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**RICE:
A Computer Program for Multicomponent
Chemically Reactive Flows at A⁺ Speeds**

by

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MASTER



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RICE: A COMPUTER PROGRAM FOR MULTICOMPONENT
CHEMICALLY REACTIVE FLOWS AT ALL SPEEDS

by

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ABSTRACT

The fluid dynamics of chemically reactive mixtures are calculated at arbitrary flow speeds with the RICE program. The dynamics are governed by the two-dimensional, time-dependent Navier-Stokes equations together with the species transport equations and the mass-action rate equations for the chemical reactions. The mass and momentum equations for the mixture are solved implicitly by the ICE technique. The equations for total energy and species transport are solved explicitly while the chemical rate equations are solved implicitly with a time step that may be a submultiple of the hydrodynamic time step. Application is made to continuous wave HF chemical lasers to compute the supersonic mixing and chemical reactions that take place in the lasing cavity.

1. INTRODUCTION

The RICE computer program has been written to study the two-dimensional dynamics of multicomponent flows with chemical reactions. The program has been applied principally to investigate the species mixing and chemical reactions that take place in the cavities of continuous flow chemical lasers. In this application, supersonic streams of reactants, which may either be impinging or flowing parallel to one another, mix under the action of molecular and turbulent diffusion and react exothermally to produce vibrationally excited species that serve as the lasing medium. The RICE program has also been applied to incompressible flows, to deflagration and detonation waves, and to the turbulent mixing of supersonic streams.¹

RICE solves the full, two-dimensional Navier-Stokes equations by the Implicit Continuous-fluid Eulerian (ICE) solution method.² The implicit solution procedure for the mass and momentum equations for the mixture uses a different technique for the pressure iteration than is described in Ref. 2. In

place of solving a Poisson equation for the pressure field, a relaxation technique, devised by Chorin³ and modified by Hirt and Cook,⁴ is used. This procedure provides a more convenient treatment for the boundary conditions. An explicit solution of the total energy equation follows the solution of the mass and momentum equations. The species transport equations use Fick's law⁵ to model the effects of molecular diffusion. Separate transport equations are solved explicitly for each species. The effects of nonequilibrium chemical reactions are described through an implicit solution of the mass-action rate equations with generalized Arrhenius kinetics. The total energy equation includes the effects of the energy flux due to species diffusion and of the heats of formation from the chemical reactions.

The differential equations that govern the dynamics are given in Sec. II. The finite difference equations and the solution method are described in Sec. III. The initial and boundary conditions and numerical stability are also discussed in this

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section. A method that provides a considerable increase in accuracy for the same computational mesh and significantly decreases the computational time is described in Ref. 6.

The computer program is described in Sec. IV. Card by card descriptions of the input data are given. The FORTRAN symbols, flow diagrams, and FORTRAN listing are given in Appendixes A-C.

A comprehensive example problem is solved in Sec. V. The fluid dynamics, species mixing, and chemical reactions that take place in the cavity of a continuous flow chemical laser are calculated to illustrate the features of the code. The input data is prepared in detail and samples of the various printed and plotted output are shown.

II. THE MATHEMATICAL MODEL

The differential equations that govern the fluid dynamics, species mixing, and chemical reactions are presented in this section. The equations are written in cylindrical coordinates with axial symmetry and zero azimuthal velocity. The equations for plane coordinates are obtained by setting the radial distance r equal to unity and the normal stress component $\sigma_{\phi\phi}$ equal to zero.

A. Mixture Equations

The motion of the fluid mixture is governed by the equations for mass, momentum, and energy conservation. These are the continuity equation,

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial \rho v r}{\partial r} + \frac{\partial \rho u}{\partial z} = 0, \quad (2.1)$$

the usual Navier-Stokes equations,

$$\frac{\partial \rho v}{\partial t} + \frac{1}{r} \frac{\partial \rho v^2 r}{\partial r} + \frac{\partial \rho u v}{\partial z} = -\frac{\partial p}{\partial r} + \frac{1}{r} \frac{\partial \sigma_{rr} r}{\partial r} + \frac{\partial \sigma_{rz}}{\partial z} - \frac{\sigma_{\phi\phi}}{r} \quad (2.2)$$

$$\frac{\partial \rho u}{\partial t} + \frac{1}{r} \frac{\partial \rho u v r}{\partial r} + \frac{\partial \rho u^2}{\partial z} = -\frac{\partial p}{\partial z} + \frac{1}{r} \frac{\partial \sigma_{rz} r}{\partial r} + \frac{\partial \sigma_{zz}}{\partial z}, \quad (2.3)$$

and the energy equation,

$$\frac{\partial \rho E}{\partial t} + \frac{1}{r} \frac{\partial \rho E v r}{\partial r} + \frac{\partial \rho E u}{\partial z} = -\frac{1}{r} \frac{\partial p v r}{\partial r} - \frac{\partial p u}{\partial z} + \frac{1}{r} \frac{\partial}{\partial r} (\sigma_{rr} v r + \sigma_{rz} u r) + \frac{\partial}{\partial z} (\sigma_{rz} v + \sigma_{zz} u)$$

$$- \frac{1}{r} \frac{\partial r q_r}{\partial r} - \frac{\partial q_z}{\partial z} + \dot{q}_c. \quad (2.4)$$

In these equations, ρ is the density; v and u are the velocity components in the r and z directions respectively; p is the pressure; σ_{rr} , σ_{rz} , $\sigma_{\phi\phi}$, and σ_{zz} are the components of viscous stress; E is the specific total energy given by

$$E = 1/2 (u^2 + v^2) + i \quad (2.5)$$

where i is the specific internal energy; q_r and q_z are the r and z components of energy flux due to heat conduction and species diffusion; and \dot{q}_c is the rate of energy release from chemical reactions.

The constitutive equation for a Newtonian fluid relates the viscous stress tensor to the rate of strain tensor:

$$\sigma_{rr} = 2\mu \frac{\partial v}{\partial r} + \lambda \left(\frac{1}{r} \frac{\partial v r}{\partial r} + \frac{\partial u}{\partial z} \right)$$

$$\sigma_{rz} = \mu \left(\frac{\partial u}{\partial r} + \frac{\partial v}{\partial z} \right)$$

(2.6)

$$\sigma_{zz} = 2\mu \frac{\partial u}{\partial z} + \lambda \left(\frac{1}{r} \frac{\partial v r}{\partial r} + \frac{\partial u}{\partial z} \right)$$

$$\sigma_{\phi\phi} = 2\mu \frac{v}{r} + \lambda \left(\frac{1}{r} \frac{\partial v r}{\partial r} + \frac{\partial u}{\partial z} \right),$$

where μ and λ are the first and second coefficients of viscosity.

The energy flux components q_r and q_z are given by

$$q_r = -\kappa \frac{\partial T}{\partial r} - \sum_k \rho h_k D_k \frac{\partial (c_k / \rho)}{\partial r},$$

and

$$q_z = -\kappa \frac{\partial T}{\partial z} - \sum_k \rho h_k D_k \frac{\partial (c_k / \rho)}{\partial z}, \quad (2.7)$$

where κ is the thermal conductivity of the mixture, T is the temperature, h_k is the specific enthalpy of species k , D_k is the effective binary diffusion coefficient for species k into the mixture, and ρ_k is the density of species k . The first term in Eq. (2.7) is the energy flux due to thermal

conductivity, while the second term is the flux due to the interdiffusion of the species. For this latter term, Fick's law is used to describe the effects of ordinary diffusion which is the only mixing mechanism considered. Other mixing mechanisms associated with pressure and temperature gradients are generally small compared to ordinary diffusion for continuous flow chemical laser systems.

The rate of energy release from chemical reactions \dot{q}_c is defined in Sec. II.C.

The caloric equation of state of the mixture that expresses the pressure as a function of the density and specific internal energy is arbitrary. In this report the perfect gas relation,

$$p = (\gamma - 1) \rho I, \quad (2.8)$$

is used, where γ is the specific heat ratio $\gamma = C_p/C_v$. The specific heats of the fluid mixture at constant pressure and constant volume are given by

$$C_p = \rho^{-1} \sum_k (C_p)_k \rho_k$$

and (2.9)

$$C_v = \rho^{-1} \sum_k (C_v)_k \rho_k$$

where $(C_p)_k$ and $(C_v)_k$ are the constant specific heats for species k at constant pressure and constant volume, respectively.

B. Species Transport Equations

The motions of the individual species are determined through the species transport equations:

$$\frac{\partial \rho_k}{\partial t} + \frac{1}{r} \frac{\partial \rho_k v r}{\partial r} + \frac{\partial \rho_k u}{\partial z} = \frac{1}{r} \frac{\partial}{\partial r} \left[\rho D_k r \frac{\partial (\rho_k / \rho)}{\partial r} \right] + \frac{\partial}{\partial z} \left[\rho D_k \frac{\partial (\rho_k / \rho)}{\partial z} \right] + (\dot{\rho}_k)_c, \quad (2.10)$$

where $(\dot{\rho}_k)_c$ is the rate of change of the density of species k from chemical reactions and is defined in Sec. II.C. As in Eq. (2.7), ordinary diffusion, described by Fick's law, is the only mixing mechanism considered.

Mass conservation requires that the sum of the species densities should equal the density of the mixture, i.e.,

$$\rho = \sum_k \rho_k. \quad (2.11)$$

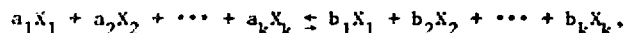
If we sum Eq. (2.10) over all the species and use Eq. (2.11) with the mixture continuity equation, Eq. (2.1), we obtain the result that

$$\sum_k \left\{ \frac{1}{r} \frac{\partial}{\partial r} \left[\rho D_k r \frac{\partial (\rho_k / \rho)}{\partial r} \right] + \frac{\partial}{\partial z} \left[\rho D_k \frac{\partial (\rho_k / \rho)}{\partial z} \right] \right\} = 0, \quad (2.12)$$

since mass is neither created nor destroyed by chemistry. In other words, Eq. (2.12) states that molecular diffusion alone produces no net mass transfer, hence no change in the mixture density. Equation (2.12) is identically satisfied when D_k is the same for all species. In general, however, this is not the case and Eq. (2.12) is viewed as a constraint on the diffusion coefficients.

C. Chemistry Equations

The equations that govern the finite rate chemical reactions are described in this section. A chemical reaction is written as



where X_k represents the chemical species and a_k and b_k are the dimensionless stoichiometric coefficients, some of which may be zero. In the example, X_1 through X_4 correspond to $F, H_2, HF,$ and H respectively, while

$$a_k = [1, 1, 0, 0] \text{ and } b_k = [0, 0, 1, 1].$$

The rates at which species concentrations are changing during the reaction are proportional to one another according to the law of definite proportions. For Eq. (2.13), the law of definite proportions is written as

$$\frac{\dot{\rho}_1}{M_1(b_1 - a_1)} = \frac{\dot{\rho}_2}{M_2(b_2 - a_2)} = \frac{\dot{\rho}_k}{M_k(b_k - a_k)}, \quad (2.14)$$

where M_k is the molecular weight of species k . Equation (2.14) provides a natural definition for the reaction progress variable ω ,

$$\dot{\omega} \equiv \frac{\dot{\rho}_k}{M_k (b_k - a_k)} \quad (2.15)$$

The reaction rate is defined as the rate of change of ω . The dependence of the reaction rate upon the species concentrations and thermodynamic state is expressed by the dilute-gas or mass-action rate so that

$$\dot{\omega} = K_f \prod_k (\rho_k/M_k)^{a_k} - K_b \prod_k (\rho_k/M_k)^{b_k}, \quad (2.16)$$

where K_f and K_b are the rate multipliers for the forward and backward reactions. The rate multipliers have the form

$$K_f \text{ or } K_b = CT^\gamma e^{-E^\pm/T} \quad (2.17)$$

with constants C , γ , and E^\pm which is the ratio of the activation energy to the universal gas constant R . The constants are generally different for the forward and backward reactions. With $\gamma = 0$, Eq. (2.17) reduces to the Arrhenius form.

The rate of energy release \dot{q}_c from a chemical reaction is given by

$$\dot{q}_c = q\dot{\omega}, \quad (2.18)$$

where q is the heat of reaction which is positive for exothermic reactions and negative for endothermic reactions. The rate of change of the density of species k from a chemical reaction is obtained from Eqs. (2.15) and (2.16),

$$(\dot{\rho}_k)_c = M_k (b_k - a_k)\dot{\omega}. \quad (2.19)$$

In the presence of several chemical reactions, the net rate of energy release and the net rate of change of species densities are simply the sum of the rates for each reaction.

III. THE FINITE DIFFERENCE EQUATIONS AND NUMERICAL METHOD

The purpose of this section is to define the finite difference equations that are used to approximate the differential equations presented in Sec. II and to describe the numerical method for their solution. The solution method is based on the ICE technique. It is quite general and permits the solution of a variety of different flows ranging from very compressible to completely incompressible. For incompressible flows the method reduces to the Simplified Marker and Cell Method.⁷

Equations (2.1) to (2.4) are written in a more general form than those in Ref. 2 in order to incorporate variable coefficients of viscosity and thermal conductivity and to include the additional effects of species diffusion and chemical reactions in the energy equation. The method of solution is altered slightly to include these effects and to incorporate a different iteration procedure for the pressure and velocity field that simplifies the inclusion of various boundary conditions. This new iteration scheme is equivalent to that in Ref. 2.

The flow region of interest is divided into a large number of finite-size, space-fixed, rectangular zones called cells. Collectively, these cells form the computing mesh over which the finite difference equations are to be solved. Figure 1 shows a typical computational cell and the locations of

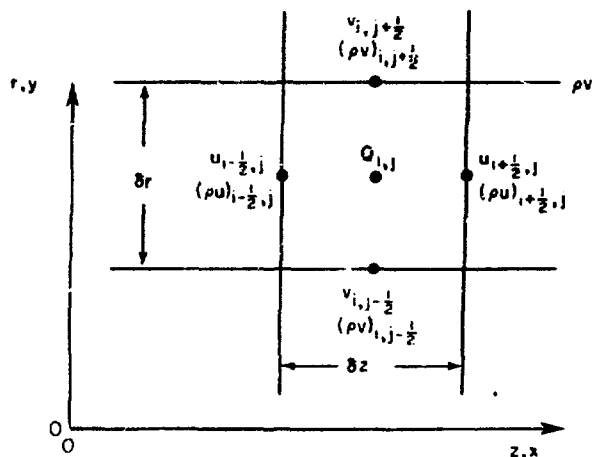


Fig. 1. A typical computational cell and the locations of the variables that appear in the finite difference equations.

the variables that appear in the finite difference equations.

The components of velocity and momentum density are centered on the boundaries between cells as indicated, and $Q_{i,j}$ represents cell-centered quantities such as ρ , ρE , c^2 , $p(\bar{p})$, I , μ , λ , κ , D_k , and ρ_k where c is the adiabatic sound speed and \bar{p} is a pressure that is defined later.

The solution is accomplished by algebraically solving the finite difference equations over a time step δt . The solution at time $t = \delta t$ is calculated using the specified initial conditions at time $t = 0$. In general, the solution at $t = (n+1)\delta t$ is calculated using the solution at $t = n\delta t$.

A. Mass and Momentum

The finite difference approximation to the continuity equation for the mixture, Eq. (2.1), is written as

$$\begin{aligned} \rho_{i,j}^{n+1} = & \tilde{\rho}_{i,j} + \theta \delta t \left\{ \frac{1}{r_j \delta r} \left[(\rho v)_{i,j-\frac{1}{2}}^{n+1} r_{j-\frac{1}{2}} \right. \right. \\ & \left. \left. - (\rho v)_{i,j+\frac{1}{2}}^{n+1} r_{j+\frac{1}{2}} \right] + \frac{1}{\delta z} \left[(\rho u)_{i-\frac{1}{2},j}^{n+1} - (\rho u)_{i+\frac{1}{2},j}^{n+1} \right] \right\} \end{aligned} \quad (3.1)$$

where the components of momentum density at time level $(n+1)$ are defined later and $\tilde{\rho}_{i,j}$ is determined from quantities at time level n :

$$\begin{aligned} \tilde{\rho}_{i,j} = & \rho_{i,j}^n + \delta t \left\{ (1-\theta) \left[\frac{1}{r_j \delta r} \left[(\rho v)_{i,j-\frac{1}{2}}^n r_{j-\frac{1}{2}} \right. \right. \right. \\ & \left. \left. - (\rho v)_{i,j+\frac{1}{2}}^n r_{j+\frac{1}{2}} \right] + \frac{1}{\delta z} \left[(\rho u)_{i-\frac{1}{2},j}^n - (\rho u)_{i+\frac{1}{2},j}^n \right] \right\} \\ & + \frac{1}{r_j (\delta r)^2} \left[r_{j+\frac{1}{2}} \tau_{i,j+\frac{1}{2}} \left(\rho_{i,j+1}^n - \rho_{i,j}^n \right) \right. \\ & \left. - r_{j-\frac{1}{2}} \tau_{i,j-\frac{1}{2}} \left(\rho_{i,j}^n - \rho_{i,j-1}^n \right) \right] \\ & + \frac{1}{(\delta z)^2} \left[\tau_{i+\frac{1}{2},j} \left(\rho_{i+1,j}^n - \rho_{i,j}^n \right) \right. \\ & \left. - \tau_{i-\frac{1}{2},j} \left(\rho_{i,j}^n - \rho_{i-1,j}^n \right) \right] \end{aligned} \quad (3.2)$$

In these equations θ is a parameter used to vary the relative time centering of the convection terms. It

ranges in value from zero for a purely explicit calculation to 1.0 for a completely time advanced treatment of the convection terms. A value $\theta = 0.5$ is usually chosen for most compressible flow calculations because this value time centers the terms and eliminates first order time errors that arise in the difference procedure.

The diffusion terms in Eq. (3.2), i.e., the terms involving τ , are added to cancel low order diffusional truncation errors. These errors, when left alone, can lead to numerical instability. The τ terms are calculated from the values of τ' given by

$$\begin{aligned} (\tau')_{i,j+\frac{1}{2}} = & -(2\theta - 1) \frac{\delta t}{2} \left\{ \left(v_{i,j+\frac{1}{2}}^n \right)^2 + \frac{1}{2} \left[(c^2)_{i,j}^n \right. \right. \\ & \left. \left. + (c^2)_{i,j+1}^n \right] \right\} \\ & + \frac{\delta r}{8 r_{j+\frac{1}{2}}} \left(r_{j+3/2} v_{i,j+3/2}^n - r_{j-\frac{1}{2}} v_{i,j-\frac{1}{2}}^n \right), \end{aligned} \quad (3.3)$$

$$\begin{aligned} (\tau')_{i+\frac{1}{2},j} = & -(2\theta - 1) \frac{\delta t}{2} \left\{ \left(u_{i+\frac{1}{2},j}^n \right)^2 + \frac{1}{2} \left[(c^2)_{i,j}^n \right. \right. \\ & \left. \left. + (c^2)_{i+1,j}^n \right] \right\} \\ & + \frac{\delta z}{8} \left(u_{i+3/2,j}^n - u_{i-\frac{1}{2},j}^n \right), \end{aligned} \quad (3.4)$$

where the square of the adiabatic sound speed is $c^2 = \gamma(\gamma - 1)I$ for a perfect gas. The value of τ is determined from the algebraic sign of τ' ,

$$\tau_{i,j+\frac{1}{2}} = \begin{cases} (1 + \xi) (\tau')_{i,j+\frac{1}{2}} & \text{if } (\tau')_{i,j+\frac{1}{2}} \geq 0 \\ (1 - \xi) (\tau')_{i,j+\frac{1}{2}} & \text{if } (\tau')_{i,j+\frac{1}{2}} < 0, \end{cases} \quad (3.5)$$

where ξ is a constant ranging between zero and unity. The other values of τ' and τ are found similarly.

This procedure of variable coefficients of diffusion has proven very successful over a variety of problems tested. It has obvious advantages over the scheme originally proposed for the ICE method be-

cause it automatically supplies just the amount of diffusion required to stabilize the computational scheme and applies it only in regions where it is necessary. The extension of this procedure to the full set of field equations is described in Ref. 6.

The finite difference approximations to the momentum equations, Eqs. (2.2) and (2.3), are written as

$$(\rho v)_{i,j+\frac{1}{2}}^{n+1} = (\tilde{\rho v})_{i,j+\frac{1}{2}} + \frac{\Delta \delta t}{\delta r} \delta \bar{p}_{i,j} \quad (3.6)$$

and

$$(\rho u)_{i+\frac{1}{2},j}^{n+1} = (\tilde{\rho u})_{i+\frac{1}{2},j} + \frac{\phi \delta t}{\delta z} \delta \bar{p}_{i,j}, \quad (3.7)$$

where the tilde values of momentum density are computed from quantities at time level n , and where $\delta \bar{p}_{i,j}$ is obtained by iterating on the condition that the finite difference approximation to the continuity equation, Eq. (3.1), is satisfied to within a specified deviation from zero. The iteration procedure for determining $\delta \bar{p}_{i,j}$ is described later. The role of ϕ is similar to that of θ in Eq. (3.1). The tilde values of momentum density are given by

$$\begin{aligned} (\tilde{\rho v})_{i,j+\frac{1}{2}} = & (\rho v)_{i,j+\frac{1}{2}}^n + \delta t \left[\frac{1}{r_{j+\frac{1}{2}} \delta r} \left\{ r_j \left[(\rho v)^2_{i,j} - (\sigma_{rr})_{i,j} \right] - r_{j+1} \left[(\rho v)^2_{i,j+1} - (\sigma_{rr})_{i,j+1} \right] \right\} \right. \\ & + \frac{1}{\delta z} \left[(\rho uv)_{i-\frac{1}{2},j+\frac{1}{2}} - (\sigma_{rz})_{i-\frac{1}{2},j+\frac{1}{2}} - (\rho uv)_{i+\frac{1}{2},j+\frac{1}{2}} + (\sigma_{rz})_{i+\frac{1}{2},j+\frac{1}{2}} \right] + \frac{1}{\delta r} (p_{i,j}^n - p_{i,j+1}^n) \\ & \left. - \frac{1}{r_{j+\frac{1}{2}}} (\sigma_{\phi\phi})_{i,j+\frac{1}{2}} \right], \end{aligned} \quad (3.8)$$

and

$$\begin{aligned} (\tilde{\rho u})_{i+\frac{1}{2},j} = & (\rho u)_{i+\frac{1}{2},j}^n + \delta t \left[\frac{1}{r_j \delta r} \left\{ r_{j-\frac{1}{2}} \left[(\rho uv)_{i+\frac{1}{2},j-\frac{1}{2}} - (\sigma_{rz})_{i+\frac{1}{2},j-\frac{1}{2}} \right] - r_{j+\frac{1}{2}} \left[(\rho uv)_{i+\frac{1}{2},j+\frac{1}{2}} - (\sigma_{rz})_{i+\frac{1}{2},j+\frac{1}{2}} \right] \right\} \right. \\ & \left. + \frac{1}{\delta z} \left[(\rho u^2)_{i,j} - (\sigma_{zz})_{i,j} - (\rho u^2)_{i+1,j} + (\sigma_{zz})_{i+1,j} + p_{i,j}^n - p_{i+1,j}^n \right] \right]. \end{aligned} \quad (3.9)$$

In Eqs. (3.8) and (3.9) straightforward centered differences are used for the various terms. Typical terms are given by

$$\begin{aligned} (\rho v^2)_{i,j} &= \frac{1}{4} \rho_{i,j}^n (v_{i,j+\frac{1}{2}}^n + v_{i,j-\frac{1}{2}}^n)^2, \\ (\sigma_{rr})_{i,j} &= \frac{2}{\delta r} u_{i,j}^2 (v_{i,j+\frac{1}{2}}^n - v_{i,j-\frac{1}{2}}^n) \\ &+ \lambda_{i,j}^n \left[\frac{1}{r_j \delta r} (r_{j+\frac{1}{2}} v_{i,j+\frac{1}{2}}^n \right. \\ &\left. - r_{j-\frac{1}{2}} v_{i,j-\frac{1}{2}}^n) + \frac{1}{\delta z} (u_{i+\frac{1}{2},j}^n - u_{i-\frac{1}{2},j}^n) \right], \\ (\rho uv)_{i-\frac{1}{2},j+\frac{1}{2}} &= \frac{1}{16} (\rho_{i,j}^n + \rho_{i,j+1}^n + \rho_{i-1,j+1}^n \\ &+ \rho_{i-1,j}^n) (u_{i-\frac{1}{2},j}^n \\ &+ u_{i-\frac{1}{2},j+1}^n) (v_{i,j+\frac{1}{2}}^n + v_{i-1,j+\frac{1}{2}}^n), \end{aligned}$$

$$\begin{aligned}
(\sigma_{rz})_{i-\frac{1}{2},j+\frac{1}{2}} &= \frac{1}{4} (u_{i,j}^n + u_{i,j+1}^n + u_{i-1,j+1}^n \\
&+ u_{i-1,j}^n) \left[\frac{1}{\delta r} (u_{i-\frac{1}{2},j+1}^n - u_{i-\frac{1}{2},j}^n) \right. \\
&+ \left. \frac{1}{\delta z} (v_{i,j+\frac{1}{2}}^n - v_{i-1,j+\frac{1}{2}}^n) \right], \\
(\rho v)_{i,j+\frac{1}{2}} &= \frac{1}{r_{j+\frac{1}{2}}} (u_{i,j}^n + u_{i,j+1}^n) v_{i,j+\frac{1}{2}}^n + \frac{1}{4} (\lambda_{i,j}^n \\
&+ \lambda_{i,j+1}^n) \left[\frac{1}{r_{j+\frac{1}{2}} \delta r} (r_{j+1} (v_{i,j+\frac{3}{2}}^n \right. \\
&+ v_{i,j+\frac{1}{2}}^n) - r_j (v_{i,j+\frac{1}{2}}^n + v_{i,j-\frac{1}{2}}^n)) \right] \\
&+ \frac{1}{\delta z} \left[(u_{i+\frac{1}{2},j}^n + u_{i+\frac{1}{2},j+1}^n) - (u_{i-\frac{1}{2},j}^n \right. \\
&+ u_{i-\frac{1}{2},j+1}^n) \left. \right].
\end{aligned}$$

$$(\rho u^2)_{i,j} = \frac{1}{4} \lambda_{i,j}^n (u_{i+\frac{1}{2},j}^n + u_{i-\frac{1}{2},j}^n)^2.$$

The remaining terms in Eqs. (3.8) and (3.9) are defined similarly.

The viscosity coefficients are variables here rather than constants as they were in the original formulation of the ICE method. This proves very helpful in problems for which the variation of viscosity with temperature is important and, as shown later, for inserting the appropriate viscosity values into the equations to maintain numerical stability.

The solution of Eqs. (3.1), (3.6), and (3.7) for $c_{i,j}^{n+1}$, $(\rho v)_{i,j+\frac{1}{2}}^{n+1}$, and $(\rho u)_{i+\frac{1}{2},j}^{n+1}$ is accomplished by iterating on the pressure $\bar{p}_{i,j} = p_{i,j}^n + \delta \bar{p}_{i,j}$. The original ICE method obtained the \bar{p} pressure field by solving a Poisson equation and from this the mass and momentum densities were determined. The iteration procedure in RICE that simultaneously solves for the \bar{p} pressure and mass and momentum densities is desirable for the ease with which different boundary conditions can be incorporated into the computer program.

The criterion for convergence of the iteration procedure is that the continuity equation, Eq. (3.1), is satisfied to within a specified small amount ϵ , i.e., Eq. (3.1) is written as

$$\begin{aligned}
D &= \rho_{i,j}^{n+1} - \bar{\rho}_{i,j} - \delta t \left[\frac{1}{r_j \delta r} \left\{ (\rho v)_{i,j-\frac{1}{2}}^{n+1} r_{j-\frac{1}{2}} \right. \right. \\
&- \left. \left. (\rho v)_{i,j+\frac{1}{2}}^{n+1} r_{j+\frac{1}{2}} \right\} + \frac{1}{\delta z} \left\{ (\rho u)_{i-\frac{1}{2},j}^{n+1} - (\rho u)_{i+\frac{1}{2},j}^{n+1} \right\} \right],
\end{aligned} \quad (3.10)$$

and the convergence requirement is $|D| < \epsilon$. The procedure is begun by estimating the mass and momentum densities at time level $(n+1)$ as the mass density at time level n and the tile values of momentum density, but the choice is arbitrary.

If the convergence criterion $|D| < \epsilon$ is satisfied, the quantities in cell (i,j) are not changed. If however, the criterion is not satisfied, the pressure is changed by an amount

$$\delta \bar{p}_{i,j} = - \Omega D / \left[1 / (c^2)_{i,j}^n + 2 \delta t^2 (\delta r^{-2} + \delta z^{-2}) \right], \quad (3.11)$$

$$\text{i.e., } \bar{p}_{i,j} \leftarrow \bar{p}_{i,j} + \delta \bar{p}_{i,j}, \quad (3.12)$$

where Ω is a constant over-relaxation factor usually chosen between 1.0 and 1.8. At the start of the iteration $\bar{p}_{i,j} = p_{i,j}^n$. The choice for the value of Ω is problem-dependent to some extent. If the flow is rather compressible with Mach number greater than unity, good predictions of $\delta \bar{p}$ are obtained for $\Omega = 1$. For very small values of the Mach number, Ω greater than 1.5 produces the most rapid convergence.

When the \bar{p} pressure is changed according to Eq. (3.11) the mass and momentum densities are also changed as follows

$$\rho_{i,j}^{n+1} \leftarrow \rho_{i,j}^{n+1} + \delta \bar{p}_{i,j} / (c^2)_{i,j},$$

$$(\rho u)_{i+\frac{1}{2},j}^{n+1} \leftarrow (\rho u)_{i+\frac{1}{2},j}^{n+1} + \frac{\delta \bar{p}}{\delta z} \delta \bar{p}_{i,j},$$

$$(\rho u)_{i-\frac{1}{2},j}^{n+1} \leftarrow (\rho u)_{i-\frac{1}{2},j}^{n+1} - \frac{\delta \bar{p}}{\delta z} \delta \bar{p}_{i,j},$$

$$(\rho v)_{i,j+\frac{1}{2}}^{n+1} \leftarrow (\rho v)_{i,j+\frac{1}{2}}^{n+1} + \frac{\delta \bar{p}}{\delta r} \delta \bar{p}_{i,j},$$

$$(\rho v)_{i,j-\frac{1}{2}}^{n+1} \leftarrow (\rho v)_{i,j-\frac{1}{2}}^{n+1} - \frac{\phi \delta t}{\delta r} \delta \bar{p}_{i,j}. \quad (3.13)$$

This process is repeated in all computing cells until $|D| < \epsilon$ in every cell of the computing mesh.

When the convergence criterion is satisfied for every cell, the values of the mass and momentum densities are the solution values at time level $(n+1)$. In addition, the \bar{p} pressure field is an intermediate pressure that reflects the density at time level $(n+1)$ and the specific internal energy at time level (n) . The velocities are obtained from the mass and momentum densities as

$$u_{i+\frac{1}{2},j}^{n+1} = 2(\rho u)_{i+\frac{1}{2},j}^{n+1} / (\rho_{i,j}^{n+1} + \rho_{i+1,j}^{n+1}),$$

$$v_{i,j+\frac{1}{2}}^{n+1} = 2(\rho v)_{i,j+\frac{1}{2}}^{n+1} / (\rho_{i,j}^{n+1} + \rho_{i,j+1}^{n+1}). \quad (3.14)$$

B. Total Energy

The velocity components of the mixture at time level $(n+1)$ obtained after the iteration procedure are used for the explicit calculation of the total energy density. An intermediate value (ρE) of the total energy density is obtained that neglects the effects of species mixing and chemistry in Eq. (2.4). The finite difference equation for (ρE) is

$$(\rho E)_{i,j} = (\rho E)_{i,j}^n + \frac{\delta t}{r_j \delta r} \left[r_{j-\frac{1}{2}} \left\{ v_{i,j-\frac{1}{2}}^{n+1} \left[(\rho E)_{i,j-\frac{1}{2}}^n + \bar{p}_{i,j-\frac{1}{2}} - (\sigma_{rr})_{i,j-\frac{1}{2}} \right] - (\sigma_{rz})_{i,j-\frac{1}{2}} u_{i,j-\frac{1}{2}}^{n+1} - (\hat{\kappa})_{i,j-\frac{1}{2}}^n (I_{i,j}^n - I_{i,j-1}^n) / \delta r \right\} - r_{j+\frac{1}{2}} \left\{ v_{i,j+\frac{1}{2}}^{n+1} \left[(\rho E)_{i,j+\frac{1}{2}}^n + \bar{p}_{i,j+\frac{1}{2}} - (\sigma_{rr})_{i,j+\frac{1}{2}} \right] - (\sigma_{rz})_{i,j+\frac{1}{2}} u_{i,j+\frac{1}{2}}^{n+1} - (\hat{\kappa})_{i,j+\frac{1}{2}}^n (I_{i,j+\frac{1}{2}}^n - I_{i,j}^n) / \delta r \right\} \right] + \frac{\delta t}{\delta z} \left[u_{i-\frac{1}{2},j}^{n+1} \left[(\rho E)_{i-\frac{1}{2},j}^n + \bar{p}_{i-\frac{1}{2},j} - (\sigma_{zz})_{i-\frac{1}{2},j} \right] - (\sigma_{rz})_{i-\frac{1}{2},j} v_{i-\frac{1}{2},j}^{n+1} \right]$$

$$- (\hat{\kappa})_{i-\frac{1}{2},j}^n (I_{i,j}^n - I_{i-1,j}^n) / \delta z$$

$$- \left[u_{i+\frac{1}{2},j}^{n+1} \left[(\rho E)_{i+\frac{1}{2},j}^n + \bar{p}_{i+\frac{1}{2},j} - (\sigma_{zz})_{i+\frac{1}{2},j} \right] - (\sigma_{rz})_{i+\frac{1}{2},j} v_{i+\frac{1}{2},j}^{n+1} - (\hat{\kappa})_{i+\frac{1}{2},j}^n (I_{i+1,j}^n - I_{i,j}^n) / \delta z \right]. \quad (3.15)$$

In this equation all quantities that are required at spatial locations in the mesh other than where they are defined (recall Fig. 1) are obtained by simple averages, e.g.,

$$(\rho E)_{i,j-\frac{1}{2}}^n = 1/2 \left[(\rho E)_{i,j}^n + (\rho E)_{i,j-1}^n \right],$$

$$(\sigma_{rr})_{i,j-\frac{1}{2}} = \frac{1}{2\delta r} (\mu_{i,j}^n + \mu_{i,j-1}^n) (v_{i,j+\frac{1}{2}}^{n+1} - v_{i,j-\frac{1}{2}}^{n+1}) + 1/4 (\lambda_{i,j}^n + \lambda_{i,j-1}^n) \left[\frac{1}{r_{j-\frac{1}{2}} \delta r} (r_{j+\frac{1}{2}} v_{i,j+\frac{1}{2}}^{n+1} - r_{j-\frac{1}{2}} v_{i,j-\frac{1}{2}}^{n+1}) + \frac{1}{\delta z} (u_{i+\frac{1}{2},j}^{n+1} + u_{i-\frac{1}{2},j-1}^{n+1} - u_{i-\frac{1}{2},j}^{n+1} - u_{i-\frac{1}{2},j-1}^{n+1}) \right],$$

and similarly for the other quantities. The energy flux due to thermal conductivity in Eq. (2.7) has been written in terms of gradients of I rather than T , and κ has been replaced by $\hat{\kappa}$ in Eq. (3.15). This gradient transformation is correct only when C_v is a constant and $\hat{\kappa} = \kappa / C_v$. However, since the thermal conduction term is used for numerical stability in Eq. (3.15) the I -gradient form is retained even when C_v is variable. This form allows for a significantly larger time step than would be possible otherwise. Numerical stability is discussed in detail in Sec. III.F.

A tilde value of the specific internal energy is obtained from the tilde value of the total energy density as

$$\tilde{I}_{i,j} = (\tilde{\rho E})_{i,j} / \rho_{i,j}^{n+1} - 1/8 \left[(u_{i+\frac{1}{2},j}^{n+1} + u_{i-\frac{1}{2},j}^{n+1})^2 + (v_{i,j+\frac{1}{2}}^{n+1} + v_{i,j-\frac{1}{2}}^{n+1})^2 \right]. \quad (3.16)$$

For the flow of a single fluid, the tilde values of (ρE) and I are in fact the values at time level $(n+1)$. For multicomponent flows the energy flux due to species diffusion is added to $(\tilde{\rho E})$ after solution of the species transport equations and the energy release (or absorption) from chemical reaction is included after solution of the chemistry equations.

C. Species Transport

The solution procedure for the species transport equations is similar to the procedure used for solution of the total energy equation. A tilde value of species density is obtained by solving the finite-difference approximation to Eq. (2.10) neglecting the species diffusion and chemistry terms. These terms are again treated separately and their respective contributions are added to the tilde value to yield the final species density at time level $(n+1)$. This procedure, while not a necessity in the solution, enables each effect to be handled separately and greatly simplifies the programming of the computer code.

The tilde value of the density of species k is

$$\begin{aligned} (\tilde{\rho}_k)_{i,j} = & (\rho_k)_{i,j}^n + \delta t \left[\frac{1}{r_j \delta r} \left[r_{j-\frac{1}{2}} (\rho_k v)_{i,j-\frac{1}{2}} \right. \right. \\ & - r_{j+\frac{1}{2}} (\rho_k v)_{i,j+\frac{1}{2}} \left. \right] + \frac{1}{\delta z} \left[(\rho_k u)_{i-\frac{1}{2},j} \right. \\ & - (\rho_k u)_{i+\frac{1}{2},j} \left. \right] + \frac{1}{r_j (\delta r)^2} \left[r_{j+\frac{1}{2}} \beta_{i,j+\frac{1}{2}} \left[(\rho_k)_{i,j+1}^n \right. \right. \\ & - (\rho_k)_{i,j}^n \left. \right] - r_{j-\frac{1}{2}} \beta_{i,j-\frac{1}{2}} \left[(\rho_k)_{i,j}^n - (\rho_k)_{i,j-1}^n \right] \left. \right] \\ & + \frac{1}{(\delta z)^2} \left[\beta_{i+\frac{1}{2},j} \left[(\rho_k)_{i+1,j}^n - (\rho_k)_{i,j}^n \right] \right. \\ & \left. - \beta_{i-\frac{1}{2},j} \left[(\rho_k)_{i,j}^n - (\rho_k)_{i-1,j}^n \right] \right] \left. \right], \quad (3.17) \end{aligned}$$

where interpolated donor cell differencing is used for the convection terms such that

$$\begin{aligned} (\rho_k v)_{i,j-\frac{1}{2}} = & 1/2 \left[(\rho_k)_{i,j}^n + (\rho_k)_{i,j-1}^n - \frac{\delta t}{\delta r} \left[(\rho_k)_{i,j}^n \right. \right. \\ & \left. \left. - (\rho_k)_{i,j-1}^n \right] v_{i,j-\frac{1}{2}}^{n+1} \right] v_{i,j-\frac{1}{2}}^{n+1} \end{aligned}$$

and

$$\begin{aligned} (\rho_k u)_{i-\frac{1}{2},j} = & 1/2 \left[(\rho_k)_{i,j}^n + (\rho_k)_{i-1,j}^n - \frac{\delta t}{\delta z} \left[(\rho_k)_{i,j}^n \right. \right. \\ & \left. \left. - (\rho_k)_{i-1,j}^n \right] u_{i-\frac{1}{2},j}^{n+1} \right] u_{i-\frac{1}{2},j}^{n+1} \quad (3.18) \end{aligned}$$

and similarly for $(\rho_k v)_{i,j+\frac{1}{2}}$ and $(\rho_k u)_{i+\frac{1}{2},j}$. The diffusion terms in Eq. (3.17), i.e., the terms involving β , are added to cancel low order diffusional truncation errors similar to the τ terms in Eq. (3.2). In like manner, the β terms are calculated from the values of the β^* terms given by

$$(\beta^*)_{i,j+\frac{1}{2}} = \frac{\delta r}{8 r_{j+\frac{1}{2}}} (r_{j+\frac{3}{2}} v_{i,j+\frac{3}{2}}^{n+1} - r_{j-\frac{1}{2}} v_{i,j-\frac{1}{2}}^{n+1}),$$

and

$$(\beta^*)_{i+\frac{1}{2},j} = \frac{\delta z}{8} (u_{i+\frac{1}{2},j}^{n+1} - u_{i-\frac{1}{2},j}^{n+1}), \quad (3.19)$$

with

$$\beta_{i,j+\frac{1}{2}} = \begin{cases} (1 + \xi) (\beta^*)_{i,j+\frac{1}{2}} & \text{if } (\beta^*)_{i,j+\frac{1}{2}} \geq 0 \\ (1 - \xi) (\beta^*)_{i,j+\frac{1}{2}} & \text{if } (\beta^*)_{i,j+\frac{1}{2}} < 0, \end{cases} \quad (3.20)$$

where ξ again ranges between zero and unity. The other values of β^* and β are found similarly.

To achieve rigid conservation of mass, i.e., to insure that the mixture density equals the sum of the species densities in a computational cell, the tilde density of the last species is calculated as

$$(\tilde{\rho}_{NS})_{i,j} = \rho_{i,j}^{n+1} - \sum_{k=1}^{NS-1} (\tilde{\rho}_k)_{i,j}, \quad (3.21)$$

where NS is the total number of species. Mass conservation is insured when the sum of the species tilde densities equals the mixture density, since species diffusion and chemistry produce no net mass change. This approach is simple to include in the computer program and has produced excellent results.

The effects of species diffusion are calculated in accord with Eq. (2.10) subject to the constraint that there is no net mass transfer as expressed by Eq. (2.12). This constraint is enforced in the solution algorithm by requiring that there be no net mass transfer across any boundary of the computational cell. In finite difference form this yields the conditions that

$$\begin{aligned} \sum_k (\delta f_k)_{i,j+\frac{1}{2}} &= \sum_k (\delta f_k)_{i-\frac{1}{2},j} = \sum_k (\delta f_k)_{i,j-\frac{1}{2}} \\ &= \sum_k (\delta f_k)_{i+\frac{1}{2},j} = 0, \end{aligned} \quad (3.22)$$

where

$$\begin{aligned} (\delta f_k)_{i,j+\frac{1}{2}} &= 1/4 \left[(D_k)_{i,j} + (D_k)_{i,j+1} \right] (\rho_{i,j}^{n+1}) \\ &\quad + \rho_{i,j+1}^{n+1} \left\{ \left[(\tilde{\rho}_k) / \rho^{n+1} \right]_{i,j+1} \right. \\ &\quad \left. - \left[(\tilde{\rho}_k) / \rho^{n+1} \right]_{i,j} \right\} / \delta r, \\ (\delta f_k)_{i+\frac{1}{2},j} &= 1/4 \left[(D_k)_{i,j} + (D_k)_{i+1,j} \right] (\rho_{i,j}^{n+1}) \\ &\quad + \rho_{i+1,j}^{n+1} \left\{ \left[(\tilde{\rho}_k) / \rho^{n+1} \right]_{i+1,j} \right. \\ &\quad \left. - \left[(\tilde{\rho}_k) / \rho^{n+1} \right]_{i,j} \right\} / \delta z, \end{aligned} \quad (3.23)$$

for the top and right boundaries of the cell with similar expressions for the bottom and left boundaries. The diffusion coefficient $(D_k)_{i,j}$ is evaluated for low density gases as

$$(D_k)_{i,j} = \alpha_k \eta_{i,j},$$

where

$$\alpha_k = (M_H / M_k)^{\frac{1}{2}}, \quad (3.24)$$

and

$$\eta_{i,j} = \eta_0 (T_{i,j})^{\frac{1}{2}} / \left\{ \rho_{i,j}^{n+1} \left[(C_p)_{i,j} - (C_v)_{i,j} \right] \right\}$$

α_k is scaled to the molecular weight of atomic hydrogen, $M_H = 1.0$, and η_0 is a constant. The coefficient α_k describes the dependence of D_k on the molecular weight of species k. This inverse square root dependence is analogous to the dependence of the mean molecular velocity on the molecular weight at constant temperature in kinetic theory. The specific heats are given by Eq. (2.9) as

$$(C_p)_{i,j} = \sum_k (C_p)_k (\tilde{\rho}_k)_{i,j} / \rho_{i,j}^{n+1}$$

$$(C_v)_{i,j} = \sum_k (C_v)_k (\tilde{\rho}_k)_{i,j} / \rho_{i,j}^{n+1}$$

and the temperature as

$$T_{i,j} = \bar{Y}_{i,j} / (C_v)_{i,j}. \quad (3.25)$$

Equation (3.22) is identically satisfied, as is Eq. (2.12), when D_k has the same value for all species. This is the case, to good approximation, when the species have sufficiently similar molecular weights and the mixture density is sufficiently rarefied.

Generally, however, the diffusion coefficients are different for the different species so that Eq. (3.22) is not identically satisfied. If a summation yields a positive value instead of zero, those elements that are positive are reduced in magnitude. On the other hand, if a summation yields a negative value, those elements that are negative are reduced in magnitude. This is accomplished through a reduction factor so that on the top boundary of the cell

$$(\delta f_k^+)_{i,j+\frac{1}{2}} + (\delta f_k^+)_{i,j+\frac{1}{2}} (1 - \Delta/\Delta^+) \text{ for } \Delta \geq 0,$$

or

$$(\delta f_k^-)_{i,j+\frac{1}{2}} + (\delta f_k^-)_{i,j+\frac{1}{2}} (1 - \Delta/\Delta^-) \text{ for } \Delta < 0 \quad (3.26)$$

where $(\delta f_k^+)_{i,j+\frac{1}{2}}$ and $(\delta f_k^-)_{i,j+\frac{1}{2}}$ are the positive and negative elements respectively and Δ represents summations, i.e.,

$$\Delta = \sum_k (\delta f_k)_{i,j+\frac{1}{2}},$$

$$\Delta^+ = \sum_k (\delta f_k^+)_{i,j+\frac{1}{2}}, \quad \Delta^- = \sum_k (\delta f_k^-)_{i,j+\frac{1}{2}}.$$

A similar procedure is used for the right, bottom, and left boundaries.

The species tilde densities are updated to include the effects of molecular diffusion described in Eq. (2.10)

$$\begin{aligned} (\tilde{\rho}_k)_{i,j} &\leftarrow (\tilde{\rho}_k)_{i,j} + \delta t \left[\frac{1}{r_j \delta r} \left[r_{j+\frac{1}{2}} (\delta f_k)_{i,j+\frac{1}{2}} \right. \right. \\ &\quad \left. \left. - r_{j-\frac{1}{2}} (\delta f_k)_{i,j-\frac{1}{2}} \right] + \frac{1}{\delta z} \left[(\delta f_k)_{i+\frac{1}{2},j} \right. \right. \\ &\quad \left. \left. - (\delta f_k)_{i-\frac{1}{2},j} \right] \right], \end{aligned} \quad (3.27)$$

which assures that the mixture density $\rho_{i,j}^{n+1}$ does not change.

The energy flux due to the interdiffusion of the species is described by Eqs. (2.4) and (2.7) and is added to the tilde value of the total energy density as

$$\begin{aligned} (\delta \tilde{E})_{i,j} &\leftarrow (\delta \tilde{E})_{i,j} \\ &+ \delta t \left[\frac{1}{r_j \delta r} \left[r_{j+\frac{1}{2}} \sum_k (C_p)_k T_{i,j+\frac{1}{2}} (\delta f_k)_{i,j+\frac{1}{2}} \right. \right. \\ &\quad \left. \left. - r_{j-\frac{1}{2}} \sum_k (C_p)_k T_{i,j-\frac{1}{2}} (\delta f_k)_{i,j-\frac{1}{2}} \right] \right] \end{aligned}$$

$$\begin{aligned} &+ \frac{1}{\delta z} \left[\sum_k (C_p)_k T_{i+\frac{1}{2},j} (\delta f_k)_{i+\frac{1}{2},j} \right. \\ &\quad \left. - \sum_k (C_p)_k T_{i-\frac{1}{2},j} (\delta f_k)_{i-\frac{1}{2},j} \right] \end{aligned} \quad (3.28)$$

D. Chemistry

The effects of a finite rate chemical reaction on the species densities are described by Eqs. (2.10), (2.16), and (2.19). To determine the progress of the reaction during the computational time step from $t = n\delta t$ to $t = (n+1)\delta t$, Eq. (2.16) is solved. The net effect of several reactions is simply the sum of the effects of each reaction and is discussed at the end of this section.

Equation (2.16) is solved implicitly for the change in concentration of a particular species, designated as the reference species for the reaction. The reference species is chosen automatically by the program as the species with the lowest concentration, i.e., with minimum value of

$|(\tilde{\rho}_k)_{i,j} / M_k^{(b_k - a_k)}|$, and a negative rate of change of concentration. The implicit solution of Eq. (2.16) insures that the concentration of the reference species, and hence the concentrations of the other species, will not be driven negative during the time step δt . In finite difference form Eq. (2.16) is written as

$$\begin{aligned} (\rho_r)_{i,j}^{n+1} / M_r &= \frac{(\tilde{\rho}_r)_{i,j} / M_r + \delta t a_r K_b \prod_{k=1}^{NS} [(\tilde{\rho}_k)_{i,j} / M_k]^{b_k}}{1 + \frac{\delta t a_r M_r K_f}{(\tilde{\rho}_r)_{i,j}} \prod_{k=1}^{NS} [(\tilde{\rho}_k)_{i,j} / M_k]^{a_k}} \\ &\text{for } \dot{\omega} \geq 0 \end{aligned} \quad (3.29)$$

or

$$\begin{aligned} (\rho_r)_{i,j}^{n+1} / M_r &= \frac{(\tilde{\rho}_r)_{i,j} / M_r + \delta t b_r K_f \prod_{k=1}^{NS} [(\tilde{\rho}_k)_{i,j} / M_k]^{a_k}}{1 + \frac{\delta t b_r M_r K_b}{(\tilde{\rho}_r)_{i,j}} \prod_{k=1}^{NS} [(\tilde{\rho}_k)_{i,j} / M_k]^{b_k}} \\ &\text{for } \dot{\omega} < 0 \end{aligned}$$

where subscript r refers to the reference species and $\dot{\omega}$ is evaluated explicitly as

$$\dot{\omega} = K_f \prod_{k=1}^{NS} \left[(\tilde{\rho}_k)_{i,j} / M_k \right]^{a_k} - K_b \prod_{k=1}^{NS} \left[(\tilde{\rho}_k)_{i,j} / M_k \right]^{b_k}. \quad (3.30)$$

The selection of the appropriate reference species is accomplished automatically in the computer program for each computational cell at each time step. The rate multipliers are determined from Eq. (2.17) where the temperature is calculated from Eq. (3.25) using the most updated values of $(\tilde{\rho}_k)_{i,j}$ from Eq. (3.27) and $\tilde{T}_{i,j}$ from Eqs. (3.28) and (3.16).

The final values of the total energy density and the species densities are calculated from the increment in the progress variable ω defined through Eq. (2.15). The progress increment is determined from the solution for the reference species, i.e.,

$$\delta\omega = \left[(\rho_r)_{i,j}^{n+1} - (\tilde{\rho}_r)_{i,j} \right] / \left[M_r (b_r - a_r) \right]. \quad (3.31)$$

The rate of heat release due to chemistry, the last term in Eq. (2.4), is given by Eq. (2.18). Accordingly, the value of the total energy density at time level (n+1) is

$$(\rho E)_{i,j}^{n+1} = (\tilde{\rho E})_{i,j} + q \delta\omega. \quad (3.32)$$

The rate of change of the species densities due to chemistry, the last term in Eq. (2.10), is given by Eq. (2.19) so that the final values of the species densities are

$$(\rho_k)_{i,j}^{n+1} = (\tilde{\rho}_k)_{i,j} + \delta\omega M_k (b_k - a_k). \quad (3.33)$$

When several reactions are occurring simultaneously, a progress increment $\delta\omega_\ell$ is calculated for each reaction. In this case Eqs. (3.32) and (3.33) are replaced by

$$(\rho E)_{i,j}^{n+1} = (\tilde{\rho E})_{i,j} + \sum_{\ell=1}^{NR} q_\ell \delta\omega_\ell, \quad (3.34)$$

and

$$(\rho_k)_{i,j}^{n+1} = (\tilde{\rho}_k)_{i,j} + \sum_{\ell=1}^{NR} \delta\omega_\ell M_k (b_{k\ell} - a_{k\ell}), \quad (3.35)$$

where NR is the total number of reactions.

In certain situations it is necessary to utilize a time step δt_c which is a submultiple of the hydrodynamic time step δt for solution of Eq. (3.29). Such a situation can arise, for example, when a particular species is being consumed in different reactions at different rates or when the characteristic time for the chemistry is fast, but not infinite, compared to the characteristic time for the fluid dynamics. The final solution is obtained by subcycling through Eqs. (3.29) - (3.35) the integral number of times necessary with δt replaced by δt_c .

The computational cycle is completed with the calculation of the final value of the specific internal energy from Eq. (3.16) where $(\rho E)^{n+1}$ is used in place of $(\tilde{\rho E})$ and the final pressure from the equation of state, Eq. (2.8).

$$P_{i,j}^{n+1} = (Y_{i,j}^{n+1} - 1) \rho_{i,j}^{n+1} I_{i,j}^{n+1}, \quad (3.36)$$

where

$$Y_{i,j}^{n+1} = (C_p)_{i,j}^{n+1} / (C_v)_{i,j}^{n+1}$$

and the specific heats are given by Eq. (2.9) as

$$(C_p)_{i,j}^{n+1} = \sum_k (C_p)_k (\rho_k)_{i,j}^{n+1} / \rho_{i,j}^{n+1}$$

$$(C_v)_{i,j}^{n+1} = \sum_k (C_v)_k (\rho_k)_{i,j}^{n+1} / \rho_{i,j}^{n+1}.$$

E. Initial and Boundary Conditions

To begin the solution of the finite difference equations in time, it is necessary to specify a set of initial conditions for each computational cell. Values are required for ρ , u , v , I , and ρ_k , which are the dependent variables in the governing equations. Uniform initial conditions are specified conveniently in the computer program through the input data.

Several different boundary conditions around the perimeter of the computing mesh are programmed:

- 1) No-slip rigid walls,

- 2) Free-slip rigid walls,
- 3) Prescribed input,
- 4) Continuitive output.

For the first two, the rigid walls are also adiabatic or nonconducting. Rigid walls can be specified along any boundary of the computing mesh. The free-slip wall is equivalent to a reflective plane of symmetry. Input can be prescribed anywhere along the left and top boundaries of the mesh with up to two distinct inflow openings on each boundary. Inflow is prescribed along the left boundary by specifying values for ρ , u , $v = 0$, I , and ρ_k and along the top boundary by specifying values for ρ , $u = 0$, v , I , and ρ_k . A continuative output boundary can be prescribed anywhere along the right boundary with up to two distinct openings. The bottom boundary of the computing mesh is either a free-slip or no-slip, adiabatic, rigid wall.

The prescribed boundary conditions are enforced through the use of fictitious cells that surround the computing mesh as shown in Fig. 2. For rigid walls the tangential velocities are set in the fictitious cells according to Fig. 3, which illustrates the situation for the bottom boundary.

The velocities are set similarly for rigid walls along the other boundaries. The velocities are the only quantities that are set in the non-fluid cells. When the value of any quantity is needed on a wall boundary, e.g., the value of u that is required to compute J_{rz} on the bottom boundary for the z-momentum equation, it is obtained

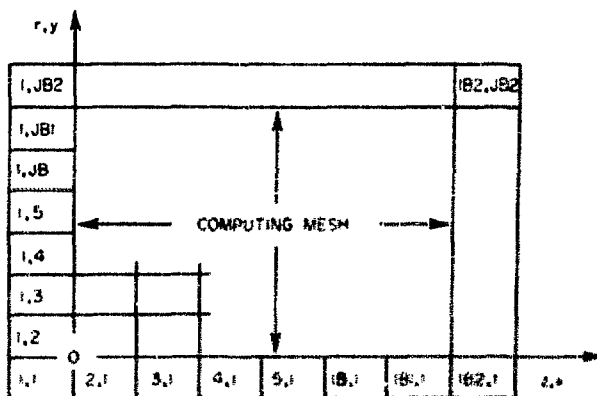


Fig. 2. Computing mesh and surrounding fictitious cells.

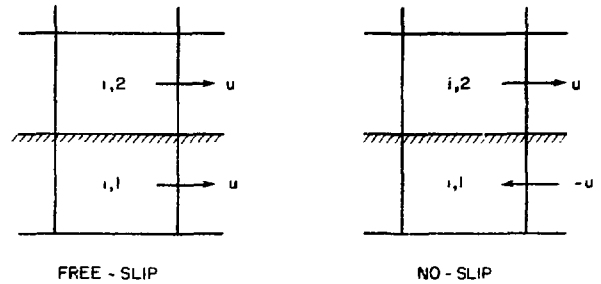


Fig. 3. Velocity boundary conditions for free-slip and no-slip rigid walls.

from averages of the nearby quantities in the fluid.

At an inflow boundary the specified quantities are located on the cell boundary with the u or v components of velocity. Figure 4 shows typical inflow cells along the left and top of the computing mesh. Values of quantities at the center of an inflow cell are obtained by linear extrapolation from their values on the boundary and nearby in the fluid.

The right boundary of the computing mesh can be a continuative outflow boundary, a rigid wall, or a combination with up to two outflow openings. The continuative outflow boundary is gradient-free in the axial direction across columns IB, IB1, and IB2 for all quantities except the velocities.

The boundary conditions that are available around the perimeter of the computing mesh are appropriate for the calculation of a variety of interior flows. The calculation of exterior flows, i.e., flows around obstacles, is also possible with the RICE program through the option of specifying obstacles in the interior of the computing mesh.

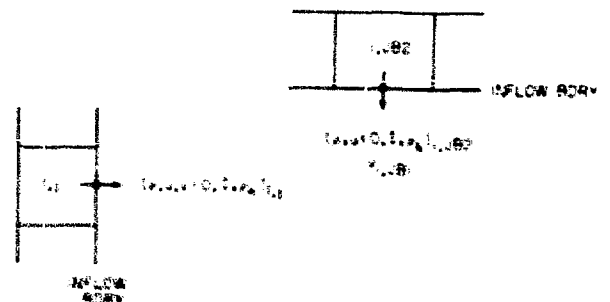


Fig. 4. Typical inflow cells along the left and top boundaries of the computing mesh.

Obstacles are built from combinations of solid and diagonally cut rectangular cells. The boundaries of an obstacle can be a combination of free-slip and no-slip, adiabatic, rigid walls and the right and bottom boundaries can have prescribed inflow to the computing mesh when they coincide with the cell boundaries. A continuative outflow boundary is not available for the interior obstacles. The boundary conditions are enforced on the interior obstacles in the same way as they are around the perimeter of the mesh for obstacle boundaries that coincide with cell boundaries. For obstacle boundaries that are formed by diagonally cut cells, the treatment of boundary conditions is described in Ref. 8.

F. Numerical Stability

The finite difference equations described earlier in this section for the mixture and species are generally unstable unless artificial diffusion of some sort is added. An unstable solution either oscillates or grows unbounded in time and in no way resembles the physical flow. Estimates of the amount of artificial diffusion needed for stability can easily be made. However, the computational time step is inversely proportional to the excess diffusion added so that overestimates can be costly in the total computer time required to obtain a solution. In addition, excessive diffusion reduces the spatial resolution of the calculation and hence the accuracy for a given cell size.

In the mass equation for the mixture, diffusion is added in the calculation of $\bar{\rho}$ in Eq. (3.2) through the \bar{v} -terms. The amount of diffusion needed is determined very accurately by calculating for each cell the value of the low-order diffusional truncation errors, which are the source of nonlinear instabilities. Diffusion is added in an amount to cancel these errors, which often have values that are orders of magnitude different in the r- and z-directions.

The momentum equations for the mixture, Eqs. (3.6) and (3.7), are stabilized by adding diffusion through the viscosity coefficients μ and λ . The amount of diffusion needed is estimated as

$$(2\mu + \lambda)/\rho > 1/2(u_{\max})^2 \delta t \text{ and } 1/2(v_{\max})^2 \delta t \quad (3.37)$$

and

$$\mu/\rho > 1/2(u_{\max})^2 \delta t \text{ and } 1/2(v_{\max})^2 \delta t, \quad (3.38)$$

which were derived from a truncation error analysis neglecting the second-order spatial errors. Inequalities (3.37) and (3.38) reduce to a single inequality when $\lambda = \mu$. The computational time step is restricted by the amount of excess diffusion furnished according to the relation

$$(2\mu + \lambda)\delta t/\rho < 1/2(\delta r)^2(\delta z)^2/[(\delta r)^2 + (\delta z)^2] \quad (3.39)$$

derived from a Fourier analysis. The total diffusion added in accord with inequality (3.37) is considered excess to insure stability in a stagnation region. A similar inequality exists for the excess diffusion in the mass equation but need not be considered since inequality (3.39) is by far the more restrictive one. Simultaneous satisfaction of inequalities (3.37) - (3.39) generally provides a numerically stable solution to the momentum equations.

The total energy equation, Eq. (3.15), is stabilized by adding diffusion through the coefficient $\hat{\kappa}$. The amount of diffusion needed is estimated as

$$\hat{\kappa}/\rho > 1/2[(\gamma u)_{\max}]^2 \delta t \text{ and } 1/2[(\gamma v)_{\max}]^2 \delta t, \quad (3.40)$$

which again is derived from a truncation error analysis neglecting the second-order spatial errors. The maximum excess diffusion in a stagnation region is $\hat{\kappa}/\rho$ which results in an inequality similar to (3.39), i.e.,

$$\hat{\kappa}\delta t/\rho < 1/2(\delta r)^2(\delta z)^2/[(\delta r)^2 + (\delta z)^2]. \quad (3.41)$$

The stability of the species transport equations is provided by locally canceling the low-order diffusional truncation errors as is done in the mass equation for the mixture.

In summary, the finite difference equations in RICE are generally numerically stable when μ , λ , $\hat{\kappa}$, and δt are chosen to satisfy simultaneously the inequalities (3.37) - (3.41). These inequalities reduce to inequalities involving only the ratio μ/ρ

and δt when λ and $\hat{\kappa}$ are written as

$$\lambda = A\mu, \quad \hat{\kappa} = B\mu \quad (3.42)$$

where A and B are constants usually chosen as unity and $(\gamma_{\max})^2$ respectively. For this choice, inequalities (3.37), (3.38), and (3.40) reduce to a single inequality. In addition, for the usual case where $(\gamma_{\max})^2 \leq 3$, inequality (3.41) is automatically satisfied when (3.39) is satisfied.

The values of δt and μ/ρ determined for numerical stability are constants specified by the input data. To insure that the ratio $\mu_{i,j}/\rho_{i,j}$ is a constant in the presence of varying density, the shear viscosity is computed as

$$\mu_{i,j} = (\mu/\rho) \rho_{i,j} \quad (3.43)$$

In certain situations the time step may have to be reduced because of strong coupling between the chemistry and the fluid dynamics. Strong coupling occurs when either the heat of reaction or the reaction rate is sufficiently large that a drastic change is produced in the internal energy density and hence the pressure in a single hydrodynamic time step.

IV. THE COMPUTER PROGRAM

The RICE computer program is described in this section. A global description of the subroutines and their functions and a card-by-card description of the input data are given. The program details are presented in three appendixes. Appendix A defines the FORTRAN IV symbols that are used in the program. The flow diagrams for each subroutine are presented in Appendix B and the FORTRAN IV listing of the program is given in Appendix C.

A. Global Description

The structure of the program and calling sequence for the various subroutines is shown in Fig. 5. The calculation begins with the RICE main program. The input data is read and in the case where the calculation is being continued from the results of a previous calculation, those results are read from TAPES by subroutine RTAPES. In this case the data read from TAPES serves as the initial conditions for the new calculation; otherwise, uniform initial conditions are set as directed by the input

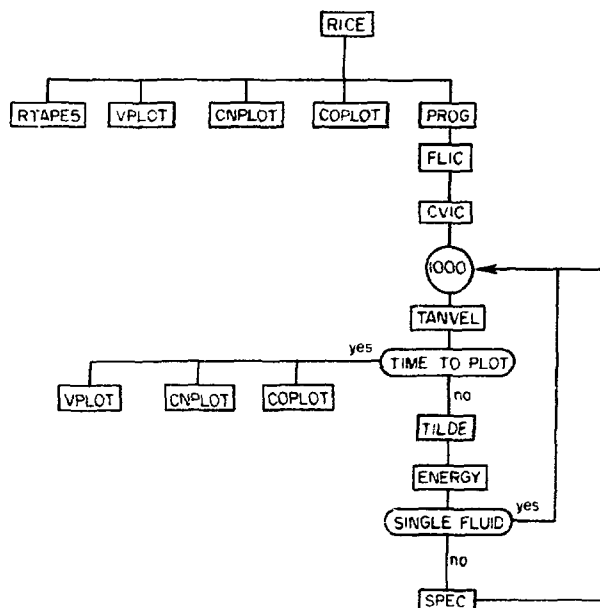


Fig. 5. Structure of the RICE program and the calling sequence for the various subroutines.

data. The plot routines VPL0T, CNPLOT, and COPL0T are called next to convert the r, z coordinates of the computing mesh boundaries to the appropriate coordinates for later plots on microfilm. The final call is to subroutine PROG, which assumes control of the calculation from this point to the end. The first call by PROG is to subroutine FLIC. FLIC assigns values to the matrix of flags $FL_{i,j}$ that is used to distinguish the various types of cells in the computing mesh and around its perimeter. Thirteen different types of cells exist. Subroutine CVIC is called next to set initial conditions and inflow boundary data. The setting of initial conditions is bypassed in CVIC when the initial data is obtained from tape. The inflow boundary data must be specified in all cases, however, which offers the option of changing the inflow boundary data from what was on tape. Statement 1000 begins the repetitive portion of the computational cycle. Calculation of c^2 , u , T , and p are made prior to calling subroutine TANVEL. TANVEL sets the tangential velocities in the fictitious cells that form the rigid wall boundaries around the computing mesh and in the solid cells that form the boundaries of interior obstacles. Plots on microfilm are made at designated time increments. Subroutine VPL0T plots the velocity vectors for each cell in the computing mesh, which display the direction and magnitudes of the fluid motion. CNPLOT plots contours of designated

quantities. Contours of ρ , p , I , T , Mach number, and species densities can be selected. The single plot produced by subroutine COPLOT shows the distributions and relative concentrations in the computing mesh of the species selected for contour plots. This routine is convenient for producing color plots of the species distributions. In addition to plotted data, printed data is also available on microfilm and paper at designated time intervals, which do not have to be the same as the intervals for plotted data. Subroutine TILDE is called next to calculate values for $\bar{\rho}$, \bar{p} , and \bar{u} . TILDE also performs the pressure iteration, which yields the final values for ρ^{n+1} , p^{n+1} , and u^{n+1} and the value for \bar{p} . Subroutine ENERGY follows TILDE for the calculation of the total energy density neglecting the effects of species diffusion and chemistry. For a single fluid the computational cycle is completed and return is to statement 1000. Subroutine SPEC is called for multicomponent flows to solve the species transport and chemistry equations and to update the total energy density to its final value. This completes the cycle for multicomponent flows and return is to statement 1000.

B. The Preprocessor (PREP) Program

The preprocessor is a feature of the RICE program that provides a capability for true variable dimensioning. From the size of the computing mesh (IB2,JB2) and the number of species NSPEC, the blocks of COMMON data are automatically constructed and written on file FSET8. The blocks are then read from this file and inserted in the RICE programs using the UPDATE features on the CDC-7600. To change the dimensions of COMMON variables, the UPDATE feature requires the following three cards.

```
*IDENT, name,
*DELETE, RCOM2. 24, RCOM2. 31
*READ, FSET8.
```

In this way only the precise amount of data storage needed for each problem is allocated in the machine. The large core memory of the CDC-7600 can be used by changing the word COMMON to LCM in format number 44 in the PREP program, which is listed in Appendix C.

C. Input Data

The input data is described card by card in this section. The total number of cards generally varies from one problem to the next. The first data card is read by PREP and is followed by an end-

of-file card while the remaining cards are read by RICE.

Card No. 1: IB2, JB2, NSPEC (Format 3I6) where

IB2 = the number of cells in the z-direction including those in the two fictitious columns at the right and left boundaries.

JB2 = the number of cells in the r-direction including those in the two fictitious rows at the top and bottom boundaries.

NSPEC = the total number of species in the problem, $1 \leq \text{NSPEC} \leq 7$. NSPEC cannot be zero here since it is used to establish array dimensions.

Card No. 2: End-of-file card.

Card No. 3: NAME (Format 10A8), where cols. 2-80 are used for problem identification on plots and data prints.

Card No. 4: SLG, VEL, DEN, SMØ, TEM (Format 12F6.2) where these are the physical scales that have been used to establish the dimensionless input data for the problem.

SLG = L_s , the length scale.

VEL = U_s , the velocity scale.

DEN = ρ_s , the density scale.

SMØ = M_s , the molecular weight scale.

TEM = T_s , the temperature scale.

These quantities are used for reference only and are not used in the program.

Card No. 5: ITD, NTD, NSDMP, NFILE, NWDMP (Format 24I3) where

ITD = 0. TAPE5 is neither read nor written (NTD through NWDMP are not used).

= 1. TAPE5 is written but not read (NTD and NFILE are not used).

= 2. TAPE5 is read but not written (NSDMP and NWDMP are not used).

= 3. TAPE5 is read and written.

NTD = the number of the data set (dump) on TAPE5 that contains the data to be used for initial conditions.

NSDMP = the number of cycles between writes (dumps) on TAPE5.

NFILE = the number of the last dump that was written on TAPE5.

NWDMP = the number of the first dump to be

written on TAPE5. Generally NWDMP = NFILE + 1.

Card No. 6: IB2, JB2, NØ, (NSL(K), K=1,4), LPR, CYCLE, ITC, (JPLØT(K), K=1,5), NSPEC, (ISPEC(K), K=1,7), NR (Format 8I3, I6, 15I3) where

IB2 = the same as on card no. 1.
 JB2 = the same as on card no. 1.
 NØ = the number of obstacles.

NSL(K) = the flags for rigid boundaries around the perimeter of the computing mesh. Values of either 0 for free slip or 1 for no slip are assigned for the bottom, right, top, and left boundaries in that order. The assigned values are ignored for inflow and outflow cells.

LPR = -2. omits plot identification, velocity vector plot (VPLØT), contour plots (CNPLØT) and all printed data on film. Used primarily to produce color plot by subroutine CØPLØT.
 = -1. same as LPR = -2 except does not omit contour plots (CNPLØT).
 = 0. Same as LPR = -2 except omits color plot (CØPLØT) instead of velocity vector plot (VPLØT).
 = 1. allows all plotting and printing on film and printing on paper at the designated time intervals.
 = 2. same as LPR = 1 except omit CØPLØT.
 = 4. allows printing on paper only.
 = 5. allows plotting and printing on film only.

CYCLE = the number of the computational cycle at which the calculation is to begin. CYCLE is also a counter which is advanced by one at each time step.

ITC = 1 for cylindrical coordinates or 0 for Cartesian coordinates.

JPLØT(K) = the flags for contour plots of ρ , p, I, T, and Mach number, in that order. When contour plots are desired JPLØT = 1, otherwise JPLØT = 0.

NSPEC = the number of species in the problem, $0 \leq \text{NSPEC} \leq 7$. NSPEC may be 0 or 1 for a single fluid where the only difference is in the temperature calculation, i.e., $C_v = 1$ for NSPEC = 0 and

C_v is specified later for NSPEC = 1.

ISPEC(K) = the flags for contour plots of species densities for up to seven species. When density contours are desired for species k, ISPEC(k) = 1, otherwise ISPEC(k) = 0.

NR = the number of chemical reactions, $\text{NR} \leq 3$.

Card No. 7: DX, DY, TIME, DT, TSTØP, TPR, TPL, TPLD, DTC (Format 12F6.2) where

DX = $\delta z(\delta x)$, the cell dimension in the z-direction.
 DY = $\delta r(\delta y)$, the cell dimension in the r-direction.
 TIME = the initial time for the problem. TIME is also a counter and is advanced by δt each cycle.
 DT = δt , the computational time step for the fluid dynamics.
 TSTØP = the time at which the calculation is to stop. The total number of computational cycles to be made is $(\text{TSTØP} - \text{TIME})/\text{DT}$.
 TPR = the time interval for printing data on paper. Successive prints on paper are made until CYCLE is advanced from its initial value to values ≥ 0 . From then on, printing on paper occurs at the specified time interval TPR.
 TPL = the time interval for plotting data on film. Successive plots on film are made until CYCLE is advanced from its initial value to values > 1 . From then on, plotting occurs at the specified time interval TPL.
 TPLD = the time interval for printing data on film. Successive prints on film are made until CYCLE is advanced from its initial value to values > 1 . From then on, printing on film occurs at the specified time interval TPLD.
 DTC = δt_c , the computational time step for solution of the chemistry equations. The ratio $\delta t/\delta t_c$ must be an integer.

Card No. 8: ALA, BIE, THETA, PHI, ØMEGA, GAMMA, DXØU, ASQ (Format 12F6.2) where

ALA = A, the ratio of the viscosity coefficients λ/μ (usually 1.0 since the viscosities are artificial), see Eq. (3.42).

BIE = B, the ratio of the coefficient \hat{R} to the shear viscosity (usually $B = (\gamma_{\max})^2$ from truncation error considerations), see Eq. (3.42).

THETA = θ , the time level parameter for the convection terms in the mixture mass equation, Eq. (3.1). A value of $\theta = 1/2$ is usually used for most compressible flows, while $\theta = 1$ is used for incompressible flows.

PHI = ϕ , the time level parameter for the pressure gradient in the momentum equations, Eqs. (3.6) and (3.7). The values of ϕ are usually chosen similar to the values of θ .

OMEGA = Ω , the constant over-relaxation factor for the pressure iteration, Eq. (3.11). The value of Ω is usually chosen as unity for compressible flows and ≥ 1.5 for incompressible flows.

GAMMA = γ , the specific heat ratio for a single fluid problem. When NSPEC > 0, γ is a cell variable determined from the specific heats of the mixture given by Eq. (2.9).

DXDU = the scale for the velocity vectors in the velocity vector plots. It is usually chosen as the smaller of $\delta z/u$ and $\delta r/v$, where u and v are estimates of the largest velocity components expected in the computing mesh.

ASQ = the sound speed used for incompressible flow calculations. ASQ = 0 for compressible flows and ASQ is set so that the maximum Mach number in the computing region is less than 10^{-5} for incompressible flows.

Card No. 9: FLØ(M), M = 1,12 (Format 12F6.2), where

FLØ(M) = the coordinates of the flow openings along the right, top, and left boundaries of the computing mesh. The coordinates along the right and left boundaries must be integral multiples of δr , while those along the top boundary must be integral multiples of δz . The openings along the right boundary are by definition outflow openings, while those along the top and left

boundaries are inflow openings. FLØ(1)-FLØ(4) define the r-coordinates of the openings along the right boundary in the direction of increasing r. Figure 6, illustrates the cases for two, one, and zero openings on the right boundary. The origin of the coordinate system is the upper corner of the cell (1,1). FLØ(5)-FLØ(8) define the z-coordinates of the openings along the top boundary in the direction of increasing z. The assignment of z-coordinates is similar to the cases illustrated in Fig. 6. FLØ(9)-FLØ(12) define the r-coordinates of the openings along the left boundary in the direction of increasing r similar to what is done along the right boundary.

Card No. 10: UØ, VØ, VINT1, VINT2, UINL1, UINL2

(Format 12F6.2) where

UØ = the initial value of u for the fluid cells.

VØ = the initial value of v for the fluid cells.

VINT1 = the radial velocity of the fluid flowing into the computing mesh through the first opening along the top boundary.

VINT2 = the radial velocity of the fluid flowing into the computing mesh through the second opening along the top boundary.

UINL1 = the axial velocity of the fluid flowing into the computing mesh through the first opening along the left boundary.

UINL2 = the axial velocity of the fluid flow-

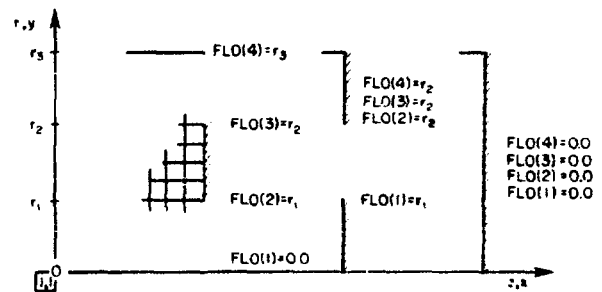


Fig. 6. Description of flow openings along the right boundary. The figure illustrates two, one, and zero openings.

ing into the computing mesh through the second opening along the left boundary.

Card No. 11: RH00, RINT1, RINT2, RINL1, RINL2 (Format 12F6.2) where

RH00 = ρ_0 , the initial value of ρ for the fluid cells. This quantity must always be non-zero even when the initial data is obtained from TAPE5 since it is used to define ϵ which establishes the convergence requirement for the pressure iteration, see Eq. (3.10). The value of ϵ is set in subroutine CVIC as $\epsilon = 10^{-4}$ RH00. RH00 is also used in specifying the constant value for the ratio $\mu/\rho = \mu_0/\rho_0$ determined for numerical stability.

RINT1 = the density of the fluid flowing into the computing mesh through the first opening along the top boundary.

RINT2 = the density of the fluid flowing into the computing mesh through the second opening along the top boundary.

RINL1 = the density of the fluid flowing into the computing mesh through the first opening along the left boundary.

RINL2 = the density of the fluid flowing into the computing mesh through the second opening along the left boundary.

Card No. 12: MU0, MINT1, MINT2, MINL1, MINL2 (Format 12F6.2) where

MU0 = μ_0 , the initial value of the shear viscosity μ for the fluid cells. MU0 and RH00 are used to specify the constant value for the ratio $\mu/\rho = \mu_0/\rho_0$ determined for numerical stability.

MINT1 = the shear viscosity of the fluid flowing into the computing mesh through the first opening along the top boundary.

MINT2 = the shear viscosity of the fluid flowing into the computing mesh through the second opening along the top boundary.

MINL1 = the shear viscosity of the fluid flowing into the computing mesh through the first opening along the left boundary.

MINL2 = the shear viscosity of the fluid flowing into the computing mesh through the second opening along the left boundary.

The values of the shear viscosity of the fluid flowing into the computing mesh must be set in accord with the densities assigned on card no. 11 and the required ratio of μ/ρ determined for numerical stability.

Card No. 13: SIE0, SIET1, SIET2, SIEL1, SIEL2 (Format 12F6.2) where

SIE0 = the initial value of the specific internal energy I for the fluid cells.

SIET1 = the specific internal energy of the fluid flowing into the computing mesh through the first opening along the top boundary.

SIET2 = the specific internal energy of the fluid flowing into the computing mesh through the second opening along the top boundary.

SIEL1 = the specific internal energy of the fluid flowing into the computing mesh through the first opening along the left boundary.

SIEL2 = the specific internal energy of the fluid flowing into the computing mesh through the second opening along the left boundary.

This completes the input data for problems involving a single fluid with NSPEC = 0 and no interior obstacles. The following additional data are required when NSPEC > 0.

Card No. 14: ETA0 (Format 12F6.2) where

ETA0 = η_0 , the constant used for calculating the molecular diffusion coefficients for the species, see Eq. (3.24).

Card No. 15: FA0(1), FAT1(1), FAT2(1), FAL1(1), FAL2(1) (Format 12F6.2) where

FA0(1) = the initial value of the density of species (1) for the fluid cells.

FAT1(1) = the density of species (1) flowing into the computing mesh through the first opening along the top boundary.

FAT2(1) = the density of species (1) flowing into the computing mesh through the second opening along the top boundary.

FAL1(1) = the density of species (1) flowing into the computing mesh through the first opening along the left boundary.

FAL2(1) = the density of species (1) flowing into the computing mesh through the second opening along the left boundary.

Card Nos. 16-21: Similar to card no. 15 but for the remaining species (2) through (7). The species densities prescribed for the initial and boundary conditions should sum to the values prescribed for the mixture densities.

Card No. 22: SM(K), K=1,7 (Format 12F6.2) where

SM(K) = M_k , the molecular weight of species k.

Card No. 23: EP(K), K=1,7 (Format 12F6.2) where

EP(K) = the minimum value for the concentration of species k that can enter into a chemical reaction. EP(k) usually equals zero.

Card No. 24: GAMA(K), K=1,7 (Format 12F6.2) where

GAMA(K) = γ_k , the specific heat ratio for species k.

Card No. 25: CV(K), K=1,7 (Format 12F6.2) where

CV(K) = $(C_v)_k$, the specific heat at constant volume for species k.

Card No. 26: ALPHA(K), K=1,7 (Format 12F6.2) where

ALPHA(K) = α_k , a function of M_k for the calculation of the molecular diffusion coefficient, see Eq. (3.24).

The following data cards define the chemical reactions according to Eq. (2.13) and their respective rate multipliers given by Eq. (2.17). One card is used for each reaction and its rate multipliers. The total number of reactions, and hence the total number of data cards, is NR defined on card no. 6. If either NSPEC or NR is zero on card no. 6, the chemical reaction data should be omitted.

Card No. 27: (AM(K,L), K=1,7), (BM(K,L), K=1,7), Q(L), CF(L), ZETAF(L), EF(L), CB(L), ZETAB(L), EB(L) (Format 14I2, 2x, 7F6.2) where this card illustrates the data for chemical reaction number L.

AM(K,L) = a_k , the stoichiometric coefficients of the reactants, see Eq. (2.13).

BM(K,L) = b_k , the stoichiometric coefficients of the products, see Eq. (2.13).

Q(L) = q, the heat of reaction, see Eq. (2.18).

CF(L) = C, a constant for the calculation of the forward rate multiplier K_f , see

Eq. (2.17).

ZETAF(L) = ζ , the temperature exponent for the calculation of the forward rate multiplier, see Eq. (2.17).

EF(L) = E^\dagger , the ratio of the activation energy to the universal gas constant for the forward rate multiplier, see Eq. (2.17).

CB(L) = C, a constant for the calculation of the backward rate multiplier, see Eq. (2.17).

ZETAB(L) = ζ , the temperature exponent for the calculation of the backward rate multiplier, see Eq. (2.17).

EB(L) = E^\dagger , the ratio of the activation energy to the universal gas constant for the backward rate multiplier, see Eq. (2.17).

The following data cards define the interior obstacles. The number of obstacles is $N\emptyset$ specified on card no. 6. Five data cards are required to define each obstacle. If $N\emptyset$ is zero these data cards should be omitted.

Card No. 28: IT \emptyset (N), NS \emptyset (N), (\emptyset B(M,N), M = 1,6), (\emptyset IB(M,N), M = 1,2) (Format 2I3, 11F6.2) where this card illustrates the data for obstacle number N.

IT \emptyset (N) = the flags that define the type of obstacle. An obstacle must be rectangular or triangular in shape and can be made up of one or more cells. By combining obstacles, shapes other than simple rectangles and triangles are produced. Rectangular obstacles can have a single flow opening along either the right or bottom boundary to provide inflow to the computing mesh. The four obstacle types are shown in Fig. 7.

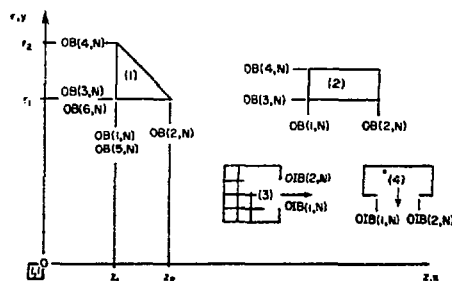


Fig. 7. Description of obstacles that can be placed in the interior of the computing mesh.

NS \emptyset (N) = the flags that define the boundaries of obstacle number N as free slip, NS \emptyset (N) = 0, or no slip, NS \emptyset (N) = 1.

\emptyset B(M,N) = the coordinates that define the location of the obstacle, see Fig. 7. For rectangular obstacles the z-coordinates of the left and right boundaries and the r-coordinates of the bottom and top boundaries define the obstacle's size and location. These coordinates are specified by \emptyset B(1,N) - \emptyset B(4,N). Triangular obstacles require additional data to specify the (z,r)-coordinates of the 90° angle. These coordinates are specified in \emptyset B(5,N) and \emptyset B(6,N), respectively, and are not used for rectangular obstacles.

\emptyset IB(M,N) = the coordinates that define the flow opening along either the right or bottom boundary of the obstacle when these boundaries coincide with the cell boundaries, see Fig. 7. An opening along the right boundary must be an integral multiple of δr in height, while an opening along the bottom boundary must be an integral multiple of δz in width. The height or width of the opening is \emptyset IB(2,N) - (\emptyset IB(1,N)).

Card No. 29: UINR \emptyset (N), RINR \emptyset (N), MINR \emptyset (N), SIER \emptyset (N) (Format 12F6.2) where for obstacle number N

UINR \emptyset (N) = axial velocity of the fluid flowing into the computing mesh from a type (3) obstacle.

RINR \emptyset (N) = density of the fluid flowing into the computing mesh from a type (3) obstacle.

MINR \emptyset (N) = shear viscosity of the fluid flowing into the computing mesh from a type (3) obstacle. The value of MINR \emptyset (N) should be determined as MINR \emptyset (N) = (μ_o/ρ_o) RINR \emptyset (N).

SIER \emptyset (N) = specific internal energy of the fluid flowing into the computing mesh from a type (3) obstacle.

Card No. 30: VINB \emptyset (N), RINB \emptyset (N), MINB \emptyset (N), SIEB \emptyset (N) (Format 12F6.2) where for obstacle number N

VINB \emptyset (N) = the radial velocity of the fluid flowing into the computing mesh from a

type (4) obstacle.

RINB \emptyset (N) = the density of the fluid flowing into the computing mesh from a type (4) obstacle.

MINB \emptyset (N) = the shear viscosity of the fluid flowing into the computing mesh from a type (4) obstacle. The value of MINB \emptyset (N) should be determined as MINB \emptyset (N) = (μ_o/ρ_o) RINB \emptyset (N).

SIEB \emptyset (N) = the specific internal energy of the fluid flowing into the computing mesh from a type (4) obstacle.

Card No. 31: FAR \emptyset (K,N), K = 1,7 (Format 12F6.2)

where for obstacle number N









FAR \emptyset (K,N) = the density of species k flowing into the computing mesh from a type (3) obstacle.

Card No. 32: FAB \emptyset (K,N), K = 1,7 (Format 12F6.2) where for obstacle number N

FAB \emptyset (K,N) = the density of species k flowing into the computing mesh from a type (4) obstacle.

Immediately after all the input data is read, it is written on paper and microfilm by the RICE main program. Following this, control is transferred to subroutine PR \emptyset G which then calls subroutine FLIC. The cell flags that differentiate the various types of cells are set in FLIC and printed on paper and film at the beginning of subroutine CVIC. The printed input data and cell flags provide a convenient check on the setup of the problem. The flagging scheme for the various computational cells is described in Table I.

TABLE I
CELL FLAGS

FL(I,J)	Cell Types
	Solid and fluid cells:
1	(a) Fluid cell
2	(b) Solid cell with free-slip boundary
3	(c) Solid cell with no-slip boundary
4	(d) Outflow cell
5	(e) Inflow cell
	Diagonally cut cells (solid portion is shaded):
6	(a)  With free-slip boundary
7	(b)  With free-slip boundary
8	(c)  With free-slip boundary
9	(d)  With free-slip boundary
10	(e)  With no-slip boundary
11	(f)  With no-slip boundary
12	(g)  With no-slip boundary
13	(h)  With no-slip boundary

V. EXAMPLE PROBLEM

The capabilities of the RICE program are demonstrated through the calculation of an example problem. The complex fluid dynamics, species mixing, and nonequilibrium chemical reactions that take place in the lasing cavity of a continuous flow chemical laser provide a realistic and comprehensive problem for calculation. The particular laser system to be considered is an HF laser designed by the Aerospace Corporation.⁹ F-atoms enter the lasing cavity through a bank of two-dimensional supersonic nozzles while H_2 is injected under high pressure through orifices located at the nozzle exit plane between adjacent nozzles. A portion of the nozzle bank is shown schematically in Fig. 8. The full nozzle bank contains 37 nozzles and is 1.25 cm deep. The F-atoms are obtained by the dissociation of SF_6 . A nitrogen diluent is added for control of the exit conditions. Under conditions of complete dissociation of the SF_6 , the fluorine nozzles flow N_2 , S, and F. Hydrogen enters the lasing cavity under high pressure through a perforated tube. For the calculation, the series of perforations is approximated as a two-dimensional slit. The F-atoms and H_2 mix and react in the lasing cavity to produce vibrationally excited HF which serves as the lasing medium.

A. Input

Neglecting boundary layers, the uniform flow conditions at the exit plane of the fluorine nozzle are given in Table II. These conditions imply an exit Mach number of 4.3, a temperature of 656°K, and an exit pressure of 6.77×10^3 dynes/cm² (5.0 torr) for the mixture.

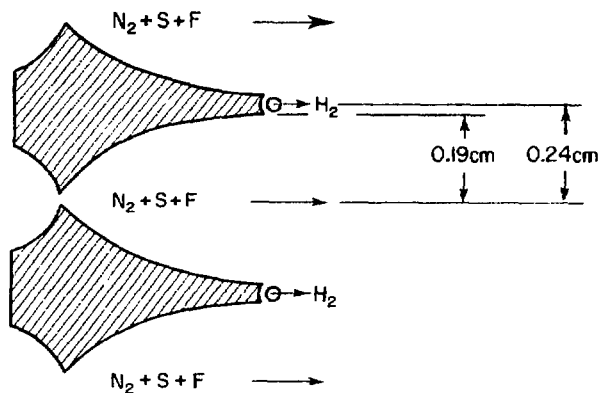


Fig. 8. Cross-sectional view of a portion of the laser nozzle bank.

Hydrogen enters the lasing cavity through a narrow slit, 0.016 cm, under the sonic conditions given in Table III. The injection pressure for these conditions is 2.96×10^5 dynes/cm² (222 torr).

The chemical reactions of H_2 with F populate several vibrational levels of HF that provide the lasing medium. For the purpose of this example problem, a single reaction equation is solved,



where the vibrational states of HF are represented collectively by HF^* . The rate multiplier for the forward reaction K_f is given by Eq. (2.17), with $C = 1.6 \times 10^{14}$ cm³/mole/s, $\zeta = 0$, and $E^\ddagger = 800^\circ\text{K}$ from Ref. 10, while for the backward reaction, $K_b = 0$. The heat of reaction is $q = 5 \times 10^{11}$ erg/mole. Table IV summarizes the data describing the chemical reaction.

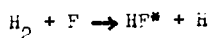
TABLE II
FLOW CONDITIONS AT THE EXIT PLANE OF THE FLUORINE NOZZLES

Mixture:	u (cm/s)	v (cm/s)	ρ (g/cm ³)	I (erg/g)
$H_2 + S + F$	2.30×10^5	0.	3.35×10^{-6}	4.82×10^9
Species (k):	ρ_k (g/cm ³)	M_k (g/mole)	γ_k	$(C_v)_k$ (erg/g/°K)
1 = N_2	3.06×10^{-6}	28.0	1.40	7.47×10^6
2 = S	6.30×10^{-8}	32.0	1.67	3.92×10^6
3 = F	2.25×10^{-7}	19.0	1.67	6.61×10^6

TABLE III
HYDROGEN INJECTION CONDITIONS

Mixture:	u (cm/s)	v (cm/s)	ρ (g/cm ³)	I (erg/g)
H ₂	1.33×10^5	0.	2.35×10^{-5}	3.15×10^{10}
Species (k):	ρ_k (g/cm ³)	M_k (g/mole)	γ_k	$(C_v)_k$ (erg/g/°K)
H = H ₂	2.35×10^{-5}	2.0	1.4	1.05×10^8

TABLE IV
CHEMICAL REACTION DATA



Species (k):	ρ_k (g/cm ³)	M_k (g/mole)	γ_k	$(C_v)_k$ (erg/g/°K)
$\phi = HF^*$	-	20.0	1.40	1.05×10^7
$\psi = H$	-	1.0	1.67	1.26×10^8

$$a_k: 0, 0, 1, 1, 0, 0$$

$$b_k: 0, 0, 0, 0, 1, 1$$

$$k_f = C T^{\xi} e^{-E^{\dagger}/T} \text{ where } C = 1.0 \times 10^{11} \text{ cm}^3/\text{mole/s}, \xi = 0, E^{\dagger} = 800^{\circ}\text{K}$$

$$k_b = C T^{\xi} e^{-E^{\dagger}/T} \text{ where } C = \xi = E^{\dagger} = 0$$

$$q = 5 \times 10^{11} \text{ erg/mole}$$

Mixing of the species is produced through the action of molecular diffusion. Coefficients that describe the diffusion of the various species into the mixture are obtained by approximating the mixture as pure nitrogen. The diffusion coefficients are defined by the data in Table V.

TABLE V
DIFFUSION COEFFICIENTS

$$D_k = \alpha_k \eta \text{ (cm}^2/\text{s)}, \quad \eta = \eta_0 T^{3/2} / \nu \text{ (cm}^2/\text{s)},$$

$$\alpha_k = (M_H / M_k)^{1/2}$$

$$\eta_0 = 224 \text{ dynes (}^{\circ}\text{K)}^{-3/2} \text{ s}^{-1}$$

$$\alpha_k = 0.189, 0.177, 0.329, 0.707, 0.224, 1.0$$

The computational region begins slightly upstream of the nozzle exit plane and its upper and lower boundaries coincide with the center line of

the hydrogen slit and the axis of the lower, adjacent fluorine nozzle, respectively. The computing region is shown in Fig. 9.

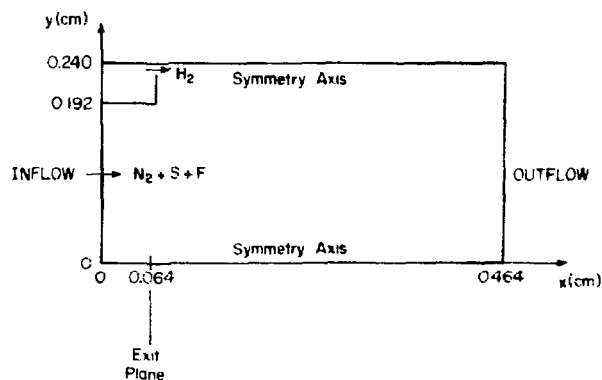


Fig. 9. Geometry of the computing region for the sample problem.

The dimensions of the computational cells are $\delta x = 0.008$ cm and $\delta y = 0.008$ cm. The number of cells in the x- and y-directions are $IB2 = 62$ and $JB2 = 32$, respectively.

The flow openings along the right and left boundaries are specified in Table VI.

TABLE VI
FLOW OPENING DATA

$FL\phi_m$ (cm):	0.,	0.240,	0.240,	0.240,
	0.,	0.,	0.,	0.,
	0.,	0.192,	0.192,	0.192

The shape of the interior obstacle is rectangular so that it can be described by a single RICE obstacle. The half-width of the H_2 injection slit is 0.008 cm. The data describing the obstacle geometry is given in Table VII.

TABLE VII
OBSTACLE DATA

OB_m (cm):	0,	0.064,	0.192,	0.240
OIP_m (cm):	0.232,	0.240		

The viscosity coefficients, thermal conductivity, and time step are determined for numerical stability by simultaneously satisfying inequalities (3.37)-(3.41). These inequalities reduce to

$$\mu/\rho > 2.65 \times 10^{10} \delta t, \dots (3.37), (3.38), (3.40)$$

$$\mu/\rho < 5.33 \times 10^{-6}/\delta t, \dots (3.39)$$

$$\mu/\rho < 5.73 \times 10^{-6}/\delta t, \dots (3.41)$$

when $A = 1.$, and $B = (\gamma_{\max})^2 = 2.79$ in Eq. (3.42). Inequality (3.41) is satisfied automatically when (3.39) is satisfied. A solution of (3.37) and (3.39) yields

$$\delta t = 5 \times 10^{-9} s, \mu/\rho = 221 \text{ cm}^2/s. \quad (5.2)$$

The above sets of data, given in Tables II-VII, with Eq. (5.2) are dimensionally consistent and can be used as input data for the calculation. However, dimensionless quantities that are more nearly of unit order are obtained by appropriately scaling the data. A convenient choice of scales is given in Table VIII.

The number of computational cycles required to obtain a steady state solution can be estimated as

$$\# \text{ cycles} \approx 2.5 (IB2-2) \delta x / (u_{\text{input}} \delta t) \quad (5.3)$$

where u_{input} refers to a typical axial velocity at the inflow boundary. With u_{input} as 2.3×10^5 cm/s, Eq. (5.3) indicates that about 1040 cycles are needed to obtain a steady state.

TABLE VIII
PHYSICAL SCALES

$$L_s = 1 \text{ cm}, u_s = 10^5 \text{ cm/s}, \rho_s = 10^{-5} \text{ g/cm}^3,$$

$$M_s = 1 \text{ g/mole}, T_s = 100^\circ K$$

The dimensionless quantities denoted by $\bar{\quad}$ are obtained as

$$\bar{u} = u/u_s, \bar{v} = v/u_s$$

$$\bar{\rho} = \rho/\rho_s$$

$$\bar{I} = I/u_s^2$$

$$\bar{M}_k = M_k/M_s$$

$$\bar{C}_v = C_v T_s / u_s^2$$

$$\bar{C} = C \rho_s L_s / (M_s u_s)$$

$$\bar{E}^+ = E^+ / T_s$$

$$\bar{q} = q / (u_s^2 M_s)$$

$$\bar{\eta}_o = \eta_o T_s^{3/2} / (\rho_s L_s u_s^3)$$

$$\bar{\delta t} = \delta t u_s / L_s$$

$$\bar{\mu} = \mu / (\rho_s u_s L_s)$$

$$\bar{\delta x} = \delta x / L_s, \bar{\delta y} = \delta y / L_s$$

Dimensionless quantities are used in the example problem.

B. Output

The dimensionless input data printed by RICE on paper and film is shown in Table IX. Although the problem contains six species, N_{SPEC} is set to 7 to introduce a fictitious species whose density should be zero everywhere in the computing mesh for all time. The density of this last species is calculated by Eq. (3.21) and provides an indication of how well the sum of the real species densities compares to the mixture density. To minimize the influence of the fictitious species, its properties, M_7 , γ_7 , $(C_v)_7$, and α_7 , are set to zero.

The time step for solution of the chemistry equations δt_c is set equal to the hydrodynamic time step δt because the reactant concentrations in the mix region are expected to be low and a low reaction rate will be produced. This is in fact confirmed by computing the characteristic time for the reaction from the steady solution data.

Table X shows the cell flags produced by subroutine FLIC and printed on paper by subroutine CVIC.

The initial values of the flow variables specified by the input data are printed on paper and film

and reproduced for rows $j = 30-32$ in Table XI. The data, printed across the page, corresponds to i, j , $(FL_{i,j})$, $(u_{i,j})$, $(v_{i,j})$, $(\rho_{i,j})$, $(p_{i,j})$, $(I_{i,j})$, $(T_{i,j})$, $(\nu_{i,j})$ for the mixture, followed by i, j , $(FL_{i,j})$, $(\rho_k)_{i,j}$ for the species where $k = 1-7$. The seven species are designated in Table XI by the letters A-G, respectively.

Similarly, the data at the end of one computational cycle is printed in Table XII for the same rows. In accord with the input data, i.e., $CYCLE = 0$, this print occurs only on film unless paper printouts are specified by setting $CYCLE$ equal to a negative number.

A steady state solution is obtained after 1000 cycles. Plots of the velocity vector field, contours of ρ , p , I , T , Mach number, and species densities, and the distribution of the species in the computing mesh are shown in Fig. 10. These plots are produced in accord with the specification of TPL.

The printed data is given in Table XIII for rows 20-22. This data is printed on paper and film as specified by TPR and TPLD.

TABLE XI

INITIAL DATA AT CYCLE = 0, TIME = 0

CYCLE =	U	TIME =	0.000	RICE	L.A.	REPORT	PROBLEM---	8/23/74		
1	J	FL	U	V	RHO	PB	SIE	TEMP.	MU	
1	30	2	0.	0.	0.	0.	0.	0.	0.	0.
2	30	2	0.	0.	0.	0.	0.	0.	0.	0.
3	30	2	0.	0.	0.	0.	0.	0.	0.	0.
4	30	2	0.	0.	0.	0.	0.	0.	0.	0.
5	30	2	0.	0.	0.	0.	0.	0.	0.	0.
6	30	2	0.	0.	0.	0.	0.	0.	0.	0.
7	30	2	0.	0.	0.	0.	0.	0.	0.	0.
8	30	2	0.	0.	0.	0.	0.	0.	0.	0.
9	30	2	0.	0.	0.	0.	0.	0.	0.	0.
10	30	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
11	30	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
12	30	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
13	30	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
14	30	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
15	30	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
1	31	2	0.	0.	0.	0.	0.	0.	0.	0.
2	31	2	0.	0.	0.	0.	0.	0.	0.	0.
3	31	2	0.	0.	0.	0.	0.	0.	0.	0.
4	31	2	0.	0.	0.	0.	0.	0.	0.	0.
5	31	2	0.	0.	0.	0.	0.	0.	0.	0.
6	31	2	0.	0.	0.	0.	0.	0.	0.	0.
7	31	2	0.	0.	0.	0.	0.	0.	0.	0.
8	31	2	0.	0.	0.	0.	0.	0.	0.	0.
9	31	5	1.3300E+00	0.	2.3500E+00	2.9610E+00	3.1500E+00	3.0000E+00	5.1900E-03	
10	31	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
11	31	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
12	31	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
13	31	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
14	31	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
15	31	1	2.3000E+00	0.	3.3500E-01	6.4588E-02	4.8200E-01	6.4525E+00	7.4000E-04	
1	32	2	0.	0.	0.	0.	0.	0.	0.	0.
2	32	2	0.	0.	0.	0.	0.	0.	0.	0.
3	32	2	0.	0.	0.	0.	0.	0.	0.	0.
4	32	2	0.	0.	0.	0.	0.	0.	0.	0.
5	32	2	0.	0.	0.	0.	0.	0.	0.	0.
6	32	2	0.	0.	0.	0.	0.	0.	0.	0.
7	32	2	0.	0.	0.	0.	0.	0.	0.	0.
8	32	2	0.	0.	0.	0.	0.	0.	0.	0.
9	32	2	1.3300E+00	0.	0.	0.	0.	0.	0.	0.
10	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.
11	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.
12	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.
13	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.
14	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.
15	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.

TABLE XI (cont)

CYCLE= 0 TIME= 0.000 RICE L.A. REPORT PROBLEM---0/23/74
SPECIES DENSITIES

I	J	FL	A	B	C	D	E	F	G
1	30	2	0.	0.	0.	0.	0.	0.	0.
2	30	2	0.	0.	0.	0.	0.	0.	0.
3	30	2	0.	0.	0.	0.	0.	0.	0.
4	30	2	0.	0.	0.	0.	0.	0.	0.
5	30	2	0.	0.	0.	0.	0.	0.	0.
6	30	2	0.	0.	0.	0.	0.	0.	0.
7	30	2	0.	0.	0.	0.	0.	0.	0.
8	30	2	0.	0.	0.	0.	0.	0.	0.
9	30	2	0.	0.	0.	0.	0.	0.	0.
10	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
11	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
12	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
13	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
14	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
15	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
1	31	2	0.	0.	0.	0.	0.	0.	0.
2	31	2	0.	0.	0.	0.	0.	0.	0.
3	31	2	0.	0.	0.	0.	0.	0.	0.
4	31	2	0.	0.	0.	0.	0.	0.	0.
5	31	2	0.	0.	0.	0.	0.	0.	0.
6	31	2	0.	0.	0.	0.	0.	0.	0.
7	31	2	0.	0.	0.	0.	0.	0.	0.
8	31	2	0.	0.	0.	0.	0.	0.	0.
9	31	5	0.	0.	0.	2.3500E+00	0.	0.	0.
10	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
11	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
12	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
13	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
14	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
15	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
1	32	2	0.	0.	0.	0.	0.	0.	0.
2	32	2	0.	0.	0.	0.	0.	0.	0.
3	32	2	0.	0.	0.	0.	0.	0.	0.
4	32	2	0.	0.	0.	0.	0.	0.	0.
5	32	2	0.	0.	0.	0.	0.	0.	0.
6	32	2	0.	0.	0.	0.	0.	0.	0.
7	32	2	0.	0.	0.	0.	0.	0.	0.
8	32	2	0.	0.	0.	0.	0.	0.	0.
9	32	2	0.	0.	0.	0.	0.	0.	0.
10	32	2	0.	0.	0.	0.	0.	0.	0.
11	32	2	0.	0.	0.	0.	0.	0.	0.
12	32	2	0.	0.	0.	0.	0.	0.	0.
13	32	2	0.	0.	0.	0.	0.	0.	0.
14	32	2	0.	0.	0.	0.	0.	0.	0.
15	32	2	0.	0.	0.	0.	0.	0.	0.

TABLE XII

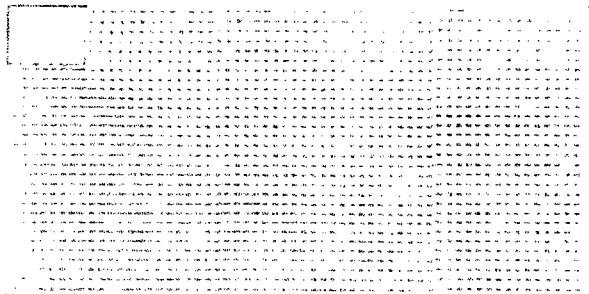
SOLUTION DATA AT CYCLE = 1, TIME = 0.0005

CYCLE:	1	TIME:	.001	RICE	L.S.	REPORT	FACELEN	---	0/23/PA			
1	2	FL	U	V	ANO	FD	SIC	TEMP.	PU			
1	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
2	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
3	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
4	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
5	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
6	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
7	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
8	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
9	30	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
10	30	1	2.0773E+00	-9.7210E-02	2.9197E-01	7.3261E-02	6.2731E-01	7.2617E+00	6.4494E-04			
11	30	1	2.3132E+00	-5.2692E-03	3.3115E-01	6.0219E-02	4.3402E-01	6.1000E+00	7.3149E-04			
12	30	1	2.3000E+00	0.	3.3500E-01	6.0977E-02	4.3506E-01	6.0000E+00	7.4000E-04			
13	30	1	2.3000E+00	0.	3.3500E-01	6.4093E-02	4.8279E-01	6.4630E+00	7.4000E-04			
14	30	1	2.3000E+00	0.	3.3500E-01	6.4500E-02	4.8200E-01	6.4525E+00	7.4000E-04			
15	30	1	2.3000E+00	0.	3.3500E-01	6.4500E-02	4.8200E-01	6.4525E+00	7.4000E-04			
1	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
2	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
3	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
4	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
5	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
6	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
7	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
8	31	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
9	31	5	1.3300E+00	0.	2.3500E+00	2.9610E+00	3.1900E+00	3.0000E+00	5.1900E-03			
10	31	1	1.6275E+00	0.	5.4377E-01	6.4390E-01	2.9607E+00	6.0822E+00	1.2012E-03			
11	31	1	2.3061E+00	0.	3.3322E-01	1.4440E-01	1.0034E+00	1.4318E+01	7.3000E-04			
12	31	1	2.3000E+00	0.	3.3500E-01	5.8390E-02	4.3501E-01	5.8319E+00	7.4000E-04			
13	31	1	2.3000E+00	0.	3.3500E-01	6.4636E-02	4.8236E-01	6.4573E+00	7.4000E-04			
14	31	1	2.3000E+00	0.	3.3500E-01	6.4500E-02	4.8200E-01	6.4525E+00	7.4000E-04			
15	31	1	2.3000E+00	0.	3.3500E-01	6.4500E-02	4.8200E-01	6.4525E+00	7.4000E-04			
1	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
2	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
3	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
4	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
5	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
6	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
7	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
8	32	2	0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
9	32	2	1.3300E+00	0.	0.	0.	0.	0.	0.	0.	0.	0.
10	32	2	1.6275E+00	0.	0.	0.	0.	0.	0.	0.	0.	0.
11	32	2	2.3061E+00	0.	0.	0.	0.	0.	0.	0.	0.	0.
12	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.	0.	0.
13	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.	0.	0.
14	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.	0.	0.
15	32	2	2.3000E+00	0.	0.	0.	0.	0.	0.	0.	0.	0.

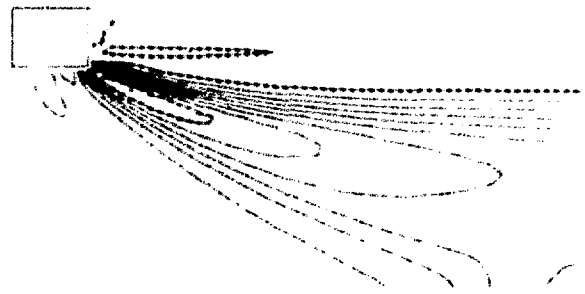
TABLE XII (cont)

CIRCLE: 1 TIME: .001 RICE L.A. REPORT PROGRAM--0/23/70
SPECIES DENSITIES

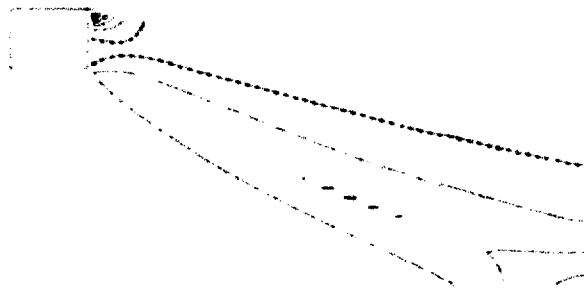
	1	2	FL	A	B	C	D	E	F	G
	1	30	2	0.	0.	0.	0.	0.	0.	0.
	2	30	2	0.	0.	0.	0.	0.	0.	0.
	3	30	2	0.	0.	0.	0.	0.	0.	0.
	4	30	2	0.	0.	0.	0.	0.	0.	0.
	5	30	2	0.	0.	0.	0.	0.	0.	0.
	6	30	2	0.	0.	0.	0.	0.	0.	0.
	7	30	2	0.	0.	0.	0.	0.	0.	0.
	8	30	2	0.	0.	0.	0.	0.	0.	0.
	9	30	2	0.	0.	0.	0.	0.	0.	0.
	10	30	1	2.9244E-01	0.	0.	1.1041E-03	0.	0.	-1.5747E-03
	11	30	1	3.3000E-01	0.	0.	0.	0.	0.	1.0060E-03
	12	30	1	3.3528E-01	0.	0.	0.	0.	0.	-2.7634E-04
	13	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
	14	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
	15	30	1	3.3500E-01	0.	0.	0.	0.	0.	0.
	1	31	2	0.	0.	0.	0.	0.	0.	0.
	2	31	2	0.	0.	0.	0.	0.	0.	0.
	3	31	2	0.	0.	0.	0.	0.	0.	0.
	4	31	2	0.	0.	0.	0.	0.	0.	0.
	5	31	2	0.	0.	0.	0.	0.	0.	0.
	6	31	2	0.	0.	0.	0.	0.	0.	0.
	7	31	2	0.	0.	0.	0.	0.	0.	0.
	8	31	2	0.	0.	0.	0.	0.	0.	0.
	9	31	3	0.	0.	0.	2.3500E+00	0.	0.	0.
	10	31	1	2.9505E-01	0.	0.	2.3104E-01	0.	0.	1.6004E-02
	11	31	1	3.1951E-01	0.	0.	1.2021E-03	0.	0.	1.2432E-02
	12	31	1	3.3513E-01	0.	0.	0.	0.	0.	-1.2703E-04
	13	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
	14	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
	15	31	1	3.3500E-01	0.	0.	0.	0.	0.	0.
	1	32	2	0.	0.	0.	0.	0.	0.	0.
	2	32	2	0.	0.	0.	0.	0.	0.	0.
	3	32	2	0.	0.	0.	0.	0.	0.	0.
	4	32	2	0.	0.	0.	0.	0.	0.	0.
	5	32	2	0.	0.	0.	0.	0.	0.	0.
	6	32	2	0.	0.	0.	0.	0.	0.	0.
	7	32	2	0.	0.	0.	0.	0.	0.	0.
	8	32	2	0.	0.	0.	0.	0.	0.	0.
	9	32	2	0.	0.	0.	0.	0.	0.	0.
	10	32	2	0.	0.	0.	0.	0.	0.	0.
	11	32	2	0.	0.	0.	0.	0.	0.	0.
	12	32	2	0.	0.	0.	0.	0.	0.	0.
	13	32	2	0.	0.	0.	0.	0.	0.	0.
	14	32	2	0.	0.	0.	0.	0.	0.	0.
	15	32	2	0.	0.	0.	0.	0.	0.	0.



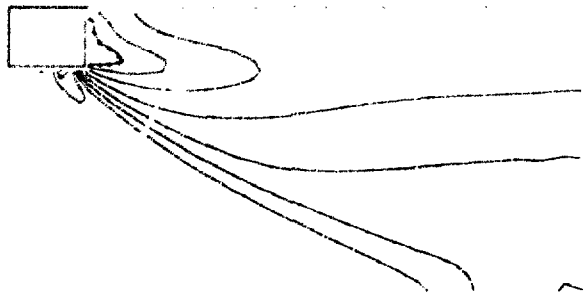
Velocity vectors



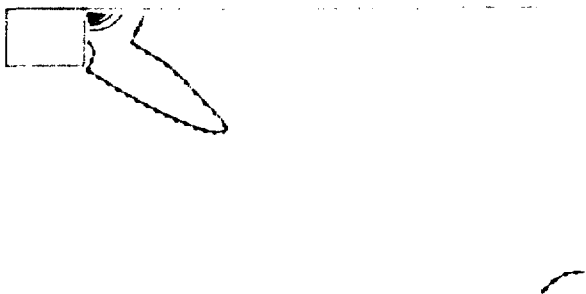
Temperature T , high (H) = 13.6239, low (L) = 2.4502,
interval = 1.3967



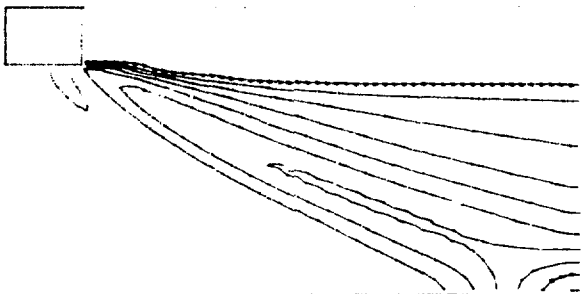
Density ρ , high (H) = 1.5006, low (L) = 0.2787,
interval = 0.1527



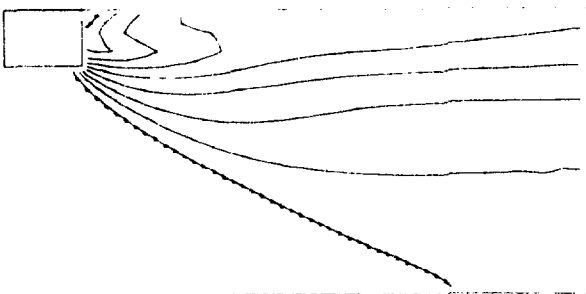
Mach number M , high (H) = 5.0426, low (L) = 0.8328,
interval = 0.5262



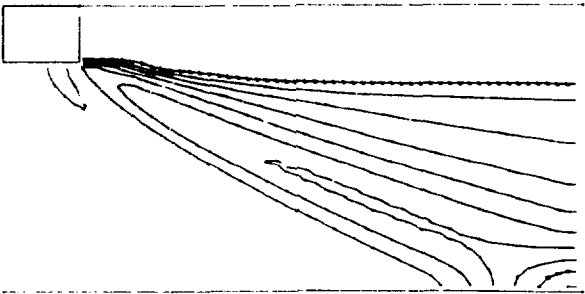
Pressure p , high (H) = 1.8860, low (L) = 0.2483,
interval = 0.2050



Density of N_2 (species A), high (H) = 0.6801,
low (L) = 0.0756, interval = 0.0756

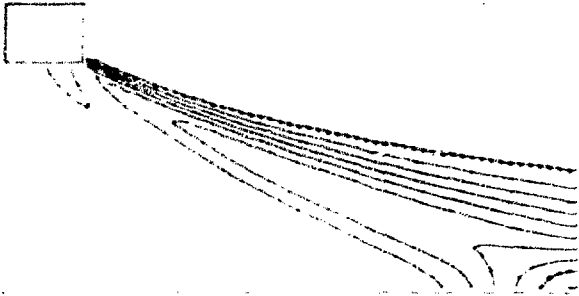


Specific internal energy I , high (H) = 2.8769,
low (L) = 0.5983, interval = 0.2848

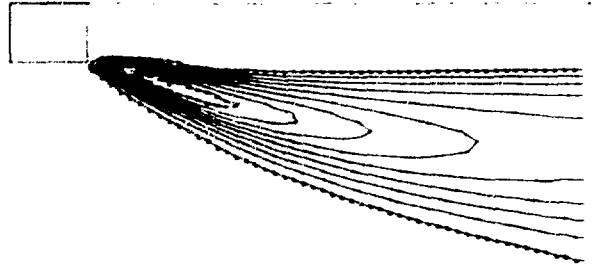


Density of S (species B), high (H) = 0.0140,
low (L) = 0.0016, interval = 0.0016

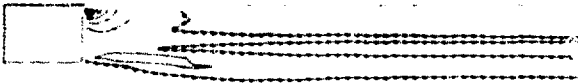
Fig. 10. Plots of the velocity vector field, contours of ρ , p , I , T , Mach number, and species densities, and the distribution of the species in the computing mesh.



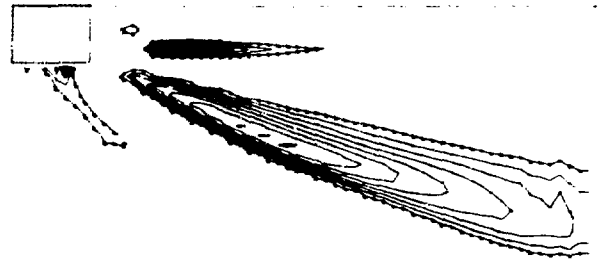
Density of F (species C), high (H) = 0.0500,
low (L) = 0.0056, interval = 0.0056



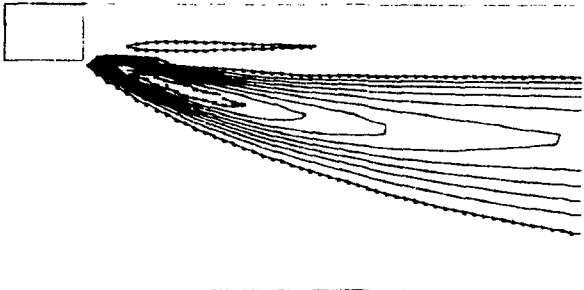
Density of H (species F), high (H) = 0.0011,
low (L) = 0.0001, interval = 0.0001



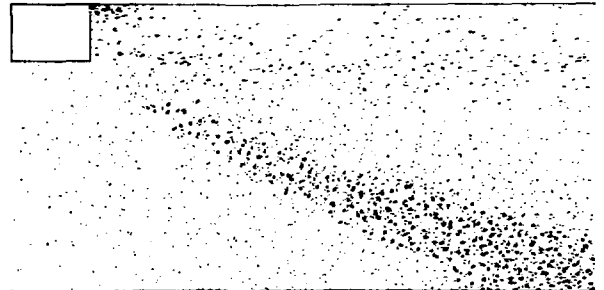
Density of H₂ (species D), high (H) = 1.4913,
low (L) = 0.1657, interval = 0.1657



Density of fictitious species (species G), high
(H) = 0.0034, low (L) = 0.0004, interval = 0.0004



Density of HF (species E), high (H) = 0.0258,
low (L) = 0.0029, interval = 0.0029



Distribution of species densities

Fig. 10 (cont)

TABLE XIII

SOLUTION DATA AT CYCLE = 1000, TIME = 0.5

CYCLE= 1000 TIME= 0.000 RICE L.A. REPORT PROBLEM---8/23/74									
I	J	FL	U	V	RHO	FE	SIE	TEMP.	MU
1	20	5	2.3000E+00	0.	3.3500E-01	6.7662E-02	4.8200E-01	6.5658E+00	7.4000E-04
2	20	1	2.3008E+00	1.1909E-04	3.3496E-01	6.7593E-02	4.8158E-01	6.5601E+00	7.3992E-04
3	20	1	2.3012E+00	6.6789E-04	3.3480E-01	6.7394E-02	4.8038E-01	6.5440E+00	7.3955E-04
4	20	1	2.3005E+00	5.8260E-04	3.3475E-01	6.7338E-02	4.8005E-01	6.5391E+00	7.3945E-04
5	20	1	2.2985E+00	-7.0293E-04	3.3504E-01	6.7643E-02	4.8181E-01	6.5650E+00	7.4000E-04
6	20	1	2.2988E+00	-2.4609E-03	3.3559E-01	6.8224E-02	4.8515E-01	6.6064E+00	7.4129E-04
7	20	1	2.2973E+00	-2.5001E-03	3.3600E-01	6.8626E-02	4.8742E-01	6.6402E+00	7.4220E-04
8	20	1	2.3000E+00	8.5346E-04	3.3569E-01	6.8306E-02	4.8558E-01	6.6164E+00	7.4153E-04
9	20	1	2.3009E+00	6.9191E-03	3.3437E-01	6.6911E-02	4.7755E-01	6.5086E+00	7.3860E-04
10	20	1	2.3123E+00	1.0266E-02	3.3245E-01	6.4705E-02	4.6447E-01	6.3307E+00	7.3436E-04
11	20	1	2.3099E+00	7.5704E-04	3.3163E-01	6.3121E-02	4.5422E-01	6.1881E+00	7.3259E-04
12	20	1	2.2897E+00	-3.3002E-02	3.3516E-01	6.4967E-02	4.6258E-01	6.2928E+00	7.4036E-04
13	20	1	2.2440E+00	-9.5775E-02	3.4731E-01	7.4054E-02	5.0883E-01	6.9062E+00	7.6720E-04
14	20	1	2.1760E+00	-1.7928E-01	3.7192E-01	9.3615E-02	6.0069E-01	8.1308E+00	8.2155E-04
15	20	1	2.1038E+00	-2.6662E-01	4.0967E-01	1.2398E-01	7.2219E-01	9.7564E+00	9.0495E-04
1	21	5	2.3000E+00	0.	3.3500E-01	6.7662E-02	4.8200E-01	6.5658E+00	7.4000E-04
2	21	1	2.3017E+00	2.3551E-04	3.3489E-01	6.7503E-02	4.8102E-01	6.5526E+00	7.3976E-04
3	21	1	2.3020E+00	9.9807E-04	3.3458E-01	6.7139E-02	4.7886E-01	6.5231E+00	7.3908E-04
4	21	1	2.2993E+00	1.9459E-04	3.3471E-01	6.7294E-02	4.7979E-01	6.5347E+00	7.3936E-04
5	21	1	2.2956E+00	-2.4822E-03	3.3548E-01	6.8166E-02	4.8489E-01	6.6037E+00	7.4107E-04
6	21	1	2.2948E+00	-4.4699E-03	3.3635E-01	6.9109E-02	4.9033E-01	6.6783E+00	7.4299E-04
7	21	1	2.2995E+00	-1.3272E-03	3.3630E-01	6.9001E-02	4.8963E-01	6.6711E+00	7.4208E-04
8	21	1	2.3088E+00	7.0977E-03	3.3461E-01	6.7154E-02	4.7893E-01	6.5273E+00	7.3915E-04
9	21	1	2.3175E+00	1.3783E-02	3.3180E-01	6.3932E-02	4.5981E-01	6.2677E+00	7.3294E-04
10	21	1	2.3147E+00	4.2426E-03	3.3024E-01	6.1563E-02	4.4488E-01	6.0600E+00	7.2948E-04
11	21	1	2.2865E+00	-3.6619E-02	3.3435E-01	6.4243E-02	4.5853E-01	6.2390E+00	7.3857E-04
12	21	1	2.2230E+00	-1.1088E-01	3.4968E-01	7.7114E-02	5.2628E-01	7.1346E+00	7.7242E-04
13	21	1	2.1385E+00	-2.0803E-01	3.8027E-01	1.0379E-01	6.5134E-01	8.8033E+00	8.4000E-04
14	21	1	2.0576E+00	-2.9543E-01	4.2435E-01	1.4305E-01	8.0425E-01	1.0800E+01	9.3730E-04
15	21	1	1.9972E+00	-3.6404E-01	4.7301E-01	1.8736E-01	9.4472E-01	1.2483E+01	1.0440E-03
1	22	5	2.3000E+00	0.	3.3500E-01	6.7662E-02	4.8200E-01	6.5658E+00	7.4000E-04
2	22	1	2.3032E+00	3.6838E-04	3.3475E-01	6.7336E-02	4.8004E-01	6.5393E+00	7.3945E-04
3	22	1	2.3022E+00	1.4077E-03	3.3429E-01	6.6804E-02	4.7689E-01	6.4954E+00	7.3843E-04
4	22	1	2.2957E+00	-7.5382E-04	3.3492E-01	6.7573E-02	4.8148E-01	6.5565E+00	7.3982E-04
5	22	1	2.2900E+00	-5.0152E-03	3.3653E-01	6.9460E-02	4.9256E-01	6.7069E+00	7.4338E-04
6	22	1	2.2940E+00	-5.9100E-03	3.3733E-01	7.0344E-02	4.9764E-01	6.7784E+00	7.4514E-04
7	22	1	2.3093E+00	4.7205E-03	3.3549E-01	6.8177E-02	4.8496E-01	6.6097E+00	7.4107E-04
8	22	1	2.3248E+00	1.7365E-02	3.3132E-01	6.3361E-02	4.5636E-01	6.2218E+00	7.3188E-04
9	22	1	2.3235E+00	1.1771E-02	3.2821E-01	5.9278E-02	4.3101E-01	5.8718E+00	7.2500E-04
10	22	1	2.2847E+00	-3.3734E-02	3.3233E-01	6.2571E-02	4.4931E-01	6.1065E+00	7.3410E-04
11	22	1	2.2001E+00	-1.1874E-01	3.5077E-01	8.0224E-02	5.4582E-01	7.3909E+00	7.7483E-04
12	22	1	2.0959E+00	-2.2177E-01	3.8723E-01	1.1579E-01	7.1358E-01	9.6332E+00	8.5538E-04
13	22	1	2.0054E+00	-3.1213E-01	4.3623E-01	1.6530E-01	9.0402E-01	1.1995E+01	9.6361E-04
14	22	1	1.9414E+00	-3.7206E-01	4.8464E-01	2.1610E-01	1.0645E+00	1.3730E+01	1.0706E-03
15	22	1	1.9003E+00	-4.0047E-01	5.1950E-01	2.5677E-01	1.1824E+00	1.4664E+01	1.1476E-03

TABLE XIII (cont)

CYCLE= 1000 TIME= 0.000 RICE L.A. REPORT PROBLEM--8/23/74

SPECIES DENSITIES									
I	J	FL	A	B	C	D	E	F	G
1	20	5	3.0600E-01	6.3000E-03	2.2500E-02	0.	0.	0.	0.
2	20	1	3.0596E-01	6.2993E-03	2.2497E-02	5.4570E-08	3.8801E-08	1.9873E-09	2.0292E-04
3	20	1	3.0580E-01	6.2960E-03	2.2486E-02	-4.6779E-08	-4.0536E-08	3.4059E-10	2.1054E-04
4	20	1	3.0578E-01	6.2955E-03	2.2484E-02	1.4885E-08	6.6898E-08	1.4890E-09	1.9299E-04
5	20	1	3.0604E-01	6.3009E-03	2.2503E-02	-1.4365E-07	-1.0777E-07	-5.8626E-09	1.9050E-04
6	20	1	3.0655E-01	6.3114E-03	2.2540E-02	-1.2616E-07	1.5271E-07	-7.0183E-09	1.8066E-04
7	20	1	3.0688E-01	6.3182E-03	2.2565E-02	-8.3502E-08	-2.3883E-07	1.9164E-08	2.3236E-04
8	20	1	3.0655E-01	6.3113E-03	2.2540E-02	1.8115E-08	5.3956E-07	3.5999E-08	2.9206E-04
9	20	1	3.0525E-01	6.2847E-03	2.2446E-02	4.5479E-07	-6.4176E-07	6.9003E-08	3.7978E-04
10	20	1	3.0349E-01	6.2484E-03	2.2314E-02	-1.1610E-07	2.0001E-06	-1.0295E-08	3.8932E-04
11	20	1	3.0288E-01	6.2359E-03	2.2273E-02	-1.6426E-06	-3.6463E-06	1.2698E-07	2.3854E-04
12	20	1	3.0655E-01	6.3114E-03	2.2538E-02	6.6178E-07	5.0662E-06	-8.8003E-08	-2.4554E-04
13	20	1	3.1840E-01	6.5552E-03	2.3415E-02	-1.4757E-05	-1.0532E-05	-2.9155E-06	-1.0234E-03
14	20	1	3.4187E-01	7.0386E-03	2.5134E-02	-6.8179E-06	1.3764E-05	-1.7289E-06	-2.1354E-03
15	20	1	3.7733E-01	7.7606E-03	2.7742E-02	-5.5459E-06	-3.0017E-05	-2.2608E-06	-3.1296E-03
1	21	5	3.0600E-01	6.3000E-03	2.2500E-02	0.	0.	0.	0.
2	21	1	3.0596E-01	6.2979E-03	2.2492E-02	1.4638E-07	4.2304E-08	5.6744E-09	2.0367E-04
3	21	1	3.0562E-01	6.2922E-03	2.2473E-02	-2.3749E-07	4.9721E-08	-1.6699E-09	1.9853E-04
4	21	1	3.0579E-01	6.2956E-03	2.2484E-02	5.1168E-08	-1.7754E-08	-1.4140E-09	1.4216E-04
5	21	1	3.0651E-01	6.3104E-03	2.2538E-02	-8.0180E-07	1.2823E-07	-2.7429E-08	1.2951E-04
6	21	1	3.0728E-01	6.3263E-03	2.2593E-02	-1.8719E-08	-1.9978E-07	2.9814E-08	1.5470E-04
7	21	1	3.0713E-01	6.3232E-03	2.2584E-02	1.9185E-07	5.2214E-07	1.0454E-07	2.6800E-04
8	21	1	3.0548E-01	6.2894E-03	2.2460E-02	8.4140E-07	-4.3929E-07	1.1847E-07	3.6123E-04
9	21	1	3.0286E-01	6.2353E-03	2.2271E-02	1.3265E-06	1.9189E-06	1.1961E-07	4.3729E-04
10	21	1	3.0166E-01	6.2106E-03	2.2177E-02	-3.5792E-06	-2.1926E-06	1.0179E-07	1.9579E-04
11	21	1	3.0594E-01	6.2988E-03	2.2500E-02	-4.2569E-06	4.7192E-06	1.2076E-07	-3.8974E-04
12	21	1	3.2095E-01	6.6078E-03	2.3593E-02	-1.0955E-05	-5.9236E-06	-2.1776E-06	-1.4544E-03
13	21	1	3.5007E-01	7.2073E-03	2.5753E-02	-5.6918E-05	2.3905E-06	-9.9674E-06	-2.6992E-03
14	21	1	3.9105E-01	8.0513E-03	2.8656E-02	1.3989E-04	3.6616E-06	2.5478E-05	-3.5758E-03
15	21	1	4.3508E-01	8.9584E-03	3.1195E-02	6.4787E-04	5.7739E-04	1.1430E-04	-3.5654E-03
1	22	5	3.0600E-01	6.3000E-03	2.2500E-02	0.	0.	0.	0.
2	22	1	3.0575E-01	6.2949E-03	2.2481E-02	6.2118E-07	3.9903E-07	2.1960E-08	2.1959E-04
3	22	1	3.0539E-01	6.2875E-03	2.2455E-02	-1.3117E-06	-2.4807E-07	-2.5622E-08	1.5830E-04
4	22	1	3.0603E-01	6.3007E-03	2.2502E-02	-1.0119E-07	3.5852E-07	-1.3895E-08	0.3829E-05
5	22	1	3.0752E-01	6.3314E-03	2.2612E-02	-3.5302E-06	-6.0311E-07	-0.4672E-08	6.6052E-05
6	22	1	3.0810E-01	6.3433E-03	2.2656E-02	3.3048E-06	5.5372E-07	2.4046E-07	2.2199E-04
7	22	1	3.0625E-01	6.3052E-03	2.2514E-02	1.8407E-06	1.5779E-06	3.9179E-07	4.1152E-04
8	22	1	3.0233E-01	6.2244E-03	2.2232E-02	3.9390E-06	1.3928E-06	2.2659E-07	5.3149E-04
9	22	1	2.9977E-01	6.1717E-03	2.2031E-02	-2.3675E-06	3.1833E-06	5.2720E-07	2.3830E-04
10	22	1	3.0425E-01	6.2640E-03	2.2380E-02	-2.6937E-05	2.9107E-07	-5.6434E-08	-5.4240E-04
11	22	1	3.2233E-01	6.6362E-03	2.3678E-02	-1.8699E-05	7.6912E-06	-1.6372E-06	-1.8660E-03
12	22	1	3.5689E-01	7.3476E-03	2.6272E-02	-5.1153E-05	-4.5554E-05	-7.6440E-06	-3.1700E-03
13	22	1	4.0178E-01	8.2727E-03	2.9231E-02	4.9362E-04	1.2341E-04	6.0161E-05	-3.7334E-03
14	22	1	4.4460E-01	9.1555E-03	3.0763E-02	1.5051E-03	1.4974E-03	1.8503E-04	-3.0623E-03
15	22	1	4.7361E-01	9.7542E-03	2.9459E-02	3.0673E-03	4.6584E-03	3.7182E-04	-1.4200E-03

REFERENCES

1. W. C. Rivard, T. D. Butler, and O. A. Farmer, "Numerical Calculations of Viscous Supersonic Jet Mixing," Los Alamos Scientific Laboratory report (to be published).
 2. F. H. Harlow and A. A. Amsden, "A Numerical Fluid Dynamics Calculation Method for All Flow Speeds," J. Comp. Phys. 8, 197-213 (1971).
 3. A. J. Chorin, "Numerical Study of Thermal Convection in a Fluid Layer Heated from Below," AEC report NYO-1480-61 (August 1966).
 4. C. W. Hirt and J. L. Cook, "Calculating Three-Dimensional Flows around Structures and over Rough Terrain," J. Comp. Phys. 10, 324-340 (1972).
 5. R. B. Bird, W. E. Stewart, and E. N. Lightfoot, Transport Phenomena (John Wiley and Sons, Inc., New York, 1960), Chap. 16, p. 502.
 6. W. C. Rivard, O. A. Farmer, T. D. Butler, and P. J. O'Rourke, "A Method for Increased Accuracy in Eulerian Fluid Dynamics Calculations," Los Alamos Scientific Laboratory report LA-5426-MS (October 1973).
 7. A. A. Amsden and F. H. Harlow, "The SMAC Method: A Numerical Technique for Calculating Incompressible Fluid Flows," Los Alamos Scientific Laboratory report LA-4370 (May, 1970).
 8. T. D. Butler, "Recent Advances in Computational Fluid Dynamics," in Computing Methods in Applied Sciences and Engineering, Part 2, Lecture Notes in Computer Science no. 11 (1974).
 9. H. Nirels and D. J. Spencer, "Power and Efficiency of a Continuous HF Chemical Laser," IEEE J. Quant. Elect. 7, 501-507 (1971).
 10. N. Cohen, "A Review of Rate Coefficients for Reactions in the H_2-F_2 Laser System," Aerospace Corp. report TR-0172(2779)-2 (1971).
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APPENDIX A

DEFINITION OF FORTRAN VARIABLES

The FORTRAN variables that appear in COMMON storage or that are used for input data are defined here in alphabetical order. The input data is defined in detail, card by card, in Sec. IV so that input variables are defined here by referencing the particular data card on which they appear.

FORTRAN Symbol	Algebraic Symbol	Definition
ALA	A	Input data card no. 8.
ALPHA(K)	α_k	Input data card no. 26.
AM(K,L)	$a_{k,l}$	Input data card no. 27.
ASQ	-	Input data card no. 8.
BIE	b	Input data card no. 8.
BM(K,L)	$b_{k,l}$	Input data card no. 27.
CB(L)	C_l	Input data card no. 27.
CF(L)	C_l	Input data card no. 27.
CQ(I,J)	-	Dummy array used to store variables for plotting.
CSQ(I,J)	$(c^2)_{i,j}$	Square of the adiabatic sound speed. Computed in subroutine PRDG as $c^2 = \gamma(\gamma - 1)I$.
CV(K)	$(C_v)_k$	Input data card no. 25.
CYCLE	-	Input data card no. 6.
DDX	-	Reciprocal of δz (δx). Computed in subroutine CVIC.
DDY	-	Reciprocal of δr (δy). Computed in subroutine CVIC.
DEN	ρ_s	Input data card no. 4.
DRHOB(I,K)	-	Temporary storage for the mass flux of species k across the top boundary of cell (i,j) produced by molecular diffusion to be used later as the mass flux across the bottom boundary of cell (i,j+1). Computed in subroutine SPEC as $(\delta f_k)_{i,j+1}$ according to Eq. (3.23).
DT	δt	Input data card no. 7.
DTC	δt_c	Input data card no. 7.
DX	$\delta z(dx)$	Input data card no. 7.
DXO	-	Input data card no. 8.
DY	$\delta r(\delta y)$	Input data card no. 7.
EB(L)	E_l^+	Input data card no. 27.
EF(L)	E_l^-	Input data card no. 27.
EP(K)	-	Input data card no. 23.
ERRD	ϵ	Deviation from zero for convergence of the pressure iteration. Computed in subroutine CVIC as $\epsilon = 10^{-5} \rho_0$.
ETA(I,J)	$\eta_{i,j}$	Factor for the calculation of the molecular diffusion coefficients, $b_k = v_k \eta$. Computed in subroutine SPEC as $\eta = \eta_0 T^{3/2}/p$.
ETAO	η_0	Input data card no. 14.
FA(I,J,K)	$(\rho_k)_{i,j}$	Density of species k in cell (i,j).
FABO(K,N)	-	Input data card no. 32.
FAL1(K)	-	Input data card no. 15.
FAL2(K)	-	Input data card no. 15.
FAO(K)	-	Input data card no. 15.
FARO(K,N)	-	Input data card no. 31.

<u>FØRTRAN</u> <u>Symbol</u>	<u>Algebraic</u> <u>Symbol</u>	<u>Definition</u>
FAT1(K)	-	Input data card no. 15.
FAT2(K)	-	Input data card no. 15.
FL(1,J)	-	Cell flags (see Table I). Computed in subroutine FLIC.
FLØ(M)	-	Input data card no. 9.
GAMA(K)	γ_k	Input data card no. 24.
GAMMA	γ	Input data card no. 8.
IB	-	Number of cells in the z(x)-direction excluding the two fictitious columns along the right and left boundaries of computing mesh. Computed in program RICE as $IB = IB2-2$.
IB1	-	Computed in program RICE as $IB1 = IB2-1$.
IB2	-	Input data cards no. 1 and no. 6.
ISPEC(K)	-	Input data card no. 6.
IT	-	The number of iterations performed to satisfy Eq. (3.10).
ITC	-	Input data card no. 6.
ITD	-	Input data card no. 5.
ITMAX	-	The maximum number of iterations allowed for any cell when attempting to satisfy Eq. (3.10). Set in subroutine CVIC as $ITMAX = 1000$.
ITØ(N)	-	Input data card no. 28.
JB	-	Number of cells in the r(y)-direction excluding the two fictitious rows along the bottom and top boundaries of computing mesh. Computed in program RICE as $JB = JB2-2$.
JB1	-	Computed in program RICE as $JB1 = JB2-1$.
JB2	-	Input data cards no. 1 and no. 6.
JNM	-	Job identification obtained from the JØB card and printed on film.
JPLOT(M)	-	Input data card no. 6.
LPR	-	Input data card no. 6.
MINBØ(N)	-	Input data card no. 30.
MINT1	-	Input data card no. 12.
MINT2	-	Input data card no. 12.
MU(1,J)	$\mu_{i,j}$	Shear viscosity. Computed in subroutine PRØG according to Eq. (3.43).
MUØ	μ_0	Input data card no. 12.
NAME(M)	-	Input data card no. 3.
NCYDMP	-	The number of cycles between writes (dumps) on TAPE5 as specified by the input variable NSDMP. Set in program RICE as $NCYDMP = NSDMP$.
NFILE	-	Input data card no. 5.
NØ	-	Input data card no. 6.
NR	-	Input data card no. 6.
NSDMP	-	Input data card no. 5.
NSL(M)	-	Input data card no. 6.
NSØ(N)	-	Input data card no. 28.
NSPEC	-	Input data cards no. 1 and no. 6.
NTD	-	Input data card no. 5.
NWDMP	-	Input data card no. 5.
ØB(M,N)	-	Input data card no. 28.
ØIB(M,N)	-	Input data card no. 28.
ØMEGA	-	Input data card no. 8.

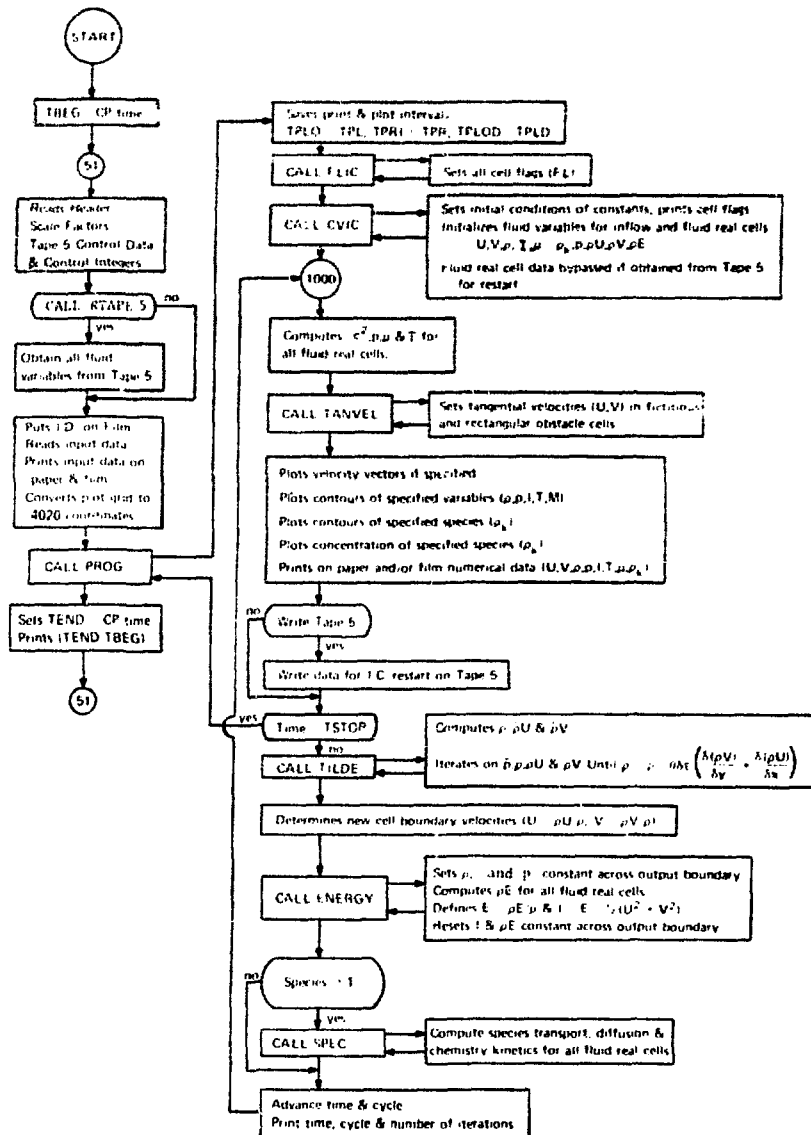
FORTTRAN Symbol	Algebraic Symbol	Definition
P(I,J)	$P_{i,j}$	Final static pressure of the mixture. Computed in subroutine PRØG according to Eq. (3.36).
PB(I,J)	$\bar{P}_{i,j}$	Temporary static pressure of the mixture obtained by the pressure iteration. Computed in subroutine TILDE according to Eqs. (3.12).
PFAC	-	Term used in the pressure iteration for the calculation of the increment \bar{p} given by Eq. (3.11). Computed in subroutine CVIC as $PFAC = 2\phi\delta t^2 (\delta r^{-2} + \delta z^{-2})$.
PHI	ϕ	Input data card no. 8.
Q(L)	q_L	Input data card no. 27.
RE(I,J)	$(\rho E)_{i,j}$	Total energy density. Computed in subroutine ENERGY according to Eq. (3.15) and updated in SPEC according to Eqs. (3.28) and (3.34).
RFLB(I)	-	Temporary storage for the mixture mass flux across the top boundary of cell (i,j) to be used later as the flux across the bottom boundary of cell (i,j+1).
RHØ(I,J)	$\rho_{i,j}$	Mass density of the mixture. Computed in subroutine TILDE according to Eq. (3.1).
RHØØ	ρ_o	Input data card no. 11.
RHØT(I,J)	$\tilde{\rho}_{i,j}$	Tilde value of the mixture density. Computed in subroutine TILDE according to Eq. (3.2).
RHØU(I,J)	$(\rho u)_{i+\frac{1}{2},j}$	Axial component of momentum density. Computed in subroutine TILDE according to Eq. (3.9).
RHØUT(I,J)	$(\rho u)_{i+\frac{1}{2},j}$	Tilde value of the axial component of momentum density. Computed in subroutine TILDE according to Eq. (3.9).
RHØV(I,J)	$(\rho v)_{i,j+\frac{1}{2}}$	Radial component of momentum density. Computed in subroutine TILDE according to Eq. (3.6).
RHØVT(I,J)	$(\tilde{\rho} v)_{i,j+\frac{1}{2}}$	Tilde value of the radial component of momentum density. Computed in subroutine TILDE according to Eq. (3.8).
RINBØ(N)	-	Input data card no. 30.
RINL1	-	Input data card no. 11.
RINL2	-	Input data card no. 11.
RINRØ(N)	-	Input data card no. 29.
RINT1	-	Input data card no. 11.
RINT2	-	Input data card no. 11.
RJ(J)	r_j	Radial coordinate of the center of the (J)th row of computational cells. Computed in subroutine CVIC as $RJ(J) = (J-1)\delta r - \delta r/2$.
RJ2(J)	$r_{j+\frac{1}{2}}$	Radial coordinate of the top boundary of (J)th row of computational cells. Computed in subroutine CVIC as $RJ2(J) = (J-1)\delta r$.
RRHØ	ρ_o^{-1}	Reciprocal of the initial density ρ . Computed in subroutine CVIC.
SECREQ	-	Computer time requested for the problem in seconds. Computed in program RICE from JØB card data.
SIE(I,J)	$I_{i,j}$	Specific internal energy. Computed in subroutine ENERGY according to Eq. (3.16) and updated in subroutine SPEC following the updates of the total energy density according to Eqs. (3.28) and (3.34).
SIEBØ(N)	-	Input data card no. 30.
SIEL1	-	Input data card no. 13.
SIEL2	-	Input data card no. 13.
SIEØ	-	Input data card no. 13.
SIERØ(N)	-	Input data card no. 29.
SIET1	-	Input data card no. 13.

<u>FORTRAN</u> <u>Symbol</u>	<u>Algebraic</u> <u>Symbol</u>	<u>Definition</u>
SIET2	-	Input data card no. 13.
SLG	l_s	Input data card no. 4.
SM(K)	M_k	Input data card no. 22.
SMØ	M_s	Input data card no. 4.
STREB(I)	-	Temporary storage for the energy flux across the top boundary of cell (i,j) to be used later as the flux across the bottom boundary of cell (i,j+1).
TBEG	-	Time at the beginning of the program execution.
TE(i,j)	$T_{i,j}$	Computed in program RICE. Temperature computed according to Eq. (3.25) following the solutions of Eq. (3.21), (3.28), and (3.34).
TEM	T_s	Input data card no. 4.
TFAB(I,K)	-	Temporary storage for the mass flux of species k across the top boundary of cell (i,j) to be used later as the flux across the bottom boundary of cell (i,j+1).
THETA	"	Input data card no. 8.
TIME	-	Input data card no. 7.
TPL	-	Input data card no. 7.
TPLD	-	Input data card no. 7.
TPR	-	Input data card no. 7.
TSTØP	-	Input data card no. 7.
U(I,J)	$u_{i+1/2,j}$	Axial component of velocity. Computed in subroutine PRØG according to Eq. (3.14).
UCØN	-	Factor used in the pressure iteration, Eq. (3.13).
UINL1	-	Input data card no. 10.
UINL2	-	Input data card no. 10.
UINRØ(N)	-	Input data card no. 29.
UØ	-	Input data card no. 10.
V(I,J)	$v_{i,j+1/2}$	Radial component of velocity. Computed in subroutine PRØG according to Eq. (3.14).
VCØN	-	Factor used in the pressure iteration, Eq. (3.13). Computed in CVIC as $VCØN = \rho \delta t / \delta r$.
VEL	u_s	Input data card no. 4.
VINBØ(N)	-	Input data card no. 30.
VINT1	-	Input data card no. 10.
VINT2	-	Input data card no. 10.
VØ	-	Input data card no. 10.
XI	ξ	Parameter used in the calculation of τ and β in Eqs. (3.5) and (3.20). Set in subroutine CVIC as $XI = 1$.
ZETAB(L)	ζ_Q	Input data card no. 27.
ZETAF(L)	ζ_f	Input data card no. 27.

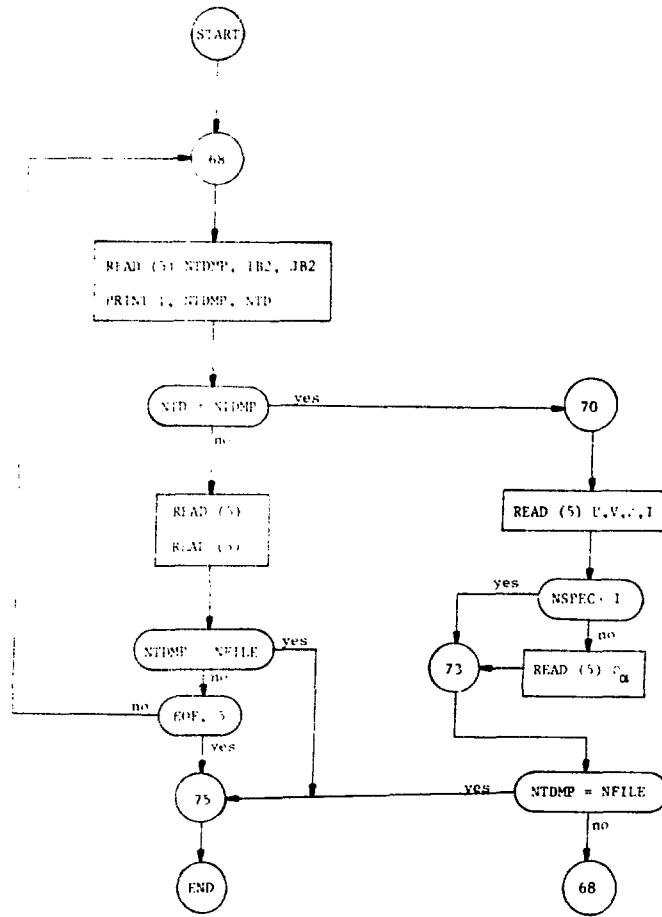
APPENDIX B

FLOW DIAGRAMS FOR RICE SUBROUTINES

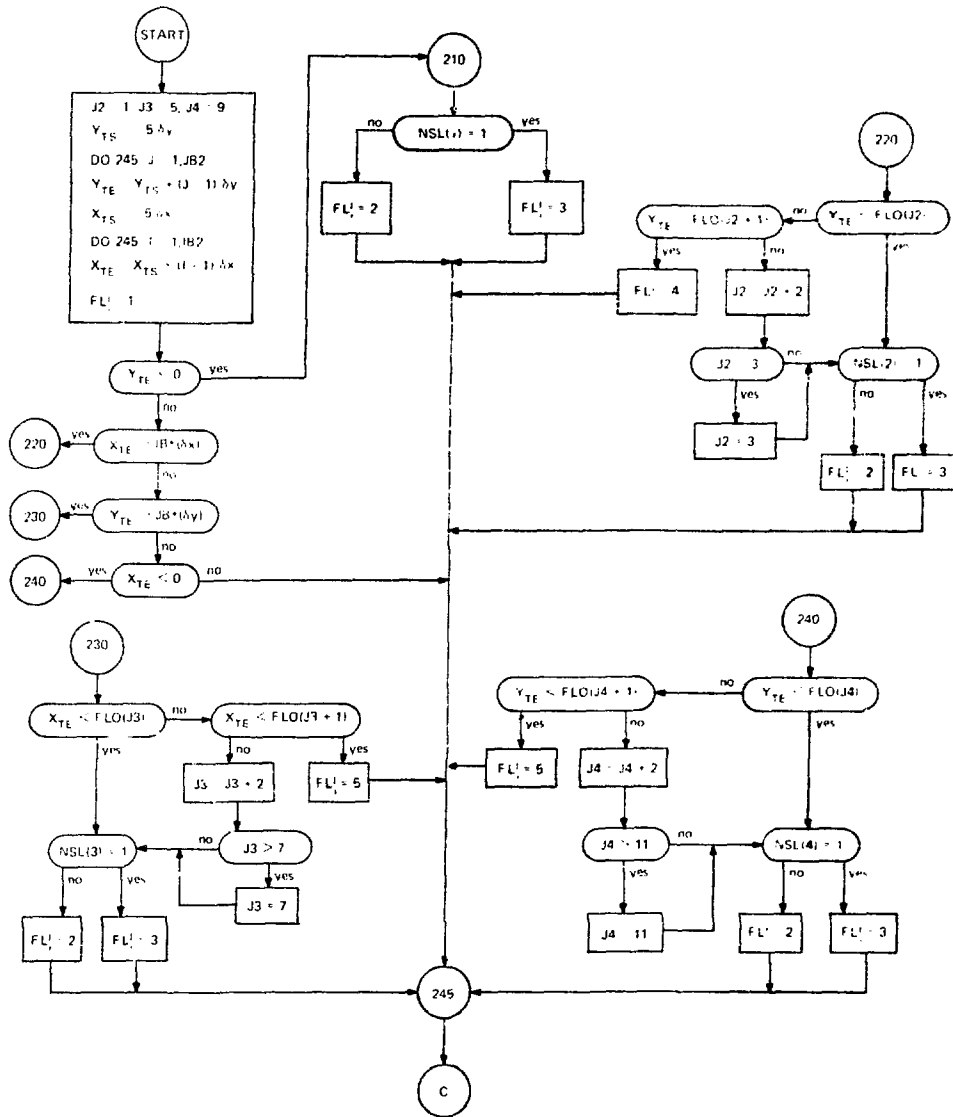
Flow diagrams for each subroutine of the RICE program are presented in this appendix except for the three subroutines VPLLOT, CNFLOT, and COUTOT which deal entirely with plotting. A FORTRAN listing of these subroutines is given in Appendix C along with the listings of the other subroutines. The flow diagrams presented here are for RICE, PROG, RTAPE5, FLIC, CVIC, TANVEL, ENERGY, and SPEC in that order.

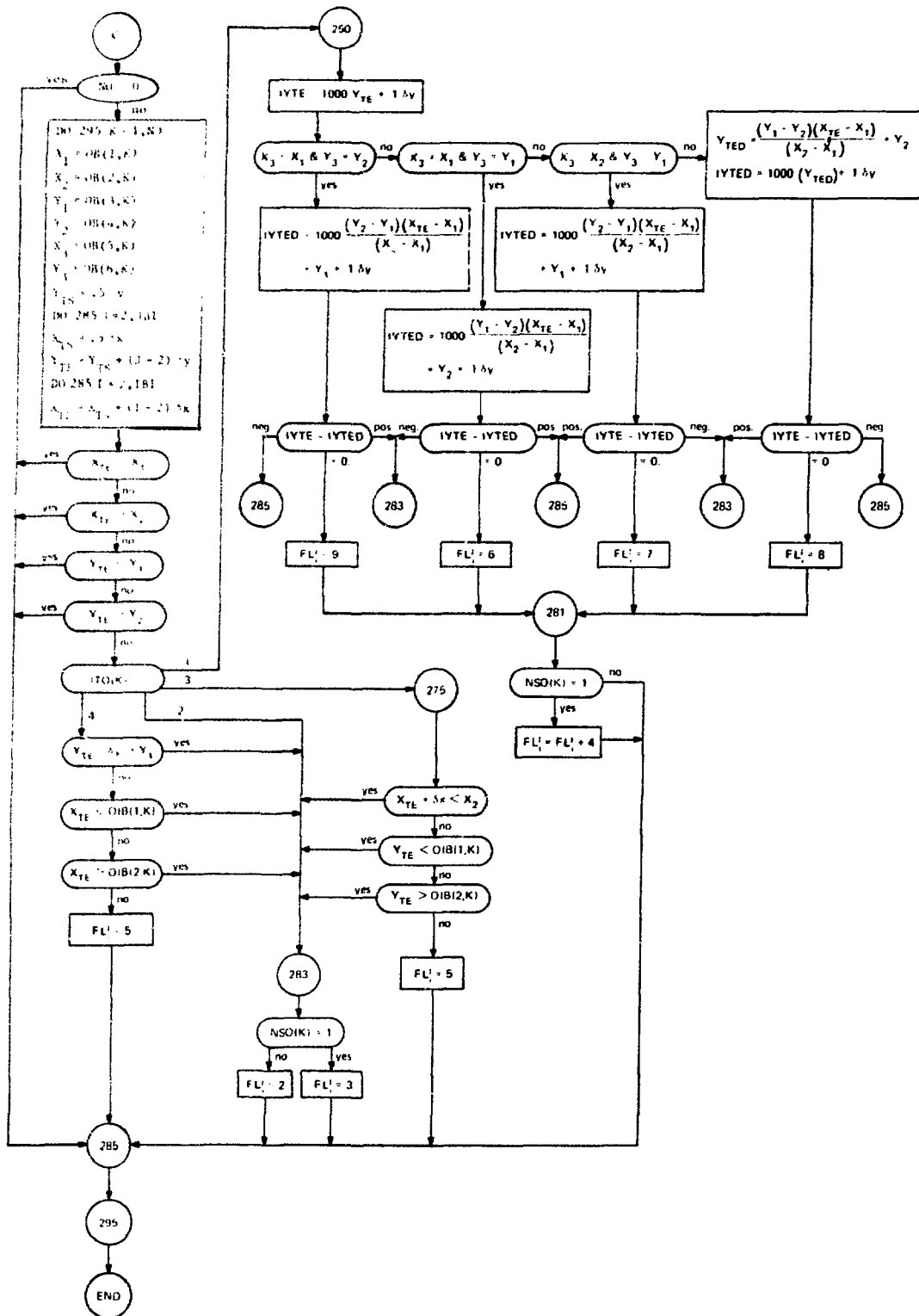


SUBROUTINE RTAPE 5

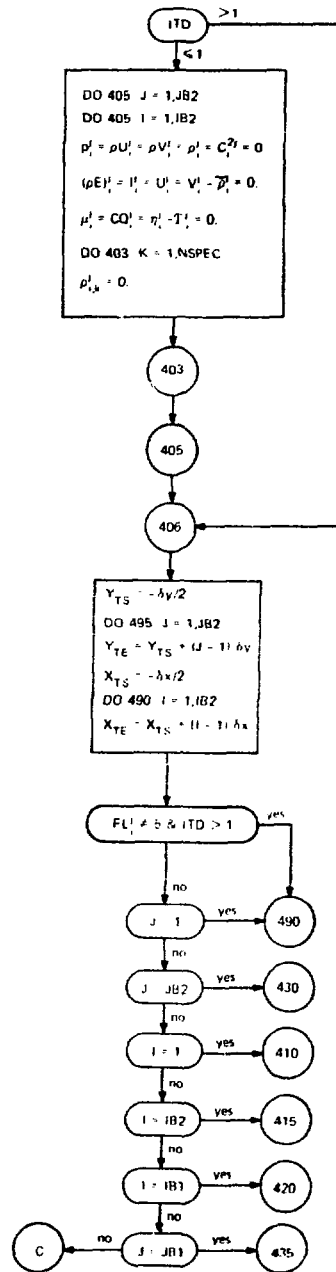
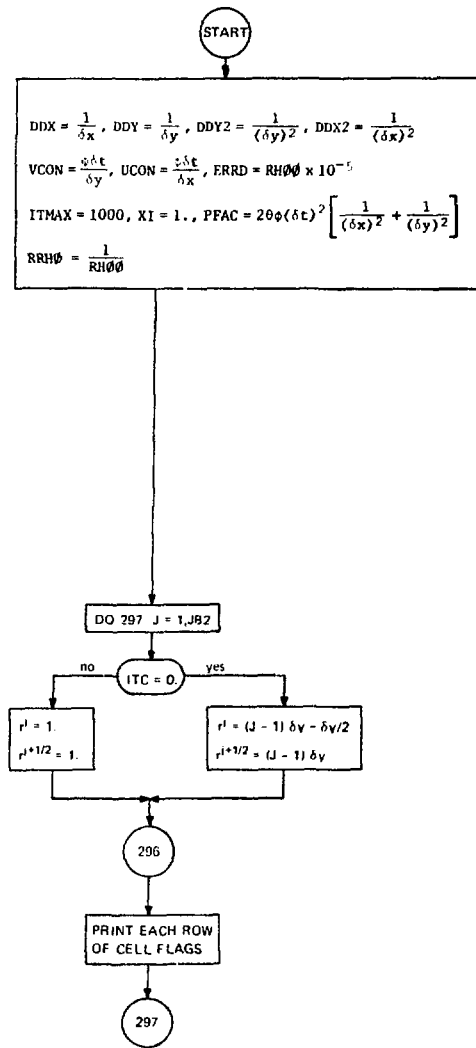


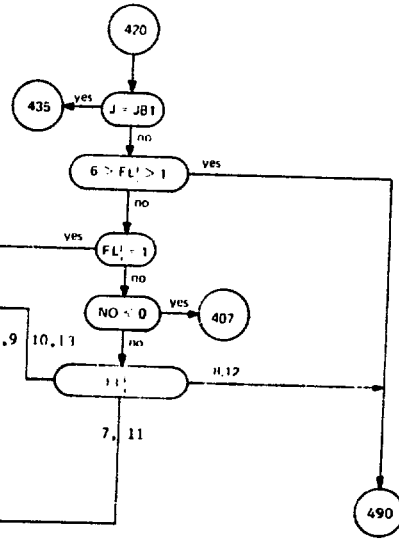
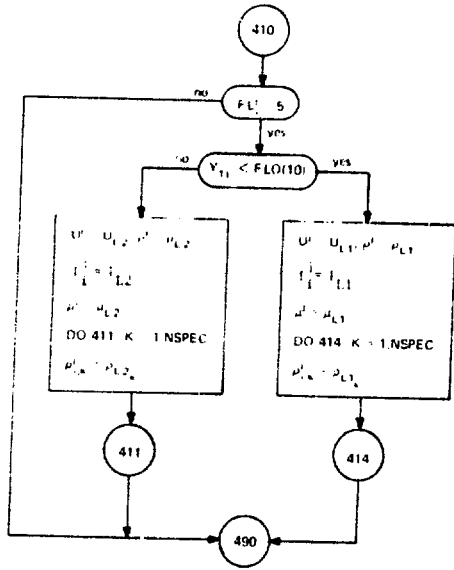
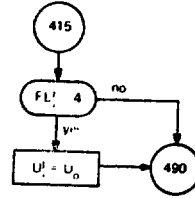
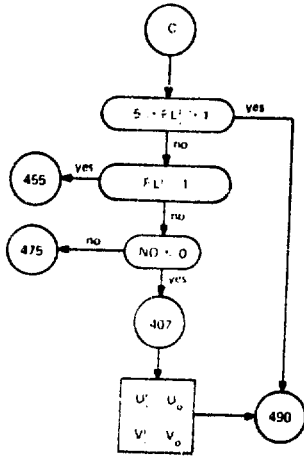
SUBROUTINE FLIC
(Sets cell flags)

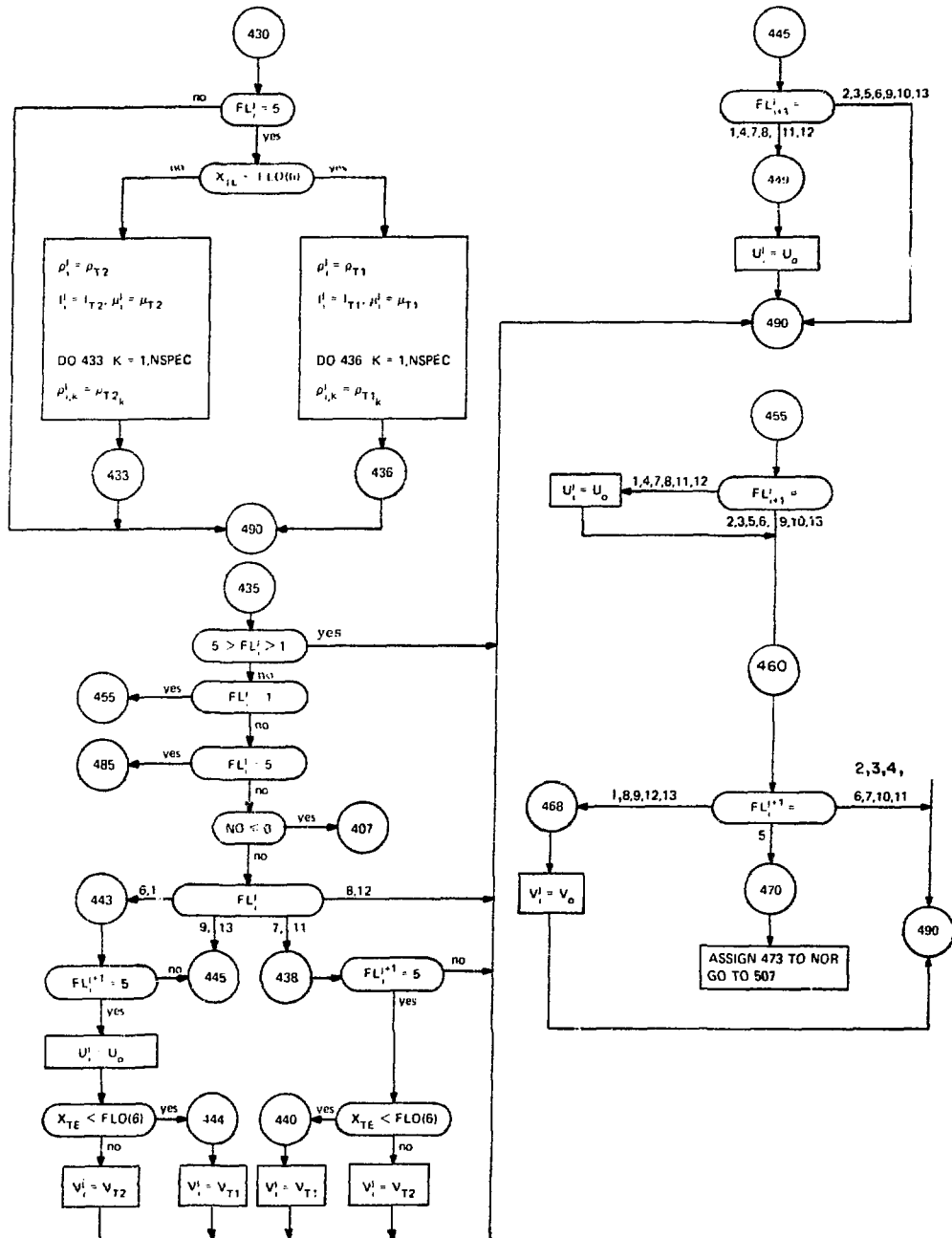


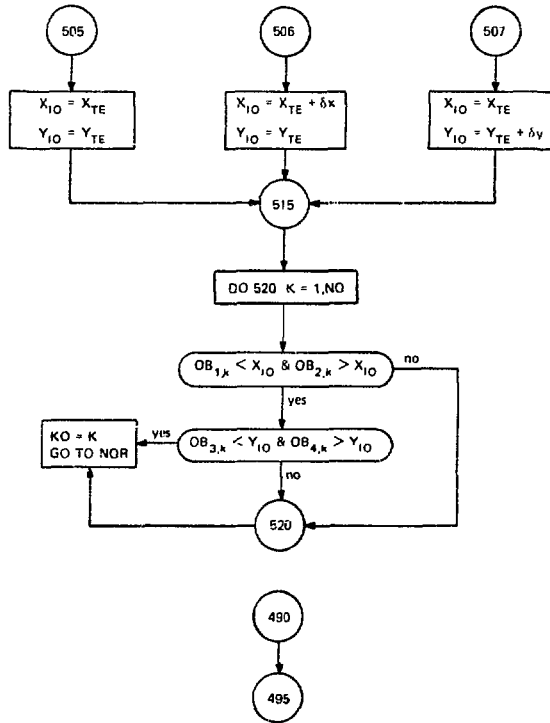
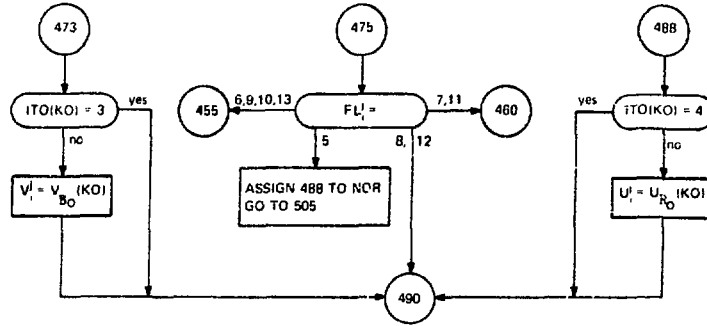


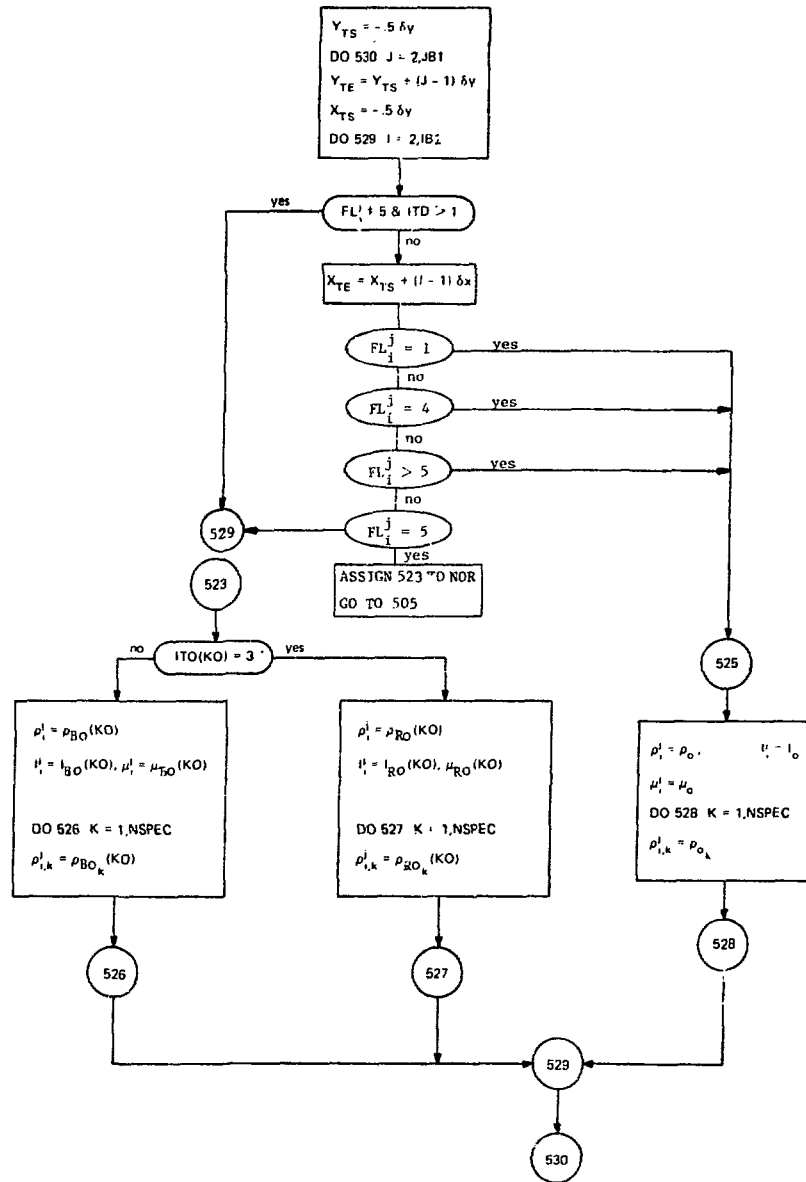
SUBROUTINE CVIC

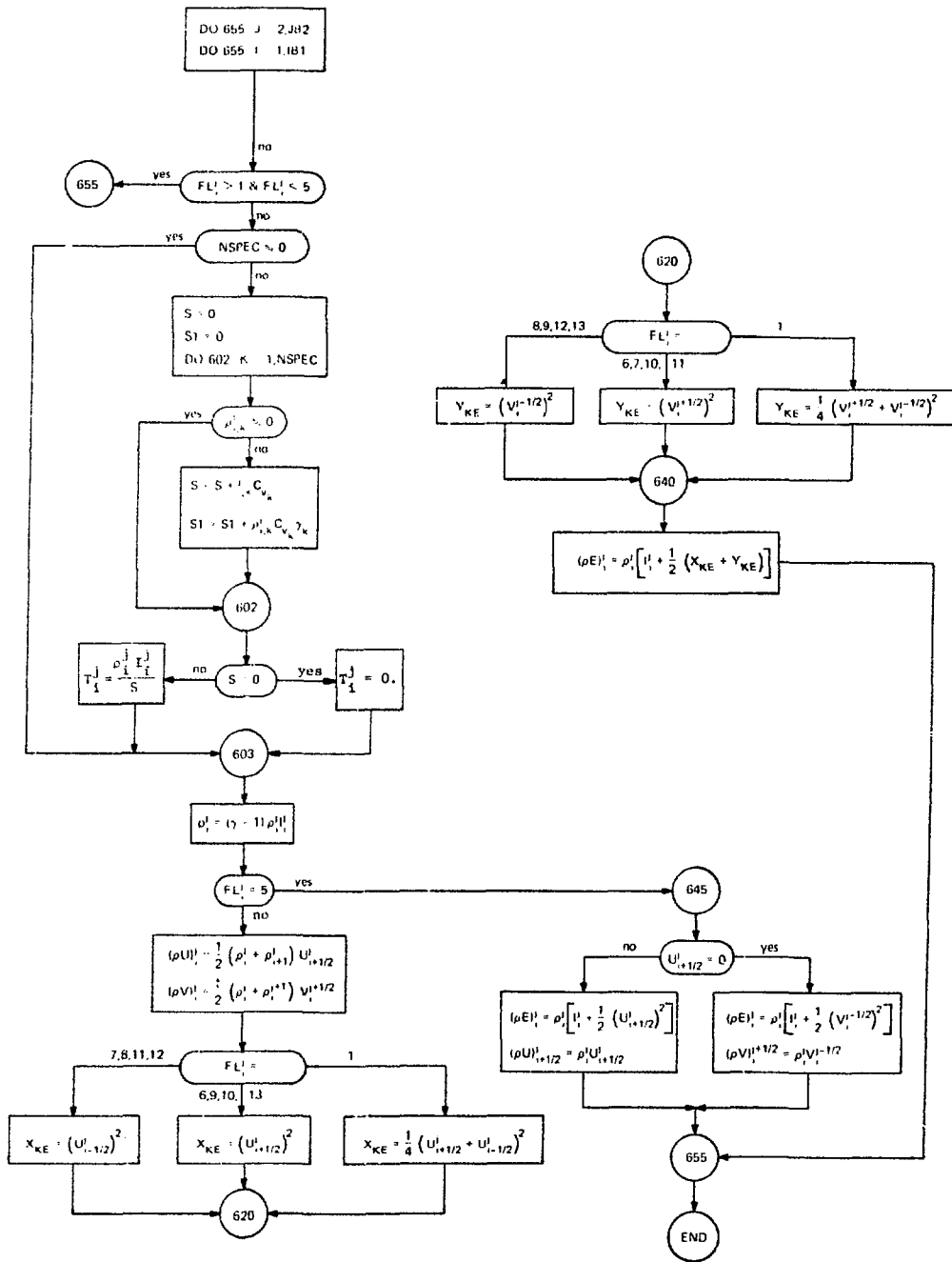




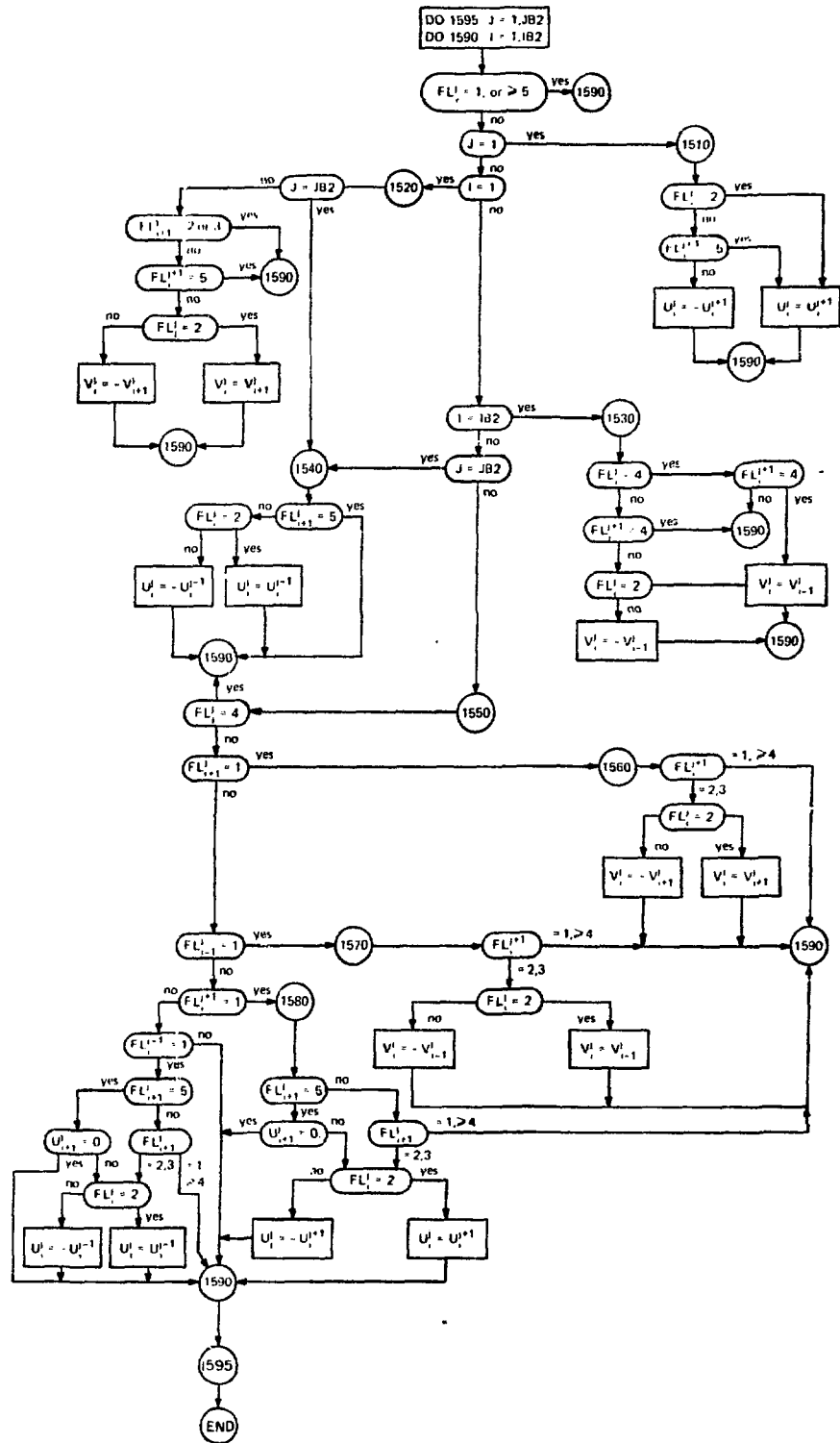




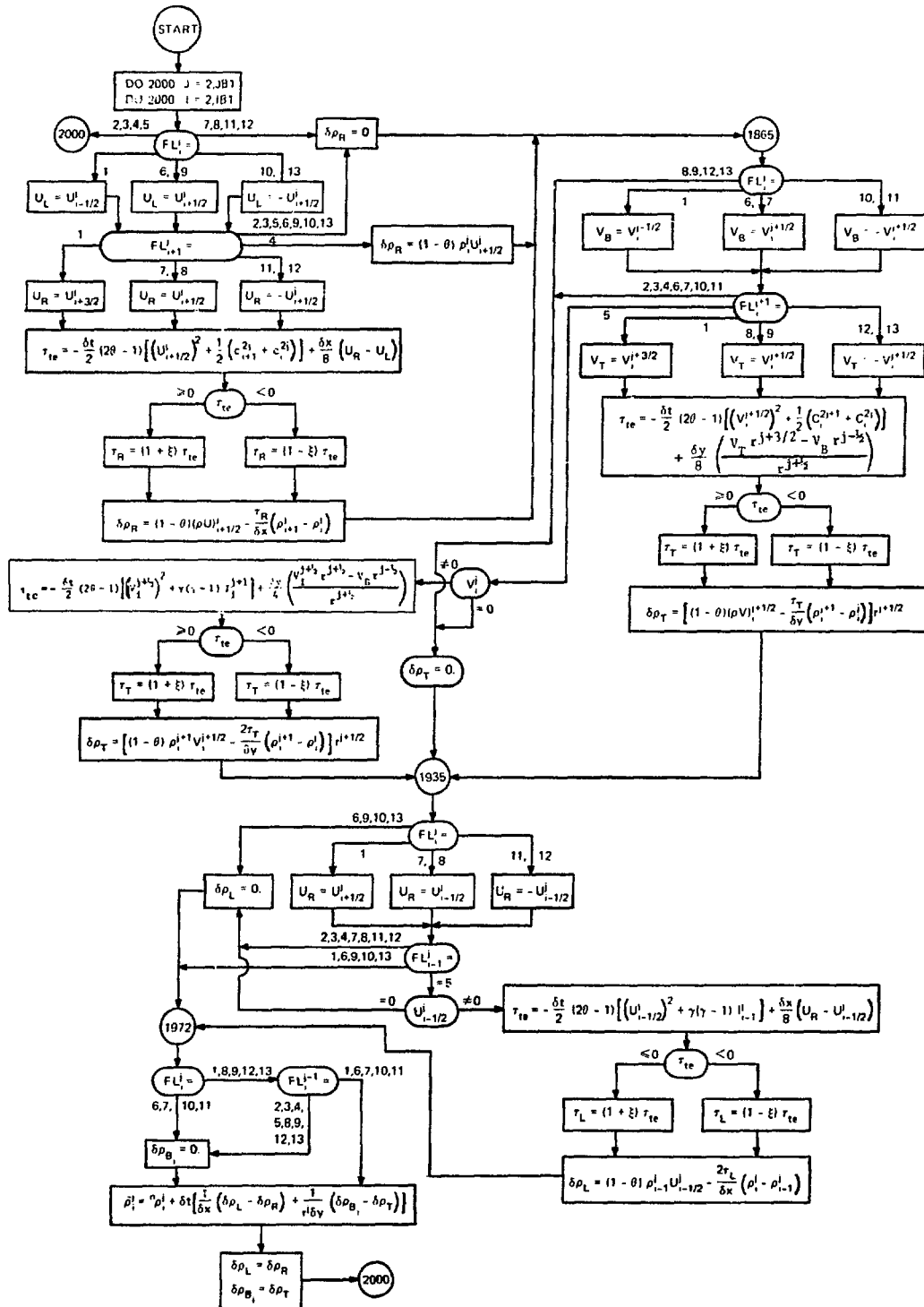




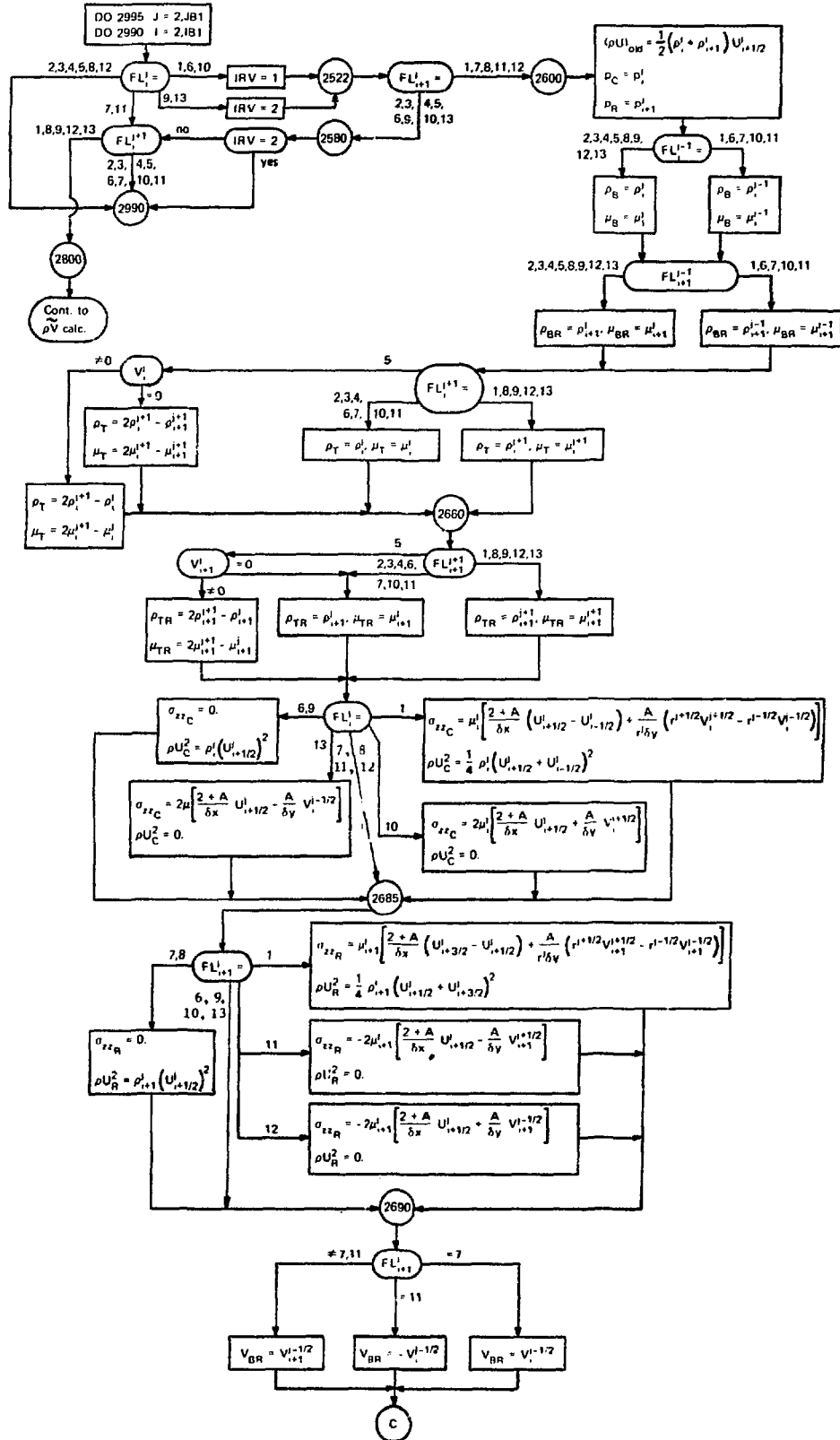
SUBROUTINE TANVEL
 (Setting tangential velocities in fictitious and rectangular obstacle cells)

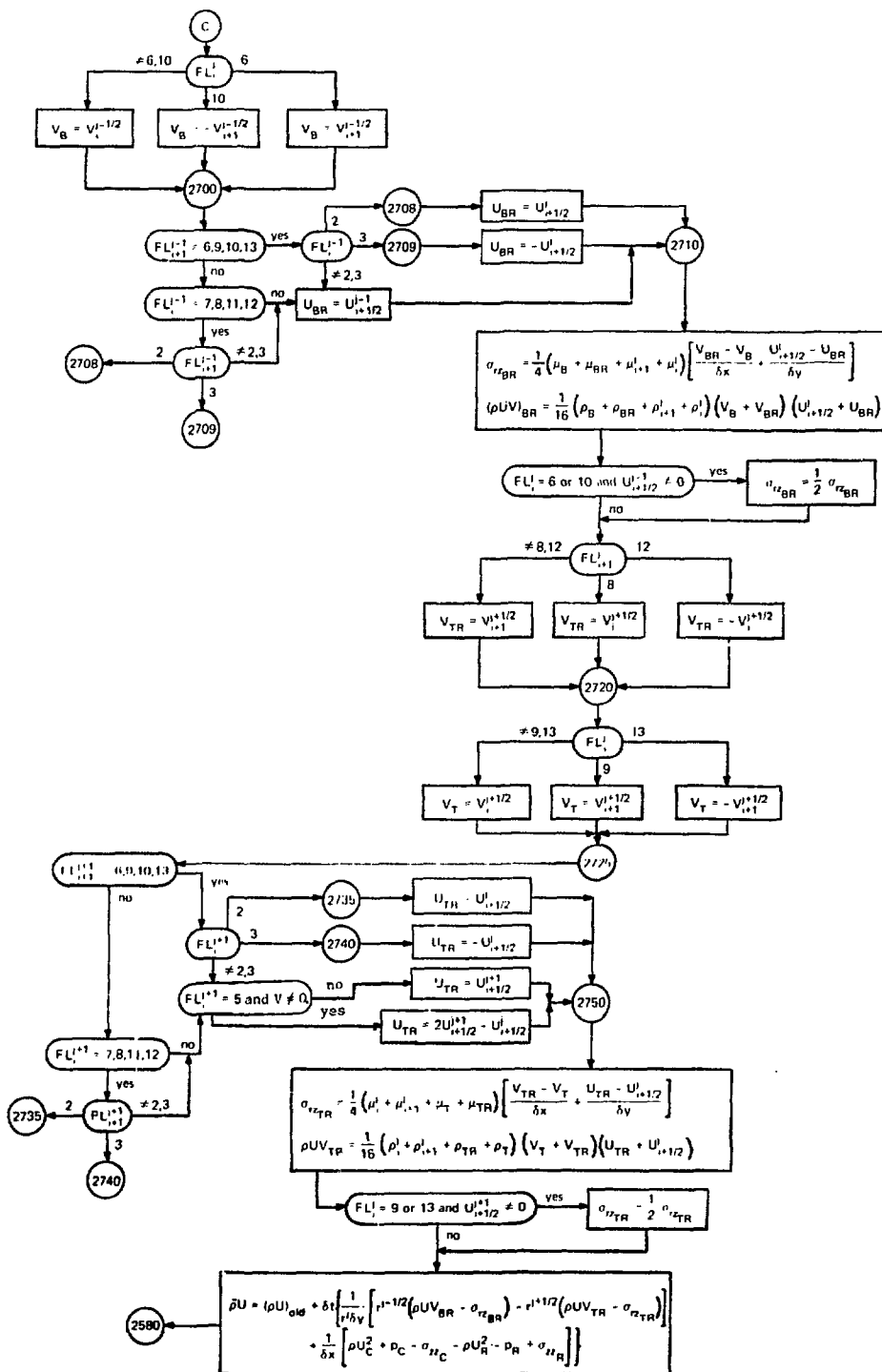


SUBROUTINE TILDE
(ρ Calculation)

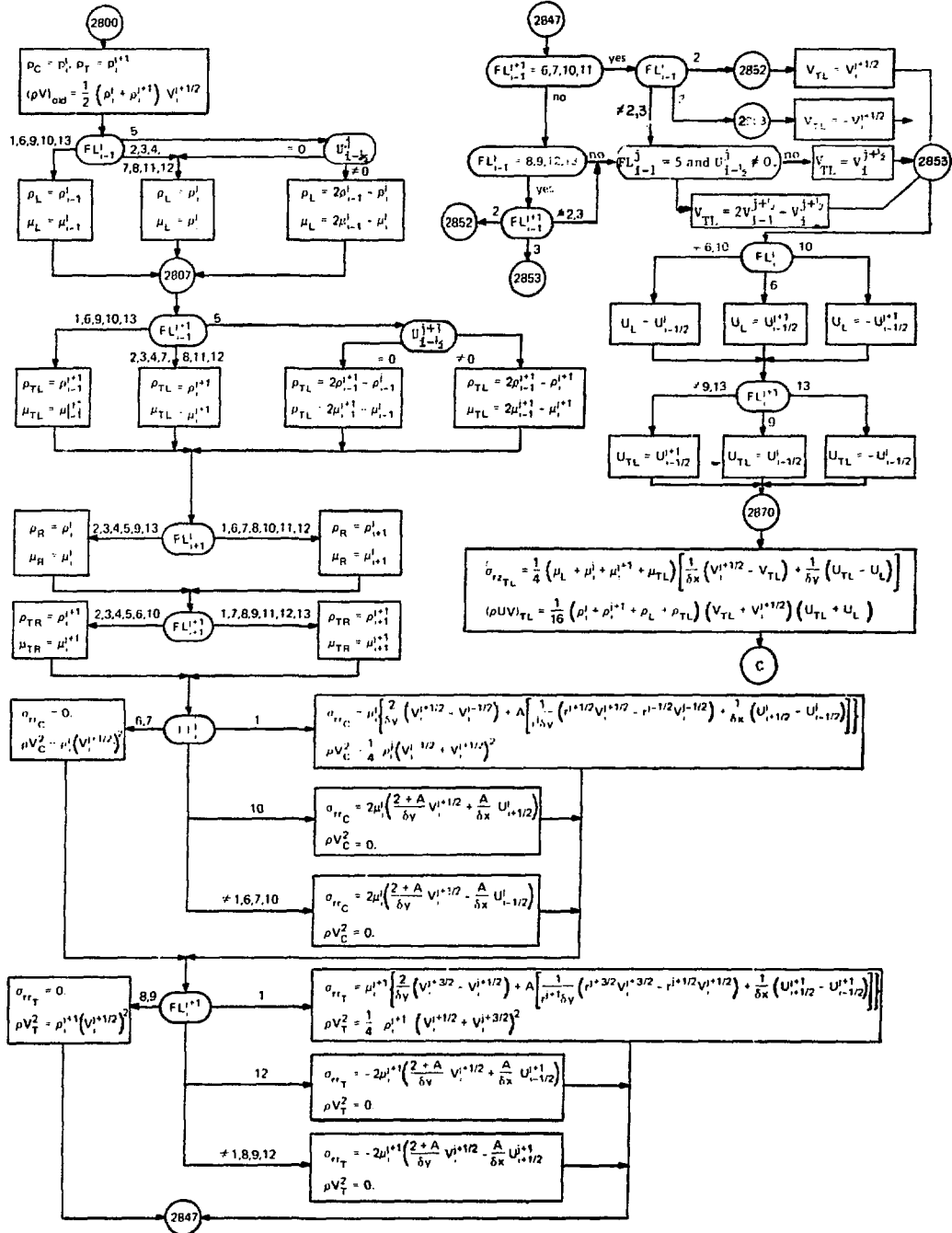


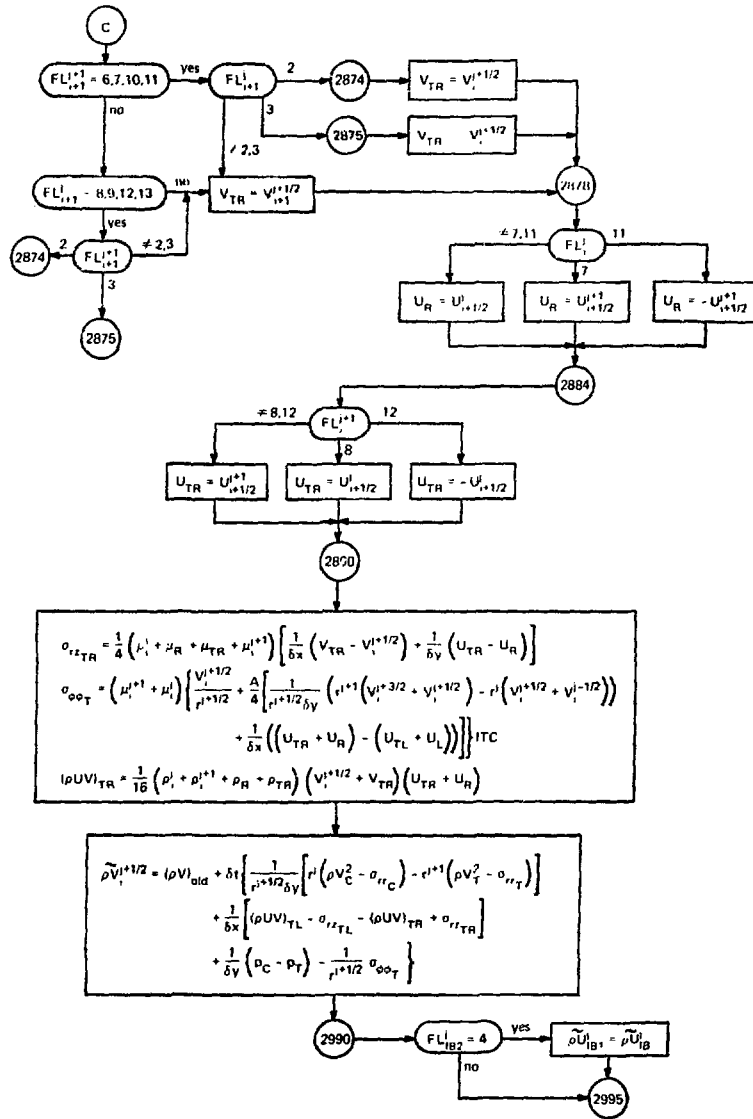
TILDE continue (1)
 (ρU Calculation)



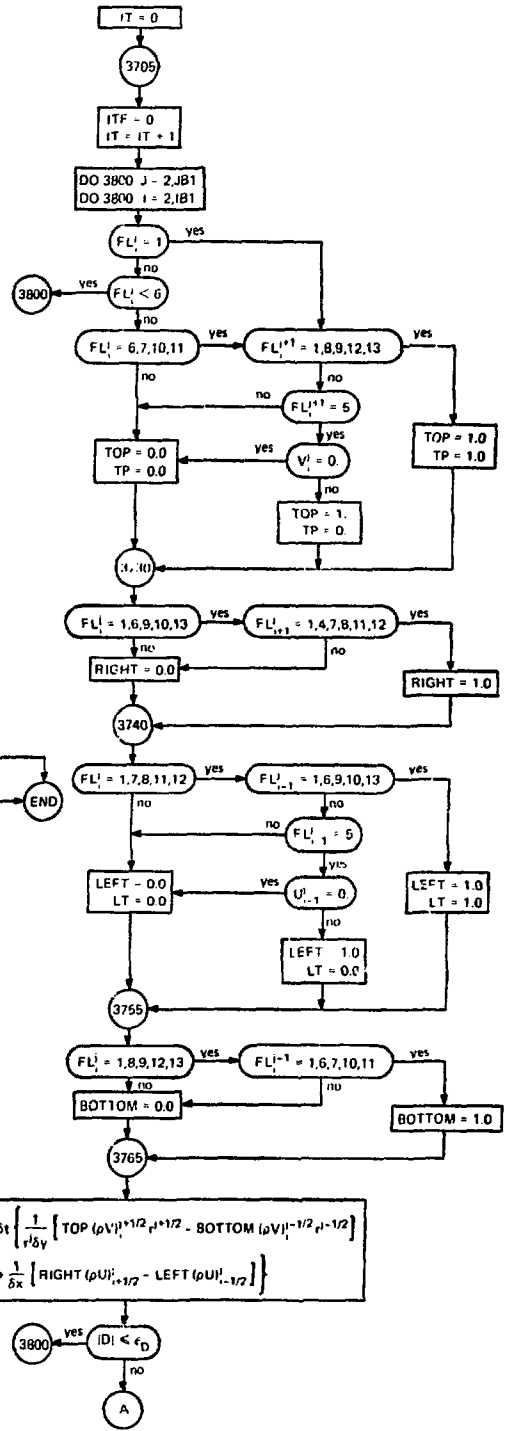
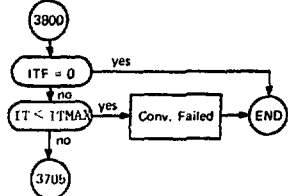
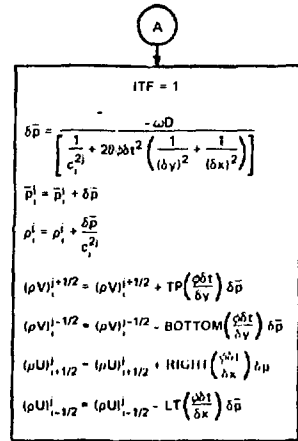


TILDE continue (3)
(ρV Calculation)

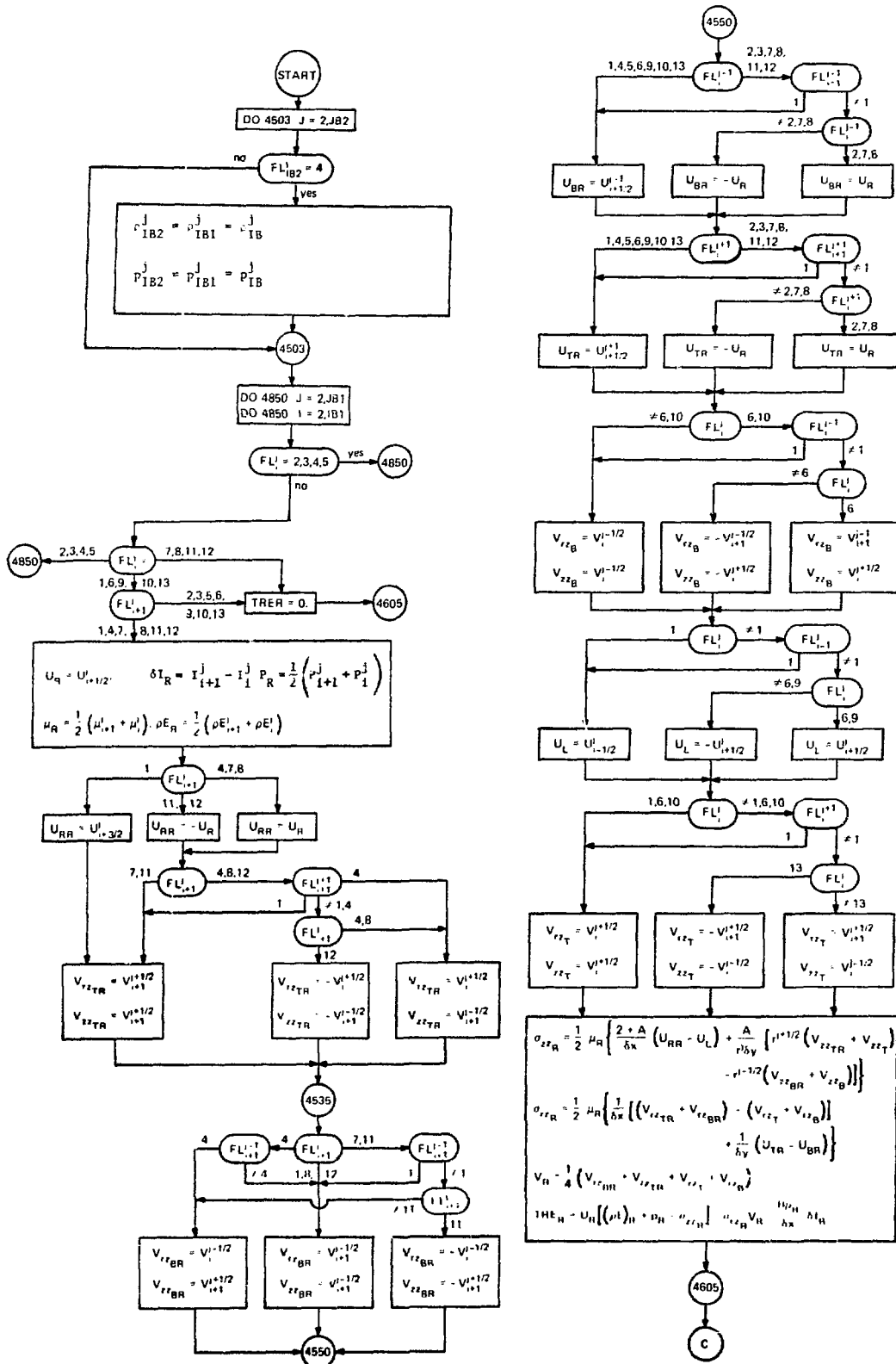


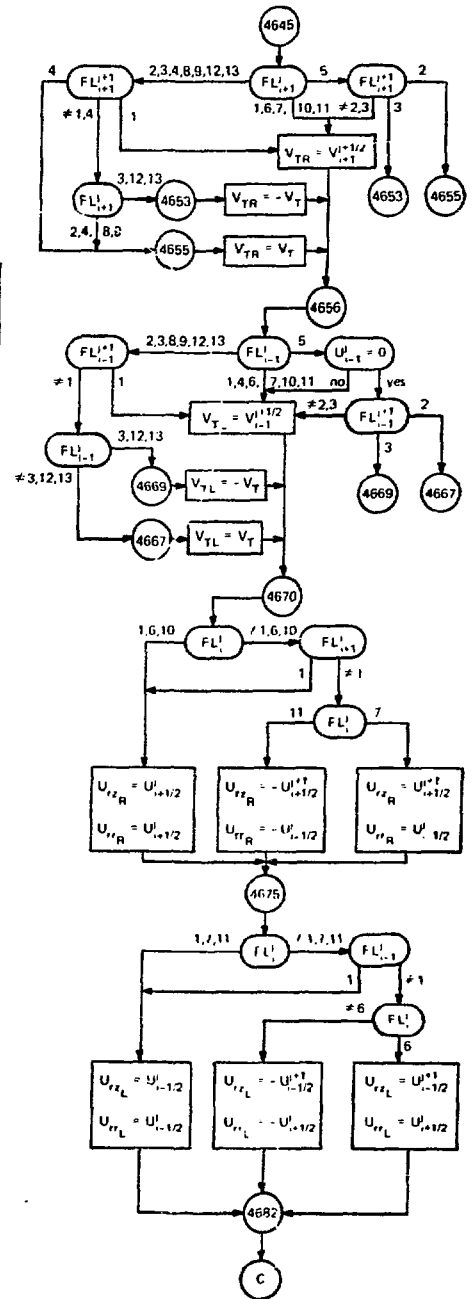
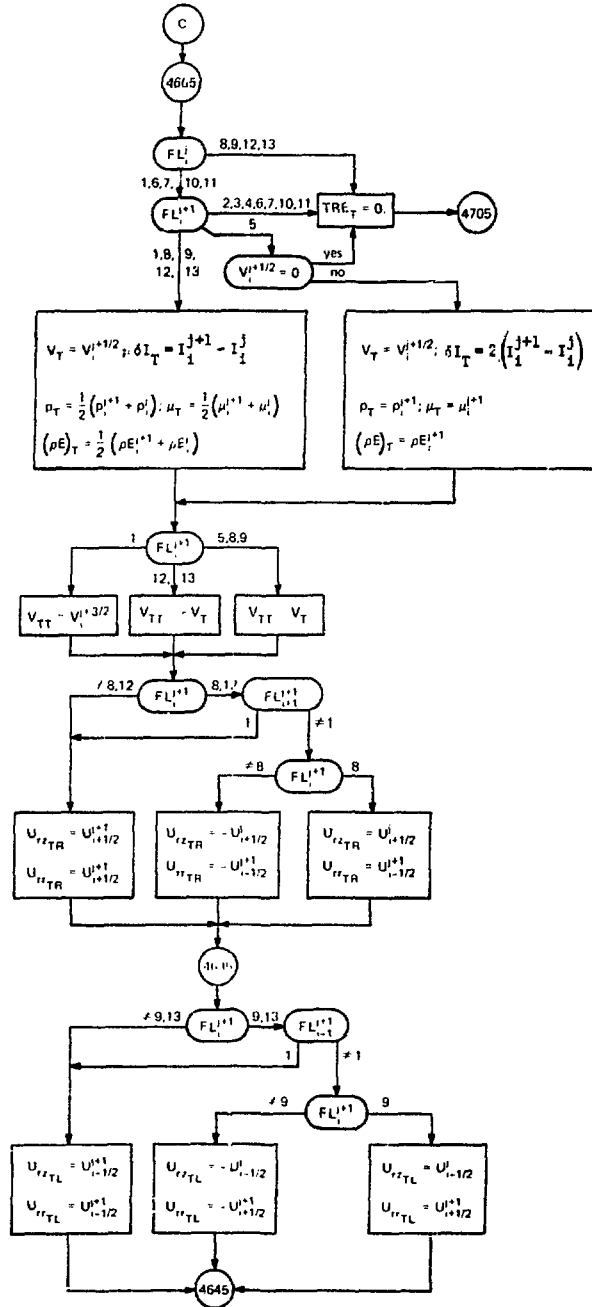


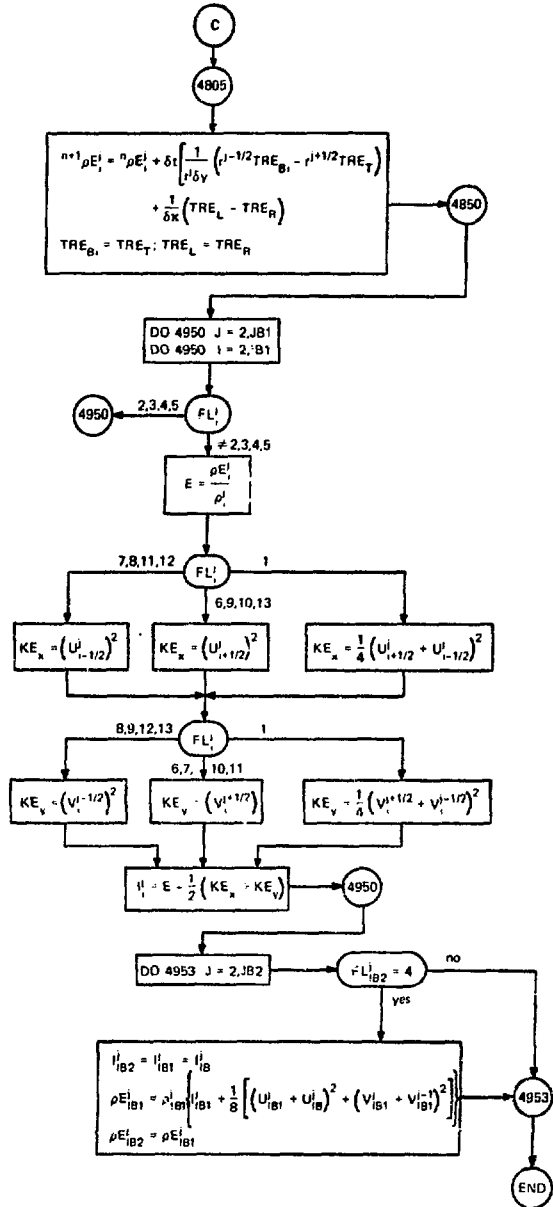
TILDE continue (5)
 (Iteration Section)



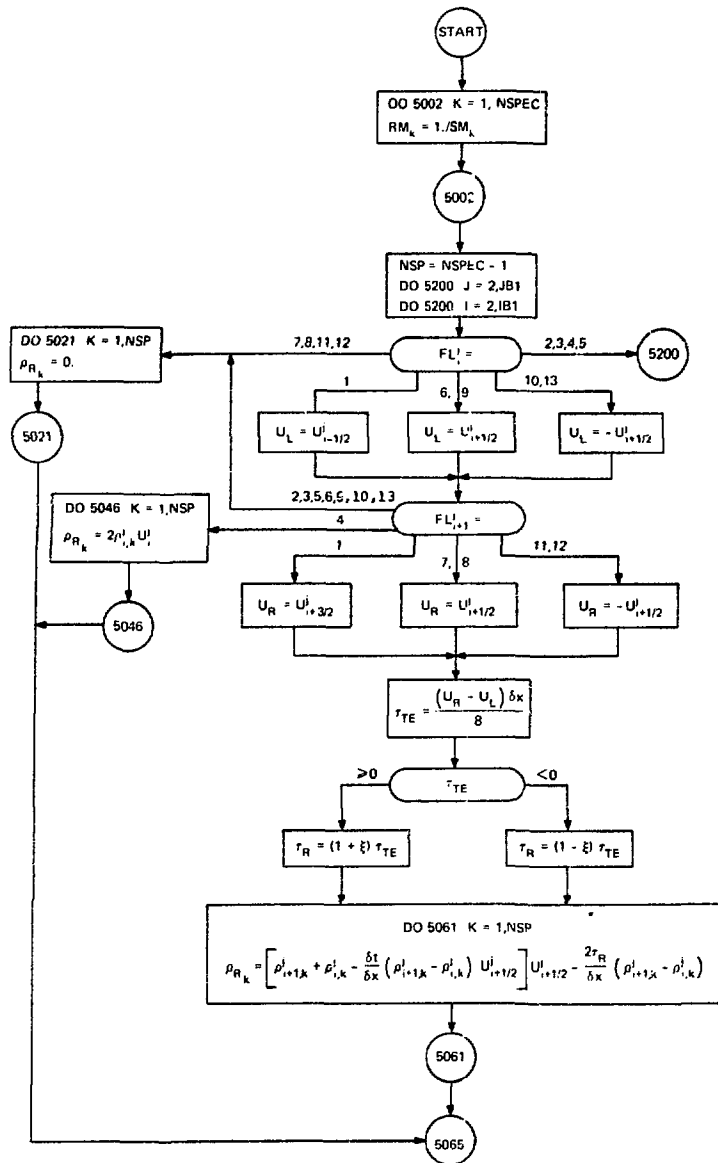
SUBROUTINE ENERGY
(ρE) & I Calculation)

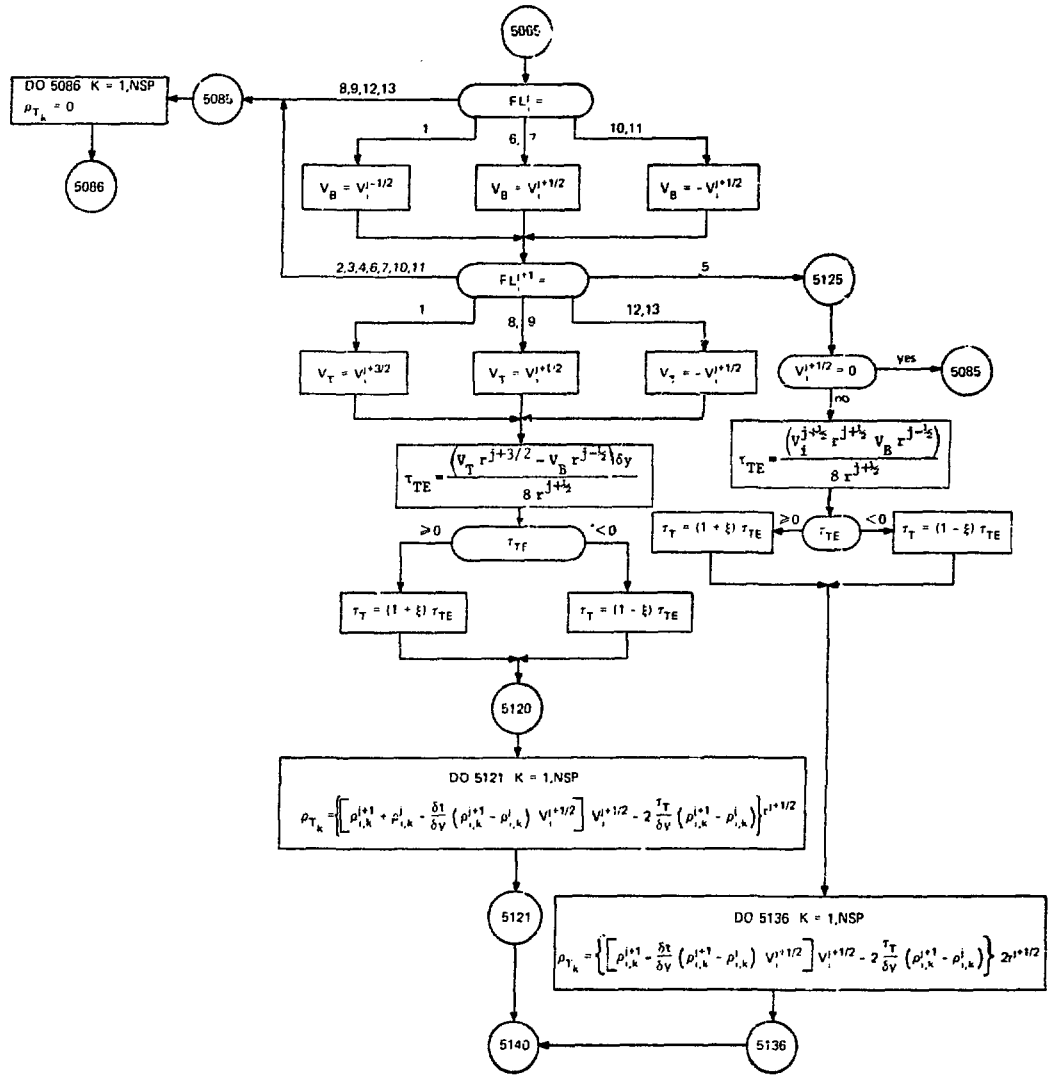


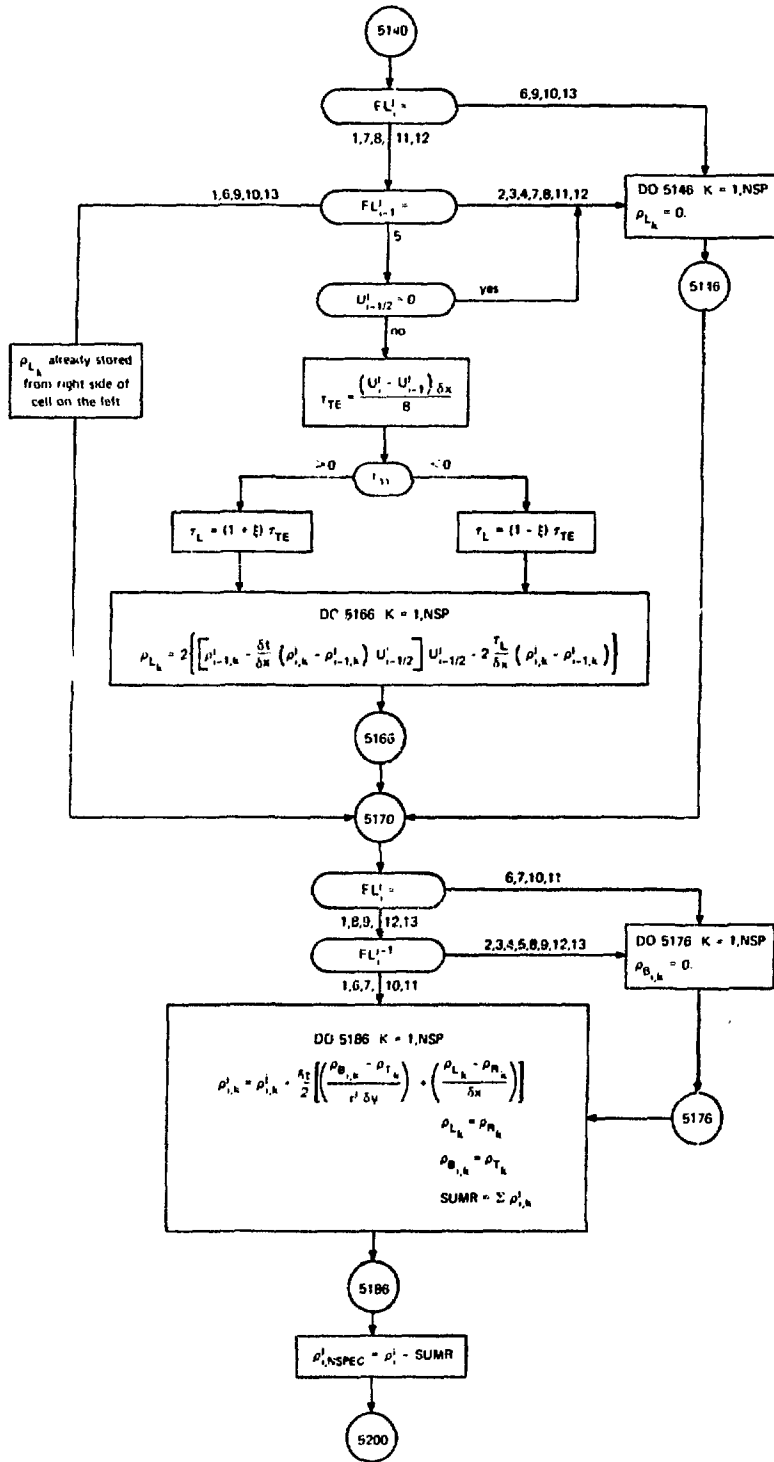




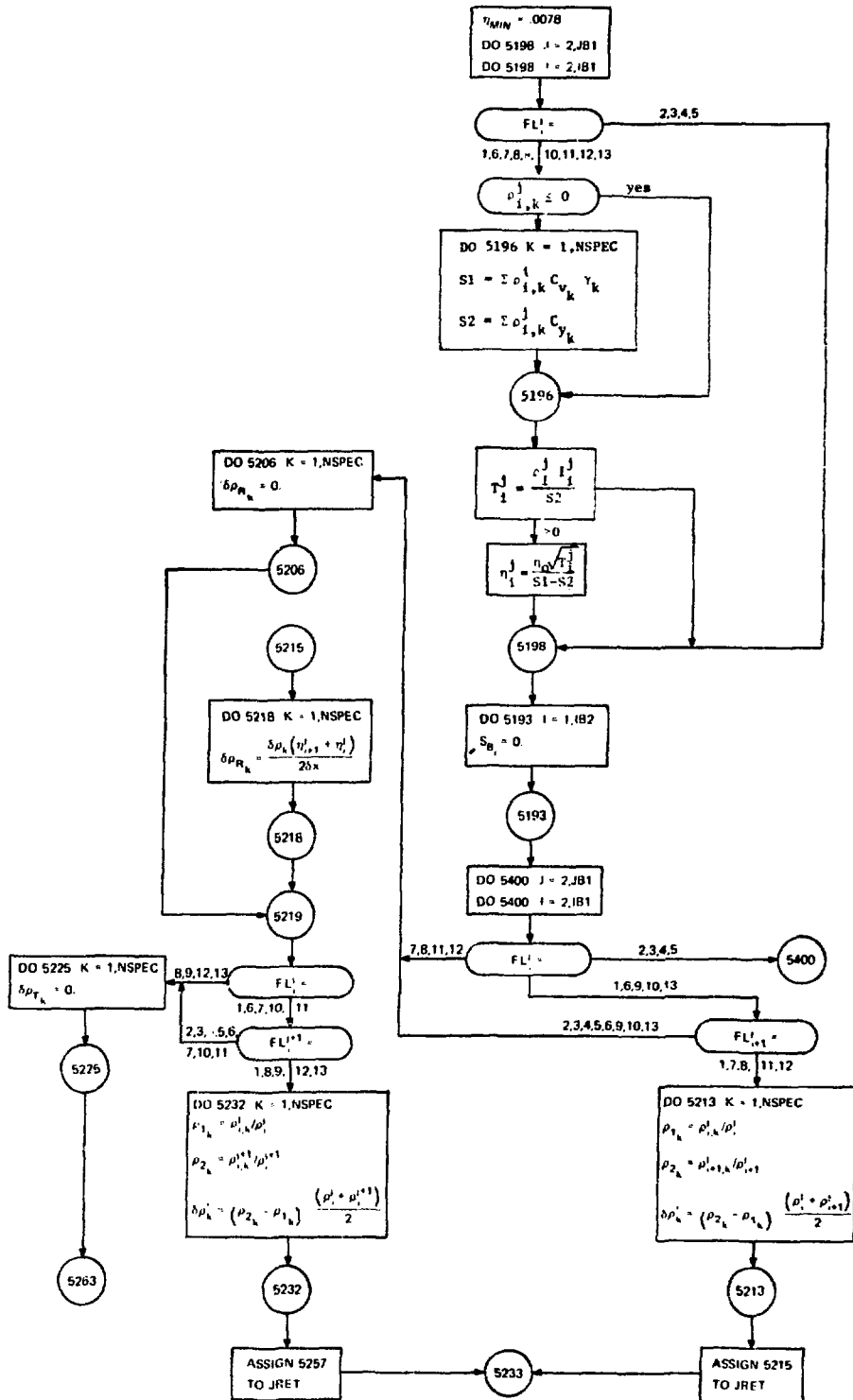
SUBROUTINE SPEC
(Species Convection Calculation)

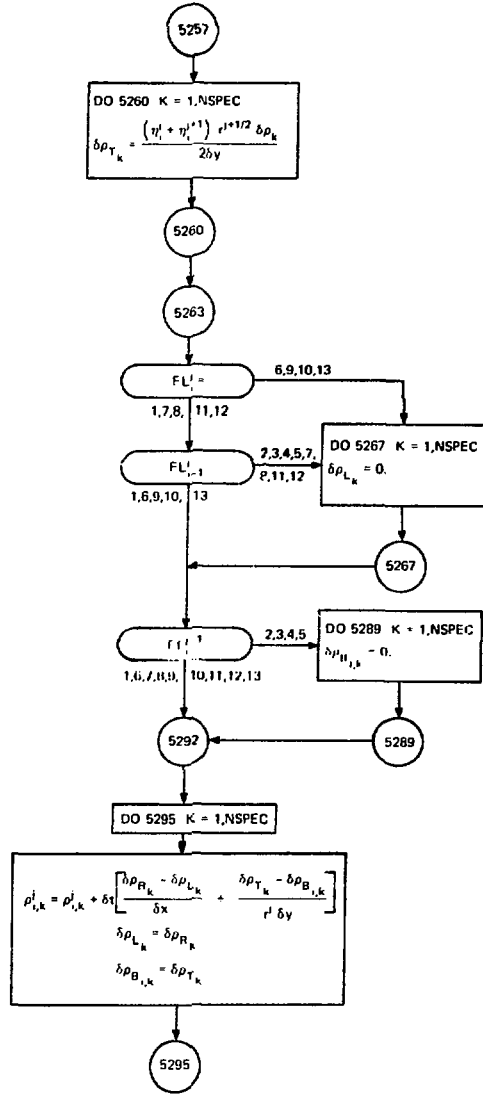
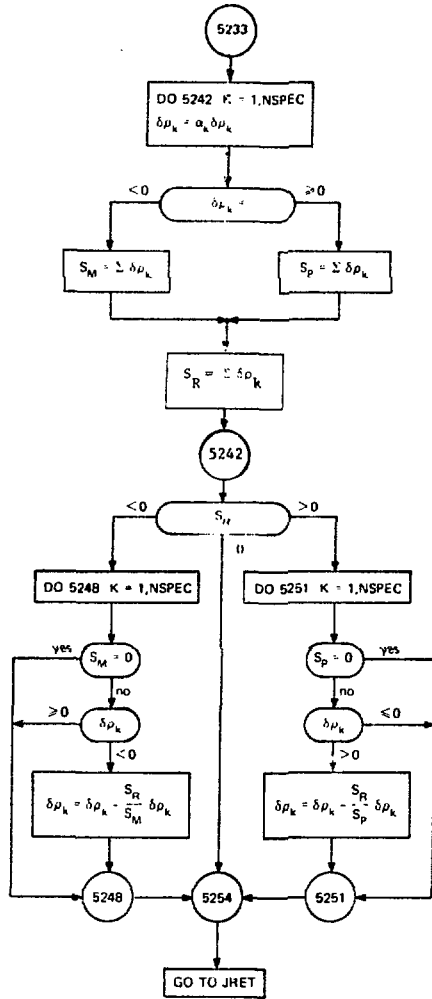




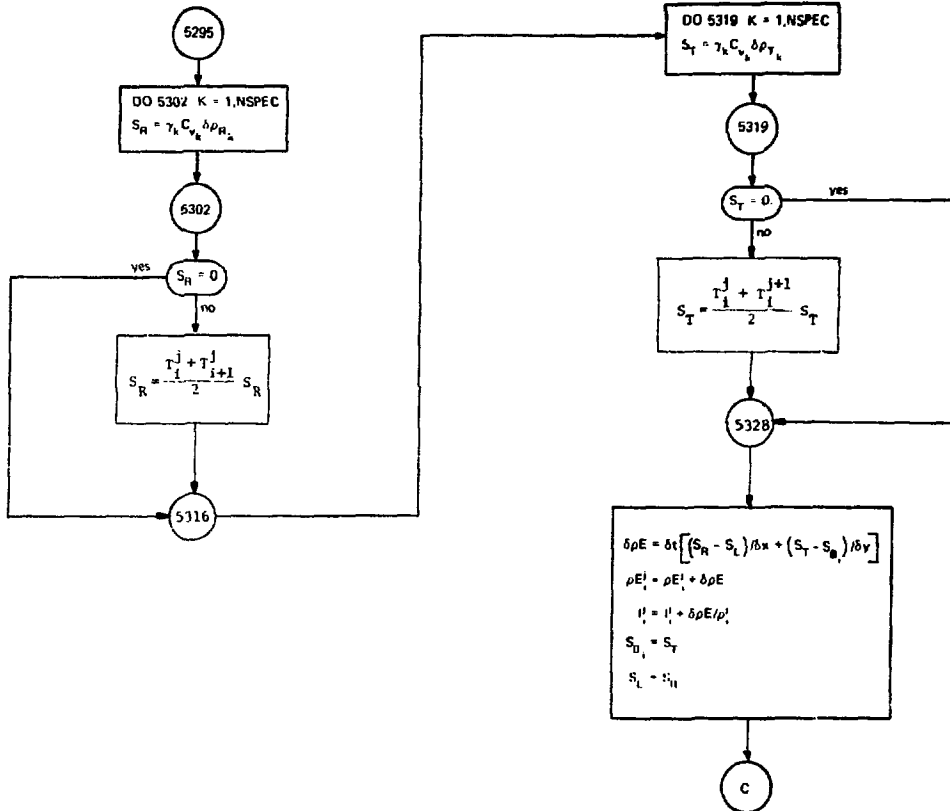


SPEC Continue (3)
 (Species Diffusion Calculation)

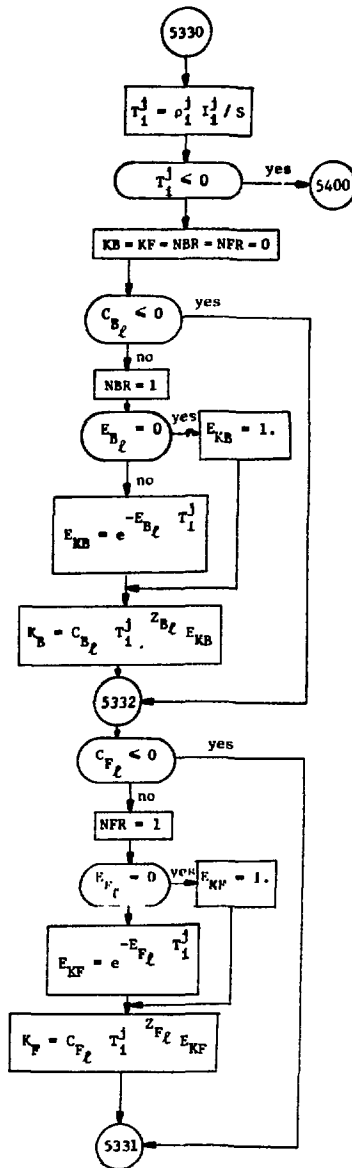
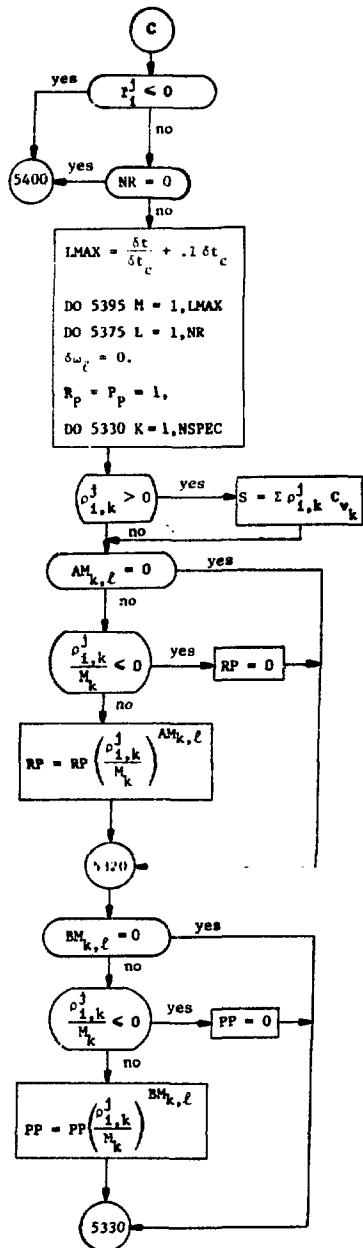


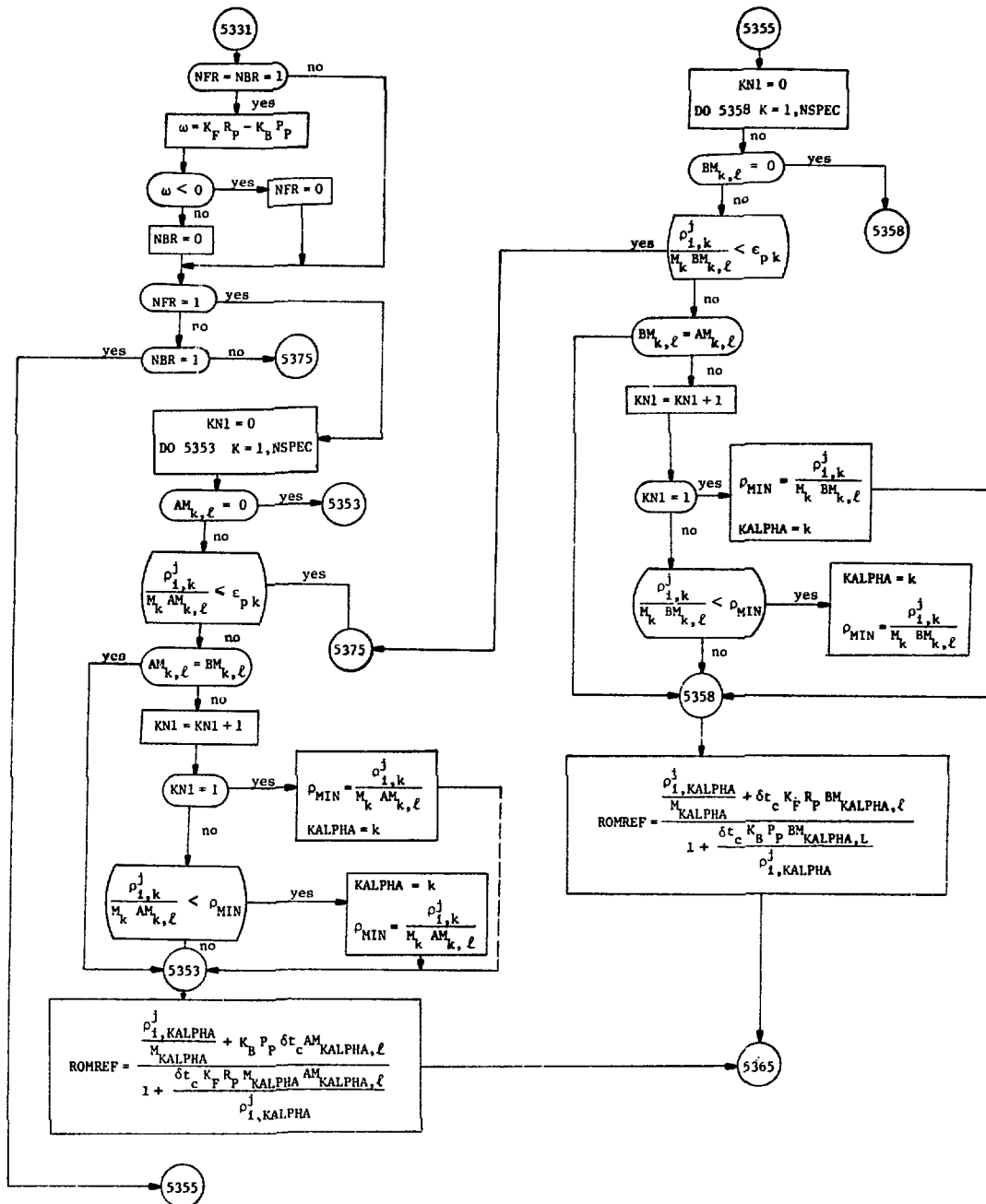


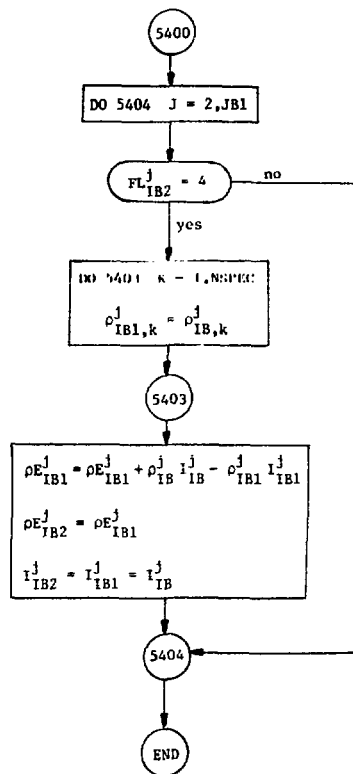
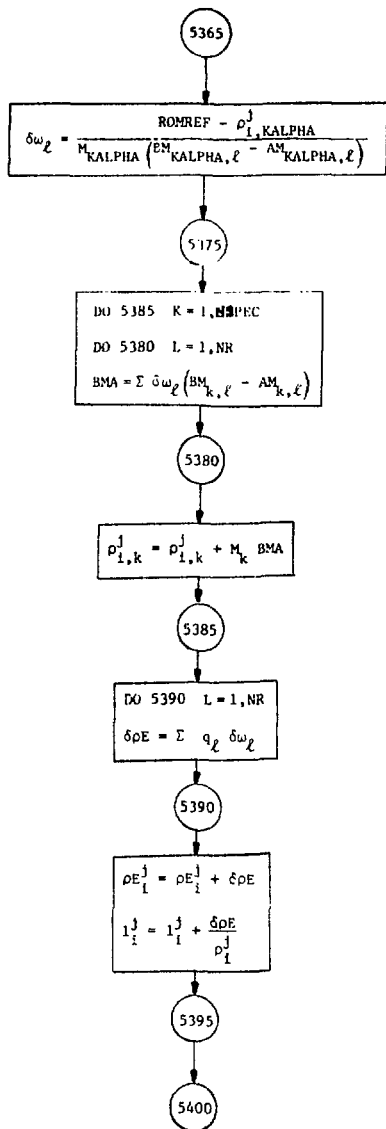
SPEC Continue (5)
(ENTHALPY DIFFUSION)



SPEC Continue (6)
(Chemistry Section)








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PROGRAM RICE(INP,OUT,FILM,FSET12=FILM,FSET5,FSET9=OUT,FSET10=INP) RICE6      3
C**** TAPE-5 DATA FOR STORAGE AND RESTART RCOM1      2
2 COMMON/TAPE5/ITD,NTD,NSOMP,NFILE,NMOMP,NCYOMP RCOM1      3
C**** THE RCOM1 DATA BLOCK IS USED IN RICE(MAIN-PROGRAM),PROG AND RTAPE5 RCOM1      4
C RCOM1      5
C**** THE RCOM2 DATA BLOCK IS COMMON TO RICE AND ALL SUBROUTINES RCOM1      6
C**** BOTH RCOM1 AND RCOM2 ARE LOADED USING *COMDECK FEATURE OF (UPDATE) RCOM1      7
2 COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC, RCOM2      2
1 ISPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC,ALA,BIE,THETA, RCOM2      3
2PHI,OMEGA,GAMMA,DXOU,ASO RCOM2      4
2 COMMON/ICCD/IB,JB,IBI,IBI,NAME(10),JNM,TBEG,SECREQ,DDX,DDY RCOM2      5
1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,X1,IT RCOM2      6
2 COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1, RCOM2      7
IRINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIE1,SIE2, RCOM2      8
2SIEL1,SIEL2 RCOM2      9
2 REAL MUO,MINT1,MINT2,MINL1,MINL2 RCOM2      10
2 COMMON/SPEC/ETA0,FA0(7),FAT1(7),FAT2(7), RCOM2      11
IFAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3), RCOM2      12
2BM(7,3),Q(3),CF(3),ZETAF(3),EF(3),CB(3),ZETAB(3),EB(3) RCOM2      13
2 COMMON/OBSD/IT0(20),NS0(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20) RCOM2      14
1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20), RCOM2      15
2SIEBO(20),FARO(7,20),FABO(7,20) RCOM2      16
2 INTEGER AM,BM RCOM2      17
2 REAL MINRO,MINBO RCOM2      18
C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP) RCOM2      19
C**** AND THE *READ FEATURE OF (UPDATE) RCOM2      20
C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/ RCOM2      21
C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC RCOM2      22
C RCOM2      23
2 LCM/CELLD/FL( 62, 32),U( 62, 32),V( 62, 32 RCOM2      24
1),RHO( 62, 32),SIE( 62, 32),PI( 62, 32 RCOM2      25
2),MU( 62, 32),CSQ( 62, 32),RHOT( 62, 32),RHOU( 62 RCOM2      26
3, 32),RHOV( 62, 32),RE( 62, 32),ETA( 62, 32),CQ( RCOM2      27
4 62, 32),FA( 62, 32, 7),RJ( 32),RJ2( RCOM2      28
5 32),RFLB( 62),TFAB( 62, 7),TE( 62, 32) RCOM2      29
2 DIMENSION RHOUT( 62, 32),RH0VT( 62, 32),PB( RCOM2      30
1 62, 32),DRHOB( 62, 7),STREB( 62) RCOM2      31
2 EQUIVALENCE (RHOU,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB), RCOM2      32
1(TFAB,DRHOB) RCOM2      33
2 INTEGER FL,CYCLE RCOM2      34
2 REAL MU RCOM2      35
1 FORMAT(24I3) RICE8      6
2 FORMAT(2I3,11F6.2) RICE8      7
3 FORMAT(1H036I3) RICE8      8
4 FORMAT(12F6.2) RICE8      9
5 FORMAT(10A8) RICE8      10
6 FORMAT(*0UO=*1PE13.4* VO=*1PE13.4* VINT1=*1PE13.4* VINT2=*1P RICE8      11
1E13.4* UINL1=*1PE13.4* UINL2=*1PE13.4) RICE8      12
7 FORMAT(1HI) RICE8      13
8 FORMAT(1H 2I3,1PB13.4) RICE8      14
9 FORMAT(*1CASE NO. *13* CP TIME=*F8.1) RICE8      15
10 FORMAT(1H 1P12E11.3) RICE8      16
11 FORMAT(8I3,16,15I3) RICE8      17
12 FORMAT(14I2,2X,7F6.2) RICE8      18
13 FORMAT(*0 UINRO RINRO MINRO SIERO*) RICE8      19

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14 FORMAT(*0 VINBO            RINBO            MINBO            SIEBO*)            RICE8            20
15 FORMAT(*0 FA(1)R            FA(2)R            FA(3)R            FA(4)R            FA(5)R            RICE8            21
1    FA(6)R            FA(7)R*)            RICE8            22
16 FORMAT(*0ITD=*13* NTD=*13* NSDMP=*15* NFILE=*13* NNDMP=*15)            RICE8            23
17 FORMAT(*0                    RHOO=*1PE13.4*            RINT1=*1PE13.4*            RINT2 RICE8            24
1=*1PE13.4*            RINL1=*1PE13.4*            RINL2=*1PE13.4)            RICE8            25
19 FORMAT(*0                    MUO=*1PE13.4*            MINT1=*1PE13.4*            MINT2 RICE8            26
1=*1PE13.4*            MINL1=*1PE13.4*            MINL2=*1PE13.4)            RICE8            27
20 FORMAT(*0IB2=*13* JB2=*13* NO=*13* NSL=*413* LPR=*13            RICE8            28
1* CYCLE=*15* ITC=*12* JPLOT=*512* NSPEC=*12* ISPEC=-712* NR=* RICE8            29
212)                    RICE8            30
21 FORMAT(*0INFLOW DATA            --RIGHT--            ----- RICE8            31
1-----TOP-----            --LEFT--*)            RICE8            32
22 FORMAT(*0DX=*1PE10.3* DY=*1PE10.3* T=*1PE10.3* DT=*1PE10.3* TSTOP= RICE8            33
1*1PE10.3* TPR=*1PE10.3* TPL=*1PE10.3* TPLD=*1PE10.3* DTC=*1PE10.3) RICE8            34
23 FORMAT(*0                    -- OBSTACLE DATA ---*/) RICE8            35
24 FORMAT(*0ITO NSO            OB(1)            OB(2)            OB(3)            OB(4)            RICE8            36
1OB(5)            OB(6)            OIB(1)            OIB(2)*)            RICE8            37
25 FORMAT(*0                    SIEO=*1PE13.4*            SIET1=*1PE13.4*            SIET2 RICE8            38
1=*1PE13.4*            SIEL1=*1PE13.4*            SIEL2=*1PE13.4)            RICE8            39
26 FORMAT(*0ALA=*1PE10.3* BIE=*1PE10.3* THETA=*1PE10.3* PHI=* RICE8            40
11PE10.3* OMEGA=*1PE10.3* GAMMA=*1PE10.3* DXOU=*1PE10.3* ASQ=* RICE8            41
21PE10.3 //)            RICE8            42
27 FORMAT(*0                    ETAO=*1PE13.4)            RICE8            43
28 FORMAT(*0 FA(1)B            FA(2)B            FA(3)B            FA(4)B            FA(5)B            RICE8            44
1 FA(6)B            FA(7)B*)            RICE8            45
29 FORMAT(14 *                    FAO=*1PE13.4*            FAT1=*1PE13.4*            FAT2=*1P RICE8            46
1E13.4*            FAL1=*1PE13.4*            FAL2=*1PE13.4)            RICE8            47
30 FORMAT(*0SPEC.NO*)            RICE8            48
32 FORMAT(*0                    -- SPECIES DATA ---*/ ) RICE8            49
33 FORMAT(*0MOLE WT(SM)=*1P10E13.4)            RICE8            50
34 FORMAT(*0EPSILON(EP)=*1P10E13.4)            RICE8            51
35 FORMAT(*0                    (GAMA)=*1P10E13.4)            RICE8            52
36 FORMAT(*0 SP.HEAT(CV)=*1P10E13.4)            RICE8            53
37 FORMAT(*0 DIF.(ALPHA)=*1P10E13.4)            RICE8            54
38 FORMAT(*1                    --SPECIES REACTION DATA--*) RICE8            55
39 FORMAT(*0                    AM(7)            BM(7)            Q            RICE8            56
1            CF            ZETAF            EF            CB            ZETAB            RICE8            57
2            EB*)            RICE8            58
40 FORMAT(713,6X,713,1P7E12.4)            RICE8            59
41 FORMAT(*0                    --SCALING QUANTITIES--*) RICE8            60
42 FORMAT(*0LENGTH (CM)=*1PE11.4*            VELOCITY (CM/SEC)=*1PE11.4*            D RICE8            61
1ENSITY (GM/CC)=*1PE11.4*            MOLECULAR WT.(GM/MOLE)=*1PE11.4)            RICE8            62
43 FORMAT(*0TEMPERATURE (DEG.K)=*1PE11.4*            TIME (SEC)=*1PE11.4*            RICE8            63
1CONCENTRATION (MOLES/CC)=*1PE11.4 //)            RICE8            64
C**** ITD=0--DOES NOT READ OR WRITE TAPE (5)            RICE8            65
C**** ITD=1--DOES NOT READ TAPE (5) BUT WRITES TAPE(5)            RICE8            66
C**** ITD=2--READS TAPE,DOES NOT WRITE TAPE            RICE8            67
C**** ITD=3--READS AND WRITES TAPE (5)            RICE8            68
C**** NTD= NO. ON TAPE -5- TO READ DATA AT-----            RICE8            69
C**** NSDMP= FREQUENCY AT WHICH DATA IS WRITTEN ON TAPE-5- (CYCLE-INTERV RICE8            70
C**** NFILE = NO. ON TAPES OF LAST DUMP TAKEN FROM A PREVIOUS RUN            RICE8            71
C                    RICE8            72
C                    RICE8            73
C                    RICE8            74

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6	SECRETQ=NCREQ*27.5E-9	RICE8	75
C		RICE8	76
	C**** START OF -READ- INPUT DATA	RICE8	77
C		RICE8	78
11	51 READ 5,NAME	RICE8	79
17	READ 4,SLG,VEL,DEN,SMO,TEM	RICE8	80
35	READ 1,ITD,NTD,NSDMP,NFILE,NWDMP	RICE8	81
53	READ 11,IB2,JB2,NO,(NSL(M),M=1,4),LPR,CYCLE,ITC,(JPLOT(M),M=1,5)	RICE8	82
	1,NSPEC,(ISPEC(K),K=1,7),NR	RICE8	83
105	NCYDMP=NSDMP \$ NCASE=0	RICE8	84
C		RICE8	85
	C**** OBTAINS FLUID VARIABLES FROM TAPES IF (ITD.GE.2)	RICE8	86
107	IF (ITD.GE.2)CALL RTAPES	RICE8	87
113	CALL ADV(3)	RICE8	88
115	CALL LINCNT(64)	RICE8	89
C		RICE8	90
	C**** SPACES FILM 3-FRAMES,SETS FILM LINE COUNT AND PUTS JOB ID ON FILM	RICE8	91
117	CALL GETQ(4LKJBN,JN:1)	RICE8	92
121	READ 4,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC	RICE8	93
147	READ 4,ALA,BIE,THETA,PHI,OMEGA,GAMMA,DXOU,ASO	RICE8	94
173	READ4,(FLO(M),M=1,12)	RICE8	95
201	READ 4,UO,VO,VINT1,VINT2,UINL1,UINL2	RICE8	96
221	READ 4,RHO,RINT1,RINT2,RINL1,RINL2	RICE8	97
237	READ 4,MUO,MINT1,MINT2,MINL1,MINL2	RICE8	98
255	READ 4,SIEO,SIET1,SIET2,SIEL1,SIEL2	RICE8	99
273	IF(NSPEC.LT.1)GO TO 46	RICE8	100
C		RICE8	101
	C**** READS SPECIES DATA IF(NSPEC.GE.1),BYPASSES IF(NSPEC.LE.0)	RICE8	102
C		RICE8	103
276	READ 4,ETAO	RICE8	104
303	DO 52 K=1,7	RICE8	105
305	READ 4,FAO(K),FAT1(K),FAT2(K),FAL1(K),FAL2(K)	RICE8	106
327	52 CONTINUE	RICE8	107
331	READ 4,(SM(K),K=1,7)	RICE8	108
337	READ 4,(EP(K),K=1,7)	RICE8	109
345	READ 4,(GAMA(K),K=1,7)	RICE8	110
353	READ 4,(CV(K),K=1,7)	RICE8	111
361	READ 4,(ALPHA(K),K=1,7)	RICE8	112
367	IF(NR.LT.1)GO TO 46	RICE8	113
	C**** READ ONE DATA CARD FOR EACH (NR) REACTION * * * * *	RICE8	114
372	DO 49 L=1,NR	RICE8	115
373	READ 12,(AM(K,L),K=1,7),(BM(K,L),K=1,7),Q(L),CF(L),ZETAF(L),EF(L),	RICE8	116
	ICB(L),ZETAB(L),EB(L)	RICE8	117
433	49 CONTINUE	RICE8	118
436	46 CONTINUE	RICE8	119
436	IF(NO.EQ.0)GO TO 53	RICE8	120
C		RICE8	121
	C**** READS A SET OF FIVE CARDS FOR EACH OBSTACLE * * * * *	RICE8	122
C		RICE8	123
437	DO 55 N=1,NO	RICE8	124
441	READ 2,ITO(N),NSO(N),(OB(M,N),M=1,6),(OIB(M,N),M=1,2)	RICE8	125
462	READ 4,UINRO(N),RINRO(N),MINRO(N),SIERO(N)	RICE8	126
502	READ 4,VINBO(N),RINBO(N),MINBO(N),SIEBO(N)	RICE8	127
522	READ 4,(FARO(K,N),K=1,7)	RICE8	128
532	READ 4,(FARO(K,N),K=1,7)	RICE8	129

542	55 CONTINUE	RICEB	130
	C	RICEB	131
	C**** END OF READ INPUT DATA-----PRINT ALL INPUT DATA READ FROM CARDS	RICEB	132
545	53 KTAPE=9	RICEB	133
	C**** PRINTS ALL INPUT DATA (TAPE-9), THEN COPIES ON FILM (TAPE-12) * * *	RICEB	134
546	54 WRITE(KTAPE,5)NAME	RICEB	135
554	TI=SLG/VEL	RICEB	136
556	CON=DEN/SMO	RICEB	137
560	WRITE(KTAPE,41)	RICEB	138
564	WRITE(KTAPE,42)SLG,VEL,DEN,SMO	RICEB	139
600	WRITE(KTAPE,43)TEM,TI,CON	RICEB	140
612	WRITE(KTAPE,16)ITD,NTD,NSDMP,NFILE,NWDMP	RICEB	141
630	WRITE(KTAPE,20)IB2,JB2,NO,(NSL(K),K=1,4),LPR,CYCLE,ITC	RICEB	142
	1,(JPLOT(K),K=1,5),NSPEC,(ISPEC(K),K=1,7),NR	RICEB	143
662	WRITE(KTAPE,22)DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC	RICEB	144
710	WRITE(KTAPE,26)ALA,BIE,THETA,PHI,OMEGA,GAMMA,DXOU,ASQ	RICEB	145
734	WRITE(KTAPE,21)	RICEB	146
740	WRITE(KTAPE,10)(FLO(K),K=1,12)	RICEB	147
746	WRITE(KTAPE,6)UO,VO,VINT1,VINT2,UINL1,UINL2	RICEB	148
766	WRITE(KTAPE,17)RHOO,RINT1,RINT2,RINL1,RINL2	RICEB	149
1004	WRITE(KTAPE,19)MUO,MINT1,MINT2,MINL1,MINL2	RICEB	150
1022	WRITE(KTAPE,25)SIEO,SIET1,SIET2,SIEL1,SIEL2	RICEB	151
1040	WRITE(KTAPE,32)	RICEB	152
1044	IF(NSPEC.LT.1)GO TO 59	RICEB	153
	C	RICEB	154
	C**** PRINTS SPECIES DATA ONLY WHEN NSPEC IS GREATER THAN ZERO	RICEB	155
1047	WRITE(KTAPE,27)ETAO	RICEB	156
1054	WRITE(KTAPE,30)	RICEB	157
1060	DO 58 K=1,7	RICEB	158
1062	WRITE(KTAPE,29)K,FAO(K),FAT1(K),FAT2(K),FAL1(K),FAL2(K)	RICEB	159
1106	58 CONTINUE	RICEB	160
1110	WRITE(KTAPE,33)(SM(K),K=1,7)	RICEB	161
1116	WRITE(KTAPE,34)(EP(K),K=1,7)	RICEB	162
1124	WRITE(KTAPE,35)(GAMA(K),K=1,7)	RICEB	163
1132	WRITE(KTAPE,36)(CV(K),K=1,7)	RICEB	164
1140	WRITE(KTAPE,37)(ALPHA(K),K=1,7)	RICEB	165
1146	IF(NR.LT.1)GO TO 59	RICEB	166
1151	WRITE(KTAPE,38)	RICEB	167
1154	WRITE(KTAPE,39)	RICEB	168
1160	DO 56 L=1,NR	RICEB	169
1162	WRITE(KTAPE,40)(AM(K,L),K=1,7),(BM(K,L),K=1,7),Q(L),CF(L),ZETAF(L)	RICEB	170
	1,EF(L),CB(L),ZETAB(L),EB(L)	RICEB	171
1222	56 CONTINUE	RICEB	172
1225	59 CONTINUE	RICEB	173
	C	RICEB	174
	C**** PRINTS OBSTACLE DATA ONLY IF COMPUTING REGION CONTAINS OBSTACLES	RICEB	175
1225	IF(KTAPE.EQ.9)NSDMP=NSDMP+CYCLE	RICEB	176
1231	WRITE(KTAPE,23)	RICEB	177
1235	IF(NO.EQ.0) GO TO 60	RICEB	178
1236	DO 57 N=1,NO	RICEB	179
1240	WRITE(KTAPE,24)	RICEB	180
1243	WRITE(KTAPE,8)ITO(N),NSO(N),(OB(M,N),M=1,6),(OIB(M,N),M=1,2)	RICEB	181
1265	WRITE(KTAPE,13)	RICEB	182
1271	WRITE(KTAPE,10)UINRO(N),RINRO(N),MINRO(N),SIERO(N)	RICEB	183
1311	WRITE(KTAPE,14)	RICEB	184

1315	WRITE(KTAPE,10)VINBO(N),RINBO(N),MINBO(N),SIEBO(N)	RICE8	185
1335	WRITE(KTAPE,15)	RICE8	186
1341	WRITE(KTAPE,10)(FARO(K,N),K=1,7)	RICE8	187
1351	WRITE(KTAPE,28)	RICE8	188
1355	WRITE(KTAPE,10)(FABO(K,N),K=1,7)	RICE8	189
1365	57 CONTINUE	RICE8	190
1370	60 CONTINUE	RICE8	191
1370	IF(KTAPE.NE.9)GO TO 62	RICE8	192
1372	CALL ADV(1)	RICE8	193
1374	KTAPE=12 \$ GO TO 54	RICE8	194
1376	62 CONTINUE	RICE8	195
1376	IB=IB2-2	RICE8	196
1400	IB1=IB2-1	RICE8	197
1401	JB=JB2-2	RICE8	198
1403	JB1=JB2-1	RICE8	199
	C**** CONVERTS ALL GRID DATA TO 4020 NUMBERS IN ALL PLOT ROUTINES . . .	RICE8	200
1404	CALL VPLOT(0)	RICE8	201
1405	CALL CNPLOT(0)	RICE8	202
1407	CALL COPLOT(0)	RICE8	203
	C**** TRANSFERS TO CONTROL PROGRAM FOR TIME DEPENDENT CALC.	RICE8	204
1411	CALL PROG	RICE8	205
1412	CALL SECOND(TEND)	RICE8	206
1414	NCASE=NCASE+1 \$ TCASE=TEND-TBEG	RICE8	207
1420	WRITE(9,9)NCASE,TCASE	RICE8	208
1427	GO TO 51 \$ END	RICE8	209
	C	RICE8	210
	C	RICE8	211
	C**** END OF THE MAIN PROGRAM	RICE8	212
	C	RICE8	213
	C	RICE8	214

	SUBROUTINE PROG	RICE8	215
	C**** TAPE-5 DATA FOR STORAGE AND RESTART	RCOM1	2
1	COMMON/TAPED/ITD,NTD,NSDMP,NFILE,NWOMP,NCYDMP	RCOM1	3
	C**** THE RCOM1 DATA BLOCK IS USED IN RICE(MAIN-PROGRAM),PROG AND RTAPE5	RCOM1	4
	C	RCOM1	5
	C**** THE RCOM2 DATA BLOCK IS COMMON TO RICE AND ALL SUBROUTINES	RCOM1	6
	C**** BOTH RCOM1 AND RCOM2 ARE LOADED USING *COMDECK FEATURE OF (UPDATE)	RCOM1	7
1	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASQ	RCOM2	4
1	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SCCREQ,DDX,DDY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,X1,IT	RCOM2	6
1	COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RH00,RINT1,	RCOM2	7
	IRINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIEO,SJET1,SJET2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
1	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
1	COMMON/SPECD/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	IFAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
1	COMMON/OBSD/ITO(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FABO(7,20)	RCOM2	16
1	INTEGER AM,BM	RCOM2	17
1	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
1	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHOT(62, 32),RHOV(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CQ(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
1	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
1	EQUIVALENCE (RHOV,RHOVT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
1	INTEGER FL,CYCLE	RCOM2	34
1	REAL MU	RCOM2	35
	1 FORMAT(24I3)	RICE8	218
	3 FORMAT(1H036I3)	RICE8	219
	4 FORMAT(1H 1P10E13.5)	RICE8	220
	5 FORMAT(1H0,1P6E15.4)	RICE8	221
	7 FORMAT(2I5,7(2X,1PE12.5))	RICE8	222
	8 FORMAT(*0TAPE 5 DUMP NO.=*15* CYCLE=*15* TIME=*F10.4)	RICE8	223
	9 FORMAT(*1CYCLE=*15* TIME=*F8.3,10A8)	RICE8	224
	30 FORMAT(* 1 J FL U V RHO PB	RICE8	225
	1 SIE TEMP. MU*)	RICE8	226
	31 FORMAT(1H 313,1P10E12.4)	RICE8	227
	32 FORMAT(* SPECIES DENSITIES*)	RICE8	228
	33 FORMAT(* 1 J FL A B C D	RICE8	229
	1 E F G*)	RICE8	230
	41 FORMAT(* ITER=*14* TIME=*F7.2* CYCLE=*14* CP=*1PE10.2	RICE8	231

	1*	GRINDS=*IPE(2.5)	RICE8	232
1		TPRI=TPR+TIME	RICE8	233
3		TPLO=TPL+TIME	RICE8	234
4		TPLOD=TPLD+TIME	RICE8	235
6		TRDISK=2100.	RICE8	236
10		CALL FLIC	RICE8	237
	C****	FLIC---SETS ALL CELL FLAGS	RICE8	238
	C		RICE8	239
	C****	CVIC---SETS UP INITIAL CONDITIONS FOR FLUID VARIABLES FROM INPUT	RICE8	240
	C****	DATA	RICE8	241
11		CALL CVIC	RICE8	242
12		CALL SECOND(TCP)	RICE8	243
	C*****	START OF TIME STEP-----END OF I.C.SETUP *****	RICE8	244
	C		RICE8	245
	C		RICE8	246
	C		RICE8	247
14	1000	CONTINUE	RICE8	248
14		JC=0	RICE8	249
15		DO 1025 J=2,JBI	RICE8	250
17		JC=JC+1B2	RICE8	251
20		DO 1025 I=2,1B1	RICE8	252
22		IJ=I+JC	RICE8	253
23		IMJ=IJ-1	RICE8	254
24		IJM=IJ-1B2	RICE8	255
26		IF(FL(IJ).GT.1.AND.FL(IJ).LT.6)GO TO 1025	RICE8	256
40		IF(NSPEC.LE.0)GO TO 1004	RICE8	257
41		SUM=0.	RICE8	258
42		SUM1=0.	RICE8	259
43		DO 1003 K=1,NSPEC	RICE8	260
44		KZ=1B2*JB2*(K-1)	RICE8	261
47		IJK=IJ+KZ	RICE8	262
51		IF(FA(IJK).LE.0.)GO TO 1003	RICE8	263
55		SUM=SUM+FA(IJK)*CV(K)	RICE8	264
61		SUM1=SUM1+FA(IJK)*CV(K)*GAMA(K)	RICE8	265
63	1003	CONTINUE	RICE8	266
66		IF(SUM.NE.0.)GAMMA=SUM1/SUM	RICE8	267
70		IF(SUM.LE.0.)TE(IJ)=0.	RICE8	268
75		IF(SUM.GT.0.)TE(IJ)=RHO(IJ)*SIE(IJ)/SUM	RICE8	269
105	1004	CONTINUE	RICE8	270
106		CSQ(IJ)=GAMMA*(GAMMA-1.)*SIE(IJ)+ASQ	RICE8	271
	C****	CALC.C**2,P AND MU AT END OF TIME STEP ALL DATA TIME UPDATED * * *	RICE8	272
	C		RICE8	273
113		MU(IJ)=MUO*RHO(IJ)*RRHO	RICE8	274
120		IF(ASQ.GT.0.)GO TO 1025	RICE8	275
122		P(IJ)=(GAMMA-1.)*RHO(IJ)*SIE(IJ)	RICE8	276
		1+ASQ*(RHO(IJ)-RHOO)	RICE8	277
135		IF(P(IJ).LT.0.)P(IJ)=0.	RICE8	278
141	1025	CONTINUE	RICE8	279
146		DO 1030 J=2,JBI	RICE8	280
150		IF(FL(1B2,J).NE.4)GO TO 1030	RICE8	281
155		CSQ(1B2,J)=CSQ(1B1,J)+CSQ(1B,J)	RICE8	282
167		MU(1B2,J)=MU(1B1,J)+MU(1B,J)	RICE8	283
200		P(1B2,J)=P(1B1,J)+P(1B,J)	RICE8	284
212		TE(1B2,J)=TE(1B1,J)+TE(1B,J)	RICE8	285
223	1030	CONTINUE	RICE8	286

	C*****SETS TANGENTIAL VEL. IN FICTIOUS AND RECTANGULAR OBSTACLE CELLS	RICE8	287
226	CALL TANVEL	RICE8	288
	C	RICE8	289
	C	RICE8	290
	C*****PRINT SECTION (2000) *****	RICE8	291
	C*****LPR=-2 OMTS GRAPH IDENTIFICATION,OMITS PRINTED DATA ON FILM	RICE8	292
	C*****LPR=-2 OMTS VPLOT AND CNPLOT (USE FOR MOVIE OR COLOR PLOT)	RICE8	293
	C*****LPR=-1 OMTS GRAPH IDENTIFICATION,OMITS PRINTED DATA ON FILM	RICE8	294
	C*****LPR=-1 OMTS VPLOT	RICE8	295
	C*****LPR= 0 OMTS GRAPH IDENTIFICATION,OMITS PRINTED DATA ON FILM	RICE8	296
	C*****LPR= 0 OMTS CNPLOT AND COPLOT	RICE8	297
	C*****LPR= 1 ALLOWS ALL PLOTTING AND PRINTING ON FILM,AND PRINTING ON P	RICE8	298
	C*****LPR= 2 ALLOWS ALL PLOTTING AND PRINTING ON FILM,AND PRINTING ON P	RICE8	299
	C*****LPR= 2 OMTS COPLOT	RICE8	300
	C*****LPR= 4 BYPASSES ALL PLOTTING,PRINTS NUM.DATA AT SPECIFIED TIMES	RICE8	301
	C*****LPR= 5 BYPASSES ALL PRINTING,PLOTS DATA AND GRAPHS	RICE8	302
227	IF (LPR.EQ.-2)GO TO 2360	RICE8	303
231	IF (LPR.LT.0)GO TO 2167	RICE8	304
232	IF (LPR.EQ.4)GO TO 2170	RICE8	305
234	IF (CYCLE.LE.1)GO TO 2068	RICE8	306
236	IF (TIME*.000001.LT.TPLO)GO TO 2170	RICE8	307
242	2068 CONTINUE	RICE8	308
	C**** VECTOR PLOT SECTION	RICE8	309
	C**** IF PLOTTING SPECIFIED BY LPR,THEN PLOT ARE MADE WHEN TPLO.LE.TIME	RICE8	310
	C	RICE8	311
242	CALL ADV(1)	RICE8	312
244	CALL VPLOT(1)	RICE8	313
246	DO 2165 J=2,J81	RICE8	314
250	DO 2165 I=2,I8	RICE8	315
251	XX1=(I-1.5)*DX	RICE8	316
254	YY1=(J-1.5)*DY	RICE8	317
256	IF (FL(I,J).EQ.1) GO TO 2163	RICE8	318
264	IF (FL(I,J).EQ.5) GO TO 2165	RICE8	319
270	IF (FL(I,J).GT.1.AND.FL(I,J).LT.5) GO TO 2165	RICE8	320
301	NFL=FL(I,J)-5 \$ GO TO (2153,2155,2157,2159,2162,2162,2162,2162)NFL	RICE8	321
321	2153 XX2=XX1+ U(I ,J)*DXOU \$ YY2=YY1+ V(I ,J)*DXOU \$ GO TO 2164	RICE8	322
335	2155 XX2=XX1+ U(I-1,J)*DXOU \$ YY2=YY1+ V(I ,J)*DXOU \$ GO TO 2164	RICE8	323
351	2157 XX2=XX1+ U(I-1,J)*DXOU \$ YY2=YY1+ V(I,J-1)*DXOU \$ GO TO 2164	RICE8	324
365	2159 XX2=XX1+ U(I ,J)*DXOU \$ YY2=YY1+ V(I,J-1)*DXOU \$ GO TO 2164	RICE8	325
404	2163 XX2=XX1+.5*(U(I-1,J)+U(I,J))*DXOU	RICE8	326
412	YY2=YY1+.5*(V(I,J-1)+V(I,J))*DXOU	RICE8	327
420	GO TO 2164	RICE8	328
421	2162 XX2=XX1 \$ YY2=YY1	RICE8	329
424	2164 CALL VPLOT(2,XX1,YY1,XX2,YY2)	RICE8	330
430	2165 CONTINUE	RICE8	331
	C***** END OF VECTOR PLOT SECTION-----START OF CONTOUR PLOT SECTION* *	RICE8	332
	C	RICE8	333
	C**** PLOTS---RHO,P,SIE,T,M---FOR ALL REAL FLUID CELLS AS SPECIFIED BY	RICE8	334
	C**** JPLOT(L),EACH ARRAY STORED IN DUMMY ARRAY--CQ--TO TRANSFER TO PLOT	RICE8	335
	C**** ROUTINES	RICE8	336
	C	RICE8	337
435	2167 CONTINUE	RICE8	338
435	IF (LPR.EQ.0)GO TO 2170	RICE8	339
436	IF (CYCLE.LE.1)GO TO 2169	RICE8	340
441	IF (TIME*.000001.LT.TPLO)GO TO 2170	RICE8	341

444	TPLO=TPLO+TPL	RICE8	342
446	2169 CONTINUE	RICE8	343
446	DO 2325 L=1,5	RICE8	344
450	IF(JPLOT(L).NE.1) GO TO 2325	RICE8	345
452	DO 2320 J=1,J82	RICE8	346
454	DO 2320 I=1,I82	RICE8	347
455	IF(FL(I,J).GT.1.AND.FL(I,J).LT.5) GO TO 2321	RICE8	348
470	GO TO (2307,2309,2311,2313,2315)L	RICE8	349
501	2307 CQ(I,J)=RHO(I,J) \$ GO TO 2320	RICE8	350
510	2309 CQ(I,J)= PB(I,J) \$ GO TO 2320	RICE8	351
517	2311 CQ(I,J)=SIE(I,J) \$ GO TO 2320	RICE8	352
526	2313 CQ(I,J)=TE(I,J)	RICE8	353
534	GO TO 2320	RICE8	354
535	2315 IF(FL(I,J).GT.1.AND.FL(I,J).LT.6) GO TO 2321	RICE8	355
551	IF(FL(I,J).EQ.1)GO TO 2314	RICE8	356
556	NFL=FL(I,J)-5 \$ GO TO(2316,2317,2318,2319,2316,2317,2318,2319)NFL	RICE8	357
574	2314 CQ(I,J)=SQRT((U(I,J)+U(I-1,J))**2+(V(I,J)+V(I,J-1))**2)/	RICE8	358
	ICSQ(I,J)*.5 \$ GO TO 2320	RICE8	359
625	2316 CQ(I,J)=SQRT((U(I,J)**2+V(I,J)**2)/CSQ(I,J)) \$ GO TO 2320	RICE8	360
647	2317 CQ(I,J)=SQRT((U(I-1,J)**2+V(I,J)**2)/CSQ(I,J)) \$ GO TO 2320	RICE8	361
671	2318 CQ(I,J)=SQRT((U(I-1,J)**2+V(I,J-1)**2)/CSQ(I,J)) \$ GO TO 2320	RICE8	362
713	2319 CQ(I,J)=SQRT((U(I,J)**2+V(I,J-1)**2)/CSQ(I,J)) \$ GO TO 2320	RICE8	363
735	2321 CQ(I,J)=0.	RICE8	364
741	2320 CONTINUE	RICE8	365
746	CALL CNPLOT(1)	RICE8	366
750	CALL CNPLOT(2,L)	RICE8	367
752	2325 CONTINUE	RICE8	368
754	IF(NSPEC.LT.1) GO TO 2170	RICE8	369
757	2330 DO 2355 K=1,NSPEC	RICE8	370
761	IF(1SPEC(K).NE.1) GO TO 2355	RICE8	371
763	DO 2350 J=1,J82	RICE8	372
765	DO 2350 I=1,I82	RICE8	373
766	IF(FL(I,J).GT.1.AND.FL(I,J).LT.5) GO TO 2350	RICE8	374
1001	CQ(I,J)=FA(I,J,K)	RICE8	375
1007	IF(CQ(I,J).LT.0.)CQ(I,J)=0.	RICE8	376
1017	2350 CONTINUE	RICE8	377
1024	CALL CNPLOT(1)	RICE8	378
1026	CALL CNPLOT(3,K)	RICE8	379
1030	2355 CONTINUE	RICE8	380
	C**** END OF CONTOUR PLOT SECTION-----START OF COLOR PLOT SECTION* * *	RICE8	381
	C	RICE8	382
	C**** PLOTS SPECIFIED SPECIES (FA) DENSITIES ON ONE FRAME	RICE8	383
	C**** USES DIFFERENT SYMBOLS FOR BLACK AND WHITE. COPLOT SUBROUTINE MUST	RICE8	384
	C**** BE CHANGED FOR COLOR-USING ALL DOTS AND DIFFERENT COLORS	RICE8	385
	C	RICE8	386
1033	2360 IF(LPR.EQ.0)GO TO 2170	RICE8	387
1034	IF(LPR.EQ.2)GO TO 2170	RICE8	388
1036	2365 CALL ADV(1)	RICE8	389
1040	CALL COPLOT(1)	RICE8	390
1042	DO 2375 K=1,NSPEC	RICE8	391
1044	IF(1SPEC(K).NE.1) GO TO 2375	RICE8	392
1046	DO 2370 J=1,J82	RICE8	393
1050	DO 2370 I=1,I82	RICE8	394
1051	IF(FA(I,J,K).LT.0.)GO TO 2368	RICE8	395
1057	IF(FL(I,J).GT.1.AND.FL(I,J).LT.6) GO TO 2368	RICE8	396

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1071	IF (FA(I,J,K).LT.EP(K))GO TO 2368			RICE8	397
1105	PTCL=10000./((18*JB)*RRHO			RICE8	398
1112	CQ(I,J)=FA(I,J,K)*PTCL+.5			RICE8	399
1116	GO TO 2370			RICE8	400
1117	2368 CQ(I,J)=0.			RICE8	401
1123	2370 CONTINUE			RICE8	402
1130	CALL COPL0T(2,K)			RICE8	403
1132	2375 CONTINUE			RICE8	404
1135	2170 CONTINUE			RICE8	405
1135	CALL SECOND(TNOW)			RICE8	406
C****	RELEASES DISK DATA TO TAPE EVERY 35 MINUTES * * * * *			RICE8	407
1137	IF(TNOW-TBEG.LT.TRDISK) GO TO 2174			RICE8	408
1143	TRDISK=TRDISK+2100.			RICE8	409
1144	CALL DATAREL(5LFSETS)			RICE8	410
1146	2174 CONTINUE			RICE8	411
1146	KTAPE=9			RICE8	412
C****	WRITES FLUID VARIABLES U,V,RHO,P,I,T,MU (TAPE-9) ALSO ON FILM* * * * *			RICE8	413
1147	IF(LPR.EQ.5)GO TO 2266			RICE8	414
1151	IF(SECREQ-20..LE.TNOW-TBEG)GO TO 2248			RICE8	415
1156	IF(CYCLE.LT.0)GO TO 2248			RICE8	416
1160	IF(TIME+.000001.LT.TPRI)GO TO 2266			RICE8	417
1163	TPRI=TPRI+TPR			RICE8	418
1165	2248 CONTINUE			RICE8	419
1165	2250 CALL ADV(2)			RICE8	420
1167	2252 WRITE(KTAPE,9)CYCLE,TIME,NAME			RICE8	421
1201	WRITE(KTAPE,30)			RICE8	422
1205	IJC=0			RICE8	423
1206	DO 2265 J=1,JB2			RICE8	424
1210	DO 2265 I=1,IB2			RICE8	425
1211	IJC=IJC+1			RICE8	426
1212	IF(IJC.LT.56)GO TO 2255			RICE8	427
1214	IJC=0 \$ WRITE(KTAPE,9)CYCLE,TIME,NAME			RICE8	428
1226	WRITE(KTAPE,30)			RICE8	429
1232	2255 WRITE(KTAPE,31)I,J,FL(I,J),U(I,J),V(I,J),RHO(I,J),PB(I,J)			RICE8	430
	I,SIE(I,J),TE(I,J),MU(I,J)			RICE8	431
1332	2265 CONTINUE			RICE8	432
1337	IF(NSPEC.LT.1)GO TO 2264			RICE8	433
1342	CALL ADV(1)			RICE8	434
1343	WRITE(KTAPE,9)CYCLE,TIME,NAME			RICE8	435
1355	WRITE(KTAPE,32)			RICE8	436
1361	WRITE(KTAPE,33)			RICE8	437
1365	IJC=0			RICE8	438
C****	WRITES SPECIES DENSITIES (TAPE-9) ALSO ON FILM (TAPE-12) * * * * *			RICE8	439
1366	DO 2263 J=1,JB2			RICE8	440
1370	DO 2263 I=1,IB2			RICE8	441
1371	IF(IJC.LT.56)GO TO 2262			RICE8	442
1373	IJC=0			RICE8	443
1374	WRITE(KTAPE,9)CYCLE,TIME,NAME			RICE8	444
1405	WRITE(KTAPE,32) \$ WRITE(KTAPE,33)			RICE8	445
1415	2262 WRITE(KTAPE,31)I,J,FL(I,J),(FA(I,J,K),K=1,NSPEC)			RICE8	446
1451	IJC=IJC+1			RICE8	447
1453	2263 CONTINUE			RICE8	448
1460	2264 CONTINUE			RICE8	449
1460	2266 IF(LPR.EQ.4)GO TO 2267			RICE8	450
1462	IF(LPR.LE.0)GO TO 2267			RICE8	451

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1463      IF(SECREQ-20..LE.TNOW-TBEG)GO TO 2268      RICE8      452
1470      IF(CYCLE.LE.1)GO TO 2268      RICE8      453
1473      IF(TIME+.000001.LT.TPLOD)GO TO 2267      RICE8      454
1476      TPLOD=TPLOD+TPLD      RICE8      455
1500  2268 IF(KTAPE.EQ.12)GO TO 2267      RICE8      456
1502      CALL ADV(1)      RICE8      457
1504      KTAPE=12 $ GO TO 2252      RICE8      458
1506  2267 CONTINUE      RICE8      459
1506      IF(ITD.EQ.1.OR.ITD.EQ.3)GO TO 2270      RICE8      460
1516      GO TO 2280      RICE8      461
1516  2270 CONTINUE      RICE8      462
1516      IF(SECREQ-20..LE.TNOW-TBEG)GO TO 2274      RICE8      463
1523      IF(CYCLE.EQ.NSDMP)GO TO 2274 $ GO TO 2280      RICE8      464
1526  2274 WRITE(9,3)NWDMP,CYCLE,TIME      RICE8      465
C      RICE8      466
C**** WRITES DATA ON TAPES FOR RESTART IF ITD = 1 OR 3      RICE8      467
1540      NSDMP=NSDMP+NCYOMP      RICE8      468
1542      WRITE(5) NWDMP,1B2,JB2      RICE8      469
1553      WRITE(5)((U(I,J),V(I,J),RHO(I,J),SIE(I,J),I=1,1B2),J=1,JB2)      RICE8      470
1621      IF(NSPEC.LT.1)GO TO 2278      RICE8      471
1624      WRITE(5)((FA(I,J,K),I=1,1B2),J=1,JB2),K=1,NSPEC)      RICE8      472
1647  2278 CONTINUE      RICE8      473
1647      IF(SECREQ-20..LE.TNOW-TBEG) CALL EXIT      RICE8      474
1655      NWDMP=NWDMP+1      RICE8      475
1657  2280 CONTINUE      RICE8      476
1657      IF(SECREQ-20..LE.TNOW-TBEG)CALL EXIT      RICE8      477
C*****END OF CYCLE,PRINT AND PLOT FINISHED*****      RICE8      478
C**** START OF NEW CYCLE----ALL QUANTITIES CORRESPOND IN TIME-----      RICE8      479
C**** STOPS CALC. 20 SEC. BEFORE REQUESTED TIME ON JOB CARD USED TO      RICE8      480
C**** ALLOW TIME FOR OUTPUT      RICE8      481
C      RICE8      482
C      RICE8      483
1665      IF(TIME+.000001.GE.TSTOP)GO TO 5000      RICE8      484
C**** CALCULATES THE NECESSARY TILDE QUANTITIES--RHOVT,RHOVT AND RHOT **      RICE8      485
1671      CALL TILDE      RICE8      486
C      REGION 4000 DETERMINES NEW CELL BOUNDARY VELOCITIES      RICE8      487
C      RICE8      488
C**** VELOCITIES ARE DETERMINED FROM RHOV,RHOV,AND RHO      RICE8      489
C      RICE8      490
1672      JC=0      RICE8      491
1673  4000 DO 4400 J=2,JB1      RICE8      492
1675      JC=JC+1B2      RICE8      493
1676      DO 4400 I=2,1B1      RICE8      494
1700      IJ=I+JC      RICE8      495
1701      IPJ=IJ+1      RICE8      496
1702      JJP=IJ+1B2      RICE8      497
1704      NFL=FL(IJ)      RICE8      498
1707      GO TO (4050,4200,4200,4200,4200,4050,4200,4200,4050,4050,4200,4200)      RICE8      499
1,4050)NFL      RICE8      500
1727  4050 NFL=FL(IPJ)      RICE8      501
1732      GO TO (4100,4200,4200,4150,4200,4200,4100,4100,4200,4200,4100,4100)      RICE8      502
1,4200)NFL      RICE8      503
1752  4100 U(IJ)=2.*RHOV(IJ)/(RHO(IJ)+RHO(IPJ)) $ GO TO 4200      RICE8      504
1763  4150 U(IJ)=RHOV(IJ)/RHO(IJ) $ GO TO 4200      RICE8      505
1770  4200 NFL=FL(IJ)      RICE8      506

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	SUBROUTINE RTAPE5	RICE8	542
	C**** TAPE-5 DATA FOR STORAGE AND RESTART	RCOM1	2
1	COMMON/TAPE5/ITO,NTD,NSDMP,NFILE,NNDMP,NCYDMP	RCOM1	3
	C**** THE RCOM1 DATA BLOCK IS USED IN RICE(MAIN-PROGRAM),PROG AND RTAPE5	RCOM1	4
	C	RCOM1	5
	C**** THE RCOM2 DATA BLOCK IS COMMON TO RICE AND ALL SUBROUTINES	RCOM1	6
	C**** BOTH RCOM1 AND RCOM2 ARE LOADED USING *COMDECK FEATURE OF (UPDATE)	RCOM1	7
1	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASQ	RCOM2	4
1	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECREQ,DDX,DDY	RCOM2	5
	I,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,XI,IT	RCOM2	6
1	COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,	RCOM2	7
	IRINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIET1,SIET2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
1	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
1	COMMON/SPEC0/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	IFAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
1	COMMON/OBSD/ITO(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	I,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FABO(7,20)	RCOM2	16
1	INTEGER AM,BM	RCOM2	17
1	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
1	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),PI(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHOT(62, 32),RHOU(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CO(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
1	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
1	EQUIVALENCE (RHOU,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
1	INTEGER FL,CYCLE	RCOM2	34
1	REAL MU	RCOM2	35
	1 FORMAT(24I3)	RICE8	545
1	68 READ(5) NTDMP,IB2,JB2	RICE8	546
12	WRITE(9,1)NTDMP,NTD	RICE8	547
22	IF(NTD.EQ.NTDMP)GO TO 70	RICE8	548
24	READ (5)	RICE8	549
27	READ (5)	RICE8	550
32	IF(NTDMP.EQ.NFILE)GO TO 75	RICE8	551
34	IF(EOF,5)75,68	RICE8	552
37	70 READ (5)((U(1,J),V(1,J),RHO(1,J),SIE(1,J),I=1,IB2),J=1,JB2)	RICE8	553
105	IF(NSPEC.LT.1)GO TO 73	RICE8	554
110	READ (5)((FA(1,J,K),I=1,IB2),J=1,JB2),K=1,NSPEC)	RICE8	555
133	73 CONTINUE	RICE8	556
133	IF(NTDMP.NE.NFILE)GO TO 68	RICE8	557
135	75 CONTINUE	RICE8	558

135	RETURN \$ END	RICE8	559
C		RICE8	560
C		RICE8	561
C	***** END OF THE SUBROUTINE RTAPES *****	RICE8	562
C		RICE8	563
C		RICE8	564

	SUBROUTINE TILDE	RICE6	565
1	COMMON/GEOMD/1B2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASQ	RCOM2	4
1	COMMON/ICCD/1B,JB,1B1,JB1,NAME(10),JNM,TBEG,SECREC,DDX,DDY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,XI,IT	RCOM2	6
1	COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,	RCOM2	7
	1RINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIE1,SIE2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
1	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
1	COMMON/SPEC0/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q(3),CF(3),ZETAF(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
1	COMMON/OBSD/1TO(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FABO(7,20)	RCOM2	16
1	INTEGER AM,BM	RCOM2	17
1	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO 1B2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
1	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHOT(62, 32),RHOV(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CQ(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
1	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
1	EQUIVALENCE (RHOV,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
1	INTEGER FL,CYCLE	RCOM2	34
1	REAL MU	RCOM2	35
1	JC=0	RICE8	567
	C	RICE8	568
	C**** START OF CALC.FOR MASS EQ.,INTERMEDIATE SOLUTION (RHOT)	RICE8	569
	C	RICE8	570
2	DO 2000 J=2,JB1	RICE8	571
4	JC=JC+1B2	RICE8	572
5	DO 2000 I=2,1B1	RICE8	573
7	IJ=I+JC	RICE8	574
10	IPJ=IJ+1	RICE8	575
11	IMJ=IJ-1	RICE8	576
12	IJP=IJ+1B2	RICE8	577
14	IJM=IJ-1B2	RICE8	578
14	IMJM=IJM-1	RICE8	579
15	IPJM=IJM+1	RICE8	580
16	IMJP=IJP-1	RICE8	581
20	IPJP=IJP+1	RICE8	582
21	NFL=FL(IJ) \$ GO TO(1805,2000,2000,2000,2000,1810,1820,1820,1810,	RICE8	583
	11815,1820,1820,1815)NFL	RICE8	584
44	1805 UL=U(IMJ) \$ GO TO 1825	RICE8	585
50	1810 V=V(IJ,I) \$ GO TO 1825	RICE8	586


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503 1962 IF(U(IMJ).EQ.0.)GO TO 1960                      RICEB                      642
506     TAUTE=-.5*DT*(2.0*THETA-1.0)*(U(IMJ)**2+GAMMA*(GAMMA-1.)*SIE(IMJ))                      RICEB                      643
      I+.125*DX*(UR-U(IMJ))                      RICEB                      644
526     IF(TAUTE.LT.0.)GO TO 1965                      RICEB                      645
530     TAUL=(1.+X1)*TAUTE $ GO TO 1970                      RICEB                      646
533 1965 TAUL=(1.-X1)*TAUTE                      RICEB                      647
536 1970 RFL=(1.-THETA)*RHO(IMJ)*U(IMJ)-2.*DDX*TAUL*(RHO(IJ)-RHO(IMJ))                      RICEB                      648
553 1972 IF(FL(IJ).EQ.1)GO TO 1980                      RICEB                      649
557     NFL=FL(IJ)-5 $ GO TO(1975,1975,1980,1980,1975,1975,1980,1980)NFL                      RICEB                      650
574 1975 RFLB(I)=0. $ GO TO 1985                      RICEB                      651
577 1980 NFL=FL(IJM) $ GO TO(1985,1975,1975,1975,1975,1975,1985,1985,1975,1975
      I,1985,1985,1975,1975)NFL                      RICEB                      653
624 1985 RHOT(IJ)=RHO(IJ)+DT*(DDX*(RFL-RFLR)+DDY/RJ(IJ)*(RFL(I)-RFLT))                      RICEB                      654
637     RFL=RFLR                      RICEB                      655
641     RFLB(I)=RFLT                      RICEB                      656
644 2000 CONTINUE                      RICEB                      657
C**** INTERMEDIATE MASS DENSITY CALC.COMPLETED                      RICEB                      658
C                      RICEB                      659
C**** START OF CALC.FOR MOMENTUM EQ.,INTERMEDIATE SOLUTION (RHOUT-RHOVT)                      RICEB                      660
C                      RICEB                      661
651     JC=0                      RICEB                      662
652     DO 2995 J=2,JB1                      RICEB                      663
653     JC=JC+1B2                      RICEB                      664
654     IBJ=JC+1B                      RICEB                      665
655     IB1J=IBJ+1                      RICEB                      666
657     IB2J=IBJ+2                      RICEB                      667
661     DO 2990 I=2,IB1                      RICEB                      668
662     IJ=I+JC                      RICEB                      669
663     IF(FL(IJ).GT.1.AND.FL(IJ).LE.5)GO TO 2990                      RICEB                      670
676     IPJ=IJ+1                      RICEB                      671
676     IMJ=IJ-1                      RICEB                      672
677     IJP=IJ+1B2                      RICEB                      673
701     IJM=IJ-1B2                      RICEB                      674
701     IMJM=IJM-1                      RICEB                      675
702     IPJM=IJM+1                      RICEB                      676
703     IMJP=IJP-1                      RICEB                      677
705     IPJP=IJP+1                      RICEB                      678
705     IF(FL(IJ).EQ.1)GO TO 2520                      RICEB                      679
710     NFL=FL(IJ)-5 $ GO TO(2520,2582,2990,2550,2520,2582,2990,2550)NFL                      RICEB                      680
C**** DETERMINES WHETHER TO CALC.OR SKIP RHOUT(I,J)                      RICEB                      681
C**** CALC. IF FL(I,J)=1,6,9,10 OR 13 AND IF(FL(I+1,J)=1,7,8,11 OR 12                      RICEB                      682
C                      RICEB                      683
726 2520 IRV=1                      RICEB                      684
727 2522 IF(FL(IPJ).EQ.1)GO TO 2600                      RICEB                      685
733     IF(FL(IPJ).LT.6)GO TO 2580                      RICEB                      686
736     NFL=FL(IPJ)-5                      RICEB                      687
741     GO TO(2580,2600,2600,2580,2580,2600,2600,2580)NFL                      RICEB                      688
754 2550 IRV=2 $ GO TO 2522                      RICEB                      689
C**** DETERMINES WHETHER TO CALC.OR SKIP RHOVT(IJ)                      RICEB                      690
C**** CALC. IF FL(I,J)=1,6,7,10 OR 11 AND IF(FL(I,J+1)=1,8,9,12 OR 13                      RICEB                      691
C                      RICEB                      692
756 2580 IF(IRV.EQ.2)GO TO 2990                      RICEB                      693
760 2582 IF(FL(IJP).EQ.1)GO TO 2800                      RICEB                      694
764     IF(FL(IJP).LT.6)GO TO 2990                      RICEB                      695
767     NFL=FL(IJP)-5                      RICEB                      696

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772	GO TO(2990,2990,2800,2800,2990,2990,2800,2800)NFL	RICE8	697
	C**** CALC.RHOUT,FLUID ON BOTH SIDES OF U	RICE8	698
	C	RICE8	699
1005	2600 CONTINUE	RICE8	700
1007	PC=P(IJ)	RICE8	701
1011	RUOLD=.5*U(IJ)*(RHO(IJ)+RHO(IPJ))	RICE8	702
1017	PR=P(IPJ)	RICE8	703
1021	NFL=FL(IJM)	RICE8	704
1024	GO TO(2615,2612,2612,2612,2612,2615,2615,2612,2612,2615,2615,2612,	RICE8	705
	2612)NFL	RICE8	706
1044	2612 RHOB=RHO(IJ) \$ VISB=MU(IJ) \$ GO TO 2625	RICE8	707
1052	2615 RHOB=RHO(IJM) \$ VISB=MU(IJM) \$ GO TO 2625	RICE8	708
1060	2625 NFL=FL(IPJM) \$ GO TO(2635,2630,2630,2630,2630,2635,2635,2630,	RICE8	709
	2630,2635,2635,2630,2630)NFL	RICE8	710
1103	2630 RHOB=RHO(IPJ) \$ VISBR=MU(IPJ) \$ GO TO 2640	RICE8	711
1111	2635 RHOB=RHO(IPJM) \$ VISBR=MU(IPJM) \$ GO TO 2640	RICE8	712
1117	2640 CONTINUE	RICE8	713
1117	NFL=FL(IJP) \$ GO TO(2655,2642,2642,2642,2642,2642,2642,2655,	RICE8	714
	2655,2642,2642,2655,2655)NFL	RICE8	715
1142	2642 IF(FL(IJP).NE.5)GO TO 2650	RICE8	716
1146	IF(V(IJ).EQ.0.)GO TO 2648	RICE8	717
1150	RTOP=2.*RHO(IJP)-RHO(IJ) \$ VIST=2.*MU(IJP)-MU(IJ) \$GOTO 2660	RICE8	718
1163	2648 RTOP=2.*RHO(IJP)-RHO(IPJP) \$ VIST=2.*MU(IJP)-MU(IPJP)	RICE8	719
1177	GO TO 2660	RICE8	720
1177	2650 RTOP=RHO(IJ) \$ VIST=MU(IJ) \$ GO TO 2660	RICE8	721
1205	2655 RTOP=RHO(IJP) \$ VIST=MU(IJP) \$ GO TO 2660	RICE8	722
1213	2660 NFL=FL(IPJP) \$ GO TO(2670,2665,2665,2665,2665,2665,2670,	RICE8	723
	2670,2665,2665,2670,2670)NFL	RICE8	724
1236	2665 IF(FL(IPJP).NE.5)GO TO 2668	RICE8	725
1242	IF(V(IPJ).EQ.0.)GO TO 2668	RICE8	726
1244	RHOTR=2.*RHO(IPJP)-RHO(IPJ) \$ VISTR=2.*MU(IPJP)- MU(IPJ)	RICE8	727
1257	GO TO 2675	RICE8	728
1257	2668 RHOTR=RHO(IPJ)	RICE8	729
1262	VISTR=MU(IPJ) \$ GO TO 2675	RICE8	730
1265	2670 RHOTR=RHO(IPJP)	RICE8	731
1270	VISTR=MU(IPJP) \$ GO TO 2675	RICE8	732
1273	2675 CONTINUE	RICE8	733
1273	NFL=FL(IJ) \$ GO TO(2677,2685,2685,2685,2685,2678,2685,2685,	RICE8	734
	2678,2679,2685,2685,2680)NFL	RICE8	735
1322	2677 SZZC=MU(IJ)*((2.+ALA)*U(IJ)-U(IMJ))*DDX+ALA*DDY/RJ(J)*	RICE8	736
	(RJ2(J)*V(IJ)-RJ2(J-1)*V(IJM)))	RICE8	737
1342	RU2C=.25*RHO(IJ)*(U(IJ)+U(IMJ))*2	RICE8	738
1350	GO TO 2685	RICE8	739
1352	2678 SZZC=0.	RICE8	740
1353	RU2C=RHO(IJ)*U(IJ)**2	RICE8	741
1357	GO TO 2685	RICE8	742
1360	2679 SZZC=2.*MU(IJ)*((2.+ALA)*U(IJ)*DDX+ALA*DDY*V(IJ))	RICE8	743
1372	RU2C=0.	RICE8	744
1373	GO TO 2685	RICE8	745
1374	2680 SZZC=2.*MU(IJ)*((2.+ALA)*U(IJ)*DDX-ALA*DDY*V(IJM))	RICE8	746
1407	RU2C=0.	RICE8	747
1411	GO TO 2685	RICE8	748
1411	2685 NFL=FL(IPJ) \$ GO TO(2686,2690,2690,2690,2690,2690,2687,2687,	RICE8	749
	2690,2690,2688,2689,2690)NFL	RICE8	750
1440	2686 SZZR=MU(IPJ)*((2.+ALA)*DDX*(U(IPJ)-U(IJ))+ALA*DDY/RJ(J)*	RICE8	751

	I(RJ2(J)*V(IPJ)-RJ2(J-1)*V(IPJM))	RICE6	752
1460	RUZR=.25*RHO(IPJ)*(U(IPJ)+U(IJ))*2	RICE8	753
1466	GO TO 2690	RICE8	754
1467	2687 SZZR=0.	RICE8	755
1470	RUZR=RHO(IPJ)*U(IJ)**2	RICE8	756
1475	GO TO 2690	RICE8	757
1476	2688 SZZR=2.*MU(IPJ)*(-(2.+ALA)*CUX*U(IJ)+ALA*DDY*V(IPJ))	RICE8	758
1511	RUZR=0.	RICE8	759
1512	GO TO 2690	RICE8	760
1513	2689 SZZR=2.*MU(IPJ)*(-(2.+ALA)*DDX*U(IJ)-ALA*DDY*V(IPJM))	RICE8	761
1527	RUZR=0.	RICE8	762
1531	GO TO 2690	RICE8	763
1531	2690 IF(FL(IPJ).EQ.7)GO TO 2695	RICE8	764
1535	IF(FL(IPJ).EQ.11)GO TO 2693	RICE8	765
1540	VBR=V(IPJM) \$ GO TO 2696	RICE8	766
1543	2693 VBR=-V(IJM) \$ GO TO 2696	RICE8	767
1547	2695 VBR=V(IJM) \$ GO TO 2696	RICE8	768
1553	2696 IF(FL(IJ).EQ.6)GO TO 2699	RICE8	769
1557	IF(FL(IJ).EQ.10)GO TO 2698	RICE8	770
1562	VB=V(IJM) \$ GO TO 2700	RICE8	771
1565	2698 VB=-V(IPJM) \$ GO TO 2700	RICE8	772
1571	2699 VB= V(IPJM) \$ GO TO 2700	RICE8	773
1575	2700 IF(FL(IPJM).EQ.6)GO TO 2701	RICE8	774
1601	IF(FL(IPJM).EQ.9)GO TO 2701	RICE8	775
1604	IF(FL(IPJM).EQ.10)GO TO 2701	RICE8	776
1607	IF(FL(IPJM).EQ.13)GO TO 2701	RICE8	777
1612	IF(FL(IJM).EQ. 7)GO TO 2703	RICE8	778
1615	IF(FL(IJM).EQ. 8)GO TO 2703	RICE8	779
1620	IF(FL(IJM).EQ.11)GO TO 2703	RICE8	780
1623	IF(FL(IJM).EQ.12)GO TO 2703 \$GO TO 2702	RICE8	781
1627	2701 IF(FL(IJM).EQ. 2)GO TO 2708	RICE8	782
1633	IF(FL(IJM).EQ. 3)GO TO 2709	RICE8	783
1636	2702 UBR=U(IJM) \$ GO TO 2710	RICE8	784
1642	2703 IF(FL(IPJM).EQ.2)GO TO 2708	RICE8	785
1646	IF(FL(IPJM).EQ.3)GO TO 2709 \$ GO TO 2702	RICE8	786
1651	2708 UBR= U(IJ) \$ GO TO 2710	RICE8	787
1655	2709 UBR=-U(IJ) \$ GO TO 2710	RICE8	788
1663	2710 SRZBR=.25*(V1SB+V1SBR+MU(IPJ)+MU(IJ))*((VBR-VB)*DDX I+(U(IJ)-UBR)*DDY)	RICE8	789
1700	RUVBR=(RHO(IJ)+RHO(IPJ)+RHOB+RHOBR)*(VB+VBR)*(U(IJ)+UBR)*.0625	RICE8	791
1714	IF(FL(IJ).EQ. 6.AND.U(IJM).NE.0.)SRZBR=SRZBR*.5	RICE8	792
1730	IF(FL(IJ).EQ.10.AND.U(IJM).NE.0.)SRZBR=SRZBR*.5	RICE8	793
1743	IF(FL(IPJ).EQ.8)GO TO 2715	RICE8	794
1747	IF(FL(IPJ).EQ.12)GO TO 2712	RICE8	795
1752	VTR=V(IPJ) \$ GO TO 2720	RICE8	796
1754	2712 VTR=-V(IJ) \$ GO TO 2720	RICE8	797
1760	2715 VTR=V(IJ) \$ GO TO 2720	RICE8	798
1764	2720 IF(FL(IJ).EQ.9)GO TO 2723	RICE8	799
1770	IF(FL(IJ).EQ.13)GO TO 2722	RICE8	800
1773	VT=V(IJ) \$ GO TO 2725	RICE8	801
1775	2722 VT=-V(IPJ) \$ GO TO 2725	RICE8	802
2001	2723 VT=V(IPJ) \$ GO TO 2725	RICE8	803
2005	2725 IF(FL(IPJP).EQ. 6)GO TO 2727	RICE8	804
2011	IF(FL(IPJP).EQ. 9)GO TO 2727	RICE8	805
2014	IF(FL(IPJP).EQ.10)GO TO 2727	RICE8	806

2017	IF (FL (IPJP).EQ.13)GO TO 2727	RICE6	807
2022	IF (FL (IJP).EQ. 7)GO TO 2729	RICE8	808
2025	IF (FL (IJP).EQ. 8)GO TO 2729	RICE8	809
2030	IF (FL (IJP).EQ.11)GO TO 2729	RICE8	810
2033	IF (FL (IJP).EQ.12)GO TO 2729 \$GO TO 2728	RICE8	811
2037	2727 IF (FL (IJP).EQ. 2)GO TO 2735	RICE8	812
2043	IF (FL (IJP).EQ. 3)GO TO 2740	RICE8	813
2746	2728 IF (FL (IJP).EQ.5.AND.V(IJ).NE.0.)UTR=2.*U(IJP)-U(IJ)	RICE8	814
2065	IF (FL (IJP).NE.5)UTR=U(IJP)	RICE8	815
2073	GO TO 2750	RICE8	816
2074	2729 IF (FL (IPJP).EQ.2)GO TO 2735	RICE8	817
2100	IF (FL (IPJP).EQ.3)GO TO 2740 \$ GO TO 2728	RICE8	818
2103	2735 UTR= U(IJ) \$ GO TO 2750	RICE8	819
2107	2740 UTR=-U(IJ) \$ GO TO 2750	RICE8	820
2113	2750 CONTINUE	RICE8	821
2115	SRZTR=.25*(MU(IJ)+MU(IPJ)+V1ST+V1STR)*((VTR -VT)*DDX+ 1(UTR-U(IJ))*DDY)	RICE8	822
2132	RUVTR=(RHO(IJ)+RHO(IPJ)+RHOTR+RTOP)*(VT+VTR)*(U(IJ)+UTR)*.0525	RICE8	823
2145	IF (FL (IJ).EQ. 9.AND.U(IJP).NE.0.)SRZTR=SRZTR*.5	RICE8	824
2161	IF (FL (IJ).EQ.13.AND.U(IJP).NE.0.)SRZTR=SRZTR*.5	RICE8	825
2175	T1=(RJ2(IJ-1)*RUVBR-SRZBR)-RJ2(IJ)*(RUVTR-SRZTR)/(R(IJ)*DY)	RICE8	827
2210	T2=(RU2C+ PC-SZ2C-RU2R-PR+SZZR)*DDX	RICE8	828
2217	RHOUT(IJ)=RUOLD*DT*(T1+T2)	RICE8	829
	C**** INTERMEDIATE -- AXIAL MOMENTUM CALC.COMPLETE * * * * *	RICE8	831
	C	RICE8	832
	C**** FINISHED RHOUT(I,J) CALC.----START (R)/VT(I,J) CALC.	RICE8	833
	C	RICE8	834
2224	GO TO 2580	RICE8	835
2224	2800 CONTINUE	RICE8	836
2226	PC=P(IJ)	RICE8	837
2230	RVOLD=.5*V(IJ)*(RHO(IJ)+RHO(IPJ))	RICE8	838
2236	PT=P(IJP)	RICE8	839
2240	NFL=FL (IMJ) \$ GO TO(2801,2805,2805,2805,2803,2801,2805,2805, 12801,2801,2805,2805,2801)NFL	RICE8	841
2263	2801 RHOL=RHO(IMJ) \$ V1SL=MU(IMJ) \$ GO TO 2807	RICE8	842
2271	2803 IF (U(IMJ).EQ.0) GO TO 2805	RICE8	843
2274	RHOL=2.*RHO(IMJ)-RHO(IJ) \$ V1SL=2.*MU(IMJ)-MU(IJ) \$GOTO 2807	RICE8	844
2307	2805 RHOL=RHO(IJ) \$ V1SL=MU(IJ) \$ GO TO 2807	RICE8	845
2315	2807 NFL=FL (IMJP) \$ GO TO(2802,2810,2810,2810,2809,2808,2810 ,2810, 12808,2808,2810,2810,2808)NFL	RICE8	847
2340	2808 RHOTL=RHO(IMJP) \$ V1STL=MU(IMJP) \$ GO TO 2815	RICE8	848
2346	2809 IF (U(IMJP).EQ.0)GO TO 2813	RICE8	849
2351	RHOTL=2.*RHO(IMJP)-RHO(IJP) \$ V1STL=2.*MU(IMJP)-MU(IJP)	RICE8	850
2363	GO TO 2815	RICE8	851
2364	2810 RHOTL=RHO(IJP) \$ V1STL=MU(IJP) \$ GO TO 2815	RICE8	852
2372	2813 RHOTL=2.*RHO(IMJP)-RHO(IMJ) \$ V1STL=2.*MU(IMJP)-MU(IMJ)	RICE8	853
2406	GO TO 2815	RICE8	854
2406	2815 CONTINUE	RICE8	855
2406	NFL=FL (IPJ) \$ GO TO(2818,2817,2817,2817,2817,2818,2818,2818, 12817,2818,2818,2818,2817)NFL	RICE8	857
2431	2817 RHOR=RHO(IPJ) \$ V1SR=MU(IPJ) \$ GO TO 2820	RICE8	858
2437	2818 RHOR=RHO(IPJ) \$V1SR=MU(IPJ) \$ GO TO 2820	RICE8	859
2445	2820 NFL=FL (IPJP) \$ GO TO(2822,2821,2821,2821,2821,2821,2821,2822,2822, 12822,2821,2822,2822,2822)NFL	RICE8	860
2470	2821 RHOTR=RHO(IJP) \$ V1STR=MU(IJP) \$ GO TO 2825	RICE8	861

2476	2822	RHOTR=RHO(IJP) \$ VISTR=MU(IJP) \$ GO TO 2825	RICE6	862
2504	2825	CONTINUE	RICE8	863
2504		IF(FL(IJ).NE.1)GO TO 2828	RICE8	864
2510		RV2C=.25*RHO(IJ)*(V(IJ)+V(IMJ))*2	RICE8	865
2516		SRRC=MU(IJ)*(2.*DDY*(V(IJ)-V(IMJ))+ALA*(DDY/RJ(J)*(RJ2(J)+V(IJ)-RJ2(J-1)*V(IMJ))+DDX*(U(IJ)-U(IMJ))))\$ GO TO 2838	RICE8	866
2547	2828	IF(FL(IJ).EQ.6)GO TO 2830	RICE8	867
2553		IF(FL(IJ).EQ.7)GO TO 2830	RICE8	868
2556		IF(FL(IJ).EQ.10)GO TO 2833	RICE8	869
2561		RV2C=0.	RICE8	870
2561		SRRC=2.*MU(IJ)*((2.+ALA)*DDY*V(IJ)-ALA*DDX*U(IMJ))\$GO TO 2838	RICE8	871
2600	2830	SRRC=0.	RICE8	872
2601		RV2C=RHO(IJ)*V(IJ)**2	RICE8	873
2605		GO TO 2838	RICE8	874
2606	2833	SRRC=2.*U(IJ)*((2.+ALA)*DDY*V(IJ)+ALA*DDX*U(IJ))	RICE8	875
2620		RV2C=0.	RICE8	876
2621	2838	IF(FL(IJP).EQ.1)GO TO 2840	RICE8	877
2625		IF(FL(IJP).EQ.8)GO TO 2843	RICE8	878
2630		IF(FL(IJP).EQ.9)GO TO 2843	RICE8	879
2633		IF(FL(IJP).EQ.12)GO TO 2845	RICE8	880
2636		RV2T=0.	RICE8	881
2636		SRRT=-2.*MU(IJP)*((2.+ALA)*DDY*V(IJ)-ALA*DDX*U(IJP))\$GOTO2847	RICE8	882
2657	2840	SRRT=MU(IJP)*(2.*DDY*(V(IJP)-V(IJ))+ALA*(DDY/RJ(J+1)*(RJ2(J+1)*V(IJP)-RJ2(J)*V(IJ))+DDX*(U(IJP)-U(IMJP))))	RICE8	883
2703		RV2T=.25*RHO(IJP)*(V(IJ)+V(IJP))*2	RICE8	884
2711		GO TO 2847	RICE8	885
2712	2843	SRRT=0.	RICE8	886
2713		RV2T=RHO(IJP)*V(IJ)**2	RICE8	887
2720		GO TO 2847	RICE8	888
2720	2845	SRRT=2.*MU(IJP)*((-2.+ALA)*DDY*V(IJ)-ALA*DDX*U(IMJP))	RICE8	889
2735		RV2T=0.	RICE8	890
2736	2847	IF(FL(IMJP).EQ.6)GO TO 2848	RICE8	891
2742		IF(FL(IMJP).EQ.7)GO TO 2848	RICE8	892
2745		IF(FL(IMJP).EQ.10)GO TO 2848	RICE8	893
2750		IF(FL(IMJP).EQ.11)GO TO 2848	RICE8	894
2753		IF(FL(IMJ).EQ.8)GO TO 2850	RICE8	895
2756		IF(FL(IMJ).EQ.9)GO TO 2850	RICE8	896
2761		IF(FL(IMJ).EQ.12)GO TO 2850	RICE8	897
2764		IF(FL(IMJ).EQ.13)GO TO 2850 \$ GO TO 2849	RICE8	898
2770	2848	IF(FL(IMJ).EQ.2)GO TO 2852	RICE8	899
2774		IF(FL(IMJ).EQ.3)GO TO 2853	RICE8	900
2777	2849	IF(FL(IMJ).EQ.5.AND.U(IMJ).NE.0.)VTL=2.*V(IMJ)-V(IJ)	RICE8	901
3016		VTL=V(IMJ)	RICE8	902
3021		GO TO 2855	RICE8	903
3022	2850	IF(FL(IMJP).EQ.2)GO TO 2852	RICE8	904
3026		IF(FL(IMJP).EQ.3)GO TO 2853 \$ GO TO 2849	RICE8	905
3031	2852	VTL=V(IJ) \$ GO TO 2855	RICE8	906
3035	2853	VTL=-V(IJ) \$ GO TO 2855	RICE8	907
3041	2855	IF(FL(IJ).EQ.6)GO TO 2858	RICE8	908
3045		IF(FL(IJ).EQ.10)GO TO 2860	RICE8	909
3050		UL=U(IMJ) \$ GO TO 2863	RICE8	910
3053	2858	UL=U(IMJP) \$ GO TO 2863	RICE8	911
3057	2860	UL=-U(IMJP) \$ GO TO 2863	RICE8	912
3063	2863	IF(FL(IJP).EQ.9)GO TO 2865	RICE8	913
3067		IF(FL(IJP).EQ.13)GO TO 2868	RICE8	914

3072	UTL=U(IJ); \$ GO TO 2870	RICE8	917
3075	2865 UTL=U(IJ); \$ GO TO 2870	RICE8	918
3101	2868 UTL=-U(IJ); \$ GO TO 2870	RICE8	919
3107	2870 SRZTL=.25*(V(SL+MU(IJ)+MU(IJP)+VISTL)*((V(IJ)-VTL)*DDX+ I(UTL-UL)*DDY)	RICE8	920
		RICE8	921
3124	RUVTL=(RHO(IJ)+RHO(IJP)+RHOL+RHOTL)*(VTL+V(IJ))*(UTL+UL)*.0625	RICE8	922
3140	IF(FL(IPJP).EQ.6)GO TO 2871	RICE8	923
3144	IF(FL(IPJP).EQ.7)GO TO 2871	RICE8	924
3147	IF(FL(IPJP).EQ.10)GO TO 2871	RICE8	925
3152	IF(FL(IPJP).EQ.11)GO TO 2871	RICE8	926
3155	IF(FL(IPJP).EQ.8)GO TO 2873	RICE8	927
3161	IF(FL(IPJP).EQ.9)GO TO 2873	RICE8	928
3164	IF(FL(IPJP).EQ.12)GO TO 2873	RICE8	929
3167	IF(FL(IPJP).EQ.13)GO TO 2873 \$GO TO 2872	RICE8	930
3172	2871 IF(FL(IPJP).EQ.2)GO TO 2874	RICE8	931
3176	IF(FL(IPJP).EQ.3)GO TO 2875	RICE8	932
3201	2872 VTR=V(IJP) \$ GO TO 2878	RICE8	933
3205	2873 IF(FL(IPJP).EQ.2)GO TO 2874	RICE8	934
3211	IF(FL(IPJP).EQ.3)GO TO 2875 \$ GO TO 2872	RICE8	935
3214	2874 VTR=V(IJ) \$ GO TO 2878	RICE8	936
3220	2875 VTR=-V(IJ) \$ GO TO 2878	RICE8	937
3224	2878 IF(FL(IJ).EQ.7)GO TO 2880	RICE8	938
3230	IF(FL(IJ).EQ.11)GO TO 2882	RICE8	939
3233	UR=U(IJ) \$ GO TO 2884	RICE8	940
3235	2880 UR=U(IJP) \$ GO TO 2884	RICE8	941
3241	2882 UR=-U(IJP) \$ GO TO 2884	RICE8	942
3245	2884 IF(FL(IJP).EQ.8)GO TO 2886	RICE8	943
3251	IF(FL(IJP).EQ.12)GO TO 2888	RICE8	944
3254	UTR=U(IJP) \$ GO TO 2890	RICE8	945
3256	2886 UTR=U(IJ) \$ GO TO 2890	RICE8	946
3262	2888 UTR=-U(IJ) \$ GO TO 2890	RICE8	947
3275	2890 SRZTR=.25*(MU(IJ)+VISR+VISTR+MU(IJP))*((VTR-V(IJ))*DDX+(UTR-UR)* IDDY)	RICE8	948
		RICE8	949
3310	RUVTR=(RHO(IJ)+RHO(IJP)+RHOR+RHOTR)*(V(IJ)+VTR)*(UTR+UR)*.0625	RICE8	950
3321	S00T=(MU(IJP)+MU(IJ))*(V(IJ)/RJ2(J)+.25*ALA*IDDY/RJ2(J)+ I(RJ(J+1)*(V(IJP)+V(IJ))-RJ(J)*(V(IJ)+V(IJ))))+ IDDX*((UTR+UR)-(UTL+UL))*ITC	RICE8	951
		RICE8	952
		RICE8	953
3352	RHOVT(IJ)=RVOLD*DT*((RJ(J)*(RV2C -SRRC)-RJ(J+1)*(RV2T-SRRT))/ I(RJ2(J)*DY)+(RUVTL-SRZTL-RUV TR+SRZTR)*DDX+(PC-PT)*DDY- 2S00T/RJ2(J))	RICE8	954
		RICE8	955
		RICE8	956
	C**** INTERMEDIATE -- RADIAL MOMENTUM CALC.COMPLETE * * * * *	RICE8	957
3404	2990 CONTINUE	RICE8	958
3407	IF(FL(1B2J).EQ.4)RHOUT(1B1J)=RHOUT(1B1J)	RICE8	959
3416	2995 CONTINUE	RICE8	960
	C	RICE8	961
	C**** END OF TILDE CALC.---ARRAYS OF RHOT,RHOUT AND RHOVT STORED	RICE8	962
	C	RICE8	963
	C**** START OF ITERATION TO OBTAIN FINAL VALUES OF RHOU,RHOV AND RHO	RICE8	964
3421	IT=0	RICE8	965
3422	3705 ITF=0	RICE8	966
3423	IT=IT+1	RICE8	967
3425	JC=0	RICE8	968
3426	DO 3800 J=2,JB1	RICE8	969
3427	JC=JC+1B2	RICE8	970
3430	DO 3800 I=2,1B1	RICE8	971

3432	IJ=1+JC	RICE8	972
3433	IPJ=IJ+1	RICE8	973
3434	IMJ=IJ-1	RICE8	974
3435	IJP=IJ+182	RICE8	975
3437	IJM=IJ-182	RICE8	976
3437	IF(FL(IJ).GT.1.AND.FL(IJ).LT.6)GO TO 3800	RICE8	977
3451	DCSQ=1./CSQ(IJ)	RICE8	978
3454	IF(FL(IJ).EQ.1)GO TO 3710	RICE8	979
3460	NFL=FL(IJ)-5	RICE8	980
3462	GO TO(3710,3710,3725,3725,3710,3710,3725,3725)NFL	RICE8	981
3475	3710 NFL=FL(IJP)	RICE8	982
3500	GO TO(3715,3725,3725,3725,3717,3725,3725,3715,3715,3725,3725,3715,3715)NFL	RICE8	983
3520	3715 TOP=1.0	RICE8	984
3521	TP=1.0	RICE8	985
3523	GO TO 3730	RICE8	986
3524	3717 IF(V(IJ).EQ.0.)GO TO 3725	RICE8	987
3527	TOP=1.0	RICE8	988
3530	TP=0.	RICE8	989
3531	GO TO 3730	RICE8	990
3531	3725 TOP=0.	RICE8	991
3532	TP=0.	RICE8	992
3533	3730 IF(FL(IJ).EQ.1)GO TO 3733	RICE8	993
3537	NFL=FL(IJ)-5	RICE8	994
3541	GO TO(3733,3738,3738,3733,3733,3738,3738,3733)NFL	RICE8	995
3554	3733 NFL=FL(IPJ)	RICE8	996
3557	GO TO(3735,3738,3738,3735,3738,3738,3735,3735,3738,3738,3735,3735,3738)NFL	RICE8	997
3577	3735 RIGHT=1.0	RICE8	998
3601	GO TO 3740	RICE8	999
3601	3738 RIGHT=0.	RICE8	1000
3602	3740 IF(FL(IJ).EQ.1)GO TO 3743	RICE8	1001
3606	NFL=FL(IJ)-5	RICE8	1002
3610	GO TO(3753,3743,3743,3753,3753,3743,3743,3753)NFL	RICE8	1003
3623	3743 NFL=FL(IMJ)	RICE8	1004
3626	GO TO(3745,3753,3753,3753,3748,3745,3753,3753,3745,3745,3753,3753,3745)NFL	RICE8	1005
3646	3745 SLEFT=1.0	RICE8	1006
3647	SLT=1.0	RICE8	1007
3651	GO TO 3755	RICE8	1008
3652	3748 IF(U(IMJ).EQ.0.)GO TO 3753	RICE8	1009
3655	SLEFT=1.0	RICE8	1010
3656	SLT=0.0	RICE8	1011
3657	GO TO 3755	RICE8	1012
3660	3753 SLEFT=0.0	RICE8	1013
3661	SLT=0.0	RICE8	1014
3661	3755 IF(FL(IJ).EQ.1)GO TO 3758	RICE8	1015
3665	NFL=FL(IJ)-5	RICE8	1016
3667	GO TO(3763,3763,3758,3758,3763,3763,3758,3758)NFL	RICE8	1017
3702	3758 IF(FL(IJM).EQ.1)GO TO 3760	RICE8	1018
3706	IF(FL(IJM).LT.6)GO TO 3763	RICE8	1019
3711	NFL=FL(IJM)-5	RICE8	1020
3714	GO TO(3760,3760,3763,3763,3760,3760,3763,3763)NFL	RICE8	1021
3727	3760 BOTTOM=1.0	RICE8	1022
3731	GO TO 3765	RICE8	1023
		RICE8	1024
		RICE8	1025
		RICE8	1026

	SUBROUTINE ENERGY	RICE8	1053
1	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTG,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASQ	RCOM2	4
1	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECREQ,DDX,DDY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,XI,IT	RCOM2	6
1	COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,	RCOM2	7
	IRINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIEO,SIET1,SIET2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
1	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
1	COMMON/SPEC/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
1	COMMON/OBSD/I10(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	1,MINRO(20),SIEPO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FABO(7,20)	RCOM2	16
1	INTEGER AM,BM	RCOM2	17
1	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
1	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHO(62, 32),RHOV(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CQ(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
1	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
1	EQUIVALENCE (RHOV,RHOVT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
1	INTEGER FL,CYCLE	RCOM2	34
1	REAL MU	RCOM2	35
1	DO 4503 J=2,JB2	RICE8	1055
3	IBJ=IB2*(J-1)+IB	RICE8	1056
7	IB1J=IBJ+1	RICE8	1057
7	IB2J=IBJ+2	RICE8	1058
11	IB1JM=IB1J-IB2	RICE8	1059
12	IF (FL(1B2J).NE.4)GO TO 4503	RICE8	1060
	C	RICE8	1051
	C**** RHO AND P ARE SET CONTINUOUS(= COL.1B) AT OUTFLOW BOUNDARY	RICE8	1062
	C	RICE8	1063
16	RHO(1B2J)=RHO(1B1J)=RHO(1BJ)	RICE8	1064
24	P(1B2J)=P(1B1J)=P(1BJ)	RICE8	1065
33	4503 CONTINUE	RICE8	1066
36	JC=0	RICE8	1067
37	DO 4850 J=2,JB1	RICE8	1068
40	JC=JC+1B2	RICE8	1069
41	DO 4850 I=2,1B1	RICE8	1070
43	IJ=I+JC	RICE8	1071
	C	RICE8	1072
	C**** START OF RE CALC. BYPASS ALL CALC. IF FL(IJ)=2,3,4 OR 5	RICE8	1073
	C	RICE8	1074

44	IF (FL(IJ).GT.1.AND.FL(IJ).LT.6)GO TO 4850	RICE6	1075
56	IPJ=IJ+1	RICE8	1076
56	IMJ=IJ-1	RICE8	1077
57	IJP=IJ+1B2	RICE8	1078
61	IJM=IJ-1B2	RICE8	1079
61	IMJM=IJM-1	RICE8	1080
62	IPJM=IJP+1	RICE8	1081
63	IMJP=IJP-1	RICE8	1082
65	IPJP=IJP+1	RICE8	1083
C		RICE8	1084
C****	START OF ENERGY-DENSITY FLUX CALC.	RICE8	1085
C		RICE8	1086
65	IF (FL(IJ).EQ.1)GO TO 4510 \$ NFL=FL(IJ)-5	RICE8	1087
73	GO TO(4510,4507,4507,4510,4510,4507,4507,4510)NFL	RICE8	1088
106	4507 TRER=0. \$ GO TO 4605	RICE8	1089
110	4510 NFL=FL(IPJ)	RICE8	1090
113	GO TO(4515,4512,4512,4515,4512,4512,4515,4515,4512,4512,4515,4515,	RICE8	1091
	14512)NFL	RICE8	1092
133	4512 TRER=0. \$ GO TO 4605	RICE8	1093
137	4515 UR=U(IJ)	RICE8	1094
141	DIR=SIE(IPJ)-SIE(IJ)	RICE8	1095
144	PBR=(PB(IPJ)+PB(IJ))* .5	RICE8	1096
151	RMU=(MU(IPJ)+MU(IJ))* .5 \$ RER=(RE(IPJ)+RE(IJ))* .5	RICE8	1097
163	IF (FL(IPJ).EQ.1)GO TO 4521	RICE8	1098
167	IF (FL(IPJ).EQ.4)GO TO 4519	RICE8	1099
172	IF (FL(IPJ).EQ.7)GO TO 4519	RICE8	1100
175	IF (FL(IPJ).EQ.8)GO TO 4519	RICE8	1101
200	URR=-UR \$ GO TO 4522	RICE8	1102
202	4519 URR=UR \$ GO TO 4522	RICE8	1103
204	4521 URR=U(IPJ) \$ GO TO 4532	RICE8	1104
210	4522 IF (FL(IPJ).EQ.7)GO TO 4532	RICE8	1105
214	IF (FL(IPJ).EQ.11)GO TO 4532	RICE8	1106
217	IF (FL(IPJ).EQ.1)GO TO 4532	RICE8	1107
222	IF (FL(IPJ).EQ.4)GO TO 4527	RICE8	1108
225	IF (FL(IPJ).EQ.12)GO TO 4529	RICE8	1109
231	4527 VZTR=V(IPJM) \$ VRZTR=V(IJ) \$ GO TO 4535	RICE8	1110
237	4529 VZTR=-V(IPJM) \$ VRZTR=-V(IJ) \$ GO TO 4535	RICE8	1111
245	4532 VZTR=VRZTR=V(IPJ)	RICE8	1112
251	4535 IF (FL(IPJ).EQ.1)GO TO 4541	RICE8	1113
255	IF (FL(IPJ).EQ.8)GO TO 4541	RICE8	1114
260	IF (FL(IPJ).EQ.12)GO TO 4541	RICE8	1115
263	IF (FL(IPJ).EQ.4)GO TO 4543	RICE8	1116
266	4537 IF (FL(IPJM).EQ.1)GO TO 4541	RICE8	1117
272	IF (FL(IPJ).EQ.11)GO TO 4545	RICE8	1118
275	4539 VRZBR=V(IJM) \$ VZBR=V(IPJ) \$ GO TO 4550	RICE8	1119
303	4543 IF (FL(IPJM).EQ.4)GO TO 4539	RICE8	1120
307	4541 VZBR=V(IPJM) \$ VRZBR=V(IPJM) \$ GO TO 4550	RICE8	1121
315	4545 VRZBR=-V(IJM) \$ VZBR=-V(IPJ) \$ GO TO 4550	RICE8	1122
323	4550 NFL=FL(IJM) \$ GO TO(4554,4552,4552,4554,4554,4554,4552,4552,	RICE8	1123
	14554,4554,4552,4552,4554)NFL	RICE8	1124
346	4552 IF (FL(IPJM).EQ.1)GO TO 4554	RICE8	1125
352	IF (FL(IJM).EQ.2)GO TO 4556	RICE8	1126
355	IF (FL(IJM).EQ.7)GO TO 4556	RICE8	1127
360	IF (FL(IJM).EQ.8)GO TO 4556	RICE8	1128
363	GO TO 4558	RICE8	1129

364	4554	UBR=U(IJM) \$ GO TO 4560	RICE8	1130
370	4556	UBR=UR \$ GO TO 4560	RICE8	1131
372	4558	UBR=-UR \$ GO TO 4560	RICE8	1132
374	4560	NFL=FL(IJP) \$ GO TO(4564,4562,4562,4564,4564,4564,4562,4562, 14564,4564,4562,4562,4564)NFL	RICE8	1133
			RICE8	1134
417	4562	IF(FL(IJP),EQ.1)GO TO 4564	RICE8	1135
423		IF(FL(IJP),EQ.2)GO TO 4566	RICE8	1136
426		IF(FL(IJP),EQ.7)GO TO 4566	RICE8	1137
431		IF(FL(IJP),EQ.8)GO TO 4566	RICE8	1138
434		GO TO 4568	RICE8	1139
435	4564	UTR=U(IJP) \$ GO TO 4570	RICE8	1140
441	4566	UTR=UR \$ GO TO 4570	RICE8	1141
443	4568	UTR=-UR \$ GO TO 4570	RICE8	1142
445	4570	IF(FL(IJ),EQ.6)GO TO 4574	RICE8	1143
451		IF(FL(IJ),EQ.10)GO TO 4574	RICE8	1144
454	4572	VZB=V(IJM) \$ VRZB=V(IJM) \$ GO TO 4580	RICE8	1145
462	4574	IF(FL(IJM),EQ.1)GO TO 4572	RICE8	1146
466		IF(FL(IJ),EQ.6)GO TO 4578	RICE8	1147
471		VRZB=-V(IJM) \$ VZB=-V(IJ) \$ GO TO 4580	RICE8	1148
477	4578	VRZB=V(IJM) \$ VZB=V(IJ)	RICE8	1149
505	4580	IF(FL(IJ),EQ.1)GO TO 4582	RICE8	1150
511		IF(FL(IJM),EQ.1)GO TO 4582	RICE8	1151
514		IF(FL(IJ),EQ.6)GO TO 4586	RICE8	1152
517		IF(FL(IJ),EQ.9)GO TO 4586	RICE8	1153
522		GO TO 4584	RICE8	1154
523	4582	UL=U(IJM) \$ GO TO 4590	RICE8	1155
527	4584	UL=-U(IJ) \$ GO TO 4590	RICE8	1156
533	4586	UL=U(IJ) \$ GO TO 4590	RICE8	1157
537	4590	IF(FL(IJ),EQ.1)GO TO 4592	RICE8	1158
543		IF(FL(IJ),EQ.6)GO TO 4592	RICE8	1159
546		IF(FL(IJ),EQ.10)GO TO 4592	RICE8	1160
551		IF(FL(IJP),EQ.1)GO TO 4592	RICE8	1161
554		IF(FL(IJ),EQ.13)GO TO 4594	RICE8	1162
557		VRZT=V(IJP) \$ VZZT=V(IJM) \$ GO TO 4600	RICE8	1163
565	4592	VRZT=V(IJ) \$ VZZT=V(IJ) \$ GO TO 4600	RICE8	1164
573	4594	VRZT=-V(IJP) \$ VZZT=-V(IJM) \$ GO TO 4600	RICE8	1165
601	4600	CONTINUE	RICE8	1166
607		SZZR=RMU*.5*(12.+ALA)*DDX*(URR-UL)+ALA*DDY/F(IJ)*(RJ2(IJ)*(VZZTR+ 1VZZT)-RJ2(J-1)*(VZZBR+VZZB))	RICE8	1167
			RICE8	1168
627		SRZR=RMU*.5*!DDX*(1VRZTR+VRZBR)-(VRZT+VRZB)+DDY*(UTR-UBR)	RICE8	1169
637		VR=.25*(VRZBR+VRZTR+VRZT+VRZB)	RICE8	1170
	C****	ENERGY-DENSITY FLUX ACROSS RIGHT BOUNDARY=TRER	RICE8	1171
	C		RICE8	1172
643		TRER=UR*(RER+PBR-SZZR)-SRZR+VR-BIE*RMU*DDX*DIR	RICE8	1173
654	4605	IF(FL(IJ),EQ.1)GO TO 4607 \$ NFL=FL(IJ)-5	RICE8	1174
662		GO TO(4607,4607,4609,4609,4607,4607,4609,4609)NFL	RICE8	1175
675	4607	NFL=FL(IJP) \$ GO TO(4615,4610,4610,4610,4612,4610,4610,4615, 14615,4610,4610,4615,4615)NFL	RICE8	1176
			RICE8	1177
720	4609	CONTINUE	RICE8	1178
720	4611	TRET=0. \$ GO TO 4705	RICE8	1179
722	4612	IF(V(IJ),EQ.0.)GO TO 4610	RICE8	1180
726	4614	VT=V(IJ)	RICE8	1181
730		DTI=2.*(SIE(IJP)-SIE(IJ))	RICE8	1182
735		PT=PB(IJP) \$ TMU=MU(IJP) \$ RET=RE(IJP) \$ GO TO 4618	RICE8	1183
746	4615	VT=V(IJ)	RICE8	1184

750		DIT=SIE(IJP)-SIE(IJ)	RICE8	1185
753		PT=.5*(PB(IJP)+PB(IJ))	RICE8	1186
760		TMU=.5*(MU(IJP)+MU(IJ)) \$ RET=.5*(RE(IJP)+RE(IJ))	RICE8	1187
772	4618	IF(FL(IJP).EQ.1)GO TO 4620	RICE8	1188
776		IF(FL(IJP).EQ.5)GO TO 4624	RICE8	1189
1001		IF(FL(IJP).EQ.8)GO TO 4624	RICE8	1190
1004		IF(FL(IJP).EQ.9)GO TO 4624	RICE8	1191
1707		VTT=-VT \$ GO TO 4626	RICE8	1192
1011	4620	VTT=V(IJP) \$ GO TO 4626	RICE8	1193
1015	4624	VTT=VT	RICE8	1194
1017	4626	IF(FL(IJP).EQ. 8)GO TO 4628	RICE8	1195
1023		IF(FL(IJP).EQ.12)GO TO 4628	RICE8	1196
1026	4627	URZTR=U(IJP)	RICE8	1197
1031		URRTR=U(IJP) \$ GO TO 4635	RICE8	1198
1034	4628	IF(FL(IJP).EQ.1)GO TO 4627	RICE8	1199
1040		IF(FL(IJP).EQ.8)GO TO 4632	RICE8	1200
1043		URZTR=-U(IJ) \$ URRTR=-U(IMJP) \$ GO TO 4635	RICE8	1201
1051	4632	URZTR=U(IJ) \$ URRTR=U(IMJP)	RICE8	1202
1057	4635	IF(FL(IJP).EQ. 9)GO TO 4637	RICE8	1203
1063		IF(FL(IJP).EQ. 3)GO TO 4637	RICE8	1204
1066	4636	URRTL=U(IMJP) \$ URZTL=U(IMJP) \$ GO TO 4645	RICE8	1205
1074	4637	IF(FL(IMJP).EQ.1)GO TO 4636	RICE8	1206
1100		IF(FL(IJP).EQ.9)GO TO 4642	RICE8	1207
1103		URZTL=-U(IMJ) \$ URRTL=-U(IJP) \$ GO TO 4645	RICE8	1208
1111	4642	URZTL=U(IMJ) \$ URRTL=U(IJP)	RICE8	1209
1117	4645	NFL=FL(IPJ) \$ GO TO(4648,4649,4649,4649,4647,4648,4648,4649, 14649,4648,4648,4649,4649,4649)NFL	RICE8	1210
1142	4647	IF(FL(IPJP).EQ.2)GO TO 4655	RICE8	1211
1146		IF(FL(IPJP).EQ.3)GO TO 4653	RICE8	1212
1151	4648	VTR=V(IPJ) \$ GO TO 4656	RICE8	1213
1155	4649	IF(FL(IPJP).EQ.1)GO TO 4648	RICE8	1214
1161		IF(FL(IPJP).EQ.4)GO TO 4655	RICE8	1215
1164		IF(FL(IPJ).EQ. 2)GO TO 4655	RICE8	1216
1167		IF(FL(IPJ).EQ. 8)GO TO 4655	RICE8	1217
1172		IF(FL(IPJ).EQ. 9)GO TO 4655	RICE8	1218
1175		IF(FL(IPJ).EQ.4)GO TO 4655	RICE8	1219
1200	4653	VTR=-VT \$ GO TO 4656	RICE8	1220
1202	4655	VTR=VT \$ GO TO 4656	RICE8	1221
1204	4656	NFL=FL(IMJ) \$ GO TO(4659,4661,4661,4659,4657,4659,4659,4661, 14661,4659,4659,4661,4661)NFL	RICE8	1222
1227	4657	IF(U(IMJ).NE.0.)GO TO 4659	RICE8	1223
1232	4658	IF(FL(IMJP).EQ.2)GO TO 4667	RICE8	1224
1236		IF(FL(IMJP).EQ.3)GO TO 4669	RICE8	1225
1241	4659	VTL=V(IMJ) \$ GO TO 4670	RICE8	1226
1245	4661	IF(FL(IMJP).EQ.1)GO TO 4659	RICE8	1227
1251		IF(FL(IMJ).EQ. 3)GO TO 4669	RICE8	1228
1254		IF(FL(IMJ).EQ.12)GO TO 4669	RICE8	1229
1257		IF(FL(IMJ).EQ.13)GO TO 4669	RICE8	1230
1262	4667	VTL=VT \$ GO TO 4670	RICE8	1231
1264	4669	VTL=-VT \$ GO TO 4670	RICE8	1232
1266	4670	IF(FL(IJ).EQ. 1)GO TO 4672	RICE8	1233
1272		IF(FL(IJ).EQ. 6)GO TO 4672	RICE8	1234
1275		IF(FL(IJ).EQ.10)GO TO 4672	RICE8	1235
1300		IF(FL(IPJ).EQ.1)GO TO 4672	RICE8	1236
1303		IF(FL(IJ).EQ.7)GO TO 4674	RICE8	1237

1306	URZR=-U(IJ) \$ URR=-U(IMJ) \$ GO TO 4675	RICE8	1240
1314	4672 URZR=U(IJ) \$ URR=U(IJ) \$ GO TO 4675	RICE8	1241
1322	4674 URZR=U(IJ) \$ URR=U(IMJ)	RICE8	1242
1330	4675 IF(FL(IJ).EQ. 1)GO TO 4677	RICE8	1243
1334	IF(FL(IJ).EQ. 7)GO TO 4677	RICE8	1244
1337	IF(FL(IJ).EQ.11)GO TO 4677	RICE8	1245
1342	IF(FL(IMJ).EQ. 1)GO TO 4677	RICE8	1246
1345	IF(FL(IJ).EQ.6)GO TO 4680	RICE8	1247
1350	URZL=-U(IMJ) \$ URRL=-U(IJ) \$ GO TO 4682	RICE8	1248
1356	4677 URZL=U(IMJ) \$ URRL=U(IMJ) \$ GO TO 4682	RICE8	1249
1364	4680 URZL=U(IMJ) \$ URRL=U(IJ)	RICE8	1250
1372	4682 IF(FL(IJ).EQ. 1) GO TO 4684	RICE8	1251
1376	IF(FL(IMJ).EQ. 1)GO TO 4684	RICE8	1252
1401	IF(FL(IJ).EQ.6)GO TO 4690	RICE8	1253
1404	IF(FL(IJ).EQ.7)GO TO 4690	RICE8	1254
1407	VB=-V(IJ) \$ GO TO 4695	RICE8	1255
1412	4684 VB=V(IMJ) \$ GO TO 4695	RICE8	1256
1416	4690 VB=V(IJ)	RICE8	1257
1424	4695 SRRT=TMU*(DDY*(VTI-VB)+ALA*.5*(DDY/RJ2(IJ)*(RJ1(IJ)+1)*(VTI+VTI- IRJ(IJ)*(VT+VB))+DDX*(URRTR+URR-URRTL-URRL))	RICE8	1258
1450	SRZT=.5*TMU*(DDX*(VTR-VTL)+DDY*(URZTR+URZTL-URZR-URZL))	RICE8	1260
1461	UT=.25*(URZTR+URZTL+URZL+URZR)	RICE8	1261
	C**** ENERGY-DENSITY FLUX ACROSS TOP BOUNDARY=TRET	RICE8	1262
	C	RICE8	1263
1465	TRET=VT*(RET+PT-SRRT)-SRZT*UT-BIE*TMU*DDY*DIT	RICE8	1264
1476	4705 IF(FL(IJ).EQ. 1)GO TO 4707	RICE8	1265
1502	NFL=FL(IJ)-5	RICE8	1266
1504	GO TO(4709,4707,4707,4709,4709,4707,4707,4709)NFL	RICE8	1267
1517	4707 NFL=FL(IMJ) \$ GO TO(4755,4709,4709,4709,4712,4755,4709,4709, 14755,4755,4709,4709,4755)NFL	RICE8	1268
1542	4709 TREL=0. \$ GO TO 4755	RICE8	1270
1544	4712 IF(U(IMJ).EQ.0.)GO TO 4709	RICE8	1271
1547	UL=U(IMJ)	RICE8	1272
1551	DIL=2.*(SIE(IJ)-SIE(IMJ))	RICE8	1273
1555	PL=PB(IMJ)	RICE8	1274
1560	XMUL=MU(IMJ) \$ REL=RE(IMJ) \$ ULL=U(IMJ)	RICE8	1275
1566	VTL=V(IMJ) \$ VBL=V(IMJ)	RICE8	1276
1572	IF(FL(IJ).EQ. 2)GO TO 4716	RICE8	1277
1576	IF(FL(IJ).EQ. 6)GO TO 4716	RICE8	1278
1601	IF(FL(IJ).EQ. 9)GO TO 4716	RICE8	1279
1604	IF(FL(IJ).EQ. 3)GO TO 4718	RICE8	1280
1607	IF(FL(IJ).EQ. 10)GO TO 4718	RICE8	1281
1612	IF(FL(IJ).EQ. 13)GO TO 4718	RICE8	1282
1615	UTL=U(IMJ) \$ GO TO 4720	RICE8	1283
1620	4716 UTL=UL \$ GO TO 4720	RICE8	1284
1622	4718 UTL=-UL	RICE8	1285
1624	4720 IF(FL(IMJ).EQ. 2)GO TO 4722	RICE8	1286
1630	IF(FL(IMJ).EQ. 6)GO TO 4722	RICE8	1287
1633	IF(FL(IMJ).EQ. 9)GO TO 4722	RICE8	1288
1636	IF(FL(IMJ).EQ. 3)GO TO 4724	RICE8	1289
1641	IF(FL(IMJ).EQ. 10)GO TO 4724	RICE8	1290
1644	IF(FL(IMJ).EQ. 13)GO TO 4724	RICE8	1291
1647	UBL=U(IMJ) \$ GO TO 4730	RICE8	1292
1652	4722 UBL=UL \$ GO TO 4730	RICE8	1293
1654	4724 UBL=-UL	RICE8	1294


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1656 4730 IF(FL(IJ).EQ.1)GO TO 4732 RICEB 1295
1662 IF(FL(IJ).EQ.7)GO TO 4734 RICEB 1296
1665 IF(FL(IJ).EQ.8)GO TO 4734 RICEB 1297
1670 UR=-U(IMJ) $ GO TO 4736 RICEB 1298
1673 4732 UR=U(IJ) $ GO TO 4736 RICEB 1299
1677 4734 UR=U(IMJ) RICEB 1300
1702 4736 IF(FL(IJ).EQ. 7)GO TO 4738 RICEB 1301
1706 IF(FL(IJ).EQ.11)GO TO 4740 RICEB 1302
17.1 VZB=V(IJ) $ VRB=V(IJ) $ GO TO 4742 RICEB 1303
1716 4738 VZB=V(IJ) $ VRB=V(IMJ) $ GO TO 4742 RICEB 1304
1724 4740 VZB=-V(IJ) $ VRB=-V(IMJ) RICEB 1305
1732 4742 IF(FL(IJ).EQ. 8)GO TO 4744 RICEB 1306
1736 IF(FL(IJ).EQ.12)GO TO 4746 RICEB 1307
1741 VZZT=V(IJ) $ VRZT=V(IJ) $ GO TO 4750 RICEB 1308
1745 4744 VZZT=V(IJ) $ VRZT=V(IMJ) $ GO TO 4750 RICEB 1309
1753 4746 VZZT=-V(IJ) $ VRZT=-V(IMJ) RICEB 1310
1764 4750 SZL=XMUL*.5*(12.+ALA)*DDX*(UR-ULL)+ALA*DDY/RJ(J)*(RJ2(J)*
I(VZZT+VTL)-RJ2(J-1)*(VZB+VBL)) RICEB 1311
2006 SRZL=.5*XMUL*(DDX*(VRZT+VRZB-VTL-VBL)+DDY*(UTL-UJBL)) RICEB 1313
2017 VL=.25*(VRZT+VRZB+VTL+VBL) RICEB 1314
C**** ENERGY-DENSITY FLUX ACROSS LEFT BOUNDARY=TREL . . . . . RICEB 1315
C RICEB 1316
2022 TREL=UL*(REL+PL-SZL)-SRZL*VL-BIE*XMUL*DIL*DDX RICEB 1317
2034 4755 IF(FL(IMJ).EQ.2)GO TO 4757 RICEB 1318
2040 IF(FL(IMJ).EQ.3)GO TO 4757 RICEB 1319
2043 IF(FL(IMJ).EQ.5)GO TO 4757 RICEB 1320
2046 GO TO 4760 RICEB 1321
2046 4757 STREB(1)=0. RICEB 1322
2051 4760 CONTINUE RICEB 1323
C**** RICEB 1324
C**** RE(IJ) CALC.COMPLETE RICEB 1325
C RICEB 1326
2054 4805 RE(IJ)= RE(IJ)+DT*(DDY/RJ(J)*(RJ2(J-1)*STREB(1)-RJ2(J)*TRET)+
IDDX*(TREL-TREB)) RICEB 1327
2072 STREB(1)=TRET RICEB 1328
C RICEB 1329
C RICEB 1330
C**** SETS TOP FLUX QUANTITY INTO BOTTOM AND RIGHT FLUX QUANTITY INTO RICEB 1331
C**** LEFT TO AVOID CALCULATING OVER AGAIN RICEB 1332
C RICEB 1333
2075 TREL=TREB RICEB 1334
2076 4850 CONTINUE RICEB 1335
2103 JC=0 RICEB 1336
2104 DO 4950 J=2,JB1 RICEB 1337
2105 JC=JC+1B2 RICEB 1338
2106 DO 4950 I=2,IB1 RICEB 1339
2110 IJ=I+JC RICEB 1340
2111 IF(FL(IJ).GT.1.AND.FL(IJ).LT.6)GO TO 4950 RICEB 1341
2124 IMJ=IJ-1 RICEB 1342
2125 IJM=IJ-1B2 RICEB 1343
C RICEB 1344
C**** OBTAINS INTERNAL ENERGY FROM TOTAL ENERGY-DENSITY RICEB 1345
C RICEB 1346
2126 EN=RE(IJ)/RHO(IJ) RICEB 1347
2132 IF(FL(IJ).EQ.1)GO TO 4905 RICEB 1348
2135 NFL=FL(IJ)-5 $ GO TO(4908,4910,4910,4908,4908,4910,4910,4908)NFL RICEB 1349

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2153	4905	XKE=.25*(U(IJ)+U(IMJ))**2 \$ GO TO 4915	RICE8	1350
2162	4908	XKE=U(IJ)**2 \$ GO TO 4915	RICE8	1351
2166	4910	XKE=U(IMJ)**2	RICE8	1352
2171	4915	IF(FL(IJ).EQ.)GO TO 4917	RICE8	1353
2175		NFL=FL(IJ)-5 \$ GO TO(4919,4919,4921,4921,4919,4919,4921,4921)NFL	RICE8	1354
2212	4917	YKE=.25*(V(IJ)+V(IJM))**2 \$ GO TO 4925	RICE8	1355
2221	4919	YKE=V(IJ)**2 \$ GO TO 4925	RICE8	1356
2225	4921	YKE=V(IJM)**2	RICE8	1357
2230	4925	SIE(IJ)=EN-.5*(XKE+YKE)	RICE8	1358
2236	4950	CONTINUE	RICE8	1359
2243		DO 4953 J=2,JB2	RICE8	1360
2245		IBJ=IB2*(J-1)+1B	RICE8	1361
2251		IB1J=IBJ+1	RICE8	1362
2251		IB2J=IBJ+2	RICE8	1363
2253		IB1JM=IB1J-IB2	RICE8	1364
2254		IF(FL(IB2J).NE.4)GO TO 4953	RICE8	1365
	C		RICE8	1366
	C****	SETS SIE AND RE CONST.AT OUTFLOW BOUNDARY	RICE8	1367
	C****	ENERGY CHANGE TO RE(IB1,J) DOES NOT CONTAIN KINETIC ENERGY AS SPEC	RICE8	1368
	C****	CALC. ONLY CHANGES INTERNAL ENERGY	RICE8	1369
	C		RICE8	1370
2260		SIE(IB2J)=SIE(IB1J)=SIE(IBJ)	RICE8	1371
2267		RE(IB1J)=RHO(IB1J)*(SIE(IB1J)+.125*(U(IB1J)+U(IBJ))**2+ I (V(IB1J)+V(IB1JM))**2))	RICE8	1372
			RICE8	1373
2304		RE(IB2J)=RE(IB1J)	RICE8	1374
2307	4953	CONTINUE	RICE8	1375
2312		RETURN \$ END	RICE8	1376
	C		RICE8	1377
	C		RICE8	1378
	C****	END OF THE SUBROUTINE ENERGY	RICE8	1379
	C		RICE8	1380
	C		RICE8	1381

	SUBROUTINE SPEC	RICE8	1382
1	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASO	RCOM2	4
1	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECREO,DDX,DDY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,X1,IT	RCOM2	6
1	COMMON/INFLD/FLO(12),UO,VO,VINT1,INT2,UINL1,UINL2,RHO0,RINT1,	RCOM2	7
	IRINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIE1,SIE2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
1	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
1	COMMON/SPEC/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
1	COMMON/OBSD/I10(20),NS0(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FARO(7,20)	RCOM2	16
1	INTEGER AM,BM	RCOM2	17
1	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
1	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHO(62, 32),RHOU(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CO(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
1	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	31
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
1	EQUVALENCE (RHOU,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
1	INTEGER FL,CYCLE	RCOM2	34
1	REAL MU	RCOM2	35
1	DIMENSION OMEGA(3),RM(7)	RICE8	1384
1	DIMENSION DRHO(7),DRHOR(7),DRHOL(7),DRHOT(7),DRHOP(7)	RICE8	1385
	1,RHO1(7),RHO2(7),FAL(7),FAR(7),FAT(7)	RICE8	1386
1	REAL KF,KB	RICE8	1387
1	DIMENSION SUMB(100)	RICE8	1388
1	DO 5002 K=1,NSPEC	RICE8	1389
3	IF(SMI(K).GT.0.)RM(K)=1./SMI(K)	RICE8	1390
7	5002 IF(SMI(K).LE.0.)RM(K)=0.	RICE8	1391
16	5000 NSP=NSPEC-1	RICE8	1392
20	JC=0	RICE8	1393
	C	RICE8	1394
	C**** START SPECIES DENSITY-(FA) CALC.	RICE8	1395
	C**** START OF SPECIES CONVECTION CALCULATION	RICE8	1396
	C	RICE8	1397
21	DO 5200 J=2,JB1	RICE8	1398
22	JC=JC+IB2	RICE8	1399
23	DO 5200 I=2,IB1	RICE8	1400
25	IJ=I*JC	RICE8	1401
26	IPJ=IJ+1	RICE8	1402
27	IMJ=IJ-1	RICE8	1403

30	IJP=IJ+182	RICE8	1404
32	IJM=IJ-182	RICE8	1405
32	IMJM=IJM-1	RICE8	1406
33	IPJM=IJM+1	RICE8	1407
34	IMJP=IJP-1	RICE8	1408
36	IPJP=IJP+1	RICE8	1409
37	NFL=FL(IJ) \$ GO TO(5005,5200,5200,5200,5200,5010,5020,5020,5010, 15015,5020,5020,5015)NFL	RICE8	1410
		RICE8	1411
62	5005 UL=U(IMJ) \$ GO TO 5025	RICE8	1412
66	5010 UL=U(IJ) \$ GO TO 5025	RICE8	1413
72	5015 UL=-U(IJ) \$ GO TO 5025	RICE8	1414
76	5020 DO 5021 K=1,NSP	RICE8	1415
103	5021 FAR(K)=0.	RICE8	1416
105	GO TO 5065	RICE8	1417
105	5025 NFL=FL(IPJ) \$ GO TO(5030,5020,5020,5045,5020,5020,5035,5035,5020 1,5020,5040,5040,5020)NFL	RICE8	1418
		RICE8	1419
130	5030 UR=U(IPJ) \$ GO TO 5050	RICE8	1420
134	5035 UR=U(IJ) \$ GO TO 5050	RICE8	1421
140	5040 UR=-U(IJ) \$ GO TO 5050	RICE8	1422
144	5045 DO 5046 K=1,NSP	RICE8	1423
161	KZ=182*JB2*(K-1)	RICE8	1424
163	IJK=IJ+KZ	RICE8	1425
164	5046 FAR(K)=2.*FA(IJK)*U(IJ)	RICE8	1426
173	GO TO 5065	RICE8	1427
173	5050 TAUTE=0.125*DX*(UR-UL)	RICE8	1428
177	IF(TAUTE.LT.0.) GO TO 5055	RICE8	1429
200	TAUR=(1.+X1)*TAUTE \$ GO TO 5060	RICE8	1430
203	5055 TAUR=(1.-X1)*TAUTE	RICE8	1431
206	5060 DO 5061 K=1,NSP	RICE8	1432
230	KZ=182*JB2*(K-1)	RICE8	1433
232	IJK=IJ+KZ	RICE8	1434
233	IPJK=IJK+1	RICE8	1435
234	5061 FAR(K)=(FA(IPJK)+FA(IJK)-DT*DDX*(FA(IPJK)-FA(IJK))*U(IJ))* IU(IJ)-2.*DDX*TAUR*(FA(IPJK)-FA(IJK))	RICE8	1436
		RICE8	1437
251	5065 IF(FL(IJ).EQ.1)GO TO 5070	RICE8	1438
255	NFL=FL(IJ)-5 \$ GO TO(5075,5075,5085,5085,5080,5080,5085,5085)NFL	RICE8	1439
272	5070 VB=V(IJM) \$ GO TO 5090	RICE8	1440
276	5075 VB=V(IJ) \$ GO TO 5090	RICE8	1441
302	5080 VB=-V(IJ) \$ GO TO 5090	RICE8	1442
306	5085 DO 5086 K=1,NSP	RICE8	1443
313	5086 FAT(K)=0.	RICE8	1444
315	GO TO 5140	RICE8	1445
315	5090 NFL=FL(IJP) \$ GO TO(5095,5085,5085,5085,5125,5085,5085,5100,5100 1,5085,5085,5105,5105)NFL	RICE8	1446
		RICE8	1447
340	5095 VT=V(IJP) \$ GO TO 5110	RICE8	1448
344	5100 VT=V(IJ) \$ GO TO 5110	RICE8	1449
350	5105 VT=-V(IJ)	RICE8	1450
353	5110 TAUTE=.125*DY*(VT*RJ2(J+1)-VB*RJ2(J-1))/RJ2(J)	RICE8	1451
364	IF(TAUTE.LT.0.)GO TO 5115	RICE8	1452
366	TAUT=(1.+X1)*TAUTE \$ GO TO 5120	RICE8	1453
371	5115 TAUT=(1.-X1)*TAUTE	RICE8	1454
374	5120 DO 5121 K=1,NSP	RICE8	1455
421	KZ=182*JB2*(K-1)	RICE8	1456
423	IJK=IJ+KZ	RICE8	1457
424	IPJK=IJK+182	RICE8	1458

425	5121	FAT(K)=((FA(IJPK)+FA(IJK)-DT*DDY*(FA(IJPK)-FA(IJK))*V(IJ))	RICE8	1459
		1*V(IJ)-2.*DDY*TAUT*(FA(IJPK)-FA(IJK)))*RJ2(J)	RICE8	1460
443		GO TO 5140	RICE8	1461
443	5125	IF(V(IJ).EQ.0.) GO TO 5085	RICE8	1462
446		TAUTE=.125*DY*(V(IJ)*RJ2(J)-VB*RJ2(J-1))/RJ2(J)	RICE8	1463
457		IF(TAUTE.LT.0.) GO TO 5130	RICE8	1464
460		TAUT=(1.+X1)*TAUTE \$ GO TO 5135	RICE8	1465
463	5130	TAUT=(1.-X1)*TAUTE	RICE8	1466
466	5135	DO 5136 K=1,NSP	RICE8	1467
513		KZ=IB2*JB2*(K-1)	RICE8	1468
515		IJK=IJ+KZ	RICE8	1469
516		IJPK=IJK+IB2	RICE8	1470
517	5136	FAT(K)=((FA(IJPK)-DT*DDY*(FA(IJPK)-FA(IJK))*V(IJ))*V(IJ)	RICE8	1471
		1-2.*DDY*TAUT*(FA(IJPK)-FA(IJK)))*2.*RJ2(J)	RICE8	1472
536	5140	IF(FL(IJ).EQ.1) GO TO 5150	RICE8	1473
542		NFL=FL(IJ)-5 \$ GO TO(5145,5150,5150,5145,5145,5150,5150,5145)NFL	RICE8	1474
557	5145	DO 5146 K=1,NSP	RICE8	1475
564	5146	FAL(K)=0.	RICE8	1476
566		GO TO 5170	RICE8	1477
566	5150	NFL=FL(IMJ) \$ GO TO(5170,5145,5145,5145,5155,5170,5145,5145,5170	RICE8	1478
		1,5170,5145,5145,5170)NFL	RICE8	1479
611	5155	IF(U(IMJ).EQ.0.)GO TO 5145	RICE8	1480
614		TAUTE=0.125*DX*(U(IJ)-U(IMJ))	RICE8	1481
621		IF(TAUTE.LT.0.) GO TO 5160	RICE8	1482
623		TAUL=(1.+X1)*TAUTE \$ GO TO 5165	RICE8	1483
626	5160	TAUL=(1.-X1)*TAUTE	RICE8	1484
631	5165	DO 5166 K=1,NSP	RICE8	1485
653		KZ=IB2*JB2*(K-1)	RICE8	1486
655		IJK=IJ+KZ	RICE8	1487
656		IMJK=IJK-1	RICE8	1488
657	5166	FAL(K)=2.*(FA(IMJK)-DT*DDX*(FA(IJK)-FA(IMJK))*U(IMJ))	RICE8	1489
		IU(IMJ)-2.*DDX*TAUL*(FA(IJK)-FA(IMJK)))	RICE8	1490
674	5170	IF(FL(IJ).EQ.1) GO TO 5180	RICE8	1491
700		NFL=FL(IJ)-5 \$ GO TO(5175,5175,5180,5180,5175,5175,5180,5180)NFL	RICE8	1492
715	5175	DO 5176 K=1,NSP	RICE8	1493
724	5176	TFAB(1,K)=0.	RICE8	1494
727		GO TO 5185	RICE8	1495
727	5180	NFL=FL(IJM) \$ GO TO(5185,5175,5175,5175,5175,5185,5185,5175,5175	RICE8	1496
		1,5185,5185,5175,5175)NFL	RICE8	1497
752	5185	CONTINUE	RICE8	1498
752		SUMR=0.	RICE8	1499
753		DO 5186 K=1,NSP	RICE8	1500
774		KZ=IB2*JB2*(K-1)	RICE8	1501
777		IJK=IJ+KZ	RICE8	1502
1000		FA(IJK)=FA(IJK)+0.5*DT*(DDY/RJ(J)*(TFAB(1,K)-FAT(K))+DDX*	RICE8	1503
		(FAL(K)-FAR(K)))	RICE8	1504
1012		FAL(K)=FAR(K)	RICE8	1505
1013		TFAB(1,K)=FAT(K)	RICE8	1506
1015	5186	SUMR=SUMR+FA(IJK)	RICE8	1507
1023		IJNS=IB2*JB2*NSP+IJ	RICE8	1508
1026		FA(IJNS)=RHO(IJ)-SUMR	RICE8	1509
1033	5200	CONTINUE	RICE8	1510
	C		RICE8	1511
	C***	ALL SPECIES DENSITY CHANGES DUE TO CONVECTION,ADDED TO-FA-ARRAY	RICE8	1512
	C		RICE8	1513

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C***** START OF SPECIES DIFFUSION CALCULATION
C
1040      JC=0                                RICE8  1514
1041      DO 5198 J=2,JBI                     RICE8  1515
1042      JC=JC+182                           RICE8  1516
1043      DO 5198 I=2,181                     RICE8  1517
1044      IJ=I+JC                             RICE8  1518
1045      IF (FL(IJ).GT.1.AND.FL(IJ).LT.6) GO TO 5198 RICE8  1519
1046      SUM1=0.                             RICE8  1520
1060      SUM2=0.                             RICE8  1521
1061      DO 5196 K=1,NSPEC                   RICE8  1522
1063      IF (FA(I,J,K).LE.0.160 TO 5196     RICE8  1523
1074      SUM1=SUM1+FA(I,J,K)*CV(K)*GAMA(K)  RICE8  1524
1100      SUM2=SUM2+FA(I,J,K)*CV(K)         RICE8  1525
1102      5196 CONTINUE                       RICE8  1526
1106      TE(IJ)=RHO(IJ)*SIE(IJ)/SUM2       RICE8  1527
1112      TE1J=TE(IJ)                        RICE8  1528
1114      ETA(IJ)=ETA0*SQRT(TE1J)/(SUM1-SUM2) RICE8  1529
1124      5198 CONTINUE                       RICE8  1530
1131      DO 5193 I=1,182                     RICE8  1531
1136      5193 SUMB(I)=0.                    RICE8  1532
1140      JC=0                                RICE8  1533
1141      DO 5400 J=2,JBI                     RICE8  1534
1142      SUML=0.                             RICE8  1535
1142      JC=JC+182                           RICE8  1536
1144      DO 5400 I=2,181                     RICE8  1537
1146      IJ=I+JC                             RICE8  1538
1147      IF (FL(IJ).GT.1.AND.FL(IJ).LT.6) GO TO 5400 RICE8  1539
1161      IPJ=IJ+1                            RICE8  1540
1161      IMJ=IJ-1                            RICE8  1541
1162      IJP=IJ+182                          RICE8  1542
1164      IJM=IJ-182                          RICE8  1543
1164      IMJM=IJM-1                          RICE8  1544
1165      IPJM=IJM+1                          RICE8  1545
1166      IMJP=IJP-1                          RICE8  1546
1170      IPJP=IJP+1                          RICE8  1547
C
C*****FLUX ACROSS CELL RIGHT BOUNDARY
1170      IF (FL(IJ).EQ.1) GO TO 5209        RICE8  1550
1173      NFL=FL(IJ)-5 $ GO TO(5209,5203,5203,5209,5209,5203,5203,5209)NFL RICE8  1551
1211      5203 DO 5206 K=1,NSPEC              RICE8  1552
1213      5206 DRHOR(K)=0. $ GO TO 5219      RICE8  1553
1217      5209 NFL=FL(IPJ) $ GO TO(5212,5203,5203,5203,5203,5203,5212,5212, RICE8  1554
1242      5212 DO 5213 K=1,NSPEC              RICE8  1555
1264      KZ=182*JB2*(K-1)                   RICE8  1556
1266      IJK=IJ+KZ                           RICE8  1557
1267      IPJK=IJK+1                          RICE8  1558
1270      RHO1(K)=FA(IJK)/RHO(IJ)            RICE8  1559
1274      RHO2(K)=FA(IPJK)/RHO(IPJ)         RICE8  1560
1277      5213 DRHOP(K)=(RHO2(K)-RHO1(K))*5*(RHO(IJ)+RHO(IPJ)) RICE8  1561
1303      ASSIGN 5215 TO JRET $ GO TO 5233   RICE8  1562
1305      5215 DO 5218 K=1,NSPEC             RICE8  1563
1323      5218 DRHOR(K)=.5*DDX*DRHO(K)*(ETA(IPJ)+ETA(IJ)) RICE8  1564
C

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	C*****FLUX ACROSS CELL TOP BOUNDARY	RICE8	1569
1325	5219 IF (FL(IJ).EQ.1)GO TO 5221 \$ NFL=FL(IJ)-5	RICE8	1570
1333	GO TO(5221,5221,5224,5224,5221,5221,5224,5224)NFL	RICE8	1571
1346	5221 NFL=FL(IJP) \$ GO TO(5231,5224,5224,5224,5224,5224,5224,5231,5231,5224,5224,5231,5231)NFL	RICE8	1572
1371	5224 DO 5225 K=1,NSPEC	RICE8	1574
1373	5225 DRHOT(K)=0. \$ GO TO 5263	RICE8	1575
1377	5231 DO 5232 K=1,NSPEC	RICE8	1576
1421	KZ=I82*JB2*(K-1)	RICE8	1577
1423	IJK=IJ+KZ	RICE8	1578
1424	IJPK=IJK+I82	RICE8	1579
1426	RHO1(K)=FA(IJK)/RHO(IJ)	RICE8	1580
1432	RHO2(K)=FA(IJPK)/RHO(IJP)	RICE8	1581
1435	5232 DRHOP(K)=(RHO2(K)-RHO1(K))*5*(RHO(IJ)+RHO(IJP))	RICE8	1582
1441	ASSIGN 5257 TO JRET	RICE8	1583
1442	5233 SDR=0. \$ SDP=0. \$ SDM=0.	RICE8	1584
1444	DO 5242 K=1,NSPEC	RICE8	1585
1446	DRHO(K)=ALPHA(K)*DRHOP(K)	RICE8	1586
1450	IF (DRHO(K).LT.0.)GO TO 5236	RICE8	1587
1452	SDP=SDP+DRHO(K) \$ GO TO 5242	RICE8	1588
1454	5236 CONTINUE	RICE8	1589
1454	SDM=SDM+DRHO(K) \$ GO TO 5242	RICE8	1590
1457	5242 SDR=SDR+DRHO(K)	RICE8	1591
1464	IF (SDR)5245,5254,5250	RICE8	1592
1465	5245 DO 5248 K=1,NSPEC	RICE8	1593
1467	IF (SDM.EQ.0.)GO TO 5248	RICE8	1594
1470	IF (DRHO(K).GE.0.)GO TO 5248	RICE8	1595
1472	DRHO(K)=DRHO(K)-DRHO(K)*SDR/SDM	RICE8	1596
1474	5248 CONTINUE \$ GO TO 5254	RICE8	1597
1477	5250 DO 5251 K=1,NSPEC	RICE8	1598
1501	IF (SDP.EQ.0.)GO TO 5251	RICE8	1599
1502	IF (DRHO(K).LE.0.)GO TO 5251	RICE8	1600
1504	DRHO(K)=DRHO(K)-DRHO(K)*SDR/SDP	RICE8	1601
1506	5251 CONTINUE \$ GO TO 5254	RICE8	1602
1511	5254 GO TO JRET	RICE8	1603
1514	5257 DO 5260 K=1,NSPEC	RICE8	1604
1533	5260 DRHOT(K)=.5*DDY*(ETA(IJ)+ETA(IJP))*RJ2(J)*DRHO(K)	RICE8	1605
	C	RICE8	1606
	C*****FLUX ACROSS CELL LEFT BOUNDARY	RICE8	1607
1535	5263 IF (FL(IJ).EQ.1)GO TO 5269 \$ NFL=FL(IJ)-5	RICE8	1608
1543	GO TO(5266,5269,5269,5266,5266,5269,5269,5266,5266)NFL	RICE8	1609
1556	5266 DO 5267 K=1,NSPEC	RICE8	1610
1560	5267 DRHOL(K)=0. \$ GO TO 5283	RICE8	1611
1564	5269 NFL=FL(IMJ) \$ GO TO(5283,5266,5266,5266,5266,5283,5266,5266,5283,5283,5266,5266,5283)NFL	RICE8	1612
	C	RICE8	1613
	C*****FLUX ACROSS CELL BOTTOM BOUNDARY	RICE8	1614
1607	5283 IF (FL(IJM).GT.1.AND.FL(IJM).LE.5)GO TO 5288	RICE8	1615
1622	GO TO 5292	RICE8	1616
1622	5288 DO 5289 K=1,NSPEC	RICE8	1617
1624	[K=I82*(K-1)+1	RICE8	1618
1627	5289 DRHOB(K)=0. \$ GO TO 5292	RICE8	1619
1635	5292 CONTINUE	RICE8	1620
1635	DO 5295 K=1,NSPEC	RICE8	1621
1653	IJK=IJ+I82*JB2*(K-1)	RICE8	1622
		RICE8	1623

2254	5354	ROMREF=(FA(I,J,KALPHA)*RM(KALPHA)+DTC*AM(KALPHA,L)*KB*PP)/ I(I.+DTC*AM(KALPHA,L)*SM(KALPHA)*KF*RP/FA(I,J,KALPHA))	RICE6	1734
			RICE8	1735
2277		GO TO 5365	RICE8	1736
2300	5355	CONTINUE	RICE8	1737
	C****	FINDS THE MINIMUM CONCENTRATION WHICH WILL BE THE REFERENCE SPECIE	RICE8	1738
	C****	FOR THE BACKWARD REACTION	RICE8	1739
2300		KN1=0	RICE8	1740
2301		DO 5358 K=1,NSPEC	RICE8	1741
2303		KLB=LB+K	RICE8	1742
2304		IF(BM(KLB).EQ.0)GO TO 5358	RICE8	1743
2306		IJK=I+IB2*JB2*(K-1)	RICE8	1744
2312		ROM=FA(IJK)*RM(K)/BM(KLB)	RICE8	1745
2320		IF(ROM.LE.EP(K))GO TO 5375	RICE8	1746
2323		IF(BM(KLB).EQ.AM(KLB))GO TO 5358	RICE8	1747
2326		KN1=KN1+1	RICE8	1748
2327		IF(KN1.EQ.1)RMIN=ROM	RICE8	1749
2332		IF(KN1.EQ.1)KALPHA=K	RICE8	1750
2335		IF(KN1.EQ.1)GO TO 5358	RICE8	1751
2336		IF(ROM.LT.RMIN)KALPHA=K	RICE8	1752
2342		IF(ROM.LT.RMIN)RMIN=ROM	RICE8	1753
2345	5356	CONTINUE	RICE8	1754
2350	5359	ROMREF=(FA(I,J,KALPHA)*RM(KALPHA)+DTC*BM(KALPHA,L)*KF*RP)/ I(I.+DTC*BM(KALPHA,L)*SM(KALPHA)*KB*PP/FA(I,J,KALPHA))	RICE8	1755
			RICE8	1756
2373	5365	OMEGA(L)=(ROMREF-FA(I,J,KALPHA)*RM(KALPHA))/(BM(KALPHA,L)- IAM(KALPHA,L))	RICE8	1757
			RICE8	1758
2412	5375	CONTINUE	RICE8	1759
2415		DO 5385 K=1,NSPEC	RICE8	1760
2416		BMA=0.	RICE8	1761
2417		DO 5380 L=1,NR	RICE8	1762
2427	5380	BMA=BMA+(BM(K,L)-AM(K,L))*OMEGA(L)	RICE8	1763
2434		FA(I,J,K)=FA(I,J,K)+SM(K)*BMA	RICE8	1764
2444	5385	CONTINUE	RICE8	1765
2446		DRE=0.	RICE8	1766
2447		DO 5390 L=1,NR	RICE8	1767
2454	5390	DRE=DRE+Q(L)*OMEGA(L)	RICE8	1768
2460		RE(IJ)=RE(IJ)+DRE	RICE8	1769
2462		SIE(IJ)=SIE(IJ)+DRE/RHO(IJ)	RICE8	1770
	C		RICE8	1771
	C****	RE(IJ) AND SIE(IJ) UPDATED TO INCLUDE CHANGES DUE TO CHEMICAL	RICE8	1772
	C****	REACTION	RICE8	1773
	C		RICE8	1774
2467	5395	CONTINUE	RICE8	1775
2472	5400	CONTINUE	RICE8	1776
2477		DO 5404 J=2,JB1	RICE8	1777
2501		IF(FL(IB2,J).NE.4)GO TO 5404	RICE8	1778
2506		DO 5403 K=1,NSPEC	RICE8	1779
2522		FA(IB1,J,K)=FA(IB,J,K)	RICE8	1780
2524	5403	CONTINUE	RICE8	1781
	C		RICE8	1782
	C****	SPECIES DENSITY(FA),RE AND SIE ARE SET CONSTANT AT OUTFLOW BND.	RICE8	1783
	C****	ENERGY CHANGE TO RE(IB1,J) DOES NOT CONTAIN KINETIC ENERGY	RICE8	1784
	C		RICE8	1785
2534		RE(IB1,J)=RE(IB1,J) + RHO(IB,J)*SIE(IB,J) - RHO(IB1,J)*SIE(IB1,J)	RICE8	1786
2545		RE(IB2,J)=RE(IB1,J)	RICE8	1787
2547		SIE(IB2,J)=SIE(IB1,J)=SIE(IB,J)	RICE8	1788

2561	5404	CONTINUE		RICE6	1789
2564		RETURN SEND		RICE8	1790
		C		RICE8	1791
		C		RICE8	1792
		C****	END OF THE SUBROUTINE SPEC	RICE8	1793
		C		RICE8	1794
		C		RICE8	1795

	SUBROUTINE FLIC	RICE8	1796
1	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPLOT(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTG,ALA,BIG,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASO	RCOM2	4
1	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECREQ,DOX,DDY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,XI,IT	RCOM2	6
1	COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,	RCOM2	7
	1RINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIE1,SIE2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
1	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
1	COMMON/SPECD/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
1	COMMON/OBSD/ITO(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FABO(7,20)	RCOM2	16
1	INTEGER AM,BM	RCOM2	17
1	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
1	LCM/CELLD/FL(62, 32),UI(62, 32),VI(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSO(62, 32),RHOT(62, 32),RHOUI(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CG(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
1	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHO(62, 7),STREB(62)	RCOM2	31
1	EQUIVALENCE (RHOU,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1)TFAB,DRHO(RCOM2	33
1	INTEGER FL,CYCLE	RCOM2	34
1	REAL MU	RCOM2	35
1	RAD=DY*JB	RICE8	1798
	C	RICE8	1799
	C**** THIS SUB.SETS CELL FLAGS BASED ON INPUT DATA,THERE ARE 13 TYPES	RICE8	1800
	C	RICE8	1801
3	ZAX=DX*IB	RICE8	1802
6	J2=1 \$J3=5 \$J4=9	RICE8	1803
11	YTS=-.5*DY	RICE8	1804
13	DO 245 J=1,JB2	RICE8	1805
14	XTS=-.5*DX	RICE8	1806
15	YTE=YTS+DY*(J-1)	RICE8	1807
23	DO 245 I=1,IB2	RICE8	1808
26	XTE=XTS+DX*(I-1)	RICE8	1809
	C	RICE8	1810
	C**** SETS EACH CELL FLAG,FL(I,J)=1,CELL FLAG WILL BE CHANGED FOR OTHER	RICE8	1811
	C TYPES	RICE8	1812
32	FL(I,J)=1	RICE8	1813
35	IF(YTE.LT.0.)GO TO 210	RICE8	1814
36	IF(XTE.GT.ZAX)GO TO 220	RICE8	1815
42	IF(YTE.GT.RAD)GO TO 230	RICE8	1816
44	IF(XTE.LT.0.)GO TO 240	RICE8	1817

46	GO TO 245	RICEB	1818
	C*****SETS FLAG FOR BOTTOM ROW	RICEB	1819
	C	RICEB	1820
46	210 IF(NSL(1).EQ.1)GO TO 212	RICEB	1821
50	FL(1,J)=2 \$ GO TO 245	RICEB	1822
55	212 FL(1,J)=3	RICEB	1823
62	GO TO 245	RICEB	1824
	C*****SETS FLAGS FOR RIGHT (1B2) COLUMN	RICEB	1825
	C	RICEB	1826
62	220 IF(YTE.LT.FLO(J2)) GO TO 222	RICEB	1827
65	IF(YTE.LT.FLO(J2+1)) GO TO 228	RICEB	1828
67	J2=J2+2 \$ IF(J2.GT.3)J2=3	RICEB	1829
73	IF(YTE.GT.FLO(J2).AND.YTE.LT.FLO(J2+1))GO TO 228	RICEB	1830
105	222 IF(NSL(2).EQ.1) GO TO 227	RICEB	1831
107	FL(1,J)=2 \$ GO TO 245	RICEB	1832
114	227 FL(1,J)=3 \$ GO TO 245	RICEB	1833
121	228 FL(1,J)=4 \$ GO TO 245	RICEB	1834
	C*****SETS FLAGS FOR TOP (JB2) ROW	RICEB	1835
	C	RICEB	1836
126	230 IF(XTE.LT.FLO(J3)) GO TO 232	RICEB	1837
131	IF(XTE.LT.FLO(J3+1)) GO TO 238	RICEB	1838
133	J3=J3+2 \$ IF(J3.GT.7)J3=7	RICEB	1839
137	IF(YTE.GT.FLO(J3).AND.YTE.LT.FLO(J3+1))GO TO 238	RICEB	1840
151	232 IF(NSL(3).EQ.1) GO TO 237	RICEB	1841
153	FL(1,J)=2 \$ GO TO 245	RICEB	1842
160	237 FL(1,J)=3 \$ GO TO 245	RICEB	1843
165	238 FL(1,J)=5 \$ GO TO 245	RICEB	1844
	C*****SETS FLAGS FOR LEFT COLUMN	RICEB	1845
	C	RICEB	1846
172	240 IF(YTE.LT.FLO(J4)) GO TO 242	RICEB	1847
175	IF(YTE.LT.FLO(J4+1)) GO TO 248	RICEB	1848
177	J4=J4+2 \$ IF(J4.GT.11)J4=11	RICEB	1849
203	IF(YTE.GT.FLO(J4).AND.YTE.LT.FLO(J4+1))GO TO 248	RICEB	1850
215	242 IF(NSL(4).EQ.1) GO TO 247	RICEB	1851
217	FL(1,J)=2 \$ GO TO 245	RICEB	1852
224	247 FL(1,J)=3 \$ GO TO 245	RICEB	1853
231	248 FL(1,J)=5	RICEB	1854
236	245 CONTINUE	RICEB	1855
243	IF(NO.LE.0)RETURN	RICEB	1856
	C	RICEB	1857
	C**** DEFINES OBSTACLE,(IF ANY),CELL FLAGS BASED ON DATA (OB,01B,1TO,NSO	RICEB	1858
	C	RICEB	1859
246	DO 295 K=1,NO	RICEB	1860
250	X1=OB(1,K) \$ X2=OB(2,K) \$ Y1=OB(3,K) \$ Y2=OB(4,K)	RICEB	1861
261	X3=OB(5,K) \$ Y3=OB(6,K)	RICEB	1862
266	YTS=.5*DY	RICEB	1863
271	DO 285 J=2,JB1	RICEB	1864
272	XTS=.5*DX	RICEB	1865
273	YTE=YTS+DY*FLOAT(J-2)	RICEB	1866
300	DO 285 I=2,1B1	RICEB	1867
302	XTE=XTS+DX*FLOAT(I-2)	RICEB	1868
305	IF(XTE.LT.X1) GO TO 285	RICEB	1869
310	IF(XTE.GT.X2) GO TO 285	RICEB	1870
313	IF(YTE.LT.Y1) GO TO 285	RICEB	1871
315	IF(YTE.GT.Y2) GO TO 285	RICEB	1872

320	IF(I10(K).EQ.1)GO TO 250	RICE8	1873
322	IF(I10(K)-3)283,275,270	RICE8	1874
325	250 IYTE=1000.*YTE+.1*DY	RICE8	1875
	C	RICE8	1876
	C**** CELL(I,J) IS A PARTIAL CELL	RICE8	1877
	C	RICE8	1878
331	IF(X3.EQ.X1.AND.Y3.EQ.Y2)GO TO 255	RICE8	1879
341	IF(X3.EQ.X1.AND.Y3.EQ.Y1)GO TO 260	RICE8	1880
350	IF(X3.EQ.X2.AND.Y3.EQ.Y1)GO TO 265	RICE8	1881
	C*****TRIANGLE LIES IN THIRD QUADRANT	RICE8	1882
	C	RICE8	1883
356	YTED=(Y1-Y2)/(X2-X1)*(XTE-X1)+Y2	RICE8	1884
364	IYTED=1000.*YTED+.1*DY	RICE8	1885
367	IF(IYTE-IYTED)285,278,283	RICE8	1886
	C*****TRIANGLE LIES IN FOURTH QUADRANT	RICE8	1887
	C	RICE8	1888
372	255 IYTED=1000.*((Y2-Y1)/(X2-X1)*(XTE-X1)+Y1)+.1*DY	RICE8	1889
403	IF(IYTE-IYTED)285,279,283	RICE8	1890
	C*****TRIANGLE LIES IN FIRST QUADRANT	RICE8	1891
	C	RICE8	1892
406	260 IYTED=1000.*((Y1-Y2)/(X2-X1)*(XTE-X1)+Y2)+.1*DY	RICE8	1893
417	IF(IYTE-IYTED)283,276,285	RICE8	1894
	C*****TRIANGLE LIES IN SECOND QUADRANT	RICE8	1895
	C	RICE8	1896
422	265 IYTED=1000.*((Y2-Y1)/(X2-X1)*(XTE-X1)+Y1)+.1*DY	RICE8	1897
433	IF(IYTE-IYTED)283,277,285	RICE8	1898
436	270 IF(YTE-DY.GT.Y1)GO TO 283	RICE8	1899
443	IF(XTE.LT.O1B(1,K))GO TO 283	RICE8	1900
447	IF(XTE.GT.O1B(2,K))GO TO 283	RICE8	1901
	C	RICE8	1902
	C**** CELL(I,J) IS A SOLID WITH INFLOW ACROSS THE BOTTOM BOUNDARY	RICE8	1903
	C	RICE8	1904
453	FL(I,J)=5 \$ GO TO 295	RICE8	1905
460	275 IF(XTE+DX.LT.X2)GO TO 283	RICE8	1906
464	IF(YTE.LT.O1B(1,K))GO TO 283	RICE8	1907
470	IF(YTE.GT.O1B(2,K))GO TO 283	RICE8	1908
	C	RICE8	1909
	C**** CELL(I,J) IS A SOLID WITH INFLOW ACROSS THE RIGHT BOUNDARY	RICE8	1910
	C	RICE8	1911
474	FL(I,J)=5 \$ GO TO 285	RICE8	1912
501	276 FL(I,J)=6 \$ GO TO 281	RICE8	1913
506	277 FL(I,J)=7 \$ GO TO 281	RICE8	1914
513	278 FL(I,J)=8 \$ GO TO 281	RICE8	1915
520	279 FL(I,J)=9 \$ GO TO 281	RICE8	1916
525	281 IF(INSO(K).EQ.1)FL(I,J)=FL(I,J)+4 \$ GO TO 285	RICE8	1917
537	283 IF(INSO(K).EQ.1)GO TO 284	RICE8	1918
	C	RICE8	1919
	C**** CELL(I,J) IS A SOLID	RICE8	1920
	C	RICE8	1921
542	FL(I,J)=2 \$ GO TO 285	RICE8	1922
547	284 FL(I,J)=3	RICE8	1923
554	285 CONTINUE	RICE8	1924
561	295 CONTINUE	RICE8	1925
564	RETURN	RICE8	1926
565	END	RICE8	1927

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C		RICE8	1928
C		RICE8	1929
C	*** END OF THE SUBROUTINE FLIC	RICE8	1930
C		RICE8	1931
C		RICE8	1932

		RICE8	1933
	SUBROUTINE CVIC		
	C**** TAPE-5 DATA FOR STORAGE AND RESTART	RCOM1	2
1	COMMON/TAPED/ITD,NTD,NSDMP,NFILE,NWDMP,NCYDMP	RCOM1	3
	C**** THE RCOM1 DATA BLOCK IS USED IN RICE(MAIN-PROGRAM),PROG AND RTAPES	RCOM1	4
	C	RCOM1	5
	C**** THE RCOM2 DATA BLOCK IS COMMON TO RICE AND ALL SUBROUTINES	RCOM1	6
	C**** BOTH RCOM1 AND RCOM2 ARE LOADED USING *COMDECK FEATURE OF (UPDATE)	RCOM1	7
1	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPLOT(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,OTC,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASQ	RCOM2	4
1	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECREQ,DDX,DDY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,X1,IT	RCOM2	6
1	COMMON/INFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHOO,RINT1,	RCOM2	7
	IRINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIEO,SIET1,SIET2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
1	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
1	COMMON/SPEED/ETAO,FAO(7),FAT1(7),FAT2(7),	RCOM2	11
	1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),C(3),CF(3),ZETAF(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
1	COMMON/OBSD/ITO(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FABO(7,20)	RCOM2	16
1	INTEGER AM,BM	RCOM2	17
1	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
1	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RH0(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHOT(62, 32),RHOU(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CQ(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
1	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
1	EQUIVALENCE (RHOU,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
1	INTEGER FL,CYCLE	RCOM2	34
1	REAL MU	RCOM2	35
	3 FORMAT(1H06312)	RICE8	1936
	4 FORMAT(1H1)	RICE8	1937
	C	RICE8	1938
	C**** THIS SUBROUTINE SETS SOME PROBLEM CONSTANTS AND DEFINES THE	RICE8	1939
	C**** COMPUTING MESH FLUID VARIABLE INITIAL CONDITIONS FROM INPUT DATA	RICE8	1940
	C	RICE8	1941
1	PRINT 4	RICE8	1942
	C	RICE8	1943
	C**** DEFINES PROGRAM CONSTANTS BASED ON INPUT DATA	RICE8	1944
	C	RICE8	1945
5	DDX=1./DX \$ DDY=1./DY	RICE8	1946
10	VCON=PHI*DT*DDY \$DDX2=1./DX**2 \$ DDY2=1./DY**2	RICE8	1947
16	UCON=PHI*DT*DDX	RICE8	1948
20	ERRD=RHO0*.00001	RICE8	1949


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22      ITMAX=1000.                                RICE8 1950
23      PFAC=2.*THETA*PHI*DT**2*(DDY2+DDX2)       RICE8 1951
31      XI=1.                                       RICE8 1952
33      RRHO=1./RHOO                                RICE8 1953
35      DO 297 J=1,JB2                              RICE8 1954
C                                             RICE8 1955
C**** DETERMINES COORDINATES TO BE USED---RECTANGULAR(ITC=0),CYL.(ITC=1) RICE8 1956
C                                             RICE8 1957
37      IF(ITC.EQ.1)GO TO 294                       RICE8 1958
42      RJ(J)=1.                                     RICE8 1959
43      RJ2(J)=1.                                    RICE8 1960
46      GO TO 296                                    RICE8 1961
54      294 RJ(J)=(J-1)*DY-DY/2.                   RICE8 1962
56      RJ2(J)=(J-1)*DY                             RICE8 1963
61      296 CONTINUE                                 RICE8 1964
61      KPR=JB2-J+1                                 RICE8 1965
64      WRITE(9,3),(FL(1,KPR),I=1,1B2)             RICE8 1966
76      297 WRITE(12,3),(FL(1,KPR),I=1,1B2)       RICE8 1967
114     PRINT 4                                      RICE8 1968
C          -----PRINTS CELL FLAGS-----        RICE8 1969
C**** CLEARS ARRAYS----BYPASSES IF RESTART DATA READ FROM TAPES RICE8 1970
C                                             RICE8 1971
117     IF(1TD.GT.1)GO TO 406                       RICE8 1972
123     DO 405 J=1,JB2                              RICE8 1973
124     DO 405 I=1,1B2                              RICE8 1974
125     P(I,J)=RHOU(I,J)=RHOV(I,J)=PB(I,J)=0.      RICE8 1975
143     RHOVT(I,J)=RHOUT(I,J)=RHOT(I,J)=CSQ(I,J)=0. RICE8 1976
160     RE(I,J)=U(I,J)=V(I,J)=SIE(I,J)=0.          RICE8 1977
175     RHO(I,J)=MU(I,J)=CQ(I,J)=ETA(I,J)=0.       RICE8 1978
212     TE(I,J)=0.                                  RICE8 1979
215     DO 403 K=1,NSPEC                            RICE8 1980
225     FA(I,J,K)=0.0                               RICE8 1981
226     403 CONTINUE                                RICE8 1982
230     405 CONTINUE                                RICE8 1983
235     406 CONTINUE                                RICE8 1984
235     YTS=-.5*DY                                  RICE8 1985
237     DO 495 J=1,JB2                              RICE8 1986
241     YTE=YTS+DY*(J-1)                            RICE8 1987
245     XTS=-.5*DX                                  RICE8 1988
250     DO 490 I=1,1B2                              RICE8 1989
251     IF(FL(I,J).NE.5.AND.1TD.GT.1)GO TO 490     RICE8 1990
264     XTE=XTS+DX*(I-1)                            RICE8 1991
C                                             RICE8 1992
C**** SETS ALL INFLOW DATA INTO FICTIOUS CELL IF FL(I,J)=5 RICE8 1993
C**** U-VEL.=0. AT TOP BOUNDARY,V-VEL.=0. AT LEFT BOUNDARY RICE8 1994
C                                             RICE8 1995
270     IF(J.EQ.1)GO TO 490                          RICE8 1996
272     IF(J.EQ.JB2)GOTO 430                        RICE8 1997
273     IF(I.EQ.1)GO TO 410                          RICE8 1998
274     IF(I.EQ.1B2)GO TO 415                       RICE8 1999
276     IF(I.EQ.1B1)GO TO 420                      RICE8 2000
277     IF(J.EQ.JB1)GO TO 435                      RICE8 2001
301     IF(FL(I,J).GT.1.AND.FL(I,J).LT.5)GO TO 490 RICE8 2002
314     IF(FL(I,J).EQ.1)GO TO 455                  RICE8 2003
321     IF(NO.LE.0)GO TO 407                       RICE8 2004

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1206	520 CONTINUE	RICE6	2115
1211	521 KO=K \$ GO TO NOR	RICE8	2116
1216	490 CONTINUE	RICE8	2117
1221	495 CONTINUE	RICE8	2118
1223	YTS=-.5*DY	RICE8	2119
1225	DO 530 J=2,JB1	RICE8	2120
1227	YTE=YTS+DY*(J-1) \$ XTS=-.5*DX	RICE8	2121
1235	DO 529 I=2,IB2	RICE8	2122
1237	IF (FL(I,J).NE.5.AND.(TD.GT.1))GO TO 529	RICE8	2123
1252	XTE=XTS+DX*(I-1)	RICE8	2124
1256	IF (FL(I,J).EQ.1)GO TO 525	RICE8	2125
1263	IF (FL(I,J).EQ.4)GO TO 525	RICE8	2126
1267	IF (FL(I,J).GT.5)GO TO 525	RICE8	2127
1274	IF (FL(I,J).NE.5)GO TO 529	RICE8	2128
1277	ASSIGN 523 TO NOR \$ GO TO 505	RICE8	2129
1301	523 IF (ITO(KO).EQ.3)GOTO 524	RICE8	2130
	C	RICE8	2131
	C**** SETS OBSTACLE INFLOW CELLS TO INPUT DATA VALUES	RICE8	2132
	C	RICE8	2133
1304	RHO(I,J)=RINBO(KO) \$ SIE(I,J)=SIEBO(KO)	RICE8	2134
1313	MU(I,J)=MINBO(KO)	RICE8	2135
1316	DO 526 K=1,NSPEC	RICE8	2136
1320	526 FA(I,J,K)=FABO(K,KO) \$ GO TO 529	RICE8	2137
1332	524 RHO(I,J)=RINRO(KO) \$ SIE(I,J)=SIERO(KO)	RICE8	2138
1342	MU(I,J)=MINRO(KO)	RICE8	2139
1345	DO 527 K=1,NSPEC	RICE8	2140
1347	527 FA(I,J,K)=FARO(K,KO) \$ GO TO 529	RICE8	2141
	C	RICE8	2142
	C**** SETS SPECIFIED VALUES INTO ALL FLUID REAL CELLS	RICE8	2143
	C	RICE8	2144
1361	525 RHO(I,J)=RHOO \$ SIE(I,J)=SIEO \$ MU(I,J)=MUO	RICE8	2145
1374	DO 528 K=1,NSPEC	RICE8	2146
1375	528 FA(I,J,K)=FAO(K) \$ GO TO 529	RICE8	2147
1405	529 CONTINUE	RICE8	2148
1410	530 CONTINUE	RICE8	2149
1412	600 DO 655 J=2,JB2	RICE8	2150
1414	DO 655 I=1,IB1	RICE8	2151
1415	IF (FL(I,J).GT.1.AND.FL(I,J).LT.5)GO TO 655	RICE8	2152
	C	RICE8	2153
	C**** DEFINES COMPUTED FLUID VARIABLES	RICE8	2154
1430	IF (NSPEC.LE.0)GO TO 603	RICE8	2155
1431	SUM=0.	RICE8	2156
1432	SUMI=0.	RICE8	2157
1433	DO 602 K=1,NSPEC	RICE8	2158
1434	IF (FA(I,J,K).LE.0.)GO TO 602	RICE8	2159
1445	SUM=SUM+FA(I,J,K)*CV(K)	RICE8	2160
1450	SUMI=SUMI+FA(I,J,K)*CV(K)*GAMA(K)	RICE8	2161
1453	602 CONTINUE	RICE8	2162
1456	IF (SUM.NE.0.)GAMMA=SUMI/SUM	RICE8	2163
1460	IF (SUM.LE.0.)TE(I,J)=0.	RICE8	2164
1466	IF (SUM.GT.0.)TE(I,J)=RHO(I,J)*SIE(I,J)/SUM	RICE8	2165
1502	603 CONTINUE	RICE8	2166
1502	P(I,J)=(GAMMA-1.)*RHO(I,J)*SIE(I,J)	RICE8	2167
1515	IF (FL(I,J).EQ.5)GO TO 645	RICE8	2168
1523	RHO(I,J)=(RHO(I,J)+RHO(I+1,J))*U(I,J)*.5	RICE8	2169

1531	RHOV(I,J)=(RHO(I,J)+RHO(I,J+1))*V(I,J)*.5	RICE8	2170
1540	IF (FL(I,J).EQ.1)GO TO 605 \$ NFL=FL(I,J)-5	RICE8	2171
1547	GO TO 1610,615,615,610,610,615,615,610)NFL	RICE8	2172
1562	605 XKE=.25*(U(I,J)+U(I-1,J))*2 \$ GO TO 620	RICE8	2173
1573	610 XKE=U(I,J)**2 \$ GO TO 620	RICE8	2174
1600	615 XKE=U(I-1,J)**2	RICE8	2175
1605	620 IF (FL(I,J).EQ.1)GO TO 625 \$ NFL=FL(I,J)-5	RICE8	2176
1616	GO TO (630,630,635,635,630,630,635,635)NFL	RICE8	2177
1631	625 YKE=.25*(V(I,J)+V(I,J-1))*2 \$ GO TO 640	RICE8	2178
1642	630 YKE=V(I,J)**2 \$ GO TO 640	RICE8	2179
1647	635 YKE=V(I,J-1)**2	RICE8	2180
1654	640 RE(I,J)=RHO(I,J)*(SIE(I,J)+.5*(XKE+YKE))	RICE8	2181
1671	GO TO 655	RICE8	2182
1671	645 IF (U(I,J).EQ.0.) GO TO 650	RICE8	2183
1677	RE(I,J)=RHO(I,J)*(SIE(I,J)+.5*U(I,J)**2)	RICE8	2184
1704	RHOV(I,J)=RHO(I,J)*U(I,J)	RICE8	2185
1710	GO TO 655	RICE8	2186
1714	650 RE(I,J)=RHO(I,J)*(SIE(I,J)+.5*V(I,J-1)**2)	RICE8	2187
1722	RHOV(I,J)=RHO(I,J)*V(I,J-1)	RICE8	2188
1726	655 CONTINUE	RICE8	2189
1733	RETURN	RICE8	2190
1734	END	RICE8	2191
C		RICE8	2192
C		RICE8	2193
C	*** END OF THE SUBROUTINE CVIC *****	RICE8	2194
C		RICE8	2195
C		RICE8	2196

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SUBROUTINE VPLOT1K,XX1,YY1,XX2,YY2)
14 COMMON/GEOMD/182,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPLOT(5),NSPEC,
11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TP,PLD,OTC,ALA,BIE,THE1A,
2PHI,OMEGA,GAMMA,DXOU,ASO
14 COMMON/ICCD/18,JB,18,JB1,NAME(10),JNM,TBEG,SECREG,DOX,DOY
1,UCON,VCIN,FRRD,ITMAX,PFAC,RRHO,X1,IT
14 COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,
1RINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIE1,SIE12,
2SIEL1,SIEL2
14 REAL MUO,MINT1,MINT2,MINL1,MINL2
14 COMMON/SPECD/ETA0,FA0(7),FAT1(7),FAT2(7),
1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),
2BM(7,3),OI(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)
14 COMMON/OBSD/1TO(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20),
1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),
2SIEBO(20),FARO(7,20),FABO(7,20)
14 INTEGER AM,BM
14 REAL MINRO,MINBO
C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM PREP)
C**** AND THE *READ FEATURE OF (UPDATE)
C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD
C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO 182,JB2 AND NSPEC
C
14 LCM/CELLD/FL( 62, 32),UI( 62, 32),VI( 62, 32
1),RHO( 62, 32),SIE( 62, 32),PI( 62, 32
2),MUI( 62, 32),CSO( 62, 32),RHO1( 62, 32),RHOUI( 62
3, 32),RHOVI( 62, 32),REI( 62, 32),ETA( 62, 32),CO(
4 62, 32),FA( 62, 32, 7),RJI( 32),RJJ(
5 32),FB( 62),TFAB( 62, 7),TE( 62, 32)
14 DIMENSION RHOUT( 62, 32),RHOVT( 62, 32),PB(
1 62, 32),DRHO( 62, 7),STREB( 62)
14 EQUIVALENCE (JU,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,FLB),
1(TFAB,DRHO)
14 INTEGER FL,CYCLE
14 REAL MU
14 DIMENSION KFLO(12),KOB(6,20),KOIB(2,20)
C K=0 CONVERT GRID,K=1 PLOTS GRID,K=2 CONVERTS AND PLOTS VECTORS
2015 FORMAT(20X,A10)
2016 FORMAT(3X,10A8* T=*1PE12.5* CYCLE=*15)
14 IF(K-1)15,25
16 1)YB=916
17 XL=0.
20 XR=18*DX
22 YT=JB*DY
25 YB=0.
25 IF(XR.LE.1.13556*YT)GO TO 2
31 1XL=0 $ 1XR=1022 $ 1YT=916-YT*1022/XR $ GO TO 5
40 2 X=XR*450/YT $ 1XL=511-X $ 1XR=511*X $ 1YT=16
C*****CONVERTS GRID TO 4020 COORDINATES---K=0
52 5 CONTINUE
52 DO B J=1,12
54 IF(J.GE.5.AND.J.LE.8) GO TO 6
65 CALL CONVRT(FLO(J),KFLO(J),YB,YT,1YB,1YT)
73 GO TO 8
77 6 CALL CONVRT(FLO(J),KFLO(J),XL,XR,1XL,1XR)

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111	9 CONTINUE	RICEB	2219
113	IF (NO.LE.0) RETURN	RICEB	2220
116	DO 14 N=1,NO	RICEB	2221
120	DO 9 J=1,2	RICEB	2222
121	9 CALL CC VRT(KOB1J,N),KOB1J,N,XL,KR,IXL,IXR)	RICEB	2223
137	CALL CONV(KOB15,N),KOB15,N,XL,KR,IXL,IXR)	RICEB	2224
150	DO 10 J=3,4	RICEB	2225
155	10 CALL CONV(KOB1J,N),KOB1J,N,YB,YT,LYB,LYT)	RICEB	2226
173	CALL CONV(KOB16,N),KOB16,N,YB,YT,LYB,LYT)	RICEB	2227
204	DO 11 J=1,2	RICEB	2228
211	IF (IT0INI.EQ.3) CALL CONV(KOB1J,N),KOB1J,N,XL,KR,IXL,IXR)	RICEB	2229
227	11 IF (IT0INI.EQ.4) CALL CONV(KOB1J,N),KOB1J,N,XL,KR,IXL,IXR)	RICEB	2230
247	14 CONTINUE	RICEB	2231
252	RETURN	RICEB	2232
	C****PLOTS GRID USING DRV(KX1)	RICEB	2233
253	15 CONTINUE	RICEB	2234
253	CALL ADV(1)	RICEB	2235
255	NGR=0	RICEB	2236
256	IF (LPR.LE.0) GO TO 17	RICEB	2237
263	CALL L(INCNT)GO	RICEB	2238
264	WRITE (12,2015) JGR	RICEB	2239
275	WRITE (12,2016) NAME,TIME,CYCLE	RICEB	2240
315	17 CONTINUE	RICEB	2241
315	CALL DRV(IXL,LYB,IXR,LYB)	RICEB	2242
321	IF (FLO1 2).LE.FLO1 1) GO TO 101 \$CALL DRV(IXR,LYB,IXR,KFLO1 1)	RICEB	2243
324	IF (FLO1 3).LE.FLO1 2) GO TO 100	RICEB	2244
342	CALL DRV(IXR,KFLO1 2),IXR,KFLO1 3) \$ CALL DRV(IXR,KFLO1 4),IXR,LYT)	RICEB	2245
355	GO TO 102	RICEB	2246
361	100 CALL DRV(IXR,KFLO1 2),IXR,LYT)	RICEB	2247
366	GO TO 102	RICEB	2248
372	101 CALL DRV(IXR,LYB,IXR,LYT)	RICEB	2249
401	102 IF (FLO1 6).LE.FLO1 5) GO TO 111 \$ CALL DRV(IXL,LYT,KFLO1 6),LYT)	RICEB	2250
411	IF (FLO1 7).LE.FLO1 6) GO TO 110	RICEB	2251
417	CALL DRV(KFLO1 6),LYT,KFLO1 7),LYT) \$ CALL DRV(KFLO1 8),LYT,IXR,LYT)	RICEB	2252
430	GO TO 112	RICEB	2253
434	110 CALL DRV(KFLO1 6),LYT,IXR,LYT)	RICEB	2254
440	GO TO 112	RICEB	2255
444	111 CALL DRV(IXL,LYT,IXR,LYT)	RICEB	2256
453	112 IF (FLO1 10).LE.FLO1 9) GO TO 121 \$ CALL DRV(IXL,LYB,IXL,KFLO1 9)	RICEB	2257
463	IF (FLO1 11).LE.FLO1 10) GO TO 120	RICEB	2258
471	CALL DRV(IXL,KFLO1 10),IXL,KFLO1 11) \$ CALL DRV(IXL,KFLO1 12),IXL,LYT)	RICEB	2259
504	GO TO 122	RICEB	2260
510	120 CALL DRV(IXL,KFLO1 10),IXL,LYT)	RICEB	2261
515	GO TO 122	RICEB	2262
521	121 CALL DRV(IXL,LYB,IXL,LYT)	RICEB	2263
530	122 CONTINUE	RICEB	2264
530	IF (NO.LE.0) RETURN	RICEB	2265
533	DO 295 N=1,NO \$ KX1=KOB(1,N) \$ KX2=KOB(2,N) \$ KY1=KOB(3,N)	RICEB	2266
544	KY2=KOB(4,N) \$ KX3=KOB(5,N) \$ KY3=KOB(6,N)	RICEB	2267
553	IF (IT0INI.EQ.1) GO TO 250	RICEB	2268
556	CALL DRV(KX1,KY1,KX1,KY2) \$ CALL DRV(KX1,KY2,KX2,KY2)	RICEB	2269
564	IF (IT0INI)=3) 205,215,225	RICEB	2270
572	205 CALL DRV(KX1,KY1,KX2,KY1) \$ CALL DRV(KX2,KY1,KX2,KY2) \$ GO TO 295	RICEB	2271
605	215 CALL DRV(KX1,KY1,KX2,KY1) \$ CALL DRV(KX2,KY1,KX2,KO1B(1,N))	RICEB	2272
620	CALL DRV(KX2,KO1B(2,N),KX2,KY2) \$ GO TO 295	RICEB	2273

633	225	CALL DRV(KX2,KY1,KX2,K/2) \$ CALL DRV(KX1,KY1,KO1B(1,N),KY1)	RICE8	2274
646		CALL DRV(KO1B(2,N),KY1,KX2,KY1) \$ GO TO 295	RICE8	2275
657	250	IF(OB(5,N).EQ.OB(1,N).AND.OB(6,N).EQ.OB(3,N)) GO TO 255	RICE8	2276
673		IF(OB(5,N).EQ.OB(2,N).AND.OB(6,N).EQ.OB(4,N)) GO TO 255	RICE8	2277
706		IF(OB(5,N).EQ.OB(2,N).AND.OB(6,N).EQ.OB(3,N)) GO TO 260	RICE8	2278
721		IF(OB(5,N).EQ.OB(1,N).AND.OB(6,N).EQ.OB(4,N)) GO TO 260	RICE8	2279
734		GO TO 295	RICE8	2280
734	255	CALL DRV(KX2,KY1,KX3,KY3) \$ CALL DRV(KX1,KY2,KX3,KY3)	RICE8	2281
743		CALL DRV(KX1,KY2,KX2,KY1) \$ GO TO 295	RICE8	2282
752	260	CALL DRV(KX1,KY1,KX3,KY3) \$ CALL DRV(KX2,KY2,KX3,KY3)	RICE8	2283
761		CALL DRV(KX1,KY1,KX2,KY2)	RICE8	2284
767	295	CONTINUE	RICE8	2285
772		IF(NGR.EQ.1) GO TO 22	RICE8	2286
774		NGR=1	RICE8	2287
775		GO TO 17	RICE8	2288
775	22	CONTINUE	RICE8	2289
775		RETURN	RICE8	2290
		C*****CONVERTS AND PLOTS VEL.VECTORS FOR EACH REAL CELL---K=2	RICE8	2291
776	25	CONTINUE	RICE8	2292
776		CALL CONVRT(XX1,IX1,XL,XR,IXL,IXR)	RICE8	2293
1002		CALL CONVRT(XX2,IX2,XL,XR,IXL,IXR)	RICE8	2294
1011		CALL CONVRT(YY1,IY1,YB,YT,,YB,IYT)	RICE8	2295
1020		CALL CONVRT(YY2,IY2,YB,YT,,YB,IYT)	RICE8	2296
1027		CALL DRV(IX1,IY1,IX2,IY2)	RICE8	2297
1032		RETURN	RICE8	2298
1033		END	RICE8	2299
		C	RICE8	2300
		C	RICE8	2301
		C**** END OF THE SUBROUTINE VPLOT *****	RICE8	2302
		C	RICE8	2303
		C	RICE8	2304

	SUBROUTINE CNPLOT(K,JSP)	RICEB	2305
6	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPLO(15),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLO,OTC,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASO	RCOM2	4
6	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECRETQ,DDX,ODY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,XI,IT	RCOM2	6
6	COMMON/INPFLD/FLO(12),UD,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,	RCOM2	7
	IRINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIE11,SIE12,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
6	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
6	COMMON/SPECQ/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	IFAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q1(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
6	COMMON/OBSD/ITO(20),NSO(20),OB(6,20),OIB(2,20),UINRO(20),PINRO(20)	RCOM2	14
	1,MINRO(20),SIERO(20),VINGO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FARO(7,20)	RCOM2	16
6	INTEGER AM,BM	RCOM2	17
6	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
6	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHOT(62, 32),RHOU(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CO(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
6	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
6	EQUIVALENCE (RHOU,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
6	INTEGER FL,CYCLE	RCOM2	34
6	REAL MU	RCOM2	35
	2001 FORMAT(4X,*RHO*)	RICEB	2307
	2002 FORMAT(4X,*PB*)	RICEB	2308
	2003 FORMAT(4X,*SIE*)	RICEB	2309
	2004 FORMAT(4X,*TEMPERATURE*)	RICEB	2310
	2005 FORMAT(4X,*MACH NO.*)	RICEB	2311
	2006 FORMAT(4X,*SPEC.FA*)	RICEB	2312
	2007 FORMAT(4X,*SPEC.FB*)	RICEB	2313
	2008 FORMAT(4X,*SPEC.FC*)	RICEB	2314
	2009 FORMAT(4X,*SPEC.FD*)	RICEB	2315
	2010 FORMAT(4X,*SPEC.FE*)	RICEB	2316
	2011 FORMAT(4X,*SPEC.FF*)	RICEB	2317
	2012 FORMAT(4X,*SPEC.FG*)	RICEB	2318
	2015 FORMAT(20X,A10)	RICEB	2319
	2016 FORMAT(3X,10A8* T=*1PE12.5* CYCLE=*15)	RICEB	2320
	2017 FORMAT(3X,*QMX=*FB.4,* QMN=*FB.4,* MAX.CON.LINE=*FB.4,* MIN.	RICEB	2321
	ICON.LINE=*FB.4,* INTERVAL=*FB.4)	RICEB	2322
C	K=0 CONVERT GRID,K=1 PLOTS GRID,K=2 CONVERTS AND PLOTS CONTOUR	RICEB	2323
6	DIMENSION ZC(20),CON(11)	RICEB	2324
6	DIMENSION XY(2),YX(2)	RICEB	2325
6	DIMENSION KFLO(12),KOB(6,20),KOIB(2,20)	RICEB	2326

ROW NUMBER	CODE	NUMBER	LINE NO.	TABLE NO.	PAGE NO.
6	IF (K-111.15.25			RICE6	2327
10	1 IYB=916			RICE6	2328
11	XL=0.			RICE6	2329
12	XR=18*DX			RICE6	2330
14	YT=JR*DY			RICE6	2331
17	YB=0.			RICE6	2332
17	IF (XR.LE.1.13556*YF) GO TO 2			RICE6	2333
23	1XL=0 \$ IXR=1022 \$ IYF=916-YT*1022/XR \$ GO TO 5			RICE6	2334
32	2 X=XR*450/YT \$ IXL=511-X \$ IXR=311-X \$ IYF=16			RICE6	2335
	C*****CONVERTS GRID TO 4020 COORDINATES---K=0			RICE6	2336
44	5 CONTINUE			RICE6	2337
44	DO 8 J=1,12			RICE6	2338
46	IF (J.GE.5.AND.J.LE.8) GO TO 6			RICE6	2339
57	CALL CONVRT(FLO(J),KFLO(J),YB,YT,IYB,IYF)			RICE6	2340
63	GO TO 8			RICE6	2341
65	6 CALL CONVRT(FLO(J),KFLO(J),XL,XR,IXL,IXR)			RICE6	2342
75	8 CONTINUE			RICE6	2343
77	IF (NO.LE.0) RETURN			RICE6	2344
102	DO 14 N=1,NO			RICE6	2345
104	DO 9 J=1,2			RICE6	2346
105	9 CALL CONVRT(OBJ(N),KOBJ(N),XL,XR,IXL,IXR)			RICE6	2347
121	CALL CONVRT(OB(5,N),KOB(5,N),XL,XR,IXL,IXR)			RICE6	2348
130	DO 10 J=3,4			RICE6	2349
133	10 CALL CONVRT(OBJ(N),KOBJ(N),YB,YT,IYB,IYF)			RICE6	2350
147	CALL CONVRT(OB(6,N),KOB(6,N),YB,YT,IYB,IYF)			RICE6	2351
156	DO 11 J=1,2			RICE6	2352
161	IF (ITO(N).EQ.3) CALL CONVRT(OIB(J,N),KOIB(J,N),YB,YT,IYB,IYF)			RICE6	2353
175	11 IF (ITO(N).EQ.4) CALL CONVRT(OIB(J,N),KOIB(J,N),XL,XR,IXL,IXR)			RICE6	2354
213	14 CONTINUE			RICE6	2355
216	RETURN			RICE6	2356
	C*****PLOTS GRID USING DRV---K 1			RICE6	2357
217	15 CONTINUE			RICE6	2358
217	CALL ADV(1)			RICE6	2359
221	NGR=0			RICE6	2360
222	IF (LPR.LE.0) GO TO 17			RICE6	2361
225	CALL LINCNT(60)			RICE6	2362
226	WRITE (12,2015) JNM			RICE6	2363
235	WRITE (12,2016) NAME,TIME,CYCLE			RICE6	2364
252	17 CONTINUE			RICE6	2365
252	CALL DRV(IXL,IYB,IXR,IYB)			RICE6	2366
256	IF (FLO(2).LE.FLO(1)) GO TO 101 \$ CALL DRV(IXR,IYB,IXR,KFLO(1))			RICE6	2367
266	IF (FLO(3).LE.FLO(2)) GO TO 100			RICE6	2368
272	CALL DRV(IXR,KFLO(2),IXR,KFLO(3)) \$ CALL DRV(IXR,KFLO(4),IXR,IYF)			RICE6	2369
302	GO TO 102			RICE6	2370
304	100 CALL DRV(IXR,KFLO(2),IXR,IYF)			RICE6	2371
310	GO TO 102			RICE6	2372
312	101 CALL DRV(IXR,IYB,IXR,IYF)			RICE6	2373
320	102 IF (FLO(6).LE.FLO(5)) GO TO 111 \$ CALL DRV(IXL,IYF,KFLO(5),IYF)			RICE6	2374
326	IF (FLO(7).LE.FLO(6)) GO TO 110			RICE6	2375
332	CALL DRV(KFLO(6),IYF,KFLO(7),IYF) \$ CALL DRV(KFLO(8),IYF,IXR,IYF)			RICE6	2376
342	GO TO 112			RICE6	2377
344	110 CALL DRV(KFLO(6),IYF,IXR,IYF)			RICE6	2378
350	GO TO 112			RICE6	2379
352	111 CALL DRV(IXL,IYF,IXR,IYF)			RICE6	2380
360	112 IF (FLO(10).LE.FLO(9)) GO TO 121 \$ CALL DRV(IXL,IYB,IXL,KFLO(9))			RICE6	2381

366	IF(FLO(11).LE.FLO(10))GO TO 120	RICEB	2382
372	CALL DRV1(XL,KFLO(10),IXL,KFLO(11))\$CALL DRV1(XL,KFLO(12),IXL,IY1)	RICEB	2383
402	GO TO 122	RICEB	2384
404	120 CALL DRV1(XL,KFLO(10),IXL,IY1)	RICEB	2385
410	GO TO 122	RICEB	2386
412	121 CALL DRV1(XL,IYB,IML,IY1)	RICEB	2387
420	122 CONTINUE	RICEB	2388
420	IF(ND.LE.0)RETURN	RICEB	2389
423	DO 295 N=1,ND \$ KX1=KOB(1,N) \$ KX2=KOB(2,N) \$ KY1=KOB(3,N)	RICEB	2390
434	KY2=KOB(4,N) \$ KX3=KOB(5,N) \$ KY3=KOB(6,N)	RICEB	2391
443	IF(I1TOINI.EQ.1) GO TO 250	RICEB	2392
446	CALL DRV1(KX1,KY1,KX2,KY2) \$ CALL DRV1(KX1,KY2,KX2,KY2)	RICEB	2393
454	IF(I1TOINI-3)205,215,225	RICEB	2394
461	205 CALL DRV1(KX1,KY1,KX2,KY1) \$ CALL DRV1(KX2,KY1,KX2,KY2) \$ GO TO 295	RICEB	2395
472	215 CALL DRV1(KX1,KY1,KX2,KY1) \$ CALL DRV1(KX2,KY1,KX2,KO1B(1,N))	RICEB	2396
503	CALL DRV1(KX2,KO1B(2,N),KX2,KY2) \$ GO TO 295	RICEB	2397
512	225 CALL DRV1(KX2,KY1,KX2,KY2) \$ CALL DRV1(KX1,KY1,KO1B(1,N),KY1)	RICEB	2398
523	CALL DRV1(KO1B(2,N),KY1,KX2,KY1) \$ GO TO 295	RICEB	2399
532	250 IF(OB(5,N).EQ.OB(1,N).AND.OB(6,N).EQ.OB(3,N)) GO TO 255	RICEB	2400
545	IF(OB(5,N).EQ.OB(2,N).AND.OB(6,N).EQ.OB(4,N)) GO TO 255	RICEB	2401
560	IF(OB(5,N).EQ.OB(2,N).AND.OB(6,N).EQ.OB(3,N)) GO TO 260	RICEB	2402
573	IF(OB(5,N).EQ.OB(1,N).AND.OB(6,N).EQ.OB(4,N)) GO TO 260	RICEB	2403
606	GO TO 295	RICEB	2404
606	255 CALL DRV1(KX2,KY1,KX3,KY3) \$ CALL DRV1(KX1,KY2,KX3,KY3)	RICEB	2405
615	CALL DRV1(KX1,KY2,KX2,KY1) \$ GO TO 295	RICEB	2406
622	260 CALL DRV1(KX1,KY1,KX3,KY3) \$ CALL DRV1(KX2,KY2,KX3,KY3)	RICEB	2407
631	CALL DRV1(KX1,KY1,KX2,KY2)	RICEB	2408
636	295 CONTINUE	RICEB	2409
641	IF(NGR.EQ.1) GO TO 22	RICEB	2410
643	NGR=1	RICEB	2411
644	GO TO 17	RICEB	2412
644	22 CONTINUE	RICEB	2413
644	RETURN	RICEB	2414
645	25 CONTINUE	RICEB	2415
645	XS=XL+DX/2. \$ YS=YB+DY/2.	RICEB	2416
653	DO 28 J=2,JB1	RICEB	2417
654	DO 28 I=2,IB1	RICEB	2418
654	E .		
662	IF(FL(I,J).NE.1)GO TO 28	RICEB	2419
662	QMN=QMX=CQ(I,J)	RICEB	2420
666	GO TO 29	RICEB	2421
666	28 CONTINUE	RICEB	2422
673	29 CONTINUE	RICEB	2423
673	DO 41 J=2,JB1	RICEB	2424
675	DO 41 I=2,IB1	RICEB	2425
675	IF(FL(I,J).GT.1.AND.FL(I,J).LT.6) GO TO 41	RICEB	2426
711	C*****CALCULATES -SPACING BETWEEN CONTOUR LINES (DQ)-MAX.CQ (QMX)-MIN.CQ	RICEB	2427
711	IF(CQ(I,J).LT.QMN) QMN=CQ(I,J)	RICEB	2428
721	IF(CQ(I,J).GT.QMX)QMX=CQ(I,J)	RICEB	2429
732	41 CONTINUE	RICEB	2430
737	DQ=(QMX-QMN)/10. \$ SUM=QMN \$ CC=0.	RICEB	2431
743	MIND=2	RICEB	2432
745	DO 43 I=1,11	RICEB	2433
746	CON(I)=SUM+(I-1)*DQ	RICEB	2434
753	IF(CC.GT.0.) GO TO 43	RICEB	2435
755	IF(CON(I).LE.QMN) GO TO 43	RICEB	2436

1405	69 L12=L24=1 \$ GO TO 74	RICE6	2492
1410	70 L12=1 \$ GO TO 74	RICE8	2493
1412	71 L13=1 \$ GO TO 74	RICE8	2494
1414	72 L24=1 \$ GO TO 74	RICE8	2495
1416	73 L34=1 \$ GO TO 74	RICE8	2496
1420	74 CONTINUE	RICE8	2497
1420	DO 93 N=1,11	RICE8	2498
	C*****IF CON.GT.CO SETS KN=1----IF CON.LE.CO SETS KN=0	RICE8	2499
1422	M=12-N \$ K1=K2=K3=K4=1	RICE8	2500
1427	IF(CON(M).LE.CO(1 ,J))K1=0	RICE8	2501
1436	IF(CON(M).LE.CO(1+1,J))K2=0	RICE8	2502
1445	IF(CON(M).LE.CO(1 ,J+1))K3=0	RICE8	2503
1454	IF(CON(M).LE.CO(1+1,J+1))K4=0	RICE8	2504
1463	IF(K1*K2*K3*K4.NE.0)GO TO 93	RICE8	2505
1470	IF((K1+K2+K3+K4).NE.0)GO TO 75	RICE8	2506
1471	GO TO 93	RICE8	2507
	C*****FINDS TWO INTERSECTION POINTS OF FOUR CELL REGION	RICE8	2508
1472	75 IC=0	RICE8	2509
1473	IF((K1+K3).NE.1)GO TO 77	RICE8	2510
1476	IF(L13.EQ.1)GO TO 77	RICE8	2511
1477	DR=0. \$ I11=1 \$ IC=IC+1 \$ ASSIGN 77 TO KR1 \$ GO TO 86	RICE8	2512
1504	77 IF((K1+K2).NE.1)GO TO 79	RICE8	2513
1507	IF(L12.EQ.1)GO TO 79	RICE8	2514
1510	DZ=0. \$ J11=J \$ IC=IC+1 \$ ASSIGN 79 TO KR1 \$ GO TO 87	RICE8	2515
1515	79 IF((K2+K4).NE.1)GO TO 81	RICE8	2516
1520	IF(L24.EQ.1)GO TO 81	RICE8	2517
1521	DR=DX \$ I11=1+1 \$ IC=IC+1 \$ ASSIGN 81 TO KR1 \$ GO TO 86	RICE8	2518
1527	81 IF((K3+K4).NE.1)GO TO 83	RICE8	2519
1532	IF(L34.EQ.1)GO TO 83	RICE8	2520
1533	DZ=DY \$ J11=J+1 \$ IC=IC+1 \$ ASSIGN 83 TO KR1 \$ GO TO 87	RICE8	2521
1541	83 GO TO 93	RICE8	2522
1546	86 XY(IC)=XD+DR	RICE8	2523
1547	YX(IC)=YD+DY*((CON(M)-CQ(111,J1))/(CQ(111,J+1)-CQ(111,J)))	RICE8	2524
1557	IF(IC.EQ.2)GO TO 89 \$ GO TO KR1	RICE8	2525
1570	87 YX(IC)=YD+DZ	RICE8	2526
1571	XY(IC)=XD+DX*((CON(M)-CQ(1,J11))/(CQ(1+1,J11)-CQ(1,J11)))	RICE8	2527
1601	IF(IC.EQ.2)GO TO 89 \$ GO TO KR1	RICE8	2528
	C*****CONVERTS AND PLOTS CONTOURS FOR FOUR REAL CELLS----K=2	RICE8	2529
1606	89 CALL CONVRT(XY(1) ,IX1,XL,XR,IXL,IXR)	RICE8	2530
1613	CALL CONVRT(XY(2) ,IX2,XL,XR,IXL,IXR)	RICE8	2531
1620	CALL CONVRT(YX(1) ,IY1,YB,YT,IYB,IYT)	RICE8	2532
1625	CALL CONVRT(YX(2) ,IY2,YB,YT,IYB,IYT)	RICE8	2533
1632	IF(M.EQ.10) CALL PLT(IX1,IY1,24)	RICE8	2534
1640	IF(M.EQ.MINO) CALL PLT(IX1,IY1,35)	RICE8	2535
1647	CALL DRV(IX1,IY1,IX2,IY2)	RICE8	2536
1657	93 CONTINUE	RICE8	2537
1661	95 CONTINUE	RICE8	2538
1664	97 CONTINUE	RICE8	2539
1666	RETURN	RICE8	2540
1667	END	RICE8	2541
	C	RICE8	2542
	C	RICE8	2543
	C***** END OF THE SUBROUTINE CNPLOT	RICE8	2544
	C	RICE8	2545
	C	RICE8	2546

	SUBROUTINE COPLOTT(K,JJSP)	RICE6	2547
6	COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC,	RCOM2	2
	11SPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTG,ALA,BIE,THETA,	RCOM2	3
	2PHI,OMEGA,GAMMA,DXOU,ASQ	RCOM2	4
6	COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECREQ,DDX,DDY	RCOM2	5
	1,UCON,VCON,ERRD,ITMAX,PFAC,RRHO,XI,IT	RCOM2	6
6	COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,	RCOM2	7
	1RINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIET1,SIET2,	RCOM2	8
	2SIEL1,SIEL2	RCOM2	9
6	REAL MUO,MINT1,MINT2,MINL1,MINL2	RCOM2	10
6	COMMON/SPEC0/ETA0,FA0(7),FAT1(7),FAT2(7),	RCOM2	11
	1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),	RCOM2	12
	2BM(7,3),Q(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)	RCOM2	13
6	COMMON/OBSD/IT0(20),NS0(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)	RCOM2	14
	1,MINRO(20),SIERO(20),VINBO(20),RINBO(20),MINBO(20),	RCOM2	15
	2SIEBO(20),FARO(7,20),FABO(7,20)	RCOM2	16
6	INTEGER AM,BM	RCOM2	17
6	REAL MINRO,MINBO	RCOM2	18
	C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)	RCOM2	19
	C**** AND THE *READ FEATURE OF (UPDATE)	RCOM2	20
	C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/	RCOM2	21
	C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC	RCOM2	22
	C	RCOM2	23
6	LCM/CELLD/FL(62, 32),U(62, 32),V(62, 32	RCOM2	24
	1),RHO(62, 32),SIE(62, 32),P(62, 32	RCOM2	25
	2),MU(62, 32),CSQ(62, 32),RHOI(62, 32),RHOI(62	RCOM2	26
	3, 32),RHOV(62, 32),RE(62, 32),ETA(62, 32),CQ(RCOM2	27
	4 62, 32),FA(62, 32, 7),RJ(32),RJ2(RCOM2	28
	5 32),RFLB(62),TFAB(62, 7),TE(62, 32)	RCOM2	29
6	DIMENSION RHOUT(62, 32),RHOVT(62, 32),PB(RCOM2	30
	1 62, 32),DRHOB(62, 7),STREB(62)	RCOM2	31
6	EQUIVALENCE (RHOV,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),	RCOM2	32
	1(TFAB,DRHOB)	RCOM2	33
6	INTEGER FL,CYCLE	RCOM2	34
6	REAL MU	RCOM2	35
	C K=0 CONVERT GRID,K=1 PLOTS GRID,K=2 CONVERTS AND PLOTS SPECIES	RICE8	2549
6	DIMENSION KFLO(12),KOB(6,20),KOIB(2,20)	RICE8	2550
	2015 FORMAT(20X,A7)	RICE8	2551
	2016 FORMAT(3X,10A8* T=*IPE12.5* CYCLE=*15)	RICE8	2552
6	IF(K-1)1,15,25	RICE8	2553
10	1 IYB=916	RICE8	2554
11	XL=0.	RICE8	2555
12	XR=IB*DX	RICE8	2556
14	YT=JB*OY	RICE8	2557
17	YB=0.	RICE8	2558
17	IF(IXR.LE.1.13556*YT)GO TO 2	RICE8	2559
23	1XL=0 \$ IXR=1022 \$ IYT=916-YT*1022/XR \$ GO TO 5	RICE8	2560
32	2 X=XR*450/YT \$ IXL=511-X \$ IXR=511+X \$ IYT=16	RICE8	2561
	C****CONVERTS GRID TO 4020 COORDINATES---K=0	RICE8	2562
44	5 CONTINUE	RICE8	2563
44	DO B J=1,12	RICE8	2564
46	IF(J.GE.5.AND.J.LE.8) GO TO 6	RICE8	2565
57	CALL CONVRT(FLO(J),KFLO(J),YB,YT,IYB,IYT)	RICE8	2566
63	GO TO 8	RICE8	2567
65	6 CALL CONVRT(FLO(J),KFLO(J),XL,XR,IXL,IXR)	RICE8	2568

75	8 CONTINUE	RICE8	2569
77	IF (NO.LE.0) RETURN	RICE8	2570
102	DO 14 N=1,NO	RICE8	2571
104	DO 9 J=1,2	RICE8	2572
105	9 CALL CONVRT(OB(J,N),KOB(J,N),XL,XR,IXL,IXR)	RICE8	2573
121	CALL CONVRT(OB(5,N),KOB(5,N),XL,XR,IXL,IXR)	RICE8	2574
130	DO 10 J=3,4	RICE8	2575
133	10 CALL CONVRT(OB(J,N),KOB(J,N),YB,YT,IYB,IYT)	RICE8	2576
147	CALL CONVRT(OB(6,N),KOB(6,N),YB,YT,IYB,IYT)	RICE8	2577
156	DO 11 J=1,2	RICE8	2578
161	IF (ITO(N).EQ.3) CALL CONVRT(OIB(J,N),KOIB(J,N),YB,YT,IYB,IYT)	RICE8	2579
175	11 IF (ITO(N).EQ.4) CALL CONVRT(OIB(J,N),KOIB(J,N),XL,XR,IXL,IXR)	RICE8	2580
213	14 CONTINUE	RICE8	2581
216	RETURN	RICE8	2582
	C*****PLOTS GRID USING DRV---K=1	RICE8	2583
217	15 CONTINUE	RICE8	2584
217	NGR=0	RICE8	2585
220	IF (LPR.LE.0) GO TO 17	RICE8	2586
222	CALL LINCNT(60)	RICE8	2587
223	WRITE (12,2015) JNM	RICE8	2588
232	WRITE (12,2016) NAME,TIME,CYCLE	RICE8	2589
247	17 CALL DRV(IXL,IYB,IXR,IYB)	RICE8	2590
253	IF (FLO(2).LE.FLO(1)) GO TO 101 \$CALL DRV(IXR,IYB,IXR,KFLO(1))	RICE8	2591
263	IF (FLO(3).LE.FLO(2)) GO TO 103	RICE8	2592
267	CALL DRV(IXR,KFLO(2),IXR,KFLO(3)) \$ CALL DRV(IXR,KFLO(4),IXR,IYT)	RICE8	2593
277	GO TO 102	RICE8	2594
301	103 CALL DRV(IXR,KFLO(2),IXR,IYT)	RICE8	2595
305	GO TO 102	RICE8	2596
307	101 CALL DRV(IXR,IYB,IXR,IYT)	RICE8	2597
315	102 IF (FLO(6).LE.FLO(5)) GO TO 111 \$ CALL DRV(IXL,IYT,KFLO(5),IYT)	RICE8	2598
323	IF (FLO(7).LE.FLO(6)) GO TO 110	RICE8	2599
327	CALL DRV(KFLO(6),IYT,KFLO(7),IYT) \$ CALL DRV(KFLO(8),IYT,IXR,IYT)	RICE8	2600
337	GO TO 112	RICE8	2601
341	110 CALL DRV(KFLO(6),IYT,IXR,IYT)	RICE8	2602
345	GO TO 112	RICE8	2603
347	111 CALL DRV(IXL,IYT,IXR,IYT)	RICE8	2604
355	112 IF (FLO(10).LE.FLO(9)) GO TO 121 \$ CALL DRV(IXL,IYB,IXL,KFLO(9))	RICE8	2605
363	IF (FLO(11).LE.FLO(10)) GO TO 120	RICE8	2606
367	CALL DRV(IXL,KFLO(10),IXL,KFLO(11)) \$CALL DRV(IXL,KFLO(12),IXL,IYT)	RICE8	2607
377	GO TO 122	RICE8	2608
401	120 CALL DRV(IXL,KFLO(10),IXL,IYT)	RICE8	2609
405	GO TO 122	RICE8	2610
407	121 CALL DRV(IXL,IYB,IXL,IYT)	RICE8	2611
415	122 CONTINUE	RICE8	2612
415	IF (NO.LE.0) RETURN	RICE8	2613
420	DO 295 N=1,NO \$ KX1=KOB(1,N) \$ KX2=KOB(2,N) \$ KY1=KOB(3,N)	RICE8	2614
431	KY2=KOB(4,N) \$ KX3=KOB(5,N) \$ KY3=KOB(6,N)	RICE8	2615
440	IF (ITO(N).EQ.1) GO TO 250	RICE8	2616
443	CALL DRV(KX1,KY1,KX1,KY2) \$ CALL DRV(KX1,KY2,KX2,KY2)	RICE8	2617
451	IF (ITO(N)-3) 205,215,225	RICE8	2618
456	205 CALL DRV(KX1,KY1,KX2,KY1) \$ CALL DRV(KX2,KY1,KX2,KY2) \$ GO TO 295	RICE8	2619
467	215 CALL DRV(KX1,KY1,KX2,KY1) \$ CALL DRV(KX2,KY1,KX2,KOIB(1,N))	RICE8	2620
500	CALL DRV(KX2,KOIB(2,N),KX2,KY2) \$ GO TO 295	RICE8	2621
507	225 CALL DRV(KX2,KY1,KX2,KY2) \$ CALL DRV(KX1,KY1,KOIB(1,N),KY1)	RICE8	2622
520	CALL DRV(KOIB(2,N),KY1,KX2,KY1) \$ GO TO 295	RICE8	2623

527	250	IF (OB(5,N).EQ.OB(1,N).AND.OB(6,N).EQ.OB(3,N)) GO TO 255	RICE8	2624
542		IF (OB(5,N).EQ.OB(2,N).AND.OB(6,N).EQ.OB(4,N)) GO TO 255	RICE8	2625
555		IF (OB(5,N).EQ.OB(2,N).AND.OB(6,N).EQ.OB(3,N)) GO TO 260	RICE8	2626
570		IF (OB(5,N).EQ.OB(1,N).AND.OB(6,N).EQ.OB(4,N)) GO TO 260	RICE8	2627
603		GO TO 295	RICE8	2628
603	255	CALL DRV(KX2,KY1,KX3,KY3) \$ CALL DRV(KX1,KY2,KX3,KY3)	RICE8	2629
612		CALL DRV(KX1,KY2,KX2,KY1) \$ GO TO 295	RICE8	2630
617	260	CALL DRV(KX1,KY1,KX3,KY3) \$ CALL DRV(KX2,KY2,KX3,KY3)	RICE8	2631
626		CALL DRV(KX1,KY1,KX2,KY2)	RICE8	2632
633	295	CONTINUE	RICE8	2633
636		IF (NGR.EQ.1) GO TO 22	RICE8	2634
640		NGR=1	RICE8	2635
641		GO TO 17	RICE8	2636
641	22	CONTINUE	RICE8	2637
641		RETURN	RICE8	2638
		C**** CONVERTS AND PLOTS SPECIES FOR EACH REAL CELL---K=2	RICE8	2639
		C**** TO PLOT IN COLOR USE ICHAR=42 AND CHANGE COLOR FOR EACH SPECIES	RICE8	2640
		C	RICE8	2641
642	25	CONTINUE	RICE8	2642
642		GO TO (35,37,39,41,43,44,46)JJSP	RICE8	2643
655	35	ICHR=42 \$ GO TO 45	RICE8	2644
657	37	ICHR=16 \$ GO TO 45	RICE8	2645
661	39	ICHR=44 \$ GO TO 45	RICE8	2646
663	41	ICHR=32 \$ GO TO 45	RICE8	2647
665	43	ICHR=63 \$ GO TO 45	RICE8	2648
667	44	ICHR=58 \$ GO TO 45	RICE8	2649
671	46	ICHR=13 \$ GO TO 45	RICE8	2650
673	45	CONTINUE	RICE8	2651
673		DO 100 J=2,JB2	RICE8	2652
675		YB1=YB+(J-2)*DY	RICE8	2653
701		DO 100 I=2,IB2	RICE8	2654
703		IF (FL(I,J).GT.1.AND.FL(I,J).LT.6) GO TO 100	RICE8	2655
720		XL1=XL+(I-2)*DX	RICE8	2656
725		KK=CQ(I,J)	RICE8	2657
727		IF (KK.LT.1) GO TO 100	RICE8	2658
731		DO 50 L=1,KK	RICE8	2659
		C	RICE8	2660
		C**** IF COLOR MOVIE IS BEING MADE,RANDSV AND RANDST MUST BE USED TO	RICE8	2661
		C**** KEEP DOTS STEADY IN EACH CELL (START RANDOM WITH SAME NUMBER)	RICE8	2662
		C	RICE8	2663
733		Y1Y=RANDOM(DUMMY)*DY+YB1	RICE8	2664
737		X1X=RANDOM(DUMMY)*DX+XL1	RICE8	2665
744		IF (FL(I,J).EQ.1) GO TO 65	RICE8	2666
752		XPC=X1X-XL1	RICE8	2667
753		YPC=Y1Y-YB1	RICE8	2668
756		NFL=FL(I,J)-5 \$ GO TO (52,54,56,58,52,54,56,58)NFL	RICE8	2669
776	52	YLINE= DY-DY*DDX*XPC	RICE8	2670
1001		IF (YPC.LE.YLINE)GO TO 50 \$ GO TO 65	RICE8	2671
1004	54	YLINE= DY*DDX*XPC	RICE8	2672
1006		IF (YPC.LE.YLINE)GO TO 50 \$ GO TO 65	RICE8	2673
1012	56	YLINE= DY-DY*DDX*XPC	RICE8	2674
1015		IF (YPC.GE.YLINE)GO TO 50 \$ GO TO 65	RICE8	2675
1020	58	YLINE= DY*DDX*XPC	RICE8	2676
1022		IF (YPC.GE.YLINE)GO TO 50 \$ GO TO 65	RICE8	2677
1026	65	CONTINUE	RICE8	2678

1026	CALL CONVRT(YIY,IY,YB,YT,IYB,IYT)	RICE6	2679
1033	CALL CONVRT(XIX,IX,XL,XR,IXL,IXR)	RICE8	2680
1037	CALL PLT(IX,IY,ICHAR)	RICE8	2681
1044	50 CONTINUE	RICE8	2682
1047	100 CONTINUE	RICE8	2683
1054	RETURN	RICE8	2684
1055	END	RICE8	2685
	C	RICE8	2686
	C	RICE8	2687
	C**** END OF THE SUBROUTINE COPLOT	RICE8	2688
	C	RICE8	2689
	C	RICE8	2690

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SUBROUTINE TANVEL
COMMON/GEOMD/IB2,JB2,NO,NSL(4),LPR,CYCLE,ITC,JPL0T(5),NSPEC,
1 ISPEC(7),NR,DX,DY,TIME,DT,TSTOP,TPR,TPL,TPLD,DTC,ALA,BIE,THETA,
2PHI,OMEGA,GAMMA,DXOU,ASQ
COMMON/ICCD/IB,JB,IB1,JB1,NAME(10),JNM,TBEG,SECREO,DDX,DDY
1 UCON,VCON,ERRD,ITMAX,PFAC,RRHO,X1,IT
COMMON/INPFLD/FLO(12),UO,VO,VINT1,VINT2,UINL1,UINL2,RHO0,RINT1,
1 RINT2,RINL1,RINL2,MUO,MINT1,MINT2,MINL1,MINL2,SIE0,SIE1,SIE2,
2SIEL1,SIEL2
REAL MUO,MINT1,MINT2,MINL1,MINL2
COMMON/SPEC/ETA0,FA0(7),FAT1(7),FAT2(7),
1FAL1(7),FAL2(7),SM(7),EP(7),GAMA(7),CV(7),ALPHA(7),AM(7,3),
2BM(7,3),O(3),CF(3),ZETA(3),EF(3),CB(3),ZETAB(3),EB(3)
COMMON/OBSD/IT0(20),NS0(20),OB(6,20),OIB(2,20),UINRO(20),RINRO(20)
1 MINRO(20),SIE0(20),VINBO(20),RINBO(20),MINBO(20),
2SIEBO(20),FARO(7,20),FAB0(7,20)
INTEGER AM,BM
REAL MINRO,MINBO
C**** /CELLD/ COMMON BLOCK IS LOADED USING A PRE-PROCESSOR PROGRAM(PREP)
C**** AND THE *READ FEATURE OF (UPDATE)
C**** THIS ALLOWS A VARIABLE SUBSCRIPT FOR ALL ARRAYS IN /CELLD/
C**** DATA ARE READ FROM A CARD TO SET DIMENSIONS TO IB2,JB2 AND NSPEC
C
LCM/CELLD/FL( 62, 32),U( 62, 32),V( 62, 32)
1 1),RHO( 62, 32),SIE( 62, 32),P( 62, 32)
2),MU( 62, 32),CSQ( 62, 32),RHOT( 62, 32),RHOV( 62
3, 32),RHOVT( 62, 32),RE( 62, 32),ETA( 62, 32),CO(
4 62, 32),FA( 62, 32, 7),RJ( 32),RJ2(
5 32),RFLB( 62),TFAB( 62, 7),TE( 62, 32)
1 DIMENSION RHOUT( 62, 32),RHOVT( 62, 32),PB(
1 62, 32),DRHO( 62, 7),STREB( 62)
1 EQUIVALENCE (RHOV,RHOUT),(RHOV,RHOVT),(P,PB),(STREB,RFLB),
1 (TFAB,DRHO)
1 INTEGER FL,CYCLE
1 REAL MU
1 JC=-1B2
3 1500 DO 1595 J=1,JB2
5 JC=JC+1B2
6 DO 1590 I=1,1B2
10 IJ=I+JC
11 IF(FL(IJ).EQ.1)GO TO 1590
15 IF(FL(IJ).GE.5)GO TO 1590
20 IPJ=IJ+1
21 IMJ=IJ-1
21 IJP=IJ+1B2
23 IJM=IJ-1B2
23 IF(IJ.EQ.1)GO TO 1510
25 IF(1.EQ.1)GO TO 1520
27 IF(1.EQ.1B2)GO TO 1530
30 IF(IJ.EQ.JB2)GO TO 1540
31 GO TO 1550
C*****BOTTOM ROW
32 1510 IF(FL(IJ).EQ.2)GO TO 1514
36 IF(FL(IJP).EQ.5)GO TO 1514
41 U(IJ)=-U(IJP) $ GO TO 1590

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RICEB 2691
RCOM2 2
RCOM2 3
RCOM2 4
RCOMP 4
RCOMP 4
RCOM2 7
RCOM2 8
RCOMP 9
RCOM2 11
RCOM2 12
RCOM2 13
RCOM2 14
RCOM2 15
RCOM2 16
RCOM2 17
RCOM2 18
RCOM2 19
RCOM2 20
RCOM2 21
RCOM2 22
RCOM2 23
RCOM2 24
RCOM2 25
RCOM2 26
RCOM2 27
RCOM2 28
RCOMP 29
RCOM2 30
RCOM2 31
RCOM2 32
RCOM2 33
RCOM2 34
RCOM2 35
RICEB 2693
RICEB 2694
RICEB 2695
RICEB 2696
RICEB 2697
RICEB 2698
RICEB 2699
RICEB 2700
RICEB 2701
RICEB 2702
RICEB 2703
RICEB 2704
RICEB 2705
RICEB 2706
RICEB 2707
RICEB 2708
RICEB 2709
RICEB 2710
RICEB 2711
RICEB 2712

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45	1514	U(IJ)=U(IJP) \$ GO TO 1590	RICE6	2713
		C*****FIRST COLUMN	RICE8	2714
52	1520	IF(J.EQ.JB2)GO TO 1540	RICE8	2715
54		IF(FL(IPJ).EQ.2)GO TO 1590	RICE8	2716
60		IF(FL(IPJ).EQ.3)GO TO 1590	RICE8	2717
63		IF(FL(IJP).EQ.5)GO TO 1590	RICE8	2718
66		IF(FL(IJ).EQ.2)GO TO 1524	RICE8	2719
72		V(IJ)=-V(IPJ) \$ GO TO 1590	RICE8	2720
75	1524	V(IJ)=V(IPJ) \$ GO TO 1590	RICE8	2721
		C*****LAST COLUMN	RICE8	2722
102	1530	IF(FL(IJ).NE.4)GO TO 1536	RICE8	2723
106		IF(FL(IJP).NE.4)GO TO 1590	RICE8	2724
111	1534	V(IJ)=V(IMJ) \$ GO TO 1590	RICE8	2725
116	1536	IF(FL(IJP).EQ.4)GO TO 1590	RICE8	2726
122		IF(FL(IJ).EQ.2)GO TO 1534	RICE8	2727
125		V(IJ)=-V(IMJ) \$ GO TO 1590	RICE8	2728
		C*****LAST ROW	RICE8	2729
131	1540	IF(FL(IPJ).EQ.5)GO TO 1590	RICE8	2730
135		IF(FL(IJ).EQ.2)GO TO 1544	RICE8	2731
140		U(IJ)=-U(IJM) \$ GO TO 1590	RICE8	2732
144	1544	U(IJ)=U(IJM) \$ GO TO 1590	RICE8	2733
		C*****REGULAR CELLS OF COMPUTING MESH (2,1B1) (2,JB2)*****	RICE8	2734
151	1550	IF(FL(IJ).EQ.4)GO TO 1590	RICE8	2735
155		IF(FL(IPJ).EQ.1)GO TO 1560	RICE8	2736
160		IF(FL(IMJ).EQ.1)GO TO 1570	RICE8	2737
163		IF(FL(IJP).EQ.1)GO TO 1580	RICE8	2738
166		IF(FL(IJM).NE.1)GO TO 1590	RICE8	2739
		C*****FL(IJ)=SOLID=2,3 AND FL(IJM)=FLUID=1	RICE8	2740
172		IF(FL(IPJ).EQ.1)GO TO 1590	RICE8	2741
175		IF(FL(IPJ).EQ.5)GO TO 1566	RICE8	2742
200		IF(FL(IPJ).GE.4)GO TO 1590	RICE8	2743
203	1553	IF(FL(IJ).EQ.2)GO TO 1554	RICE8	2744
207		U(IJ)=-U(IJM) \$ GO TO 1590	RICE8	2745
213	1554	U(IJ)=U(IJM) \$ GO TO 1590	RICE8	2746
220	1556	IF(U(IPJ).E.C.)GO TO 1590	RICE8	2747
223		GO TO 1553	RICE8	2748
		C*****FL(IJ)=SOLID=2,3 AND FL(IPJ)=FLUID=1	RICE8	2749
223	1560	IF(FL(IJP).EQ.1)GO TO 1590	RICE8	2750
227		IF(FL(IJP).GE.4)GO TO 1590	RICE8	2751
232		IF(FL(IJ).EQ.2)GO TO 1564	RICE8	2752
236		V(IJ)=-V(IPJ) \$ GO TO 1590	RICE8	2753
242	1564	V(IJ)=V(IPJ) \$ GO TO 1590	RICE8	2754
		C*****FL(IJ)=SOLID=2,3 AND FL(IMJ)=FLUID=1	RICE8	2755
247	1570	IF(FL(IJP).EQ.1)GO TO 1590	RICE8	2756
253		IF(FL(IJP).GE.4)GO TO 1590	RICE8	2757
256		IF(FL(IJ).EQ.2)GO TO 1574	RICE8	2758
262		V(IJ)=-V(IMJ) \$ GO TO 1590	RICE8	2759
266	1574	V(IJ)=V(IMJ) \$ GO TO 1590	RICE8	2760
		C*****FL(IJ)=SOLID=2,3 AND FL(IJP)=FLUID=1	RICE8	2761
273	1580	IF(FL(IPJ).EQ.1)GO TO 1590	RICE8	2762
277		IF(FL(IPJ).EQ.5)GO TO 1566	RICE8	2763
302		IF(FL(IPJ).GE.4)GO TO 1590	RICE8	2764
305	1583	IF(FL(IJ).EQ.2)GO TO 1584	RICE8	2765
311		U(IJ)=-U(IJP) \$ GO TO 1590	RICE8	2766
315	1584	U(IJ)=U(IJP) \$ GO TO 1590	RICE8	2767

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322	1586	IF (UTIPJ).EQ.0, GO TO 1590	RICE8	2768
325		GO TO 1583	RICE8	2769
325	1590	CONTINUE	RICE8	2770
330	1595	CONTINUE	RICE8	2771
332		RETURN & END	RICE8	2772