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INTEGRATED LOW EMISSIONS CLEANUP SYSTEM FOR
DIRECT COAL FUELED TURBINES
(Moving Bed, Fluid Bed Contactor/Ceramic Filter)

Twenty-Third Quarterly Report

Quarterly Status for the Period April - June 1993

By

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D. M. Bachovchin
W. C. Yang
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T. E. Lippert, Project Mgr.

July 19, 1993

Work Performed under Contract: DE-AC21-87MC24257

For

U. S. Department of Energy
Office of Fossil Energy
Morgantown Energy Technology Center
Morgantown, West Virginia

DOE - COTR: R. A. Dennis

Prepared by:
Westinghouse Electric Corporation
Science and Technology Center
Pittsburgh, Pennsylvania

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PATENT STATUS

This technical report is being transmitted in advance of DOE patent clearance and no further dissemination or publication shall be made of the report without prior approval of the DOE Patent Counsel.

TECHNICAL STATUS

This technical report is being transmitted in advance of DOE review and no further dissemination or publication shall be made of the report without prior approval of the DOE Project/Program Manager.

ABSTRACT

The United States Department of Energy, Morgantown Energy Research Center (DOE/METC), is sponsoring the development of direct coal-fired turbine power plants as part of their Heat Engines program. A major technical challenge remaining for the development of the direct coal-fired turbine is high-temperature combustion gas cleaning to meet environmental standards for sulfur oxides and particulate emissions, as well as to provide acceptable turbine life.

The Westinghouse Electric Corporation, Science & Technology Center, is evaluating two Integrated Low Emissions Cleanup (ILEC) concepts that have been configured to meet this technical challenge: a baseline ceramic barrier filter ILEC concept, and a fluidized bed ILEC concept. These ILEC concepts simultaneously control sulfur, particulate, and alkali contaminants in the high-pressure combustion gases at turbine inlet temperatures up to 2300°F. This document reports the status of a program in the nineteenth quarter to develop this ILEC technology for direct coal-fired turbine power plants.

EXECUTIVE SUMMARY

During the Twenty-Third Quarter of the program, the Phase II tasks for the fabrication of the bench-scale test facility have been completed. Component shakedown has also been completed. During this quarter, the Phase II Test Plan has been restructured to deal specifically with effective pulse cleaning in PFBC. The nature of the flyash and the use of additives are major aspects of the program. A Phase II Topical Report was prepared and submitted to DOE for review and approval.

1. INTRODUCTION

Development of direct coal-fueled turbine power cycles, in the Department of Energy Heat Engines program, is focused on staged, slagging combustor designs that potentially provide high performance, compact and low cost power generation systems. The power generation systems demand high performance from hot-gas cleaning equipment to meet environmental requirements and to satisfy turbine protection requirements, using concepts that are, as yet, undeveloped.

To provide emissions control and turbine protection from gas- and solid-phase contaminants in direct coal-fired turbine systems, contractors are currently testing: beneficiation of coal to minimize ash and sulfur content; injection of sulfur sorbents into or following the combustor; staged combustion to limit NO_x formation; slag removal by impaction; inertial particle collection; and barrier filters within the combustor-cleanup train. While there is a basis for the development of some of these proposed approaches to hot-gas cleaning a number of concerns make the development of an innovative, integrated, low emission, gas cleanup (ILEC) concept desirable. Specific concerns include the high cost of highly beneficiated coals, the economic penalty of separate gas cleaning functions arranged in series, the potentially limited ability of in-situ sulfur control to achieve low sulfur emissions, the potentially limited ability of inertial collection to achieve sufficiently low particulate emissions, and the need for gas-phase alkali control to provide acceptable turbine life.

New approaches for sulfur and alkali control may be required at the proposed temperature levels of some direct coal-fired systems, and new approaches for particulate control may be required in the environment of potentially molten and/or sticky particles. An

integrated, multi-function cleaning stage may be an economic requirement when using minimally-cleaned, high-sulfur, high-ash coals.

In addition, the ILEC system must be compatible with the application. In its programs on Heat Engines, the Department of Energy is attempting to develop coal-fueled turbines for large electric utility power plants, for industrial power plants, and for small, stationary and transportation power generation systems. This broad range of applications encompasses a large variety of turbine sizes and designs, a range of turbine operating conditions, different arrangements for coupling the coal combustor to the gas turbine, and greatly differing gas cleanup requirements. ILEC concepts that can be adapted to all of these applications are needed.

In this program, two advanced, high-temperature Integrated Low Emissions Cleanup concepts are addressed that combine particulate and gas phase contaminant removal in a single, compact filter device that is intended for operation in direct, coal-fueled turbine systems. The program will investigate the key process and design parameters of the concepts, evaluating both a "baseline" and a fluid bed ceramic filter with immersed barrier filters. In both concepts finely sized sulfur and alkali sorbents are injected into the combustion gas stream, react with the gas-phase sulfur and alkali species while modifying the sticky nature of the ash that is carried over from the combustor. Additives may also be injected to control the filter coal behavior. Sorbent and ash particles are collected on ceramic barrier filters placed in the contactor vessel.

The program has been divided into three phases. Phase I of the program deals with critical laboratory testing and conceptual commercial design evaluation. Phase I has been completed, although continuation of some key Phase I test work has been undertaken. In Phase II, upgrading of a HTHP bench-scale facility will take place along with the design and procurement of the baseline integrated cleanup test system. Phase II

has been initiated. Phase III of the program involves the actual HTHP bench-scale testing and engineering assessment of the integrated cleanup devices and systems.

2. WESTINGHOUSE ILEC CONCEPTS

The Westinghouse ILEC concepts are extrapolations to higher temperatures of gas cleaning technologies being developed for similar technical purposes in other applications. These generally lower temperature technologies are:

- ceramic barrier filter particulate control (up to 1700°F)
- fluidized bed filtration (up to 1200°F)
- sulfur sorbent injection into high-temperature gas streams (up to 3000°F), and fluidized bed desulfurization (up to 2000°F)
- alkali sorbent injection into high-temperature gas streams (up to 1600°F)

These technologies are currently being developed for applications that require high-pressure gas cleaning at temperatures up to about 1700°F (Pressurized fluid bed combustion and pressurized coal gasification systems, for example). Additional technical basis for the development of these ILEC concepts is provided by the Department of Energy and GRI development programs for high temperature heat recovery systems using fluidized bed heat exchangers,¹ and for high temperature ceramic heat exchangers that operate at temperatures exceeding those required for direct coal-fired turbines.^{2,3}

Ceramic barrier filters have the potential to provide extremely high particle removal efficiencies at high gas temperatures. Testing at temperatures up to 1700°F has shown that they can exceed the particulate removal needed for both environmental standards and for turbine erosion and deposition protection. The major concern for their use in direct coal-fired turbine applications is that adhesive particles (slag

particles or sticky fly ash particles) will be emitted from the coal combustor that may form a filter cake that is difficult to remove from the filter elements by normal pulse cleaning. It is the premise of the ILEC concepts proposed in this program that the combustion gas containing adhesive particles will interact with added sorbent particles, or inert additive particles, to either remove the adhesive particles before they reach the ceramic barrier filter elements, or to modify the filter cake adhesive nature so that it is removable. This premise is applied in the two ILEC concepts pictured in Figures 2.1 and 2.2.

In the first concept shown in Figure 2.1, the "baseline" ILEC concept, is a ceramic barrier filter vessel having a design much like that of the ceramic barrier filters vessels being developed for lower temperature applications. An array of vertical filter elements, candle-type or cross-flow type, is supported from a tube sheet, and is housed in a refractory-lined pressure vessel. Filter cake is periodically released from the filter elements by back-pulsing with clean gas. The released filter cake drops into a conical bin at the base of the vessel for removal. The baseline ILEC concept is operated with the injection of sulfur sorbents, alkali sorbents, and possibly selected deposit-modifying additives (e.g., kaolin) that produce a filter cake on the filter elements that is easily removed by pulsed cleaning. The potential success of the baseline ILEC concept is suggested by deposit formation observed in other programs that inject sulfur sorbents into conventional coal-fired furnaces, and programs that have injected deposit additives into coal-fired turbine gases.^{4,5,6} The injected sulfur sorbents are -325 mesh calcium-based sorbents, or advanced sulfur sorbents (strontium carbonate, for example), that effectively capture SO_2 at the turbine inlet temperatures in the relatively short contact times available. The injected alkali sorbent is -325 mesh emathlite, hectorite, or others, that removes alkali species (sodium and potassium components) from the gas to meet projected turbine alkali limits. The

WESTINGHOUSE ILEC CONCEPT

Figure 2.1 - ILEC Concept

effectiveness of emathlite has been demonstrated at a small-scale at temperatures up to about 1600°F in both reducing and oxidizing gases.⁷ Other alkali sorbents such as hectorite and bauxite are also candidates.

The second ILEC concept, in Figure 2.2, is a fluid bed filter concept. In this concept the combustion products are passed through a fluidized bed of either inert particles or sulfur sorbent particles. The adhesive particles agglomerate with the fluid bed media, removing them from the gas. The effectiveness of fluidized bed filters for particle removal by agglomeration phenomena has been demonstrated in other development programs at lower temperatures. Ceramic candle filters are vertically immersed into the fluid bed to prevent the elutriation of coarse particles, or the entrainment of fine particles from the fluid bed. In addition, the mixing action of the fluid bed provides cleaning of the filter cake from the ceramic candle filter surfaces, resulting in the potential elimination, or minimization, of the pulsed gas filter cleaning system. A similar fluid bed filter concept, using immersed candle filter elements in the bed, has been previously proposed for use in catalytic reactor systems.⁸

The fluid bed media has a particle size similar to particles used in bubbling PFBC applications. The fluid bed media if inert could be either alumina, sintered dolomite, slag particles generated in the combustor, or fly ash particles generated from the plant solid waste. The most economical material is used. If the fluid bed media is to function as a sulfur sorbent, it would be a cheap, calcium-based material such as dolomite. Sulfur sorbent particles and alkali sorbent particles can also be injected into the gas stream prior to the fluid bed filter.

The gas distributor for the fluid bed requires a design that is free from plugging of the orifice holes. Prior technology development suggests that water cooling, or air cooling, of the distributor plate to some critical temperature, combined with the selection of large orifices having sufficiently high gas velocities will provide protection against

Figure 2.2 - Fluid Bed ILEC Concept

deposit formation and plugging. The resulting fluid bed is relatively compact because the immersed ceramic candle filters permit the size of the freeboard region above the fluid bed to be minimized. The captured adhesive particles are removed with a continuous underflow stream of bed media. Fine particles that are not adhesive in nature will tend to segregate to the top of the fluid bed where they can be separately removed from the vessel.

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3. PROGRAM STRUCTURE AND OBJECTIVES

The program is being conducted in three phases to demonstrate at the bench scale the ILEC concepts. Phase I of the program has been completed, but some Phase I extended testing is being conducted. Phase I of the program deals with laboratory sorbent screening tests, cold flow testing, and commercial system evaluation of the ILEC concepts to support the bench-scale facility design and testing in Phases II and III. In Phase II, upgrading of a HTHP facility will take place along with the design and procurement of the filter test systems. The bench-scale test program will utilize an existing, high temperature, high pressure (HTHP) facility located at the Westinghouse Science and Technology Center. The facility will be upgraded for coal feeding to attain a range of combustion gas conditions that would be typical of the conditions expected at the exhaust of direct coal-fired combustors being developed in the current DOE Heat Engines programs. This facility will be used in Phase III to test the components and advanced design features of the baseline ILEC systems and to verify the engineering design principles of the concepts.

4. SUMMARY OF TWENTY-THIRD QUARTER PROGRAM STATUS

4.1 - PHASE I CONTINUATION: SUPPLEMENTAL LAB-SCALE TESTING

Objectives: Conduct laboratory testing that supports the bench-scale facility design and operation, as well as testing of critical fluid bed ILEC concept issues.

OBJECTIVE I-1 - TEST PLAN DEVELOPMENT

Identify areas requiring supplemental laboratory testing to support the bench-scale facility modification design and operation. Include critical issues for fluid bed ILEC concept. Define detailed test plan for each supplemental area. The test plan shall be reviewed and approved by the DOE COR.

Status

The test plan development has been completed. Some aspects of the test plan have been modified as the program focus and issues have been re-established. No effort has been expended on this task during this quarter.

OBJECTIVE I-5.1 - ENTRAINED SULFUR REMOVAL

Conduct tests of HTHP sulfur removal in the existing entrained reactor at specific test conditions to optimize sorbent properties and operating conditions for effective sulfur removal, as detailed in the Objective I-1 test plan.

Scope

Conduct tests to measure sulfur removal kinetics with the specific sulfur removal sorbents to be used in bench-scale testing. Preliminary range of test conditions:

- 1850 to 2100°F
- calcium-based sorbents (limestone, dolomite, hydrated lime)
- 0.1 to 1 second gas residence time
- oxidizing conditions
- sorbent particle size a parameter

Analyze the reaction products and the kinetic data. Confirm the existing entrained sulfur removal model by evaluation of known DCFT test data. Select the sulfur sorbent types, sizes and feed rates to be used in the bench-scale testing.

Status

This testing has been completed, with an option to return to complete some critical testing if needed at a later date. The data collected has been combined with past data, including DCFT tests reported by Solar Turbines, and an evaluation has been completed. Commercial ILEC sulfur removal performance has been projected. The sulfur removal evaluation was presented in the Twelfth Quarterly Report. No effort was expended on this task during this quarter.

OBJECTIVE I-5.2 - ALKALI REMOVAL

Modify the entrained reactor and conduct tests, as detailed in the Objective I-1 test plan, of HTHP alkali removal at specific conditions to optimize sorbent properties and operating conditions for effective alkali removal.

Scope

Design the entrained reactor modification required to test alkali removal kinetics. Modify the equipment. Conduct tests to measure alkali removal kinetics with the specific alkali removal sorbents to be used in bench-scale testing. Preliminary range of test conditions:

- 1850 to 2100°F
- emathlite and hectorite sorbents
- 0.1 to 1 second gas residence time
- oxidizing and reducing conditions
- sorbent particle size a parameter

Analyze the reaction products and the kinetic data, and re-assess the existing entrained alkali removal model. Select the alkali sorbent types, sizes and feed rates to be used in the bench-scale testing.

Status

A total of 22 tests have been conducted in the program, with temperatures of 1850 and 2100°F, and NaCl vapor contents ranging from 1.3 to 112 ppmw. Two operating modes of testing were used to assess the relative contributions of the entrained and the cake removal. In all of the tests the gas-particle contact time in the entrained zone was 2 seconds, and in the cake zone the particles resided for 15 minutes. The test results have been reported in the 15th and 16th Quarterly Reports. Conversions up to 9.24 weight percent of the emathlite reaction product

were measured, almost 50% of the saturation conversion of emathlite. In general, the performance under entrained conditions was better than with a cake only. The results have been correlated and estimates of commercial alkali removal performance in the ILEC have been developed. The complete evaluation will be reported in the task topical report currently in preparation.

OBJECTIVE I-5.3 - ADDITIVE SELECTION AND PERFORMANCE

Select deposit additives for the specific operating conditions, coal ash types, alkali and sulfur sorbents to be used in the bench testing. Confirm additive effectiveness in furnace tests.

Scope

Use prior test results and thermodynamic phase diagrams to select economical additives for filter cake modification. Procure these additives. Conduct furnace tests with the mixtures to confirm their performance.

Status

This objective has been reduced in scope to a minimum effort of identifying appropriate additives for Phase 3 testing. Some preliminary filter cake additive tests completed in a test unit very similar in design to the bench-scale unit under construction were evaluated and reported in the 21st Quarterly Report.

OBJECTIVE I-5.4 - FLUID BED CONCEPT CRITICAL ISSUES TESTING

Design, construct, and operate cold flow hydrodynamic simulation of fluid bed filter based on Phase I commercial conceptual design.

Scope

Identify critical issues, including distributor design, ash-bed separation, entrained sorbent mixing in the bed, filter element movement, filter element self-cleaning, element arrangement, etc. Include continuous ash feeding and ash removal capabilities. Eliminate fluidized slugging bed behavior by sizing gas flow to near 1000 actual cubic foot per minute. Prepare detailed design and assemble the facility. Select and procure commercial candle elements. Conduct tests as detailed in the Objective I-1 test plan. Re-assess critical issues and re-evaluate commercial design concept. Develop test plan for HTHP fluid bed testing.

Status

In prior cold model testing effective design and operating conditions have been identified. The major feature remaining to be developed is the removal of the fly ash particles from the fluid bed filter. The fluid bed filter concept appears to be of significant interest to some high-temperature applications:

- applications of relatively small gas flow where the tube sheet required to support the single layer of ceramic candles does not become too large in diameter to be practical;
- applications having primarily "sticky" fly ash particles that will be substantially removed by injection into the fluid bed media.

The small-scale, industrial DCFT applications such as those of Solar Turbine and Allison Gas Turbine appear to fit this description. The ability to simulate sticky fly ash particle behavior in the cold model,

while possible, would be very uncertain, and it seems likely that cold model testing will not be appropriate for the development needed for this process. Hot testing of the concepts is needed under simulated DCFT conditions.

OBJECTIVE I-6 - TOPICAL REPORTS

Prepare a Phase I Technical Report detailing the supplemental lab-scale efforts and two topical reports, i.e., High Temperature, High Pressure Deposit Additives; and Sorbents for High Temperature, High Pressure Vaporous Alkali Species Removal.

Status

Topical reports are scheduled near the completion of the appropriate Objectives. No topical reports have been completed during this quarter.

4.2 - PHASE II: BENCH-SCALE FACILITY DESIGN AND FABRICATION

OBJECTIVE II-1 - TEST PLAN DEVELOPMENT

Update from Phase I the test plan for the bench-scale facility test program based on the Westinghouse baseline ILEC concept. Include integrated particle, sulfur, and alkali removal performance, deposit additive characteristics of the filter cake, pressure drop, cleaning, and materials.

Scope

Estimate test conditions to evaluate the performance of simulated coal-fired turbine operation with the Westinghouse baseline ILEC concept. Include integrated

- particle removal performance
- sulfur removal performance
- alkali removal performance
- filter cake modification performance
- filter pressure drop and cleaning performance
- filter material behavior

Status

A revised test plan has been developed to focus on a key aspect of ceramic barrier filter technology - the effective pulse cleaning of candles in PFBC applications. The test plan is summarized in Appendix A.

OBJECTIVE II-2 - BENCH-SCALE FACILITY MODIFICATION DESIGN

Develop detailed design of the facility for the baseline ILEC concept bench-scale testing that meets the test plan requirements. Designs shall be submitted to the DOE COR for review and approval.

Scope

Utilize an existing HTHP filter test facility modified for

- temperatures up to 2100°F
- oxidizing environment
- partial coal injection/methane-fired
- sulfur removal with calcium-based sorbents
- alkali sorbent injection
- deposit additives
- cross-flow and candle filters elements

Select:

- appropriate candle material for this duty
- appropriate instrumentation for SO_x, and alkali measurement
- sorbent and additive feeding equipment and feed nozzles

Prepare:

- material and energy balances
- process flow diagrams
- equipment sizes, designs, and specifications
- vessel fabrication drawings

Status

The bench-scale facility design modifications have been completed during this quarter.

OBJECTIVE II-3 - BENCH-SCALE FACILITY FABRICATION AND ASSEMBLY

Prepare the facility for testing the baseline ILEC by modifying the existing HTHP test facility as required.

Scope

Fabricate the facility modifications and required new test vessels. Purchase equipment, candle and cross-flow filters, and instruments. Assemble the facility. Procure and characterize sulfur sorbents, alkali sorbents, deposit additives, coals, and coal ashes.

Status

During the quarter assembly of the test facility equipment has been completed, placing the filter unit into a prototypic, state-of-the-art, candle filter configuration applicable to PFBC. The standard Westinghouse candle figure configuration incorporates fail-safe devices. Procurement activities for alternative candle types and alternative flyashes are proceeding..

OBJECTIVE II-4 - BENCH-SCALE SHAKEDOWN TESTING

Conduct shakedown testing of the bench-scale facility and instruments to demonstrate the operating capabilities and acceptance to design requirements.

Scope

In support of the Objective II-2 facility modification design, operate the existing facility, prior to modification, to determine its current capabilities for high temperature operation and conduct brief tests to examine the consequences of high temperature operation. Operate the modified facility at maximum and minimum flow test conditions. Operate coal, ash, sorbent and additive feed equipment. Confirm accuracy of instrumentation.

Status

Shakedown testing of the major components and of the integrated facility were completed this quarter.

OBJECTIVE II-6 - TOPICAL REPORTS

Prepare the required Phase II Technical Report

Status

A Phase II Topical Report was completed this quarter and was submitted to DOE for review and approval.

OBJECTIVE II-7 - PROGRAM MANAGEMENT AND ADVISORY BOARD

Provide overall project management for meeting research objectives and for cost and schedule control. Continue Phase I Advisory Board activities in obtaining Heat Engine contractors' consultation and integration of ILEC cleanup research efforts through exchange of technical requirements and information.

Status

Program restructuring has occurred to a significant extent in the program, ensuring that the testing reflects the major technical issues facing ceramic barrier filter development as it relates to the Westinghouse ILEC. A cost-to-complete estimate has been developed and submitted to DOE during this quarter.

APPENDIX A

REVISED PHASE PROGRAM TEST PLAN

1. OBJECTIVES

Westinghouse STC and DOE/METC have reviewed the hot gas cleaning technology development status and issues, and have concluded that the ILEC test program should be revised to address some key areas. The objectives of the revised test program are to:

- Resolve issues relating to pulse cleaning of candles in PFBC.
- Observe relation between candle filter cleaning performance and:
 - Flyash source/ properties,
 - Temperature,
 - Pulse intensity,
 - Additives/ sulfur & alkali sorbents.
- Determine if pulse cleaning intensity and/or additives can be used to promote effective cleaning with difficult ashes.
- Determine the sulfur/alkali removal capabilities of the filter.

2. TEST SYSTEM DEFINITION

An existing test loop for ceramic barrier filters will be used for the testing. The test loop was being modified for the requirements of the original test plan, and will be modified further to meet the needs of the revised test plan. The major features are:

Configuration

- 4, 1-1/2 m candles in current PFBC holder/gasket design
- Fail-safe/regenerator in place
- Oxidizing atmosphere with injected PFBC flyashes

Parameters

- Candle Type (Schumacher, Coors, Refractron)
- Ash Source (Tidd, Tidd cyclone, Karhula, Grimethorpe)
- Additives (dolomite; kaolin; Neutralite)
- Additive procedure (premix, separate feed, precoat)
- Temperature
- Pulse tank pressure
- Pulse valve open time

Fixed Operating Conditions

- Face velocity: 7 ft/min (fixed gas volumetric flow at all conditions)
- Flyash loading: 5,000 to 10,000 ppmw
- Pressure: 100 psig

Measurements

- Gas flow and flyash flow
- Filter gas inlet and outlet temperature
- Candle filter cake temperature (on 2 to 4 candles)
- Tubesheet ΔP
- Pulse intensity in candle
- Pulse tank pressure (during pulse)

3. TEST SEQUENCE

Six test set have been defined, and are carried out in the following sequence:

- 1) Cake Permeability Tests (impact of temperature)
- 2) Cake Pulse Removal Tests (impact of temperature)
- 3) Additive Tests
- 4) Pulse Intensity Tests
- 5) Continuous Operation Tests
- 6) Sulfur/Alkali Removal Tests

The features of each of these test sets are outlined below.

4. CAKE PERMEABILITY TESTS

Objective: Observe influence of flyash source, temperature and time on filter cake permeability "stability"

Conditions: All testing with Schumacher candles

Test Parameters:

Gas/ filter cake temperature

Flyash ash type

- Tidd filter drain
- Tidd primary cyclone drain mixed with Tidd filter drain
- Grimethorpe
- Karhula

Flyash and additives

- Tidd filter drain plus 2 proportions of micronized dolomite
- Tidd filter drain plus 2 proportions of micronized kaolin

Evaluation:

Cake permeability calculated vs cake temperature

Correlation with flyash composition

Test Procedure:

Test Initiation: Raise gas inlet temperature to 1300°F following normal heatup procedure.

Step 1: Build filter cake on new candles until cake pressure drop (tubesheet minus baseline) of 20 iwg is reached -- flyash flow is discontinued at this point.

Step 2: Raise filter cake temperature in 50°F increments, holding at each temperature level long enough to determine if a stable cake permeability has been reached.

Step 3: Continue until the cake permeability shows a significant reduction, or until the gas inlet temperature reaches the maximum facility capability (about 1700°F).

Step 4: Cool the vessel slowly to 1300°F, continuing to record the tubesheet pressure drop for comparison with the heatup record.

Step 5: Pulse clean the candles with several vigorous pulses.

Parametrics: Repeat steps for each test point.

Final: Cool down without pulse cleaning, remove the candles and observe the appearance of the filter cake (photograph, measure thickness and morphology, sample bulk density)

Number of tests: 8

Number of candles used: 4 Schumacher

Flyash used: about 100 lb

Test time on-line: 96 hours

Total test period: 10 working days

5. CAKE PULSE REMOVAL TESTS

Objective: Observe temperature, time, flyash, candle type relation to cleaning performance; understand relation between cake permeability and cleanability.

Conditions: Operate with "high" pulse intensity (parameters to be selected)

Test Parameters:

Flyash type (Tidd, Grimethorpe, Karhula)

Candle type (Schumacher, Coors, Refractron)

Evaluation:

Calculate pulse cleaning effectiveness vs cake type and temperature

Support the testing with hot shear cell tests of adhesivity on a similar ceramic surface, and cohesivity

Test Matrix:

Candle	Flyash
Schumacher	Tidd
Schumacher	Tidd cyclone + filter catch.
Schumacher	Grimethorpe
Schumacher	Karhula
C2	F1
C2	F2
C3	F1

Procedure:

Step 1

- 1.1 - Heat up filter vessel, with no flyash feed, to temperature showing "normal" cake permeability in Test 1.
- 1.2 - Build cake on candles to same ΔP measured in Test 1.
- 1.3 - Hold, without flyash feeding, till steady-state.
- 1.4 - Pulse clean 3 times, at 5 minute intervals.

Step 2

- 2.1 - Ramp to temperature with unstable cake permeability in Test 1.
- 2.2 - Repeat Steps 1.2 - 1.4

Step 3

- 3.1 - Cool filter cake to the temperature of step 1.
- 3.2 - Pulse clean 3 times at 5 min intervals.

Step 4

Repeat sequence for each set of parameters.

Final: Cool down without pulse cleaning before each change of candles, remove the candles and observe the appearance of the filter cake (photograph, measure thickness and morphology, sample bulk density)

Number of tests: 7
Number of candles: 4 Schumacher, 4 Coors, 4 Refractron
Flyash used: about 100 lb
On-line testing time: 84 hours
Total test period: 11 working days

6. ADDITIVE TESTS

Objectives: Determine impact of cake additives on cleaning performance

Conditions: Selected duplicates from cake removal tests (Test 2)
All with Schumacher candles

Procedure: Repeat Test 2 procedure

Parameters:

Flyash type
Additive type (dolomite, kaolin, Neutralite)
Additive proportions (5-10 wt %)
Additive procedure
- premixed with flyash
- precoating on candles

Evaluation: Cake permeability and cleaning effectiveness with additive

Test Matrix:

Flyash	Additive	Proportion	Procedure
Tidd	Dolomite	R1	Premixed
Tidd	or	R2	Premixed
Karhula	Kaolin	R1	Premixed
Karhula		R2	Premixed
F	Neutralite	R1	Precoat
F	Neutralite	R2	Premix
F	Neutralite	R3	Premix

Number of tests: 7
Number of candles needed: 4 Schumacher
Flyash used: about 100 lb
On-line testing time: 84 hours
Total test period: 10 working days

7. PULSE INTENSITY TESTS

Objective: Determine impact of pulse intensity on cleaning

Conditions:

Selected from prior tests
All with Schumacher candles

Test Parameters:

Flyash
Pulse conditions (pulse tank pressure and pulse valve open time
-- pulse gas delivery quantity and backflow velocity)

Evaluation: Pressure drop recovery vs pulse conditions

Test Matrix:

Flyash	Tank pressure	Valve open time
Tidd	Base (Test 2)	t1
Tidd	P2	t2
Tidd	P3	t3
Tidd	P4	t4
Karhula	Base (Test 2)	t1
Karhula	P2	t2
Karhula	P3	t3
Karhula	P4	t4

Procedure:

Step 1

- 1.1 - Heat up filter vessel, with no flyash feed, to temperature showing "unstable cake permeability in Test 1.
- 1.2 - Build cake on candles to same ΔP measured in Test 1.
- 1.3 - Hold, without flyash feeding, till steady-state.
- 1.4 - Pulse clean 3 times, at 5 minute intervals.

Step 2

- 2.1 - Cool filter cake to the temperature of step 1.
- 2.2 - Pulse clean 3 times at 5 min intervals.

Parametrics: Repeat sequence for each set of parameters.

Final: Cool down without pulse cleaning before each change of candles, remove the candles and observe the appearance of the filter cake (photograph, measure thickness and morphology, sample bulk density)

Number of tests: 8

Number of candles needed: 4 Schumacher

Flyash used: about 100 lb

On-line testing time: 96 hours

Total test period: 12 working days

8. CONTINUOUS OPERATION TESTS

Objective: Perform longer-term, continuous testing to confirm performance

Conditions: Selected from prior testing
3 run conditions
48 hour operation

Procedure: Normal, steady operation conditions

Number of tests: 3

Number of candles: 12

Flyash used: about 600 to 1200 lb

On-line testing time: 144 hours

Total test period (24 hr days): 12 working days

8. SULFUR /ALKALI REMOVAL TESTS

Objective: Determine ability for in-filter sulfur/alkali removal
Determine impact on filter cake cleaning

Conditions: Selected from prior testing (all at 1550°F cake)
Dual natural gas/coal combustion
No additives with sulfur sorbent
Potential additives with alkali sorbent

Procedures: Normal flyash feeding and filter performance monitoring
Separate sulfur sorbent (dolomite) tests (5 tests)
Separate alkali sorbent (emathlite) tests (3 tests)
Combined sulfur and alkali removal tests (2 tests)

Parameters: Sulfur sorbent rate
Alkali sorbent rate

Number of tests: 10

Number of candles: 4 Schumacher

On-line testing time: 120 hours

Total test period (24 hr days): 12 working days

9. TEST PROGRAM SUMMARY

Total on-line time: 624 hours

Total test days: 80 days

Total test schedule period: 6 months

Candles needed: 30 Schumacher, 10 Coors, 10 Refractron

Flyash needed: 500-1000 lb Tidd, 100 - 500 lb Grimethorpe, 200 - 700 lb Karhula (flyash recycle will be required if sufficient flyash cannot be obtained).

Program Activities:

- Modify test facility
- Procure materials
 - 50 candles
 - flyash supply
- Conduct tests
- Data evaluation
- Program management and reporting

**DATE
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10 / 18 / 93

END