Partially-Saturated Transient Groundwater Flow Model Theory and Numerical Implementation

1975

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PARTIALLY-SATURATED TRANSIENT GROUNDWATER FLOW MODEL
THEORY AND NUMERICAL IMPLEMENTATION

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SUMMARY

This report describes the mathematical development of a computer model, the Partially-Saturated Transient Flow Model (PST), used to test the formulation for simulating isothermal, unsaturated, liquid flow in heterogeneous porous media. The fundamental equations and assumptions applying to the model are discussed. Problems encountered in modeling the flow in soils with water contents less than saturation are also delineated.

Because of the nonlinearities of the descriptive equations, finite difference approximation and an iterative technique were used to obtain solutions. The model, when tested, was computationally slow and impractical as a management tool but did demonstrate that the equation could be solved for flow entering relatively dry soils.

Several methods of dealing with the sediment hydraulic characteristics were tested.

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PARTIALLY-SATURATED TRANSIENT GROUNDWATER FLOW MODEL THEORY AND NUMERICAL IMPLEMENTATION

INTRODUCTION

At the Hanford Reservation, radioactive wastes are presently stored in the ground in unsaturated (or partially-saturated) sediments lying between 45 and 60 meters above the regional water table. Since many of the long-lived radiocontaminants are readily adsorbed on the sediments and since water movement at the moisture content found in the Hanford sediments is slow, this zone has been theoretically relied upon, in the event of a storage tank leak, as a safety factor to minimize possibility of radiocontaminants entering the water table. Thus, the ability to quantitatively calculate radiocontaminant movement in this zone is extremely important to waste management activities at Hanford.

An effort was initiated to quantitatively describe radiocontaminant movement in the vadose zone (the zone between the ground surface and the water table). To quantitatively describe radiocontaminant movement in the vadose zone, it is necessary to solve the equations for water movement and solute transport. If it is assumed that flow of water is independent of the water's chemical constituents (i.e., that the important forces governing fluid movement are physical), then the equations for fluid and mass flow can be solved sequentially rather than simultaneously, thus greatly reducing the problem of obtaining numerical solutions.

The PST Model was designed to predict the moisture movement in sediments as a function of time and space for the initial and boundary conditions, which are specified. Once a solution to the flow problem is obtained, a transport model can be used to combine the moisture movement rates with soil-waste reaction mechanisms to predict the time and spatial movement of important radiocontaminants. This report describes the theory and numerical implementation of the PST Model.

REVIEW OF LITERATURE

The infiltration of water through sediments is characteristically a two-phase flow problem, the water either replacing or being replaced by air. Since there is small resistance to flow of air, it is assumed that for isothermal conditions the problem can be reduced to the flow of the liquid phase; i.e., that of the water. Corey (1) suggested that air pressure in such a case is usually atmospheric.

These assumptions were used by Richards (2) in combining the equation of continuity and Darcy's Law to develop the generally accepted equation describing flow in a porous medium. This is a nonlinear parabolic partial differential equation in which the coefficients are a function of the dependent variable. Such equations are difficult to solve with the usual numerical techniques. One-dimensional numerical formulations of Richards' equation were reviewed by Freeze.(3) Recently, two-dimensional applications were published by Rubin,(4) Hornberger, et al., (5) Taylor and Luthin,(6) Cooley,(7) Verma and Brutsaert,(8) and Brutsaert.(9) Green and Weinaug (10) published a two-phase, two-dimensional solution but also encountered excessive computational times. Freeze(11) published a three-dimensional model that treated the entire (saturated-unsaturated transient) flow of a small geologic basin. With the exception of Freeze and Brutsaert, all of these authors used homogeneous soils. The sharp discontinuities arising from sudden application of water to relatively dry soils have not been treated.

RATIONALE OF MODEL DEVELOPMENT

The most general equations that describe liquid, vapor, heat and solute flow through unsaturated sediments are very complex. The equations for liquid and vapor movement (treated by Taylor and Cary, (12) Philip and DeVries, (13) and Letey (14) have not yet been solved for the general case.

In making simplifying assumptions, consideration should be given to the economic feasibility of solving the resultant equations, the cost of obtaining the necessary input data, and the status of the theory describing the effect. For instance, it is known that highly saline wastes can react with the sediments to change their hydraulic characteristics; however, the theory has not been developed to describe this reaction, as it must be before this effect is properly included in a model.

Because of the above mentioned considerations and the nonlinearities associated with solving even the simplified isothermal equations for waste storage tank leaks or pipeline ruptures in relatively dry heterogeneous sediments, it was decided that the first step in the development of the PST Model would be to solve the isothermal equations for the hydrogeologic and climatic conditions which prevail at the Hanford Reservation. The experience gained in solving these equations could contribute to better decisions about the feasibility and desirability of modeling other effects.

MODEL ASSUMPTIONS AND LIMITATIONS

The following assumptions, which are discussed below, were made for model development:

- 1) Darcy's law is generally accepted as valid for types of sediments and gradients that occur in the vadose zone of the Hanford Reservation. This is a generally accepted assumption used in development of equation of flow through porous media. In partially saturated flow the hydraulic conductivity is dependent upon the moisture content.
- 2) The pressure head is a unique function of the volumetric moisture content. This is to say that hysteresis is ignored. Richards (16) found that drainage was faster than wetting as the capillary pressure varied between the same values, which could be accounted for by hysteresis. For the same pressure variations, the difference in moisture contents were largest (up to 10 percent) for heavy clay soils, smallest for coarse sands (1 to 2 percent). Defining the hysteresis loops adequately presents an order of magnitude more difficult measurement problems and probably represent less error than that of using disturbed sediment samples for measuring hydraulic characteristics.
- 3) In addition, more recent work by Dane, (17) indicates that hysteresis is a second order effect when consideration is given to the accuracy with which the hydraulic conductivity can be established. The soil may be homogeneous or homogeneously layered. In the case of a two-dimensional problem the sediment layers can be either horizontal or tilted. In an axisymmetric problem the layers must be horizontal or they will appear conical in the three-dimensional view.

- 4) The pressure of the air is constant and uniform throughout the system and is used as the datum for measuring the pressure in the wetting phase. It is assumed there is no resistance to the flow of air in the system, therefore, only the wetting fluid needs to be modeled.
- 5) The soil medium is isotropic within the unit cell. Generally the Hanford sediments are isotropic; however, layering causes an apparent anisotropy.
- 6) The flow is isothermal. Moisture movement from waste discharges are not significantly affected by the normal earth thermal gradients. Therefore, the isothermal assumption will be valid for most applications. Thermally-induced liquid flow and vapor phase flow can arise from three sources: a) heat content of the waste; b) concentration of radiocontaminants on the sediments through sorption reactions and subsequent radiant heating of the liquid; and c) natural thermal gradients.

Some insight into the importance of the nonisothermal flow at low moisture content induced by natural geothermal gradients can be obtained by using techniques described in Appendix A. The equations therein are based on classical nonisothermal transport theory.

- 7) The hydraulic conductivity is a unique function of the moisture content.
- 8) Neglecting overburden is often considered an assumption in the basic equations; however, the effect of overburden is to modify the sediment matrix by increasing the bulk density which in turn changes the hydraulic characteristics of the sediments. Thus, overburden affects the input soil characteristics rather than the basic equations and can be approximately accounted for in measurement of the properties at the same bulk density as occurs in the field.
- 9) Barometric pressure changes are not accounted for. It is unlikely that liquid under leak conditions is moved by barometric changes.
- 10) The hydraulic characteristics of the sediments are not altered by the chemical composition of the waste. It has been observed that chemical wastes can react with the sediments and change their hydraulic characteristics, (15) but the specific reactions which occur and

their significance with respect to liquid and radio-contaminant movement are not known. The assumption that the hydraulic characteristics of the soil are not changed by chemicals in the waste allows the equations for fluid and mass flow to be solved sequentially, rather than simultaneously, which reduces the difficulty of obtaining numerical solutions. A significant development effort would be necessary to incorporate the effects of chemically-caused changes in hydraulic characteristics.

THEORETICAL ANALYSIS

A set of equations describing nonisothermal liquid, vapor, heat and solute flow in unsaturated sediments is presented in Appendix A. These equations incorporate the important effects which have been suggested in the literature and are presented to show the complexity of the general equations which would have to be solved if no simplifying assumptions were made. It is obvious that solving these equations for a realistically sized problem would be an impractical effort for the present state-of-the-art in numerical analysis and digital computers. The assumptions presented in the previous section were used to reduce these equations to those used in the PST Model. This development is also described in Appendix A.

The generalized equation describing isothermal, incompressible flow in porous media in two dimensions is:

$$\frac{\partial (K \frac{\partial \Phi}{\partial x})}{\partial x} + \frac{\partial (K \frac{\partial \Phi}{\partial z})}{\partial z} = \frac{\partial \theta}{\partial t} - q \quad (1)$$

where

$\Phi = \underline{P} + z$ = hydraulic potentials

θ = moisture content

K = hydraulic conductivity

x, z = spatial coordinates

t = time

q = source or sink term

When saturated flow exists or $\theta = \theta_s$, then

$$\frac{P}{\rho g} = P/\rho g$$

where

P = pressure

ρ = density of water

g = gravitational acceleration

In this case ϕ and K are functions only of the spatial coordinates, x and z .

When unsaturated flow exists or $\theta < \theta_s$,

$$\frac{P}{\rho g} = \frac{P_c}{\rho g}$$

where $\frac{P_c}{\rho g}$ = capillary pressure.

In this case ϕ , K and θ are all functions of the spatial coordinates and the capillary pressure or:

$$K = f_1(x, z, P_c)$$

$$\theta = f_2(x, z, P_c)$$

$$\phi = f_3(x, z, P_c)$$

It is these relationships which make Equation 1 nonlinear and extremely difficult to solve for large problems with sizable variations in hydraulic conductivities and moisture contents.

The capillary pressure is defined as:

$$P_c = P_{nw} - P_w$$

or the difference in pressure in the nonwetting fluid, P_{nw} , and the pressure in the wetting fluid, P_w . If the air pressure is taken as a datum for measuring the pressure of the wetting fluid (i.e., $P_{nw} = 0$), then:

$$P_c = -P_w$$

Rewriting the right side of Equation 1 using the chain rule gives:

$$\frac{\partial}{\partial x} (K \frac{\partial \phi}{\partial x}) + \frac{\partial}{\partial z} (K \frac{\partial \phi}{\partial z}) = \frac{\partial \theta}{\partial \phi} \frac{\partial \phi}{\partial t} - q \quad (2)$$

which is more easily used for the basic differential equation of the model.

AXISYMMETRIC EQUATIONS

The axisymmetric partial differential equation form of Equation 2 is:

$$\frac{1}{r} \frac{\partial}{\partial r} (Kr \frac{\partial \phi}{\partial r}) + \frac{\partial}{\partial z} (K \frac{\partial \phi}{\partial z}) = \frac{\partial \theta}{\partial \phi} \frac{\partial \phi}{\partial t} - q \quad (3)$$

where r is the radial distance from the axis of symmetry. Multiplying by r and defining:

$$\bar{K} = Kr, \quad U = r \frac{\partial \theta}{\partial \phi} \quad \text{and} \quad \hat{q} = qr \quad (4)$$

transforms Equation 3 into a form similar to Equation 2. Hence the same computer routine may be used for both problems with slight revision to take care of the redefinition.

FUNCTIONAL DESCRIPTION OF SOIL CHARACTERISTICS

Numerical solutions depend entirely on the functional relationships of K and θ to capillary pressure. These functional relationships are the hydraulic characteristics of the soil.

The dependence of the hydraulic conductivity on capillary pressure is usually determined in a dynamic flow system or calculated from steady-state measurements. (18,19,20,21,22)

Many empirical expressions have been used to describe hydraulic conductivity as a function of capillary pressure. Several have been used in this model and their limitations are discussed. One equation which relates relative hydraulic conductivity to capillary pressure, known as Gardner's equation, as modified by King, (22) has the form:

$$K_r = \frac{1}{\left(\frac{P_c}{P_1}\right)^T + b} \quad (5)$$

where

K_r is the relative hydraulic conductivity

P_c is the capillary pressure

P_1 , τ , and b are parameters of the equation determined by curve fitting techniques

Data and fitted curves for three soils are shown in Figure 1.

In order to solve the basic Equation 2 one other functional relation is required. An equation for the moisture content as a function of the capillary pressure, proposed by King (21) is:

$$\theta = \delta f \left[\frac{\cosh \left[\left(\frac{P_c}{P_o} \right)^\beta + \epsilon \right] - \gamma}{\cosh \left[\left(\frac{P_c}{P_o} \right)^\beta + \epsilon \right] + \gamma} \right] \quad (6)$$

where

P_o , δ , ϵ , γ , β are parameters

θ is the moisture content

f is the porosity of the soil

Data points and fitted moisture content curves by King (22) are shown in Figure 2.

The Equations 5 and 6 were used in test simulations. However, during the tests two limitations of this approach were noted. First, solving Equations 5 and 6 and evaluating their complex derivatives is computationally slow. Second and more importantly, Equation 6 has the property that as $P_c \rightarrow \infty$, S approaches the limit

$$\lim_{P_c \rightarrow \infty} S = \frac{\delta (\cosh \epsilon - \gamma)}{(\cosh \epsilon + \gamma)}$$

FIGURE 1. Relative Permeability Versus Capillary Pressure Curve and the Functional Fitting Equation

FIGURE 2. Capillary Pressure Versus Saturation Curves and the Functional Fitting Equation

Thus the saturation has a limiting value which depends on the curve fit used and may be larger than the background moisture contents observed in the field. In addition, as the calculated moisture content approaches this limit, numerical instability can occur since slight changes in moisture content result in large changes in capillary pressure. Thus initial moisture contents have to be set at a level greater than the limit of S and the boundary conditions also must be set to maintain this minimum level of saturation in order to avoid these numerical instability problems.

In an attempt to circumvent these problems, two other fitting methods were tried. A computer program was written to solve the modified Millington and Quirk equation for computing the hydraulic conductivity curve for partially saturated soil from the moisture retention versus suction measurements and the saturated hydraulic conductivity. (19,21) However, several problems arose during application of this method. The limited suction data that are normally collected are inadequate to accurately describe the moisture retention curve. Thus, interpolation techniques were employed with which to generate a uniformly spaced set of data from the sparse, randomly spaced suction data. In generating the hydraulic conductivity curves from these data, two types of errors were introduced, measurement and interpolation, which caused small undulations to occur in the hydraulic conductivity curves. Figure 3 shows the moisture content curve; note the undulation from the curve fitting. Figure 4 shows the resulting hydraulic conductivity curve. In the PST Model the minor reversal of slopes along the curve of saturation versus capillary pressure curves caused difficulties with time plane convergence. This problem was solved by drawing a smooth curve through the generated moisture retention data and using very closely spaced data points.

A third method developed by Campbell (23) was adopted which bypasses these problems and requires less suction data than the Millington and Quirk method and also avoids the interpolation problems. The empirical expression suggested by Campbell (23) which relates water content to capillary pressure is:

$$P_c = P_e \left(\frac{\theta}{\theta_s} \right)^{-d} \quad (7)$$

FIGURE 3. Water Content Versus Suction Head for the "A" Tank Farm Soil

FIGURE 4. Hydraulic Conductivity Versus Suction Head for the "A" Tank Farm Soil

where P_e is the air entry water pressure and θ_s is the saturated moisture content and d is an empirically determined constant. The hydraulic conductivity function is also an empirical expression (23)

$$K = K_s \left(\frac{P_e}{P_c} \right)^{2+\frac{3}{d}} \quad (8)$$

where K_s is the saturated hydraulic conductivity. These equations do not have artificially high asymptotes as occur when using King's equations and are computationally more efficient. This method of handling these functional relationships is by far the best of the methods tested.

FINITE DIFFERENCE EQUATIONS

Several different methods for writing finite difference equations exist. The Crank-Nicolson method was selected because it is unconditionally stable and experimental tests using other techniques gave unsatisfactory results. Although Crank-Nicolson guarantees unconditional stability, it does not prevent instabilities from occurring. However, any instabilities that occur are bounded and will decay, rather than grow, with time. The method basically involves writing the equations at the mid-point of the time step; i.e., to approximate the derivatives three points in the old time plane and three points in the new time plane are used, as shown in Figure 5.

FIGURE 5. Points Used in Time and Space for Crank-Nicolson Finite Difference Expression

Development of the finite difference form of Equation 2 using the Crank-Nicolson method is described in Appendix B. The resultant difference equation is

$$\phi_{i,j}^{n+1} = \frac{L^{n+1} + L^n + 2\hat{r}N^{n+1/2}\phi_{i,j}^n - \phi_{i,j}^n(Q^n) + 2q}{2\hat{r}N^{n+1/2} + Q^{n+1}} \quad (9)$$

where

$$L^{n+1} = K_{i+1/2,j}^{n+1}\phi_{i+1,j}^{n+1} + K_{i-1/2,j}^{n+1}\phi_{i-1,j}^{n+1} \\ + K_{i,j+1/2}^{n+1}\phi_{i,j+1}^{n+1} + K_{i,j-1/2}^{n+1}\phi_{i,j-1}^{n+1}$$

$$L^n = K_{i+1/2,j}^n\phi_{i+1,j}^n + K_{i-1/2,j}^n\phi_{i-1,j}^n \\ + K_{i,j+1/2}^n\phi_{i,j+1}^n + K_{i,j-1/2}^n\phi_{i,j-1}^n$$

$$Q^{n+1} = K_{i+1/2,j}^{n+1} + K_{i-1/2,j}^{n+1} + K_{i,j+1/2}^{n+1} + K_{i,j-1/2}^{n+1}$$

$$Q^n = K_{i+1/2,j}^n + K_{i-1/2,j}^n + K_{i,j+1/2}^n + K_{i,j-1/2}^n$$

$$\hat{r} = \frac{\Delta z \Delta x}{\Delta t}$$

$$N^{n+1/2} = \left(\frac{\partial \theta}{\partial P_c}\right)^{n+1/2} = \frac{\left(\frac{\partial \theta}{\partial P_c}\right)^{n+1} + \left(\frac{\partial \theta}{\partial P_c}\right)^n}{2}$$

$\Delta z, \Delta x$ = vertical and horizontal grid spacing

Δt = time increment

i, j = grid point indices

n = time plane index

An algorithm similar to the Gauss-Seidel numerical solution method was used to solve Equation 9. Minimal effort was applied to optimizing the solution technique since the main objective was to achieve operational status of the model to determine if solutions for the types of problems and hydrogeologic conditions that prevail at the Hanford Reservation could be generated.

BOUNDARY CONDITIONS

The myriad of practical flow problems which may be modeled present three basic types of boundary conditions:

- 1) boundaries along which the potential, specified

$$\phi = \text{constant}, t \geq 0$$

- 2) boundaries across which no flow occurs

$$\frac{\partial \phi}{\partial z} = 0 \text{ or } \frac{\partial \phi}{\partial x} = 0, t \geq 0$$

- 3) boundaries across which a known amount of flow occurs

$$q = \text{constant}, t \geq 0$$

Types 1 and 2 are the most common boundary conditions. Type 3, a typical example of which is the evaporation of water from a soil surface or a constant rainfall, may be modeled using a known flow rate or by a type 1 boundary if a proper potential can be determined. The type 2 boundary is normally used for describing impermeable boundaries.

GENERAL PROGRAM DESCRIPTION

The PST Model as developed handled a matrix of 6000 nodes, limited by computer storage. This capacity was increased by the computer capability to utilize partial computer words to conserve storage. Three pieces of information are packed into one memory location for each node in the problem: 1) an index for identifying the specific soil type for each node; 2) calculation type identification for the equation (internal or boundary) to be used at each node for calculating the potential; and 3) an index identifying the flux or input flow for each node.

Even then the problem size had to be restricted because grid spacing beyond a few centimeters at the wetting front in the sediments caused more rapid advancement.

Equation 9 forms the basis for the PST flow program. Equation 9 represents only the general form of the basic equation; 24 no-flow boundary equations developed from various shapes of nodes (Figure 6) are available in the program.

Since a Gauss-Seidel type iterative scheme is used for solving the resultant matrix, the hydraulic potential is solved for in a point-by-point fashion, updating all of the stored data to its latest value immediately. In the computer program the information stored at each node includes the type of soil, the type of calculation, an index to a flux value table, the potentials from the present and past time planes, the hydraulic conductivity, and Crank-Nicolson term.

FIGURE 6. Schematic Showing Shapes and Rotation of Available Boundary Nodes

Examination of Equation 9 shows that a great deal of information from the n^{th} or previous time plane is necessary to solve the problem. To avoid using large volumes of computer storage, all terms involving information from the past time plane are accumulated and stored as a single value called (for reference) the Crank-Nicolson term. This term is updated at the end of every time step for every nodal position.

The Crank-Nicolson (CN) term is zero for steady systems and also zero when all the nodes in a region are saturated and of the same soil type.

Use is made of the computer capability to utilize partial computer words to conserve storage. Three pieces of information are packed into one memory location for each node in the problem: 1) an index for identifying the specific soil type for each node (provisions are made for ten different types of soils); 2) calculation type identification for the equation (internal or boundary) to be used at each node for calculating the potential; and 3) an index identifying the flux or input flow for each node.

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APPENDIX A

GENERALIZED EQUATIONS DESCRIBING
HEAT AND MASS TRANSPORT IN UNSATURATED
POROUS MEDIA

Prepared by
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APPENDIX A

DERIVATION OF MOISTURE FLUX EQUATIONS FOR UNSATURATED SOIL

Conservation of mass requires that for a given volume of soil:

$$\frac{\partial \theta}{\partial t} = - \frac{\partial J_{wx}}{\partial x} - \frac{\partial J_{wy}}{\partial y} - \frac{\partial J_{wz}}{\partial z} + G(x,y,z) = - \nabla \cdot J_w + G(x,y,z) \quad (1)$$

where θ is mass concentration of water, t is time, J_w is mass flux of water, and G is the rate of water production (or negative consumption per unit volume of soil).

Water flux may result from gradients in matric potential, gravitational potential, osmotic potential, and temperature. One needs to consider fluxes in both the liquid and the vapor phase. Let us consider the flux in the z direction. Fluxes in other directions would be written in similar fashion but without the gravitational component. The theory of irreversible thermodynamics provides a general approach which is useful for this type of problem.³

The liquid-phase flux, denoted by superscript ℓ , can be written as:

$$J_w^\ell = - L_{ww}^\ell X_w - L_{wq}^\ell X_q - L_{ws}^\ell X_s \quad (2)$$

and the vapor phase flux, denoted by superscript v , as:

$$J_w^v = - L_{ww}^v X_w - L_{wq}^v X_q - L_{ws}^v X_s \quad (3)$$

where the L 's are transport coefficients, X 's are driving forces, and w , q , and s denote water, heat, and salt. The total flux is the sum of the liquid and vapor phase fluxes.

If we write $\beta = L_{wq}/L_{ww}$ and $\sigma = L_{ws}/L_{ww}$, where β is the heat of transport and σ is the reflection coefficient, Equations 2 and 3 become:

$$\begin{aligned} J_w = J_w^\ell + J_w^v = & - L_{ww}^\ell (X_w + \beta^\ell X_q + \sigma^\ell X_s) \\ & - L_{ww}^v (X_w + \beta^v X_q + \sigma^v X_s) \end{aligned} \quad (4)$$

The coefficients and forces must now be chosen to be dimensionally consistent. The liquid transport coefficient, L_{ww}^ℓ , is just the hydraulic conductivity, $k(\theta)$, and the driving force for water flow is the sum of the gravitational and matric potential gradients:

$$X_w = \left. \frac{\partial \Psi_m}{\partial z} \right|_T + \frac{\partial \Psi_g}{\partial z}$$

Since the matric potential, ψ_m , may vary with temperature it is necessary to specify that the gradient be taken at constant temperature.

The other driving forces are:

$$X_q = \frac{1}{T} \frac{\partial T}{\partial z}$$

$$X_s = \frac{\partial \psi_o}{\partial z}$$

Where T is the Kelvin temperature and ψ_o is the osmotic potential. With this choice of driving forces:

$$\beta^l = T \frac{\partial \psi_m}{\partial T}$$

The reflection coefficient, σ^l , is just a fraction giving the effectiveness of osmotic potential gradients in causing flow compared to the effectiveness of matric gradients.

If we define the vapor phase driving forces the same as those for liquid-phase flux, then the coefficients must take up the conversion from vapor concentration to potential since the driving force for vapor movement is a gradient in vapor concentration.

To find L_{ww}^v , we can write for isothermal vapor diffusion:

$$J_w^v = - D_v \left. \frac{\partial \rho_v}{\partial z} \right|_T = - D_v \left. \frac{\partial \rho_v}{\partial \psi} \right|_T \left. \frac{\partial \psi}{\partial z} \right|_T \quad (5)$$

where D_v is the vapor diffusivity in soil, ρ_v is the vapor density, and ψ is the sum of the matric, osmotic, and gravitational potentials. The osmotic component can be included with the others because $\sigma^v = 1$. From equation 5 the transport coefficient for vapor is:

$$L_{ww}^v = D_v \left. \frac{\partial \rho_v}{\partial \psi} \right|_T \quad (6)$$

The relationship between water potential and vapor density is:

$$\rho_v = \rho_v^0 \exp \left(\frac{\psi}{RT} \right) \quad (7)$$

where ρ_v^0 is the saturation vapor density and R is the specific gas constant for water. In the normal range of water potentials encountered in soil water flow problems, $\psi/RT \ll 1$ and Equation 7 becomes:

$$\rho_v = \rho_v^0 \exp \left(\psi/RT \right) \approx \rho_v^0 \left(1 + \frac{\psi}{RT} \right)$$

and from Equation 6:

$$L_{ww}^v = \frac{D_v \rho_v^0}{RT} \quad (8)$$

The vapor flux resulting from temperature gradients can be expressed as:

$$J_w^v = - D_v \frac{\partial \rho_v}{\partial z} = - D_v \frac{\partial \rho_v}{\partial T} \frac{\partial T}{\partial z} \quad (9)$$

The driving force for thermally induced flow is $\frac{1}{T} \frac{\partial T}{\partial z}$ so from Equation 4 and Equation 8:

$$J_w^v = - \frac{L_{ww}^v}{T} \frac{\partial T}{\partial z} = - \frac{D_v \rho_v^0}{RT^2} \beta \frac{\partial T}{\partial z} \quad (10)$$

Equating 9 and 10 and solving for β gives:

$$\beta = \frac{RT^2}{\rho_v^0} \frac{\partial \rho_v}{\partial T} \quad (11)$$

The Claussius-Clapeyron equation can be used to find $\frac{\partial \rho_v}{\partial T}$. It gives:

$$\frac{\partial \rho_v}{\partial T} = \frac{\rho_v^0 \lambda}{RT^2}$$

Where λ is the latent heat of vaporization, combining this with Equation 11 gives:

$$\beta = \lambda,$$

a result confirmed experimentally by Taylor and Cary (1964).³

Equation 4 can now be rewritten incorporating the explicit forms of the coefficients and forces giving:

$$J_w = - \left[k(\theta) + \frac{D_v \rho_v^0}{RT} \right] \left[\left(\frac{\partial \Psi_m}{\partial z} \right)_T + \frac{\partial \Psi_g}{\partial z} \right] - \left[\sigma k(\theta) + \frac{D_v \rho_v^0}{RT} \right] \left(\frac{\partial \Psi_o}{\partial z} \right)_T - \left[k(\theta) \frac{\partial \Psi_m}{\partial T} + \frac{D_v \rho_v^0 \lambda}{RT^2} \right] \frac{\partial T}{\partial z} \quad (12)$$

When temperature and salt concentration gradients are absent, the second and third terms in Equation 12 are zero. When significant transport does occur from these driving forces, the simultaneous transport of water, heat, and salt must be accounted for. The flux equations are:

$$J_s = - L_{ss} X_s - L_{sw} X_w - L_{sq} X_q \quad (13)$$

$$J_q = - L_{qq} X_q - L_{qw} X_w - L_{qs} X_s \quad (14)$$

These would be used with mass and energy conservation equations to describe temperature, salt concentration, and water content as function of position and time in the soil. If the salts are ionic, a fourth equation must be added to describe flow of electricity. One sees quickly that a complete solution to this problem would be impossibly difficult. Fortunately, considerable simplification can be achieved by considering the sizes of various terms. Both $k(\theta)$ and $\frac{D_v \rho_v^0}{RT}$ are functions of water content, since D_v depends on air-filled porosity of the soil. Philip and DeVries⁴ give:

$$D_v = D_o \nu \alpha a \quad (15)$$

where D_o is the diffusion coefficient for water vapor in air, ν is an "enhancement factor" to account for diffusion in excess of that predicted by simple theory, α is a tortuosity factor to account for the tortuous diffusion path and a is air filled porosity. We will take $\alpha = 0.66$ and $\nu = 4$ as typical of unsaturated soil. The air filled porosity, a , is:

$$a = 1 - \frac{\rho_b}{\rho_p} - \frac{\theta \rho_b}{\rho_w} \quad (16)$$

where ρ_b = bulk density, ρ_p = particle density, and ρ_w is the density of liquid water. Taking $\rho_b/\rho_p = 0.5$ and $\rho_b/\rho_w = 1.3$ gives:

$$a = 0.5 - 1.3\theta$$

and

$$D_v = D_o (1.3 - 3.4\theta).$$

At 20C, $D_o = 0.24 \text{ cm}^2 \text{ sec}^{-1}$, $\rho_v^0 = 17.3 \times 10^{-6} \text{ g cm}^{-3}$
 $R = 4.6 \text{ Bar K}^{-1}$, and $T = 293^\circ \text{K}$.

$$\frac{D_v \rho_v^0}{RT} = 3 \times 10^{-9} (1.3 - 3.4\theta) \text{ g Bar}^{-1} \text{ sec}^{-1} \text{ cm}^{-1}$$

Hydraulic conductivity as a function of water content, can be written as (Campbell, 1974):

$$k(\theta) = k_s \left(\frac{\theta}{\theta_s} \right)^d$$

where k_s and θ_s are hydraulic conductivity and water content at saturation, and d is an empirical constant. Values of k , θ_s , and d will vary of course from soil to soil, but for the moment we will assume typical values of $\theta_s = 0.38$, $k_s = 1.0 \text{ g Bar}^{-1} \text{ sec}^{-1} \text{ cm}^{-1}$ and $d = 10$. The liquid and vapor conductivity are compared in the following table:

TABLE 1. Liquid and Vapor Conductivity at Relative Moisture Contents for Typical Sandy Soil

$\frac{\theta}{\theta_s}$	$k(\theta)$	$\frac{D_v \rho_v^0}{RT}$
0.2	10^{-7}	3.0×10^{-9}
0.4	10^{-4}	2.3×10^{-9}
0.6	6×10^{-3}	1.6×10^{-9}
0.8	0.1	0.8×10^{-9}
1.0	1.0	0

Obviously, vapor transport is of little concern in isothermal flow problems.

The reflection coefficient, σ , has been measured under conditions which tend to maximize its value (sodium saturated, fine textured soil) by Letey, et.al. (1969)¹. They found $\sigma < 0.04$ for soils wetter than 0.5 Bar. Values might be expected to be even smaller for coarse textured, low salt soils. Since $\frac{\partial \Psi_0}{\partial z}$ is probably not greater than $\frac{\partial \Psi_m}{\partial z} + \frac{\partial \Psi_g}{\partial z}$, osmotically induced flow would normally be, at most, a few percent of the total. This is negligible compared to other uncertainties, so the entire second term of Equation 12 can generally be neglected.

Taylor and Stewart (1960)² give data which can be used to find $\frac{\partial \Psi_m}{\partial T}$. From their data we obtain approximately:

$$\frac{\partial \Psi_m}{\partial T} = 0.02 \Psi_m$$

Typically, Ψ_m is a few tenths of a bar in flow problems, therefore:

$$\frac{\partial \Psi_m}{\partial T} = 0.005$$

is a commonly accepted value. Using numbers from Table 1, at $\frac{\theta}{\theta_s} = 0.2$,

$$k(\theta) \frac{\partial \Psi_m}{\partial T} = 5 \times 10^{-10}$$

and, with $\lambda/T = 24330/293 = 83$ Bar/k,

$$\frac{D_v \rho_v^0 \lambda}{RT^2} = 2.6 \times 10^{-7}$$

Thermally induced liquid flow is obviously unimportant at this water content, but the vapor term would have a significant contribution anytime $\frac{\partial T}{\partial z}$ became of similar magnitude to $\frac{\partial \Psi_m}{\partial z} + \frac{\partial \Psi_g}{\partial z}$. The gravitational gradient is 10^{-3} Bar/cm, so temperature gradients as large as 10^{-3} K/cm might cause significant flow in soils with $\theta/\theta_s = 0.2$ or drier. In wetter soil $k(\theta)$ becomes much larger while the thermal term becomes smaller, and the thermally induced flow can generally be neglected.

With these simplifications, Equation 12 finally reduces to the flow equation which is normally used.

$$J_w = -k(\theta) \frac{\partial \Phi}{\partial z}$$

where $\Phi = \Psi_g + \Psi_m$. In three dimensions:

$$\bar{J}_w = -k(\theta) \nabla \Phi$$

The transient equation (Equation 1) becomes:

$$\frac{\partial \theta}{\partial t} = -\nabla \cdot \bar{J} + G(x, y, z) = \nabla \cdot [k(\theta) \nabla \Phi] + G(x, y, z)$$

Except where root extraction of water by plants occurs, $G(x, y, z) = 0$.

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APPENDIX B

DEVELOPMENT OF FINITE-DIFFERENCE EQUATIONS

APPENDIX B

The development of the finite-difference approximation to the partial differential equation is of some interest because this technique can be used systematically to develop equations for no-flow boundary nodes for a great variety of shapes by integration of the flow around the elemental block.

Equation 1 in the text may be written as

$$\underline{\nabla} \cdot (K\underline{\nabla}\phi) + q = \frac{\partial \theta}{\partial t} \quad (1)$$

where q has been added to define a source or sink term with a node.

Now consider Equation 1 in a region R and at each node point (i,j) , construct a region $r_{i,j}$ within R such that

$$0 = \iint_{r_{i,j}} \left(\underline{\nabla} \cdot (K\underline{\nabla}\phi) - \frac{\partial \theta}{\partial t} \right) dx dz \quad (2)$$

Using Green's theorem to convert the first part of Equation 2 to a line integral

$$\iint_{r_{i,j}} \left(\frac{\partial (K\underline{\nabla}\phi)}{\partial x} \right)_i - \left(-\frac{\partial (K\underline{\nabla}\phi)}{\partial z} \right)_j = \oint_{\Gamma_{i,j}} K\underline{\nabla}\phi \cdot \hat{n} dc \quad (3)$$

where $\hat{n}$ is the outward pointing normal vector and $dc^2 = dx^2 + dz^2$, $\Gamma_{i,j}$ is the boundary of $r_{i,j}$ and arc length s increases in the counterclockwise direction.

Equation 2 then becomes

$$\oint_{\Gamma_{i,j}} K\underline{\nabla}\phi \cdot \hat{n} dc - \iint_{r_{i,j}} \left(\frac{\partial \theta}{\partial t} \right) dx dz = 0 \quad (4)$$

Consider the region $r_{i,j}$ as shown in Figure B-1.

FIGURE B-1. Basic Node Net for Development of Difference Equations

The corner points of the node area are at $(i-1/2, j-1/2)$, $(i+1/2, j-1/2)$, $(i+1/2, j+1/2)$, and $(i-1/2, j+1/2)$. We can then write

$$a_{i,j} = dx dz = \Delta x \Delta z \quad (5)$$

Integrating the equation for the region, $r_{i,j}$ gives

$$\int_{z_{j+1/2}}^{z_{j-1/2}} K(x_{i-1/2}, z) \phi_x(x_{i-1/2}, z) dz = \Delta z K_{i-1/2,j} \left(\frac{\phi_{i,j}^n - \phi_{i-1,j}^n}{\Delta x} \right) \quad (6)$$

$$- \int_{z_{j-1/2}}^{z_{j+1/2}} K(x_{i+1/2}, z) \phi_x(x_{i+1/2}, z) dz = - \Delta z K_{i,j-1/2} \left(\frac{\phi_{i,j}^n - \phi_{i-1,j}^n}{\Delta x} \right) \quad (7)$$

$$\int_{i-1/2}^{i+1/2} K(x, z_{j-1/2}) \phi_z(x, z_{j-1/2}) dx = \Delta x K_{i+1/2,j} \left(\frac{\phi_{i+1,j}^n - \phi_{i,j}^n}{\Delta z} \right) \quad (8)$$

$$-\int_{i+1/2}^{i-1/2} K(x, z_{j+1/2}) \phi_z(x, z_{j+1/2}) dx = \Delta x K_{i,j+1/2} \left(\frac{\phi_{i,j+1}^n - \phi_{i,j}^n}{\Delta z} \right) \quad (9)$$

$$\int_{\Gamma_{i,j}} K \frac{\partial \phi}{\partial \hat{n}} d\Gamma = 0 \quad (10)$$

$$\iint_{r_{i,j}} \left(\frac{\partial \theta}{\partial t} \right) dx dz = \left(\frac{\theta_{i,j}^{n+1} - \theta_{i,j}^n}{\Delta t} \right) \Delta x \Delta z \quad (11)$$

$$\iint_{r_{i,j}} q dx dz = q \Delta x \Delta z$$

From the above, the basic finite-difference equation is written as:

$$L_1(K, \phi) + L_2(K, \phi) - M(\theta) - \phi_{i,j} (Q_1(K) + Q_2(K)) + \bar{q} = 0 \quad (12)$$

$$\text{where } L_1(K, \phi) = K_{i+1/2,j} \phi_{i+1} + K_{i-1/2,j} \phi_{i-1}$$

$$L_2(K, \phi) = K_{i,j+1/2} \phi_{i,j+1} + K_{i,j-1/2} \phi_{i,j-1}$$

$$M(\theta) = \Delta x \Delta z \frac{\theta_{i,j}^{n+1} - \theta_{i,j}^n}{\Delta t}$$

$$Q_1(K) = K_{i+1/2,j} + K_{i-1/2,j}$$

$$Q_2(K) = K_{i,j+1/2} + K_{i,j-1/2}$$

$$\bar{q} = q \Delta x \Delta z$$

If we assume the boundary of the region to pass through the elemental node, as in Figure B-2 with the shaded area internal to the flow regime, we can perform the foregoing integration and determine the boundary equation. The result is similar to Equation 12:

$$1/2 L_1(K, \phi) + K_{i,j-1/2} \phi_{i,j-1} \quad (13)$$

$$-M(\theta) - \{1/2 Q_1 + K_{i,j-1/2}\} \phi_{i,j} + \bar{q} = 0$$

FIGURE B-2. Boundary Node for No-flow
between Bottom and Top of Node

Note that the $j+1$ terms are not included. This results in a boundary node through which no flow may pass in the y direction or the flow is parallel to the boundary.

Through the same process, a series of boundary node equations describing no-flow boundaries were developed for the shapes of the partial nodes that fit the perimeter of an octagon. Figure A-3 shows the shapes and their various rotations where the heavy line represents the no flow side of each nodal area.

FIGURE B-3. Schematic Showing Shapes and
Rotation of Available Boundary Nodes

The utilization of these nodes prevent small right angle corner stagnation areas which hinder convergence in the analyses.

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