
(\$)

CFOUND - COST OF THE FOUNDATION FOR THE DRY COOLING TOWERS
(\$)

CH - BUNDLE COSTS FOR THE HEAT EXCHANGER (\$)

CHAILS - COST OF HAIL SCREENS PER UNIT AREA (\$/SQ FT)

CLAND - COST OF LAND COVERED BY THE DRY COOLING TOWERS (\$)

CLUVR - COST OF LOUVERS PER UNIT AREA (\$/SQ FT)

CONBAS - COST OF THE SURFACE CONDENSER (\$)

COSM - INCREMENTAL MAINTENANCE COSTS OF DRY COOLING (\$)

CPIP - COST OF THE PIPING SYSTEM (\$)

CPLEN - COST OF THE PLENUM ON TOP OF THE COOLING TOWERS (\$)

	C	CPM	- COST OF PLENUM MATERIAL PER POUND (\$/LBM)
	C	CS	- COOLING SURFACE COST (\$)
60	C	CSE	- COST OF HEADER SEALANT FOR CONNECTING PLASTIC TUBES TO THE HEADER (\$)
	C	CSTHS	- COST OF THE HAIL SCREENS FOR THE ENTIRE FRONTAL AREA OF THE HEAT EXCHANGER (\$)
	C	CSTLVR	- COST OF THE LOUVERS FOR CONTROLLING THE AIR FLOW TO THE HEAT EXCHANGERS (\$)
65	C	CWARA	- RATIO OF HEAT CAPACITY OF THE WATER TO THE AIR (DIMENSIONLESS)
	C	CYLRS	- COST OF THE FAN RING AND THE VELOCITY RECOVERY STACK IF THEY ARE USED (\$/FAN)
70	C	DELFC	- INCREMENTAL FUEL COST FOR THE SCALED UP PLANT (MILLS/KW HR)
	C	ELENG	- LENGTH OF HEAT EXCHANGER TUBES (FT)
	C	FACCC	- COST OF FAN BLADES AFTER SCALING UP THE NUMBER OF FANS (\$)
75	C	FACPF	- COST OF FAN BLADES PER FAN (\$/FAN)
	C	FACZ	- FUEL COST FOR THE BASE PLANT WITH A ZERO COST ONCE THROUGH COOLING SYSTEM (MILLS/HW HR)
	C	FACB	- FUEL COST FOR THE SCALED UP PLANT (MILLS/KW HR)
	C	FACS	- COST OF FUEL FOR POWER PLANT (CENTS/BTU)
80	C	FACR	- FIXED CHARGE RATE FOR CAPITAL PER YEAR (PERCENT/YR)
	C	FIXL	- THE FIXED LENGTH OF HEAT EXCHANGER TUBES SPECIFIED BY THE INPUT TO THE CODE (FT)
	C	FACPF	- FAN MOTOR COST PER FAN (\$/FAN)
	C	FACST	- TOTAL FAN MOTOR COST FOR THE FAN SYSTEM AFTER SCALE UP (\$)
85	C	FROW	- POWER REQUIREMENTS OF THE FAN SYSTEM (KW)
	C	HFAIR	- HORSEPOWER REQUIREMENTS OF THE FAN SYSTEM (HP)
	C	HOWAT	- HORSEPOWER REQUIREMENTS OF THE WATER PUMPING SYSTEM (HP)
90	C	HFA1	- HEAT RATE FACTOR AT POINT ONE (DIMENSIONLESS)
	C	HFA2	- HEAT RATE FACTOR AT POINT TWO (DIMENSIONLESS)
	C	HFR21	- RATIO OF HFA2 TO HFA1 USED FOR SCALING UP PLANT TO DESIGN CONDITIONS (DIMENSIONLESS)
	C	HSLVA	- SURFACE AREA COVERED BY HAIL SCREENS OR LOUVERS (SQ FT)
95	C	ITOWN	- NUMBER OF CIRCULAR TOWERS (DIMENSIONLESS)
	C	KCONV	- INTERNAL VARIABLE FOR SPECIFYING THAT THE SET OF INPUT VARIABLES LEAD TO UNREASONABLE VALUES (DIMENSIONLESS)
100	C	KGA	- VARIABLE FOR SPECIFYING GAGE OF TUBES USED IN THE CONDENSER (DIMENSIONLESS)
	C	LD	- VARIABLE FOR SPECIFYING THE DIAMETER OF THE CONDENSER TUBING (DIMENSIONLESS)
	C	NEGV	- STOPS THE PROGRAM IF THE SCALED UP FRONTAL AREA, MASS FLOW OF AIR AND SPECIFIC VOLUME OF AIR IS LESS THAN ZERO (DIMENSIONLESS)
105	C	NJMTOW	- NUMBER OF CIRCULAR TOWERS (DIMENSIONLESS)
	C	NW	- NUMBER OF HEAT EXCHANGER TUBES IN WIDTH (DIMENSIONLESS)
110	C	PER	- PERCENTAGE OF TOTAL CAPITAL COSTS OF DRY COOLING TOWER ALLOWED FOR MAINTENANCE COST (PERCENT)
	C	PLANC	- BASE PLANT COSTS (\$/KW)
	C	PLANC1	- PLANT COSTS AT POINT ONE (\$/KW)
	C	PLANC2	- PLANT COST AT POINT TWO (\$/KW)

115	C	PLANC3	- PLANT COSTS AT POINT THREE
	C	PMELEC	- COST OF ELECTRICAL WIRING FOR WATER PUMPING SYSTEM (\$)
	C		
	C	POHCND	- INDIRECT COSTS FOR SURFACE CONDENSER AS A PERCENTAGE OF BASE COSTS (PERCENT)
120	C	POHSCL	- INDIRECT COSTS FOR AHIL SCREENS AND LOUVERS AS A PERCENTAGE OF BASE COSTS (PERCENT)
	C		
	C	POHSTC	- INDIRECT COSTS FOR THE STRUCTURES AND FOUNDATION FOR THE CIRCULAR TOWER AS A PERCENTAGE OF BASE COSTS (PERCENT)
125	C	PPOW	- POWER REQUIREMENTS OF THE WATER PUMPING SYSTEM (KW)
	C	PSIZE	- SPECIFIED POWER OUTPUT OF THE PLANT AND MAKE UP SYSTEM TO THE POWER GRID (MW)
	C		
	C	PSIZ12	- POWER OUTPUT OF TURBINE AT THE TURBINE RATED BACK PRESSURE FOR A POWER OUTPUT OF THE TURBINE OF PSIZE AT DESIGN CONDITIONS (MW)
130	C	PSIZ13	- POWER OUTPUT OF TURBINE AT THE TURBINE RATED BACK PRESSURE FOR A POWER OUTPUT OF THE PLANT OF PSIZE AT DESIGN CONDITIONS (MW)
	C		
	C	PTOTAL	- TOTAL POWER OUTPUT OF THE TURBINE AT DESIGN CONDITIONS (MW)
135	C	RANGE	- TEMPERATURE DIFFERENCE OF THE WATER ENTERING AND LEAVING THE HEAT EXCHANGER (DEG F)
	C		
	C	ROOFL	- ROOF LOAD DESIGN CONDITIONS FOR STRUCTURAL COSTS OF CIRCULAR TOWERS (LBF/SQ FT)
140	C	SAFRON	- SCALED UP FRONTAL AREA OF THE HEAT EXCHANGER NORMAL TO AIR FLOW (SQ FT)
	C	SPBP	- INCREMENTAL PLANT COST BETWEEN PLANT DESIGNED AT RATED CONDITIONS (POINT 1) AND AT DESIGN CONDITIONS (POINT 2) (\$)
145	C	SPC	- COST OF PLANT AT DESIGN CONDITIONS (POINT 3)
	C	SPCD	- INCREMENTAL COST OF PLANT USING DRY COOLING TOWERS AT DESIGN CONDITIONS (POINT 3) OVER PLANT AT RATED CONDITIONS (POINT 1) (\$)
	C		
	C	STRUCC	- STRUCTURAL COST OF THE CIRCULAR TOWERS (\$)
150	C	SWLRAT	- SCALED UP WIDTH TO LENGTH RATIO OF THE HEAT EXCHANGER (DIMENSIONLESS)
	C		
	C	SW3	- SCALED UP MASS FLOW RATE OF WATER THROUGH THE HEAT EXCHANGER (LBM/HR)
	C	SW4	- SCALED UP MASS FLOW RATE OF AIR THROUGH THE HEAT EXCHANGER (LBM/HR)
155	C	TOWFCS	- TOTAL COST OF THE PIPING SYSTEM (K\$)
	C	T _D	- DESIGN TEMPERATURE OF THE DRY COOLING TOWER (DEG F)
	C	TEFF	- RATED BACK PRESSURE EFFICIENCY OF THE STEAM TURBINE (PERCENT)
160	C	T _{LA}	- LENGTH OF CONDENSER TUBING (FT)
	C	T _A	- EXIT TEMPERATURE OF THE AIR FROM THE HEAT EXCHANGER (DEG F)
	C	V _A	- SPECIFIC VOLUME OF THE AIR (CU FT/LBM)
	C	WATERW	- WEIGHT OF WATER IN THE HEAT EXCHANGER BUNDLES (LBM)
165	C	W _{HX}	- TOTAL WEIGHT OF THE HEAT EXCHANGER EXCLUDING WATER (LBM)
	C		
	C	WIDTH	- TOTAL HEAT EXCHANGER WIDTH (FT)
	C	WLRAT	- RATIO OF THE WIDTH TO THE LENGTH OF THE HEAT EXCHANGER (DIMENSIONLESS)
170	C	WPL	- WEIGHT OF THE PLENUM PER UNIT AREA (LBF/SQ FT)
	C	WSTRUCT	- TOTAL WEIGHT OF THE COOLING TOWER STRUCTURES (LBF)

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C      WTERM  - TOTAL WEIGHT OF THE HEAT EXCHANGER FRAM (LBG)
C      WTHDR  - TOTAL WEIGHT OF THE HEAT EXCHANGER HEADERS (LBF)
C      WITUB  - TOTAL WEIGHT OF THE HEAT EXCHANGER TUBES (LBF)
175  C      W3    - MASS FLOW RATE OF THE WATER THROUGH THE HEAT
C      W4    - MASS FLOW RATE OF THE AIR THROUGH THE HEAT
C           EXCHANGER (LBM/HR)
C      XNFAN  - NUMBER OF FANS IN THE FAN SYSTEM (DIMENSIONLESS)
C      XNS    - NUMBER OF SHELLS IN THE SURFACE CONDENSER
180  C           (DIMENSIONLESS)
C      XNTS   - NUMBER OF CONDENSER TUBES PER SHELL (DIMENSIONLESS)
C      XW     - TRANSVERS PITCH BETWEEN ADJACENT TUBES IN THE SAME
C           TUBE ROW OF THE HEAT EXCHANGER FROM CENTERLINE TO
C           CENTERLINE (IN)
185  C      YEPPI - PLANT SCALING FACTOR TO TAKE INTO ACCOUNT FOR PUMP
C           AND FAN POWER

      LOGICAL FXTLNG
      LOGICAL NEG5
190  LOGICAL FIRST, FXTMP
      COMMON
      $ AFR, ALPHA
      $ CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHS, CONMAT, CONW42, CAP
195  $ CBU, CSEALP, CELAST, CFS, COANG, CLUVR, CHAILS, CVM
      $ DEEPL, DESVEL, DANGLE
      $ EFFP
      $ FCR, FIRST, FIXL, FCOS, FXTMP
      $ GBEPF
      $ HXNP, HPCST
200  $ THEAT
      $ ITMAX, ITMIN
      $ UCONG
      $ KCONY, KALEXT
      $ MXEXT
205  $ NTUCAL(2), NTA
      COMMON
      $ ODR
      $ PSIZF, PER, PWCOS, PLANG, PFACT
      $ POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSLC
210  $ QREJ, QREDUCE
      $ RBP, REDUCE, ROESEL, ROEELA, ROOFL, RFIX
      $ SAAF, SIGMA, SPAMAT(2)
      $ TD, TPO(4), TEPF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
      $ TUBADG, TW
215  $ UCS, UWS
      $ VAS(5)
      $ W4V
      $ XDEPA, XW, XD
      COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFFP
220  $ CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,
      $ FPOW, DELEC, WIDTH, ELN3, VAIR, VWAT, HI, HO, T4,
      $ REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3,
      $ SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
      $ RP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELDX
225  $ TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
      $ CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPID, AST
      $ CAPCST, XNFAN, BLDANG, CPLEN, DPFEI, WHX, ATTUB, ADIA, ABLN
      $ WTHDR, WTERM, STRJCC, CPERF, HPPERF, TOTCF, EFFIN, ANTU

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230      $, AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTP, ADJTP
      $, ACTBPD, ADJBPD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
      $, CSPD, WATERW, WSTRCT, CFOUW, HUBDIA, TOWLEN, CSE, CHF
      $, CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
      COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
235      $, CLAN1, REA1, Z1, HRFAC2, W41, U1, PFOX1,
      $, FPOW1, DEFC1, WIDT1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,
      $, REWA1, W1, ZPL, C2, ZSIZ12, ZSPBP, SW41, SW31,
      $, SPC1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
      $, BP2MIN, NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONBA1, XNTS1, VELD1
      $, TL1, UCON1, FMCS1, FBAC1, EFFC1, CHI, CA1, C51
240      $, CLTC1, CFC1, CPCC1, FITC1, CSC1, CEPRE1, DEPIP1, AST1
      $, CAPCS1, XNFAN1, BLOAN1, CPLEN1, DPFE1, WH1, ATTU1, ADI1, ABL1
      $, WTHD1, WTER1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
      $, AIRFF1, WATFF1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACTTP1, ADJTP1
245      $, ACTBPD1, ADJBPD1, ACTVH1, ADJVH1, ADJPP1, THPAI1, TCTF1, AFCST1
      $, CSP1, WATER1, WSTRCT1, CFOUW1, HUBD11, TOWLE1, CSE1, CHF1
      $, CBA1, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
      COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,
      $, GAIR, FAIR, HPAIR, HPWAT, PLANCT1
      COMMON /LACALL/ SRN
250      COMMON /ESCAL/ BSECF
      COMMON /TINE/ XNS, TTD, TLA, XNTS, ARPS
      COMMON /TUBE/ KGA, FGA(7), LD, ESA(5), TID(7,6), FTF(7,6)
      COMMON /PLCOST/ WPL
      COMMON /FLSW/ FXTLNG
255      COMMON /PME/ PMELEC
      COMMON /HEADEX/ CHH, CN, CHM, CMW, CRJ, CWJ, CST, CMO, CSR, CSM, PITCHF, CPM,
      1PRESS, HEDMAT, HEDTYP, NPASS, WB
      COMMON /FAN/ FANDAP(153,10), FANDAH(153,10), FMCPP, FBCPP,
      $VELREC, AFC, ELEV, EHR
260      DATA NFGV/, FALSE./
901      FORMAT(1X, A10, "T1, RANGE, CWARA, AFROV, WLRAT", 5314.4)
      NAMELIST /DBNL/ AFROV, VA, W4, TD, T4, CWARA, RANGEI
      XTOW = ITOWN

265      C
      C      SCALING FACTOR FROM POINT 1 TO POINT 2 TO ACCOUNT FOR CHANGE
      C      IN HEAT RATE FACTOR
      C
      HRFR21=HRFAC2/HRFAC1

270      C
      C      POWER OUTPUT OF TURBINE AT RATED BACK PRESSURE (POINT 1) WHICH
      C      GIVES REQUIRED POWER OUTPUT PSIZE AT THE DESIGN
      C      BACK PRESSURE (POINT 2)
      C
      PSIZ12=PSIZE*HRFR21

275      C
      C      PLANT COSTS AT DESIGN CONDITIONS (POINT 2) WHICH INCLUDE:
      C      STEAM SUPPLY AND BACK PRESSURE SCALING TO POINT 2
      C
      PLANC2=PLANC1 * HRFR21

280      C
      C      INCREMENTAL COST OF SCALING UP PLANT DUE TO INCREASED HEAT
      C      RATE FACTOR
      C
      SPBP=(PLANC2-PLANC)*PSIZE*1.E+3.

285      C

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C      SCALING FACTOR FOR SCALING PLANT SIZE TO MEET PUMP AND FAN
C      POWER REQUIREMENTS
C
290      IF (PSIZE*1000.-PPOW-FPOW*LE*0.0) KCONV=1
      IF (KCONV.EQ.1) RETURN
      YFP=(PSIZE*1.E+3)/(PSIZE*1.E+3-PPOW-FPOW)-1.0
C
C      POWER OUTPUT OF THE TURBINE GENERATOR AT THE RATED
C      BACK PRESSURE (POINT 1) WHICH MEETS THE POWER REQUIREMENTS OF
295      THE FANS AND PUMPS (POINT 3) AND THE POWER OUTPUT OF THE
C      PLANT AT THE DESIGN BACK PRESSURE (POINT 2)
C
      PSIZ13=(1.+YFP)*PSIZ12
C
C      TOTAL POWER OUTPUT OF THE PLANT AT POINT 3
300      PTOTAL = PSIZE * (1.+YFP)
C
C      PLANT COST AT POINT 3 EXCLUDING THE DRY COOLING TOWER COST
305      PLANC3=PLANC2*(1.+YFP)
      SPC=PLANC3*PSIZE*1.E+3
C
C      INCREMENTAL COST OF PLANT DUE TO DRY COOLING TOWERS
310      SPCD= (PLANC3-PLANC) * PSIZE * 1.E+3
C
C      SCALING UP THE DRY COOLING TOWER DIMENSIONS AND THE COSTS
315      ASSOCIATED WITH IT
C
C      INDEPENDENT PARAMETERS OF THE DRY COOLING TOWER
C
      YFPP1=YFP + 1.
      SW3=W3*YFPP1
      SW4=W4*YFPP1
      SAFRON=AFRON*YFPP1
      SWLRAT=WLRAT * YFPP1
C
C      SURFACE CONDENSER DIMENSIONS AND COSTS
325
      ISUR = 1
      CALL SURCON(ISUR, KGA, LD, TLA, XNTS, ARPS, XNS, CONBAS, CONMAT
      ,POHCND)
      XNTS = XNTS*YFPP1
      CONBAS = CONBAS*YFPP1
330
C
C      SCALE THE NUMBER OF TUBES IN WIDTH AND THE WIDTH OF THE
C      HEAT EXCHANGER
C
335      IF (FXTLNG) WIDTH=SAFRON/FIXL
      IF (.NOT.FXTLNG) WIDTH=SQRT(SWLRAT*SAFRON)
      TOWLEN = WIDTH / (XTOW*2.)
      NW=WIDTH/XW*12.
C
C      CHECK ON THE EXIT TEMPERATURE OF THE AIR LEAVING THE HEAT
340      EXCHANGER
C

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      T4=CHADA*RANGE+TD
      VA=53.35*(TD+460.)/(15.*144.)
345      IF(SAFCON.LT.0.0) NEGV=.TRUE.
      IF(VA.LT.0.0) NE3V=.TRUE.
      IF(SW4.LT.0.0) NEGV=.TRUE.
      IF(NEGV) WRITE(6,DRNL)
      IF(NEGV) STOP
350      41 CONTINUE
      C
      C
      C      FAN AND PUMP POWER
      C
      FPOW=FPOW * YFPP1
355      PPOW=PPOW * YFPP1
      HPWAT=HPWAT * YFPP1
      HPAIR=HPAIR * YFPP1
      XNFAN=XNFAN*YFPP1
      C
      C
      C      THE NUMBER OF FANS AND THE MOTOR, BLADE, AND ELECTRICAL
      C      WIRING COSTS OF THE FAN SYSTEM
      C
      FMCST=XNFAN*FMCPE
      FBACC=FBCPE*XNFAN
365      CFANEL = CFANEL * YFPP1
      C
      C
      C      ELECTRICAL WIRING COST OF THE PIPING SYSTEM
      C
      PMELEC = PMELEC * YFPP1
370      C
      C
      C      DIMENSIONS AND WEIGHT OF THE HEAT EXCHANGER
      C
      ATUBC = (CA + CH + CS + CSE) * BSECFI
      ATUBC = ATUBC*YFPP1
375      AAIR=AAIR * YFPP1
      WHX=WHX*YFPP1
      WTTUB=WTTUB*YFPP1
      WTHDR=WTHDR*YFPP1
      WTERM=WTERM*YFPP1
380      WATERW = WATERW * YFPP1
      C
      C
      C      INCREASED FUEL COST OF THE PLANT
      C
      C      FUEL COST, FOR THE BASE PLANT WITH A CONVENTIONAL TURBINE
      C      OPERATING AT RATED BACK PRESSURE
      FCBZ=FCOS * 3413.E-5 / TEFF
385      C
      C
      C      INCREASED FUEL COST FOR THE SCALED UP PLANT
      FCB3 = FCOS * 3413.E-5*(HRFAC2/TEFF) * (1.+YFP)
390      DELFC=FCB3-FCBZ
      C
      C
      C      LAND AND PIPING COSTS
      C
      CLAND = COSTL*SAFRON
495      CPIPI = TCWFCS * YFPP1 * 1000.
      C
      C
      C      PLENUM SIZE AND COSTS
      CTOWD = CTOWD * YFPP1

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400      CPLEN = CPM * WPL * (ITOWN * 3.14159/4. * CTOWD**2
$ - XNFAN * 3.14159/4. * (ADIA+3.5)**2)
      CPLEN = CPLEN * POHSTC
C
C      STRUCTURE AND FOUNDATION COSTS
405      CALL STRUCT(CTOWD, WHX, WATERW, ROOFL, STRUCC, CFOUND, WSTRUCT,
$      NUMTOW, ELENG, POHSTC)
      CFOUND = POHSTC * CFOUND
C
C      LOUVER AND HAIL SCREEN COSTS
410      HSLVA = CTOWD * NUMTOW * 3.14159 * ELENG
      CSTLVR = CLUVR * HSLVA * POHSCL
      CSTHS = CHAILS * HSLVA * POHSCL
415      C
C      TOTAL COST OF DRY COOLING TOWER
C
      CCOS = FBACC + ATURC + FMCST + CPLEN + STRUCC + CFOUND
$ + CSTLVR + CSTHS + CFANEL*XNFAN/YFPP1 + CYLRNG*XNFAN
420      COSM = PER * (CCOS + CPIP + CONBAS) / (PSIZE*CAPF*8760.)
C
C      ANNUAL INCREMENTAL COST DUE TO MAINTENANCE OF DRY COOLING
C      TOWERS
425      C
C      INCREMENTAL COST OF DRY COOLING TOWER
C
      OLDOST = (CCOS+SPCD+CLAND+CPIC+CONBAS)*FCR/(PSIZE*CAPF*8760.)
$ + COSM*DELFC
430      RETURN
      END

```

SUBROUTINE SERCH

THIS ROUTINE SEEKS MINIMUM BY SINGLE VARIABLE SEARCH METHOD

LOGICAL FXTLNG

COMMON /LACALL/ SRN

DIMENSION C(5)

COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF

S, CLAND, REAIR, Z,HRFAC2, W4, U, PPOW,

S, FPOW, DELEC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4,

S, REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3,

S, SPC,PTOTAL,PLANC3,SAFRON, AAIR, YFP, SPCD,PSIZ13, WT2,

S, BP2, NW2, TCOS, DELPA,DELPWT,DELPWC,CONBAS, XNTSX, VELOX

S, TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS

S, CLTC, CFC, CPCC, FITCO, CSC,CEPREP,DELP1P, AST

S, CAPCST, XNFAN,BLDANG, CPLEN, DPPEL, WHX, WTTUB, ADIA, ABLN

S, WTHDR, WTRFM,STRUCC,CFPERF,HPERF, TOTCF, EFFIN, ANTU

S, AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTTP, ADJTP

S, ACTBD, ADJBD, ACTVH, ADJUH, ADJPPF, THPAIR, TCTF, AFCST

S, CSO, WATERW, WSTRCT, CFOUN, HUBDIA, TOWLEN, CSE, CHF

S, CBA, NUMTOW, CTOWD, ATUBC, CSTLV, CSTHS, CYLRNG, CFANEL

COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1

S, CLAN1, REAI1, Z1,HRFA2S, W41, U1, PPOW1,

S, FPOW1, DEFC1, WID1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,

S, REW1, NW1,ZPLNC2,ZSIZ12, ZSPBP, SW41, SW31,

S, SPC1,PTOT1,PLNC31, AFR01, AAIR1,YFPMIN, SPCD1, SPS13,WT2MIN,

S, BP2MIN,NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1,CONBA1, XNTS1, VELO1

S, TL1, UCON1, FMC1, FBAC1, EFFC1, CH1, CA1, CS1

S, CLTC1, CFC1, CPCC1,FITC01, CSC1,CEPRE1,DEPI1, AST1

S, CAPCST1,XNFAN1,BLOAN1,CPLEN1,DPPEL1, WH1, WTTU1, ADI1, ABL1

S, WTHD1, WTR1,STRUC1,CFMPF1, HPPF1,TOTCF1,EFFIN1, ANTU1

S, AIRFF1, WATFF1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACTTP1, ADJTP1

S, ACTBD1, ADJBD1, ACTVH1, ADJUH1, ADJPP1, THPAI1, TCTF1, AFCST1

S, CSO1, WATER1, WSTRC1, CFOUN1, HUBD1, TOWLE1, CSE1, CHF1

S, CBA1, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1

COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,

S, GAIR, FAIR, HPAIR, HPWAT, PLANC1

LOGICAL FIRST, FXTMP

COMMON

S, AFTR, ALPHA

S, CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2,CAFI

S, CRU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHA1LS, CVM

S, DEEPL, DESVEL, DANGLE

S, EFFP

S, FCR, FIRST, FIXL, FCOS, FXTMP

S, GREFF

S, HXNP, HPCST

S, IHEAT

S, ITMAX, ITMIN

S, JCONG

S, KCON, KALEXT

S, MXEXT

S, NTUCAL(2), NTA

COMMON

S, ODR

S, PSIZE, PER, PWCOS, PLANC, PFACT

S, POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCN


```

      S ,QREJ, QREDUCE
      S ,RSP, REDUCE, ROESEL, ROELA, ROOFL, RFIX
60    S ,SAAF, SIGMA, SPAMAT(2)
      S ,TD, TPO(4), TEFF, TLIM, TLPA, TSEALP, TELAST, THFIN, TFIX
      S ,TUBARG, TW
      S ,U,S, UWS
      S ,V,S(5)
55    S ,W=V
      S ,XDEPA, XW, XD
      COMMON /FLSW/ FXTLNG
      COMMON /TINE/ XNS,TTD,TLA,XNTS,ARPS
      CWARL = 0.0
70    IF(FXTMP) CALL ROOT(TFIX,RFIX,TTD,TD,CWARL)
      IF(FXTMP .AND. VAR(3) .GT. 0.90*CWARL) VAR(3) = 0.90*CWARL
      DO 50 IVAL=1,5
50    VAL(IVAL)=VAR(IVAL)
      SRN="/SERCH-1/ "
75    CALLI CALC(VAL(1),VAL(2),VAL(3),VAL(4),VAL(5),1)
      CALLI STORE
      C(1)=5.
      C(2)=1.
      C(3)=1.
80    C(4)=CAF
      C(5)=50.
      IB=1
      IF(FXTLNG) IB=2
      DO 3 I=IB,5
85    M=6-I
      K=3
      DO 9 IX=1,5
9    VAL(IX)=VAR(IX)
      KC=0
90    1 J=0
      2 VAL(M)=VAR(M)+C(M)
      IF(FXTMP) VAL(1) = TFIX
      IF(FXTMP) VAL(2) = RFIX
      IF(FXTMP .AND. VAL(3) .GT. 0.90*CWARL) GO TO 7
95    IF(M.GT.3) GO TO 10
      IF(VAL(1) .GT. TLIM) GO TO 4
      H = VAL(3)*VAL(2)/(VAL(1)-TTD-TD)
16    IF(H.GE.1.) GO TO 4
      IF(4LOG(1.-H)/VAL(3).LE.-1.) GO TO 4
100    10 SRN="/SERCH-2/ "
      CALLI CALC(VAL(1),VAL(2),VAL(3),VAL(4),VAL(5),M)
      IF(KCONV.EQ.1) GO TO 4
      C
      IF(DELPA.LT.XDEPA) GO TO 3
      IF(DELPA.LE.XDEPA) GO TO 3
105    IF(TCOS.GE.TCOS1) GO TO 4
      J=1
      CALLI STORE
      GO TO 2
110    3 IF(K.EQ.1) KC=1
      4 IF(J.EQ.1) GO TO 7
      5 VAL(M)=VAR(M)-C(M)
      IF(FXTMP) VAL(1) = TFIX
      IF(FXTMP) VAL(2) = RFIX
      IF(VAL(M).LE.0.0) GO TO 7

```

```
115      H = VAL(3)*VAL(2)/(VAL(1)-TTD-TD)
18      IF(H.GE.1.) GO TO 7
      IF(ALOG(1.-H)/VAL(3).LE.-1.) GO TO 7
      SPN="/SERCH-3/ "
      CALL CALC(VAL(1),VAL(2),VAL(3),VAL(4),VAL(5),M)
120      IF(KC.EQ.1) GO TO 7
      C
      IF(DEPA.LT.XDEPA) GO TO 6
      IF(DEPA.LE.XDEPA) GO TO 6
      IF(TCOS.GE.TCOS1) GO TO 7
      CALL STORE
125      KC=0
      GO TO 5
      6 IF(K.EQ.1) KC=1
      7 IF(KC.EQ.1) CALL CHNGE(M)
      K=K-1
130      IF(K.EQ.0) GO TO 8
      C(M)=C(M)/5.
      GO TO 1
      8 CONTINUE
      RETURN
135      END
```

SUBROUTINE SETUP(TSTAR,TEND,VUCASE)

INPUT DESCRIPTION

FOR BNW1 PLASTIC CIRCULAR TOWER
 DECEMBER 10 1976

IN THE DESCRIPTIONS BELOW THE SYMBOL (DF) MEANS
 DECIMAL FRACTION

CARD	TYPE	COLUMNS	FORMAT	NAME OF VARIABLE	DESCRIPTION AND (UNITS)
A1	1-80	(8A10)	DESCR(I)	R	COMMENTS OR CASE DESCRIPTION TO BE PRINTED AT TOP OF FIRST OUTPUT PAGE. ANY NUMBER OF TYPE A1 CARDS MAY BE USED BUT A BLANK A1 CARD IS NOT ALLOWED.
A2	1-80	BLANK IN ALL COLUMNS. ONE TYPE A2 CARD ONLY			
B1	1-10	E10.0,	TSTAR	R	LOWEST DESIGN TEMPERATURE TO USE (DEGREES F)
	11-20	E10.0,	TEND	R	HIGHEST DESIGN TEMPERATURE TO USE (DEGREES F)
	21-30	E10.0,	VAS(1)	R	INITIAL VALUE FOR TURBINE OUTLET TEMPERATURE (DEGREES F)
	31-40	E10.0,	VAS(3)	R	INITIAL VALUE FOR CWRA, RATIO OF MCP WATER / MCP AIR (DF)
	41-50	E10.0,	VAS(4)	R	INITIAL VALUE FOR APRON, AIR SIDE FRONTAL AREA (SQ FT)
	51-60	E10.0,	VAS(5)	R	INITIAL VALUE FOR WLRAT, RATIO OF HEAT EXCHANGER WIDTH/LENGTH (DF)
	61-70	E10.0,	FIXL	R	LENGTH OF HEAT EXCHANGER (FT). IF THE ABSOLUTE VALUE OF FIXL=0, THEN THE PROGRAM WILL CALCULATE THE LENGTH.
	71-80	E10.0)	DEEPL	R	LIMITING VALUE FOR NUMBER OF TUBES (NUMBER OF TUBES)

```

60      IF THE ABSOLUTE VALUE OF DEEPL = 0.0
      THEN THE PROGRAM WILL COMPUTE THE
      DEPTH WITH NO CONSTRAINTS

      *DEEPL IMPLIES CONSTRAINT OF GREATER
      THAN OR EQUAL TO DEEPL

      *DEEPL IMPLIES CONSTRAINT OF LESS
      THAN OR EQUAL TO DEEPL.

65      C.....
      C.....

70      C1      1-40      (8F5.0, TA(I)      R:  TEMPERATURES REPRESENTATIVE OF
      TPER(I) FRACTION OF YEAR (DEGREES F)
      C A U T I O N  =  HIGHEST TA
      MUST BE FIRST

75      41-80      8F5.0)  TPER(I)      R:  FRACTION OF YEAR OVER WHICH TEMPERA-
      TURE TA(I) IS TYPICALLY (OF)

80      C.....
      C2      1-40      (8F5.0, TA(I)      R:  CONTINUATION OF TA(I) FOR I= 9 TO 16.
      41-80      8F5.0)  TPER(I)      R:  CONTINUATION OF TPER(I)
      NOTE - A TYPE C2 CARD IS REQUIRED EVEN IF BLANK.

85      C.....
      C.....
      C D1      4-10      (E10.0, PSIZE      R:  BASE PLANT SIZE (MEGAWATTS)
      11-20      E10.0, TEFF      R:  BASE THERMAL EFFICIENCY (OF)
90      21-30      E10.0, CAPF      R:  CAPACITY FACTOR (OF)
      31-40      E10.0, FCR      R:  FIXED CHARGE RATE (OF)
95      41-50      E10.0, PER      R:  RATIO MAINTENANCE COST TO CAPITAL
      COST (OF)
      51-60      E10.0, CCM      R:  CONSTRUCTION COST MULTIPLIER (OF)
100     61-70      E10.0, ELEV      R:  SITE ELEVATION ABOVE SEA LEVEL (FT)
      71-80      E10.0) ROOFL      R:  ROOF LOAD (LB/SQ FT)

105     C.....
      C.....
      C E1      1-10      (E10.0, FCOS      R:  FUEL COST (CENTS/MMBTU)
      11-20      E10.0, PWCOS      R:  REPLACEMENT POWER COST (MILLS/KWH)
110     21-30      E10.0, PLANC      R:  POWER PLANT CONSTRUCTION COST ($/KW)
      31-40      E10.0, COSTL      R:  COST OF LAND ($/SQ FT)

```

SUBROUTINE: SETUP

74/74 OPT=1

FTN 4.2+74351

12/20/76

115	C	41-50	E10.0,	CSSPKW	R	COST OF STEAM SUPPLY (\$/KW)
	C					
	C	51-60	E10.0,	CAPCHG	R	CAPACITY CHARGE (\$/MEGAWATT)
	C					
	C	61-70	E10.0)	HPCST	R	COST OF ELECTRIC MOTORS (\$/HP)
120	C					
	C					
	C					
	C					
125	C	E2 1-10	(E10.0,	POHBAF	R	INDIRECT COST FACTORS FOR BUNDLE ASSEMBLY AND FRAME
	C					
	C	11-20	E10.0,	POHFAN	R	FANS
	C					
	C	21-30	E10.0	POHLEC	R	ELECTRICAL
130	C					
	C	31-40	E10.0	POHCIR	R	CIRCULATION PIPING
	C					
	C	41-50	E10.0	POHCND	R	CONDENSER
	C					
135	C	51-60	E10.0,	POHSTC	R	STRUCTURE
	C					
	C	61-70	E10.0)	POHSCL	R	SCREENS AND LOUVERS
	C					
	C					
140	C					
	C	F1 1-10	(F10.0,	RBP	R	TURBINE RATING BACK PRESSURE (INCHES OF MERCURY)
	C					
	C	11-70	4F15.8)	TPO(I)	R	COEFFICIENTS FOR THIRD ORDER POLYNOMIAL FOR HEAT RATE AS A FUNCTION OF TURBINE BACK PRESSURE.
145	C					
	C					
	C					
	C					
150	C					
	C	G1 1-10	(E10.0,	EFFP	R	EFFICIENCY OF PUMPS (DF)
	C					
	C	11-20	E10.0)	DPRESS	R	PIPING DESIGN PRESSURE (PSI)
	C					MAY BE
155	C					50.
	C					70.
	C					125.
	C					
	C					
160	C					
	C					
	C	H1 1-10	(E10.0,	VELREC	R	CONTROL VARIABLE.
	C					=1 FOR VELOCITY RECOVERY
	C					=0 FOR NO VELOCITY RECOVERY
165	C					
	C	11-20	E10.0,	XDEPA	R	MINIMUM AIR SIDE PRESSURE DROP THRU HEAT EXCHANGER (LB FORCE/SQ FT)
	C					
	C	21-30	E10.0,	TLIM	R	MAXIMUM STEAM TEMPERATURE FOR THE TURBINE (DEGREES F).
170	C					
	C					

74/74. OPT=1

FTN 4.2+74351

12/20/86

Line	Code	Field	Unit	Description	Notes
175	31-40	E10.0	TOWMIN	R	THE MINIMUM ALLOWABLE NUMBER OF TOWERS PER GROUP. ASSUMED 1 IF NOT SPECIFIED
180	41-50	E10.0	PFACT	R	PACKING FACTOR, RATIO OF CIRCULAR TOWER ROOF AREA TO FAN SWEEP AREA (DF)
185	51-60	E10.0	TFIX	R	FIXED TURBINE OUTLET TEMPERATURE (F). ENTRY IS IGNORED IF BLANK OR ZERO
190	61-70	E10.0	RFIX	R	FIXED RANGE (F). ENTRY IS IGNORED IF BLANK OR ZERO
195	71-80	E10.0	TOWMAX	R	MAXIMUM ALLOWABLE NUMBER OF TOWERS. ASSUMED 9999 IF BLANK OR ZERO
200	H2 1-10	E10.0	GBEFF	R	FAN GEARBOX EFFICIENCY
205	I1 1-10	(E10.0)	CPM	R	PLENUM COST (\$/LB)
210	11-20	E10.0	WPL	R	WEIGHT OF PLENUM MATERIAL (LB/SQ FT)
215	21-30	E10.0	CLUVR	R	COST OF LOUVERS (\$/SQ FT)
220	31-40	E10.0	CHALS	R	COST OF HAIL SCREENS (\$/SQ FT)
225	41-50	E10.0	UCS	R	UNIT COST OF STACK \$/LB
230	51-60	E10.0	UWS	R	UNIT WT OF STACK LB/CU FT
235	61-70	E10.0	CVM	R	FAN RING MATERIAL UNIT COST \$/LB
240	71-80	E10.0	WFM	R	UNIT WT OF STRAIGHT CYLINDER LB/SQ FT
245	J1 1-20	(2A10)	NTUCAL	I	CONTROL VARIABLE FOR SPECIFYING THE METHOD TO BE USED TO CALCULATE NTU. NTUCAL MUST BEGIN IN COLUMN 1.

CROSS FLOW
COUNTER FLOW
TABLE

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230      C      CROSS FLOW OR COUNTER FLOW CAUSES
      C      CALCULATION OF NTU BY EQUATIONS.
      C      TABLE CAUSES TABLE LOOKUP OF NTU.
      C
      C      21-30   F10.0, HXNP   R  NUMBER OF PASSES THRU HEAT EXCHANGER
235      C      31-40   F10.0, WB    R  HEADER LENGTH (FEET)
      C      41-50   F10.0, NTUB   R  NUMBER OF TUBES THRU PLATE FINS
      C      51-60   F10.0, SS     R  SUPPORT SPACING (FT)
240      C
      C.....
      C.....
      C
245      C  J2   1-10   (E10.0, DESVEL R  DESIGN WATER VELOCITY FOR PIPING
      C      C      (FT/SEC)
      C      11-20   E10.0, REDUCE  R  MINIMUM STEP CHANGE IN PIPE DIAMETER
      C      C      FOR TOWER PIPING (INCHES)
      C      C      MAY BE 6, 12, OR 18
250      C      21-30   E10.0, QREDUCE R  MINIMUM STEP CHANGE IN PIPE DIAMETER
      C      C      FOR QUADRANT HEADERING. (INCHES)
      C      C      MAY BE 6, 12, OR 18
255      C      31-40   E10.0, DIST  R  DISTANCE FROM TOWER TO CONDENSER
      C      C      ROOM (FT)
      C
      C.....
      C.....
260      C  K1   1-10   (F10.0, XW    R  TUBE TRANSVERSE PITCH (NORMAL TO AIR
      C      C      FLOW) (INCHES)
      C      11-20   F10.0, XD      R  TUBE PITCH IN DIRECTION OF AIR FLOW
265      C      C      (INCHES)
      C      21-30   F10.0, XDG     R  TUBE DIAGONAL PITCH (INCHES)
      C      31-40   A10,   TUBARG  R  TUBE ARRANGEMENT, MUST BEGIN IN
270      C      C      COLUMN 1. MAY BE-
      C      C      STAGGERED
      C      C      INLINE
      C
      C      ASSUMED TO BE STAGGERED IF OMITTED
275      C      41-50   A10,   HCCALC R  CONTROL VARIABLE TO SELECT METHOD
      C      C      TO BE USED IN CALCULATING FRICTION
      C      C      FACTOR AND HEAT TRANSFER COEFFICIENT
      C      C      FOR AIR FLOWING ACROSS STAGGERED
280      C      C      TUBES. MAY BE 1 OR 2
      C      C      (ASSUMED 2 IF BLANK)
      C
      C      HCCALC=1 SPECIFIES MCADAMS RELATION-
285      C      C      SHIP FOR HEAT TRFR AND FOR
      C      C      FRICTION FACTOR

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74/74. OPT=1

FTN 4,2+74351

12/20/16.

LINE NO.	ITEM NO.	ITEM NAME	UNIT	DESCRIPTION
290				HCCALC=2 SPECIFIES MCADAMS RELATIONSHIP FOR FRICTION FACTOR AND ZUKAUSKAS RELATIONSHIP FOR HEAT TRANSFER COEFF.
295	51-60	F10.0) DANGLE	R	BASE ANGLE FOR DELTA HEAT EXCHANGER (DEGREES)
300	L1	1-10 (F10.0, ODL)	R	HX LINER OUTSIDE DIAMETER (INCHES)
		11-20 F10.0, DI	R	HX LINER INSIDE DIAMETER (INCHES)
305		21-30 F10.0, GAGLIN	R	GAGE OF HX LINER TUBE (MAY BE 22. 20. 19. 18. 17. 16. 15. 14.5 14. 13. 12. 11. 10.)
310	31-50	2A10, TUBMAT, XTUBMA	R	LINER MATERIAL. MUST BEGIN IN COL 31 MAY BE - POLYETHYLENE, POLYPROPYLENE, POLYVINYLCHLORIDE
315	51-60	F10.0) CONL	R	THERMAL CONDUCTIVITY OF LINER MATERIAL (BTU/(HR SQFT DEG F/ FT))
320	M1	1-20 (2A10, SPAMAT	R	SPACER MATERIAL. MUST BEGIN IN CARD COLUMN 1. MAY BE POLYVINYLCHLORIDE, POLYCARBONATE
325	21-30	F10.0, CSEALP	R	SEAL PLATE COST (\$/LB)
330	31-40	F10.0, TSEALP	R	SEAL PLATE THICKNESS (IN)
	41-50	F10.0, CELAST	R	ELASTOMER COST (\$/LB)
	51-60	F10.0, TELAST	R	ELASTOMER LAYER THICKNESS (IN)
335	61-70	F10.0, ROESEL	R	SEAL PLATE DENSITY (LB/CU IN)
	71-80	F10.0, ROELA	R	ELASTOMER DENSITY (LB/CU IN)
340	N1	1-10 (E10.0, CASTC	R	FIXED CASTING COST FOR SPACERS

					(\$/SPACER)
345	C	11-20	E10.0,	EPRPC	R END PREPARATION COST (\$/TUBE)
	C	21-30	E10.0)	CFS	R FRAME UNIT COST (\$/LB)
350	C				
	C				
	C	P1	1-20	(2A10,	HEDTYP, R HEADER TYPE. MUST START IN COLUMN 1.
	C			XHEDTY	R MAY BE -
355	C				WELD REMOVABLE
	C				WELD PLUG
	C				FORM REMOVABLE
	C				FORM PLUG
360	C	21-30	F10.0,	HEDMAT	R HEADER MATERIAL. MUST START IN
	C				COLUMN 21. MAY BE -
	C				ALUMINUM
	C				STEEL
365	C	31-40	F10.0)	TW	R THICKNESS OF HEADER MATERIAL, INCHES
	C				
	C				
370	C	01	1-10	(E10.0,	CRJ R COST OF ROLLED JOINT, TUBE TO HEADER
	C				(\$/TUBE)
	C		11-20	E10.0,	CWJ R COST OF WELDED JOINT, TUBE TO HEADER
	C				(\$/TUBE)
375	C		21-30	E10.0,	CHH R TUBE AND PLUG HOLE PREPARATION COST
	C				(\$/HOLE)
	C		31-40	E10.0,	CN R NOZZEL AND ATTACHING COST (\$/HOLE)
380	C		41-50	E10.0,	CMW R COST OF HEADER MACHINING AND WELDING
	C				(\$/FT)
	C		51-60	E10.0,	CST R STRUCTURAL STEEL COST (\$/LB)
385	C		61-70	E10.0)	CBJ R COST OF BOLTED HEADER JOINT (\$/FT)
	C				
	C				
390	C	R1	1-10	(E10.0,	XNS R NUMBER OF CONDENSER SHELLS
	C		11-20	E10.0,	VELN R NOMINAL DESIGN VELOCITY THRU CONDENSER
	C				TUBES (FT/SEC)
395	C		21-30	E10.0,	ODC R CONDENSER TUBE O.D. (INCHES)
	C		31-40	E10.0,	GA R CONDENSER TUBE WALL GAGE. MAY BE
	C				12. 14. 16. 18. 20. 22. 24.

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400      C      41-50  E10+0,  FC      R  CLEANLINESS FACTOR (DF)
      C
      C      51-60  E10+0,  TTD      R  TERMINAL TEMPERATURE DIFFERENCE
      C      (DEGREES F)
405      C      61-80  2A10)  CONMAT,  R  CONDENSER TUBING MATERIAL. MUST START IN
      C      CONMA2      R  COLUMN 61. MAY BE:
      C
      C      ADMIRALTY
      C      CU-10 NI
      C      304 S/S WELDED
410      C
      C
415      C.....
      C.....
      C      S1      1-5  (15,  LFB      I  LFB AND LFE SPECIFY FIRST AND LAST
      C      5-10  15,  LFE      I  POSITION TO BE CONSIDERED IN THE
420      C      TABLE OF FANS. DEFAULT VALUES ARE:
      C      LFB=1 AND LFE=153
      C
      C      -----
      C      DIAMETER      IFAN      LFAN
      C      -----
425      C      24.      1      27
      C      26.      28      54
      C      28.      55      88
430      C      30.      89      111
      C      40.      112      135
      C      50.      136      153
      C
      C      11-15  15      MXEXT      I  THE MAXIMUM ALLOWABLE NUMBER OF
435      C      CALLS TO SUBROUTINE XTENDI FOR ANY
      C      ONE DESIGN TEMPERATURE.
      C
      C      DEFAULT VALUE IS 10
      C
      C.....
440      C.....
      C      U1      2-72  NAMELIST INPUT CARD.      NAMELIST NAME IS "READIN"
      C      AT LEAST 1 TYPE U1 CARD IS REQUIRED.
      C      IN ITS SIMPLEST FORM THE U1 CARD IS
445      C      "READIN NUCASE=0 SENDI
      C      BEGINNING IN CARD COLUMN 2.
      C
      C      VARIABLES IN NAMELIST "READIN" ARE--
450      C      DANGLE, DESVEL, DIST,  DI,      FIXL,  LFB,
      C      LFE,  NUCASE,  ODL,  PFACT,  QREDUCE,  REDUCE,
      C      RFIX,  TFIX,  TLIM,  TOWMAX,  TOWMIN,  VELREC,
      C      XD,  XDG,  XW
455      C
      C      AFTER THE INITIAL CASE IS DESCRIBED WITH CARD TYPES A1-U1
      C      THEN ANY NUMBER OF TYPE U1 CARDS MAY BE USED TO REDEFINE

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C      ANY OF THE VARIABLES IN THE NAMELIST FOR ADDITIONAL CASES
C
C      NUCASE IS A CONTROL VARIABLE TO SPECIFY HOW THE DATA
460 C      FOR THE NEXT CASE ARE TO BE READ.
C
C      NUCASE = 0 SPECIFIES THAT THE DATA FOR THE NEXT
C      CASE ARE TO BE READ FROM A COMPLETE SET
C      OF A1 THRU U1 CARDS
465 C
C      NUCASE = 1 SPECIFIES THAT DATA FOR THE NEXT CASE
C      ARE TO BE READ FROM NAMELIST CARDS
C
REAL NTUB
470 DIMENSION TOD(6),TGA(7)
COMMON/DJB/DI,XDG,SF
COMMON/INDIS/DIST
COMMON/HEADX/CHH,CN,CHM,CW,CWJ,CST,CMO,CSR,CSM,PITCHF,CPH,
IPRESS,HEDMAT,HEDTYP,NPASS,WB
475 COMMON/SURFEX/ODL,GAGLIN,NTUB,TUBMAT,FINTYP,FINMAT,CFB,APLATE,
$COATC,ZINCC,CATC,SS,EPRPC,XTUBMA,XHEDTY,XFINTY
COMMON/FLSW/FXTLNG
COMMON/TINE/XNS,TTD,TLA,XNTS,ARPS
COMMON/TINE2/CCM
480 COMMON/TUBE/KGA,FGA(7),LO,ESA(5),TID(7,6),FTF(7,6)
COMMON/OHTC/FC,CU(5),VELN
COMMON/SINK/ VAR(5),CPIPI,CCOSI, W3I,COSMI, EFFI
$ CLANI,REAI, ZI,HRFA2S, W4I, U1,PPOWI,
485 $ FPOWI,DEFCI,WIDT1,ELEN1,VARI,VWAT1, HI, HO1, T4I,
$ REWA1, NW1,ZPLNC2,ZSIZ12,ZSPBP, SW4I, SW3I,
$ SPC1,PTOT1,PLNC3I,AFROI,AAIR1,YFPMIN,SPCI,SPS13,WT2MIN,
$ BP2MIN,NW2MIN,TCOS1,DEPA1,DPWT1,DPWC1,CONBA1,XNTS1,VELDI
$ TLAI,UCON1,FMOS1,FBAC1,EFFCI, CH1, CAI, CSI
490 $ CLT1, CFC1,CPCC1,FITC1, CSC1,CEPRE1,DEPIPI, AST1
$ CAPCI,XNFANI,BLDANI,CPLENI,DPFEL1, WH1,WTU1, ADI1, ABL1
$ WTH1, WTR1,STRUC1,CEMPF1, HPP1,TOTCF1,EFFIN1, ANTU1
$ AIRF1, WATF1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACTTP1, ADJTP1
$ ACTBP1, ADJBP1, ACTVH1, ADJVH1, ADJPP1, THPA1, TCTF1, AFCST1
495 $ CS1, WATER1, WSTR1, CFOUN1, HUBDI1, TOWLE1, CSE1, CHF1
$ ,CS41, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLAN1, CFAE1
COMMON/SCALER/HRFAC1,SSCD,PLAVCI,CASSS1,
$ GAIR,FAIR,HPAIR,HPMAT,PLAVCI
COMMON/FNLOOP/LFB,LFE
COMMON/PLCOST/WPL
500 LOGICAL FXTLNG
DIMENSION DECCR(3)
LOGICAL FIRST,FXTMP
COMMON
505 $ AFTR,ALPHA
$ ,CAPF,CSSPKW,CONF,CONL,COSTL,CAPCHG,CONMAT,CONMA2,CAP
$ ,CBJ,CSEAL,CELAST,CFS,COANG,CLUVR,CHAILS,CVM
$ ,DEEPL,DESVEL,DANGLE
$ ,EFFP
$ ,FCR,FIRST,FXL,FCOS,FXTMP
510 $ ,GAEFF
$ ,HXDP,HPCST
$ ,IHEAT
$ ,ITMAX,ITMIN

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515 $ ,JCONS
$ ,KCONV, KALEXT
$ ,MEXET
$ ,NTUCAL(2), NTA
COMMON
$ OORI
520 $ ,PSIZE, PER, PWCOS, PLANC, PFACT
$ ,POHRAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCL
$ ,QREJ, QREDUCE
$ ,RJP, REDUCE, ROESEL, ROELA, ROOFL, RFIX
$ ,SAAF, SIGMA, SPAMAT(2)
525 $ ,TJ, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
$ ,TJBA-G, TW
$ ,UCS, UWS
$ ,VAS(5)
$ ,WFW
530 $ ,XDEPA, XW, XD
COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
$ , CLAND, REAIR, Z,HRFAC2, W4, U, PPOW,
$ ,FPQW, DELFC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4,
535 $ ,REWAT, NW,PLANC2,PSIZ12, SP3P, SW4, SW3,
$ ,SPC,PTOTAL,PLANC3,SAFRON, AAIR, YFP, SPCD,PSIZ13, WT2,
$ ,BP2, NW2, TCOS, DELPA,DELPWT,DELPWC,CONBAS, XNTSX, VELOX
$ , TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
$ , CLTC, CFC, CPCC, FITCO, CSC,CEPREP,DELP1P, AST
$ ,CANCST, XNFAN,BLDANG, CPLEN, JPFEL, WHX, WTTUB, ADIA, ABLN
540 $ , WTHAR, WTRFM,STRUCC,CFPERF,HPERF, TOTCF, EFFIN, ANTU
$ , AIRFF, WATFF, XMOD, TCTPF, FDCPF, FMTRC, ACCTTP, ADJTP
$ , ACTBD, ADJRPD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
$ , CSRD, WATERW, WSTRCT, CFOUND, HUBDIA, TOWLEN, CSE, CHF
$ ,CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
545 COMMON /VARVAR/ TPER(16), TA(15)
COMMON /INT/TIN(15),FTIN(15)
COMMON /PH2O/TH2O(16),PROP(16,2)
COMMON /CFHL/VELT(15),TELT(15),#BLT(15,2)
COMMON /FAN/ FANDAP(153,10),FANDAH(153,10),FMCPP, FBCPP,
550 $VELREC,AFC,ELEV,EHR
COMMON /PRESS/ IPRESS
NAMELIST/READIN/VELREC,TLIM,TFIX,RFIX,TOWMIN,TOWMAX,DESVEL,REDUCE,
$ QREDUCE,DIST,XW,XD,XDG,DANGLE,ODL,DI,FXLL,LFB,LFE,NUCASE,PFACT
DATA BLANK/"
555 C
C
C SURFACE CONDENSER TUBE O.D. AND TUBE GAGE ARRAYS
DATA TOD/0.625,0.750,0.875,1.000,1.125,1.250/
DATA TGA/12.,14.,16.,18.,20.,22.,24./
560 C
C
C EXTERNAL SURFACE AREA (SQ FT) OF CONDENSER TUBE PER LINEAR
C FOOT AS A FUNCTION OF TUBE O.D.
C
DATA ESA/0.1636,0.1963,0.2291,0.2618,0.2944,0.3271/
565 C
C
C TUBE WALL GAGE CORRECTION FACTOR FOR OVERALL HEAT TRANSFER
C COEFFICIENT FOR ADMIRALTY METAL, ARSENICAL COPPER OR
C ALUMINUM TUBES FOR SURFACE CONDENSERS
C
DATA FGA/0.87,0.92,0.96,1.00,1.02,1.04,1.06/
570

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C
C      CONDENSER TUBE I.D. AND GPM PER FPS VELOCITY THROUGH TUBE AS
C      A FUNCTION OF TUBE GAGE AND TUBE O.D.
C
575      DATA TID/0.407,0.459,0.495,0.527,0.555,0.569,0.581,
$          0.532,0.584,0.620,0.552,0.680,0.694,0.706,
$          0.657,0.709,0.745,0.777,0.805,0.819,0.831,
$          0.782,0.834,0.870,0.902,0.930,0.944,0.956,
$          0.907,0.959,0.995,1.027,1.055,1.069,1.081,
580      $          1.032,1.084,1.120,1.152,1.180,1.194,1.206/
$      DATA FTF/0.405,0.515,0.600,0.630,0.754,0.793,0.826,
$          0.593,0.835,0.941,1.041,1.132,1.173,1.220,
$          1.057,1.231,1.359,1.473,1.586,1.642,1.690,
$          1.497,1.703,1.853,1.992,2.117,2.182,2.137,
585      $          2.014,2.251,2.424,2.582,2.725,2.797,2.861,
$          2.607,2.877,3.071,3.249,3.409,3.490,3.560/

C
C      CONDENSER INLET TEMPERATURE ARRAY INLET TEMPERATURE
C      CORRECTION FACTOR FOR OVERALL HEAT TRANSFER COEFFICIENT FOR
590      SURFACE CONDENSERS
C
$      DATA TIN/30.,35.,40.,45.,50.,55.,60.,65.,70.,75.,80.,85.,
$          90.,95.,100./
$      DATA FTIN/0.545,0.613,0.679,0.743,0.805,0.863,0.917,0.962,
595      $          1.000,1.025,1.042,1.060,1.074,1.093,1.100/

C
C      VELOCITY CONSTANT FOR OVERALL HEAT TRANSFER COEFFICIENT AS A
C      FUNCTION OF TUBE O.D.
C
600      DATA CU/257.,267.,263.,263.,259.,259./

C
C      WATER TEMPERATURE ARRAY AND WATER DENSITY AND VISCOSITY AS A
C      FUNCTION OF TEMPERATURE
C
605      DATA TH20/32.,40.,50.,60.,70.,80.,90.,100.,110.,120.,130.,
$          140.,150.,160.,170.,180./
$      DATA DPROP/62.42,62.42,62.38,62.34,62.27,62.17,62.11,61.99,
$          61.84,61.73,61.54,61.39,61.20,61.01,60.79,60.57,
$          4.33,3.75,3.17,2.71,2.37,2.08,1.85,1.65,1.49,
610      $          1.36,1.24,1.14,1.04,0.97,0.90,0.84/

C
C      CONDENSER TUBE VELOCITY ARRAY AND TUBE END LOSS PER PASS AND
C      WATERBOX LOSS FOR SINGLE AND TWO PASS CONDENSERS AS A
615      FUNCTION OF VELOCITY
C
$      DATA VELT/1.,1.5,2.,2.5,3.,3.5,4.,4.5,5.,5.5,6.,6.5,7.,7.5,8./
$      DATA TELT/.005,.035,.060,.110,.160,.220,.280,.360,.450,.540,
$          .643,.752,.873,1.002,1.146/
620      DATA WBLT/.02,.035,.070,.110,.170,.220,.303,.395,.488,.605,.723,
$          .950,.987,1.136,1.293,
$          .04,.06,.09,.14,.20,.28,.37,.47,.58,.71,.841,
$          .938,1.149,1.314,1.487/
89      FORMAT('INPUT ERROR. THE SUM OF THE TPER(I) SHOULD BE 1.0000')
6000      FORMAT('H1///T05,"BNW1 DRY COOLING TOWER COST MODEL -- ",
$          " PLASTIC TUBE, CIRCULAR TOWER VERSION.",
$          " ,T80,"THIS RUN MADE ",A10,"X,A10)
425

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5001 FORMAT(8A10)
6001 FORMAT(T21,8A10)
630 5002 FORMAT(8E10.0)
6002 FORMAT(/1X,8G15.8)
5003 FORMAT(16F5.0)
6003 FORMAT(/1X,8F8.1,9F8.4)
5004 FORMAT(F10.0,4F15.8)
635 6004 FORMAT(/1X,F10.2,4G15.8)
5005 FORMAT(2A10,6F10.0)
6005 FORMAT(/1X,2A10,1X,6G15.8)
5006 FORMAT(3F10.0,2A10,F10.0)
640 6006 FORMAT(/1X,3F10.5,1X,2A10,F10.5)
5007 FORMAT(3A10,5F10.0)
6007 FORMAT(/1X,2A10,1X,A10,5G15.8)
5008 FORMAT(9IS)
6008 FORMAT(/1X,8I6)
5009 FORMAT(6E10.0,2A10)
645 6009 FORMAT(/1X,6G15.8,5X,2A10)
7060 FORMAT(T6,"TSTAR",T21,"TEND",T35,"VAS(1)",T51,"VAS(3)"
$ ,T56,"VAS(4)",T81,"VAS(5)",T96,"FIXL",T111,"DEEPL")
7090 FORMAT(4X,"TA(1)",3X"TA(2)",3X"TA(3)",3X"TA(4)",3X"TA(5)"
$ ,3X"TA(6)",3X"TA(7)",3X"TA(8)",1X"TPER(1)",1X"TPER(2)",1X"TPER(3)"
$ ,1X"TPER(4)",1X"TPER(5)",1X"TPER(6)",1X"TPER(7)",1X"TPER(8)"
650 7120 FORMAT(4X"TA(9)",2X"TA(10)",2X"TA(11)",2X"TA(12)",2X"TA(13)"
$ 2X"TA(14)",2X"TA(15)",2X"TA(16)",1X"TPER(9)",TPER(10)TPER(11)TPER(12)
$ 2TPER(13)TPER(14)TPER(15)TPER(16))
7150 FORMAT(T5,"PSIZE",T23,"TEFF",T39,"CAPF",T54,"FCR",T69,"PER"
$ ,T94,"CCM",T96,"ELEV",T108,"ROOFL")
655 7180 FORMAT(T5,"PCOS",T23,"PWCOS",T39,"PLAN",T52,"COSTL",T67,"CSSPKW"
$ ,T92,"CAPCH",T97,"HPCST")
7185 FORMAT(T5,"POHBAF",T20,"POHFAN",T35,"POHLEC",T50,"POHCIR",
$ T65,"POHCND",T80,"POHSTC",T95,"POHSCL")
660 7210 FORMAT(T5,"RBP",T17,"TPO(1)",9X"TPD(2)",9X"TPD(3)",9X"TPD(4)")
7240 FORMAT(T5,"HEFF",T20,"DPRESS")
7270 FORMAT(T4,"VELREC",T20,"XDEPA",T35,"TLIM",T50,"TOWMIN",T65,"PFACT"
$ ,T73,"TFIX",T90,"RFIX",T105,"TOWMAX")
7300 FORMAT(T5,"CPM",T20,"WPL",T35,"CLUVR",T50,"CHAILS",T65,"UCS",T80
$ ,T95,"CVM",T110,"WFW")
665 7330 FORMAT(T5,"NTUCAL",T24,"HXNP",T44,"WB",T58,"VTUB",T75,"SS"
$ )
7335 FORMAT(T5,"DESVEL",T21,"REDUCE",T35,"QREDUCE",T50,"DIST")
7360 FORMAT(T6,"XW",T18,"XD",T28,"XDG",T35,"TUBARG",H"CALC",T53
$ ,"DANGLE")
670 7390 FORMAT(5X"ODL",12X"DI",9X"GAGLIN",9X"TUBMA",13X"CONL")
7400 FORMAT(T5,"SPAMAT",T28,"CSEALP",T43,"TSEALP",T56,"CELAST"
$ ,T73,"TELAST",T88,"ROESEL",T103,"ROEELA")
675 7450 FORMAT(5X,"CASTC",10X,"EPREPC",10X,"CFS")
7480 FORMAT(T4,"HEDTYP",T24,"HEDMAT",T36,"TW")
7510 FORMAT(5X,"CRJ",12X,"CWJ",12X,"CHH",12X,"CN",12X,"CMW",12X,"CST",
$ 12X,"CBJ")
7540 FORMAT(5X,"XNS",12X,"VELN",11X"ODC",12X"GA",13X"FC",13X"TYD"
$ ,15X"CONMAT")
680 7570 FORMAT(T4,"LFB",T11,"LFE",T15,"MXEXT")
7280 FORMAT(5X,"GBEFF")

```

C

```

DO 18 I=1,5
18 VAR(I) = 0.0

```

```

685      TCOS = 0.0
      C
      FXTNG=.FALSE.
      FXTMP = .FALSE.
      CALL DATE(DOY)
690      CALL TIME(HEURE)
      WRITE(4,6000) DOY,HEURE
      IF(NUCASE.GT. 0) GO TO 110
      C
      CARDS A1 = A2
795      30 READ(5,5001) DESCR
      DO 35 I=1,8
      IF(DESCR(I).NE.BLANK) GOTO 37
      35 CONTINUE
      GOTO 40
700      37 WRITE(4,6001) DESCR
      GOTO 30
      40 CONTINUE
      C
      CARD B1
705      READ(5,5002) TSTAR, TEND, VAS(1), VAS(3), VAS(4), VAS(5)
      $ ,FIXL, DEEPL
      WRITE(4,5002) TSTAR,TEND, VAS(1), VAS(3), VAS(4), VAS(5)
      $ ,FIXL, DEEPL
710      WRITE(4,7050)
      C
      CARD C1
      READ(5,5003) (TA(I),I=1,8) , (TPER(I),I=1,8)
      WRITE(4,5003) (TA(I),I=1,8) , (TPER(I),I=1,8)
715      WRITE(4,7090)
      C
      CARD C2
      READ(5,5003) (TA(I),I=9,16) , (TPER(I),I=9,16)
      WRITE(4,5003) (TA(I),I=9,16) , (TPER(I),I=9,16)
720      WRITE(4,7120)
      C
      CARD D1
      READ(5,5002) PSIZE, TEFF, CAPF, FCR, PER, CCM, ELEV, ROOFL
      WRITE(4,5002) PSIZE, TEFF, CAPF, FCR, PER, CCM, ELEV, ROOFL
725      WRITE(4,7150)
      C
      CARD E1
      READ(5,5002) FCOS, PWCOS, PLANC, COSTL, CGSPKW, CAPCHG, HPCST
      WRITE(4,5002) FCOS, PWCOS, PLANC, COSTL, CGSPKW, CAPCHG, HPCST
730      WRITE(4,7180)
      C
      CARD E2
      READ(5,5002) POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC
      $ ,POHSCL
735      WRITE(4,5002) POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC
      $ ,POHSCL
      WRITE(4,7185)
      C
      CARD F1
740      READ(5,5004) RBP, (TPO(I),I=1,4)
      WRITE(4,5004) RBP, (TPO(I),I=1,4)
      WRITE(4,7210)

```

```

C
CARD G1
745   READ(5,5002) EFPF, DPRESS
      WRITE(6,5002) EFPF, DPRESS
      DPRESS = DPRESS + 1.E-30
      IPRESS = DPRESS
      WRITE(4,7240)

C
750   CARD H1
      READ(5,5002) VELREC, XDEPA, TLIM, TOWMIN, PFACT, TFIX, RFIX
      S
      WRITE(6,5002) VELREC, XDEPA, TLIM, TOWMIN, PFACT, TFIX, RFIX
      S
      TOWMAX
755   ITMIN = TOWMIN + 1.E-30
      IF (ITMIN .LT. 1) ITMIN = 1
      ITMAX = TOWMAX + 1.E-30
      IF (ITMAX .LT. 1) ITMAX = 9999
      IF (ITMAX .LT. ITMIN) STOP "TOWMAX IS LESS THAN TOWMIN"
760   IF (TLIM .LT. 1.) TLIM = 180.
      IF (TFIX.GT.0.0 .AND. RFIX.GT.0.0) FXTMP = .TRUE.
      WRITE(4,7270)
      IF (VAS(1) .LE. 0.0) VAS(1) = TSTAR + (TLIM-TA(1))-5.

C
765   CARD H2
      READ(5,5002) GBEFF
      WRITE(6,5002) GBEFF
      WRITE(6,7280)

C
770   CARD I1
      READ(5,5002) CPM, WPL, CLUVR, CHAILS, UCS, UWS, CVM, WFW
      WRITE(6,5002) CPM, WPL, CLUVR, CHAILS, UCS, UWS, CVM, WFW
      WRITE(6,7300)

C
775   CARD J1
      READ(5,5005) NTUCAL, HXNP, WB, NTUB, SS
      WRITE(6,5005) NTUCAL, HXNP, WB, NTUB, SS
      WRITE(6,7330)

C
780   CARD J2
      READ(5,5002) DESVEL, REDUCE, QREDUCE, DIST
      WRITE(6,5002) DESVEL, REDUCE, QREDUCE, DIST
      WRITE(4,7335)

C
785   CARD K1
      READ(5,5006) XW, XD, XDG, TUBARG, HCCALC, DANGLE
      IF (TUBARG .EQ. " ") TUBARG = "STAGGERED "
      IF (HCCALC .EQ. " ") HCCALC = "2. "
      IF (TUBARG .EQ. "STAGGERED " .AND. HCCALC .EQ. "1")
790   IF (TUBARG .EQ. "STAGGERED " .AND. HCCALC .EQ. "2")
      IF (TUBARG .EQ. "INLINE ") IHEAT = 3
      WRITE(6,5006) XW, XD, XDG, TUBARG, HCCALC, DANGLE
      WRITE(6,7360)
      CONVERT DEGREES TO RADIANS
      COANG = COS(DANGLE * 3.14159 / 180.)
795   9990 FORMAT("0IHEAT=",I3)
      WRITE(6,9990) IHEAT
C

```

*) IHEAT=1
*) IHEAT=2


```

      CARD L1
000      READ(5,5006) ODL, DI, GAGLIN, TUBMAT, XTUBMA, CONLI
          WRITE(4,6006) ODL, DI, GAGLIN, TUBMAT, XTUBMA, CONLI
          WRITE(4,7390)
      C
      CARD M1
005      READ(5,5005) SPAMAT,CSEALP,TSEALP,CELAST,TELAST,ROESEL,ROEELA
          WRITE(4,6005) SPAMAT,CSEALP,TSEALP,CELAST,TELAST,ROESEL,ROEELA
          WRITE(4,7400)
      C
      CARD N1
010      READ(5,5002) CASTC, EPREPC, CFS
          WRITE(4,5002) CASTC, EPREPC, CFS
          WRITE(4,7450)
      C
      CARD P1
015      READ(5,5007) HEDTYP, XHEDTY, HEDMAT, TW
          WRITE(4,6007) HEDTYP, XHEDTY, HEDMAT, TW
          WRITE(4,7490)
      C
      CARD Q1
020      READ(5,5002) CRJ, CWJ, CHH, CN, CMW, CST, CBJ
          WRITE(4,5002) CRJ, CWJ, CHH, CN, CMW, CST, CBJ
          WRITE(4,7510)
      C
      CARD R1
025      READ(5,5009) XNS, VELN, ODC, GA, FC, TTD, CONMAT, CONMA2
          WRITE(4,5009) XNS, VELN, ODC, GA, FC, TTD, CONMAT, CONMA2
          WRITE(4,7540)
      C
      CARD S1
030      READ(5,5008) LFB, LFE, MXEXT
          WRITE(4,5008) LFB, LFE, MXEXT
          WRITE(4,7570)
          IF (MXEXT.LT. 1) MXEXT = 10
          IF (LFE.LT. LFB) STOP "LFB EXCEEDS LFE ON INPUT CARD"
035      C
          EHR = 3414.43 / TEFF
          IF (FIXL.GT.0.0) FXTLNG=.TRUE.
          DO 45 I=1,16
          IF (TPER(I).LT.1.E-20) GOTO 46
          NTA=J
040      45 CONTINUE
          46 CONTINUE
          SUMP=0.0
          DO 20 I=1,16
          SUMP=SUMP + TPER(I)
045      20 SUMP=SUMP + TPER(I)
          IF (ABS(SUMP-1.0).LT.1.E-10) GOTO 22
          WRITE(4,69)
          STOP
          22 CONTINUE
050      C
      C DETERMINE POSITION OF TUBE O.D. AND GAGE IN RESPECTIVE ARRAYS
      C
055      DO 99 I=1,6
          LD = I

```

```

      IF( ABS(ODC-TOD(LD)) .LT. .001) GOTO 1011
99  CONTINUE
      STOP "ILLEGAL VALUE FOR CONDENSER TUBE OD"
C
860  1011 DO 98 I= 1,7
      KGA = I
      IF( ABS(GA-TGA(KGA)) .LT. .001) GOTO 100
98  CONTINUE
      STOP "ILLEGAL VALUE FOR CONDENSER TUBE GAGE"
C
865  100 CONTINUE
C
      CALL COSTEX(DUM1)
C
870  RETURN
C
      110 CONTINUE
      READ(5,READIN)
      IF(NUCASE.EQ. 0) RETURN
875  WRITE(4,6002) TSTAR,TEND, VAS(1), VAS(3), VAS(4), VAS(5)
      * ,FIXL,DEEPL
      WRITE(4,7060)
      WRITE(4,6003) (TA(I),I=1,8), (TPER(I),I=1,8)
      WRITE(4,7120)
880  WRITE(4,6002) PSIZE, TEFF, CAPFL, FCR, PER, CCM, ELLEV, ROOFL
      WRITE(4,7150)
      WRITE(4,6002) FCOS, PHCOS, PLANC, COSTL, CSSPKW, CAPCHG, HPCST
      WRITE(4,7180)
      WRITE(4,6002) POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC
885  * ,POHSCL
      WRITE(4,7185)
      WRITE(4,6004) RBP, (TPO(I),I=1,4)
      WRITE(4,7210)
      WRITE(4,6002) EFPF, DPRESS
890  WRITE(4,7240)
      WRITE(4,6002) VELREC, XDEPA, TLIM, TOWMIN, PFACT, TFIX, RFIX
      * ,TOWMAX
      ITMIN = TOWMIN + 1.E-30
      IF (ITMIN .LT. 1) ITMIN = 1
895  ITMAX = TOWMAX + 1.E-30
      IF (ITMAX .LT. 1) ITMAX = 9999
      IF (ITMAX .LT. ITMIN) STOP "TOWMAX IS LESS THAN TOWMIN"
      IF (TLIM .LT. 1) TLIM = 180.
      IF (TFIX .GT. 0.0 .AND. RFIX .GT. 0.0) FXTEND = .TRUE.
900  WRITE(4,7270)
      WRITE(4,6002) GBEFF
      WRITE(4,7280)
      WRITE(4,6002) CPM, WPL, CLUVR, CHAILS, UCS, UWS, CVM, WFW
      WRITE(4,7300)
905  WRITE(4,6005) NTUCAL, HXNP, WB, NTUB, SS
      WRITE(4,7330)
      WRITE(4,6002) DESVEL, REDUCE, QREDUCE, DIST
      WRITE(4,7335)
      WRITE(4,6006) XW, XD, XDG, TUBARG, HCCALC, DANGLE
910  WRITE(4,7360)
      CDANG = COS(DANGLE * 3.14159 / 180.)
      WRITE(4,6006) ODL, DI, GAGLIN, TUBMAT, XTUBMA, CONLI

```

SUBROUTINE SETUP

74/74 OPT=1

FTN 4.2+7*351

12/20/76

```

915      WRITE(4,7390)
        WRITE(4,6005) SPAMAT,CSEALP,TSEALP,CELAST,TELAST,ROESEL,ROEELA
        WRITE(4,7400)
        WRITE(4,6002) CASTC, EPREPC, CFS
        WRITE(4,7450)
        WRITE(4,6007) HEDTYP, XHEDTY, HEDMAT, TW
920      WRITE(4,7480)
        WRITE(4,6002) CRJ, C=J, CMH, CN, CMW, CST, CSU
        WRITE(4,7510)
        WRITE(4,6009) XNS, VELN, ODC, GA, FC, ITD, CONMAT, CONMA2
        WRITE(4,7540)
925      WRITE(4,6008) LFB, LFE, MTEXT
        WRITE(4,7570)
        IF(FIXL.GT.0.0) FXTLNG=.TRUE.
        END

```

SUBROUTINE SHOT(L)

C
C THIS ROUTINE ESTABLISHES A STARTING PLACE FOR THE MINIMIZING PRO-
C CEDURE BY SAMPLING POINTS AROUND THE STARTING VALUES PROVIDED.

5

LOGICAL FXTLNG
DIMENSION T(3),CHW(4),RANG(3),AFRO(3),WLRA(4),VAM(5)
LOGICAL FIRST, FXTMP
COMMON

10

S AFTR, ALPHA
S CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAFI
S CBU, CSEALP, CELAST, CFS, COANG, CLUVR, CHALS, CVM
S DEEPL, DESVEL, DANGLE
S EEPF

15

S FOR, FIRST, FIXL, FCOS, FXTMP
S GREFF
S HXNP, HPCST
S IHEAT

20

S ITMAX, ITMIN
S JCONG
S KCONV, KALEXT
S MXEXT
S NTUCAL(2), NTA

25

COMMON
S ODR
S PSIZE, PER, PWCOS, PLANC, PFACT
S POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSLC
S GREJ, GREduce
S RBP, REDUCE, ROESL, ROELA, ROOFL, RFIX
S SAAF, SIGMA, SPAMAT(2)
S TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
S TJ9AGG, TW
S UCS, UWS
S VAS(5)

35

S WFN
S XDEP, XW, XD
COMMON /FLSW/ FXTLNG
COMMON /LACALL/ SRN

40

COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
S CLAND, REAR, Z, HRFAC2, W4, U, PPOW, T4,
S FPOW, DEFC, WIDTH, ELENG, VAIR, VWAT, HI, HO,
S REWAT, NW, PLANC2, PSIZ12, SP3P, SW4, SW3,
S SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
S BP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELOX
S TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
S CLTC, CFC, CPCC, FITCO, CSC, CEPREP, DELPID, AST
S CAPCST, XNFAN, BLDANG, CPLEN, DPFE, WHX, WTTUB, ADIA, ABLNI
S WTHR, WTERM, STRUCC, CPERF, HPERF, TOTCF, EFFIN, AVTU
S AIREF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTIP, ADJTP
S ACTBPD, ADJBPD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
S CSPD, WATERW, WSTRCT, CFOWD, HUBDIA, TOWLEN, CSE, CHF
S CBA, NUMTOW, CTOWD, ATURC, CSTLVR, CSTHS, CYLRNG, CFANEL

50

COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
S CLAN1, REA1, Z1, HRFAC2S, W41, U1, PPOW1, T41,
S FPOW1, DEFC1, WIDTH1, ELENG1, VAIR1, VWAT1, HI1, HO1,
S REW1, NW1, PLNC2, ZSIZ12, ZSP3P, SW41, SW31,
S SPC1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPSI3, WT2MIN

55

```

      $ BP2MIN,NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONSA1, XNTS1, VELD1
      $, TLA1, UCON1, FMCS1, FBAC1, EFFC1, CH1, CA1, CS1
60    $, CLTC1, CFC1, CPCC1, FITC1, CSC1, CEPRE1, DEPI1, AST1
      $, CAPCS1, XNFAN1, BLDAN1, CPLEN1, DPFE1, WH1, WTTU1, ADI1, ABL1
      $, WTH1, WTR1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
      $, AIRFE1, WATFE1, XNMOD1, TCTPE1, FDCPE1, FMTPE1, ACTT1, ADJTP1
      $, ACTHT1, ADJRP1, ACTVH1, ADJVM1, ADJPP1, THPA1, TCTF1, AFCST1
65    $, CS1, WATER1, WSTRC1, CFOWN1, HUSD1, TOWLE1, CSE1, CHF1
      $, CBAL, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
      COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,
      $ GAIR, FAIR, HPAIR, HPWAT, PLAVCT1
      COMMON /TIME/ XNS, TTD, TLA, XNTS, ARPS
70    9500 FORMAT('0IN SHOT AT CHECKPOINT A. VAR(4)=",1PE12.4,6X,"VAM(4)=",
      $E12.4,6X,"DAFRO=",E12.4)
      9501 FORMAT('0IN SHOT AT CHECKPOINT B. I=",I1,6X,"DAFRO=",1PE12.4,6X,
      $ "VAR(4)=",E12.4,6X,"AFRO(I)=",E12.4)
      9502 FORMAT('0IN SHOT AT CHECKPOINT C. I=",I1,6X,"VAR(4)=",1PE12.4,
75    $ 6X,"FAF=",E12.4)
      IF (EXT=MP) CALL ROOT(TFIX,RFIX,TTD,TD,CHARL)
      IDB=0
      IF (L.EQ.2) GO TO 31
      DO 1 IS=1,5
80    1 VAM(IS)=0.0
      TCOS1=0.
      TCOS2=0.
      DO 20 I=1,3
      T(I)=V.S(I)+(I-2)*5.
65    IF (EXT=MP) T(I) = TFIX
      IF (T(I) .GT. 180.) T(I) = 180.
      20 IF (T(I) .LE. 0.0) T(I) = 10.0
      DO 21 I=1,4
      CWAR(I)=VAS(3)+(I-2)*2.
90    21 IF (CWAR(I).LE.0.) CWAR(I)=.5
      IF (.NOT. EXT=MP) GO TO 24
      CWAR(1) = CWARL*0.90
      CWAR(2) = CWARL*0.80
      CWAR(3) = CWARL*0.70
95    CWAR(4) = CWARL*0.60
      24 CONTINUE
      DO 22 I=1,4
      WLRA(I)=VAS(5)+(I-2)*10.
100    22 IF (WLRA(I).LE.0.) WLRA(I)=5.
      AFRO(1)=VAS(4)/2.
      AFRO(2)=VAS(4)
      AFRO(3)=VAS(4)*2.
      DT1=1.
      DCWAR=1.
105    DAFRO=1.
      DWLRA=1.
      LC=4
      LW=4
      GO TO 31
110    31 DT1=VAS(1)-VAM(1)
      DCWAR=VAR(3)-VAM(3)
      DAFRO=VAR(4)-VAM(4)
      C
      IF (DAFRO.LE.0.0.AND.IDB.NE.0) WRITE(6,9500) VAR(4),VAM(4),DAFRO
      *** CHECKPOINT

```

```

115      DWLRA=VAR(5)-VAM(5)
      IF(DT1.EQ.0.0.OR.DT1.EQ.VAR(1)) GO TO 33
      DO 32 I=1,3
      T(I) = VAR(1) - (I-1) * DT1/2.
120      IF(FXTMP) T(I) = TFIX
      32 CONTINUE
      GO TO 35
      33 DO 34 I=1,3
      T(I)=VAR(1)+(I-2)*2.
      IF(FXTMP) T(I) = TFIX
125      34 IF(T(I).GE.170.) T(I)=170.
      35 IF(DCWAR.EQ.0.0.OR.DCWAR.EQ.VAR(3)) GO TO 37
      DO 36 I=1,4
      CWAR(I)=VAR(3) - (I-1)*DCWAR/3.
      IF(CWAR(I).LE.0.0) CWAR(I)=0.25
130      36 CONTINUE
      GO TO 39
      37 DO 38 I=1,3
      CWAR(I)=VAR(3) + (I-2)
      IF(CWAR(I).LE.0.0) CWAR(I)=0.25
135      38 CONTINUE
      LC=3
      39 IF(DAFRO.EQ.0.0.OR.DAFRO.EQ.VAR(4)) GO TO 41
      DO 40 I=1,3
      40 AFRO(I)=VAR(4)-(I-1)*DAFRO/2.
140      C
      IF(IDB.EQ.0) GOTO 43
      DO 3040 I=1,3
      IF(AFRO(I).LE.0.0) WRITE(6,9501) I,DAFRO,VAR(4),AFRO(I)
      8040 CONTINUE
      GO TO 43
      41 FAF=.5F5
      TC=ABS(FAF-VAR(4))
      IF(TC.T1.E+4) FAF=FAF*0.9
      DO 42 I=1,3
      AFRO(I)=VAR(4)+(I-2)*FAF
      IF( AFRO(I).LE. 0.0) AFRO(I)=1000. * I
      42 CONTINUE
      C
      IF(IDB.EQ.0) GOTO 43
155      DO 8042 I=1,3
      IF(AFRO(I).LE.0.0) WRITE(6,9502) I,VAR(4),FAF
      8042 CONTINUE
      43 IF(DWLRA.EQ.0.0.OR.DWLRA.EQ.VAR(5)) GO TO 45
      DO 44 I=1,4
      44 WLRA(I)=VAR(5)-(I-1)*DWLRA/3.
      GO TO 51
      45 DO 46 I=1,3
      46 WLRA(I)=VAR(5)+(I-2)*5.
      LW=3
160      51 DO 15 IT=1,3
      DO 15 IC=1,LC
      IF(CWAR(IC).EQ.0.0) WRITE(6,9504) IC
      9504 FORMAT('01' SHOT, DIVISION BY ZERO. CWAR('',I2,'')=0.0")
      RANGL = (T(IT)-TTD-TD)*(1.-EXP(-CWAR(IC)))/CWAR(IC)
170      2 RANG(1)=.9*RANGL
      RANG(2)=.7*RANGL

```

```

RANG(3)=.5*RANGL
IF(FXTEMP) RANG(1) = RFIX
IF(FXTEMP) RANG(2) = RFIX
175 IF(FXTEMP) RANG(3) = RFIX
DO 15 IP=1,3
DO 15 IA=1,3
DO 15 IW=1,LW
KCALC=1
180 IF(IR.GT.1.OR.IC.GT.1) KCALC=2
IF(IA.GT.1) KCALC=4
IF(IW.GT.1) KCALC=5
SRN="/SHOT-1/ "
185 CALL CALC(T(IT),RANG(IP),CWAR(IC),AFRO(IA),WLRA(IW),KCALC)
IF(KCONV.EQ.1) GO TO 15
C IF(DELTA.LT.XDEPA) GO TO 16
IF(DELTA.LE.XDEPA) GO TO 16
IF(TCOS1.EQ.0.) GO TO 14
C IF(TCOS.GT.TCOS1) GO TO 16
190 IF(TCOS.GE.TCOS1) GO TO 16
IF(TCOS2.EQ.0.) GO TO 18
C IF(TCOS1.GT.TCOS2) GO TO 14
IF(TCOS1.GE.TCOS2) GO TO 14
18 TCOS2=TCOS1
195 DO 19 II=1,5
19 VAM(II)=VAR(II)
14 TCOS1=TCOS
VAR(1)=T(IT)
VAR(2)=RANG(IP)
200 VAR(3)=CWAR(IC)
VAR(4)=AFRO(IA)
VAR(5)=WLRA(IW)
CAF=AFRO(1)*.1
GO TO 15
205 16 IF(L.EQ.2) GO TO 15
IF(TCOS2.EQ.0.) GO TO 17
IF(TCOS.GE.TCOS2) GO TO 15
C IF(TCOS.GT.TCOS2) GO TO 15
210 17 TCOS2=TCOS
VAM(1)=T(IT)
VAM(3)=CWAR(IC)
VAM(4)=AFRO(IA)
VAM(5)=WLRA(IW)
15 CONTINUE
215 IF(ID3.EQ.0) RETURN
WRITE(4,553)TCOS1,VAR(1),VAR(2),VAR(3),VAR(4),VAR(5)
553 FORMAT(" TCOS1="E12.5," T11="F4.0," RANG1="F7.4," CWAR1="F7.3,
1" AFRO1="E10.3," WLRA1="F4.0)
RETURN
220 END

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SUBROUTINE SPDES (TD, TS, TR, TTD, XNS, CHLD, VELD, RHO, ARPS, TLA, XNTS, HDLD
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SUBROUTINE SPDES DESIGNS A SINGLE PRESSURE SURFACE CONDENSER
IN ACCORDANCE WITH HEAT EXCHANGE INSTITUTE (HEI) STANDARDS
FOR SURFACE CONDENSERS FOR GIVEN DESIGN VALUES OF TURBINE
EXHAUST STEAM SATURATION TEMPERATURE, CIRCULATING WATER
TEMPERATURE RISE IN THE CONDENSER, CONDENSER TERMINAL
TEMPERATURE DIFFERENCE, CLEANLINESS FACTOR, TUBE SIZE AND
NOMINAL VELOCITY THROUGH THE TUBES, AND FOR A GIVEN TUBE
MATERIAL

DEFINITION OF VARIABLES

ARPS - AREA PER CONDENSER SHELL (SQ FT)
AST - TOTAL AREA OF CONDENSER SHELLS (SQ FT)
CHLD - HEAT TRANSFERED IN THE CONDENSER (BTU/HR)
CU - ARRAY OF VELOCITY CONSTANTS FOR THE OVERALL HEAT
TRANSFER COEFFICIENT AS A FUNCTION OF THE TUBE
OUTSIDE DIAMETER (DIMENSIONLESS)
DELPWC - PRESSURE DROP OF THE WATER THROUGH THE CONDENSER
(LBF/SQ FT)
EFFC - EFFECTIVENESS OF THE CONDENSER (DIMENSIONLESS)
ESA - ARRAY OF EXTERNAL SURFACE AREA OF CONDENSER TUBE
PER LINEAR FOOT AS A FUNCTION OF TUBE OUTSIDE
DIAMETER ((SQ FT/FT)
FC - FOULING FACTOR FOR THE OVERALL HEAT TRANSFER
COEFFICIENT (DIMENSIONLESS)
FGA - ARRAY OF TUBE WALL GAGE CORRECTION FACTORS FOR THE
OVERALL HEAT TRANSFER COEFFICIENT FOR ADMIRALTY
METAL, ARSENICAL COPPER OR ALUMINUM TUBES FOR
SURFACE CONDENSERS (DIMENSIONLESS)
FPL - LENGTH OF FLOW PATH PER SHELL (FT)
FTF - ARRAY OF GPM PER FPS VELOCITY THRU TUBES AS A
FUNCTION OF TUBE GAGE AND TUBE OUTSIDE DIAMETER
(GPM/FT/SEC)
FTI - INLET TEMPERATURE CORRECTION FACTOR FOR THE
OVERALL HEAT TRANSFER COEFFICIENT (DIMENSIONLESS)
FTIN - ARRAY OF INLET TEMPERATURE CORRECTION FACTORS AS
A FUNCTION OF INLET TEMPERATURES (DIMENSIONLESS)
GDM - VOLUMETRIC FLOW RATE THROUGH THE CONDENSER
(GALLONS/MINUTE)
GDM - VOLUMETRIC FLOW RATE OF WATER THROUGH THE CONDENSER
(GALLONS/MINUTE)
GPMS - VOLUMETRIC FLOW RATE OF WATER THROUGH EACH SHELL
OF THE CONDENSER (GALLONS/MINUTE)
HDLOS - HEAD LOSS OF THE WATER THROUGH THE CONDENSER (FT)
HOLS - HEAD LOSS OF THE WATER THROUGH THE TUBES OF THE
CONDENSER (FT/100 FT)
PROP - ARRAY OF THE WATER PROPERTIES DENSITY AND VISCOSITY
AS A FUNCTION OF TEMPERATURE (LBM/CU FT LBM/FT HR)
RHO - DENSITY OF THE WATER (LBM/CU FT)
TAVT - AVERAGE TEMPERATURE OF THE WATER GOING THROUGH THE
CONDENSER (DEG F)
TOLM - LOG MEAN TEMPERATURE DIFFERENCE OF THE CONDENSER
(DEG F)
TE - EXIT TEMPERATURE OF THE WATER LEAVING THE CONDENSER


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C      (DEG F)
60      C      TELOS - HEAD LOSS OF THE WATER IN THE CONDENSER DUE TO
C      C      TUBE END EFFECTS (FT)
C      C      TELT - ARRAY OF HEAD LOSSES DUE TO TUBE END EFFECTS AS A
C      C      FUNCTION OF WATER VELOCITY (FT)
C      C      TH20 - ARRAY OF WATER TEMPERATURES (DEG F)
C      C      TI - INLET TEMPERATURE OF THE WATER ENTERING THE
65      C      CONDENSER (DEG F)
C      C      TID - ARRAY OF INSIDE TUBE DIAMETERS AS A FUNCTION
C      C      OF TUBE GAGE AND OUTSIDE DIAMETER (IN)
C      C      TIN - INLET TEMPERATURE ARRAY USED IN CONJUNCTION WITH
C      C      THE INLET TEMPERATURE CORRECTION FACTOR (DEG F)
70      C      TLA - INTEGER VALUE OF FLOW PATH LENGTH PER SHELL (FT)
C      C      TR - TEMPERATURE RANGE OF THE WATER FLOWING THROUGH THE
C      C      CONDENSER (DEG F)
C      C      TS - TURBINE EXHAUST STEAM SATURATION TEMPERATURE
C      C      (DEG F)
75      C      TTD - TERMINAL TEMPERATURE DIFFERENCE BETWEEN THE
C      C      SATURATED STEAM TEMPERATURE AND EXIT TEMPERATURE
C      C      OF THE WATER LEAVING THE CONDENSER (DEG F)
C      C      UCON - OVERALL HEAT TRANSFER COEFFICIENT OF THE CONDENSER
C      C      (BTU/HR- $32$  FT-DEG F)
80      C      VELD - VELOCITY OF THE WATER THRU THE TUBES OF THE
C      C      CONDENSER (FT/SEC)
C      C      VELN - INITIAL GUESS OF THE VELOCITY OF THE WATER IN THE
C      C      CONDENSER TUBES (FT/SEC)
C      C      VELT - ARRAY OF VELOCITIES USED IN CONJUNCTION WITH THE
85      C      TUBE END LOSS ARRAY AND THE WATER BOX LOSS ARRAY
C      C      (FT/SEC)
C      C      VIS - VISCOSITY OF THE WATER (LBM/FT-HR)
C      C      WRLOS - ARRAY OF HEAD LOSS IN THE WATER BOXES OF THE
C      C      CONDENSER AS A FUNCTION OF THE VELOCITY OF THE
90      C      WATER IN THE CONDENSER TUBES (FT)
C      C      WBLT - LOSS OF HEAD IN THE WATER BOX OF THE CONDENSER (FT)
C      C      XNP - NUMBER OF PASSES THE WATER MAKES THROUGH THE
C      C      CONDENSER SHELL (DIMENSIONLESS)
C      C      XNS - NUMBER OF CONDENSER SHELLS (DIMENSIONLESS)
95      C      XNTS - NUMBER OF TUBES PER CONDENSER SHELL (DIMENSIONLESS)
C
COMMON /RPRT2/ DMM ,TI ,TE ,TOLM ,XNP
S ,VELD7,DELPW7,ARPS7,TLA7,XNTS7,XNS7,TS7
COMMON /TUBE/ KGA,FGA(7),LD,ESA(5),TID(7,6),FTF(7,6)
100 COMMON /OHTC/ FC,CU(6),VELN
COMMON /INLT/ TIN(15),FTIN(15)
COMMON /PH20/ TH20(15),PROP(16,2)
COMMON /STEM/ TSTM(51),PSTM(51)
COMMON /CFHL/ VELT(15),TFLT(15),WBLT(15,2)
105 COMMON /SUPPLY/ VAL(5),CPID,CCOS,W3,COS4,EFF
S,CLAND,REAIR,Z,HFFAC2,W4,U,PROW,
$ FROW,DELF0,WIDTH,ELENG,VAIR,VWAT,HI,H0,T4,
$ REWAT,NW,PLANC2,PSIZ12,SPBP,SW4,SW3,
$ SPC,PTOTAL,PLANC3,SAPRON,AAIR,YFP,SPCD,PSIZ13,WT2,
110 $ BPR,NWR,TCOS,DELP4,DELPWT,DELPWC,CONBAS,XNTSX,VELDX
S,TLAX,UCON,FMCST,FRACC,EFFC,CH,CA,CS
$,CLTC,CFC,CPC,FITC,CSC,CEPREP,DELPID,AST
$,CAPCST,XNFAN,BLDANG,CPLEV,DPFEL,WHX,ATTUB,ADIA,ABLN
$,WTHAR,WTFRM,STRJCC,CPPERF,HPPERF,TOTCF,EFFIN,ANTU

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115      S, AIREF, WATFF, XNMOD, TCTPF, FOCPE, FMTRC, ACCTTP, ADJTP
      S, ACTBPD, ADJBPD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
      S, CSPO, WATERW, WSTRCT, CFOUND, HUBDIA, TOWLEN, CSE, CHF
      S, CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL

120      C
      C      DETERMINE CONDENSER OUTLET, INLET AND AVERAGE COOLING WATER
      C      TEMPERATURES, DENSITY OF COOLING WATER BASED ON AVERAGE
      C      TEMPERATURE, TOTAL COOLING WATER FLOW, COOLING WATER FLOW PER
      C      SHELL, LOG MEAN TEMPERATURE DIFFERENCE AND INLET TEMPERATURE
      C      CORRECTION FACTOR
125      C
      901 FORMAT(' NON INTEGER TLA. VALUE=',1PE13.6)
110      TE=TS-TTD
      TI=TE-TR
      TAVT=(TI+TE)/2.
130      RHO=TLU(TAVT,TH20,PROP,16)
      GPM=CHLD/(3.021*RHO*TR)
      C      WRITE(6,901) RHO,GPM
      GPM5=GPM/XNS
      TDLM=TR/ALOG((TR+TTD)/TTD)
135      FTI=1.1+0.001987*(TI-100.)
      IF(TI.LT.100.) FTI=TLU(TI,TIN,FTIN,15)

      C
      C      SET VELOCITY THROUGH TUBES EQUAL TO NOMINAL DESIGN VALUE AND
      C      INITIALIZE INDEX USED TO INDICATE WHETHER INITIAL OR SUB-
140      C      SEQUENT CALCULATION OF SURFACE AREA FOR GIVEN DESIGN
      C      CONDITIONS
      C
      VELD=VELN
      ISA=1

145      C
      C      DETERMINE OVERALL HEAT TRANSFER COEFFICIENT AND SURFACE AREA
      C      PER SHELL
      C
104      UCON=CU(LD)*SQRT(VELD)*FTI*FGA(KGA)*FC
150      DMM=UCON
      ARPS=(CHLD/XNS)/(UCON*TDLM)
      NAMELIST/DBGPO/
      S      ARPS,VELD,GPM5,XNP,VEL,TLA,XNS,CHLD,UCON,TDLM,ISA
      IF(LEGVAR(ARPS).NE.0) WRITE(6,DBGPO)
155      IF(LEGVAR(ARPS).NE.0) STOP 'IN SPDES1'

      C
      C      FOR INITIALLY CALCULATED VALUE OF SURFACE AREA, DETERMINE THE
      C      LENGTH OF FLOW PATH PER SHELL, THE NUMBER OF PASSES PER SHELL
      C      AND THE ACTUAL TUBE LENGTH ROUNDED TO THE NEAREST FOOT
160      C
      IF(ISA=1)100,100,101
100      FPL=ARPS*VELD*FTF(KGA,LD)/(GPM5*ESA(LD))
      IF(FPL.LT.1.E-20) WRITE(6,DBGPO)
      IF(FPL.LT.1.E-20) STOP 'IN SPDES2'
165      XNP=1.
      IF(FPL.GT.50.) XNP=2.
      TLA=4*INT(FPL/XNP)
      IF(TLA.LT.1.0) TLA=FPL/XNP
      IF(TLA.LT.1.0) WRITE(6,901) TLA
170      IF(TLA.LT.1.0) GOTO 103
      C

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C      CALCULATE ACTUAL VELOCITY THROUGH TUBES AND IF IT DOES NOT
C      AGREE WITHIN SPECIFIED LIMITS WITH THE CURRENT DESIGN VALUE,
175 C      CHANGE INDEX TO INDICATE SUBSEQUENT CALCULATION AND DETERMINE
C      SURFACE AREA USING CALCULATED VALUE OF VELOCITY
C
101  VELEGDMS=ESA(LD)*TLA*XNP/(ARPS*FTF(KGA,LD))
      IF(VEL.LT.1.E-20) WRITE(6,DBGP0)
      IF(VEL.LT.1.E-20) STOP "IN SPDES3"
180 C
      IF((ARPS(VEL-VELD)/VELD)-0.002)103,103,102
102  ISA=2
      VELD=VEL
      GO TO 104
185 C
C      DETERMINE NUMBER OF TUBES OF GIVEN SIZE PER SHELL AND TOTAL
C      CONDENSER HEAT TRANSFER SURFACE AREA
C
103  XNTS=AINT(GPMS/(VELD*FTF(KGA,LD)))+0.5)*XNP
190 XNTSX=XNTS * XNS
      AST=ARPS*XNS
C
C      DETERMINE HEAD LOSS THRU THE CONDENSER, INCLUDING TUBE-END
C      AND WATERBOX LOSSES
195 C
      VIS=TLU(TAVT,TH20,PROP(1,2),15)
      CALL HYDLOS(TID(KGA,LD),VELD,VIS,RHO,1,HOLS)
      TELOS=TLU(VELD,VELT,TELT,15)*XNP
      INP=XNP
200 WBLOS = TLU(VELD,VELT,WBLT(1,INP),15)
      HDLOS=TLA*XNP/100.*HOLS+TELOS+WBLOS
      DELPWC=HDLOS * RHO
C
C      STORAGE OF VARIABLES
205 C
      TLAX=TLA
      VELOX=VELD
      EFFC=TC/(TR+TTD)
      VELO7=VELD
      DELPW7=DELPWC
      ARPS7=ARPS
      TLA7=TLA
      XNTS7=XNTS
      XNS7=XNS
215 TS7=TS
      RETURN
      END

```

SUBROUTINE SSSCALE

SUBROUTINE SSSCALE SCALES THE STEAM SUPPLY SYSTEM UP TO OBTAIN THE SPECIFIED POWER OUTPUT OF THE PLANT (PSIZE) AT THE RATED BACK PRESSURE OF THE STEAM TURBINE. THE INCREMENTAL COST OVER THAT OF THE SYSTEM USING A CONVENTIONAL TURBINE IS CALCULATED AT THE RATED BACK PRESSURE.

DEFINITION OF VARIABLES

CASST1 - INCREMENTAL COST OF STEAM SUPPLY FOR MAKE UP OF POWER OUTPUT DUE TO INCREASED HEAT RATE AT RATED BACK PRESSURE (\$)
 CSSPKW - COST OF STEAM SUPPLY SYSTEM PER KILOWATT (\$/KW)
 HRFAC1 - HEAT RATE FACTOR OF STEAM TURBINE AT RATED BACK PRESSURE (DIMENSIONLESS)
 PLANC - COST OF POWER PLANT PER KILOWATT (\$/KW)
 PRIZE - PLANT SIZE (MW)
 RBP - STEAM TURBINE RATED BACK PRESSURE (IN HGA)
 SSCD - INCREMENTAL PLANT COST DUE TO INCREASED HEAT RATE AT RATED BACK PRESSURE OF STEAM TURBINE (\$)
 TPO - COEFFICIENTS OF THIRD ORDER HEAT RATE CURVE FIT FOR STEAM TURBINE (DIMENSIONLESS)

LOGICAL FIRST, FXTMP

COMMON

\$ AFTR, ALPHA
 \$ CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAP
 \$ CBU, CSEALP, CELAST, CFS, COANG, CLUVR, CHAITS, CVM
 \$ DEEPL, DESVEL, DANGLE
 \$ EFFP
 \$ FOR, FIRST, FIXL, FCOS, FXTMP
 \$ GREFF
 \$ HXNP, HPCST
 \$ IHEAT
 \$ ITMAX, ITMIN
 \$ JCONS
 \$ KCONV, KALEXT
 \$ MXEXT
 \$ NTUCAL(2), NTA
 COMMON
 \$ ODR
 \$ PSIZE, PER, PWCOS, PLANC, PFACT
 \$ POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSC1
 \$ QRED, QREDUCE
 \$ RBP, REDUCE, ROESEL, ROEELA, ROOFL, RFX
 \$ SAAF, SIGMA, SPAMAT(2)
 \$ TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX
 \$ TJRANG, TW
 \$ UCS, UWS
 \$ VAS(5)
 \$ WFM
 \$ XDPA, XW, XD
 COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
 \$ CLAND, REAIR, Z, HRFAC2, W4, U, PRO, W
 \$ FROW, DELFC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4
 \$ REWAT, NW, PLANC2, PSIZ12, SPBP, SW4, SW3

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60      $      SPC,PTOTAL,PLANC3,SAFRON, AAIR, YFP, SPCN,PSIZ13, WT2,
      $      BP2, NW2, TCOS, DELPA,DELPWT,DELPWC,CONBAS, XNTSX, VEL5X
      $      TLAX, UCON, FMCS, FBACC, EFFC, CH, CA, CS
      $      CLYC, CFC, CPCC, FITCO, CSC,CEPREP,DELPID, AST
      $      CAPCS, XNFAN,BLDANG, CPLEN, DPFEI, WHX, WTTUR, ADIA, ABLN
      $      WTHAR, WTERF,STRUC,CEPPEF,HPPEF, TOTCF, EFFIN, ANTU
65      $      ATREF, WATFE, XNMOD, TCTPF, FDCPF, FMTRC, ACCTP, ADJTP
      $      ACTRD, ADJBP, ACTVH, ADJVH, ADJPP, THPAIR, TCTF, AFCST
      $      CSO, WATERW, WSTRCT, CFOUND, HUBDIA, TOWLEN, CSE, CHF
      $      CRA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRN, CFANEL
      $      COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
70      $      CLAN1, REAI1, Z1,HRFA2S, W41, U1, PPOW1,
      $      FPOW1, DEFC1, WIDT1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,
      $      REW1, NW1,ZPLNC2,ZSIZ12, ZSPBP, SW41, SW31,
      $      SPC1, PTOT1,PLNC31, AFRO1, AAIR1,YFPMIN, SPCD1, SPS13,WT2MIN,
      $      BP2MIN,NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1,CONBA1, XNTS1, VELO1
75      $      TL1, UCON1, FMCS1, FBAC1, EFFC1, CH1, CA1, CS1
      $      CLT1, CFC1, CPCC1,FITC1, CSC1,CEPRE1,DEPIP1, AST1
      $      CAPCS1,XNFAN1,BLDAN1,CPLEN1,DPFEI1, WH1, WTTU1, ADI1, ABL1
      $      WTH1, WTER1,STRUC1,CEPPE1,HPPE1,TOTCF1,EFFIN1, ANTU1
      $      ATREF1, WATFE1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACCTP1, ADJTP1
80      $      ACTRD1, ADJBP1, ACTVH1, ADJVH1, ADJPP1, THPAI1, TCTF1, AFCST1
      $      CS1, WATER1, WSTRCT1, CFOUND1, HUBDI1, TOWLE1, CSE1, CHF1
      $      CRA1, NUMTOW1, CTOWD1, ATUBC1, CSTLVI, CSTHS1, CYLRN1, CFANEL
      $      COMMON /SCALR/ HRFAC1, SSCD, PLANC1, CASSS1,
      $      GAIR, FAIR, HPAIR, HPWAT, PLANCT1

85      C      EQUATION FOR HEAT RATE FACTOR AS A FUNCTION OF TURBINE
      C      BACK PRESSURE
      C
      C      HRF(P)=TPO(1) + TPO(2)*P + TPO(3)*P**2 + TPO(4)*P**3
90      C
      C      HEAT RATE FACTOR AT RATED BACK PRESSURE
      C
      C      HRFAC1=HRF(RBP)
      C
      C      INCREMENTAL STEAM SUPPLY COST DUE TO INCREASED HEAT RATE
95      C      FACTOR AT RATED BACK PRESSURE ($)
      C
      C      CASSS1=CSSPKW*(HRFAC1-1.)*PSIZE*1000.
      C
      C      PLANT COST TAKING INTO ACCOUNT INCREASED STEAM SUPPLY
100     C      COST ($/MW)
      C
      C      PLANOTE=PLANC1*PSIZE*1000. + CASSS1
      C      PLANC1=PLANCT1/(PSIZE*1000.)
105     C
      C      INCREMENTAL STEAM SUPPLY COST DUE TO INCREASED HEAT RATE
      C      OF TURBINE ($)
      C
110     C      SSCD=(PLANC1-PLANC)*1000.*PSIZE
      C      RETURN
      C      END

```

SUBROUTINE STORE

C
C
C
5
C

THIS ROUTINE IS CALLED EACH TIME A NEW LOW COST IS FOUND.
IT STORES VALUES OF COST, DESIGN, ETC. FOR THE FINAL REPORT

10

COMMON /RPRT1/ R1(2038)
COMMON /RPRT2/ R2(12)
COMMON /RPRT3/ R3(4)
COMMON /KPRT1/ SPRT1(2038)
COMMON /KPRT2/ SPRT2(12)
COMMON /KPRT3/ SPRT3(4)
COMMON /SINK/ VSTO(116)
COMMON /SUPPLY/ VIN(116)
LOGICAL FIRST, FXTMP

15

COMMON
\$ AFTR, ALPHA
\$,CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAPF
\$,CBU, CSEALP, CELAST, CFS, COANG, CLUVR, CHAELS, CVM
\$,DEEPL, DESVEL, DANGLE
20 \$,EFPF
\$,FCR, FIRST, FIXL, FCOS, FXTMP
\$,GREFF
\$,HXNP, HPCST
\$,IHEAT
25 \$,ITMAX, ITMIN
\$,JCONS
\$,KCONV, KALEXT
\$,MXEXT
\$,NTUCAL(2), NTA
30 COMMON

30

\$ ODR
\$,PSIZE, PER, PWCOS, PLANC, PFACT
\$,POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCU
35 \$,OREJ, GREUCE
\$,RAP, REDUCE, ROESL, ROELA, ROOFL, RFX
\$,SAAF, SIGMA, SPANAT(2)
\$,TD, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFX
\$,TJBAR, TW

35

\$,UCS, UWS
40 \$,VAS(5)
\$,WFW
\$,XDEPA, XW, XD
DO 1 I=1,116
VSTO(I)=VIN(I)

40

45

1 CONTINUE
DO 2 I=1,2038
SPRT1(I)=R1(I)

50

2 CONTINUE
DO 3 I=1,12
SPRT2(I)=R2(I)

3 CONTINUE
DO 4 I=1,4
SPRT3(I)=R3(I)

55

4 CONTINUE
JCONS=1
RETURN
END

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SUBROUTINE SUMCOS(FCR,PSIZE,CAPF,CCOS1,CPIP1,CONBA1,ATUHC,CPLEN,
$FBACC,FMCST,STRUCC,CFOUND,CAPCST,SPCD1,SSCD,HRFAC1,HRFAC2,YFP,
$PLANC,CLAN1,CLSUM,FCSUM,COSM1,CSTLV1,CSTHS1,CFANE1,CYLRN1
$ )

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C
C
C

THIS ROUTINE REPORTS THE FINAL COST SUMMARY

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6001 FORMAT(1H1///,T17,"C A P I T A L   C O S T   S U M M A R Y "
$ ,T72,"U N I T   E N E R G Y   C O S T   S U M M A R Y"/
$ ,T15,43(" "),T71,52(" ")///)
6010 FORMAT(
  L T2,"COOLING SYSTEM CAPITAL",T48,F13.0
  R,T69,"COOLING SYSTEM CAPITAL",T119,G12.6/)
6020 FORMAT(
  L T4,"TOWER",T35,F13.0
  R,T72,"TOWER",T106,G12.6)
6030 FORMAT(
  L T7,"HEAT EXCHANGER",T23,F13.0
  R,T75,"HEAT EXCHANGER",T93,G12.6)
6040 FORMAT(
  L T7,"PIENUM",T23,F13.0
  R,T75,"PIENUM",T93,G12.6)
6042 FORMAT(
  L T7,"LOUVERS",T23,F13.0
  R,T75,"LOUVERS",T93,G12.6)
6044 FORMAT(
  L T7,"HAIL SCREENS",T23,F13.0
  R,T75,"HAIL SCREENS",T93,G12.6)
6050 FORMAT(
  L T7,"FAN SYSTEM",T23,F13.0
  R,T75,"FAN SYSTEM",T93,G12.6)
6060 FORMAT(
  L T7,"STRUCTURE",T23,F13.0
  R,T75,"STRUCTURE",T93,G12.6)
6070 FORMAT(
  L T7,"FOUNDATION",T23,F13.0
  R,T75,"FOUNDATION",T93,G12.6)
6080 FORMAT(
  L T4,"PIPING",T35,F13.0
  R,T72,"PIPING",T106,G12.6)
6090 FORMAT(
  L T4,"CONDENSER",T35,F13.0
  R,T72,"CONDENSER",T106,G12.6)
6100 FORMAT(
  L T2,"CAPACITY PENALTY",T48,F13.0
  R,T69,"CAPACITY PENALTY",T119,G12.6)
6110 FORMAT(
  L T2,"PLANT SCALING",T48,F13.0
  R,T69,"PLANT SCALING",T119,G12.6)
6120 FORMAT(
  L T4,"STEAM SUPPLY",T35,F13.0
  R,T72,"STEAM SUPPLY",T106,G12.6)
6130 FORMAT(
  L T4,"BASE PLANT",T35,F13.0
  R,T72,"BASE PLANT",T106,G12.6)
6140 FORMAT(
  L T2,"LAND",T48,F13.0)

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```

6150 FORMAT(
      L T48,13("=")/)
60 6160 FORMAT(
      L T2,"TOTAL CAPITAL COST",T46,"$",T48,F13.0
      R T69,"TOTAL CAPITAL COST",T119,G12.6/)
6170 FORMAT(
      R T69,"ENERGY PENALTY",T119,G12.6/)
65 6180 FORMAT(
      R T69,"ADDITIONAL BASE PLANT FUEL",T119,G12.6/)
6190 FORMAT(
      R T69,"OPERATION AND MAINTENANCE",T119,G12.6/)
70 6200 FORMAT(
      R,T72,"TOTAL",T119,G12.6)
      YFPP1 = YFP * 1.
      FACTOR= FCR/(PSIZE*CAPF*9760)
      WRITE(A,6001)
      WRITE(A,6010) ((CCOS1+CPIP1+CONBA1),((CCOS1+CPIP1+CONBA1)*FACTOR))
75 80 85 90 95 100
      WRITE(A,6020) CCOS1,CCOS1*FACTOR
      WRITE(A,6030) ATUBC,ATUBC*FACTOR
      WRITE(A,6040) CPLEN,CPLEN*FACTOR
      WRITE(A,6042) CSTLV1,CSTLV1*FACTOR
      WRITE(A,6044) CTHS1,CTHS1*FACTOR
      WRITE(A,6050) (FBACC + FMCST + CYLRN1 + CFANE1)
      $ , (FBACC + FMCST + CYLRN1 + CFANE1) * FACTOR
      WRITE(A,6060) STRUCC,STRUCC*FACTOR
      WRITE(A,6070) CFOUNO,CFOUNO*FACTOR
      WRITE(A,6080) CPIP1,CPIP1*FACTOR
      WRITE(A,6090) CONBA1,CONBA1*FACTOR
      WRITE(A,6100) CAPCST,CAPCST*FACTOR
      WRITE(A,6110) SPCD1,SPCD1*FACTOR
      WRITE(A,6120) SSCD*HRFAC2/HRFAC1*YFPP1,SSCD*HRFAC2/HRFAC1*YFPP1*
      $FACTOR
90 95 100
      WRITE(A,6130) PLANC*(HRFAC2/HRFAC1*YFPP1-1.)*10.**3 * PSIZE,
      $ PLANC*(HRFAC2/HRFAC1*YFPP1-1.)*10.**3 * PSIZE* FACTOR
      WRITE(A,6140) CLAN1
      WRITE(A,6150)
      WRITE(A,6160) CLAN1+SPCD1+CAPCST+CCOS1+CPIP1+CONBA1
      $,(CLAN1+SPCD1+CAPCST+CCOS1+CPIP1+CONBA1)*FACTOR
      WRITE(A,6170) CLSUM
      WRITE(A,6180) FCSUM
      WRITE(A,6190) COSM1
      TOTAL = (CLAN1 + SPCD1 + CAPCST + CCOS1 + CPIP1 + CONBA1) *
      $ FACTOR + CLSUM + FCSUM + COSM1
      WRITE(A,6200) TOTAL
      END

```


SUBROUTINE STRUCT(DTOW, WHX, WATERW, ROOFL, CSTRUC, CFND, WSTRC,
S ITOWN, ELENG, POHSTC)

```

C
C
5  C      SUBROUTINE STRUCT DETERMINES THE COST OF THE STRUCTURES
C      AND THE FOUNDATION FOR THE CIRCULAR TOWERS . THE STRUCTURE
C      COST IS BASED ON THE HEIGHT AND DIAMETER OF EACH TOWER AND
C      THE DESIGN ROOF LOAD. THE FOUNDATION COST IS BASED ON THE
C      TOTAL WEIGHT OF THE HEAT EXCHANGERS AND THE SURFACE AREA
C      COVERED BY THE TOWERS.
10 C
C      DEFINITION OF VARIABLES
C
C      CFND      - COST OF FOUNDATION ($)
C      CSTRUC    - COST OF STRUCTURES ($)
15 C      DTOW     - TOWER DIAMETER (FT)
C      ITOWN     - NUMBER OF CIRCULAR TOWERS (DIMENSIONLESS)
C      ITOWN     - NUMBER OF CIRCULAR TOWERS (DIMENSIONLESS)
C      POHSTC    - DIRECT AND INDIRECT CONSTRUCTION COSTS FOR THE
C                  STRUCTURES (DECIMAL PERCENT)
20 C      ROOFL    - DESIGN ROOF LOAD (LBF/SQ FT)
C      WATERW    - WEIGHT OF THE WATER IN THE HEAT EXCHANGER (LBF)
C      WHX       - WEIGHT OF MATERIAL IN THE HEAT EXCHANGER (LBF)
C      WSTRC     - CIRCULAR TOWERS STRUCTURAL WEIGHT (LBF)
C
25 C      DATA PI /3.14156265/
C
C      STRUCTURAL COSTS
C
30 C      CSTRUC = ELENG * .2458 * PI/4 * DTOW**2 * ITOWN *
C      $ (.00645 * ROOFL + .726)
C
C      FOUNDATION COSTS
C
35 C      CFND = .019 * (WHX + WATERW) * .82 * PI/4 * DTOW**2 * ITOWN
C
C      STRUCTURAL WEIGHT OF COOLING TOWERS BASED ON $0.63/LB
C
C      WSTRC = CSTRUC / .63
C
40 C      STRUCTURAL COST TAKING INTO ACCOUNT DIRECT AND INDIRECT
C      CONSTRUCTION COSTS.
C
C      CSTRUC = CSTRUC * POHSTC
C      RETURN
45 C      END

```

SUBROUTINE SURCON (ISUR, KGA, LD, TLA, XNTS, ARPS, XNS, CONCST
 ,CONMAT, POHCND)

PROGRAM SURCON DETERMINES THE CAPITAL COST OF A SINGLE
 PRESSURE OR SERIES-CONNECTED SURFACE CONDENSER. REFERENCE:
 "SURFACE CONDENSERS FOR LAND INSTALLATION", FORM PL1312,
 WESTINGHOUSE ELECTRIC CORPORATION, 26 NOVEMBER 1968
 UPDATED ON FEBRUARY 12, 1976 TO CURRENT PRICES

DEFINITION OF VARIABLES

ACCF - ACCESSORY COST CORRECTION FACTOR FOR THE CONDENSER
 ADDER - INCREASES COST OF TUBING MATERIAL
 ARPS - AREA PER SHELL OF THE CONDENSER (SQ FT)
 AUXCST - AUXILIARY COST (\$)
 CFAC - LENGTH CORRECTION FACTOR (DIMENSIONLESS)
 CONCST - CONDENSER COST (\$)
 CONMAT - VARIABLE FOR CONDENSER MATERIAL (DIMENSIONLESS)
 DSCT - QUANTITY DISCOUNT FOR TUBES (DIMENSIONLESS)
 ERTCST - ERECTION COST (\$/SQ FT)
 F - TUBING LENGTH PENALTY (DIMENSIONLESS)
 FETCST - FIELD ERECTION COST (\$/SQ FT)
 FOD - TUBE SIZE FACTOR (DIMENSIONLESS)
 POHCND - INDIRECT COST FACTOR FOR THE TUBE, SHELL, AND
 FIELD ERECTION COSTS (DIMENSIONLESS)
 SHLCST - SHELL COST FOR THE CONDENSER (\$)
 TOSTPF - TOTAL COST OF TUBING MATERIAL (\$/FT)
 WT - WEIGHT OF TOTAL AMOUNT OF TUBES IN THE CONDENSER
 (LBF)
 XNS - NUMBER OF SHELLS IN THE CONDENSER (DIMENSIONLESS)
 XNTS - NUMBER OF TUBES PER SHELL (DIMENSIONLESS)

DEFINITION OF ARRAYS

TUBMA - TUBE MATERIAL (NAMES)
 CL - TUBE FIXED COSTS (\$)
 CLM - TUBE MATERIAL COSTS (\$/LBM)
 ROEL - DENSITY OF TUBE MATERIALS (LBM/CU IN)
 GAGLI - TUBE GAGE (DIMENSIONLESS)
 THKLIN - THICKNESS OF TUBE (IN)
 ODLINE - COMMON DIAMETERS OF TUBES (IN)

LOGICAL FIRST
 DIMENSION SCC1(6), SCC2(6)
 DIMENSION TUBMA(10), CL(10), CLM(10), ROEL(10), GAGLI(7),
 THKLIN(7), ODLINE(6), FF(10,7)
 COMMON /RPRT3/ TUBCST,SHLCST,FETCST,CONBA7

TUBING MATERIALS, COSTS, AND DENSITY

DATA CL / 0.00, 0.00, 0.00, 0.09, 0.04, 0.39, 0.12, 0.20, 0.15,
 * 0.10 /
 DATA CLM / 1.30, 1.52, 1.83, 1.40, 1.36, 0.44, 0.32, 1.63, 7.60,
 * 7.00 /
 DATA ROEL / 0.309, 0.323, 0.323, 0.0975, .0975, 0.284, 0.284, .290
 \$,0.163, 0.163 /
 DATA TUBMA / "ADMIRALTY ", "CU-10 NI ", "CU-30 NI ",

```

      *          "6061-T5 AL", "3003-H14 AL", "STEEL SEAM",
      *          "STEEL WELD", "304 S/S WE", "TITANIUM 1",
      *          "TITANIUM 2" /
60      C
      C          STANDARD TUBE DIAMETERS, GAGE, AND THICKNESSES
      C
      DATA ONLINE / 0.625, 0.750, 0.875, 1.000, 1.125, 1.250 /
65      DATA GAGLI / 12., 14., 16., 18., 20., 22., 24. /
      DATA THKLIN / .109, .083, .065, .049, .035, .028, .021 /

      C
      C          TUBING LENGTH PENALTIES
      C
70      C          FOR COPPER ALLOYS
      DATA (FF(1,J),J=1,7) / 0.00, 0.00, 0.00, 0.00, 0.07, 0.08, 0.09 /
      DATA (FF(2,J),J=1,7) / 0.00, 0.00, 0.00, 0.00, 0.07, 0.08, 0.09 /
      DATA (FF(3,J),J=1,7) / 0.00, 0.00, 0.00, 0.00, 0.07, 0.08, 0.09 /

      C
      C          FOR ALUMINUM
75      DATA (FF(4,J),J=1,7) / 1.00, 1.00, 1.06, 1.10, 1.14, 1.18, 1.22 /
      DATA (FF(5,J),J=1,7) / 1.00, 1.00, 1.06, 1.10, 1.14, 1.18, 1.22 /

      C
      C          FOR STEEL
80      DATA (FF(6,J),J=1,7) / 1.00, 1.00, 1.09, 1.13, 1.17, 1.21, 1.25 /
      DATA (FF(7,J),J=1,7) / 1.00, 1.00, 1.09, 1.13, 1.17, 1.21, 1.25 /

      C
      C          FOR STAINLESS STEEL
85      DATA (FF(8,J),J=1,7) / 1.00, 1.00, 1.00, 1.04, 1.08, 1.12, 1.16 /

      C
      C          FOR TITANIUM
      DATA (FF(9,J),J=1,7) / 0.00, 0.00, 0.00, 1.05, 1.05, 1.10, 1.10 /
      DATA (FF(10,J),J=1,7) / 0.00, 0.00, 0.00, 1.05, 1.05, 1.10, 1.10 /

90      C
      C          CONSTANTS FOR COST EQUATION FOR BASIC CONDENSER SHELL AS A
      C          FUNCTION OF TUBE O.D. (UPDATED FEBRUARY, 1975)
      C
      DATA SCC1 / 0.00000, 7.69583, 8.805882, 10.83636, 12.954545,
      *          15.22326 /
95      DATA SCC2 / 00000.00, 97125.00, 102154.71, 102191.92, 103272.73,
      *          102237.21 /

      C
      C          COST OF FIELD ERECTION AND TUBING PER SQUARE FOOT OF
      C          SURFACE AREA IS BASED UPON INFORMATION SUPPLIED BY
100      C          WESTINGHOUSE COMPANY AND AVERAGE WAGE LABOR RATES OBTAINED
      C          FROM JUNE 1975 CONSTRUCTION REVIEW

      DATA EPTCST / 2.50 /

105      C
      DATA FIRST/.TRUE./

      C
      C          DEFINING THE CASE UNDER CONSIDERATION
      C
110      IF(.NOT.FIRST) GOTO 35
      LFLAG=0
      DO 10 I = 1, 10
      ITUBA = I
      IF(CONVAT.EQ. TUBA(I)) GO TO 35
10      CONTINUE

```

```

115      WRITE(6,11)
          LFLAG=1
11      FORMAT(5X,"NO MATCH FOR CONDENSER TUBE MATERIAL")
          IF(LFLAG.NE.0) STOP
55      CONTINUE
120      FIRST = .FALSE.

C
C
C      DETERMINE TOTAL LENGTH OF TUBING REQUIRED AND CORRESPONDING
C      QUANTITY DISCOUNT
125      TOTLT=TLA*XNTS*XNS
C
          IF(TOTLT-50000.)102,101,101
101      DSCT=.04
          GO TO 103
130      102 IF(TOTLT-30000.)105,104,104
104      DSCT=.02
          GO TO 103
135      105 DSCT=.
103      KK = 7
          DO 106 I = 2, 8
          IF(TLA .GE. (10.0*I)) KK = I - 2
106      CONTINUE
          F = FF(ITUBMA,KK)
          ADDER = 0.00
          IF(ITUBMA .LT. 4) ADDER = F
          IF(ITUBMA .LT. 4) F = 1.00

C
C      DETERMINE TOTAL COST OF TUBING MATERIAL
145      109 WT = 12. * 3.14159 * ROEL(ITUBMA) * (ODLINE(LD)-THKLIN(KGA))
          S * THKLIN(KGA)
          TCSTPF = CLM(ITUBMA)*WT + CL(ITUBMA)
          TCSTPF = TCSTPF*F + ADDER
150      C
C      TUBE COST ARE F.O.B. COSTS, 1.11 ACCOUNTS FOR PURCHASING
C      AND SHIPPING
          TURCST = TOTLT * TCSTPF * (1.11-DSCT)
155      TURCST = TURCST * POHCND
C
C      DETERMINE SHELL COST INCLUDING LENGTH, MULTIPRESSURE, AND
C      ACCESSORY COST CORRECTIONS, AS APPROPRIATE
160      CFAC = 0.016*TLA + 0.58
          GO TO(100,111,112,113),ISUR
111      CFAC=CFAC+0.08
          GO TO 100
112      CFAC=CFAC+0.16
          GO TO 100
165      113 CFAC=CFAC+0.03*XNS*0.02
C
100      FOD = 1.00
          IF(LD .LT. 4) FOD = 0.95
          IF(LD .EQ. 6) FOD = 1.05
          ACCFI = (0.116*ALOG(XNTS) - 0.495)*FOD
170

```

SUBROUTINE SURCON

74/74 OPT=1

FTN 4.2+74351

12/20/66

```

      IF(ITURMA .EQ. 2) ACCF = (0.239*ALOG(XNTS) - 1.416)*FOD
175      THE CONDENSER SHELL COSTS WERE OBTAINED FROM WESTINGHOUSE'S
      1973 PRICE LISTING 1312
      AUXCST = 0.45*ARPS*XNS
      BSHCST = (SCC1(LD)*XNTS + SCC2(LD))
180      SHLCST=BSHCST*(CFAC+ACCF)*XNS + AUXCST
      SHLCST = SHLCST * POHCND
      C
      C
      C      DETERMINE COST OF FIELD ERECTION AND TUBING
      FETCST=ERICST*ARPS*XNS
185      FETCST = FETCST * POHCND
      C
      C
      C      DETERMINE TOTAL COST OF CONDENSER
190      CONCST=TURCST+SHLCST+FETCST
      CONB47=CONCST
      C
      RETURN
      END
```

FUNCTION TLU(X,XT,YT,NT)

FUNCTION TLU IS A FOUR-POINT LAGRANGIAN INTERPOLATION
TABLE LOOK-UP ROUTINE

DEFINITION OF VARIABLES

NT - NUMBER OF DATA POINTS
TLA - DEPENDENT VARIABLE
X - INDEPENDENT VARIABLE
XT - INDEPENDENT VARIABLE ARRAY
YT - DEPENDENT VARIABLE ARRAY

DIMENSION XT(NT),YT(NT)

DETERMINE IF INDEPENDENT VARIABLE IS WITHIN RANGE OF
TABULATED DATA

IF((X-XT(1))*(X-XT(NT)))100,100,101

DETERMINE IF TABULATED VALUES OF INDEPENDENT VARIABLE ARE
IN ASCENDING OR DESCENDING ORDER

100 IF(XT(1)-XT(2))102,102,103

DETERMINE POSITION OF INDEPENDENT VARIABLE IN ASCENDING
ARRAY

102 DO 99 I=1,NT
IF(X-XT(I))105,104,99
99 CONTINUE

DETERMINE POSITION OF INDEPENDENT VARIABLE IN DESCENDING
ARRAY

103 DO 98 I=1,NT
IF(X-XT(I))98,104,105
98 CONTINUE

IF INDEPENDENT VARIABLE IS EQUAL TO TABULATED VALUE, SET
FUNCTION EQUAL TO CORRESPONDING VALUE OF DEPENDENT VARIABLE

104 TLU=YT(I)

RETURN

IF INDEPENDENT VARIABLE IS BETWEEN FIRST TWO OR LAST TWO
TABULATED VALUES, ADJUST INDEX TO OBTAIN FOUR POINTS FOR
INTERPOLATION

105 IF(I=2)106,106,107
106 I=I+1
GO TO 103
107 IF(I=NT)108,109,109
109 I=I-1

DETERMINE FUNCTION VALUE USING FOUR-POINT LAGRANGIAN

```

      C      INTERPOLATION
      C
60      108  X1=XT(I-2)
          X2=XT(I-1)
          X3=XT(I)
          X4=XT(I+1)
      C
65      TLJ=(X-X2)*(X-X3)*(X-X4)/((X1-X2)*(X1-X3)*(X1-X4))*YT(I-2)
          S  + (X-X1)*(X-X3)*(X-X4)/((X2-X1)*(X2-X3)*(X2-X4))*YT(I-1)
          S  + (X-X1)*(X-X2)*(X-X4)/((X3-X1)*(X3-X2)*(X3-X4))*YT(I)
          S  + (X-X1)*(X-X2)*(X-X3)/((X4-X1)*(X4-X2)*(X4-X3))*YT(I+1)
      C
70      RETURN
      C
      101  WRITE(6,1000)X,XT(1),YT(1)
      1000  FORMAT(1H1,39H TABLE LOOK-UP: X NOT IN RANGE OF TABLE//
          S   5X,3HX =,F15.5,5X,7HXT(1) =,F15.5,5X,7HYT(1) =,F15.5)
75      C
          STOP
          END

```

SUBROUTINE VARIT(TA, TPER, PCST, KALL, CLSUM, FCSUM)

SUBROUTINE VARIT CALCULATES THE PERFORMANCE OF THE POWER PLANT AND DRY COOLING TOWER UNDER THE ASSUMPTION THAT THE AIR SIDE HEAT TRANSFER COEFFICIENTS AND AIR VELOCITY THROUGH THE HEAT EXCHANGER TUBES ARE UNCHANGED. THIS IS DONE FOR THE CASE HAVING THE MINIMUM INCREMENTAL COST.

DEFINITION OF VARIABLES

CAPCHG - GAS TURBINE CAPITAL COST (\$/MW)
 CAPCST - COST OF GAS TURBINE (\$)
 CAPF - PERCENTAGE OF TIME THE PLANT IS PRODUCING POWER (PERCENT)
 CCOS1 - COST OF THE DRY COOLING TOWERS (\$)
 CLAN1 - COST OF LAND TAKEN UP BY THE DRY COOLING TOWERS (\$)
 CONBA1 - COST OF SURFACE CONDENSER (\$)
 COSM1 - COST OF MAINTAINING THE DRY COOLING TOWER (\$)
 CRIP1 - COST OF PIPING AND PUMPING SYSTEMS (\$)
 CSTCL - COST OF MAKE-UP TOWER BY GAS TURBINES AT EACH AMBIENT AIR TEMPERATURE (MILLS/KW-HR)
 DELFC - INCREMENTAL FUEL COST FOR STEAM SUPPLY SYSTEM (MILLS/KW-HR)
 EFF1 - HEAT EXCHANGER EFFECTIVENESS OF DRY COOLING TOWERS (DIMENSIONLESS)
 EFFC1 - CONDENSER EFFECTIVENESS
 FCOS - FUEL COST FOR THE STEAM SUPPLY SYSTEM (MILLS/BTU)
 FAR - FIXED CHARGE RATE ON CAPITAL PER YEAR (PERCENT)
 FPOW1 - POWER REQUIREMENTS OF FAN SYSTEM (KW)
 HRFAC1 - HEAT RATE FACTOR OF STEAM TURBINE AT RATED BACK PRESSURE (DIMENSIONLESS)
 HRFAC2S - HEAT RATE FACTOR OF STEAM TURBINE AT DESIGN CONDITIONS OF POWER PLANT (DIMENSIONLESS)
 HRFAC4 - HEAT RATE FACTOR OF STEAM TURBINE AT A PARTICULAR AMBIENT AIR TEMPERATURE (DIMENSIONLESS)
 P - BACK PRESSURE OF STEAM TURBINE (IN. HG.)
 TCOS - INCREMENTAL POWER PRODUCTION COST OF THE DRY COOLED POWER PLANT FOR A PARTICULAR AMBIENT AIR TEMPERATURE (MILLS/KW-HR)
 PGEN - POWER OUTPUT OF PLANT AT A PARTICULAR AMBIENT AIR TEMPERATURE (MW)
 PPOW1 - POWER REQUIREMENTS OF THE PIPING SYSTEM (KW)
 SPS13 - POWER OUTPUT OF STEAM TURBINE AT RATED BACK PRESSURE TO PRODUCE REQUIRED OUTPUT OF PLANT OF PLANT AT DESIGN CONDITIONS (MW)
 PTOTAL - POWER OUTPUT OF PLANT AT SPECIFIED AMBIENT AIR TEMPERATURE (MW)
 PWCOS - COST OF FUEL FOR GAS TURBINE (MILLS/KW-HR)
 QTN1 - THERMAL ENERGY OUTPUT OF STEAM SUPPLY SYSTEM AT RATED BACK PRESSURE OF TURBINE (BTU/HR)
 QREJ - HEAT REJECTED AT A SPECIFIED AMBIENT AIR TEMPERATURE (BTU/HR)
 RANGE - TEMPERATURE RANGE OF WATER PASSING THROUGH THE HEAT EXCHANGER (DEG F)
 SPEC1 - INCREMENTAL COST OF PLANT DUE TO SCALE-UP OF STEAM SUPPLY SYSTEM AND THE SCALE UP OF THE PLANT TO TAKE INTO ACCOUNT FOR FAN AND PUMP POWER


```

C          REQUIREMENTS ($)
60  C      TA      - AMBIENT AIR TEMPERATURE (DEG F)
C      TEFF      - THERMAL EFFICIENCY OF CONVENTIONAL STEAM TURBINE
C                AT RATED BACK PRESSURE (DIMENSIONLESS)
C      TEFF1     - THERMAL EFFICIENCY OF STEAM TURBINE AT RATED
C                BACK PRESSURE (DIMENSIONLESS)
65  C      TEFF3   - THERMAL EFFICIENCY OF STEAM TURBINE AT POWER
C                PLANT DESIGN CONDITIONS (DIMENSIONLESS)
C      TEFF4     - THERMAL EFFICIENCY OF STEAM TURBINE ASSOCIATED
C                WITH A PARTICULAR AMBIENT AIR TEMPERATURE
C                (DIMENSIONLESS)
70  C      TPER    - PERCENT OF TIME AN AMBIENT TEMPERATURE OCCURS
C                DURING THE YEAR (PERCENT)
C      TPO       - COEFFICIENTS FOR THIRD ORDER CURVE FIT OF STEAM
C                TURBINE HEAT RATE FACTOR (DIMENSIONLESS)
C      TTDP      - TERMINAL TEMPERATURE DIFFERENCE OF SURFACE
C                CONDENSER FOR A PARTICULAR AMBIENT AIR TEMPERATURE
75  C      TTD     - TERMINAL TEMPERATURE DIFFERENCE OF SURFACE CONDENS-
C                ER AT DESIGN CONDITIONS (DEG F)
C      TI        - EXIT TEMPERATURE OF STEAM TURBINE (DEG F)
C      VCST      - TOTAL INCREMENTAL COST OF DRY COOLING (MILLS/KW-HR)
C      W2        - MASS FLOW RATE OF WATER THROUGH THE HEAT EXCHANGER
80  C                (LBM/HR)
C      PCST      - INCREMENTAL COST OF DRY COOLING FOR EACH AMBIENT
C                AIR TEMPERATURE (MILLS/KW-HR)
C      YEPMIN    - PLANT SCALING FACTOR TO TAKE INTO ACCOUNT FOR FAN
C                AND PUMP POWER (DIMENSIONLESS)
85  C
C      LOGICAL FIRST, FXTMP
C      COMMON
C      $ AFTR, ALPHA
C      $ ,CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAFI
90  C      $ ,CBU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILE, CVM
C      $ ,DESP, DESVEL, DANGLE
C      $ ,EFFP
C      $ ,FCR, FIRST, FIXL, FCOS, FXTMP
C      $ ,GREFF
95  C      $ ,HXNP, HPCST
C      $ ,IHEAT
C      $ ,ITMAX, ITMIN
C      $ ,JCONG
C      $ ,KCONV, KALEXT
100 C      $ ,MXEXT
C      $ ,NTUCAL(2), NTA
C      COMMON
C      $ OOR
C      $ ,PSIZE, PER, PWCOS, PLANC, PFACT
105 C      $ ,POHBAF, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSLC
C      $ ,PREJ, PREDUCE
C      $ ,RRP, REDUCE, ROESEL, ROELA, ROOFL, RFIX
C      $ ,SAAF, SIGMA, SPAMAT(2)
C      $ ,TD, TPO(4), TEFF, TLIM, TLRA, TSEALP, TELAST, THFIN, TFIX
110 C      $ ,TJBANG, TW
C      $ ,UCS, UWS
C      $ ,VAS(5)
C      $ ,W2V
C      $ ,XDEPA, XW, XD

```

```

115      COMMON /SCALER/ HRFAC1, SSCD, PLANC1, CASSS1,
          $ GAIR, FAIR, HPAIR, HPWAT, PLANC1
          COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
          $, CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,
120      $ FROM, DELFC, WIDTH, ELEN, VAIR, VWAT, HI, HO, T4,
          $ REWAT, NW, PLANC2, PSIZ12, SPAP, SW4, SW3,
          $ SPC, PTOT1, PLANC3, SAFR01, AAIR, YFP, SPCD, PSIZ13, WT2,
          $ BP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELOX
          $, TLAX, UCON, FMCS1, FBACC, EFFC, CH, CA, CS
          $, CLTC, CFC, CPCC, FITC, CSC, CEPREP, DEPIP, AST
125      $, CAPCS1, XNFAN1, BLDANG, CPLEN, DPPELL, WHX, WTTUB, ADIA, ABLN1
          $, WTHR, WTFRM, STRUCC, CFPERF, HPPERF, TOTCF, EFFIN, ANTU
          $, AIRFF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTTP, ADJTP
          $, ACTB01, ADJB01, ACTVH, ADJVH, ADJPP, THPA1, TCTF, AFCST
          $, CSP1, WATER1, WSTRC1, CFOUN1, HUBD1, TOWLE1, CSE, CHF
130      $, CB1, NUMTOW, CTOW1, ATUBC, CSTLVR, CSTHS, CYLRN1, CFANEL
          COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
          $, CLAN1, REA11, Z1, HRFAC2S, W41, U1, PPOW1,
          $ FROM1, DEFC1, WIDT1, ELEN1, VAIR1, VWAT1, HI1, HO1, T41,
          $ REW1, NW1, ZPLNC2, ZSIZ12, ZSP3P, SW41, SW31,
135      $ SPC1, PTOT1, PLNC31, AFRO1, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
          $ BP2MIN, NW2MIN, TCOS1, DEPA1, DPWT1, DPWC1, CONBA1, XNTS1, VELD1
          $, TL1, UCON1, FMCS1, FBAC1, EFFC1, CH1, CA1, CS1
          $, CLT1, CFC1, CPCC1, FITC1, CSC1, CEPRE1, DEPIP1, AST1
          $, CAPCS1, XNFAN1, BLDAN1, CPLEN1, DPPELL1, WH1, WTTU1, ADI1, ABL1
140      $, WTH1, WTFR1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
          $, AIRFF1, WATFF1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACCTP1, ADJTP1
          $, ACTB1, ADJB1, ACTVH1, ADJVH1, ADJPP1, THPA1, TCTF1, AFCST1
          $, CSP1, WATER1, WSTRC1, CFOUN1, HUBD1, TOWLE1, CSE1, CHF1
          $, CB1, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANEL
145      COMMON /TINE/ XNS, TTD, TLA, XNTS, ARPS

          C
          C      THERMAL EFFICIENCY OF TURBINE AT THE DESIGN POINT OF THE
          C      PLANT
          C
150      TEFF0=TEFF/HRFA2S

          C
          C      THERMAL EFFICIENCY OF TURBINE AT THE RATED BACK PRESSURE
          C
          C      TEFF1=TEFF/HRFAC1

155      C
          C      HEAT SUPPLIED BY THE STEAM SUPPLY SYSTEM
          C
          C      QIN1=3413.E+3 * SPS13/TEFF1
          C      T1=140.

160      C
          C      AMBIENT AIR TEMPERATURE AND PERCENTAGE OF YEAR OVER WHICH
          C      TEMPERATURE OCCURS.
          C
          C      1 P=EXP((7.158-9240.)/(T1+460.))
          C      HRFAC4=TPO(1)+TPO(2)*P+TPO(3)*P**2+TPO(4)*P**3
          C      TEFF4=TEFF/HRFAC4

165      C
          C      ITERATIVE LOOP FOR CALCULATING THE EXIT TEMPERATURE OF THE
          C      STEAM TURBINE AS A FUNCTION OF THE AMBIENT AIR TEMPERATURE.
          C
          C
170      C
          C      CALCULATION OF HEAT REJECTED BY THE DRY COOLING TOWERS

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      QREJ=QIN1*(1.-TEFF4)
      C
      C      TEMPERATURE RANGE OF WATER FLOWING THROUGH THE HEAT EXCHANGER
175  RANGE=QREJ/(W31*(1.+YFPMIN))
      C
      C      TEMPERAL TEMPERATURE DIFFERENCE BETWEEN THE WATER AND THE
      C      STEAM OF THE SURFACE CONDENSER
180  TTDP= RANGE/EFFC1- RANGE
      C
      C      EXIT TEMPERATURE OF THE STEAM TURBINE ON PREVIOUS EXTIMATE
      C      IF (VAP(3).ST.1.) GO TO 2
      C      T11 = RANGE/EFF1 + TA + TTDP
      C      GO TO 3
185  2 T11 = RANGE*VAR(3)/EFF1 + TA + TTDP
      C
      C      CONVERGENCE CRITERION FOR EXIT TEMPERATURE OF TURBINE
      C      3 IF (.NOT. FXTMP .AND. (T11-T1)**2 .LT. .001) GOTO 4
190  CVT = ABS( (T11-T1) / T11 )
      C      IF (FXTMP .AND. CVT .LT. 0.0001) GOTO 4
      C      T1=T11
      C      GO TO 1
      C
      C      TOTAL POWER OUTPUT OF TURBINE AT THE PARTICULAR AMBIENT
195  C      AIR TEMPERATURE
      C
      C      4 PTOTAL = QIN1*TEFF4/3413.*E+3
      C
      C      C      POWER OUTPUT FROM PLANT AT THE PARTICULAR AMBIENT AIR
200  C      TEMPERATURE
      C
      C      PGEN=PTOTAL-PPW1/1000. - FPOW1/1000.
      C      TEFFD=TEFF4
      C      IF (PGEN.GE.PSIZE) GOTO 5
205  C
      C      C      COST OF FUEL FOR GAS TURBINE MAKE UP POWER
      C
      C      CSTOL=(PSIZE-PGEN)/PSIZE*PWCOS
      C      TEFFD=TEFF3
210  C      GO TO 4
      C      5 CSTOL=0
      C
      C      C      INCREMENTAL COST OF FUEL FOR STEAM SUPPLY SYSTEM DUE TO STEAM
215  C      TURBINE OPERATING AT OFF DESIGN CONDITIONS
      C
      C      6 DELFC=FCOS*3413.*E-5*((1.+YFPMIN)/TEFFD-1./TEFF)
      C
      C      C      CAPITAL COST OF GAS TURBINE FOR MAKE UP POWER
220  C
      C      IF (KAIL.NE.1) GO TO 10
      C      CAPCST=0.0
      C      IF (PSIZE.LE.PGEN) GO TO 10
      C      CAPCST=CAPCHG*(PSIZE-PGEN)
225  10 CONTINUE
      C
      C      C      INCREMENTAL COST OF FUEL FOR STEAM SUPPLY SYSTEM DUE
      C      C      TO STEAM TURBINE OPERATING AT OFF DESIGN CONDITIONS (RATED

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230      C      BACK PRESSURE)
      C
      TCOS = (CCOS1+SPCD1+CLAN1+CPIP1+CONBA1+CAPCST)*FCR/(PSIZE+CAPP
      $ 8760.) + COSM1+DELFC+CSTCL
      PCST=TPER*TCOS
      CLSUM = CLSUM + CSTCL * TPER
235      FCSUM = FCSUM + DELFC * TPER
      935 FORMAT(T2,F6.1, T10,F6.1, T18,F5.2, T26,F7.4, T33,F7.3
      $,T41,F4.3, T47,F7.2, T54,F7.2, T62,F9.3, T72,F7.5, T81,G11.5
      $ T93,F7.4, T106,F7.3, T115,G11.5)
      2939 FORMAT(T2,"TAI,TAO,TWI,TWO,T11,RANGE,TTD",7G15.6)
240      800 CONTINUE

      C      TEMPERATURES OF FLUIDS ENTERING AND EXITING THE HEAT
      C      EXCHANGER
      C
245      C      TEMPERATURE OF AIR ENTERING THE HEAT EXCHANGER
      C      TAI = TA
      C
      C      TEMPERATURE OF AIR EXITING THE HEAT EXCHANGER
      C      TAO = TAI + VAR(3) * RANGE
250      C
      C      TEMPERATURE OF WATER EXITING THE HEAT EXCHANGER
      C      TWO = T11 - RANGE - TTD
      C
      C      TEMPERATURE OF WATER ENTERING THE HEAT EXCHANGER
255      C      TWI = RANGE + TWO
      C
      C      THE LOG MEAN TEMPERATURE DIFFERENCE OF THE FLUIDS IN THE
      C      HEAT EXCHANGER
      C
260      C      HXLMTD = 1.E+30
      C      TESTR = (TWI-TAO) / (TWO-TAI)
      C      IF(TESTR.GT. 0.0) GOTO 820
      C      WRITE(4,2939) TAI,TAO,TWI,TWO,T11,RANGE,TTD
      C      GOTO 830
265      820 IF (TESTR.EQ. 1.0) HXLMTD = TWI-TAO
      C      IF (TESTR.NE. 1.0) HXLMTD =
      C      $ ((TWI-TAO) - (TWO-TAI)) / ALOG( (TWI-TAO) / (TWO-TAI) )
      C      830 CONTINUE
270      C      INITIAL TEMPERATURE DIFFERENCE BETWEEN THE WATER AND AIR IN
      C      THE HEAT EXCHANGER
      C      HXITD = TWI - TAI
      C
      C      PRINTOUT OF HEAT EXCHANGER PERFORMANCE PARAMETERS
275      C      WRITE(4,935) TA
      C      $,T1
      C      $,P
      C      $,HPFAC4
      C      $,RANGE
280      C      $,TTDP
      C      $,HXLMTD
      C      $,HXITD
      C      $,PGEN
      C      $,DELFC
285      C      $,CSTCL

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SUBROUTINE VARIT 74/74 OPT=1

FTN 4.2.74351

12/20/76

S,TCOS
S,TPER = 100.
S,PCST
RETURN
END

290

SUBROUTINE XTEND(L)

THIS ROUTINE CHECKS EXTREME VALUES AT MINIMAL COST POINT.

```

5      DIMENSION TTRY(2),RTRY(2),CTRY(2),ATRY(2),WTRY(2)
      COMMON /SINK/ VAR(5), CPIP1, CCOS1, W31, COSM1, EFF1
      $, CLAN1, REA11, Z1, HRFAC2S, W41, U1, PPOW1,
      $ FPOW1, DELFC1, WIDTH1, ELENG1, VAIR1, VWAT1, HI1, HO1, T41,
10     $ REWAT1, NW1, PLANC2, PSIZ12, ZSP3P, SW41, SW31,
      $ SPC1, PTOT1, PLANC31, AFR01, AAIR1, YFPMIN, SPCD1, SPS13, WT2MIN,
      $ BP2MIN, NW2MIN, TCOS1, DELPA1, DPWT1, DPWC1, CONBAS1, XNTS1, VELD1
      $, TLAX1, UCON1, FMCST1, FBACC1, EFFC1, CH1, CA1, CS1
      $, CLTC1, CFC1, CPCC1, FITC1, CSC1, CEPREP1, DELPIP1, AST1
      $, CAPCS1, XNFAN1, BLDAN1, CPLEN1, DPFE1, WH1, WTTU1, ADIA1, ABL1
15     $, WTHD1, WTER1, STRUC1, CFMPF1, HPPF1, TOTCF1, EFFIN1, ANTU1
      $, AIREF1, WATFF1, XNMOD1, TCTPF1, FDCPF1, FMTRC1, ACCTP1, ADJTP1
      $, ACTBP1, ADJBP1, ACTVH1, ADJVH1, ADJPP1, THPA11, TCTF1, AFCST1
      $, CS1, WATER1, WSTRCT1, CFOUND1, HUBD11, TOWLE1, CSE1, CHF1
      $, CBA1, NUMTOW1, CTOWD1, ATUBC1, CSTLV1, CSTHS1, CYLRN1, CFANE1
20     COMMON /SUPPLY/ VAL(5), CPIP, CCOS, W3, COSM, EFF
      $, CLAND, REAIR, Z, HRFAC2, W4, U, PPOW,
      $ FPOW, DELFC, WIDTH, ELENG, VAIR, VWAT, HI, HO, T4,
      $ REWAT, NW, PLANC2, PSIZ12, SP3P, SW4, SW3,
      $ SPC, PTOTAL, PLANC3, SAFRON, AAIR, YFP, SPCD, PSIZ13, WT2,
25     $ BP2, NW2, TCOS, DELPA, DELPWT, DELPWC, CONBAS, XNTSX, VELDX
      $, TLAX, UCON, FMCST, FBACC, EFFC, CH, CA, CS
      $, CLTC, CFC, CPCC, FITC, CSC, CEPREP, DELPIP, AST
      $, CAPCST, XNFAN, BLDANG, CPLEN, DPFE1, WHX, WTTUB, ADIA, ABLN
30     $, WTHAR, WTERF, STRUC, CFPERF, HPPERF, TOTCF, EFFIN, ANTU
      $, AIREF, WATFF, XNMOD, TCTPF, FDCPF, FMTRC, ACCTP, ADJTP
      $, ACTBPD, ADJBPD, ACTVH, ADJVH, ADJPPF, THPAIR, TCTF, AFCST
      $, CS1, WATERW, WSTRCT, CFOUND, HUBDIA, TOWLEN, CSE, CHF
      $, CBA, NUMTOW, CTOWD, ATUBC, CSTLVR, CSTHS, CYLRNG, CFANEL
      LOGICAL FIRST, FXTMP
35     COMMON
      $ AFTR, ALPHA
      $, CAPF, CSSPKW, CONF, CONL, COSTL, CAPCHG, CONMAT, CONMA2, CAFI
      $, CBU, CSEALP, CELAST, CFS, CDANG, CLUVR, CHAILS, CVM
      $, DEEPL, DESVEL, DANGLE
40     $, EFFP
      $, FCR, FIRST, FIXL, FCOS, FXTMP1
      $, GBEFF
      $, HXNP, HPCST
      $, IHEAT
45     $, ITMAX, ITMIN
      $, JCONS
      $, KCONV, KALEXT
      $, MXEXT
      $, NTUCAL(2), NTA
50     COMMON
      $ OR1
      $, PSIZE, PER, PWCOS, PLANC, PFACT
      $, POHBAP, POHFAN, POHLEC, POHCIR, POHCND, POHSTC, POHSCL
      $, QREU, QREDUCE
55     $, R3P, REDUCE, ROESEL, ROEELA, ROOFL, RFIX
      $, SAAF, SIGMA, SPAMAT(2)
      $, TQ, TPO(4), TEFF, TLIM, TLPRA, TSEALP, TELAST, THFIN, TFIX

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```

      S ,TJBAEG, TW
      S ,UCS, UWS
60      S ,VAS(5)
      S ,WFEV
      S ,XDEPA, XW, XD
      COMMON /LACALL/ SRN
      COMMON /TINE/ XNS,TTD,TLA,XNTS,ARPS
85      TTRY(1)=VAR(1)-20.
      IF (TTRY(1) .LE. 0.0) TTRY(1)=10.
      TTRY(2)=VAR(1)+20.
      IF (EXTMP) TTRY(1) = TFIX
      IF (EXTMP) TTRY(2) = TFIX
70      CTRY(1)=VAR(3)-3.
      IF (CTRY(1) .LE. 0.) CTRY(1)=.5
      CTRY(2)=VAR(3)+2.
      ATRY(1)=VAR(4)+4.
      ATRY(2)=VAR(4)/4.
75      WTRY(1)=VAR(5)+40.
      WTRY(2)=VAR(5)/3.
      DO 3 I=1,2
      RANGL=(TTRY(I)-TTD-TD)*(1.-EXP(-VAR(3)))/VAR(3)
2      RTRY(1)=.9*RANGL
      RTRY(2)=.7*RANGL
80      IF (EXTMP) RTRY(1) = RFIX
      IF (EXTMP) RTRY(2) = RFIX
      SRN="/XTEND-1/"
      DO 3 IR=1,2
95      CALL CALC(TTRY(I),RTRY(IR),VAR(3),VAR(4),VAR(5),1)
      IF (CONV.EQ.1) GO TO 3
      IF (DEPA.LT.XDEPA) GO TO 3
      IF (DEPA.LE.XDEPA) GO TO 3
      IF (TCOS.GT..99*TCOS1) GO TO 3
90      TCOS1=TCOS
      VAS(1)=TTRY(I)
      VAS(3)=VAR(3)
      VAS(4)=VAR(4)
      VAS(5)=VAR(5)
85      L=1
3      CONTINUE
      DO 10 I=1,2
      RANGL=(VAR(1)-TTD-TD)*(1.-EXP(-CTRY(I)))/CTRY(I)
9      RTRY(1)=.9*RANGL
      RTRY(2)=.7*RANGL
100      IF (EXTMP) RTRY(1) = RFIX
      IF (EXTMP) RTRY(2) = RFIX
      SRN="/XTEND-3/"
      DO 10 IR=1,2
105      CALL CALC(VAR(1),RTRY(IR),CTRY(I),VAR(4),VAR(5),I)
      IF (CONV.EQ.1) GO TO 10
      IF (DEPA.LT.XDEPA) GO TO 10
      IF (DEPA.LE.XDEPA) GO TO 10
      IF (TCOS.GT..99*TCOS1) GO TO 10
110      TCOS1=TCOS
      VAS(1)=VAR(1)
      VAS(3)=CTRY(I)
      VAS(4)=VAR(4)
      VAS(5)=VAR(5)

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```

115      L=1
10      CONTINUE
        DO 11 I=1,2
          CALL CALC(VAR(1),VAR(2),VAR(3),ATRY(I),VAR(5),2+I)
          IF(XCONV.EQ.1) GO TO 11
120      C    IF(DELPA.LT.XDEPA) GO TO 11
          IF(DELPA.LE.XDEPA) GO TO 11
          IF(TCOS.GT..99*TCOS1) GO TO 11
          TCOS1=TCOS
          VAS(1)=VAR(1)
125      VAS(3)=VAR(3)
          VAS(4)=ATRY(I)
          VAS(5)=VAR(5)
          L=1
11      CONTINUE
130      SRN="/XTEND-4/"
        DO 12 I=1,2
          CALL CALC(VAR(1),VAR(2),VAR(3),VAR(4),WTRY(I),3+I)
          IF(XCONV.EQ.1) GO TO 12
135      C    IF(DELPA.LT.XDEPA) GO TO 12
          IF(DELPA.LE.XDEPA) GO TO 12
          IF(TCOS.GT..99*TCOS1) GO TO 12
          TCOS1=TCOS
          VAS(1)=VAR(1)
          VAS(3)=VAR(3)
140      VAS(4)=VAR(4)
          VAS(5)=WTRY(I)
          L=1
12      CONTINUE
13      IF(L.EQ.1) WRITE(6,13)
145      FORMAT(" XTEND CALLED, AND CHANGE MADE")
          IF (L .EQ. 1) KALEXT = KALEXT + 1
          IF (KALEXT .GT. MXEXT) STOP "CALLS TO S.R. XTEND EXCEED MXEXT"
          RETURN
        END

```